

Cite this: *Energy Environ. Sci.*,  
2025, **18**, 7373

# Monitoring chemical processes in redox flow batteries employing *in situ* and *in operando* analyses†

Ahmad Alem,<sup>a</sup> Pooria Poormehrabi,<sup>b</sup> Jonas Lins,<sup>c</sup> Lukas Pachernegg-Mair,<sup>id</sup><sup>de</sup>  
Christine Bandl,<sup>a</sup> Virginia Ruiz,<sup>id</sup><sup>fg</sup> Edgar Ventosa,<sup>id</sup><sup>fg</sup> Stefan Spirk<sup>id</sup><sup>\*de</sup> and  
Torsten Gutmann<sup>id</sup><sup>\*c</sup>

Redox flow batteries (RFBs) are promising solutions for large-scale stationary energy storage due to their scalability and long cycle life. The efficient operation of RFBs requires a thorough understanding of the complex electrochemical processes occurring during charging and discharging. This review provides an overview and perspective of *in situ* and *in operando* analytical techniques to monitor RFBs. In more detail, these advanced techniques allow for real-time observation of redox reactions, ion transport, and electrode–electrolyte interactions under working conditions, offering insights into formation of intermediate species and mechanisms of electrolyte degradation, State-of-Charge (SoC), and ion crossover. By discussing the principles, capabilities, and limitations of techniques such as nuclear magnetic resonance (NMR), electron paramagnetic resonance (EPR), ultraviolet-visible (UV-vis) spectroscopy, Raman spectroscopy, Fourier transform infrared spectroscopy (FTIR), X-ray absorption spectroscopy (XAS), electrochemical impedance spectroscopy (EIS), tomography and radiography, mass spectrometry (MS), and fluorescence microscopy this review highlights the essential role of *in situ* and *in operando* approaches in advancing RFB technology.

Received 5th March 2025,  
Accepted 2nd June 2025

DOI: 10.1039/d5ee01311a

rsc.li/ees

## Broader context

The review addresses one of the most critical issues in the development of redox flow batteries (RFBs), namely the need to understand the complex processes occurring in the solution, at the interface, and within the bulk of flow battery components. Its goal is to identify and summarize the ongoing challenges in the field that hinder the widespread adoption of RFBs in large-scale commercial energy storage applications. The review primarily focuses on *in operando* and *in situ* studies of RFBs, placing them in a broader context that includes other battery systems, such as lithium batteries and beyond. To the best of our knowledge, there are currently no such comprehensive overviews available on *in situ* and *in operando* techniques. Therefore, we believe that our review makes a significant contribution to the development of methodologies for *in situ* and *in operando* approaches in electrochemical storage and conversion systems, extending even to areas not explicitly covered in this work such as fuel cell technology.

## 1. Introduction

RFBs represent an energy storage technology that utilizes liquid electrolytes in large tanks to store electricity generated from intermittent renewable energy sources like solar, wind, and tidal power as well as providing backup energy for industrial applications.<sup>1–3</sup> In contrast to traditional lithium-ion batteries (LIBs), storage capacity and power output are independent in RFBs, making them ideal for medium to large-scale stationary energy storage applications, which demand scalability and flexibility.<sup>4,5</sup> Moreover, RFBs are supposed to have a longer lifespan than traditional batteries and feature long discharge times (12 hours and more), making them suitable for long-duration energy storage applications in microgrids and large-

<sup>a</sup> Institute of Chemistry of Polymeric Materials, Technical University of Leoben, Otto Glöckel-Strasse 2, A-8700 Leoben, Austria

<sup>b</sup> Flow-Nano S.r.l, Milano, Italy

<sup>c</sup> Institute of Inorganic and Physical Chemistry, Technical University of Darmstadt, Peter-Grünberg-Straße 8, D-64287 Darmstadt, Germany.

E-mail: gutmann@chemie.tu-darmstadt.de

<sup>d</sup> Institute of Bioproducts and Paper Technology (BPTI), Graz University of Technology, Inffeldgasse 23, A-8010 Graz, Austria. E-mail: stefan.spirk@tugraz.at

<sup>e</sup> Ecolyte GmbH Puchstraße 17, A-8020 Graz, Austria

<sup>f</sup> International Research Centre in Critical Raw Materials-ICCRAM, University of Burgos, Plaza Misael Bañuelos s/n, E-09001 Burgos, Spain

<sup>g</sup> Department of Chemistry, University of Burgos, Plaza Misael Bañuelos s/n, E-09001 Burgos, Spain

† This work is dedicated to Prof. Wolfgang Kern, who passed away during the preparation of this work.



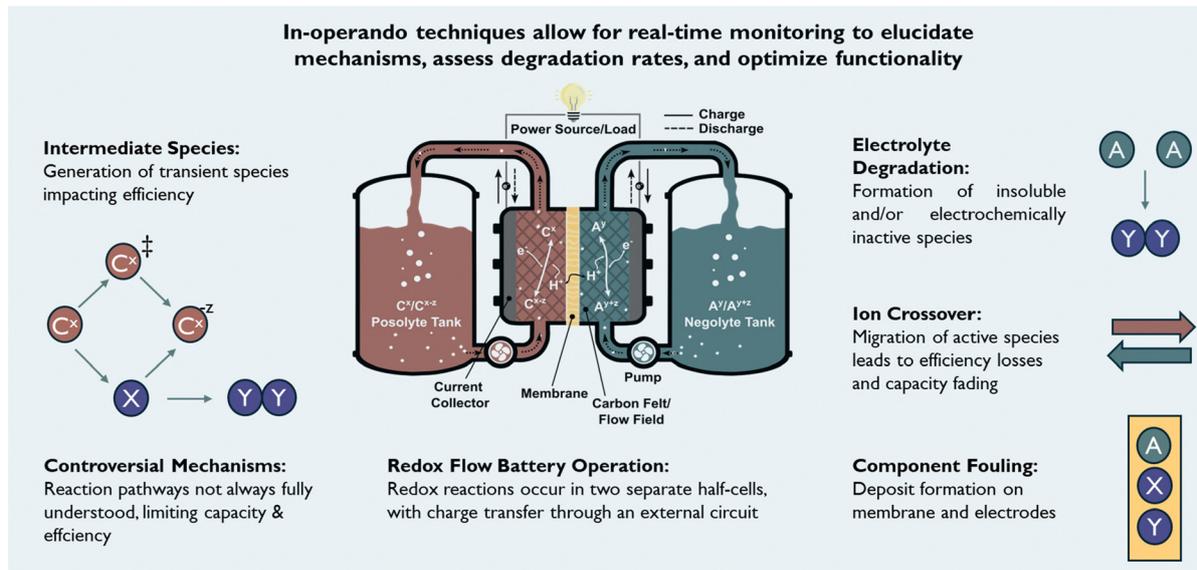
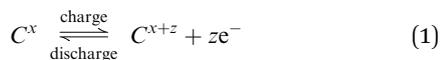


Fig. 1 Overview on challenges in progressing flow battery technology, which can be tackled by *in operando* monitoring.

scale energy storage.<sup>6</sup> Fig. 1 (middle) illustrates the working principle of RFBs, in which dissolved electro-active materials stored in external electrolyte reservoirs, referred to as catholyte (or posolyte) on the positive side and anolyte (or negolyte) on the negative side. During charge and discharge the liquid electrolyte is circulated into the electrochemical cell compartment, where redox reactions take place at the electrode surfaces, allowing for the direct conversion of chemical and electrical energy.<sup>7</sup> General cell charging/discharging reactions consisting of two half-cell reactions can be written as follows:

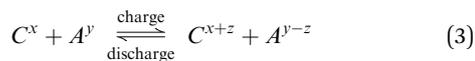
Cathode:



Anode:



Cell:



Various types of RFBs have been developed, typically sorted by their different chemistries, including all-vanadium,<sup>8</sup> zinc-bromine,<sup>9</sup> hydrogen-bromine,<sup>10</sup> all-iron,<sup>11</sup> semi-solid lithium,<sup>12</sup> all-copper,<sup>13</sup> zinc-polyiodide,<sup>14</sup> organic,<sup>4</sup> polymer,<sup>15</sup> zinc-cerium,<sup>16</sup> combined flow battery with solar energy,<sup>3</sup> and other non-aqueous systems. Enhancing cell performance across various chemistries is crucial for a broader application of the technology. However, this effort is challenged by several factors such as the low solubility of active materials in electrolytes, the limited electrochemical window of aqueous electrolytes, environmental sensitivity, limited electrolyte stability, and side reactions.<sup>7</sup> These restrict the energy density, efficiency, and lifespan of the cells and subsequently the whole battery. Redox-

mediated flow batteries (RMFBs) offer a promising solution to address challenges such as low solubility and the constrained electrochemical window of active species.<sup>8</sup> In RMFBs, soluble redox mediators facilitate electron transfer between electrodes and active species, thereby enabling enhanced energy densities.<sup>9,10</sup> While *ex situ post-mortem* analysis of RFBs rely on widely available techniques such as FTIR spectroscopy, Raman, X-ray photoelectron spectroscopy (XPS), X-ray diffraction, NMR, *etc.*, this characterization approach often produces misleading results due to relaxation effects, as applied electrical potentials affect thermodynamic and kinetic pathways. Additionally, *ex situ* characterization of active substances is challenging, caused by the high reactivity, sensitivity to sample preparation, and short lifetimes of certain oxidized and/or reduced redox-active molecules and ions within the electrolytes. Despite the necessity of profound analyses of RFBs as a part of examining new chemistries, critical questions at the molecular level remain open. This gap has driven significant efforts toward developing advanced and highly specialized characterization techniques that measure properties in real-time and under working conditions, known as *in situ* and *in operando* analyses.<sup>19</sup> These are particularly valuable as they allow monitoring of the battery's state-of-health (SoH) during operation, enabling the development of strategies to mitigate degradation, enhance the lifetime of the batteries and minimizing the error prone to sample preparation necessary for *ex situ* analyses.<sup>20</sup> Designing tools for *in situ* and *in operando* analyses is complex, as real-time monitoring requires integrating instruments into the confined space of a working cell. This integration necessitates special measures to ensure compatibility with environmental conditions such as pH, temperature, and humidity. The results from *in situ* and *in operando* analyses are more reliable than those from *ex situ post-mortem* ones, as they offer a more accurate representation of the actual conditions and dynamics of the system, minimizing the risk of



artifacts introduced during sample preparation or *post-mortem* analysis. *In situ* and *in operando* techniques also enable the identification and characterization of reaction intermediates, which are formed either by redox processes that proceed *via* different oxidation states of the anolyte/catholyte, by chemical or electrochemical reaction of compounds in the anolyte/catholyte or by electrochemical combustion of anolyte/catholyte. These intermediates are often challenging to capture in *ex situ* analyses, where they may decompose or transform during sample preparation. By preserving the integrity of the system and analyzing the sample in its natural state, *in situ* and *in operando* analyses provide crucial insights that are otherwise difficult to obtain.

### 1.1. State of the art of *in situ* and *in operando* analyses of batteries

A variety of advanced diagnostic tools have been developed and extensively used for LIBs, enhancing our understanding of their behavior.<sup>11–13</sup> In general, one can distinguish between five types of *in situ* and *in operando* analytics, namely electrochemical techniques (cyclic voltammetry (CV), EIS), spectroscopy (*e.g.* Raman, UV-vis, NMR and EPR), scattering techniques (*e.g.* X-ray scattering, neutron scattering) as well as imaging and microscopic approaches (*e.g.* electron microscopy, computer tomography, radiography).<sup>14</sup> As an example, imaging techniques for observing reaction front movement and reaction kinetics are increasingly applied, with *in situ* high-resolution transmission electron microscopy providing deep insights into interfacial processes.<sup>15</sup> Recent advancements in synchrotron methodologies have facilitated a variety of spectroscopic techniques, two-dimensional transmission X-ray microscopy, three-dimensional tomographic reconstructions, and diffraction-based imaging methods.<sup>16,17</sup> EPR imaging has been employed to monitor lithiation front displacement within paramagnetic electrodes during battery cycling, aiding in a better understanding of electrode behavior.<sup>18</sup> Furthermore, *in operando* spectroscopy techniques such as Raman spectroscopy, UV-vis spectroscopy, FTIR spectroscopy, and MS have been utilized to study processes and phenomena occurring in electrolytes and electrodes.<sup>19–22</sup> Finally, also techniques such as XPS, neutron diffraction, NMR, optical microscopy, scanning electron microscopy, atomic force microscopy, XAS, and magnetic resonance imaging (MRI) have been employed.<sup>23–29</sup> While these techniques were mostly developed for LIBs, they are now being adapted to study RFBs,<sup>30–34</sup> which face similar challenges related to electrochemical processes and degradation.

### 1.2. Problem statement, motivation and scope

All-vanadium redox flow batteries (VRFBs) are the most developed RFBs and currently used in large scale energy storage.<sup>33,35</sup> There are some detailed investigations concerning the effects of temperature on the stability of vanadium electrolytes, particularly on the formation of insoluble products such as  $VSO_4$ ,  $V_2(SO_4)_3 \cdot xH_2SO_4 \cdot yH_2O$ ,  $VOSO_4$  and  $V_2O_5$ .<sup>36,37</sup> However, there is still a lack of data that address processes at the interfaces and of suitable models describing the degradation of electrodes,

electrolytes and capacity fade due to factors such as unwanted side reactions and pH change, especially at high current densities and high states of charge, as well as the crossover of active species through the membrane, leading to reactions with species on the opposite side.<sup>46</sup> As crossover is dependent on the operation of the RFB *e.g.*, current density, and other factors such as the state of charge (SoC), it is important to monitor and optimize the operation to minimize crossover.<sup>38</sup> However, getting experimental data is non-trivial and requires *in situ* and *in operando* measurements as well as deep understanding of the chemical reactions and side-reactions.

Information considering the whole RFB system is even more scarce when it comes to less investigated complex chemistries such as in Fe, Mn, Cu, and organic RFBs.<sup>47–49</sup> For organic RFBs, the challenges are even harder as the involved chemistries and reactions vary to a large extent, which are additionally influenced by complex inter-species reactions triggered by crossover. However, the main decomposition mechanisms involve geminal diol formation & subsequent Michael addition reactions, nucleophilic substitutions, hydrolysis, disproportionation, dimerization, and tautomerization (Fig. 2), which have been extensively reviewed in the literature.<sup>39</sup>

The sheer diversity of reactions leads to a larger need for understanding on the one hand the complex chemistries itself but also how they are affected by the components (felts, membranes, electrode) and the variation in operation conditions (*e.g.* current density, state of charge). As organic flow batteries have attracted a significant amount of interest in the past years, we summarize the main chemistries in Section 1.2.1.

**1.2.1. Reactions of organic redox active molecules in flow batteries.** Basically, nucleophilic addition or substitution is a prevalent mode of chemical decomposition for aqueous RFB reactants, with various computational studies investigating their thermodynamic vulnerability to such reactions. This process involves a nucleophilic species—like water, hydroxyl/hydroperoxide anions, or reduced redox-active species—reacting with an electron-deficient redox-active species, usually the oxidized form of an organic redox couple.<sup>40</sup> During the reaction, the nucleophile may irreversibly replace a good leaving group attached to the molecule or attach to an unsubstituted position, leading to a loss of redox activity or a significant decrease in the reactant's reduction potential and solubility. The likelihood of nucleophilic attack increases with greater Lewis basicity of the nucleophile or acidity of the substrate, which was demonstrated in a benchmark study involving more than 100 000 compounds including benzene, naphthalene, anthracene, phenanthrene, and tetracene-based quinone-hydroquinone couples.<sup>41</sup> Nucleophilic reactions are also responsible for the accelerated degradation of *N*-substituted viologen derivatives in the presence of traces of oxygen in the anolyte. Nucleophilic attack by hydroxide anions generated by the oxygen reduction leads to cleavage of the *N*-substituent and dealkylation of the viologen derivative.<sup>42</sup> Dealkylation through a nucleophilic attack is the main degradation pathway of viologen derivatives in the presence of oxygen, leading to a significant decrease in the capacity of the RFB. Thus, it has been demonstrated that stability



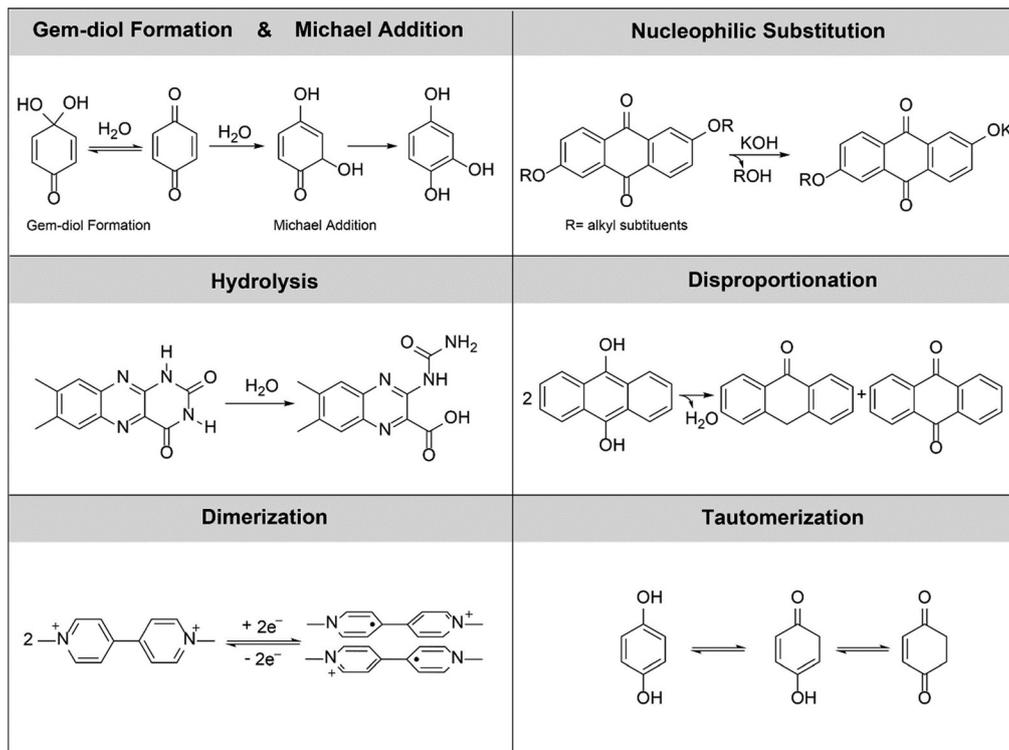


Fig. 2 Decomposition mechanisms of main organic redox active materials.<sup>39</sup> Reproduced with permission. Copyright 2020, ACS Publication.

can be improved in molecularly engineered viologen derivatives by hindering nucleophilic attack.<sup>43</sup>

Nucleophilic reactions also occur in high-potential substrates beyond quinones, including nitroxide radicals and organometallic complexes such as ferrocene (Fc) and ferrocyanide. Nitroxide radicals, for instance, possess reduction potentials around 0.8 V vs. standard hydrogen electrode (SHE), while ferrocene and ferrocyanide have reduction potentials ranging from approximately 0.4 to 0.6 V. A specific example involves the electrochemical oxidation of 4-hydroxy-(2,2,6,6-tetramethylpiperidin-1-yl)oxyl (4-HO-TEMPO), which produces 4-HO-TEMPO<sup>+</sup>. In alkaline electrolyte, this species is highly susceptible to nucleophilic addition by hydroxide ions (OH<sup>-</sup>), which leads to progressive acidification of the electrolyte. Under acidic conditions, 4-HO-TEMPO undergoes disproportionation to form 4-HO-TEMPO<sup>+</sup> and 1,4-dihydroxy-2,2,6,6-tetramethylpiperidine, with the latter being redox-inactive.<sup>44</sup>

Furthermore, the electrochemical oxidation of ferrocene and ferrocyanide yields Fc<sup>+</sup> and ferricyanide, respectively, both of which are also vulnerable to nucleophilic attack by OH<sup>-</sup>.<sup>45</sup> For Fc<sup>+</sup>, nucleophilic substitution can still occur despite the presence of protective alkyl substituents, especially when such groups are in proximity to the Fc redox center. An example of this is seen with (ferrocenylmethyl)-trimethylammonium salts, where nucleophilic substitution of the quaternary ammonium group results in the loss of trimethylamine as a leaving group.<sup>44</sup>

Disproportionation of certain redox couples can trigger chemical decomposition in redox flow batteries (RFBs). This process occurs when two identical species with the same

oxidation state undergo a redox reaction, resulting in one being reduced and the other oxidized, producing two products with different oxidation states. Capacity fade in RFBs can arise if either product is redox-inactive or has low solubility, leading to precipitation. Additionally, if one product has a significant different redox potential or similar potential but slower kinetics, this may also contribute to capacity fading during specific cycling conditions. Quinones are especially prone to disproportionation; for instance, anthrahydroquinone has been shown to disproportionate to anthrone and anthraquinone during the electrochemical reduction of unsubstituted anthraquinone in highly acidic media. The reduced form of viologen derivatives (the radical cation Vi<sup>•+</sup>) can also undergo disproportionation (2Vi<sup>•+</sup> → Vi<sup>2+</sup> + Vi<sup>0</sup>) yielding inactive neutral species that lead to capacity fading. Moreover, the radical cation of viologens can also dimerize to form inactive π-dimers, which reduces the effective concentration of active species.<sup>46</sup> Dimerization can be prevented by structural modification of viologens with charged and bulky substituents to induce electrostatic repulsion and steric interactions. Tautomerization involves the formal migration of a hydrogen atom alongside the exchange between a single bond and an adjacent double bond, all while maintaining the same carbon skeleton. Tautomers typically exhibit different thermochemical properties compared to their original molecules. If these tautomers possess significantly higher reduction potentials or lower solubilities, their formation during electrochemical cycling can lead to capacity fading and a decrease in cell energy density. Aza-substituted conjugated π-systems, such as those based on quinones, viologens, and phenazines, are particularly



prone to tautomerization during electrochemical cycling.<sup>47</sup> This susceptibility arises because the redox reactions of these organic molecules involve the reorganization of conjugated double bonds, where a tautomer may act as a metastable intermediate. In contrast, simpler aromatic molecules, like phenols, primarily exist in their enolic form, as the energy gained from rearranging to the tautomeric keto structure is outweighed by a significant reduction in resonance energy. Ketonic tautomeric structures become energetically favorable in compounds such as naphthoquinones, polyhydric phenols, and hydroxyl derivatives of polycyclic aromatic hydrocarbons. Understanding the susceptibility of different classes of aqueous organic species to these decomposition mechanisms is essential for developing molecular engineering strategies aimed at enhancing the stability of RFB reactants. It is also crucial to recognize that decay rates can increase with reactant concentration for certain chemistries, particularly those that are vulnerable to bimolecular decomposition pathways like disproportionation and dimerization. Since practical RFBs ideally operate at high reactant concentrations to maximize energy densities, it is vital to comprehensively understand the trade-off between energy density and stability.

However, there are still many unresolved mechanistic questions on the behavior of even popular redox active materials such as AQDS. In particular, there is some uncertainty regarding whether AQDS can fully access its theoretical two-electron Coulombic capacity.<sup>48</sup> Based on nuclear magnetic resonance (NMR), cyclic voltammetry (CV), and bulk electrolysis (BE) measurements, it has been suggested that reversible intermolecular dimerization of AQDS occurs at solution concentrations exceeding 10 mM, thereby inhibiting complete two-electron electrochemical reduction or reduction *via* chemical oxidants.<sup>49,50</sup> On the basis of these works, it has been speculated that CO<sub>2</sub> binds in a 1:1 anthraquinone–CO<sub>2</sub> adduct within bulk AQDS powder. When dissolved in acidic electrolyte, this AQDS–CO<sub>2</sub> adduct would undergo hydrolysis, leading to the formation of semianthraquinone, which could subsequently dimerize into semianthraquinone–anthraquinone units, yielding an overall Coulombic capacity of 1.5 electrons per AQDS molecule. In neutral to basic pH conditions, they anticipate the formation of hydroxyanthraquinone–anthraquinone dimers, resulting in a net capacity of one electron per AQDS molecule. However, the universality of this capacity-limiting mechanism is questionable, as Chen *et al.*<sup>51</sup> demonstrated that more than 95% of the theoretical capacity of AQDS was accessible in an acidic AQDS/bromine cell. This high capacity is supported by multiple reports of AQDS or anthraquinone-based chemistries at different conditions, where electrochemical access to 90% or more of the full two-electron Coulombic capacity has been observed.<sup>52–54</sup> Several studies have investigated the use of AQDS and its derivatives in full cells to analyze the current–voltage relationships in RFBs, partition voltage losses within the full cell stack, and assess the feasibility of integrating RFBs with solar cell charging systems. However, aside from contributions from bromine crossover, the origins of capacity fade in AQDS/bromine cells remain inadequately explored. Hypotheses regarding this issue include the hydroxylation and disproportionation of the

reduced anthrahydroquinone into anthraquinone and redox-inactive anthrone. Another illustrative example involves TEMPO related chemistry. As mentioned above, TEMPO and its derivatives can undergo a wide range of reactions by reaction with *e.g.* Lewis acids to the oxonium derivatives, even without applying a potential. The decomposition of TEMPO derivatives typically involves ring opening and rearrangement reactions, which occur also simultaneously. Often the main degradation products are identified or even only proposed as shown for the example of TMA–TEMPO (TMA: trimethylammonium). This molecule can decompose by a variety of pathways, including ring opening and rearrangements, finally leading to the formation of CO<sub>2</sub> (Fig. 3).<sup>55</sup>

Although the nitroxide can adopt many different mesomeric structures, for decomposition typically it is assumed that decomposition proceeds *via* the oxidized state.

**1.2.2. Methods for *in situ* and *in operando* characterization.** The example of TEMPO and anthraquinone based systems, among the most popular ones in organic flow battery research, shows the difficulty to find the origins of capacity fading in full cells. This lack of deep understanding of processes and phenomena occurring at atomic and nanoscale level of redox flow batteries' components is, however, impeding progress. Recently, a few publications reported the *in situ* and *in operando* analyses of RFB systems shedding light on some of these mechanisms.<sup>50–53</sup> For example, on-line MS<sup>57</sup> allows for investigating the electrochemical corrosion of the graphite electrode. X-ray tomography of the electrode,<sup>55</sup> acoustic attenuation coefficient analysis,<sup>52</sup> EPR and MRI<sup>56</sup> have provided insights into morphological features on different length scales. UV-vis spectroscopy of the electrolyte solutions can be used to monitor the SoC of the battery, while NMR spectroscopy allows to analyze the electrolyte composition, to recognize intermediate species and to observe potential degradation products formed during cycling (for an overview on the different techniques see already Table 1). In the following, we will provide a comprehensive review of the mentioned techniques and discuss them in the context of different chemistries. There is a notable scarcity of comprehensive reviews on this topic, whereas there are several review papers on lithium-ion, lithium sulfur and all-solid-state battery technology.<sup>33–37,57</sup> This gap highlights the need for a more extensive examination of the existing methodologies and findings in this field. Addressing this deficiency will not only enhance our understanding of the complex processes involved but also facilitate future advancements in related research areas.

A challenge in the design of *in operando* measurement setups lies also in the design of the flow cells. In some applications, there are restrictions in size and/or how to place or connect the flow battery cells to the respective instruments. In addition, challenges in material selection may be overcome, as some of the conventional cells are made of metal which is *e.g.* impeding any investigation using X-rays. The time scales of the electrochemical processes and the sensitivity of the methods need to match the ability of some measurements to capture transient phenomena accurately. For imaging techniques, the required resolution must be kept in mind: While maintaining



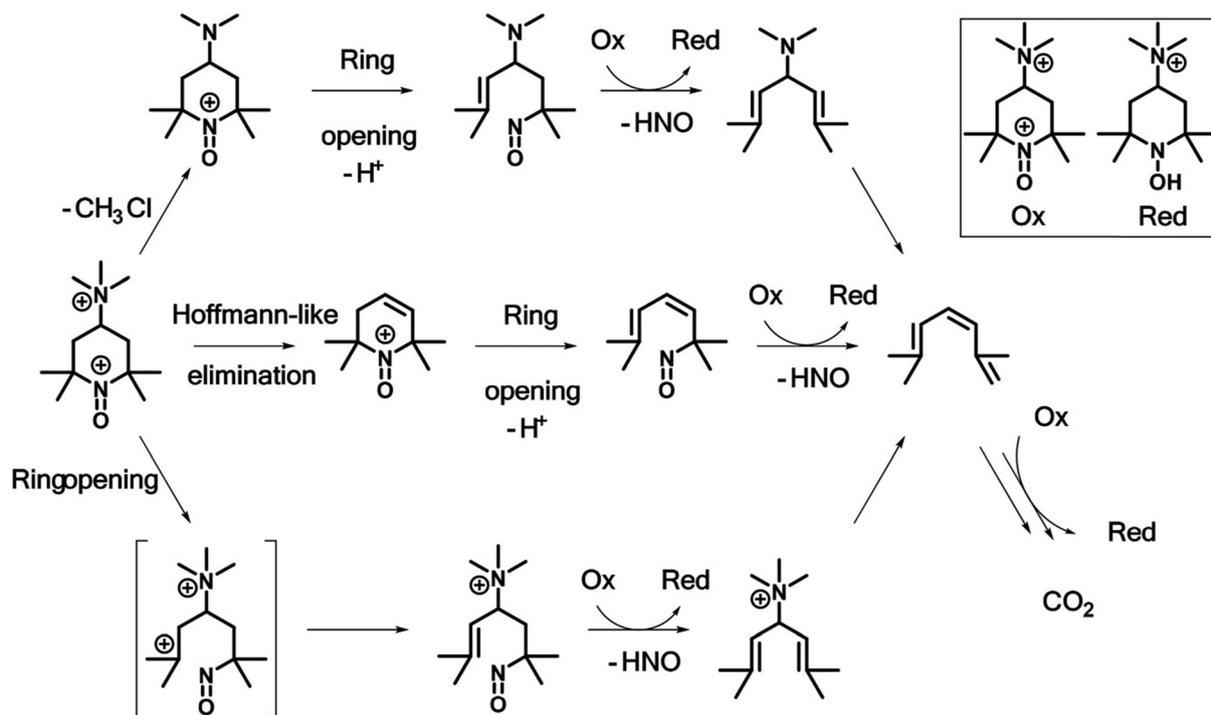


Fig. 3 Proposed decomposition pathways of TMA-TEMPO towards carbon dioxide.<sup>56</sup> Reproduced with permission. Copyright 2022, Elsevier Publication.

the same environmental conditions is trivial in lab scale single cells, for *in operando* setups, control over temperature or other parameters can be tricky. As experimental *in operando* setups may have some peculiarities on cell design and operating conditions (*e.g.* flow rate, flow channels, tubing), the results may not be always completely comparable to standard cells. In the next section, we discuss the different techniques and setups.

### 1.3. *In situ* and *in operando* NMR spectroscopy

NMR spectroscopy has been widely used for several decades to identify the structure of organic and inorganic molecules. The introduction of the concept of flow-NMR spectroscopy has enabled various novel applications in recent years.<sup>77–79</sup> As for example, it has been successfully established in reaction monitoring,<sup>80–82</sup> in quantitative analysis,<sup>83–85</sup> in combinatorial chemistry,<sup>86</sup> liquid chromatography,<sup>87</sup> and in hyperpolarization (*i.e.* PHIP or DNP).<sup>88,89</sup> Moreover, it has also been applied in heterogeneous (electro)catalysis research.<sup>90</sup>

In the past few years, it has been established as a powerful tool for analyzing electrochemical processes in RFBs on a molecular level. It allows to identify redox-active species and molecular structures of electrolytes and provides information on their concentrations. By tracking changes in the molecules/species involved in the electrochemical processes the kinetics and mechanisms of these reactions can be understood, which is one key step to optimize the performance of RFBs in the future. The adaptation needed for the RFB systems is to attach the RFB single cell to a flow through system (see Fig. 4a, inset). A potential difference to normal cells is that the tubing diameters are smaller, which may lead to different flow profiles.

As an early example in that field, Stimming and co-workers<sup>58</sup> studied asymmetric polyoxometalate electrolytes in RFBs, focusing on  $[\text{PV}_{14}\text{O}_{42}]^{9-}$  ( $\text{PV}_{14}$ ) as catholyte. To assess the stability of this diamagnetic anion upon reduction and its role as an electron carrier, they conducted *in situ*  $^{51}\text{V}$  NMR studies. During the reduction a decrease in intensity of the three signals assigned to  $[\text{PV}_{14}\text{O}_{42}]^{9-}$  with time was obtained. This was interpreted as conversion of diamagnetic  $\text{PV}_{14}$  to paramagnetic  $\text{V}^{(\text{IV})}$  species, which are not visible in NMR. During oxidation, the signals were partially recovered, suggesting the formation of  $\text{PV}_{14}$ . However, the process was not quantitative since part of the species formed during reduction have diffused from the electrode, limiting the re-oxidation process.<sup>58</sup>

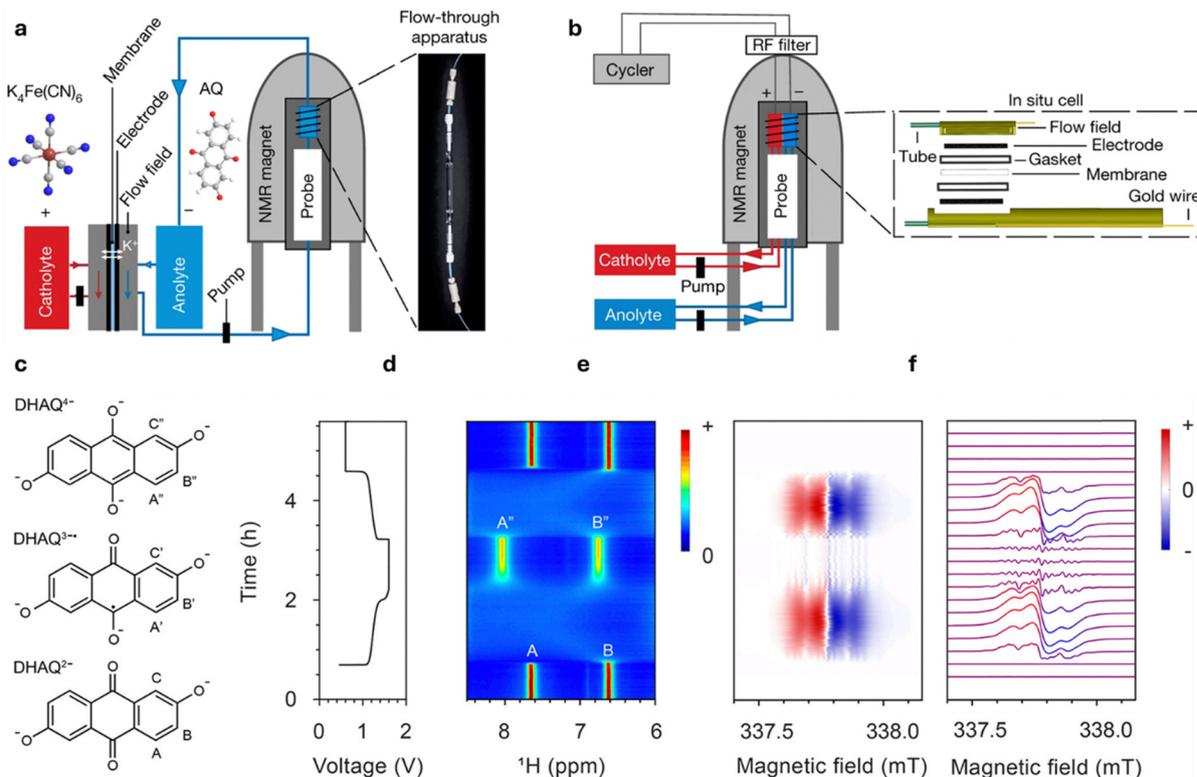
Next to this study, Zhao *et al.*<sup>59</sup> conducted a thorough NMR analysis to monitor the electrolyte properties in organic RFBs employing a combined *in situ* and *in operando* approach. In the *in situ* setup (Fig. 4a), the RFB was externally connected to an NMR probe with a flow cell, allowing high-resolution time-resolved spectra without interference from cell components. For *in operando* studies (Fig. 4b), a tiny flow battery system was positioned inside the NMR probe. Using this *in operando* mode, catholyte and anolyte can be investigated simultaneously, though with lower resolution due to signal interference from cell components.

In their *in situ* study Zhao *et al.*<sup>59</sup> used a full cell model containing 2,6-dihydroxyanthraquinone (DHAQ) as anolyte and potassium hexacyanoferrate(II) as catholyte and the  $^1\text{H}$  NMR spectra of the anolyte were monitored as function of applied voltage to quantify the SoC. Upon charging, two signals attributed to the protons close to the carbonyl redox center of DHAQ



Table 1 Summary of the role of the most developed *in situ* and *in operando* techniques for studying RFBs

Technique	Working principle	Application	Limitations	Ref.
NMR spectroscopy	Detection of nuclear spins and identification of their local environment; tracking of diamagnetic species	Monitoring the electrolyte decomposition and crossover of molecules; estimation of the SoC	Complexity of integrating the cell into the probe; no tracking of paramagnetic species feasible, limited sensitivity (typically $10^{17}$ nuclear spins are required)	58 and 59
EPR spectroscopy	Detection of unpaired electrons and their local environment; tracking of <i>para</i> -magnetic species	Monitoring radical species and electron transfer reactions; complementary technique to NMR	Complexity of integrating the cell into the probe; only tracking of paramagnetic species feasible	60 and 61
UV-vis spectroscopy	Measuring absorbance of UV-vis light absorbing active species; tracking changes in oxidation states during charge and discharge cycles	Real-time, non-invasive monitoring of SoC and total redox-active species concentration in half-cells; monitoring of redox stability in flow and static cells	Challenges for highly concentrated systems and light absorbing solvents; calibration complexity for industrial use	62 and 63
Raman spectroscopy	Probing bond-vibrations by Raman scattering	Monitoring of electrolyte composition/electrode surface/catalytic surface reactions; exploring origin of capacity fading, mechanisms of RFB failure	Sample heating; background noise by fluorescence; enhancement techniques (SERS/TERS) need calibration	64 and 65
FTIR spectroscopy	Probing bond-vibrations by infrared adsorption	Exploring mechanisms of electrochemical reactions in RFB and RMFB	Limited to IR-active species; complexity of the ATR-FTIR spectroelectrochemical setup	66 and 67
XAS	Probing element specific electron transitions through X-ray absorption/scattering	Monitoring structure and oxidation states of electrolytes and electrodes at surfaces/bulk	Requires special X-ray source ( <i>i.e.</i> synchrotron); beam strongly dampened by liquid layers; characterization of surfaces is challenging, requires advanced setups; limited to heavy atoms and thin sample layers; requires uniform, homogenous samples	68 and 69
EIS	Application of a sinusoidal signal over a wide range of frequencies; monitoring of the sinusoidal response of the system	Monitoring of RFB performance	Limited frequency range by equipment; low resolution at low frequencies	70 and 71
Tomography and radiography	X-rays or neutrons are utilized to generate high-resolution 3D images; monitoring internal structures and dynamic processes	Visualization of dendrite growth on electrode surface and quantification of dendrite characteristics; mapping concentration profiles across electrodes; studying electrodes under varying compression to optimize porosity and wetting behavior	Requiring advanced imaging setups ( <i>e.g.</i> synchrotron CT, neutron sources); difficulty in distinguishing phases ( <i>e.g.</i> electrolyte <i>vs.</i> felt) due to similar attenuation coefficients	72 and 73
MS	Measure mass-to-charge ratios of molecules	Characterize reaction products of parasitic reactions at electrodes; explore reaction products and intermediates during cycling in electrolytes	Costly and hard-to-implement online instrumentation (electrochemical MS system); custom-made sampling systems connected to the gas carrier flow; time delay between sampling and detection; compounds with identical molecular weights cannot be distinguished.	57 and 74
Fluorescence microscopy	Visualization of redox-dependent fluorescence to track redox reactions	Mapping redox-active species concentration and distribution; monitoring mass transport phenomena within porous electrodes	Requires fluorescent redox-active species; potential optical interference and fluorescence quenching by electrolyte salts.	75 and 76



**Fig. 4** (a) *In situ* and (b) *in operando* NMR setup designed for RFBs according to Zhao *et al.*<sup>59</sup> In the on-line setup (a), the battery comprises 5.0 cm<sup>2</sup> carbon felt electrodes, with a catholyte and an anolyte of potassium ferrocyanide(II) and AQ, respectively, dissolved in 1 M KOH in D<sub>2</sub>O. The volume of the flow path through the magnet including the sampling apparatus (7.3 cm<sup>3</sup>) and excluding the reservoir is 15.0 cm<sup>3</sup>. At a flow rate of 13.6 cm<sup>3</sup> min<sup>-1</sup>, the time of flight of the electrolyte out of and back into the reservoir is 1.1 min. In the operando setup (b), the miniaturized flow cell (shown on the right) consists of flow fields, tubes to flow electrolyte in and out, carbon electrodes, a cation-transport membrane and current collectors. The volume of the flow path including the cell cavity (0.032 cm<sup>3</sup>) is 7.8 cm<sup>3</sup>. At a flow rate of 2.5 cm<sup>3</sup> min<sup>-1</sup>, the time of flight of the electrolyte out of and back into the reservoir is 3.1 min. Reproduced with permission. Copyright 2020, Nature Publishing Group. RF, radiofrequency (c)–(f) *In situ* <sup>1</sup>H-NMR and EPR investigations performed during electrochemical cycling by the same group.<sup>61</sup> (c) Structures of the DHAQ<sup>2-</sup>, DHAQ<sup>3\*-</sup>, and DHAQ<sup>4-</sup> anions showing the labeling of the proton. (d) Voltage of a 10 mM DHAQ versus 15 mM K<sub>4</sub>[Fe(CN)<sub>6</sub>] and 3.75 mM K<sub>3</sub>[Fe(CN)<sub>6</sub>] full cell as a function of time. During charge, a constant current of 10 mA was applied, followed by a potential hold at 1.6 V. During discharge, a constant current of -10 mA (where the sign indicates the polarity of the electrodes) was applied, followed by a potential hold at 0.6 V. (e) NMR spectra of the anolyte in the aromatic region. The color bar (right) indicates the intensity of resonances in positive arbitrary units. The acquisition time per NMR spectrum is 95 s. (f) EPR spectra of the anolyte. The stack plot on the right shows every 10th spectrum. The acquisition time per EPR spectrum is 95 s, with a scanning time of 60 s, a coupling time of 30 s (time for automatic tuning), and a delay time of 5 s. Note that a typical continuous-wave EPR spectrum is detected and displayed as the first derivative of the absorption, and hence has negative and positive values. The color bar indicates the intensity of the resonance in arbitrary units. A different color scale is applied here because of the presence of negative peak intensities. Reproduced with permission. Copyright 2021, ACS Publication.

vanished instantly, while a signal attributed to the farthest proton from the redox center was broadened and shifted towards higher chemical shifts. This observation was interpreted by electron delocalization over the semiquinone radical anion, resulting in significant line broadening. By charging to higher voltages, the signal further shifted to higher ppm values and then moved back after reaching a maximum. At the cut-off voltage (1.7 V), signals were observed, assigned to DHAQ<sup>4-</sup> which is a diamagnetic product. Moreover, the *in situ* NMR was employed to monitor the electrolyte decomposition in the RFB. By holding the voltage at 1.7 V to ensure full reduction of DHAQ, several new peaks appeared, which were attributed to the decomposition products anthrone (DHA<sub>3</sub><sup>-</sup>) and anthrol (DHAL<sub>3</sub><sup>-</sup>). The quantity of these species was much smaller when the voltage was kept at 1.2 V. This clearly pointed out that the reduction potential influences the degradation of the

electrolyte. In addition to electrolyte degradation, *in situ* NMR enabled exploring battery self-discharge in real time.<sup>59</sup> Similarly, in another research, *in situ* NMR was used to track the transformation of the precursor compound 2,4,6,8-tetra-methylaminemethylene-1,5-naphthalenediol (TAND) to the active redox species 2,6,8-trimethylaminemethylene-3,5-dihydroxy-1,4-naphthoquinone (TANQ) during the electrochemical process.<sup>91</sup>

In a recent work, Zhao and co-workers<sup>92</sup> investigated DHAQ as anolyte and potassium hexacyanoferrate(II) as catholyte under *in situ* conditions with a low-cost benchtop NMR spectrometer (43 MHz, 1 T). Although this spectrometer has a much lower field compared to the formerly used high-field spectrometer (300 MHz, 7 T), <sup>1</sup>H NMR enabled them to identify and quantify intermediates with sufficient sensitivity, spectral and temporal resolution. Furthermore, they demonstrated the feasibility of their benchtop approach to investigate the crossover



of DHAQ and impurity molecules through the Nafion separator membrane. The crossover of molecules in RFBs may significantly impact battery performance, resulting in a potential capacity loss of up to 50% and should be thus excluded.<sup>92</sup>

Finally, significant progress in development of special probes for *in situ* NMR and MRI investigations of RFBs has been made by Berthault and co-workers.<sup>93</sup> By 3D printing, they designed a mini-RFB that was connected to a high field NMR probe and allowed to perform *in situ* NMR and imaging studies. As a proof of concept, they tested their equipment to study in real-time the redox cycle of the disodium salt of 9,10-anthraquinone-2,7-disulfonic acid (2,7 AQDS), revealing a crucial role of dimerization in electrolytes of organic RFBs.<sup>93</sup>

#### 1.4. NMR combined with *in situ* and *in operando* EPR spectroscopy

In some cases, redox processes in RFBs produce paramagnetic species, having unpaired electrons. When present in high concentrations, such radicals can limit the detection of NMR active species in electrolyte solutions. Therefore, it is necessary to employ a complementary analytical technique which provides time-resolved information on electron spins. *In situ* and *in operando* EPR spectroscopy is such a powerful tool to monitor paramagnetic species and has been widely used in catalysis, electrocatalysis as well as biochemical research as shown by several reviews.<sup>69–74</sup>

Recently, this technique has been increasingly employed to research energy storage systems, revealing information on charge transfer and storage processes.<sup>94–96</sup> Simultaneous electrochemical-EPR measurements provide insights into reaction intermediates, products, and reaction kinetics. For instance, Zhao *et al.*<sup>61</sup> reported on the development of a coupled NMR/EPR setup which was applied to investigate DHAQ in a DHAQ/K<sub>4</sub>Fe(CN)<sub>6</sub> full cell in a time window of 5 h at voltages of 0.6 to 1.6 V (Fig. 4d). They demonstrated that *in situ* EPR can be employed for quantifying the concentration of radical species formed as reaction intermediates during electrochemical cycling, while *in situ* NMR enabled to quantify concentration changes of diamagnetic species in parallel. As shown in Fig. 4e, when signals A and B disappear in the <sup>1</sup>H *in situ* NMR spectra because of the electron delocalization and intermolecular electron transfer, the *in situ* EPR spectra show a resonance at 337.78 mT, corresponding to the DHAQ<sup>3•-</sup> radical anion (Fig. 4f). As charging progresses, the EPR signal intensifies and broadens, reaching its maximum at 50% SoC. Thus, when NMR peaks disappear and provide limited information, EPR enables analyzing the radical species and the SoC.<sup>61</sup> In that paper, Zhao *et al.*<sup>97</sup> introduced an approach based on direct magnetic susceptibility measurements that allows the online *in situ* determination of the SoC which they applied on the DHAQ/K<sub>4</sub>Fe(CN)<sub>6</sub> full cell system.

In a follow-up work, Jing *et al.*<sup>60</sup> applied this NMR/EPR approach complemented with electrochemical analysis to investigate the mechanism of the recovery of DHAQ from its decomposition products 2,6-dihydroxy-anthranol (DHAL) and 2,6-dihydroxy-anthrone (DHA). This follows a two-step process,

namely (i) the oxidation of DHA(L)<sup>2-</sup> to the dimer (DHA)<sub>2</sub><sup>4-</sup>, and (ii) the oxidation of (DHA)<sub>2</sub><sup>4-</sup> to DHAQ<sup>2-</sup>.

Moreover, Jethwa *et al.*<sup>98</sup> used this NMR/EPR approach in combination with *in situ* UV-vis spectroscopy to study nitrogen-rich fused heteroaromatic quinones as promising candidates to be used in aqueous organic RFBs. As an interesting example, they investigated the electrochemical stability of the charged species during operation of a RFB containing 4,8-dioxo-4,8-dihydrobenzo[1,2-*d*:4,5-*d'*]bis([1,2,3]triazole)-1,5-diide as electrolyte, employing NMR/EPR to quantify formed species during electrochemical cycling.

Pyridinium derivatives represent another family of organic redox materials whose redox behavior has been probed by coupled *in operando* NMR and EPR spectroscopies under representative flow battery conditions.<sup>99</sup> The powerful combination of both *operando* techniques to track the performance of an extensive library of bipyridinium compounds over a range of potentials provided insights into the air tolerance of batteries containing these electrolytes. The techniques allowed identifying a correlation between the singlet-triplet free energy gap (intramolecular electron pairing) and the onset of capacity fade mechanisms. Capacity fade was linked to the reactivity of the free radical species, and  $\pi$ -dimerization is the key to suppress reactivity between these radicals and trace impurities such as dissolved oxygen.<sup>99</sup> The important findings allowed to propose strategies to mitigate capacity fade due to oxygen and stable pyridinium-based electrolytes for prolonged (days) cycling operation in air.

Combined *ex situ* NMR and *in situ* EPR characterization was also applied to investigate redox process intermediates and redox mechanisms in an aqueous organic RFB with fluorenone derivatives as anolytes.<sup>100</sup> By identifying the fluorenone radical anion intermediates during charging process, the authors proposed a possible reaction mechanism that entailed electrochemical reduction-oxidation reactions and accompanying dis- and comproportionation reactions in the charge-discharge process for the reversible ketone hydrogenation and alcohol dehydrogenation of molecularly-engineered fluorenone-based anolytes.

In a recent work, Zhang *et al.*<sup>101</sup> investigated methylene blue (MB) as catholyte in aqueous solution in a full cell. They utilized <sup>1</sup>H *in situ* NMR spectroscopy and *ex situ* EPR spectroscopy to explore the redox chemistry of MB. They observed high oxidation-stability of MB radicals generated by comproportionation as well as for reduced MB in the electrolyte solution, and identified the important role of this stability for the high reversibility of the redox chemistry of MB. All these examples clearly show the power of combined *in situ* NMR/EPR techniques to investigate the redox chemistry of organic molecules in RFBs under working conditions.

Another application of simple *in situ* EPR experiments, which are not combined with NMR spectroscopy, is the evaluation of vanadium crossover in real-time in a VRFB.<sup>102</sup> In that work, VO<sup>2+</sup> crossover through Nafion in a VRFB was monitored as a function of sulfuric acid concentration and VO<sup>2+</sup> concentration. In the experimental setup, a vanadium rich solution



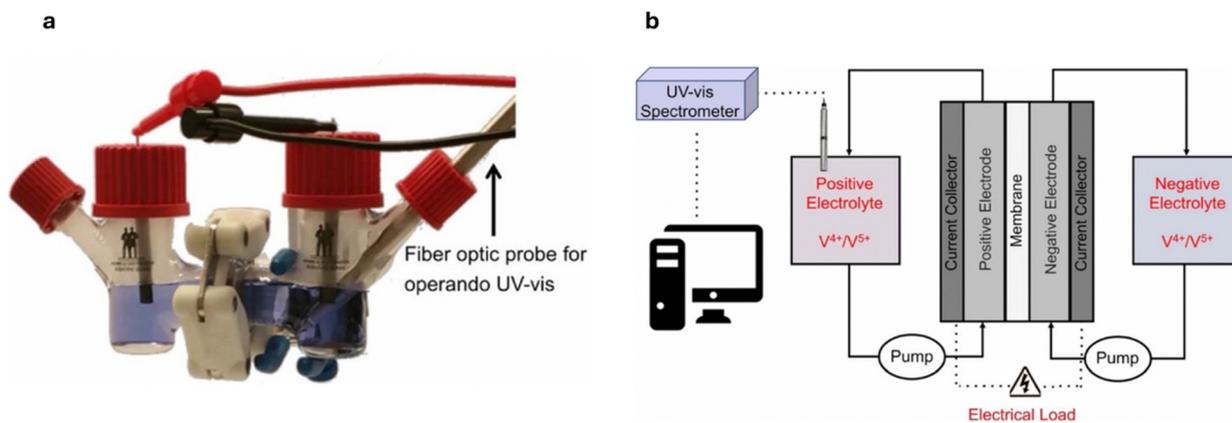


Fig. 5 Comparison of (a) an H-cell and (b) a setup where the battery is connected to a flow-through cuvette of an UV-vis spectrometer.<sup>62</sup> Reproduced with permission. Copyright 2019, IOP Science.

flowed through one side of the membrane of a permeation cell while a blank or vanadium deficient solution flowed on the other side. The blank flow solution was analyzed in an EPR cavity and the VO<sup>2+</sup> concentration was determined from the intensity of the EPR signal. Permeability values of VO<sup>2+</sup> ions across the membrane were analyzed at different temperatures to determine the effect of the viscosity of the flow solution on the permeability of the ion.<sup>102</sup>

### 1.5. *In situ* and *in operando* UV-vis spectroscopy

One significant limitation of RFBs is the loss of capacity over cycles, primarily due to ion and water crossover, hydrogen evolution, and inadequate mixing of electrolytes in the storage tanks. This leads to asymmetry in the electrolyte concentration and SoC between the positive and negative sides, resulting in charge imbalances. To address these issues effectively, real-time monitoring of both the total vanadium concentration and SoC in each half-cell is crucial. One approach to do this is to employ H-cells, as depicted in Fig. 5a. In that case, an optical fiber is inserted into the electrolyte solutions and the color change can be tracked. The advantage is that this setup is rather easy to assemble; a separate UV-vis apparatus is not needed. The disadvantage is that the kinetics and the efficiency of the battery may be compromised. The other option is to connect a flow battery to an UV-vis system and to pump the electrolyte solution through a flow-through cuvette (Fig. 5b), while continuously acquiring spectra, providing potentially a more precise determination of the SoC in a real battery.

In the cases where the color of electrolyte solutions significantly changes with the SoC as illustrated in Fig. 6a for vanadium species, UV-vis spectroscopy provides a direct and non-invasive method for analyzing the SoC.<sup>103</sup> This method serves as an advantageous alternative to the traditional open circuit voltage (OCV) measurements. Unlike OCV, which only offers a general SoC status for the VRFB system, UV-vis spectroscopy can determine the SoC of each individual electrolyte and provides information on the *e.g.*, total vanadium concentration. Optical sensing thus enhance VRFB performance monitoring by offering detailed insights into the processes governing

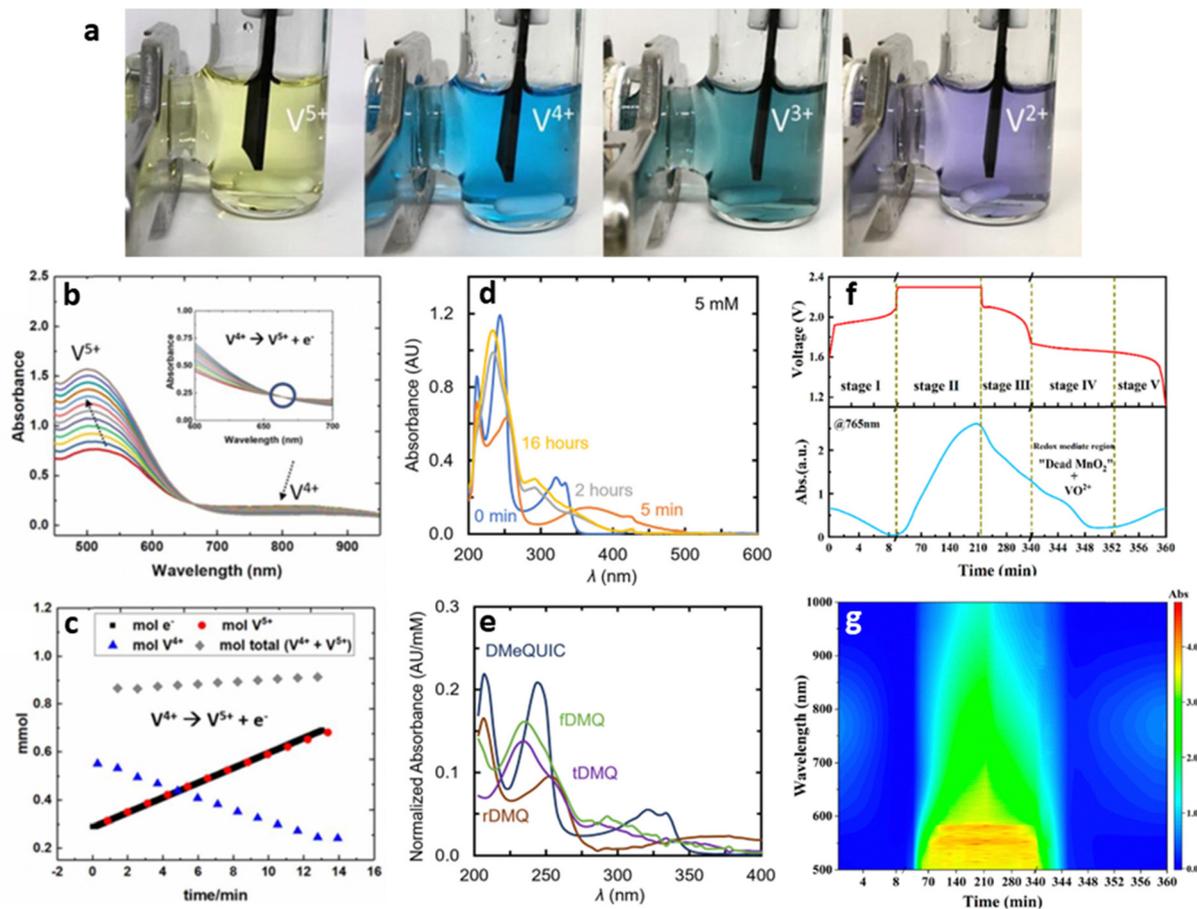
efficiency and capacity decay, facilitating optimal real-time readings and enabling advanced control strategies.<sup>103</sup> However, it is crucial to ensure the lack of electrolyte interference with the optical response of the electroactive species to deploy the full potential of UV-vis for quantitative analysis. In case of interference, contribution of the electrolyte solution to the total absorbance needs to be measured in a control experiment and subtracted.

In research conducted by Gokoglan *et al.*,<sup>62</sup> *in operando* UV-vis spectroscopy was used to monitor redox events and to quantify the concentration of redox species during battery cycling, demonstrating strong redox stability of the bioinspired redox-active material vanadium(IV/V) bis-hydroxyiminodiacetate (VBH), highlighting smooth transitions between vanadium(IV) and vanadium(V) species in non-aqueous VRFBs. *In operando* UV-vis spectroscopy also allowed for quantitative tracking of each species in real-time, offering a simple method of SoC monitoring in VRFBs.<sup>84</sup> Notably, Fig. 6b and c shows no signs of decomposition or irreversible side reactions in an operational flow cell at 10 mA cm<sup>-2</sup>. Furthermore, the data reveals a clear relationship between the change of the number of moles of electrons and of vanadium species, with their respective slopes showing a clear correlation.

In UV-vis spectroscopy, high vanadium concentration in the electrolyte often fails to follow Lambert-Beer's law, resulting in a low signal-to-noise ratio. Kyung-Hee *et al.*<sup>63</sup> developed a straightforward method for real-time SoC monitoring of VRFB systems by UV-vis spectroscopy *in operando* mode that consisted in using cuvette windows with thin path lengths (below 0.1 mm) and a concept of difference absorbance. This approach is practical for large-scale engineering applications as well in which high vanadium concentrations (*e.g.*, 2 M in 3 M sulfuric acid) without dilution are used.<sup>63</sup>

Despite extensive research, a critical question remains: How can UV-vis spectroscopy independently measure both the total vanadium concentration and SoC of both electrolytes in a VRFB, and with what accuracy? Existing literature often focused on specific electrolytes and lacked comprehensive analysis. Calibrations only provided SoC, ignoring the total vanadium





**Fig. 6** (a) H-cell experiments. During electrolytic reduction of a vanadium solution with a concentration of 0.04 M, the solution undergoes a series of color changes. Initially, the solution appears yellow due to the presence of  $V^{5+}$  ions. As the reduction process progresses, the color transitions from yellow to blue ( $V^{4+}$ ), then to green ( $V^{3+}$ ), and finally to purple ( $V^{2+}$ ).<sup>104</sup> Reproduced with permission. Copyright 2019, IOP Science. Flow-cell spectroelectrochemistry showing the decrease in the features associated with VBH in vanadium(iv) oxidation state and growth of the feature associated with VBH in vanadium(v) oxidation state, (b) measured during the discharge to 40% SoC, and (c) plot of the change of the number of moles of reduced, oxidized and total VBH (blue, red and gray data points, respectively) present during oxidation, obtained using UV-vis data at 485 and 825 nm, respectively, and for comparison the number of moles of electrons removed electrochemically (black line).<sup>62</sup> Reproduced with permission. Copyright 2019, IOP Science. (d) UV-vis spectra of 5 mM DMeQUIC after 0 min, 5 min, 2 h, and 16 h of potentiostatic reduction in a DMeQUIC– $Fe(CN)_6$  flow cell at 1.6 V. (e) UV-vis spectra of rDMQ, tDMQ, and fDMQ estimated using Bayesian inference, displayed alongside the authentic spectrum of DMeQUIC.<sup>105</sup> Reproduced with permission. Copyright 2024, ACS Publication. (f) Voltage profiles (top) and absorbance changes at 765 nm of the catholyte (bottom) in the ZMRFB with  $VOSO_4$  as function of time. (g) *In situ* UV-vis spectrum of the catholyte at the charge–discharge process of ZMRFB with 50 mM  $VOSO_4$ .<sup>106</sup> Reproduced with permission. Copyright 2024, ACS Publication.

concentration. Maurice *et al.*<sup>103</sup> addressed this gap by presenting calibration methods capable of accurately quantifying both total vanadium concentration and SoC across all vanadium electrolyte mixtures, covering concentrations from 0.91 to 1.83 M. Their study addressed three types of vanadium electrolyte mixtures used in VRFBs: (i) anolyte  $V^{2+}/V^{3+}$ , (ii)  $V^{3+}/VO^{2+}$ , and (iii) catholyte  $VO^{2+}/VO_2^+$ . Two calibration methods were provided for each electrolyte: (i) a quick empirical method based on linear regression requiring only one or two hand-picked absorbances, and (ii) a more detailed spectral deconvolution method using the entire spectrum, both based on the generalized Lambert–Beer law.<sup>107</sup> The empirical methods are suited for industrial applications where low-cost optical sensors measure SoC in real-time with slightly less accuracy. The spectral deconvolution method, which is more powerful and

computationally intensive, is better for laboratory use where spectrometers are available.

Operando UV-vis spectroscopy has also been utilized in organic RFBs. Among these, quinone-based aqueous flow batteries have the potential for large-scale, cost-effective energy storage, thanks to their reliance on earth-abundant elements, high aqueous solubility, reversible redox kinetics, and tunable chemical properties like reduction potential. In a specific quinone derivative, 9,10-anthraquinone-2,7-disulfonic acid, the formation of a quinhydrone dimer from an oxidized quinone and a reduced hydroquinone leads to deviations from ideal solution behavior and affects optical absorption according to the Lambert–Beer law.<sup>108</sup> To address this, *in situ* UV-vis spectroscopy was used to determine the molar attenuation profiles of quinone, hydroquinone, and quinhydrone, along



with an equilibrium constant ( $K_{\text{QH}_2}$ ) of about  $80 \text{ M}^{-1}$  for the quinhydrone dimer formation.<sup>108</sup> These profiles helped identifying total molecular concentration and state of charge across various quinone and hydroquinone mixtures. Density functional theory (DFT) calculations supported UV-vis findings and offered insights into the dimerization conformations. A quinone–bromine flow battery was equipped with a Pd–H reference electrode to illustrate how complexation in both negative (quinone) and positive (bromine) electrolytes influences half-cell and full-cell voltage measurements. This study highlighted the importance of considering electrolyte complexation to enhance the accuracy of electrochemical modeling in flow battery systems.<sup>108</sup>

Modak *et al.*<sup>105</sup> investigated the link between capacity fading and molecule decomposition in aqueous quinoxaline-based RFBs by combining flow cell cycling with various chemical analysis techniques, including UV-vis spectroscopy. Using Bayesian statistical inference, they calculated the rate constant of tautomerization, explaining the fade rates observed in cycled cells. They studied the cycling stability of 2,3-dimethylquinoxaline-6-carboxylic acid (DMeQUIC), pointing out that the tautomerization of its reduced form is the primary cause of capacity fading. Bayesian inference revealed that the time-varying absorbance profiles in Fig. 6d are driven by the evolution of three distinct species from DMeQUIC including its reduced form (rDMQ), a transient redox-active decay product (tDMQ), and a final redox-inactive species (fDMQ). The spectra of these pure species are shown in Fig. 6e. This method demonstrated the unique capability of combining Bayesian inference and *in operando* UV-vis spectroscopy to connect molecular decomposition with capacity fading.<sup>105</sup>

Additionally, UV-vis spectroscopy was applied for investigation of aqueous manganese RFBs, which rely on the  $\text{Mn}^{2+}/\text{MnO}_2$  two-electron transfer reaction.<sup>106</sup> These batteries are attractive due to their cost-effectiveness, high voltage, and excellent safety features. However,  $\text{MnO}_2$  tends to partially dissolve during discharge, hindering sustained operation. It dissolves and deposits even more easily when  $\text{VO}_2^+/\text{VO}_2^{2+}$  is added to the catholyte as a redox mediator. The chemical process between  $\text{MnO}_2$  and  $\text{VO}_2^+$  was clarified by *in situ* UV-vis spectroscopy and kinetic analysis, which encouraged the recovery of “dead”  $\text{MnO}_2$  with little mediator that resulted in a reversible  $\text{MnO}_2$  cathode. By examining the  $\text{VOSO}_4$ -mediated  $\text{MnO}_2$  reduction process in the Zn– $\text{Mn}^{2+}/\text{MnO}_2$  RFB (ZMRFB) during charging, it was observed that the characteristic peak at 765 nm decreased with the electrochemical oxidation of  $\text{VO}_2^+$  to  $\text{VO}_2^{2+}$  at stage I (Fig. 6f).<sup>106</sup> Thereafter, the intensity of wavelengths ranging from 1000 to 500 nm increased to varying extents (Fig. 6g), indicated the appearance of  $\text{MnO}_2$  in the flow cuvette. During discharging, decreased UV absorption suggested some  $\text{MnO}_2$  particles returned to the electrode, though some “dead”  $\text{MnO}_2$  remained.<sup>109</sup> The redox mediator facilitated the swift reduction of residual  $\text{MnO}_2$  by  $\text{VO}_2^+$ , doubling the discharging time for the  $\text{VO}_2^+/\text{VO}_2^{2+}$  reaction, enhancing discharge capacity, and reducing  $\text{MnO}_2$  aggregation, thus significantly improving the ZMRFB cycle life.<sup>106</sup> These findings

underline the crucial role of UV-vis spectroscopy in enhancing the understanding and performance of RFBs, paving the way for more efficient energy storage solutions. Moreover, other metal battery systems have been explored *in operando* such as the alkaline zinc–iron/nickel hybrid flow battery with similar motivations.<sup>110</sup>

Next to these examples, *in operando* UV-vis spectroscopy has been applied for the analysis of kinetic processes in solution, more specific of the effect of redox boosters. Lu *et al.*<sup>111</sup> investigated polysulfide-based flow batteries, whose main disadvantage is its rather sluggish kinetics. They designed a catalyst based on riboflavin, which improved the kinetics and finally the performance of the polysulfide-ferrocyanide battery to a large extent. Using *in operando* UV-vis spectroscopy, they were able to identify the kinetic processes and to finally design an efficient catalyst.

In the field of RMFBs, also known as redox-targeting flow batteries, *in operando* UV-vis spectroscopy has been applied in several works to investigate the charge transfer reaction between different pairs of solid energy boosters and soluble redox mediators. In an early report, M. Zhou *et al.*<sup>112</sup> monitored concentration changes of the catholyte redox mediator, a ferrocene-grafted ionic liquid (FcIL), during cycling of a  $\text{LiFePO}_4$ -based Lithium RFB. By using a spectro-electrochemical flow cell connected to the outlet cathodic flow channel, the concentration of FcIL during the discharging process was determined from the characteristic absorbance of the redox mediator at 630 nm. As the electrolyte was concentrated, UV-vis spectra were recorded as differential absorbance by using the fully charged catholyte as the reference. Comparison of the time-dependent concentration of the charged form of FcIL ( $\text{FcIL}^+$ ) in a cell without and loaded with the  $\text{LiFePO}_4$  solid booster showed extended time series spectra for the cell loaded with  $\text{LiFePO}_4$  during a galvanostatic measurement. In the presence of solid active material, the concentration changes of  $\text{FcIL}^+$  over the discharging process become stabilized while reaching the steady state, implying that the redox mediated process is the limiting step to sustain a constant flux of FcIL for electrode reaction under the conditions applied.<sup>112</sup>

The Prussian Blue(PB)- $[\text{Fe}(\text{CN})_6]^{4-/3-}$  is another example of solid booster/redox mediator pair where the redox mediated reaction mechanism has been investigated by *in operando* UV-vis spectroscopy, initially for an aqueous hybrid PB–Fe/Zn RFB<sup>113</sup> and more recently, for a high energy density and low cost neutral aqueous PB–Fe/ $\text{K}_2\text{S}$  RFB.<sup>114</sup> In both studies, a custom-designed spectro-electrochemical cell was connected to the outlet cathodic flow channel of a symmetric flow cell and *in operando* UV-vis spectra of the catholyte ( $[\text{Fe}(\text{CN})_6]^{4-/3-}$  redox pair) with or without PB granules were monitored during charging/discharging (Fig. 7). While  $[\text{Fe}(\text{CN})_6]^{4-}$  shows nearly no absorption at wavelengths larger than 400 nm,  $[\text{Fe}(\text{CN})_6]^{3-}$  has a high absorption band at 460 nm, allowing to probe the concentration of  $[\text{Fe}(\text{CN})_6]^{3-}$  at different stages of charge/discharge. In absence of PB booster, a linear relationship between the absorbance at 460 nm and  $[\text{Fe}(\text{CN})_6]^{3-}$  concentration was observed during the whole charge/discharge process, indicating



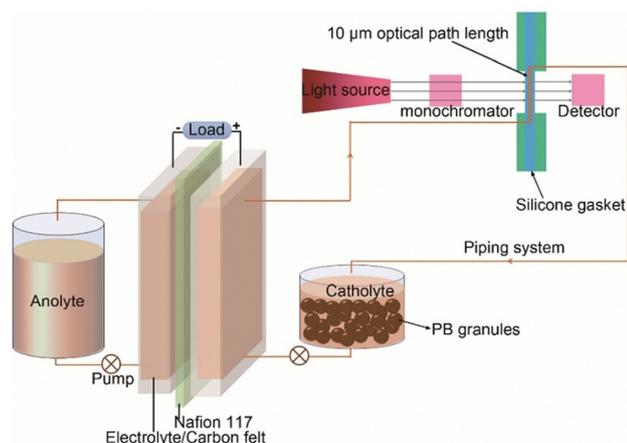


Fig. 7 Configuration of the setup for *in operando* UV-vis spectroscopy measurements at the catholyte of a RMFB.<sup>113</sup> Reproduced with permission. Copyright 2019, Cell Press Publication.

the charge/discharge capacity solely arises from the redox reactions of the  $[\text{Fe}(\text{CN})_6]^{4-/3-}$  redox pair. In presence of PB, the  $[\text{Fe}(\text{CN})_6]^{3-}$  concentration changed linearly only initially at low SoC, indicating the electrochemical reduction of  $[\text{Fe}(\text{CN})_6]^{3-}$  at the electrode, and started to deviate from linearity, reaching a steady state, at approximately 50% SoC of  $[\text{Fe}(\text{CN})_6]^{4/3-}$  electrolyte, indicating that redox mediated reaction with Prussian White (PW, the reduced form of PB) occurred. At this stage, the charge/discharge capacity arises from the redox mediated reaction between  $[\text{Fe}(\text{CN})_6]^{4-/3-}$  and PB/PW.

### 1.6. *In situ* and *in operando* Raman spectroscopy

During cycling of RFBs, redox reactions as well as absorption and desorption processes on the electrodes lead to changes in the redox states and the formation and/or breaking of chemical bonds in the components of the electrolytes and/or the electrode materials. Vibrational spectroscopic techniques, such as Raman scattering can probe these processes. Raman spectroscopy has been employed successfully in electrochemistry to monitor chemical reactions and probe intermediates as well as pH values in the electrolytes, monitor changes on catalytic electrode surfaces and investigate surface adsorbates.<sup>115,116</sup>

Unlike FTIR spectroscopy, Raman scattering is less prone to absorption in aqueous media. However, care must be taken as the focusing of an intense laser beam on a spot of typically 1  $\mu\text{m}$  in diameter causes significant heating of the sample. This may impact the reaction to be monitored and may lead to phase transitions in electrode materials or even damage the electrode material. To minimize the light-induced damage, the laser light needs to be attenuated, *e.g.*, by using a line focus if available or fast rotation of electrodes. As such, extensive control experiments must be undertaken for each system to find the optimal laser power. Furthermore, control experiments are also needed to explore possible interfering bands from the electrolyte salt in the same spectral region as the charge-storing species using identical laser radiation conditions.

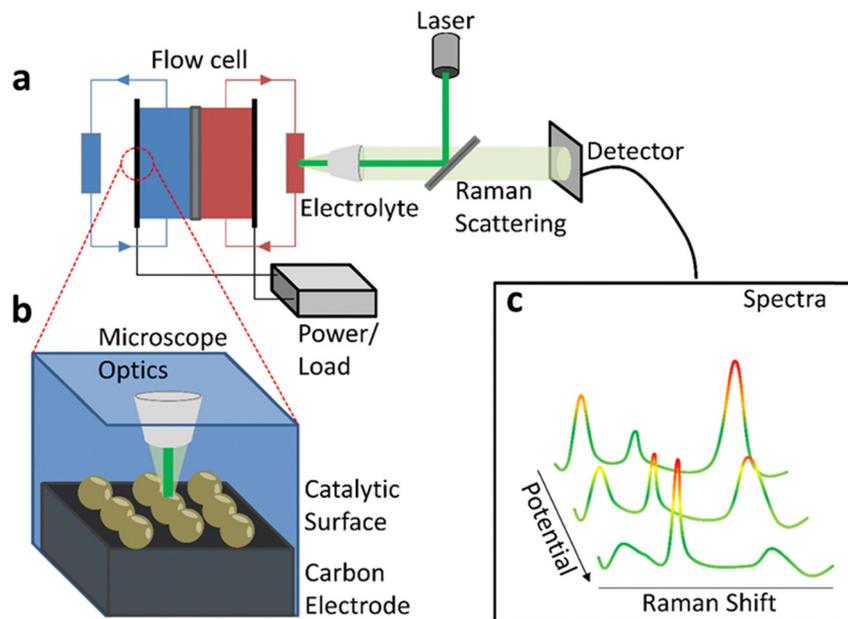
To achieve good resolution of the spectra, the weak Raman scattering needs to be acquired through confocal microscope

optics with large numerical aperture while air gaps, as well as long passages of light through the medium should be avoided to minimize losses. A schematic representation of an *operando* Raman spectroscopy setup is shown in Fig. 8a–c. A typical standard Raman spectrum may require several minutes to be acquired. To increase the related time resolution, enhancement techniques such as surface-enhanced Raman spectroscopy (SERS)<sup>117</sup> and tip-enhanced Raman spectroscopy (TERS)<sup>118</sup> may be employed to collect spectra within seconds. As the enhancement factors can vary strongly depending on the electrical potential as well as the sample history a suitable normalization procedure is required when using these techniques.

Because of the small focus area of the laser, Raman spectroscopy also allows for a highly localized investigation of electrodes with spatial resolutions of 1–2  $\mu\text{m}$ . In a recent example, Lan and Li *et al.*<sup>64</sup> investigated an electrode material made from ordered hierarchical porous Co and N co-doped carbon (OHP-Co/NC) for usage in a polysulfide/ferrocyanide RFB. They monitored the composition of the electrolyte by *in operando* Raman spectroscopy, identifying different polysulfide species, *i.e.*,  $\text{S}_2^{2-}$ ,  $\text{S}_3^{3-}$  and  $\text{S}_4^{2-}$  through their specific S–S bond stretching modes. Following the composition of the electrolyte during the charge and discharge cycle revealed a high reversibility of the electrochemical processes in this system. Owing to the high spatial resolution of Raman spectroscopy they were also able to monitor the reaction on a single OHP-Co/NC particle of approximately 2  $\mu\text{m}$  that revealed a high selectivity of this material towards  $\text{S}_4^{2-}$  and  $\text{S}_2^{2-}$ , whereas no  $\text{S}_3^{3-}$  was found. While *in operando* Raman spectroscopy of the electrolyte solution revealed more  $\text{S}_2^{2-}$  than  $\text{S}_4^{2-}$ , the *in situ* Raman spectroscopy performed on the surface of a single OHP-Co/NC particle showed a different distribution with more  $\text{S}_4^{2-}$  than  $\text{S}_2^{2-}$ . This reflects the complex interplay of the electrochemical reactions on the electrode surface and additional chemical reactions in the bulk phase of the electrolyte in this polysulfide system.<sup>119</sup>

Further applications for exploring reaction mechanisms were proposed by Zhang *et al.*,<sup>65</sup> who investigated an atomic Bi–O–Mn catalytic interface on a mesoporous  $\text{Mn}_3\text{O}_4$  sub-scaffold grafted onto carbon felts ( $\text{Bi}_1\text{-sMn}_3\text{O}_4\text{-CF}$ ) as electrodes for VRFBs. The atomic Bi–O–Mn interface catalyzes the  $\text{V}^{3+}/\text{V}^{2+}$  conversion while the mesoporous  $\text{Mn}_3\text{O}_4$  scaffold facilitates fast shuttling of redox active species from the surface to the pores leading to high performance RFBs with 77% energy efficiency up to a current density of 400  $\text{mA cm}^{-2}$  and peak power density of 1.503  $\text{W cm}^{-2}$  while maintaining durability over 1500 cycles. Using Raman spectroscopy, they confirmed the incorporation of bismuth onto  $\text{Bi}_1\text{-sMn}_3\text{O}_4\text{-CF}$  by a down-shift of 6  $\text{cm}^{-1}$  in the strong phonon Mn–O deformation vibration compared to  $\text{sMn}_3\text{O}_4\text{-CF}$  without Bi. By *in situ* Raman spectroscopy, they identified bridging intermediates of the first solvation shell of vanadium ions dissolved in  $\text{H}_2\text{SO}_4$  that are involved in the redox reaction after adsorption. For this, they compared S–O and S–OH stretch vibrations in the pure electrolyte and during oxidation and reduction at the electrode. During the oxidation they observed an increased intensity of the S–O vibration and a decreased intensity of the S–OH





**Fig. 8** (a) Scheme of an *in operando* Raman spectroscopy setup for the investigation of redox flow cells.<sup>64</sup> The laser can be focused onto the electrolyte by confocal microscope optics that will also pick up the Raman scattering and focus it on the detector. (b) Besides the electrolyte composition it is also possible to detect bound species on the surface of the electrodes.<sup>64</sup> (c) Measuring the Raman spectra *in operando* allows to correlate changes in the relative composition of the redox active species with the electrochemical potential of the cell.<sup>64</sup> Reproduced with permission. Copyright 2023, ACS Publication.

vibration as well as additional V–O–S modes. This allowed them to propose a feasible mechanism in which first  $\text{H}_2\text{O}$  dissociates from  $[\text{V}(\text{H}_2\text{O})_6]^{2+}$  upon binding to  $\text{*Bi}$ , and subsequently  $\text{SO}_4^{2-}$  is added leading to a  $\text{*Bi}[\text{V}(\text{H}_2\text{O})_5(\text{SO}_4^{2-})]$  intermediate. The intermediate promotes the charge transfer process due to its higher polarizability leading to the product  $[\text{V}(\text{H}_2\text{O})_5(\text{SO}_4^{2-})]^+$ . During the reduction process no changes in the signals of S–O and S–OH bond stretching vibrations were observed leading to the assumption of a direct adsorption and desorption process of  $[\text{V}(\text{H}_2\text{O})_6]^{3+}$  without an intermediate species.

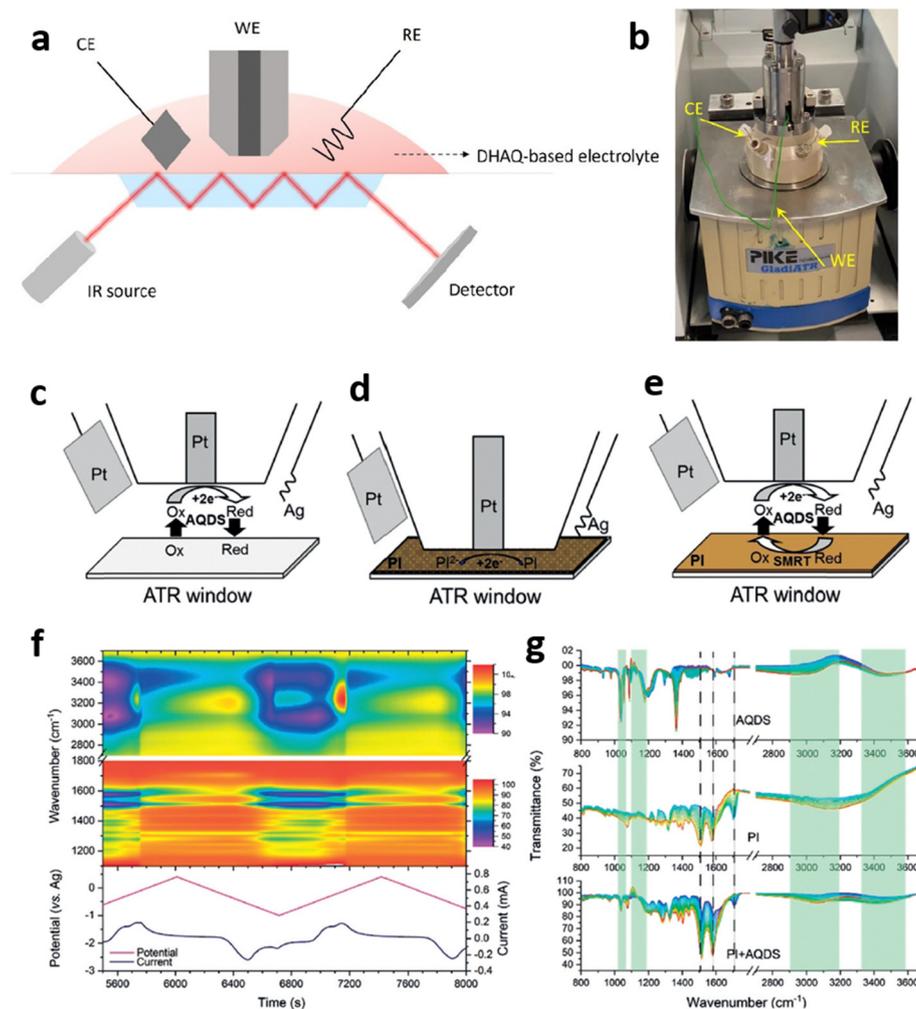
In another report by Nambafu *et al.*,<sup>120</sup> *in operando* Raman measurements, supported by DFT studies, provided compelling evidence for a specific molecular structure in a novel Fe anolyte for all-iron RFB (Fe-RFBs), specifically an Fe complex with a nitrogenous phosphonate/carboxylate mixed ligand, *N,N*-bis-(phosphonomethyl)glycine (BMPG). The findings suggest that in BMPG, mixed phosphonate/carboxylate groups ensure that the Fe ion center maintains octahedral coordination exclusively with phosphonates, leaving the carboxylate unbound for both  $\text{Fe(II)}$  and  $\text{Fe(III)}$  complexes. This structural consistency between BMPG-based  $\text{Fe(II)}$  and  $\text{Fe(III)}$  complexes helps to alleviate the slow redox reaction kinetics typically seen in  $\text{Fe}(\text{NTMPA})_2$  ((iron(II) nitrilotri(methylphosphonate acid)) anolyte, where significant ligand reorientation between the complexes occurs. The strategically modified ligand in the Fe anolyte allows enhanced performance in the Fe-RFB.<sup>120</sup>

*In operando* Raman spectroscopy was also employed by Radinger *et al.*<sup>121</sup> to monitor the reactions that occurred at the interface between graphite-based model electrodes and vanadium-containing sulfuric acid electrolyte. The growth of

various vibrational modes as the potential changed was linked to the electrocatalytic activity of the sample, allowing for the tracking of electrolyte species oxidation. Additionally, the findings revealed that vanadium reaction intermediates of dimeric origin appeared exclusively on the edge-exposed surface of graphite, which displayed notably higher electrochemical activity. Contrary to previously proposed interactions with surface oxygen, the Raman measurements revealed direct electronic interactions between vanadium ions and carbon atoms during charge transfer. More recently, Lubian *et al.*<sup>122</sup> applied time-resolved Raman spectroscopy for operando investigation of reaction mechanisms responsible for charge storage capacity decay in a 2,6-dihydroxyanthraquinone–ferrocyanide alkaline flow battery. In their work, the faradaic imbalance process was explored, showing that the presence of oxygen in the anolyte leads to progressive loss of available ferrocyanide. Self-discharge of ferricyanide when left at an open circuit was also detected by Raman spectroscopy. Moreover, the operando technique allowed tracking the crossover of 2,6-dihydroxyanthraquinone.<sup>122</sup> The report illustrated the power of Raman spectroscopy to monitor in real time chemical processes in flow battery electrolytes.

In addition to exploring reaction mechanisms, *in situ* Raman spectroscopy has been applied quantitatively for the real-time estimation of the SoC of a zinc-bromine RFB upon cycling.<sup>123</sup> Accurate estimation of the SoC in zinc-bromine RFB is very challenging. The inhomogeneous mixing of the aqueous zinc bromide phase and non-aqueous polybromide phase in the positive electrolyte, together with the simultaneous occurrence of various equilibrium reactions in the battery, *e.g.*, charge-transfer reactions, polybromide formation and complexation





**Fig. 9** (a) Schematic representation of an *in operando* ATR-FTIR setup and (b) photograph of the cell for DHAQ electrolyte. The working electrode (WE) consisted of a Pt disk (diameter: 3 mm with a Pt plate ( $4 \times 2.5 \text{ mm}^2$ ) as counter electrode and a Ag wire (diameter: 0.5 mm) as reference electrode to detect the structural evolution of 2,6-DHAQ and 1,5-DHAQ and PAQS/CB composites from 4000 to  $900 \text{ cm}^{-1}$  with a resolution of  $4 \text{ cm}^{-1}$ . The CV scan rate was  $2 \text{ mV s}^{-1}$ , and the working distance was 0.05 mm to the substrate. The blank background was 1 M KOH solution. 0.1 M 2,6-DHAQ and 1,5-DHAQ were dissolved into 1 M KOH to obtain the operando FTIR spectra during CV scans.<sup>67</sup> Reproduced with permission. Copyright 2022, Nature Publishing Group. (c)–(e) *In situ* ATR-FTIR setup for (c) 2,7-AQDS only, (d) PI only, (e) PI under reaction with 2,7-AQDS. (f) *In situ* FTIR spectra of PI during reaction with 2,7-AQDS, the color bar indicates transmittance. (g) FTIR spectra evolutions during reduction of 2,7-AQDS without PI substrate (upper), reduction of PI coated on carbon cloth without 2,7-AQDS (middle) and reduction of PI during redox-mediated reaction with 2,7-AQDS (lower).<sup>124</sup> Adapted and reproduced with permission. Copyright 2020, Wiley-VCH.

complicate SoC determination. To avoid errors arising from the inhomogeneous mixing of the aqueous and non-aqueous phases in the positive electrolyte, *in situ* Raman analysis was performed on the negative electrolyte flowing from the cell to the reservoir during the charge–discharge. In their study, Lee *et al.*<sup>123</sup> observed a strong linear relation between the Raman band intensity and total zinc bromide concentration, proving that *in situ* Raman spectroscopy is very effective for the real-time SoC estimation under operando conditions.

### 1.7. *In situ* and *in operando* FTIR spectroscopy

FTIR is another type of vibrational spectroscopy which has been used to explore *in operando* electrolyte solutions for RFB. Kautek *et al.*<sup>66</sup> conducted *in situ* absorption-reflection FTIR

spectroscopy in the formation of bromine-complexes in a zinc/bromine flow battery at gold electrodes. In this RFB, storage reactions are the cathodic deposition of zinc and the anodic formation of a nonaqueous polybromide phase. *In situ* FTIR spectroscopy measurements revealed formation of ion pairs between electrode adsorbed polybromide anions and quaternary ammonium cations, which store the bromine as polybromide complexes. Studying the complex formation capability of different cations, they were able to identify electrolyte compositions for enhanced efficiency of zinc/bromine flow batteries by improving the capability to store bromine.

Huang *et al.*<sup>67</sup> performed attenuated total reflection Fourier transform infrared spectroscopy (ATR-FTIR) to monitor changes of bonding structures of 2,6-DHAQ and 1,5-DHAQ at



different stages of reduction during CV scans using a commercialized spectro-electrochemical cell (Fig. 9a and b). The evolution of vibrations of C–O and C=C bonds of 2,6-DHAQ and 1,5-DHAQ in the range of 1300–1600  $\text{cm}^{-1}$  were recorded during CV scans. The signal of C=C gradually diminished in the cathodic scan and re-emerged in the anodic scan while C–O showed a reversed trend. Variations of the characteristic vibrations of water molecules were attributed to changes of the solvent environment associated with disruption of the water molecule network with quinone molecules through hydrogen bonding. New peaks emerging at around 1105 and 1242  $\text{cm}^{-1}$  upon reduction followed by a resting process were attributed to the presence of 2,6-dihydroxyanthrone (2,6-DHA), suggesting a disproportionation reaction producing 2,6-DHAQ and 2,6-DHA (hydrogen bond-mediated degradation process). This was not the case for 1,5-DHAQ, whose reduced state (1,5-DHAQ<sup>2-</sup>) preferably forms 1,5-DHAQ<sup>2-</sup>·H<sub>2</sub>O, for which the neighboring oxygen sites are bonded with the same water molecule preventing it from joining another DHAQ molecule (hydrogen bond-mediated protection process). Their work highlights the power of *in operando* ATR-FTIR characterization to elucidate electrochemical reaction mechanisms.<sup>67</sup>

Redox mediated processes of organic solid booster/redox mediator pairs have also been investigated by *in operando* FTIR spectroscopy for different RMFB chemistries. In a first report, the redox reaction between the quinone derivative 9,10-anthraquinone-2,7-disulphonic acid (2,7-AQDS) and the 1,4,5,8-naphthalenetetracarboxylic dianhydride polyimide (PI) in neutral electrolyte was explored during a CV scan in an ATR-FTIR spectro-electrochemical setup (Fig. 9c–e).<sup>124</sup> The PI solid booster was deposited on the ATR-FTIR window and the 2,7-AQDS solution was polarized in a three-electrode configuration. Spectral changes of 2,7-AQDS and PI alone and those of the 2,7-AQDS/PI system were monitored in separate CV experiments (Fig. 9f). The reversible vibrational changes in the region 1400–1800  $\text{cm}^{-1}$  of the FTIR spectra (imide carbonyl C=O bands) of PI measured for the 2,7-AQDS/PI system corroborated the reversible redox-mediated reactions between 2,7-AQDS and PI in both cathodic and anodic directions and the regeneration of 2,7-AQDS on the PI substrate (Fig. 9g). FTIR investigations allowed proposing a mechanism of hydrogen-bonding mediated charge transfer between 2,7-AQDS and PI in pH-neutral solutions that was corroborated by DFT calculations.<sup>124</sup>

Similarly, mechanistic studies were conducted by Huang *et al.*<sup>67</sup> using *in operando* ATR-FTIR for the solid booster/redox mediator pair 1,5-DHAQ/poly(anthraquinonyl sulfide) (PAQS). Time-dependent evolution of the FTIR spectra of PAQS was monitored during repeated CV scans. During reduction of 1,5-DHAQ, a stretching vibration of C–O bond of reduced PAQS at 1371  $\text{cm}^{-1}$  gradually appeared that vanished during oxidation of 1,5-DHAQ<sup>2-</sup>. Additional reversible changes of vibrations attributed to the aromatic rings also corroborated the reversibility of the redox mediated process.

### 1.8. *In situ* and *in operando* XAS

An important technique to probe the element specific oxidation states and structures of electrolytes and electrodes is the XAS.

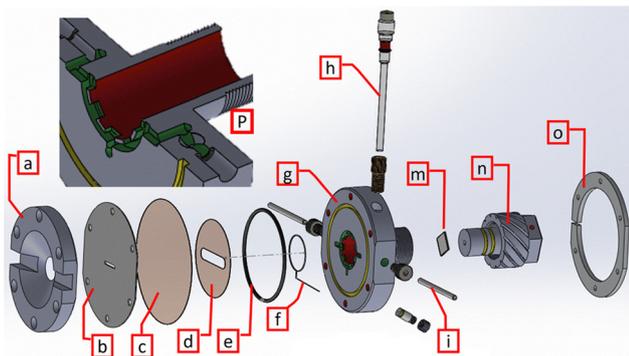
It allows the observation of electronic transitions of inner shell electrons, and selection of the X-ray energy regime allows for different penetration depths to probe the bulk phase or superficial regions.<sup>125</sup> The penetration depth is also affected by the method of detection. Both, transmission and fluorescence mode mainly contain information about the bulk phase as the surface components only make a small contribution to the resulting signal. Samples for transmission also need to be thin enough for the radiation to pass through, which is especially challenging at low X-ray energies. Measurements at very small angles under total external reflection as well as measurements of Auger electrons can provide information on the sample surface. Samples need to be homogenous, and one must consider the energy dependent absorption lengths in the material of interest as well as of substrate materials at the utilized energy for transmission or fluorescence measurements. Heat buildup and radiation damage to the sample might occur which limit the energy of X-rays used and may require cooling of the sample, albeit without freezing the electrolyte solution which would impede the flow inside a flow-cell.<sup>126</sup>

As tunable source for monochromatic X-rays a synchrotron is commonly applied and detection takes place at the absorption edge, that is the energy at which an electron is removed from an inner orbital by X-ray absorption. X-ray absorption near edge structure (XANES) yields information about the electronic configuration and coordination states while analyzing the extended X-ray absorption fine structure (EXAFS) yields information about the structure and environment of the atom.

Most XAS investigations of RFB materials have not been conducted *in situ* during operation. Instead *ex situ* investigations after cycling have been conducted to explore (i) changes undergone by electrocatalysis,<sup>127</sup> (ii) the influence of functional groups in carbon felts on the kinetics of the VO<sup>2+</sup>/VO<sub>2</sub><sup>+</sup> reaction,<sup>128</sup> and (iii) the chemical and morphological origins of improved ion conductivity in ion-conducting polymer membranes,<sup>129</sup> among other applications.<sup>130</sup> A first application of *in situ* XAS for redox flow cells was reported by Jia *et al.*<sup>68</sup> who studied the oxidation states of vanadium ions during the first charge/discharge cycle of a VRFB. They observed the K-edge of vanadium in the anolyte and catholyte using XANES in a flow cell equipped with sections of a Kapton tube as observation windows with a time resolution of 6 min per spectrum. They found that during a first charging step the oxidation of the precursor VOSO<sub>4</sub> to VO<sub>2</sub><sup>+</sup> on the cathode and the reduction of VOSO<sub>4</sub> on the anode site to V<sup>2+</sup> only reached about 82% of the theoretical maximum affecting all subsequent cycles as well. Based on their findings, they proposed an improved first charging cycle to utilize 100% of the available capacity in this system.

Probing the interface between electrode and electrolyte has proven a challenging task with XAS as the intensity of the X-ray beam is strongly attenuated already by liquid films of a few  $\mu\text{m}$  in thickness especially at low X-ray energies. Using higher energies can improve penetration into liquid layers but limits the observation to heavier nuclei. On the contrary, using thin liquid layers of a few nm leads to fast expiration of the





**Fig. 10** Exploded view of the cell: (a) top PEEK plate, (b) mask, (c) Kapton window and (d) spacer, (e) O-ring, (f) counter electrode, (g) cell body, (h) reference electrode, (i) electrolyte outlet, (m) sample, (n) sample holder column, (o) bottom aluminum plate. (P) (inset) detail of the inlet/outlet channels passing through the counter electrode compartment. The top plate (a) is designed for fluorescence measurements with a 120° view angle, which extends to 150° through two channels, allowing near 15° incidence and emergence angles. The sample is positioned close to window (c) and can be adjusted using a retractable column (n). It is secured with PELCO carbon conductive glue, and sides are coated with nitrocellulose varnish, leaving the front uncoated. The cell body (g) has a circular aperture for the sample holder, surrounded by a Pt wire counter electrode (f). Electrolyte flows through apertures (i) and channels (inset P) for circulation before and after contact with the sample. A leak-free Ag/AgCl reference electrode (h) completes the three-electrode setup, ensuring compatibility and preventing contamination. The window assembly consists of 25 μm Kapton foil and a 50 μm Kapton spacer (c) and (d) bonded to a 1.5 mm thick Teflon mask (b) with a 3 × 14 mm hole for beam access. Top and bottom plates (a) and (o) press the window against the cell body (g), allowing free volume above the sample. The electrolyte fills the counter electrode compartment (f) and (P), with all components in contact with the electrolyte made from PEEK and sealed with FFKM o-rings for leak-tightness. A peristaltic pump circulates the solution continuously refreshing the electrolyte to maintain stable cell potential.<sup>69</sup> Reproduced with permission. Copyright 2024, RSC Publication.

electrolyte during operation while formation of gas bubbles in some reactions leads to strong perturbations in the measurements. Paparoni *et al.*<sup>69</sup> presented a novel flow-cell design for *in operando* XAS with an X-ray opaque electrode surface and liquid layers down to 17 μm that allowed them to study the influence of Ni doping of Fe<sub>2</sub>O<sub>3</sub> films grown on Pt substrates on the catalysis of the oxygen evolution reaction. Their cell design (Fig. 10) facilitated the adjustment of the liquid layer thickness above the electrode sample for gradient free reactions at stable cell potentials and allowed observation of *in operando* XAS at low energy absorption edges such as iron and titanium with total transmittances of 43% for Ti and 75% for Fe.

Moreover, Lutz *et al.*<sup>131,132</sup> also conducted synchrotron experiments with spatiotemporal resolution to unravel the vanadium species gradient variation during diffusion through the membrane at different points in the flow field. Their experiments confirmed the chemical formation of V(IV) inside the membrane after exposing to V(III) on one side and V(V) on the other one. XAS was also applied by Huang *et al.*<sup>133</sup> in a Zn–Fe RFB to investigate *in operando* the Cr-doped NiFe(oxy)-hydroxide (CrNiFeOOH) catalyst used to compensate the coulombic inefficiency caused by irreversible anodic parasitic

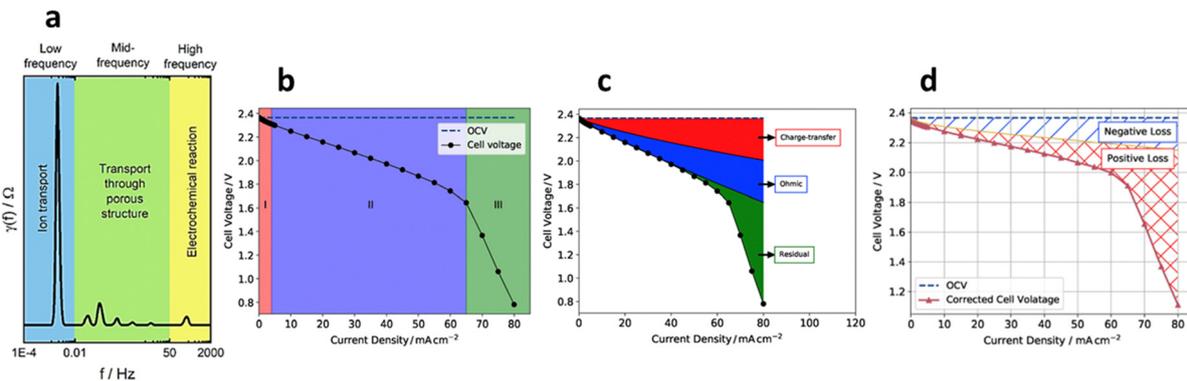
reactions that lead to unbalanced charge state of catholyte/anolyte and subsequently, to poor cycling performance. The proposed coulombic efficiency compensating strategy aimed to equalize the charge state of the [Fe(CN)<sub>6</sub>]<sup>3-/4-</sup>-based catholyte by promoting the oxygen evolution reaction (OER) in the cathodic side aided by a CrNiFeOOH catalyst placed in an external catalytic reactor column *via* a redox-mediated process.<sup>133</sup> *In operando* XAS was employed to investigate the valence states of metal species in CrNiFeOOH catalyst and analyze the reaction mechanism during the redox-mediated OER process. The normalized Cr, Fe, and Ni K-edge XANES of CrNiFeOOH catalyst collected during the charge process revealed that the oxidation states were Fe<sup>3+</sup>, Ni<sup>2+</sup>, and Cr<sup>3+</sup> in pristine CrNiFeOOH. At increased SoC using [Fe(CN)<sub>6</sub>]<sup>3-/4-</sup>-based electrolyte, observed energy shifts for the main edge and pre-edge features in Cr and Ni XANES indicated that the oxidation process of CrNiFeOOH upon charging involved the oxidation of Cr<sup>3+</sup> to Cr<sup>6+</sup> initially, followed by the oxidation of Ni<sup>2+</sup> whereas the main edge of Fe in the CrNiFeOOH catalyst remained at the same peak position, suggesting that the valence of Fe<sup>3+</sup> was unchanged. The whole redox-mediated process was similar to direct electrochemical OER with the same electrocatalyst grafted on electrodes.<sup>133</sup>

Similarly, Y. Cai *et al.*<sup>134</sup> conducted *operando* synchrotron XAS measurements to explore interface reaction mechanism of the redox-mediated process between the LiMn<sub>x</sub>Fe<sub>1-x</sub>PO<sub>4</sub> solid energy booster and [Fe(CN)<sub>6</sub>]<sup>3-/4-</sup> redox mediator in a Zn–Fe RMFB. *Operando* synchrotron XAS unveiled the reversible changes of the Fe–O and Fe–Fe bonds in the [Fe(CN)<sub>6</sub>]<sup>3-/4-</sup>-LiMn<sub>x</sub>Fe<sub>1-x</sub>PO<sub>4</sub> system during real-time monitoring.

### 1.9. *In situ* and *in operando* electrochemical techniques

EIS is one of the most used techniques for characterizing RFBs. It offers insights into the charge transfer resistance, ohmic losses, and mass transport limitations within the battery. Usually, interpreting EIS data relies on fitting equivalent circuit models and requires prior knowledge of the system. However, Schilling and co-authors<sup>135</sup> combined EIS with distribution of relaxation times (DRT) analysis, which is a mathematical approach, offering an alternative by transforming the impedance data from the frequency domain into a distribution of time constants without the need for *a priori* assumptions. This transformation reveals distinct peaks corresponding to different physicochemical processes, such as the electrochemical redox reaction, transport through the porous electrode structure, and ion transport in the electrolyte. They applied DRT analysis to investigate the V(IV)/V(V) redox reaction in VRFB half-cells, producing a spectrum that plots the distribution function of relaxation times  $\gamma(f)$  against frequency, where high-frequency peaks (above 50 Hz) correspond to redox reactions, mid-frequency peaks (10 mHz–50 Hz) to transport through the porous electrode, and low-frequency peaks (below 10 mHz) to ion diffusion in the electrolyte (Fig. 11a).<sup>135</sup> Similarly work done by Schneider *et al.*<sup>136</sup> deconvoluted the whole DRT spectra into the individual contributions from the RFB system utilizing full- and half-cell tests. Enabling the tracking of changes in the





**Fig. 11** (a) Schematic display of the proposed peak assignments to the half-cell processes using an exemplary DRT spectrum.<sup>135</sup> Reproduced with permission. Copyright 2022, Elsevier Publication. (b) Open-circuit current density and the obtained voltage-current density polarization curve of the Zn-Cr battery with its three distinct regions where I activation, II ohmic, and III residual effects (mass transfer) influence its voltage loss. (c) Resolved factors causing overpotentials in the battery systems leading to voltage loss: Charge transfer, ohmic, and residual factors. (d) Resolved polarization curve of the RFB to identify the side of major losses contributing to the system.<sup>70</sup> Reproduced with permission. Copyright 2020, Elsevier Publication.

systems, such as changes in liquid flow rate, kinetics and mass transport. Both works showcase how the use of DRT can help to better understand the measured EIS spectra and monitor changes in the system. In addition, the method serves as a fingerprint for electrode materials based on their morphology and wettability, helping in the optimization of electrodes for VRFBs. Calculation of the DRT spectra from the measured EIS spectra can readily be accomplished with the software tools from Tichter *et al.*<sup>137,138</sup> and Ciucci and co-workers.<sup>139–142</sup>

In systems such as the zinc-cerium RFB (Zn-Ce RFB), *in situ* polarization measurements coupled with EIS have been utilized by Amini *et al.*<sup>68</sup> to pinpoint performance limitations (Fig. 11b). By inserting reference electrodes in the flow paths, it was possible to decouple the contributions of the positive and negative electrodes to overall voltage losses (Fig. 11d). For example, most of the kinetic overpotential in Zn-Ce RFBs originates from the Zn/Zn<sup>2+</sup> half-cell, particularly at low current densities, where kinetic limitations dominate (Fig. 11b and c). This allows for targeted improvements in electrolyte formulation or electrode material. Further, they were able to show how the current density influences the detrimental factors of the voltage loss. Another study employed EIS while using a pulse dampener in the hydraulic circuit to collect stable low-frequency impedance spectra at operationally relevant flow rate of 25 mL min<sup>-1</sup> in a VRFB.<sup>143</sup> This allowed for the quantification of charge transfer, finite diffusion, and ohmic resistances and assessing critical physical parameters such as rate constants and effective surface areas of various electrode materials, offering a deeper understanding of how electrode structure and morphology affect performance. For example, GFD3 felt was found to be mainly limited by charge transfer resistance, whereas 10AA carbon paper displayed considerable contributions from all three types of resistance.<sup>143</sup>

Addressing battery operation at elevated temperatures is, however, a key challenge for stationary storage applications. Thus, the maximum operating temperature for vanadium solutions in flow batteries is generally capped at 40 °C to avoid the thermal precipitation of V<sub>2</sub>O. In this regard, a comprehensive

study was conducted to assess the high-temperature stability of redox solutions in VRFBs. The study compared batch (solution in flasks under temperature control) and *in operando* (RFB operation) precipitation experiments, revealing that relying solely on capacity fade to assess precipitation can be misleading due to significant influences from external oxidation and cycling parameters. *In operando* electrochemical experiments consistently showed a precipitation temperature 10–20 °C higher than batch tests at a 100% SoC for the same duration.<sup>144</sup>

A comparable method detailed the use of carbon fiber-based potential probes embedded in the membrane of a VRFB to monitor transport processes and redox reactions occurring within the membrane. By strategically placing these probes at various points within a prepared multilayer membrane stack, distinct redox potentials ( $\Phi$ ) were identified, which were linked to specific vanadium ion species ( $\Phi < -0.083$  V: V<sup>2+</sup> and V<sup>3+</sup>;  $0.183$  V  $< \Phi < 0.537$  V: V<sup>3+</sup> and VO<sup>2+</sup>;  $\Phi > 0.823$  V: VO<sub>2</sub><sup>+</sup> and VO<sub>2</sub><sup>2+</sup>). This allowed the real-time observation of processes inside the membrane both *in situ* and *in operando*. Furthermore, it was determined that reactions occur in the through-plane area of the membrane, with the position of the reaction front being influenced by the SoC in the bulk electrolytes.<sup>145</sup> Another approach in electrode design is a simple yet effective silver-silver sulfate reference electrode for use in VRFBs for evaluation of their electrochemical performance under *in operando* conditions. By inserting this reference electrode between two membrane pieces, Ventosa *et al.*<sup>71</sup> were able to gain valuable insights, as demonstrated in the study of ammoxidized graphite felts. Findings from this study revealed that the kinetics of the VO<sub>2</sub><sup>+</sup>/VO<sub>2</sub><sup>2+</sup> reaction are slower compared to the V<sup>2+</sup>/V<sup>3+</sup> reaction at the electrode, contributing to limitations in voltage efficiency.

The through-plane voltage-loss profile of a VRFB and the changes in electrolyte conditions during practical charge-discharge cycles have also been explored in several studies.<sup>146,147</sup> Results indicated that the anode half-cell reactions and the conditions of the anolyte (SoC, vanadium ion concentrations)



significantly influenced overall VRFB performance. Traditional methods for calculating efficiencies (coulombic, voltage, and energy), based on total electron input and output, have limitations, as they do not account for energy storage efficiency and charge capacity decay during cycles. A new methodology was introduced to analyze capacity decay and coulombic efficiency by focusing on electrolytes and internal cell resistance. Correlating through-plane voltage losses, electrolyte conditions, and charge storage capacity evolution helped to quantify the effects of coulombic round-trip loss, vanadium ion crossover loss, concentration loss of the limiting electrolyte, and charge imbalance loss on the coulombic storage efficiency. This comprehensive analysis method offered a valuable tool for quantifying capacity losses and optimizing high-performance VRFB systems.<sup>146</sup>

A novel response time-based approach for VRFB was developed by Wang *et al.*<sup>148</sup> to decouple the various types of polarization—ohmic, activation, and concentration—during RFB operation. It leverages the different time constants of each polarization type to identify the contributions of each type of polarization under different working conditions (*e.g.*, flow rate, compression ratio, and current density). This allowed a more detailed analysis of voltage losses during charge and discharge cycles. Results by Wang *et al.*<sup>148</sup> showed that ohmic polarization is the dominant factor of voltage loss in VRFB. The contribution of the ohmic polarization ranges from 49.6% to 78.8% depending on the type of membrane used in the study. Furthermore, the contribution of the activation polarization was determined to be 32.4%, but can be reduced to about 2.5% by chemically modifying the electrode.

Steady-state amperometry using potential step experiments with microelectrodes is highly accurate for monitoring the state of charge in RFBs. Traditionally, only part of the current response has been used for SoC and SoH assessment. A study by Schubert and co-workers<sup>149</sup> showed that analyzing the transient chronoamperometric signal provides detailed physicochemical information, allowing the use of macroelectrodes instead of microelectrodes for both *in situ* and *ex situ* SoC measurements. The use of these macroelectrodes also enables temperature- and concentration-independent SoH assessments. The technique offers fast and cost-effective *in operando* SoC measurement without the need for restricting electrolyte flow, unlike previous methods. Additionally, the developed *ex situ* microelectrode chronoamperometric method allows the investigation of electrolyte lifetime, promising a high-throughput SoH assessment.<sup>149</sup> The same group introduced also the redox targetivity as a new parameter to study organic redox mediators in TEMPO based flow batteries. *In operando* characterization of the redox target (or solid booster) *via* electrolyte SoC monitoring provided estimates for the redox target's SoC changes during cycling. In addition, targetivity was proposed to provide insights into the efficiency of the targeting reaction and the future optimization of materials, cell designs, and operational parameters for redox targeting RFBs (RTFBs).<sup>150</sup>

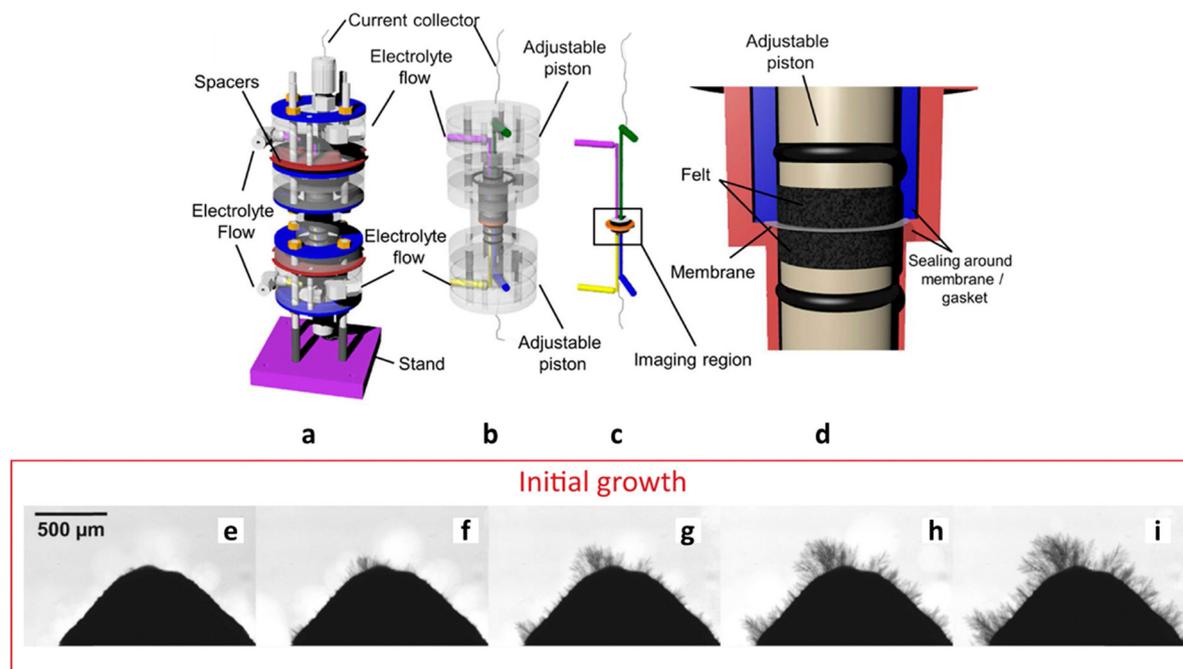
Another sensitive *in operando* technique for monitoring the SoC and average oxidation state of vanadium in VRFBs is

coulometric analysis.<sup>151</sup> This technique provides real-time data on electrolyte imbalance, which is crucial for understanding degradation processes such as ion crossover and side reactions. The sensors are integrated into the battery management system and can operate without calibration, making them ideal for long-time monitoring in industrial-scale applications. Additionally, potentiometric sensors are commonly used to track changes in the ratio of oxidized and reduced vanadium species, though they are sensitive to changes in the supporting electrolyte.<sup>152,153</sup> A microelectrode based sensor in a symmetric redox flow cell was shown to effectively measure *in operando* concentrations, highlighting its utility in such applications.<sup>13</sup> Key factors for successful implementation include attention to measurement protocols, careful material selection, and thoughtful flow cell design. Constructed from commercially available off-the-shelf components, the sensor can be easily adopted by research laboratories and integrated into existing experimental workflows, making it a valuable tool for investigating flow battery materials.

#### 1.10. *In situ* and *in operando* tomography and radiography

X-ray computed tomography (CT) has proven instrumental in characterizing felt electrodes *in operando*. Jervis *et al.*<sup>73</sup> designed a miniature flow cell enabling lab-based and synchrotron CT imaging to investigate carbon felt materials (Fig. 12a–d). This study revealed incomplete wetting of certain felt regions, resulting in areas of empty pores and electrolyte-wetted fibers. Advanced image processing techniques facilitated calculations of wetting amounts, pore size distribution, and contact angles. Moreover, X-ray CT enables the study of felts under varying *in situ* compression, providing insights into porosity, pore size distribution, and tortuosity. For instance, it was observed that significant fiber-fiber contact occurs only at 90% compression, while fiber contact with the current collector increases proportionally with compression-induced porosity reduction.<sup>154</sup> Additionally, tomography and radiography are useful tools as they enable the visualization of the interfacial processes taking place during formation of dendrites which has a detrimental effect on RFBs performance. Different tomographic methods were employed by Yufit *et al.*<sup>72</sup> to visualize dendritic growth in a zinc-air RFB in real time and to quantify various dendrite characteristics at submicron and nanoscale levels. Accordingly, they visualized the deposition of zinc dendrites onto a cone-shaped zinc anode when a negative current of 30 mA cm<sup>-2</sup> was applied between the zinc anode and a carbon air cathode. Zinc dendrites are formed after reaching a critical overpotential. The sequence of dendrite formation is shown in Fig. 12e–i, where small dendrites appear on the tip of the electrode after 214 s of deposition. As the deposition continued, dendrites at various locations on the electrode (Fig. 12f and g) are obtained. After sufficient deposition, secondary dendrites are formed on the already grown dendrites (Fig. 12h and i). This growth pattern is influenced by local crystallography and current distribution. Thereafter, ternary dendrites are grown from the secondary dendrites' trunks (Fig. 12i). In addition, Gebhard *et al.*<sup>155</sup> employed computer tomography to analyze bismuth doping of the carbon felts to improve the electrode kinetics. These studies





**Fig. 12** Design of the miniature flow cell (a), with transparent view showing internal workings of the cell (b). The path of electrolyte and working part of the cell (membrane, felt electrodes, and current collection) is shown in (c), and details of the imaging region, including the sealing that separates the two electrodes achieved by clamping the internal body (blue) onto a shelf created in the external body of the cell (red) are shown in (d). O-rings prevent electrolyte from flowing through the gap between the internal body and the adjustable piston.<sup>73</sup> Reproduced with permission. Copyright 2016, IOP Science. (e)–(i) *In operando* tomography study of zinc dendrite growth, dissolution, and regrowth in the cell without separator at a current density of  $30 \text{ mA cm}^{-2}$ . Zinc dendrite growth after (e) 214 s, (f) 388 s, (g) 561 s, (h) 734 s, and (i) 918 s.<sup>72</sup> Reproduced with permission. Copyright 2019, Elsevier Publication.

focused on deposition and dissolution processes at the carbon felt surface during charging and discharging and helped to better understand deposition patterns *in operando*.

Neutron imaging was also employed to measure spatial and temporal concentration variations in an operating redox flow cell.<sup>156</sup> By using the properties of redox-active organic materials and boron-containing electrolytes, subtractive neutron imaging was conducted to map concentration profiles across electrodes. This allowed linking concentration to cell performance through polarization experiments with changing conditions. Time-of-flight neutron imaging further clarified species and electrolyte concentrations during operation. This method provided insights into how cell polarity, voltage, and flow rate affect concentration distributions and correlated these with overall performance, offering new understanding in reactive mass transport. This technique can be applied to various (electro)-chemical systems, aiding in the development of new materials and reactor designs. Boz *et al.*<sup>157</sup> also employed *in operando* neutron radiography to monitor how electrolyte distributes within porous carbon electrodes in RFBs. The high sensitivity of neutrons to hydrogen enables this technique to distinguish between the aqueous electrolyte and the carbon electrode. This provided valuable insight into how wetting behavior changes with variations in flow rate, flow field geometry, and electrode surface treatment. However, because of the limited spatial resolution of neutron radiography, it is unable to capture interfacial phenomena like pore-level wetting dynamics or electrochemical reactions at the electrode–electrolyte interface.

To overcome this limitation, neutron imaging was combined with electrochemical techniques such as EIS and CV. These methods were used to measure the double-layer capacitance, which serves as a proxy for the electrochemical surface area and reflects how well the electrolyte contacts the internal surfaces of the electrode.<sup>157</sup> This novel combination enabled the researchers to obtain a detailed picture of how wetting behavior impacts overall battery performance.

To directly observe microporous mass transport in vanadium-based electrolytes, Tariq *et al.*<sup>158</sup> employed real-time *in situ* X-ray tomography at high resolution. Their work identified mechanisms of electrolyte flow behavior and interactions with porous carbon electrodes during initial wetting. They confirmed that non-uniform infiltration arises from the evolving surface chemistry of carbon fibers, which become more hydrophilic over time. Controlling surface functional groups may enable optimized fluid flow into electrodes, presenting opportunities for tailored electrode designs. These advances in tomographic and radiographic techniques not only enhance the understanding of structural and transport phenomena in redox flow batteries but also provide actionable insights for optimizing material properties and operational parameters, thereby paving the way for more efficient and durable energy storage systems.

### 1.11. *In situ* and *in operando* MS

MS allows for *in situ* analysis of gases released from the RFB cells while being operated. Typically, the gases evolving from the working electrode are collected in an upside-down funnel



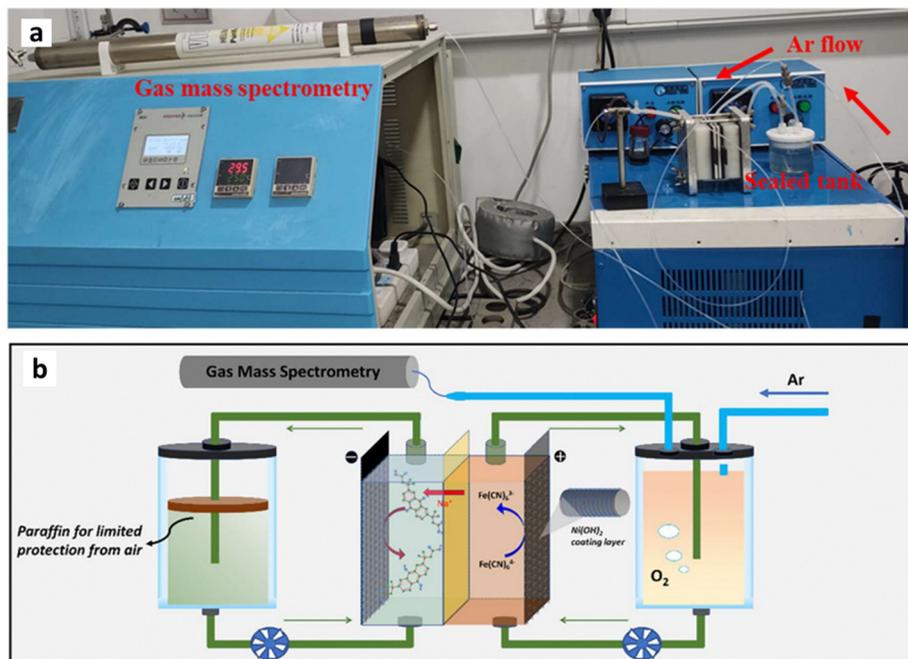


Fig. 13 (a) Device and (b) schematic of a flow battery single cell linked to a mass spectrometer.<sup>159</sup> Reproduced with permission from Wiley-VCH, Copyright 2022.

above the electrode with the rim of the funnel just below the surface of the electrolyte. Using helium or argon as carrier gases the gaseous products can be transported into the mass spectrometer. The partial pressure of the produced gases can be monitored as a function of time and subsequently quantified. A scheme showing the elements is depicted in Fig. 13.<sup>159</sup>

While selectivity and sensitivity are major advantages of MS for analysis of mixtures of products from chemical processes in RFBs, time delay between sampling and detection due to sample transfer to the mass spectrometer represents a limitation for real-time monitoring applications or detection of time-evolving products. Gas evolution typically occurs on the electrode surface due to undesired secondary reactions such as decomposition of the electrolyte or degradation of the electrodes during operation of the RFB and hence it is important to be evaluated. Thus, Liu *et al.*<sup>57</sup> conducted an on-line MS study of the electrochemical corrosion of the graphite electrode for VRFB. By monitoring and analyzing the composition of the gases evolved from the graphite anode during anodic polarization in 2 M H<sub>2</sub>SO<sub>4</sub> + 2 M VOSO<sub>4</sub>, it was possible to gain insight into the electrochemical corrosion of the graphite electrode for VRB. Evolved gases were collected in an upside-down funnel placed above the electrode with the rim of the funnel just below the electrolyte surface and carried by helium gas to the mass spectrometer. The results showed preferred formation of CO<sub>2</sub> and CO over O<sub>2</sub> on the graphite anode due to electrochemical corrosion of the graphite electrode. The investigation also revealed that the O<sub>2</sub> evolution rate is the highest one among all evolved gases if the polarization potential becomes > 1.8 V. Oxidation of VO<sup>2+</sup> to VO<sub>2</sub><sup>+</sup> on the graphite electrode in the electrolyte with high concentration of VO<sup>2+</sup> hindered carbon

oxidation reaction, retarding the electrochemical corrosion of the graphite electrode. Overall, the results highlight the power of on-line MS to characterize reaction products of parasitic reactions at the electrodes.

Later on, Sun *et al.*<sup>74</sup> demonstrated that MS can be a quantitative technique to determine the hydrogen evolution rate occurring at the negative carbon electrode of a VRFB. Samples were collected using a gas tight syringe flushed with argon gas prior to sampling and immediately injected into the mass spectrometer through a septum into the helium gas carrier. MS measurements confirmed that the evolved gas was primarily hydrogen and allowed quantifying the evolution rate. The performance of two types of carbon papers as electrodes was compared, concluding that the higher surface area electrode led to a higher hydrogen evolution rate.

More recently, operando MS experiments were performed *in situ* using a custom-made two-compartment electrochemical cell (H-cell) connected to an online electrochemical MS system to explore reaction products and intermediates during cycling of different organic electrolytes, such as anthraquinone derivatives<sup>59</sup> and bispyridinium compounds.<sup>99</sup> To sample the headspace of the anolyte in both works, the top plunger of the anolyte compartment of the designed cell was fitted with two stainless steel tubes connected to a gas line through double-shut-off quick connects. The flow of the argon carrier gas was controlled by a mass-flow controller and a pressure controller. After passing through the headspace of the anolyte, the sample gas was fed to the mass spectrometer through a heated capillary to prevent condensation. In the former report, evolution of D<sub>2</sub> during a stepped-potential experiment in DHAQ anolyte was



monitored, which was attributed to water reduction by reaction with reduced DHAQ, according to the reaction.<sup>59</sup>



In the latter work, online MS revealed a sharp steady-state decrease in oxygen partial pressure in the headspace above a bispyridinium electrolyte solution during charging under a continuous flow of 1% O<sub>2</sub> in Ar.<sup>99</sup> This oxygen consumption and the lack of change in the hydrogen partial pressure during operation indicated that the pH increase noted during cycling was linked to consumption of gaseous oxygen instead of water splitting, with reduced bispyridinium species facilitating this process. That is, MS combined with EPR findings allowed these authors to identify as a parasitic process, the reduction of trace dissolved oxygen to hydroxide anions mediated by the reduced bispyridinium anolyte.

### 1.12. *In situ* and *in operando* fluorescence microscopy

Optical fluorescence microscopy has been demonstrated to provide both high spatial and temporal resolution in monitoring redox-dependent fluorescence within flowing electrolytes.<sup>76</sup> By coupling fluorescence microscopy with electrochemistry, a direct observation of redox-active quinones' reactions and transport within porous carbon electrodes in real-time was performed.<sup>75</sup> The cell design needs to accomplish optical transparency, which is realized by using transparent polymeric materials such as polyacrylics. A scheme of a microfluidic setup is depicted in Fig. 14.<sup>160</sup>

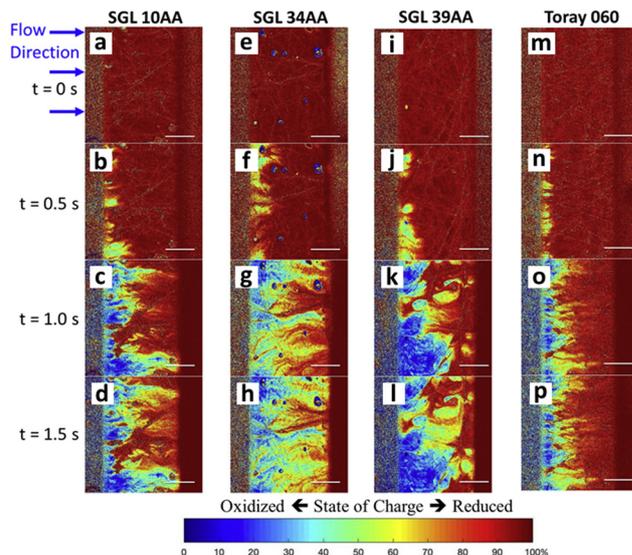


Fig. 15 Time-based advection profile of 4 carbon paper electrodes across the middle land (a)–(p). The AQDS electrolyte is fully reduced (red) within the cell at  $t = 0$ . Fully oxidized electrolyte (blue) is then forced through the cell with a syringe pump at  $100 \text{ mL h}^{-1}$ . Scale bars, 1 mm.<sup>75</sup> Reproduced with permission. Copyright 2021, Cell Press.

Surprisingly, several porous electrodes exhibited electrolyte channeling, creating distinct regions dominated by advection and diffusion. For instance, Fig. 15 illustrates fluid flow dynamics of fully reduced H<sub>2</sub>AQDS (red) and fully oxidized AQDS (blue) electrolytes within 4 types of electrodes. Non-

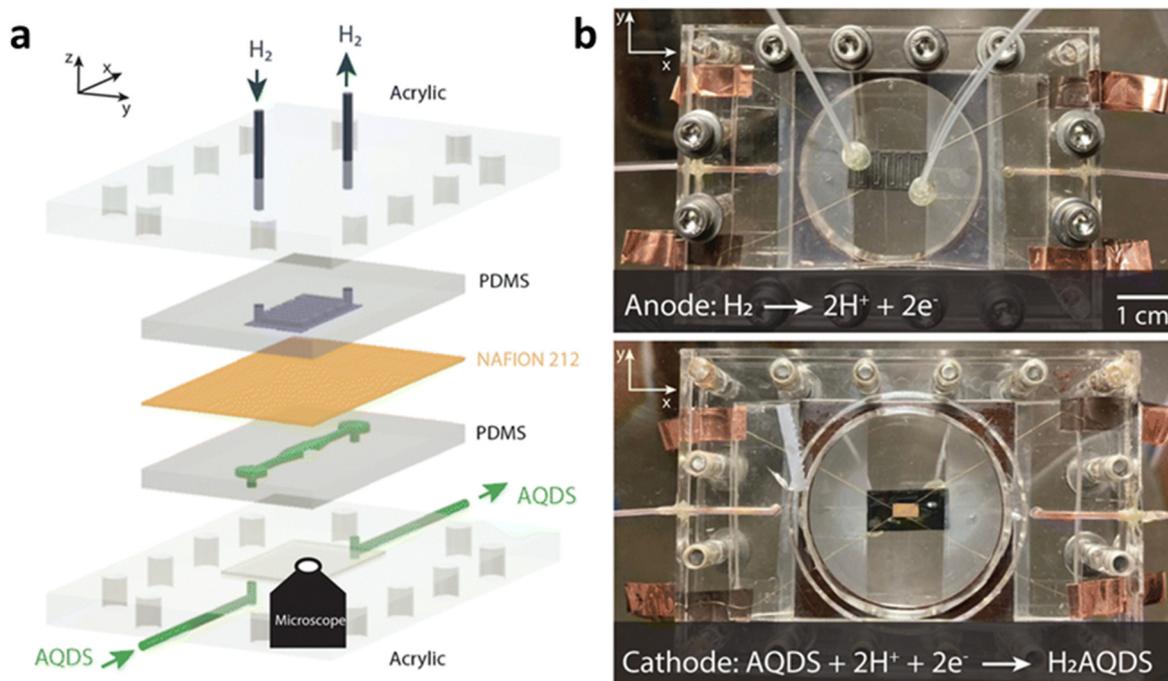


Fig. 14 Microfluidic flow cell compatible with electrochemistry and confocal microscopy. (a) Scheme of the individual components. (b) Photographs of the assembled cell from above (top) and below (bottom). The working electrode ( $3 \times 6 \text{ mm}^2$ ) is visible in the center of the bottom image. For the bottom picture a working electrode made of gold was used to ensure visibility against the counter electrode in the background.<sup>160</sup> Reproduced with permission. Copyright 2024, RSC Publication.



uniform flow is observed, with stagnant regions (red) where  $\text{H}_2\text{AQDS}$  persists due to diffusion-dominated transport. These variations in flow patterns across different electrode designs highlight significant differences in mass transport properties, even among electrodes with similar physical characteristics. This finding challenges the typical assumption that transport in porous electrodes can be modeled with homogeneous Darcy-like permeability, especially at length scales critical to systems like redox flow batteries. This research introduced a new methodology for gaining detailed spatial and temporal insights into electrolyte reactions and transport behaviors within porous electrodes.<sup>75</sup>

*In operando* quantitative electrochemical fluorescence state of charge mapping (QEFSM), a non-invasive method for studying active electrochemical systems has also been reported. This approach was complemented by a novel design of optically transparent microfluidic redox flow cells. QEFSM enabled quantitative mapping of the concentration of specific oxidation states of redox-active species within a porous electrode during its operation. In particular, confocal microscopy to map the fluorescence signal of the reduced form of 2,7-anthraquinone disulfonate (AQDS) in a series of multistep chronoamperometry experiments was employed.<sup>76,160</sup> A similar concept was exploited for electrokinetic investigations of the 5,10-bis(2-methoxyethyl)-5,10-dihydrophenazine (BMEPZ) catholyte, recently proposed as a high-performance multiredox organic molecule. By leveraging BMEPZ's inherent colorimetric properties, the study revealed the intrinsic electrochemical properties in terms of charge and mass transfer kinetics during the multiredox reaction. This was achieved through *in operando* visualization, allowing for a theoretical examination of physicochemical hydrodynamics in electrochemical systems. Based on insights into electrokinetic limitations in RFBs, the study validated an electrode geometry design that minimized the depletion region, leading to enhanced cell performance.<sup>161</sup>

### 1.13. Other analytics

Next to the more common analytics, *in operando* techniques also include the measurement of the acoustic attenuation coefficient with an ultrasonic probing system to determine the SoC.<sup>162</sup> The acoustic attenuation coefficient is only little affected by temperature variations, making it reliable for applications where temperature control is challenging. Hydrogen evolution is a significant side reaction in VRFBs affecting long-term cycling, which has also been addressed using a noninvasive ultrasonic probing method. This online technique monitors the SoC, predicts hydrogen generation, and detects hydrogen gas bubbles in anolyte solutions through a pulse-echo method that measures sound speed and the acoustic attenuation coefficient.<sup>163</sup> In both static offline and online *in operando* experiments, hydrogen gas presence led to notable changes in these measurements. Variations in the acoustic attenuation coefficient were highly correlated with gas flow rates. This method provides insights into the SoC and health of flow battery systems during operation.

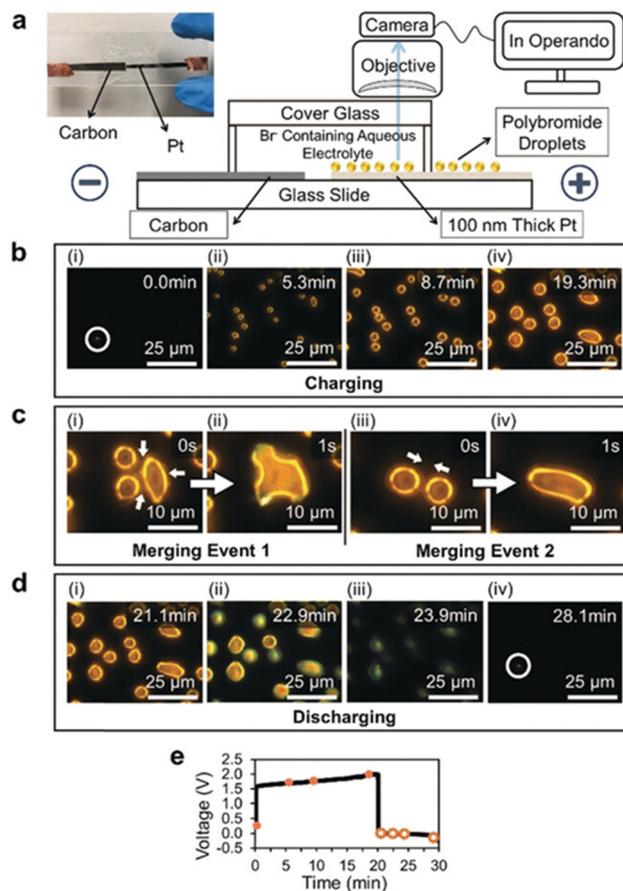


Fig. 16 (a) Schematic representation of the cell and microscope for the *in operando* visualization of bromine electrochemistry. Inset: Photograph of the setup. (b) Time-lapse DFLM images showing the formation of polybromide droplets upon charging. (c) Two sets of images recording the rapid merging of polybromide droplets, indicating their liquid nature. (d) Time-lapse DFLM images during discharging of the same cell as in (b).<sup>164</sup> Reproduced with permission. Copyright 2019, Wiley-VCH.

By employing a platform that combines dark-field light microscopy (DFLM) with a transparent electrochemical cell (Fig. 16a), Wu *et al.*<sup>164</sup> investigated a zinc-bromine RFB and were able to observe the dynamics of polybromide formation in their native environment, capturing key phenomena such as the liquid nature of the charge products, their nucleation and growth behaviors, and interactions with the Pt electrode surface.<sup>164</sup> Using a small current density ( $0.066 \text{ mA cm}^{-1}$ ), sparsely distributed polybromide products were generated for easy tracing (Fig. 16b). A surface defect (circled in Fig. 16b(i)) ensured consistent focus during the experiment. At 5 minutes, yellow spherical microstructures ( $2\text{--}3 \mu\text{m}$  in size) are formed on the Pt surface and grew to approximately  $10 \mu\text{m}$  by the end of the charging process (Fig. 16b(iv)). Neighboring droplets merged into larger ones to minimize surface energy (Fig. 16c(i, ii) and Fig. 16c(iii, iv)), showcasing their liquid nature, as evidenced by rapid merging ( $<1 \text{ s}$ ) and shape relaxation. During discharge (Fig. 16d(i–iv)), the droplets were reduced to  $\text{Br}^-$  ions, shrinking anisotropically by maintaining lateral dimensions



while decreasing in thickness. They gradually became transparent (Fig. 9d(iii)) before disappearing (Fig. 16d(iii)).

This DFLM approach also provided insights into critical issues like self-discharge and overcharging-induced side reactions, enhancing the understanding of complexing agents' roles and guiding future zinc-bromine RFB design improvements. Thus, it enables a deeper mechanistic understanding of electrochemical systems that are otherwise difficult to analyze due to sensitivity to environmental conditions.<sup>146</sup>

A novel imaging-based diagnostic approach for VRFBs was introduced by Ma *et al.*<sup>165</sup> who developed a total internal reflection imaging (TIRi) sensor capable of mapping local electrochemical activity and reversibility on graphite felt electrodes with single-fiber resolution ( $\sim 16 \mu\text{m}$ ). The TIRi system detects changes in refractive index at the electrolyte-electrode interface caused by redox reactions during CV, allowing quantification of peak oxidation and reduction currents, the reversibility ratio, and peak potential separation ( $\Delta E$ ). Their method successfully distinguished the electrochemical performance of pristine, thermally treated, and porous graphite felts, showing that higher surface area and activation improved both activity and uniformity. Beyond static mapping, the system captured dynamic bubble formation from oxygen evolution reaction (OER) in real-time, correlating bubble growth kinetics with cycle number and electrode surface characteristics. Importantly, the technique enabled spatial correlation between bubble generation zones and regions with high local activity and large  $\Delta E$ , linking overpotential-induced side reactions (like OER) directly to inhomogeneous electrode behavior. This visualization capability supports the identification of degradation hotspots and facilitates design improvements in electrode architecture and flow field management.<sup>165</sup> The TIRi method represents a significant advancement in non-invasive, high-resolution, *in situ* characterization tools for understanding spatially resolved kinetics in VRFBs.

Recent progress in *in situ* electrolyte diagnostics has introduced refractive index (RI) monitoring as a powerful tool for real-time assessment of VRFB health. Vlasov *et al.*<sup>166</sup> proposed a Fresnel-based optical RI sensor integrated with an OCV cell to determine the electrolyte's SoH without relying on cycling history. By measuring RI shifts at fixed OCV points (particularly around 1.4 V), and applying a linear calibration model, they achieved a mean prediction error as low as 1.83%, with a maximum root mean square error of 4.45%. The sensor, based on reflection coefficient measurements at the fiber-electrolyte interface, is compact, calibration-friendly, and does not require bypass channels or spectral deconvolution, making it suitable for industrial VRFB monitoring systems. Notably, their method proved sensitive to the effects of vanadium ion crossover, preferential water transfer, and imbalance processes that typically distort coulomb-based SoH estimation. A major practical outcome of this method is its ability to predict capacity fading or trigger rebalance operations mid-cycle, using instantaneous OCV and RI values, thus enabling predictive maintenance and dynamic adjustment of operational protocols. This innovation adds a valuable dimension to *in operando* flow battery

diagnostics and has strong implications for electrolyte rebalancing strategies and smart battery management systems.

## 2. Perspectives and future challenges

In the past ten years, exciting developments have been made in the field of *in situ* and *in operando* techniques for RFB analytics. Much of that progress has been inspired by the rapid development of lithium battery technology concomitant with the need to understand degradation processes. Still, the main challenge in RFBs is to ensure long term stability (20 years+) without substantial degradation of any of the battery components, which is hardly achieved for any flow battery chemistry so far. This point is important for various reasons but the major factor is that flow batteries feature high capital costs, requiring trust of the consumers to invest in the future. Therefore, longevity of the battery system is a must to mass-commercialize this technology. While *in operando* technologies just emerged in the RFB field about ten years ago, they mostly have been employed in lab scale single cell systems. While there has been a lot of progress here, there are still multiple challenges and further developments necessary, particularly with respect to novel battery chemistries and the need for improved analysis methods. Novel chemistries may open new ways of analysis for *in operando* studies. For example, novel redox active molecules carrying NMR active nuclei such as <sup>31</sup>P have been very recently used as probes to study decomposition pathways *ex situ* and it is obvious that *in operando* setups can be employed for analysis of these systems as well.<sup>45,120,167,168</sup> Like that, also redox active molecules carrying NMR active <sup>19</sup>F may be feasible in future RFB technology. Future improvements in imaging techniques or integrating composite absorption with phase contrast methodologies may overcome limitations concerning the distinction between electrolyte and carbon felts due to their similar attenuation coefficients.<sup>169</sup> Again, the introduction of markers with high atomic number (*e.g.*, iodine) may be a strategy to allow the study of deposits or reactions taking place at the felt and to investigate the effect of compression on electrolyte flow. While it is highly important to understand the underlying processes and phenomena on a single cell level, in the operation of a real battery, there are additional effects contributing to the complexity of the system (*e.g.*, shunt currents).<sup>170</sup> A next logical step is therefore to explore multi-cell setups, employing the toolbox developed by researchers in the past years. It is obvious that such studies are more challenging to perform and will require even more engineering efforts and further adaptation of setups and experiments than needed already for single cell setups. In addition, parameters such as pressure drop and flow factor can play, depending on the used chemistry, a more important role in multicell setups.<sup>171</sup> While these approaches are following engineering logics, the use of artificial intelligence (AI) will probably allow to make progress in the analysis and the design of *in operando* techniques.<sup>172,173</sup> So far designs have been based on classic engineering approaches. The adaptation of AI based methods in the design of novel *in operando*



setups is not a question of if, but when. AI derived inputs could comprise the design of novel sensor geometries, as well as experiments to monitor the battery. In addition, AI based methods may be used in data analysis to unravel non-linear correlations difficult for humans to recognize. AI applications in that field, however, must also overcome challenges related to experimental validation and computational costs. Overall, the use of AI based methods will not be the holy grail to solve the challenges of RFB technology development, but it will make a substantial contribution to advance the field in the years to come.

Future research should prioritize the development of instrumentation such as customized flow cell setups specifically designed for easier integration/coupling into RFBs with minimal interference with battery components. Addressing issues of sensitivity, calibration, and real-time adaptability will be crucial to advance these *in situ* and *in operando* methods and realize their full potential as tools for improving RFB performance at industrial scales.

### 3. Conclusion

To accelerate the large-scale industrial adaptation of RFBs, *in situ* and *in operando* analyses are crucial for unraveling complex electrochemical and chemical processes, which enable improvements in efficiency and battery lifespan. Although real-time analytical methods have been widely applied to LIBs, they remain moderately explored in RFBs. Notably, the majority of *in situ* and *in operando* studies on RFBs have emerged only since 2013. By reviewing the literature, we have tracked advancements of these techniques and their impact on RFB optimization.

*In situ* and *in operando* NMR have emerged as powerful tools, enabling researchers to monitor the formation of diamagnetic intermediate species in the electrolyte during battery operation, and to elucidate electrolyte composition changes in response to voltage variations. One significant challenge with NMR, however, is the complexity of integrating the RFB cell into the probe, making real-time monitoring difficult. EPR serves as an excellent complementary technique to NMR for tracking paramagnetic species. Like NMR, it also faces challenges in integrating operational cells. The use of UV-vis spectroscopy has proven to be a powerful tool for real-time monitoring of both SoC and total concentration of active electrolyte species, both in VRFBs and ORFBs. However, highly concentrated systems and light-absorbing solvents may introduce challenges. Raman spectroscopy, despite its power for monitoring electrode surfaces, electrolyte composition and catalytic reactions, faces shortcomings due to limited sensitivity, resolution, and background noise, often requiring enhancement techniques for broader application. Similarly, FTIR spectroscopy is useful for probing electrochemical mechanisms but often requires complex ATR-FTIR electrochemical setups. X-ray-based techniques, such as XAS, can provide valuable insights into the structure of both the electrolyte and electrode surfaces, though high-cost infrastructures and limited sensitivity to light atoms

constrain their widespread use. EIS offers details on the SoH of the battery as well as helps to analyze voltage losses in the battery systems to determine limiting factors, though it is restricted by the frequency range and low resolution at low frequencies. Advanced imaging techniques such as tomography and radiography allow for high-resolution 3D imaging of electrode structures, dendrite formation, and concentration gradients. MS enables the characterization of reaction products and intermediates in the electrolyte but is costly and requires customized sampling systems. Finally, fluorescence microscopy provides a unique approach for tracking redox-active species concentration and mass transport phenomena but requires fluorescent redox-active species.

Each of the presented techniques provides important insights into different aspects of RFB working mechanisms. However, challenges such as instrumentation complexity, cost, and integration into *in situ* and *in operando* setups remain. Future developments to address integration and sensitivity challenges are thus crucial for optimizing RFB performance and enabling large scale industrial implementation.

### Abbreviations

AI	Artificial intelligence
ATR-FTIR	Attenuated total reflection Fourier transform infrared spectroscopy
BE	Bulk electrolysis
CE	Counter electrode
CT	Computed tomography
CV	Cyclic voltammetry
DFLM	Dark-field light microscopy
DFT	Density functional theory
DRT	Distribution of relaxation times
EIS	Electrochemical impedance spectroscopy
EPR	Electron paramagnetic resonance
EXAFS	X-ray absorption fine structure
FTIR	Fourier transform infrared spectroscopy
LIBs	Lithium-ion batteries
MB	Methylene blue
MRI	Magnetic resonance imaging
MS	Mass spectrometry
NMR	Nuclear magnetic resonance
OCV	Open circuit voltage
OER	Oxygen evolution reaction
QEFMS	Fluorescence state of charge mapping
RE	Reference electrode
RFBs	Redox flow batteries
RI	Refractive Index
RMFBs	Redox-mediated flow batteries
SERS	Surface-enhanced Raman spectroscopy
SHE	Standard hydrogen electrode
SoC	State-of-charge
SoH	State-of-health
TERS	Tip-enhanced Raman spectroscopy
TIRI	Total internal reflection imaging



UV-vis	Ultraviolet-visible
VRFBs	Vanadium redox flow batteries
XANES	X-ray absorption near edge structure
XAS	X-ray absorption spectroscopy
XPS	X-ray photoelectron spectroscopy
WE	Working electrode
ZMRFB	Zn-Mn <sup>2+</sup> /MnO <sub>2</sub> RFB

## Data availability

This review paper does not contain original research data. Figures and schemes are adapted with permission from research papers accessible *via* DOI which may be requested by the corresponding authors.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

The authors gratefully acknowledge funding from the European Innovation Council (EIC) under grant agreements No. 101115293 (VanillaFlow) and No. 101046742 (MeBattery), and by the Spanish Government (Ministerio de Ciencia e Innovación, Grant PID2021-124974OB-C22).

## References

- M. Pan, M. Shao and Z. Jin, *SmartMat*, 2023, **4**, e1198.
- X. Wei, W. Pan, W. Duan, A. Hollas, Z. Yang, B. Li, Z. Nie, J. Liu, D. Reed, W. Wang and V. Sprenkle, *ACS Energy Lett.*, 2017, **2**, 2187–2204.
- A. Khataee, J. Azevedo, P. Dias, D. Ivanou, E. Dražević, A. Bentien and A. Mendes, *Nano Energy*, 2019, **62**, 832–843.
- W. Schlemmer, P. Nothdurft, A. Petzold, G. Riess, P. Frühwirt, M. Schmallegger, G. Gescheidt-Demner, R. Fischer, S. A. Freunberger, W. Kern and S. Spirk, *Angew. Chem., Int. Ed.*, 2020, **59**, 22943–22946.
- K. Teenakul, S. A. Ahmad Alem, R. Gond, A. Thakur, B. Anasori and A. Khataee, *RSC Adv.*, 2024, **14**, 12807–12816.
- M. Wu, M. Bahari, Y. Jing, K. Amini, E. M. Fell, T. Y. George, R. G. Gordon and M. J. Aziz, *Batteries Supercaps*, 2022, **5**, e202200009.
- M. Shoaib, P. Vallayil, N. Jaiswal, P. Iyapazham Vaigunda Suba, S. Sankararaman, K. Ramanujam and V. Thangadurai, *Adv. Energy Mater.*, 2024, **14**, 2400721.
- Z. Hou, X. Chen, J. Liu, Z. Huang, Y. Chen, M. Zhou, W. Liu and H. Zhou, *J. Power Sources*, 2024, **601**, 234242.
- E. Ventosa, *Curr. Opin. Chem. Eng.*, 2022, **37**, 100834.
- C. Santana Santos, T. Quast, E. Ventosa and W. Schuhmann, *ChemElectroChem*, 2024, **11**, e202400283.
- Y. Shen, S. Wang, H. Li, K. Wang and K. Jiang, *J. Energy Storage*, 2023, **64**, 107164.
- Y. Yang, J. Feijóo, V. Briega-Martos, Q. Li, M. Krumov, S. Merckens, G. Salvo, A. Chuvilin, J. Jin, H. Huang, C. J. Pollock, M. B. Salmeron, C. Wang, D. A. Muller, H. D. Abruña and P. Yang, *Curr. Opin. Electrochem.*, 2023, **42**, 101403.
- B. J. Neyhouse, K. M. Tenny, Y.-M. Chiang and F. R. Brushett, *ACS Appl. Energy Mater.*, 2021, **4**, 13830–13840.
- R. Zeis, in *Flow Batteries: From Fundamentals to Applications*, ed. C. Roth, J. Noack and M. Skyllas-Kazacos, Wiley-VCH GmbH, 2023, pp. 263–280.
- Z. Sun, J. Pan, W. Chen, H. Chen, S. Zhou, X. Wu, Y. Wang, K. Kim, J. Li, H. Liu, Y. Yuan, J. Wang, D. Su, D.-L. Peng and Q. Zhang, *Adv. Energy Mater.*, 2024, **14**, 2303165.
- M. T. Shuja, S. Thatipamula, M. W. Khan, M. Haris, R. Babarao and N. Mahmood, *Battery Energy*, 2024, **3**, 20230043.
- R. A. Vicente, I. T. Neckel, S. K. R. S. Sankaranarayanan, J. Solla-Gullon and P. S. Fernández, *ACS Nano*, 2021, **15**, 6129–6146.
- M. Sathiya, J.-B. Leriche, E. Salager, D. Gourier, J.-M. Tarascon and H. Vezin, *Nat. Commun.*, 2015, **6**, 6276.
- L. Xue, Y. Li, A. Hu, M. Zhou, W. Chen, T. Lei, Y. Yan, J. Huang, C. Yang, X. Wang, Y. Hu and J. Xiong, *Small Struct.*, 2022, **3**, 2100170.
- M. M. Amaral, C. G. Real, V. Y. Yukuhiro, G. Doubek, P. S. Fernandez, G. Singh and H. Zanin, *J. Energy Chem.*, 2023, **81**, 472–491.
- J.-H. Tian, T. Jiang, M. Wang, Z. Hu, X. Zhu, L. Zhang, T. Qian and C. Yan, *Small Methods*, 2020, **4**, 1900467.
- L. Meyer, N. Saqib and J. Porter, *J. Electrochem. Soc.*, 2021, **168**, 90561.
- M. B. Dixit, J.-S. Park, P. Kenesei, J. Almer and K. B. Hatzell, *Energy Environ. Sci.*, 2021, **14**, 4672–4711.
- H. Li, S. Guo and H. Zhou, *J. Energy Chem.*, 2021, **59**, 191–211.
- D. Liu, Z. Shadik, R. Lin, K. Qian, H. Li, K. Li, S. Wang, Q. Yu, M. Liu, S. Ganapathy, X. Qin, Q.-H. Yang, M. Wagemaker, F. Kang, X.-Q. Yang and B. Li, *Adv. Mater.*, 2019, **31**, e1806620.
- F. Strauss, D. Kitsche, Y. Ma, J. H. Teo, D. Goonetilleke, J. Janek, M. Bianchini and T. Brezesinski, *Adv. Energy Sustainability Res.*, 2021, **2**, 2100004.
- J. Tan, D. Liu, X. Xu and L. Mai, *Nanoscale*, 2017, **9**, 19001–19016.
- E. Šić, D. Fredericks, O. Pecher, S. Wegner, H. Breitzke, V. Singh, G. Buntkowsky and T. Gutmann, *Appl. Magn. Reson.*, 2024, **55**, 575–583.
- O. Pecher, J. Carretero-González, K. J. Griffith and C. P. Grey, *Chem. Mater.*, 2017, **29**, 213–242.
- O. Nolte, I. A. Volodin, C. Stolze, M. D. Hager and U. S. Schubert, *Mater. Horiz.*, 2021, **8**, 1866–1925.
- Y. A. Gandomi, D. S. Aaron, J. R. Houser, M. C. Daugherty, J. T. Clement, A. M. Pezeshki, T. Y. Ertugrul, D. P. Moseley and M. M. Mench, *J. Electrochem. Soc.*, 2018, **165**, A970.
- L. Zhang, R. Feng, W. Wang and G. Yu, *Nat. Rev. Chem.*, 2022, **6**, 524–543.
- P. Arévalo-Cid, P. Dias, A. Mendes and J. Azevedo, *Sustainable Energy Fuels*, 2021, **5**, 5366–5419.



- 34 P. Leung, X. Li, C. Ponce de León, L. Berlouis, C. T. J. Low and F. C. Walsh, *RSC Adv.*, 2012, **2**, 10125–10156.
- 35 E. Sánchez-Díez, E. Ventosa, M. Guarnieri, A. Trovò, C. Flox, R. Marcilla, F. Soavi, P. Mazur, E. Aranzabe and R. Ferret, *J. Power Sources*, 2021, **481**, 228804.
- 36 M. Skyllas-Kazacos, L. Cao, M. Kazacos, N. Kausar and A. Mousa, *ChemSusChem*, 2016, **9**, 1521–1543.
- 37 J. Ren, Y. Li, Z. Wang, J. Sun, Q. Yue, X. Fan and T. Zhao, *Int. J. Heat Mass Transfer*, 2023, **203**, 123818.
- 38 D. I. Kushner, A. R. Crothers, A. Kusoglu and A. Z. Weber, *Curr. Opin. Electrochem.*, 2020, **21**, 132–139.
- 39 D. G. Kwabi, Y. Ji and M. J. Aziz, *Chem. Rev.*, 2020, **120**, 6467–6489.
- 40 T. A. Hamlin, M. Swart and F. M. Bickelhaupt, *Chem-PhysChem*, 2018, **19**, 1315–1330.
- 41 D. P. Tabor, R. Gómez-Bombarelli, L. Tong, R. G. Gordon, M. J. Aziz and A. Aspuru-Guzik, *J. Mater. Chem. A*, 2019, **7**, 12833–12841.
- 42 C. L. Bird and A. T. Kuhn, *Chem. Soc. Rev.*, 1981, **10**, 49–82.
- 43 R. Rubio-Presa, L. Lubián, M. Borlaf, E. Ventosa and R. Sanz, *ACS Mater. Lett.*, 2023, **5**, 798–802.
- 44 A. Orita, M. G. Verde, M. Sakai and Y. S. Meng, *J. Power Sources*, 2016, **321**, 126–134.
- 45 M. Egger, I. Koehne, D. Wickenhauser, W. Schlemmer, S. Spirk and R. Pietschnig, *ACS Omega*, 2023, **8**, 10899–10905.
- 46 B. Ambrose, R. Naresh, S. Deshmukh, M. Kathiresan and P. Ragupathy, *Energy Fuels*, 2023, **37**, 18226–18242.
- 47 J. Maier, R. Yagmur, D. Wickenhauser, A. Torvisco, A.-M. Kelterer and S. Spirk, *J. Electrochem. Soc.*, 2024, **171**, 116504.
- 48 A. Pasadakis-Kavounis, V. Baj and J. Hjelm, *J. Electrochem. Soc.*, 2024, **171**, 20501.
- 49 C. Wiberg, T. J. Carney, F. Brushett, E. Ahlberg and E. Wang, *Electrochim. Acta*, 2019, **317**, 478–485.
- 50 T. J. Carney, S. J. Collins, J. S. Moore and F. R. Brushett, *Chem. Mater.*, 2017, **29**, 4801–4810.
- 51 Q. Chen, L. Eisenach and M. J. Aziz, *J. Electrochem. Soc.*, 2016, **163**, A5057.
- 52 M. R. Gerhardt, E. S. Beh, L. Tong, R. G. Gordon and M. J. Aziz, *MRS Adv.*, 2017, **2**, 431–438.
- 53 S. Jin, Y. Jing, D. G. Kwabi, Y. Ji, L. Tong, D. Porcellinis, M.-A. Goulet, D. A. Pollack, R. G. Gordon and M. J. Aziz, *ACS Energy Lett.*, 2019, **4**, 1342–1348.
- 54 M.-A. Goulet and M. J. Aziz, *J. Electrochem. Soc.*, 2018, **165**, A1466.
- 55 S. Stefan, F. Belaj, T. Madl and R. Pietschnig, *Eur. J. Inorg. Chem.*, 2010, 289–297.
- 56 O. Nolte, P. Rohland, N. Ueberschaar, M. D. Hager and U. S. Schubert, *J. Power Sources*, 2022, **525**, 230996.
- 57 H. Liu, Q. Xu and C. Yan, *Electrochem. Commun.*, 2013, **28**, 58–62.
- 58 J. Friedl, M. V. Holland-Cunz, F. Cording, F. L. Pfanschilling, C. Wills, W. McFarlane, B. Schrickler, R. Fleck, H. Wolfschmidt and U. Stimming, *Energy Environ. Sci.*, 2018, **11**, 3010–3018.
- 59 E. W. Zhao, T. Liu, E. Jónsson, J. Lee, I. Temprano, R. B. Jethwa, A. Wang, H. Smith, J. Carretero-González, Q. Song and C. P. Grey, *Nature*, 2020, **579**, 224–228.
- 60 Y. Jing, E. W. Zhao, M.-A. Goulet, M. Bahari, E. M. Fell, S. Jin, A. Davoodi, E. Jónsson, M. Wu, C. P. Grey, R. G. Gordon and M. J. Aziz, *Nat. Chem.*, 2022, **14**, 1103–1109.
- 61 E. W. Zhao, E. Jónsson, R. B. Jethwa, D. Hey, D. Lyu, A. Brookfield, P. A. A. Klusener, D. Collison and C. P. Grey, *J. Am. Chem. Soc.*, 2021, **143**, 1885–1895.
- 62 T. C. Gokoglan, S. K. Pahari, A. Hamel, R. Howland, P. J. Cappillino and E. Agar, *J. Electrochem. Soc.*, 2019, **166**, A1745.
- 63 K.-H. Shin, C.-S. Jin, J.-Y. So, S.-K. Park, D.-H. Kim and S.-H. Yeon, *J. Energy Storage*, 2020, **27**, 101066.
- 64 J. Lan, K. Li, L. Yang, Q. Lin, J. Duan, S. Zhang, X. Wang and J. Chen, *ACS Nano*, 2023, **17**, 20492–20501.
- 65 X. Zhang, A. Valencia, W. Li, K. Ao, J. Shi, X. Yue, R. Zhang and W. A. Daoud, *Adv. Mater.*, 2024, **36**, 2305415.
- 66 W. Kautek, A. Conradi, M. Sahre, C. Fabjan, J. Drobits, G. Bauer and P. Schuster, *J. Electrochem. Soc.*, 1999, **146**, 3211.
- 67 S. Huang, H. Zhang, M. Salla, J. Zhuang, Y. Zhi, X. Wang and Q. Wang, *Nat. Commun.*, 2022, **13**, 4746.
- 68 C. Jia, Q. Liu, C.-J. Sun, F. Yang, Y. Ren, S. M. Heald, Y. Liu, Z.-F. Li, W. Lu and J. Xie, *ACS Appl. Mater. Interfaces*, 2014, **6**, 17920–17925.
- 69 F. Paparoni, G. Alizon, A. Zitolo, S. J. Rezvani, A. Di Cicco, H. Magnan and E. Fonda, *Phys. Chem. Chem. Phys.*, 2024, **26**, 3897–3906.
- 70 K. Amini and M. D. Pritzker, *J. Power Sources*, 2020, **471**, 228463.
- 71 E. Ventosa, M. Skoumal, F. J. Vázquez, C. Flox and J. R. Morante, *J. Power Sources*, 2014, **271**, 556–560.
- 72 V. Yuffit, F. Tariq, D. S. Eastwood, M. Biton, B. Wu, P. D. Lee and N. P. Brandon, *Joule*, 2019, **3**, 485–502.
- 73 R. Jervis, L. D. Brown, T. P. Neville, J. Millichamp, D. P. Finegan, T. M. M. Heenan, D. J. L. Brett and P. R. Shearing, *J. Phys. D: Appl. Phys.*, 2016, **49**, 434002.
- 74 C.-N. Sun, F. M. Delnick, L. Baggetto, G. M. Veith and T. A. Zawodzinski, *J. Power Sources*, 2014, **248**, 560–564.
- 75 A. A. Wong, S. M. Rubinstein and M. J. Aziz, *Cell Rep. Phys. Sci.*, 2021, **2**, 100388.
- 76 A. A. Wong, M. J. Aziz and S. Rubinstein, *ECS Trans.*, 2017, **77**, 153.
- 77 P. A. Keifer, in *Annual Reports on NMR Spectroscopy*, ed. G. A. Webb, Academic Press, England, 2007, pp. 1–47.
- 78 F. Dalitz, M. Cudaj, M. Maiwald and G. Guthausen, *Prog. Nucl. Magn. Reson. Spectrosc.*, 2012, **60**, 52–70.
- 79 Z. Zhu, R. Luo and E. W. Zhao, *Magn. Reson. Lett.*, 2024, **4**, 100096.
- 80 M. V. Gomez and A. La Hoz, *Beilstein J. Org. Chem.*, 2017, **13**, 285–300.
- 81 A. Friebe, E. Harbou, K. Münnemann and H. Hasse, *Ind. Eng. Chem. Res.*, 2019, **58**, 18125–18133.
- 82 P. Giraudeau and F.-X. Felpin, *React. Chem. Eng.*, 2018, **3**, 399–413.



- 83 R. Kircher, S. Mross, H. Hasse and K. Münnemann, *Appl. Magn. Reson.*, 2023, **54**, 1555–1569.
- 84 A. Friebel, T. Specht, E. Harbou, K. Münnemann and H. Hasse, *J. Magn. Reson.*, 2020, **312**, 106683.
- 85 N. Zientek, K. Meyer, S. Kern and M. Maiwald, *Chem. Ing. Tech.*, 2016, **88**, 698–709.
- 86 P. A. Keifer, *Curr. Opin. Chem. Biol.*, 2003, **7**, 388–394.
- 87 A. Salgado, in *Liquid Chromatography (Third Edition): Handbooks in Separation Science*, ed. S. Fanali, B. Chankvetadze, P. R. Haddad, C. F. Poole and M.-L. Riekkola, Elsevier, 2023, pp. 743–794.
- 88 R. Kircher, H. Hasse and K. Münnemann, *Anal. Chem.*, 2021, **93**, 8897–8905.
- 89 D. Graafen, S. Ebert, O. Neudert, L. Buljubasich, M. B. Franzoni, J. F. Dechent and K. Münnemann, in *Annual Reports on NMR Spectroscopy*, ed. G. A. Webb, Academic Press, England, 2014, pp. 167–215.
- 90 M. Hunger, *Prog. Nucl. Magn. Reson. Spectrosc.*, 2008, **53**, 105–127.
- 91 Z. Zhao, T. Li, C. Zhang, M. Zhang, S. Li and X. Li, *Nat. Sustainability*, 2024, **7**, 1273–1282.
- 92 B. Wu, R. L. E. G. Aspers, A. P. M. Kentgens and E. W. Zhao, *J. Magn. Reson.*, 2023, **351**, 107448.
- 93 B. Caja-Munoz, K. Chighine, J.-P. Dognon, L. Dubois and P. Berthault, *Anal. Chem.*, 2023, **95**, 6020–6028.
- 94 H. Nguyen and R. J. Clément, *ACS Energy Lett.*, 2020, **5**, 3848–3859.
- 95 X. Sang, X. Xu, Z. Bu, S. Zhai, Y. Sun, M. Ruan and Q. Li, *Magnetochemistry*, 2023, **9**, 63.
- 96 B. Wang, W. Wang, K. Sun, Y. Xu, Y. Sun, Q. Li, H. Hu and M. Wu, *Nano Res.*, 2023, **16**, 11992–12012.
- 97 E. W. Zhao, E. J. K. Shellard, P. A. A. Klusener and C. P. Grey, *Chem. Commun.*, 2022, **58**, 1342–1345.
- 98 R. B. Jethwa, D. Hey, R. N. Kerber, A. D. Bond, D. S. Wright and C. P. Grey, *ACS Appl. Energy Mater.*, 2024, **7**, 414–426.
- 99 M. E. Carrington, K. Sokolowski, E. Jónsson, E. W. Zhao, A. M. Graf, I. Temprano, J. A. McCune, C. P. Grey and O. A. Scherman, *Nature*, 2023, **623**, 949–955.
- 100 R. Feng, X. Zhang, V. Murugesan, A. Hollas, Y. Chen, Y. Shao, E. Walter, N. P. N. Wellala, L. Yan, K. M. Rosso and W. Wang, *Science*, 2021, **372**, 836–840.
- 101 Y. Zhang, F. Li, T. Li, M. Zhang, Z. Yuan, G. Hou, J. Fu, C. Zhang and X. Li, *Energy Environ. Sci.*, 2023, **16**, 231–240.
- 102 J. S. Lawton, A. Jones and T. Zawodzinski, *J. Electrochem. Soc.*, 2013, **160**, A697.
- 103 A. A. Maurice, A. E. Quintero and M. Vera, *Electrochim. Acta*, 2024, **482**, 144003.
- 104 H. Sun, H. Takahashi, N. Nishiumi, Y. Kamada, K. Sato, K. Nedu, Y. Matsushima, A. Khosla, M. Kawakami, H. Furukawa, P. Stadler and T. Yoshida, *J. Electrochem. Soc.*, 2019, **166**, B3125.
- 105 S. V. Modak, D. Pert, J. L. Tami, W. Shen, I. Abdullahi, X. Huan, A. J. McNeil, B. R. Goldsmith and D. G. Kwabi, *J. Am. Chem. Soc.*, 2024, **146**, 5173–5185.
- 106 J. Cao, K. Yu, J. Zhang, B. Lu, J. Yu, S. Huang and F. Zhang, *ACS Sustainable Chem. Eng.*, 2024, **12**, 6320–6329.
- 107 P. Loktionov, R. Pichugov, D. Konev, M. Petrov, A. Pustovalova and A. Antipov, *J. Electroanal. Chem.*, 2022, **925**, 116912.
- 108 L. Tong, Q. Chen, A. A. Wong, R. Gómez-Bombarelli, A. Aspuru-Guzik, R. G. Gordon and M. J. Aziz, *Phys. Chem. Chem. Phys.*, 2017, **19**, 31684–31691.
- 109 S. Park, H. Lee, H. J. Lee and H. Kim, *J. Power Sources*, 2020, **451**, 227746.
- 110 D. Yu, L. Zhi, F. Zhang, Y. Song, Q. Wang, Z. Yuan and X. Li, *Adv. Mater.*, 2023, **35**, 2209390.
- 111 J. Lei, Y. Zhang, Y. Yao, Y. Shi, K. L. Leung, J. Fan and Y.-C. Lu, *Nat. Energy*, 2023, **8**, 1355–1364.
- 112 M. Zhou, Q. Huang, T. N. Pham Truong, J. Ghilane, Y. G. Zhu, C. Jia, R. Yan, L. Fan, H. Randriamahazaka and Q. Wang, *Chem*, 2017, **3**, 1036–1049.
- 113 Y. Chen, M. Zhou, Y. Xia, X. Wang, Y. Liu, Y. Yao, H. Zhang, Y. Li, S. Lu, W. Qin, X. Wu and Q. Wang, *Joule*, 2019, **3**, 2255–2267.
- 114 S. Yan, S. Huang, H. Xu, L. Li, H. Zou, M. Ding, C. Jia and Q. Wang, *ChemSusChem*, 2023, **16**, e202300710.
- 115 S. Liu, L. D'Amario, S. Jiang and H. Dau, *Curr. Opin. Electrochem.*, 2022, **35**, 101042.
- 116 X. Jia, H. Kang, G. Hou, W. Wu, S. Lu, Y. Li, Q. Wang, W. Qin and X. Wu, *Angew. Chem., Int. Ed.*, 2024, **63**, e202318248.
- 117 S. E. J. Bell, G. Charron, E. Cortés, J. Kneipp, M. L. La Chapelle, J. Langer, M. Procházka, V. Tran and S. Schlücker, *Angew. Chem., Int. Ed.*, 2020, **59**, 5454–5462.
- 118 M. D. Sonntag, E. A. Pozzi, N. Jiang, M. C. Hersam and R. P. van Duyne, *J. Phys. Chem. Lett.*, 2014, **5**, 3125–3130.
- 119 Z. Li, G. Weng, Q. Zou, G. Cong and Y.-C. Lu, *Nano Energy*, 2016, **30**, 283–292.
- 120 G. S. Nambafu, A. M. Hollas, P. S. Rice, J. M. Weller, D. Boglaienko, D. M. Reed, V. L. Sprenkle and G. Li, *Adv. Energy Mater.*, 2025, **15**, 2403149.
- 121 H. Radinger, F. Bauer and F. Scheiba, *Batteries Supercaps*, 2023, **6**, e202200440.
- 122 L. Lubian, R. Rubio-Presa, V. Ruiz, A. Colina and E. Ventosa, *J. Power Sources*, 2025, **646**, 237272.
- 123 H. J. Lee, D.-W. Kim and J. H. Yang, *J. Electrochem. Soc.*, 2017, **164**, A754.
- 124 M. Zhou, Y. Chen, M. Salla, H. Zhang, X. Wang, S. R. Mothe and Q. Wang, *Angew. Chem., Int. Ed.*, 2020, **59**, 14286–14291.
- 125 F. Paparoni, E. Mijit, H. Darjazi, F. Nobili, A. Zitolo, A. Di Cicco, R. Parmar, R. Gunnella and S. J. Rezvani, *J. Phys. Chem. C*, 2023, **127**, 8649–8656.
- 126 *Introduction to XAFS: A Practical Guide to X-ray Absorption Fine Structure Spectroscopy*, ed. G. Bunker, Cambridge University Press, Cambridge, 2010.
- 127 S. Mehboob, G. Ali, H.-J. Shin, J. Hwang, S. Abbas, K. Y. Chung and H. Y. Ha, *Appl. Energy*, 2018, **229**, 910–921.
- 128 J. Melke, J. Martin, M. Bruns, P. Hügenell, A. Schökel, S. Montoya Isaza, F. Fink, P. Elsässer and A. Fischer, *ACS Appl. Energy Mater.*, 2020, **3**, 11627–11640.
- 129 G. M. Su, I. A. Cordova, M. A. Yandrasits, M. Lindell, J. Feng, C. Wang and A. Kusoglu, *J. Am. Chem. Soc.*, 2019, **141**, 13547–13561.



- 130 Y. Wen and R. Jarvis, *Curr. Opin. Chem. Eng.*, 2022, **37**, 100836.
- 131 C. Lutz, S. Hampel, S. Beuermann, T. Turek, U. Kunz, J. Garrovoet, G. Falkenberg and U. Fittschen, *J. Synchrotron Radiat.*, 2021, **28**, 1865–1873.
- 132 C. Lutz, S. Hampel, X. Ke, S. Beuermann, T. Turek, U. Kunz, A. Guilherme Buzanich, M. Radtke and U. E. Fittschen, *J. Power Sources*, 2021, **483**, 229176.
- 133 S. Huang, M. Li, Y. Song, S. Xi, C. Wu, Z. W. J. Ang and Q. Wang, *Adv. Mater.*, 2024, **36**, 2406366.
- 134 Y. Cai, H. Zhang, T. Wang, S. Xi, Y. Song, S. Rong, J. Ma, Z. Han, C. T. J. Low, Q. Wang and Y. Ji, *Joule*, 2025, **9**, 101768.
- 135 M. Schilling, M. Braig, K. Köble and R. Zeis, *Electrochim. Acta*, 2022, **430**, 141058.
- 136 J. Schneider, T. Tichter, P. Khadke, R. Zeis and C. Roth, *Electrochim. Acta*, 2020, **336**, 135510.
- 137 T. Tichter, M. Gernhard and P. Vesborg, *Electrochim. Acta*, 2023, **469**, 143119.
- 138 T. Tichter and A. T. Marshall, *Curr. Opin. Electrochem.*, 2022, **34**, 101027.
- 139 F. Ciucci and C. Chen, *Electrochim. Acta*, 2015, **167**, 439–454.
- 140 T. H. Wan, M. Saccoccio, C. Chen and F. Ciucci, *Electrochim. Acta*, 2015, **184**, 483–499.
- 141 M. B. Effat and F. Ciucci, *Electrochim. Acta*, 2017, **247**, 1117–1129.
- 142 J. Liu, T. H. Wan and F. Ciucci, *Electrochim. Acta*, 2020, **357**, 136864.
- 143 A. M. Pezeshki, R. L. Sacci, F. M. Delnick, D. S. Aaron and M. M. Mench, *Electrochim. Acta*, 2017, **229**, 261–270.
- 144 E. H. Kirk, F. Fenini, S. N. Oreiro and A. Bentien, *Batteries*, 2021, **7**, 87.
- 145 T. Lemmermann, M. Becker, M. Stehle, M. Drache, S. Beuermann, M. S. Bogar, U. Gohs, U. E. Fittschen, T. Turek and U. Kunz, *J. Power Sources*, 2022, **533**, 231343.
- 146 H. Lim, J. S. Yi and D. Lee, *ChemSusChem*, 2019, **12**, 1459–1468.
- 147 H. Lim, J. S. Yi and D. Lee, *J. Power Sources*, 2019, **422**, 65–72.
- 148 Z. Wang, Y. Li, J. Ren, J. Sun, T. Wang, B. Liu, X. Fan and T. Zhao, *Cell Rep. Phys. Sci.*, 2023, **4**, 101395.
- 149 I. A. Volodin, C. Stolze, C. Casas Mesa, U. Haagen, C. Terechin, M. D. Hager and U. S. Schubert, *Sens. Actuators, B*, 2024, **403**, 135101.
- 150 E. Schröter, C. Stolze, J. Meyer, M. D. Hager and U. S. Schubert, *ChemSusChem*, 2023, **16**, e202300296.
- 151 P. Loktionov, D. Konev, R. Pichugov, M. Petrov and A. Antipov, *J. Power Sources*, 2023, **553**, 232242.
- 152 T. Haisch, H. Ji and C. Weidlich, *Electrochim. Acta*, 2020, **336**, 135573.
- 153 M. R. Mohamed, H. Ahmad and M. N. Abu Seman, *Elektron. Elektrotech.*, 2013, **19**, 37–42.
- 154 R. Jarvis, M. D. Kok, T. P. Neville, Q. Meyer, L. D. Brown, F. Iacoviello, J. T. Gostick, D. J. Brett and P. R. Shearing, *J. Energy Chem.*, 2018, **27**, 1353–1361.
- 155 M. Gebhard, T. Tichter, J. Schneider, J. Mayer, A. Hilger, M. Osenberg, M. Rahn, I. Manke and C. Roth, *J. Power Sources*, 2020, **478**, 228695.
- 156 R. R. Jacquemond, M. van der Heijden, E. B. Boz, E. R. Carreón Ruiz, K. V. Greco, J. A. Kowalski, V. Muñoz Perales, F. R. Brushett, K. Nijmeijer, P. Boillat and A. Forner-Cuenca, *Nat. Commun.*, 2024, **15**, 7434.
- 157 E. B. Boz, M. van der Heijden, R. R. Jacquemond, P. Boillat, J. Hjelm and A. Forner-Cuenca, *J. Electrochem. Soc.*, 2024, **171**, 53509.
- 158 F. Tariq, J. Rubio-Garcia, V. Yufit, A. Bertei, B. K. Chakrabarti, A. Kucernak and N. Brandon, *Sustainable Energy Fuels*, 2018, **2**, 2068–2080.
- 159 T. Kong, J. Liu, X. Zhou, J. Xu, Y. Xie, J. Chen, X. Li and Y. Wang, *Angew. Chem., Int. Ed.*, 2023, **62**, e202214819.
- 160 A. M. Graf, T. Cochard, K. Amini, M. S. Emanuel, S. M. Rubinstein and M. J. Aziz, *Energy Adv.*, 2024, **3**, 2468–2478.
- 161 H. Park, G. Kwon, H. Lee, K. Lee, S. Y. Park, J. E. Kwon, K. Kang and S. J. Kim, *Proc. Natl. Acad. Sci. U. S. A.*, 2022, **119**, e2114947119.
- 162 X. Zang, L. Yan, Y. Yang, H. Pan, Z. Nie, K. W. Jung, Z. D. Deng and W. Wang, *Small Methods*, 2019, **3**, 1900494.
- 163 L. Yan, X. Zang, Z. Nie, L. Zhong, Z. D. Deng and W. Wang, *J. Power Sources*, 2023, **580**, 233417.
- 164 Y. Wu, P.-W. Huang, J. D. Howe, Y. Yan, J. Martinez, A. Marianchuk, Y. Zhang, H. Chen and N. Liu, *Angew. Chem., Int. Ed.*, 2019, **58**, 15228–15234.
- 165 K. Ma, Y. Zhang, L. Liu, J. Xi, X. Qiu, T. Guan and Y. He, *Nat. Commun.*, 2019, **10**, 5286.
- 166 V. I. Vlasov, M. A. Pugach, D. S. Kopylova, A. V. Novikov, N. A. Gvozdik, A. A. Mkrtychyan, A. I. Davletkhanov, Y. Gladush, F. M. Ibanez, D. A. Gorin and K. J. Stevenson, *J. Power Sources*, 2023, **584**, 233600.
- 167 G. S. Nambafu, A. M. Hollas, S. Zhang, P. S. Rice, D. Boglajenko, J. L. Fulton, M. Li, Q. Huang, Y. Zhu, D. M. Reed, V. L. Sprenkle and G. Li, *Nat. Commun.*, 2024, **15**, 2566.
- 168 Y. Ji, M.-A. Goulet, D. A. Pollack, D. G. Kwabi, S. Jin, D. Porcellinis, E. F. Kerr, R. G. Gordon and M. J. Aziz, *Adv. Energy Mater.*, 2019, **9**, 1900039.
- 169 J. T. Lang, D. Kulkarni, C. W. Foster, Y. Huang, M. A. Sepe, S. Shimpalee, D. Y. Parkinson and I. V. Zenyuk, *Chem. Rev.*, 2023, **123**, 9880–9914.
- 170 S. Prakash Yadav, M. K. Ravikumar, S. Patil and A. Shukla, *ChemElectroChem*, 2024, **11**, e202400267.
- 171 H. Chen, S. Wang, H. Gao, X. Feng, C. Yan and A. Tang, *J. Power Sources*, 2019, **427**, 154–164.
- 172 S. Wan, H. Jiang, Z. Guo, C. He, X. Liang, N. Djilali and T. Zhao, *Energy Environ. Sci.*, 2022, **15**, 2874–2888.
- 173 T. Li, C. Zhang and X. Li, *Chem. Sci.*, 2022, **13**, 4740–4752.

