

## PAPER

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15, 2175Design and catalytic performance investigation of  
the Ni–N–C catalyst for CO<sub>2</sub>RR: a theoretical  
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The combustion of fossil fuels is increasingly contributing to global warming. The recycling of CO<sub>2</sub> plays a crucial role, and the creation of a highly efficient electrocatalyst is essential for enhancing the efficiency of the reaction. This work focused on the theoretical design of Ni–N–C catalysts with different coordination environments of Ni through quantum chemical calculations and analyzed the differences between the coordination environments of pyridine N and pyrrole N on the performance of catalytic CO<sub>2</sub> reduction to CO in order to identify the most efficient catalyst configuration. The Ni–N bonding energy of the catalyst with a vacancy was greater than that of the catalyst without a vacancy, and the activation ability of Ni-pyridine N<sub>2</sub>C<sub>1</sub>–C was the best. Ultimately, examining various catalysts for converting CO<sub>2</sub> into CO revealed that Ni-pyridine N<sub>2</sub>C<sub>1</sub>–C exhibited the most effective catalytic impact. In contrast to the energy barrier  $\Delta G = 2.9903$  eV in the absence of a catalyst, the energy barrier  $\Delta G = -1.4029$  eV during the CO<sub>2</sub> to CO catalytic reaction decreased by 4.3932 eV. This decrease was the largest among all the catalysts mentioned above, and the reaction could be spontaneous from a thermodynamic perspective. The research results provide a theoretical reference for the experimental preparation of catalysts for CO<sub>2</sub> to CO conversion and the resource utilization of CO<sub>2</sub>.

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## 1 Introduction

Post industrial revolution, swift advancements in fossil fuel technology have emitted substantial quantities of carbon dioxide (CO<sub>2</sub>) for energy, intensifying the urgency of achieving carbon neutrality.<sup>1,2</sup> Consequently, the primary emphasis is on carbon capture and utilization, making the advancement of CO<sub>2</sub> reduction a widespread issue in both academic circles and society at large.

In CO<sub>2</sub>RR, the electrocatalyst promotes the conversion of carbon dioxide into various “high-value” products with the help of electricity,<sup>3</sup> involving the transfer of six or more electrons during the electrocatalytic reaction. In these CO<sub>2</sub>RR processes, C<sub>1</sub> products (such as methane (CH<sub>4</sub>) and methanol (CH<sub>3</sub>OH)), C<sub>2</sub> products (such as ethylene (C<sub>2</sub>H<sub>4</sub>), acetic acid (CH<sub>3</sub>COOH), and ethanol (C<sub>2</sub>H<sub>5</sub>OH)), and C<sub>3</sub> products (such as *n*-propanol (C<sub>3</sub>H<sub>8</sub>O) and acetone (C<sub>3</sub>H<sub>6</sub>O)) are formed. The activity and selectivity of the electrocatalyst for reduction products are mainly oriented towards C<sub>1</sub> products, mainly CO and HCOO<sup>−</sup>, rather than the highly reduced C<sub>1</sub> and polycarbon (C<sub>2+</sub>) products. CO is the main component of syngas and gas, the

main part of C1 compounds, which can also be used as a reducing agent in the metal smelting industry. Therefore, catalysts that catalyze CO<sub>2</sub>RR to produce CO are explored in this paper. Compared to photocatalysis,<sup>4</sup> electrocatalytic CO<sub>2</sub> reduction avoids the critical problem of catalyst deactivation due to electron–hole complexation. Currently, scientists have explored a variety of catalysts that perform well,<sup>5</sup> such as pure metal catalysts,<sup>6–10</sup> alloy catalysts,<sup>11</sup> porous material catalysts,<sup>12–17</sup> atomically dispersed metal-based catalysts,<sup>18–22</sup> and metal oxide catalysts.<sup>23</sup> However, monometallic catalysts have limited performance.<sup>24–26</sup> The adsorption properties of alloy catalysts are influenced by interactions between neighboring metal atoms, and porous material catalysts can regulate electrolyte diffusion and generate a volume gradient, thus affecting local alkalinity and improving the selectivity of CO<sub>2</sub>RR. Still, they suffer from problems, such as low conductivity, poor stability, and lack of mesoporosity. The M–N–C catalysts have a lower cost than precious metal catalysts, and the metal sites generate a charge accumulation effect, which is favorable for CO<sub>2</sub> chemisorption and provides good selectivity for CO generation. Different central metal ions have distinct electronic structures, geometrical configurations and d-orbital energy levels, so selecting suitable central metal elements is crucial for improving the electrocatalytic ability of M–N–C materials by optimizing surface adsorption. Among them, transition metal elements and main group elements

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exhibit good electrocatalytic ability when acting as center metal ions (Fe, Co, Ni, Cu, Zn, Mn, Sn and Sb). Integrating transition metal nickel into the N-C substance markedly enhances the catalytic efficiency of CO<sub>2</sub>RR. Computational models indicate that incorporating single-atom Ni lowers the energy barrier for reactions in CO<sub>2</sub>RR. Once the atomically scattered Ni was secured to the carbon substance, the single-atom Ni demonstrated peak atomic usage, augmented the concentration of active sites, and enhanced the catalytic efficiency of CO<sub>2</sub>RR. Alterations in the d-orbital energy state of the central metal ion occurred as it was encircled by distinct neighboring ligands, suggesting that modifying the coordination setting of the central metal ion might control the electronic configuration of the M-N-C substance. Changes in the coordination environment can alter the nitrogen atom species by changing the coordination number of the nitrogen atoms. Good catalytic activity for CO<sub>2</sub>RR compared to other M-N<sub>x</sub> structures, such as M-N<sub>2</sub>, M-N<sub>3</sub>, and M-N<sub>5</sub>,<sup>27,28</sup> most M-N<sub>4</sub> structures, were more selective for CO in CO<sub>2</sub>RR.<sup>29–31</sup>

Nitrogen atoms can cause positive charge aggregation,<sup>32</sup> making C adjacent to N the active site for electrocatalytic CO<sub>2</sub>RR. Guo<sup>33</sup> conducted a methodical study on the activation capabilities and specificity of N-doped carbon catalysts in electrocatalytic CO<sub>2</sub>RR processes. Numerous M-N-C catalysts are known to be employed in the electrocatalytic process of CO<sub>2</sub>RR. Jia *et al.*<sup>34</sup> synthesized a single-atom Ni catalyst SA-NiNG-NV with N vacancies possessing higher CO<sub>2</sub>RR selectivity. Cheng *et al.*<sup>35</sup> synthesized a large number of Ni-N-C catalytic materials at the edges of the sites by applying microwave stripping, which exhibited extremely high activity in the electrocatalytic CO<sub>2</sub>RR process. Wang *et al.*<sup>36</sup> systematically investigated single-atom catalysts with typical transition metals as active sites, and they found that the selectivity in CO<sub>2</sub>-CO conversion was ranked as Ni > Co > Fe, and the reactivity was ranked as Co > Ni > Fe. Ni-doped catalysts had high catalytic efficiency, good stability and low price, so this study was aimed at Ni-N-C catalysts. Altering the electron configuration of the coordination center M consequently impacts its location on the active site and the catalyst's specificity. Zhao's team<sup>37</sup> discovered through DFT analysis that pyrrole N predominantly generated HCOOH during CO<sub>2</sub>RR catalysis, exhibiting the minimal overpotential of 0.24 V compared to other N-doped graphene types, while Wu<sup>38</sup> ascertained that pyridinium N, as the primary catalyst, effectively converted CO<sub>2</sub> into CO, demonstrating superior catalytic efficiency in theoretical terms.

Consequently, this study conducts theoretical analyses of the stability, CO<sub>2</sub> adsorption stability, and catalytic efficiency of each catalyst using the DMol<sup>3</sup> module in Materials Studio (MS) software. This was performed to evaluate the impact of various coordination settings, including the quantity and nature of nitrogen atom coordination and adsorption type, on the CO<sub>2</sub> reduction efficiency of the Ni-N-C catalysts, and to identify catalysts with superior performance that could inform the use

of Ni-N-C catalysts in CO<sub>2</sub>RR. DFT calculations can predict and guide experimental design, thereby conserving human and material resources while more effectively screening for catalysts with superior performance. Additionally, DFT enables a deeper understanding of reaction mechanisms.

## 2 Models and methods

Quantum chemical calculations can be used to design the required catalysts directly on MS software and calculate and predict their catalytic performance, which can reduce the time and workload required for experiments. Many repetitive tasks can be avoided, research efficiency can be improved, and the experimental cost can be reduced, which can provide references and guidance for experiments.

The 5 × 4 graphene was intercepted for reconfiguration, which retained the structural characteristics and reduced the computation. The establishment of the Ni-N-C catalyst model was completed, and geometry optimization was performed by selecting calculation in the DMol<sup>3</sup> module, selecting geometry optimization in the task module in the set up tab, and selecting customized in the quality module. Under the generalized gradient approximation (GGA), the functional chosen was selected as the Perdew-Burke-Ernzerhof (PBE) function, and the basis set with a double-valued atomic orbital plus polarization function (DNP) was chosen to describe the atomic orbitals. The energy convergence criteria, maximum force, and maximum displacement were set during geometry optimization at 2 × 10<sup>-5</sup> Ha, 0.004 Ha Å<sup>-1</sup>, and 0.005 Å, respectively. To accelerate electron convergence, the smearing was set to 0.005 Ha. The maximum number of iterations was set to 1000 in more, with medium selected for overall accuracy. The max SCF cycle was set to 1000, and the COSMO solution environment was used with water selected as the solvent. The energy calculation was also done using the DMol<sup>3</sup> module. The binding energy  $E_B$  of the catalyst was calculated according to the following formula to select the catalyst configuration with the best stability.

$$E_B = E_{\text{total}} - E_{\text{carrier+Ni}}, \quad (1.1)$$

where  $E_b$  is the average bond energy of the Ni-N bond. The average bond energy is calculated as follows:

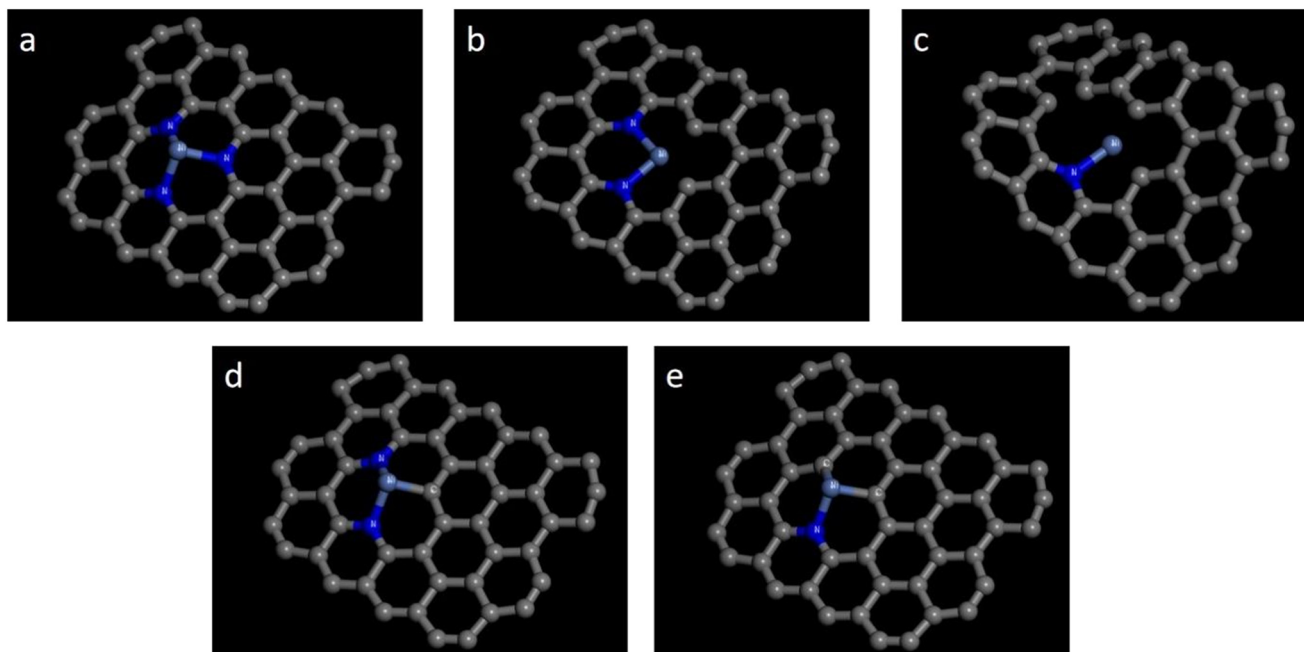
$$E_b = E_B \div n, \quad (1.2)$$

where  $n$  is the number of Ni-N bonds.

Next, the structure optimization of the Ni-N-C-CO<sub>2</sub> structure was carried out. The structure-optimized CO<sub>2</sub> was attached to the active center, and the parameters were set for structure optimization considering single-site adsorption, double-site adsorption and different atoms connected. The specific equations for calculating adsorption energy are as follows:

$$E_{\text{ads}} = E_a - E_{\text{CO}_2} - E_{\text{total}}. \quad (1.3)$$





**Fig. 1** Five configurations of Ni-pyridine  $N_nV_{3-n}$ -C catalysts: (a) Ni-pyridine  $N_3$ -C; (b) Ni-pyridine  $N_2V_1$ -C; (c) Ni-pyridine  $N_1V_2$ -C; (d) Ni-pyridine  $N_2C_1$ -C; and (e) Ni-pyridine  $N_1C_2$ -C.

Ultimately, the Gibbs free energies for the  $\text{CO}_2$  reduction to CO reaction intermediates, both catalyzed and uncatalyzed, were determined.

## 3 Results and discussion

### 3.1 Ni-N-C catalyst design

**3.1.1 Ni-Pyridine N-C catalyst design.** Ni-Pyridine  $N_nV_{3-n}$ -C catalysts were Ni-N-C catalysts with three pyridine N atoms anchoring Ni and containing vacancies. Each N atom formed a pyridine structure with a six-membered ring with C atoms, and the Ni atoms were not out of the same plane as the graphene C atoms, as shown in Fig. 1.

Ni-Pyridine  $N_nV_{4-n}$ -C catalysts were Ni-N-C catalysts consisting of four pyridine N atoms anchored to Ni atoms and containing vacancies, and each N atom formed a six-membered ring with graphene C in a pyridine structure. Fig. 2 illustrates that the Ni-pyridine  $N_nV_{4-n}$ -C catalysts can be categorized into seven configurations.

**3.1.2 Ni-Pyrrole N-C catalyst design.** Ni-Pyrrole  $N_nV_{4-n}$ -C catalysts were Ni-N-C catalysts consisting of four pyrrole N atoms anchored to Ni atoms and containing vacancies, and each N atom formed a five-membered ring with graphene C in a pyrrole structure. The Ni-pyrrole  $N_nV_{4-n}$ -C catalysts can be categorized into seven configurations, as shown in Fig. 3.

### 3.2 Stability studies of Ni-N-C catalysts

The Ni-pyridine  $N_nV_{3-n}$ -C catalyst was taken as an example, and the study calculated the average bond energies of the Ni-N and Ni-C bonds for each configuration. The results are presented in Table 1. Among the five structures, the one with

the largest bond energy was the Ni-pyridine  $N_2V_1$ -C catalyst, which had an average bond energy of  $-0.0898$  eV of the Ni-N bond, indicating that the catalyst had good stability. The largest total bond energy was the d structure, the Ni-pyridine  $N_2C_1$ -C catalyst, which was anchored by two N atoms and one C atom, with a total summed energy of  $E_B = -0.1796$  eV, showing good stability. In summary, the stable structures of the Ni-pyridine  $N_nV_{3-n}$ -C catalysts were Ni-pyridine  $N_2V_1$ -C and Ni-pyridine  $N_2C_1$ -C.

### 3.3 Effect of the number of vacancies on the performance of Ni-N-C catalysts

Subsequently, the catalysts underwent examination for the most occupied molecular orbital (HOMO) and the lowest unoccupied molecular orbital (LUMO). Both HOMO and LUMO symbolize the primary levels of molecular orbital energy. HOMO symbolizes the most filled molecular orbitals, while LUMO denotes the least occupied molecular orbital. For the energy band gap  $\Delta E = E_{\text{LUMO}} - E_{\text{HOMO}}$ , the rate of electron movement within the catalyst can be ascertained using  $\Delta E$ . A reduced  $\Delta E$  indicates a quicker electron transfer rate in the front molecular orbitals and a more catalytic catalyst.

The frontline molecular orbital energy levels and  $\Delta E$  of the three previously selected Ni-N-C catalysts are illustrated in Fig. 4–6. Compared to the catalysts without vacancies, the catalysts containing vacancies were significantly larger for  $\Delta E$ . The  $\Delta E$  of the Ni-pyridine  $N_3V_1$ -C catalyst with vacancies was  $0.872$  eV, which was more than three times larger than that of the Ni-pyridine  $N_4$ -C catalyst without vacancies ( $\Delta E = 0.278$  eV).



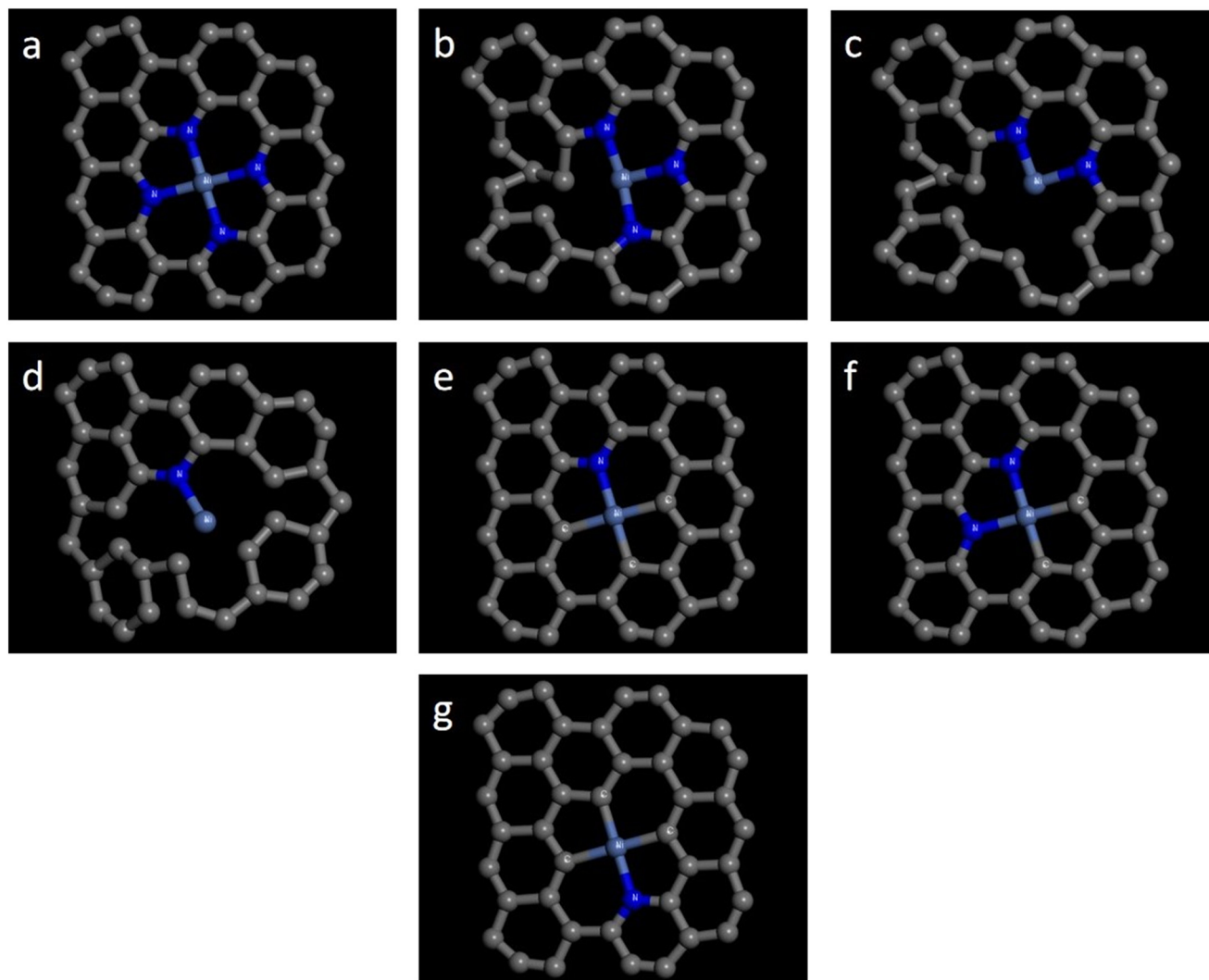


Fig. 2 Seven structures of Ni-pyridine  $N_nV_{4-n}$ -C catalysts: (a) Ni-pyridine  $N_4V_1$ -C; (b) Ni-pyridine  $N_3V_1$ -C; (c) Ni-pyridine  $N_2V_2$ -C; (d) Ni-pyridine  $N_2V_1$ -C; (e) Ni-pyridine  $N_3C_1$ -C; (f) Ni-pyridine  $N_2C_2$ -C; and (g) Ni-pyridine  $N_1C_3$ -C.

### 3.4 Study of CO<sub>2</sub> adsorption capacity of Ni-N-C catalysts

All atoms of the Ni-pyridine  $N_2V_1$ -C catalyst, Ni-pyrrole  $N_2V_2$ -C catalyst and Ni-pyridine  $N_1V_3$ -C catalyst were in the same plane, so there was no need to consider the direction of CO<sub>2</sub> binding to the catalyst during structure optimization. Only single-site and double-site adsorption, as well as Ni-C bonding and Ni-O bonding, must be considered for a total of three cases.

The Ni atoms of the Ni-pyridine  $N_2C_1$ -C catalyst and the Ni-pyridine  $N_1V_3$ -C catalyst were not in the same plane as the carrier graphene. Therefore, not only single-site and double-site adsorption but also the direction of CO<sub>2</sub> molecule adsorption had to be considered, so there were 6 cases.

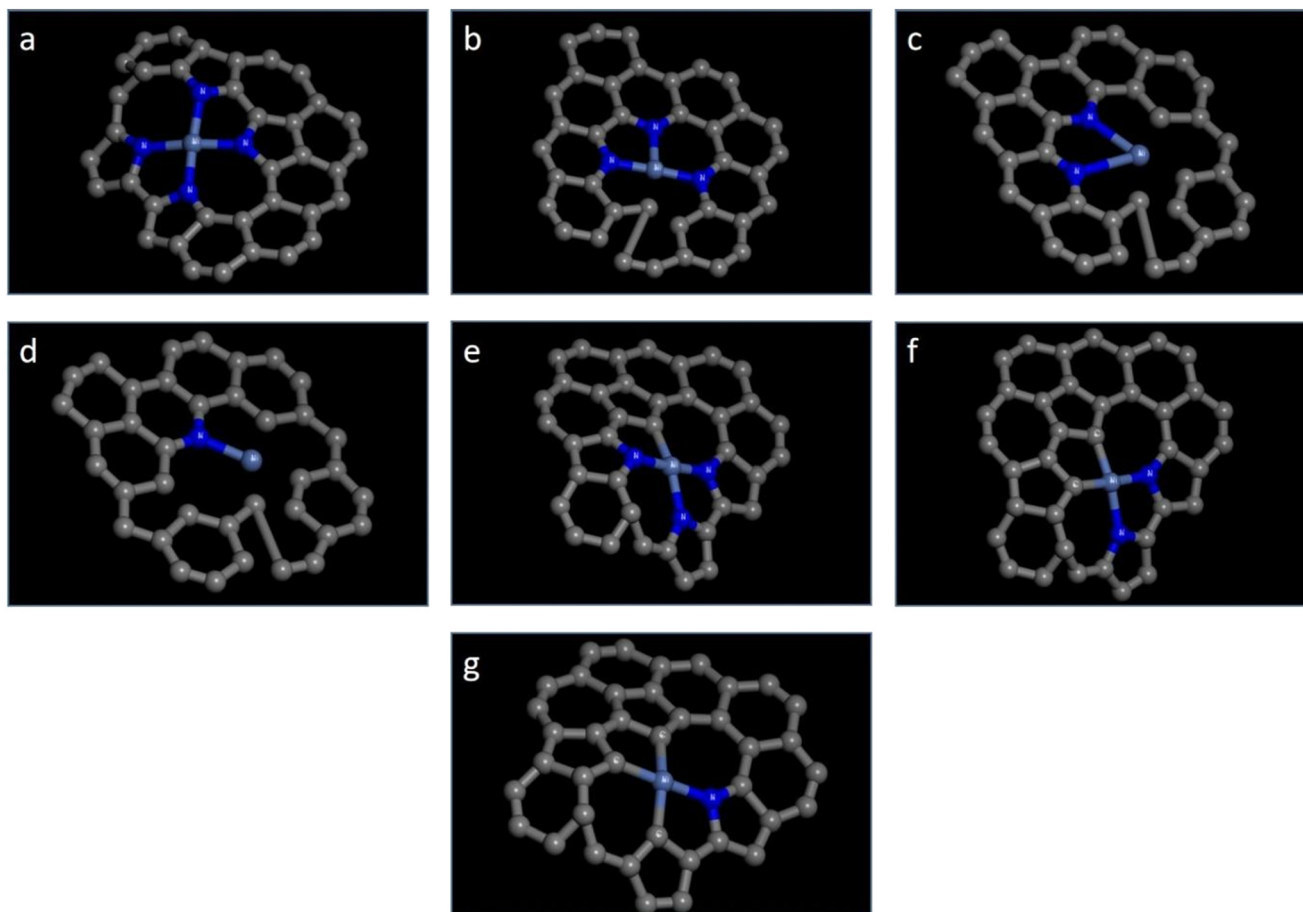
**3.4.1 Active site analysis of Ni-N-C catalysts.** The global activity analysis was carried out in the previous section using the front molecular orbital energy levels. Next, the active sites of the catalysts were determined using Fukui indices.

Table 2 demonstrates the Fukui functions for each Ni-N-C catalyst Ni atom as well as the N and C atoms attached to the Ni atom. From the table, it can be observed that the  $f(+)$  and  $f(-)$  of the Ni atoms of the six catalysts were the maximum values within the catalyst, indicating that this site could react with both Lewis acids and Lewis bases. Taking catalyst Ni-pyridine  $N_2C_1$ -C Catalyst Ni-C N-O as a case study, a periodic cell (Fig. S4†) was constructed, and the Fukui indices of all atoms were summarized in Table S1.† Therefore, it was the most suitable catalyst site.

Table 3 showed the Fukui index of CO<sub>2</sub>, from which it could be observed that the C atom of CO<sub>2</sub> had the largest  $f(+)$  and a greater positron density, so in single-site adsorption, it could be assumed that the stability of the C atom connected to the Ni atom of the catalyst was greater than that of the O atom connected to the Ni atom. Therefore, the Ni-O connection was not considered for the time being.







**Fig. 3** Seven structures of Ni-pyrrole  $N_nV_{4-n}$ -C catalysts: (a) Ni-pyrrole  $N_4$ -C; (b) Ni-pyrrole  $N_3V_1$ -C; (c) Ni-pyrrole  $N_2V_2$ -C; (d) Ni-pyrrole  $N_2V_1$ -C; (e) Ni-pyrrole  $N_3C_1$ -C; (f) Ni-pyrrole  $N_2C_2$ -C; and (g) Ni-pyrrole  $N_1C_3$ -C.

**3.4.2 Stability study of  $CO_2$  adsorption over Ni-N-C catalysts.** Next, six selected Ni-N-C catalysts with good stability were determined for adsorption stability.

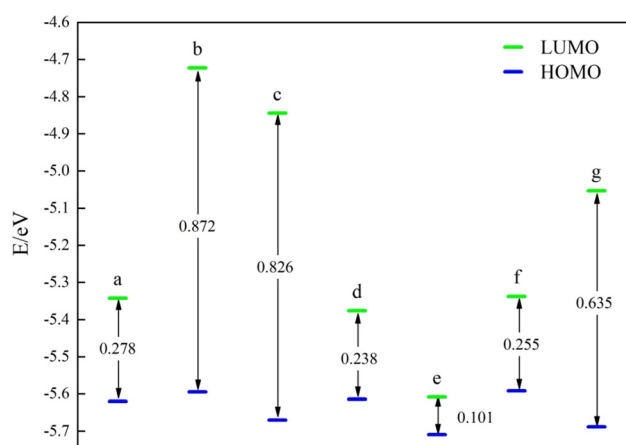
(1) *Ni-Pyridine  $N_2V_1$ -C catalysts.* The structure of the Ni- $N_2V_1$ -C- $CO_2$  intermediate was designated (Fig. S1†). The bond lengths, bond angles and adsorption energies of the Ni- $N_2V_1$ -C- $CO_2$  structure were shown in Table 4.

As shown in Table 4, the binding energies of (a) and (b) were negative and (c) was positive. Therefore, (c)  $CO_2$  could not be stabilized for adsorption. The C=O bond lengths of (a) were 1.178 Å and 1.179 Å, respectively, which were not much changed compared to the  $CO_2$  bond length of 1.178 Å. The C=O bond

lengths of (c) were both 1.178 Å, and there was no change in the bond lengths, so (a) and (b) had a low activation effect on  $CO_2$ .

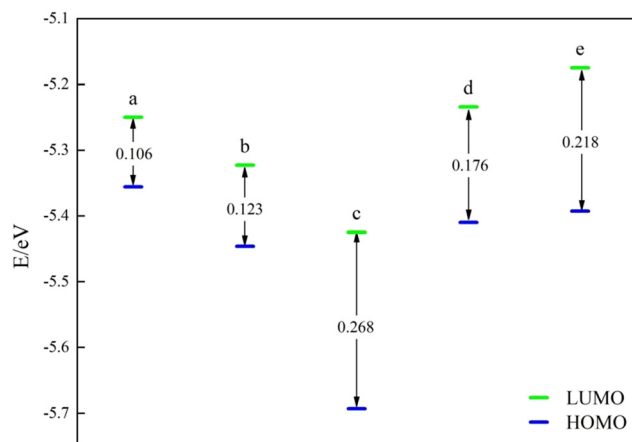
**Table 1** Bond energies of Ni-pyridine  $N_nV_{3-n}$ -C catalysts

Isomers	$E_{\text{carrier+Ni/eV}}$	$E_{\text{total/eV}}$	$E_B/\text{eV}$	$E_b/\text{eV}$
a	-3536.73	-3536.87	-0.1481	-0.0494
b	-3481.98	-3482.16	-0.1796	-0.0898
c	-3427.27	-3427.31	-0.0500	-0.0500
d	-3520.02	-3520.20	-0.1798	-0.0599
e	-3503.39	-3503.54	-0.1511	-0.0504

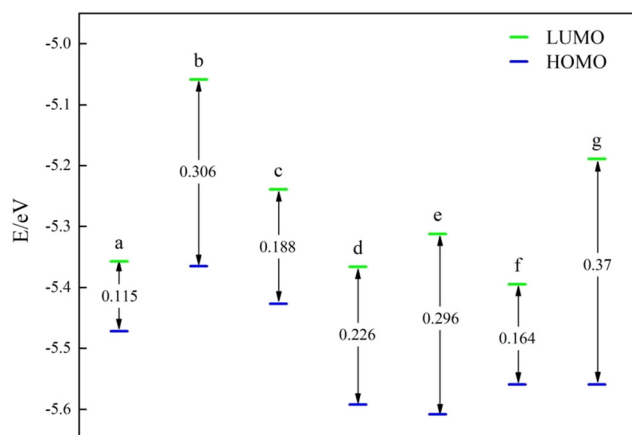


**Fig. 4** Frontline molecular orbital energy levels and  $\Delta E$  for Ni-pyridine  $N_nV_{4-n}$ -C catalysts: (a) Ni-pyridine  $N_4$ -C; (b) Ni-pyridine  $N_3V_1$ -C; (c) Ni-pyridine  $N_2V_2$ -C; (d) Ni-pyridine  $N_2V_1$ -C; (e) Ni-pyridine  $N_3C_1$ -C; (f) Ni-pyridine  $N_2C_2$ -C; and (g) Ni-pyridine  $N_1C_3$ -C.





**Fig. 5** Frontline molecular orbital energy levels and  $\Delta E$  for Ni-pyridine  $N_nV_{3-n}-C$  catalysts: (a) Ni-pyridine  $N_3-C$ ; (b) Ni-pyridine  $N_2V_1-C$ ; (c) Ni-pyridine  $N_1V_2-C$ ; (d) Ni-pyridine  $N_2C_1-C$ ; and (e) Ni-pyridine  $N_1C_2-C$ .



**Fig. 6** Frontline molecular orbital energy levels and  $\Delta E$  for Ni-pyrrole  $N_nV_{4-n}-C$  catalysts: (a) Ni-pyrrole  $N_4-C$ ; (b) Ni-pyrrole  $N_3V_1-C$ ; (c) Ni-pyrrole  $N_2V_2-C$ ; (d) Ni-pyrrole  $N_2V_1-C$ ; (e) Ni-pyrrole  $N_3C_1-C$ ; (f) Ni-pyrrole  $N_2C_2-C$ ; and (g) Ni-pyrrole  $N_1C_3-C$ .

**Table 3** Fukui index for  $CO_2$  catalysts

	$f(+)$		
	Atom	Mulliken	Hirshfeld
Ni-Pyrrole $N_1C_3-C$	C(1)	0.462	0.384
	O(2)	0.269	0.308
	O(3)	0.269	0.308

**Table 4** Adsorption energies and bond lengths of Ni-pyridine  $N_2V_1-C-CO_2$  intermediates

Isomers	$E_{ads}/eV$	$d_{C-O1}/\text{\AA}$	$d_{C-O2}/\text{\AA}$
a	-0.0092	1.178	1.179
b	-0.0087	1.178	1.178
c	0.0045	1.178	1.178

(2) *Ni-Pyridine  $N_2C_1-C$  catalysts.* The bond lengths, bond angles and adsorption energies of the Ni-pyridine  $N_2C_1-C-CO_2$  structure (Fig. 7) are presented in Table 5.

As shown in Table 5, the adsorption energies of the six structures were negative, so all were stable. The adsorption energies of the three structures where  $CO_2$  was adsorbed from the side close to the Ni atom were significantly more stable. In terms of bond lengths, the structures in which  $CO_2$  was adsorbed from the side close to the Ni atom had a larger change in  $d_{C-O}$ , which had a good activation effect on  $CO_2$  molecules.

(3) *Ni-Pyridine  $N_1V_3-C$  catalysts.* The structure of the Ni-pyridine  $N_1V_3-C-CO_2$  intermediate is shown in Fig. S2.† The bond lengths, bond angles and adsorption energies of the Ni-pyridine  $N_1V_3-C-CO_2$  intermediate are illustrated in Table 6.

In terms of binding energy, the binding energies  $E_{ads}$  of (a), (b) and (c) were lower than the energy required for  $CO_2$  to be adsorbed stably, and the adsorption of  $CO_2$  was more stable from the side close to Ni atoms than that from the side

**Table 2** Fukui index for Ni-N-C catalysts

	$f(+)$			$f(-)$		
	Atom	Mulliken	Hirshfeld	Atom	Mulliken	Hirshfeld
Ni-Pyridine $N_2V_1-C$	Ni(26)	0.050	0.030	Ni(26)	0.055	0.030
	N(25)	0.002	0.011	N(25)	0.002	0.010
	N(31)	-0.000	0.008	N(31)	0.000	0.008
Ni-Pyridine $N_2C_1-C$	Ni(26)	0.044	0.036	Ni(26)	0.055	0.030
	N(25)	0.005	0.013	N(25)	0.005	0.013
	N(31)	0.000	0.007	N(31)	0.000	0.007
Ni-Pyridine $N_1V_3-C$	N(53)	0.011	0.013	N(53)	0.011	0.013
	Ni(39)	0.053	0.030	Ni(39)	0.049	0.030
	N(19)	0.002	0.012	N(19)	0.001	0.012
Ni-Pyrrole $N_2V_2-C$	C(7)	0.002	0.012	C(7)	0.017	0.012
	C(20)	0.015	0.015	C(20)	0.016	0.015
	Ni(40)	0.076	0.039	Ni(40)	0.069	0.040
Ni-Pyrrole $N_1V_3-C$	N(19)	0.001	0.013	N(19)	0.000	0.013
	N(20)	0.002	0.014	N(20)	0.002	0.014
	Ni(39)	0.067	0.036	Ni(39)	0.065	0.037
	N(19)	0.003	0.014	N(19)	0.003	0.014
	C(7)	0.0018	0.014	C(7)	0.018	0.014
	C(20)	0.015	0.014	C(20)	0.015	0.014



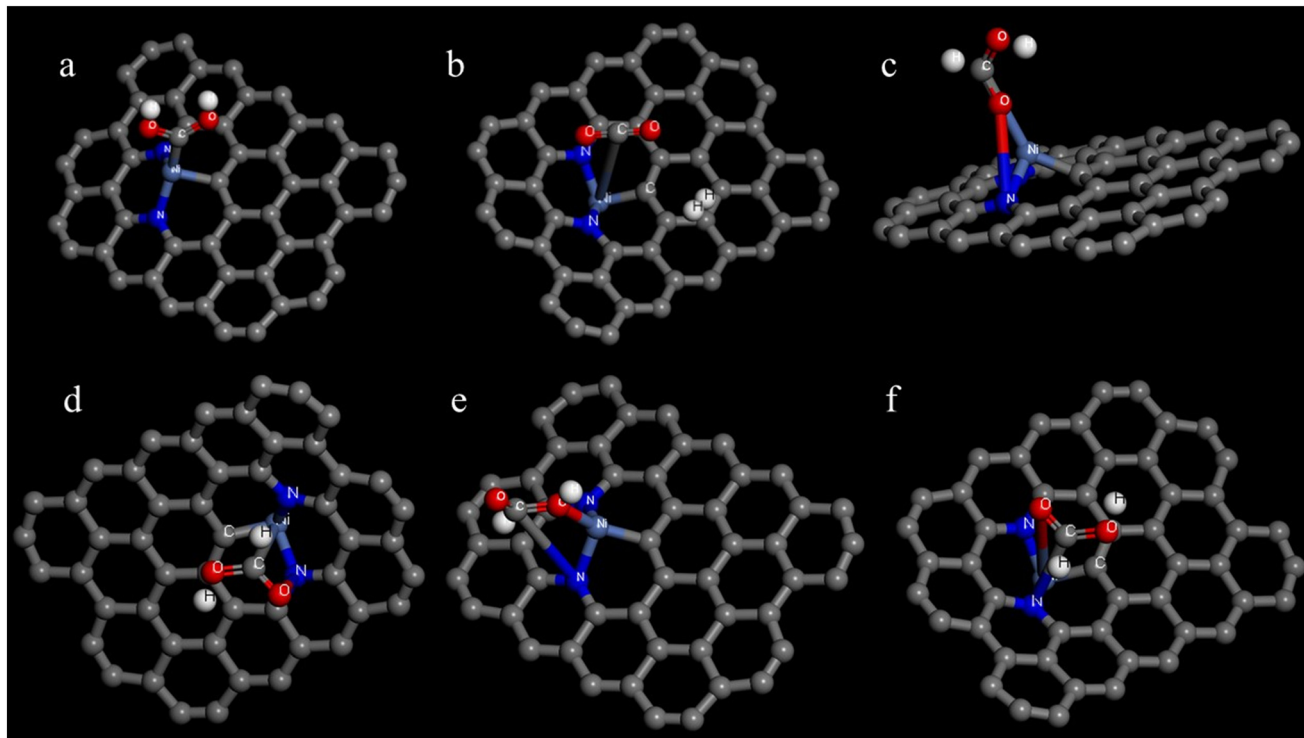


Fig. 7 Isomers of the Ni-pyridine  $N_2C_1-C-CO_2$  intermediate: (a) Ni-pyridine  $N_2C_1-C-CO_2$  single-site adsorption A; (b) Ni-pyridine  $N_2C_1-C-CO_2$  single-site adsorption B; (c) Ni-pyridine  $N_2C_1-C-CO_2$  Ni-C N-O double-site adsorption A; (d) Ni-pyridine  $N_2C_1-C-CO_2$  Ni-C N-O double-site adsorption B; (e) Ni-pyridine  $N_2C_1-C-CO_2$  Ni-O N-C double-site adsorption A; and (f) Ni-pyridine  $N_2C_1-C-CO_2$  Ni-O N-C double-site adsorption B.

far away from Ni atoms. In terms of bond lengths, the  $C=O$  bond lengths of (a) and (b) were almost unchanged compared to  $CO_2$ , so the catalytic activity of  $CO_2RR$  might be very low. The  $C=O$  bond lengths of (c) were 1.176 Å and 1.180 Å, which had a certain activation effect on  $CO_2$  molecules.

(4) *Ni-Pyrrole  $N_2V_2-C$  catalysts.* The structure of Ni-pyrrole  $N_2V_2-C-CO_2$  is shown in Fig. 8 as follows: (a) single-site adsorption, with Ni atoms attached to C atoms; (b) double-site adsorption, with Ni-C and N-O bonded; and (c) double-site adsorption, with N-O and N-C bonded. The binding energies and bond lengths of the Ni-pyrrole  $N_2V_2-C-CO_2$  intermediates are illustrated in Table 7.

In terms of binding energy, the binding energies of all three intermediates were negative, so all  $CO_2$  could be stably adsorbed on the catalyst. According to the  $C=O$  bond lengths, the three intermediates did not change much compared with  $CO_2$ . Therefore, the activation of  $CO_2$  molecules of the Ni-pyrrole  $N_2V_2-C$  catalysts was low.

(5) *Ni-Pyrrole  $N_1V_3-C$  catalysts.* Fig. S3† depicts the isomers of the Ni-pyrrole  $N_1V_3-C-CO_2$  intermediate as follows: (a) single-site adsorption, with the Ni atom attached to the C atom; (b) double-site adsorption, with Ni-C and N-O bonded; and (c) double-site adsorption, with N-O-N-C bonded. The binding energies and bond lengths of the Ni-pyrrole  $N_1V_3-C-CO_2$  intermediate are shown in Table 8.

As illustrated in Table 8, the binding energies of all three structures were negative, so  $CO_2$  could be stably adsorbed on the catalysts. However, the  $C=O$  bond lengths of (a), (b) and (c) were all 1.178 Å, which was the same as that of  $CO_2$ . Therefore, the activation of  $CO_2$  molecules by the three catalysts was low.

### 3.5 Study of the catalytic activity of catalysts for $CO_2RR$ catalyzation

#### 3.5.1 Analysis of the catalytic activity of $CO_2RR$ by single-site adsorption on catalysts.

First, the Ni-pyridine  $N_2C_1-C$

Table 5 Adsorption energies and bond lengths of Ni-pyridine  $N_2C_1-C-CO_2$  intermediates

Isomers	$E_{ads}/eV$	$d_{C-O1}/\text{\AA}$	$d_{C-O2}/\text{\AA}$
a	-0.0171	1.166	1.188
b	-0.0088	1.178	1.178
c	-0.0204	1.166	1.186
d	-0.0089	1.177	1.178
e	-0.0198	1.166	1.186
f	-0.0085	1.177	1.178

Table 6 Adsorption energies and bond lengths of Ni-pyridine  $N_1V_3-C-CO_2$  intermediates

Isomers	$E_{ads}/eV$	$d_{C-O1}/\text{\AA}$	$d_{C-O2}/\text{\AA}$
a	-0.0084	1.178	1.179
b	-0.0008	1.178	1.178
c	-0.0093	1.176	1.180
d	0.0039	1.178	1.178
e	0.0027	1.177	1.179
f	0.0018	1.177	1.178



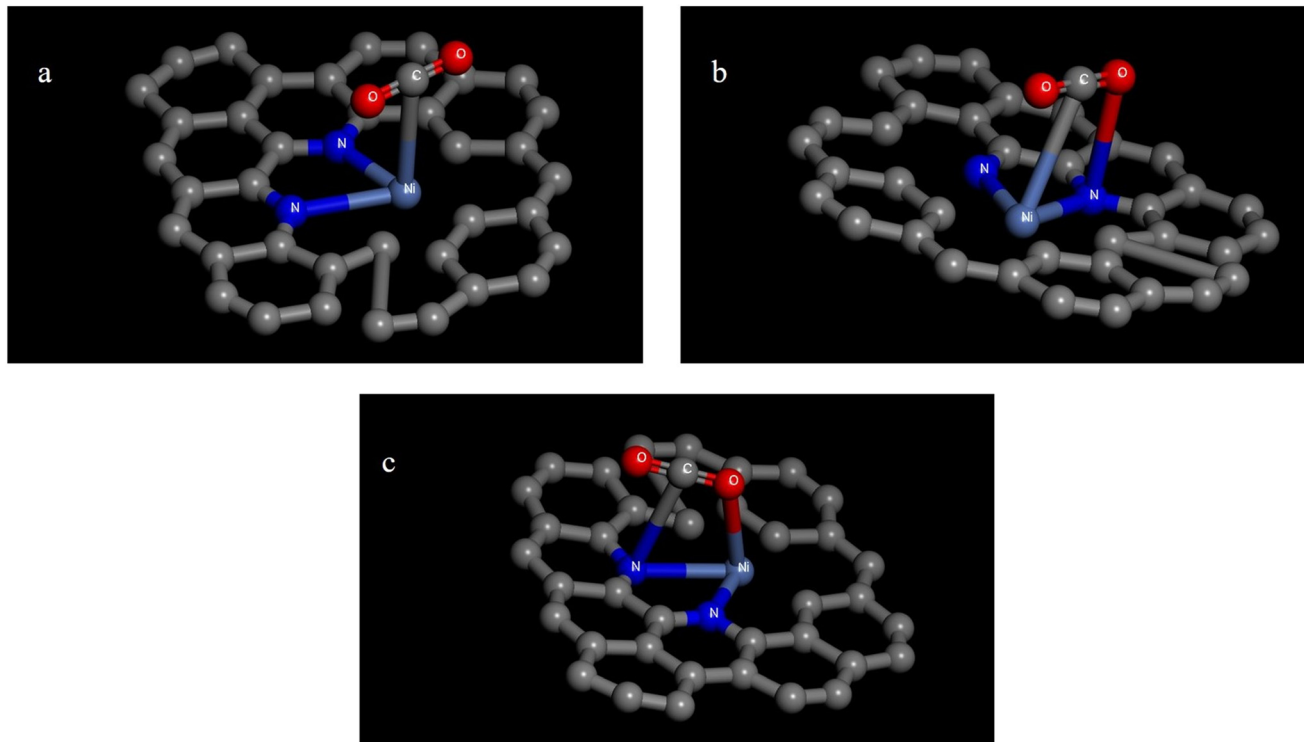


Fig. 8 Isomers of the Ni-pyrrole  $N_2V_2-C-CO_2$  intermediate: (a) Ni-pyrrole  $N_2V_2-C-CO_2$  single-site adsorption; (b) Ni-pyrrole  $N_2V_2-C-CO_2$  Ni-C N-O double-site adsorption; and (c) Ni-pyrrole  $N_2V_2-C-CO_2$  Ni-O N-C double-site adsorption.

catalysts were analyzed for single-site adsorption of  $CO_2$ . The adsorption energy data were summarized in Table S2.† The reaction paths of the five catalysts for  $CO_2$  to CO under single-site adsorption were illustrated in Fig. 9. In the same case of single-site adsorption, Ni-pyridine  $N_1V_3-C$  catalyst A had the best catalytic effect, with a reaction energy barrier  $\Delta G$  of 0.2714 eV, which was 2.7189 eV lower than that without catalyst ( $\Delta G = 2.9903$  eV). Thus, the catalyst exhibited excellent catalytic performance. The energy barriers of the reaction under Ni-pyridine  $N_2C_1-C$  catalyst A decreased by 2.6280 eV and under Ni-pyridine  $N_2C_1-C$  catalyst B decreased by 2.5789 eV, both of which had good catalytic performance. The energy barriers of the reaction under Ni-pyridine  $N_1V_3-C$  catalyst B,  $\Delta G = 0.7259$  eV, compared to that of the reaction without the catalyst,  $\Delta G = 2.9903$  eV, decreased by 2.2644 eV, which had some catalytic activity.

Based on the magnitude of the energy barriers, it could be observed that the decisive step for the uncatalyzed and Ni-pyridine  $N_1V_3-C$  catalyst B was the formation of  $^*CO$ , and the rest of the decisive step was the formation of  $^*COOH$  in the first step.

Table 7 Adsorption energies and bond lengths of Ni-pyrrole  $N_2V_2-C-CO_2$  intermediates

Isomers	$E_{ads}/eV$	$d_{C-O1}/\text{\AA}$	$d_{C-O2}/\text{\AA}$
a	-0.0093	1.177	1.179
b	-0.0096	1.177	1.178
c	-0.0094	1.178	1.178

**3.5.2 Analysis of the catalytic activity of  $CO_2RR$  by catalyst two-site adsorption.**  $CO_2$  can be categorized as Ni-C, N-O bonded and N-O, N-C bonded for two-site adsorption on catalysts, so the same catalyst had two different structures in the same two-site adsorption case.

The catalytic ability of the Ni-pyridine  $N_2C_1-C$  catalyst for two-site adsorption of  $CO_2$  from the proximal side with Ni-C, N-O bonding was first investigated. The adsorption energy data were summarized in Table S2.†

Five cases of catalyst two-site adsorption of  $CO_2$  were illustrated in Fig. 10. As observed from the figure, the Ni-pyridine  $N_2C_1-C$  catalyst Ni-C N-O A was the best catalyst with a reaction energy barrier of  $\Delta G = -1.4029$  eV, which was a decrease of 4.3932 eV compared to the energy barrier of  $\Delta G = 2.9903$  eV in the absence of the catalyst, and the reaction was exothermic and thermodynamically capable of proceeding spontaneously. The energy barrier for the reaction under Ni-pyridine  $N_2C_1-C$  catalyst Ni-O N-C B was 0.4084 eV, and the energy barrier of the reaction under Ni-pyridine  $N_2C_1-C$  catalyst Ni-C N-O B was 1.9764 eV. There was a substantial decrease in the energy barrier compared to the reaction without the

Table 8 Adsorption energies and bond lengths of Ni-pyrrole  $N_1V_3-C-CO_2$  intermediates

Isomers	$E_{ads}/eV$	$d_{C-O1}/\text{\AA}$	$d_{C-O2}/\text{\AA}$
a	-0.0090	1.178	1.178
b	-0.0101	1.178	1.178
c	-0.0099	1.178	1.178





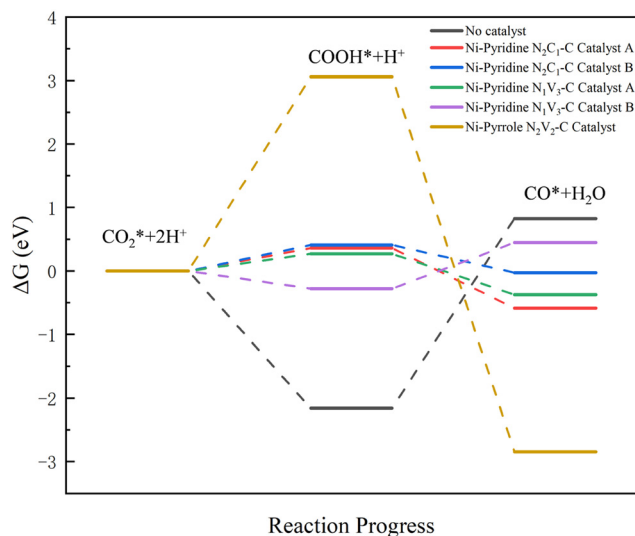


Fig. 9 Reaction path diagram for catalysts in the case of single-site adsorption (where A represents adsorption from the proximal side and B represents adsorption from the distal side).

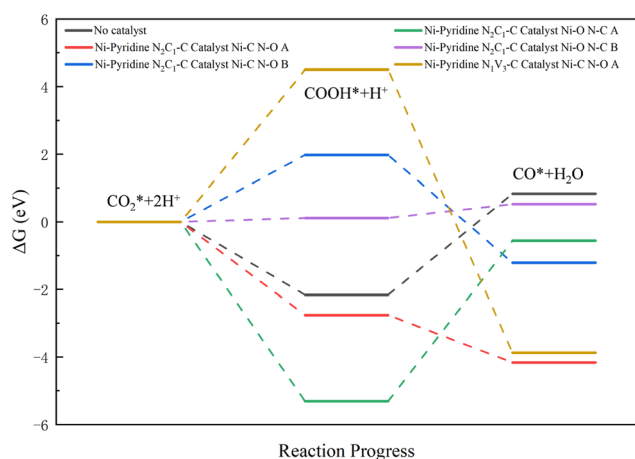


Fig. 10 Reaction path diagram for catalysts in the case of two-site adsorption (where A represents adsorption from the near side and B represents adsorption from the far side).

catalyst, so both had good catalytic activity; the rest of the catalysts had limited catalytic performance.

## 4 Conclusions

In this study, the stability, activation and catalytic performance of the catalysts were analyzed and screened for better catalysts by performing energy calculations and structure optimization of the constructed structures based on the theoretical basis of quantum chemistry. The following conclusions were obtained.

(1) Vacancies could significantly affect the catalyst properties. The Ni-N-C catalyst with vacancies had a higher Ni-N bond energy and good catalyst stability. However, its  $\Delta E$

was larger, and the electron conduction rate was slower than that of the catalyst without vacancies. The  $\Delta E$  of the Ni-pyridine  $N_3V_1$ -C catalyst was 0.872 eV, which was more than three times that of the catalyst without the Ni-pyridine  $N_4$ -C catalyst with  $\Delta E = 0.278$  eV.

(2) The catalysts with excellent activation performance for  $CO_2$  were screened as Ni-pyridine  $N_2C_1$ -C catalyst, Ni-pyridine  $N_1V_3$ -C catalyst and Ni-pyrrole  $N_2V_2$ -C catalyst. Among them, the best  $CO_2$  activation ability was the Ni-pyridine  $N_2C_1$ -C catalyst.

(3) In single-site adsorption, the best catalytic effect was achieved by Ni-pyridine  $N_1V_3$ -C catalyst A, with reaction  $\Delta G = 0.2714$  eV. In two-site adsorption, the best catalytic effect was achieved by Ni-pyridine  $N_2C_1$ -C Ni-C N-O A, with reaction  $\Delta G = -1.4029$  eV, and the reaction was able to proceed thermodynamically and spontaneously.

(4) Both single-site adsorption and dual-site adsorption reduced the reaction energy barrier compared to no catalyst. Overall, most of the catalytic activities of single-site adsorption were better than those of dual-site adsorption.

## Data availability

The data used to support the findings of this paper are included within the article.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

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