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## Efficient capture of Sr<sup>2+</sup> ions by a layered crystalline zirconium phosphate fluoride

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The effective remediation of radioactive strontium-90 (<sup>90</sup>Sr) from complex aqueous environments remains challenging due to the inherent high solubility and migration propensity of Sr<sup>2+</sup> ions. Herein, we synthesized hydrothermally a new two-dimensional (2D) crystalline zirconium phosphate fluoride [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>] featuring a layered anionic architecture of [Zr(PO<sub>4</sub>)F<sub>2</sub>]<sub>n</sub><sup>7-</sup> with intercalated [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>]<sup>+</sup> cations, which shows exceptional Sr<sup>2+</sup> remediation capability. It possesses a high maximum Sr<sup>2+</sup> adsorption capacity (*q*<sub>m</sub><sup>Sr</sup>) of 161.48 mg g<sup>-1</sup> (higher than that of many inorganic crystalline adsorbents) and fast kinetics for Sr<sup>2+</sup> capture (Sr<sup>2+</sup> removal rate (*R*<sup>Sr</sup>) of 94.89% within 1 min). Specifically, it maintains Sr<sup>2+</sup> removal efficiency in the presence of competing Cs<sup>+</sup>, K<sup>+</sup>, Na<sup>+</sup>, Ca<sup>2+</sup>, Mg<sup>2+</sup> ions and in actual aqueous systems including seawater (*R*<sup>Sr</sup> = 79.06%). X-ray photoelectron spectroscopy (XPS) and thermodynamics confirm that spontaneous Sr<sup>2+</sup> capture occurs through ion exchange processes, where the interlayered [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>]<sup>+</sup> cations in [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>] are exchanged with Sr<sup>2+</sup>. The compound [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>] represents the first crystalline inorganic zirconium phosphate fluoride ion exchange material for radionuclide capture. This work provides a high-performance ion exchanger as a candidate for radiostrontium capture.

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## Introduction

Strontium-90 (<sup>90</sup>Sr), recognized as one of the most hazardous artificial radionuclides, predominantly exists as <sup>90</sup>Sr<sup>2+</sup> ions in radioactive waste liquids. As a β-emitting radioisotope derived from the nuclear fission of <sup>235</sup>U/<sup>239</sup>Pu, <sup>90</sup>Sr exhibits a long half-life (*t*<sub>1/2</sub> = 28.6 years) and high β-particle energy (0.546 MeV),<sup>1,2</sup> posing severe environmental and health risks due to its high mobility, radiotoxicity, and biotoxicity.<sup>3,4</sup> Its chemical similarity to Ca<sup>2+</sup> facilitates bioaccumulation in human bone tissues, leading to bone cancer and leukemia.<sup>5,6</sup> On the other hand, <sup>90</sup>Sr has found significant implementation in therapeutic oncology as a radiation source for targeted bone cancer treatment.<sup>7</sup> Concurrently, its sustained decay heat generation enables essential roles in radioisotope thermoelectric generators (RTGs), particularly for powering deep-space probes and remote terrestrial monitoring systems under extreme environmental conditions.<sup>7,8</sup> Thus, the rapid separation and recovery of <sup>90</sup>Sr are critical for radioactive

waste management, human health protection, environmental sustainability, and resource recycling.<sup>7</sup> However, <sup>90</sup>Sr waste liquids are extremely complex, typically containing abundant non-radioactive ions (*e.g.*, Na<sup>+</sup>, K<sup>+</sup>, and Mg<sup>2+</sup>) and other fission products.<sup>9</sup> Therefore, highly selective capture of Sr<sup>2+</sup> from such complex radioactive matrices remains a significant challenge.

Current strategies for Sr<sup>2+</sup> removal include solvent extraction,<sup>10,11</sup> chemical precipitation,<sup>12</sup> and adsorption/ion exchange.<sup>13</sup> Among these, adsorption/ion exchange stands out for its cost-effectiveness, operational simplicity, and high efficiency.<sup>14,15</sup> Various ion exchange materials have been widely studied, such as zeolites,<sup>16</sup> layered clay minerals,<sup>17</sup> crystalline silicotitanates,<sup>18</sup> porous coordination polymers,<sup>19</sup> and metal chalcogenides.<sup>20,21</sup> Particularly, inorganic ion exchangers demonstrate potential for radionuclide remediation due to their structural robustness under extreme conditions.<sup>22</sup> Metal phosphate compounds have employed as ion exchange materials for Sr<sup>2+</sup> ion capture, attributed to their good thermostability, radiation resistance,<sup>23</sup> and inherent selective coordination capacity of phosphate groups toward multivalent cations.<sup>23–25</sup> Specifically, tetravalent metal orthophosphates exhibit superior ion exchange characteristics, particularly in nuclear waste treatment scenarios due to their thermal stability, radiation tolerance, and structural stability under acidic conditions.<sup>23,25–29</sup>

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Zirconium phosphate (ZrP) and its structural analogues have been extensively studied as classical materials for Sr<sup>2+</sup> capture.<sup>25,30,31</sup> However, most of them exhibit poor Sr<sup>2+</sup> selectivity in excessive competitive ions (such as Na<sup>+</sup>, K<sup>+</sup>, and Ca<sup>2+</sup>), severely compromising strontium capture.<sup>32–35</sup> For instance, crystalline  $\alpha$ -Zr(HPO<sub>4</sub>)<sub>2</sub>·H<sub>2</sub>O ( $\alpha$ -ZrP) exhibits adsorption capacities of 64.10 mg g<sup>-1</sup> for Cs<sup>+</sup> and 43.03 mg g<sup>-1</sup> for Sr<sup>2+</sup>.<sup>32,33</sup> Meanwhile,  $\gamma$ -Zr(PO<sub>4</sub>)H<sub>2</sub>PO<sub>4</sub>·2H<sub>2</sub>O ( $\gamma$ -ZrP) demonstrates enhanced uptake for both Rb<sup>+</sup> (129.90 mg g<sup>-1</sup>) and Sr<sup>2+</sup> (114.78 mg g<sup>-1</sup>), though excessive Na<sup>+</sup>/Ca<sup>2+</sup> ions severely compromise strontium capture.<sup>34</sup> Kinetic analyses reveal that  $\gamma$ -ZrP's ion exchange rates follow the hierarchy of Cs<sup>+</sup> > K<sup>+</sup> > Rb<sup>+</sup> > Sr<sup>2+</sup>. Recently, potassium-incorporated zirconium phosphate (K<sub>2</sub>Zr(PO<sub>4</sub>)<sub>2</sub>) shows the Sr<sup>2+</sup> capture property but with poor selectivity for Sr<sup>2+</sup> due to the effect of competitive ions (Ca<sup>2+</sup>, Na<sup>+</sup>, and H<sup>+</sup>).<sup>35</sup> Additionally, introducing fluorine into phosphate structures facilitates the formation of highly stable Zr–F bonds, enhancing crystallinity and thermal stability and improving structural diversity and robustness.<sup>36</sup> Nevertheless, crystalline inorganic zirconium phosphate fluoride has never been studied for the removal of radioactive ions.

In this work, a new crystalline zirconium phosphate fluoride [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>] is reported, which is characterized by a layered anionic framework of [Zr(PO<sub>4</sub>)F<sub>2</sub>]<sup>n-</sup> hosting intercalated [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>]<sup>+</sup> cations. It exhibits exceptional Sr<sup>2+</sup> capture across wide pH regimes (1.95–8.46). It has a high Sr<sup>2+</sup> adsorption capacity ( $q_m^{\text{Sr}} = 161.48 \text{ mg g}^{-1}$ ) and rapid capture kinetics (removal rate  $R^{\text{Sr}} = 94.89\%$  within 1 min). Further, it maintains Sr<sup>2+</sup> removal efficiency in the presence of competing Cs<sup>+</sup>, K<sup>+</sup>, Na<sup>+</sup>, Ca<sup>2+</sup>, and Mg<sup>2+</sup> ions. It is also demonstrated that the material can efficiently capture Sr<sup>2+</sup> from actual aqueous systems (especially seawater), surpassing most reported solid sorbents. This study highlights the substantial potential of layered crystalline zirconium phosphate fluorides for radionuclide capture, while establishing a rational design paradigm for developing Sr<sup>2+</sup>-selective ion-exchange materials of crystalline zirconium phosphate fluorides.

## Materials and methods

### Materials

ZrOCl<sub>2</sub>·8H<sub>2</sub>O (98.00%, Shanghai Adamas Reagent Co., Ltd.), *N,N*-dimethylacetamide (abbreviated as DMA, AR, Sinopharm Chemical Reagent Co., Ltd.), 2-hydroxyphosphonoacetic acid (abbreviated as HPAA, 50%, Shanghai Adamas Reagent Co., Ltd.), hydrofluoric acid (abbreviated as HF, AR, ≥40 nt, Shanghai Adamas Reagent Co., Ltd.), HNO<sub>3</sub> (65–68%, China Pharmaceutical Chemical Reagents Co., Ltd.), NaOH (98.00%, Greagent Reagent Co., Ltd.), SrCl<sub>2</sub>·6H<sub>2</sub>O (AR, Guangfu Co., Ltd.), CsCl (99.99%, Shanghai Longjin Metal Materials Co., Ltd.), KCl (AR, Shanghai Titan Co., Ltd.), NaCl (AR, Sinopharm Chemical Reagent Co., Ltd.), CaCl<sub>2</sub>·2H<sub>2</sub>O (74–78%, Shanghai Songjiang Silian Chemical Co., Ltd.), MgCl<sub>2</sub>·6H<sub>2</sub>O (AR, Kelong Co., Ltd.). Ultrapure water was

supplied by a certified laboratory water purification system (Model WP-UP-LH-10, Sichuan Water Treatment Equipment Co., Ltd.). All reagents were purchased directly for use without further purification.

### Synthesis of [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>]

[(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>] was synthesized through a solvothermal process using stoichiometric quantities of ZrOCl<sub>2</sub>·8H<sub>2</sub>O (2.4 mmol, 0.7735 g) and HPAA (2.4 mmol, 0.3745 g) in a mixed solvent system containing DMA (24 mL) and deionized water (5 mL). To modulate crystallization kinetics, HF (0.08 mL) was introduced as a mineralizer.<sup>37</sup> The reaction mixture was then acidified to pH 4 through precise addition of HNO<sub>3</sub> (1 mL), a critical parameter influencing layer assembly.

After homogenization *via* magnetic stirring at ambient temperature, the precursor solution was transferred to a 100 mL Teflon-lined autoclave and subjected to thermal treatment at 200 °C for 72 h under autogenous pressure. This prolonged aging period facilitated the formation of well-defined crystalline phases.

The resultant crystals were isolated by vacuum filtration, followed by sequential washing cycles with deionized water and ethanol (3 × 20 mL each) to remove residual organics. Subsequently, drying under ambient conditions yielded the target compound [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>] (relative molecular mass (*M*) = 270.28 g mol<sup>-1</sup>) as colorless plate-like crystals, where [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>]<sup>+</sup> was generated by the thermal decomposition of DMA as the starting material and (PO<sub>4</sub>)<sup>3-</sup> was generated by the thermal decomposition of HPAA.<sup>38</sup> Yield: 20.13% (calculated based on Zr content). Elemental analysis (EA) validated phase purity: theoretical: C 9.02%, H 3.03%, N 5.26%. Experimental: C 8.97%, H 3.33%, N 4.83%.

### Batch adsorption experiment

The adsorption performance evaluation of [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>] was conducted in 25 mL polyethylene bottles with caps at room temperature. The experimental setup included: phase allocation, precise dosing of [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>] (solid–liquid ratio *m/V* = 1 g L<sup>-1</sup>) and Sr<sup>2+</sup> standard solution into bottles, followed by continuous agitation on a magnetic stirrer for 12 h at ambient temperature. Post-adsorption, aliquots of the supernatant were extracted *via* syringe, filtered through 0.22 μm membranes, and diluted with 2% HNO<sub>3</sub> prior to Sr<sup>2+</sup> concentration analysis by ICP-OES or ICP-MS. The post-adsorption solid phase was isolated from the aqueous medium *via* centrifugal separation at 8000 rpm for 10 min, followed by triple rinsing with deionized water to eliminate residual ions prior to subsequent analysis.

The Sr<sup>2+</sup>-exchanged derivative of [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>] (designated as [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>]-Sr) was synthesized *via* 12 h room-temperature agitation of 200 mg adsorbent in 200 mL of Sr<sup>2+</sup> solution. The resultant [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>]-Sr underwent comprehensive characterization (PXRD, EDS,



SEM, and EA). Experimental particulars are described in the supplementary information (SI).

### Characterization techniques

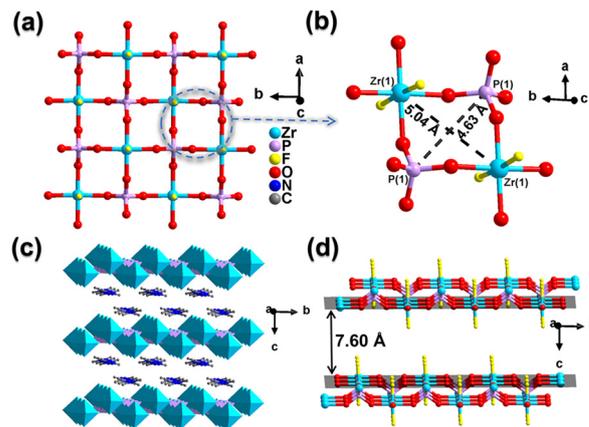
Elemental composition (C, H, N) was quantified *via* high-precision combustion analysis using a Vario EL III EA. Single-crystal X-ray diffraction analysis of  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)_2\text{F}_2]$  was performed on a Rigaku XtaLAB Synergy-R diffractometer equipped with a graphene-monochromated microfocus Mo  $K_\alpha$  radiation source ( $\lambda = 0.71073 \text{ \AA}$ ) at 100 K. Powder X-ray diffraction (PXRD) patterns were acquired at room temperature on a Rigaku Miniflex II system equipped with Cu  $K_\alpha$  radiation ( $\lambda = 1.54178 \text{ \AA}$ ), operating at 30 kV and 15 mA, with a  $2\theta$  scanning range of 5–65°. Elemental composition and spatial distribution were analyzed by energy-dispersive X-ray spectroscopy (EDS) coupled with scanning electron microscopy (SEM, JEOL JSM-6700F). Surface chemical states were investigated *via* X-ray photoelectron spectroscopy (XPS) on a ThermoFisher ESCALAB 240 Xi spectrometer using monochromatic Al  $K_\alpha$  excitation. Solution pH measurements were conducted with a Leimige E-201F digital pH meter (Shanghai, China). The concentration of  $\text{Sr}^{2+}$  and other metal ions were quantitatively measured by inductively coupled plasma optical emission spectroscopy (ICP-OES, Thermo iCAP 7400) and inductively coupled plasma mass spectrometry (ICP-MS, Thermo XSeries II), respectively. Liquid–solid separation was achieved *via* centrifugation using a G16-WS benchtop centrifuge.

## Results and discussion

### Crystal structures

Single-crystal X-ray diffraction (SC-XRD) analysis determines that  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)_2\text{F}_2]$  crystallizes in the monoclinic space group  $P2_1/m$ . The asymmetric unit comprises one Zr atom, one  $\text{PO}_4$  group, two F atoms, and one  $[(\text{CH}_3)_2\text{NH}_2]^+$  cation (Fig. S1). The Zr center adopts a distorted octahedral geometry, coordinated by four oxygen donors from distinct  $\text{PO}_4$  groups (Zr–O: 2.054–2.079  $\text{ \AA}$ ) and two F atoms (Zr–F: 1.972–2.007  $\text{ \AA}$ ). The bond angles span 86.6(3)–93.5(3)° for O–Zr–F and 88.89(10)–91.11(10)° for O–Zr–O, reflecting minor octahedral distortion (Tables S1–S3).

Alternating arrangements of  $\text{ZrO}_4\text{F}_2$  octahedra and  $\text{PO}_4$  tetrahedra by corner-sharing mode generate a 2D anionic layer of  $[\text{Zr}(\text{PO}_4)_2\text{F}_2]_n^{n-}$ , in which each  $\text{ZrO}_4\text{F}_2$  octahedron connects four  $\text{PO}_4$  tetrahedra and each  $\text{PO}_4$  tetrahedron links four  $\text{ZrO}_4\text{F}_2$  octahedra (Fig. 1a). It is found that an eight-membered ring (8-MR) window with dimensions  $4.63 \times 5.04 \text{ \AA}$  is formed by two Zr atoms, two P atoms, and four O atoms in the anionic layer (Fig. 1b). Charge-balancing  $[(\text{CH}_3)_2\text{NH}_2]^+$  cations are intercalated between adjacent layers (Fig. 1c and d), with an interlayer spacing of 7.60  $\text{ \AA}$  (defined as the shortest perpendicular distance between Zr atom of adjacent anionic layers, as defined in Fig. S1).<sup>39</sup> The relatively big interlamellar spacing and the presence of exchangeable



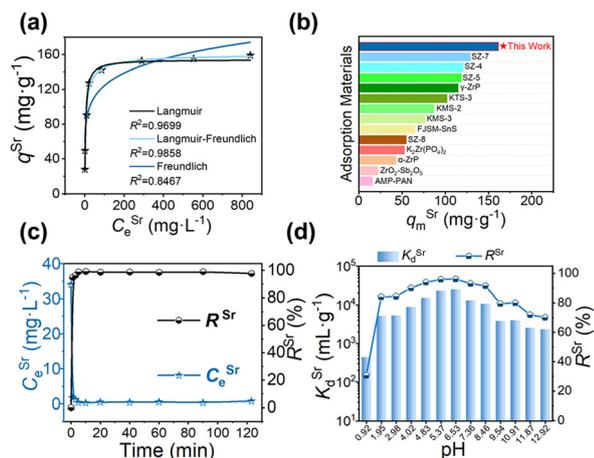
**Fig. 1** Crystal structural diagrams for the compound  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)_2\text{F}_2]$ . (a) A 2D anionic layer of  $[\text{Zr}(\text{PO}_4)_2\text{F}_2]_n^{n-}$  viewed along the  $c$ -axis. (b) Ball-and-stick representation of the eight-membered ring in the anionic layer. (c) View of the packing diagram of  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)_2\text{F}_2]$  along the  $a$ -axis. (d) The anionic  $[\text{Zr}(\text{PO}_4)_2\text{F}_2]_n^{n-}$  layers arrangement illustrating interlayer spacing (7.60  $\text{ \AA}$ ). Color scheme: Zr (cyan), P (purple), O (red), F (yellow), N (blue), C (grey).

$[(\text{CH}_3)_2\text{NH}_2]^+$  cations provide the prerequisite for the  $\text{Sr}^{2+}$  capture *via* the ion exchange way.<sup>40</sup>

### Adsorption isotherms studies

Adsorption isotherm analysis serves as a fundamental methodology for characterizing the surface characteristics and binding affinity of adsorbents, while also determining their maximum adsorption capacity ( $q_m^{\text{St}}$ ). The actual and theoretical (assuming that all available  $[(\text{CH}_3)_2\text{NH}_2]^+$  is fully exchanged by  $\text{Sr}^{2+}$ ) ion-exchange capacity is calculated by eqn (S1) and eqn (S2). The  $\text{Sr}^{2+}$  ions adsorption capacity of  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)_2\text{F}_2]$  was systematically evaluated through equilibrium isotherm studies. Experimental data were modeled using three classical adsorption isotherms: Langmuir (monolayer adsorption), Freundlich (heterogeneous surface), and Langmuir–Freundlich hybrid (multi-mechanism synergy).<sup>41</sup> Nonlinear regression analysis reveals superior correlation for the Langmuir–Freundlich model ( $R^2 = 0.9858$ ) compared to the Langmuir ( $R^2 = 0.9699$ ) and Freundlich ( $R^2 = 0.8467$ ) models (Fig. 2a, Tables S4 and S5, and eqn (S3)–(S5)). This statistical dominance indicates a complex adsorption mechanism involving both monolayer coverage and heterogeneous surface interactions.<sup>41</sup> The derived  $q_m^{\text{Sr}}$  from the Langmuir–Freundlich model reaches 161.48  $\text{ mg g}^{-1}$ , which is higher than that of some crystalline zirconium-based adsorbents such as zirconium fluorophosphonate  $[(\text{CH}_3)_2\text{NH}_2]_2[\text{ZrC}_6\text{H}_4(\text{CH}_2\text{PO}_3)_2\text{F}_2]$  (SZ-7, 129.1  $\text{ mg g}^{-1}$ ),  $[(\text{CH}_3)_2\text{NH}_2][\text{ZrCH}_2(\text{PO}_3)_2\text{F}]$  (SZ-4, 121  $\text{ mg g}^{-1}$ ),<sup>42</sup> and zirconium phosphates such as  $\gamma$ -ZrP (114.78  $\text{ mg g}^{-1}$ ),  $\text{K}_2\text{Zr}(\text{PO}_4)_2$  (52.83  $\text{ mg g}^{-1}$ ), and  $\alpha$ -ZrP (43.03  $\text{ mg g}^{-1}$ ), as visually compared in Table S6 and Fig. 2b.<sup>20,21,42–46</sup> Furthermore, the title compound  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)_2\text{F}_2]$  also outperforms some other inorganic adsorbents





**Fig. 2** Adsorption performance diagrams of the compound  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$ . (a)  $\text{Sr}^{2+}$  adsorption isotherms of  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$  fitted by the Langmuir (black line), Langmuir–Freundlich (azure line), and Freundlich (blue line) models. (b) Comparison of the adsorption capacities of  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$  with other reported inorganic adsorbents for  $\text{Sr}^{2+}$ . (c) The kinetic curves of  $\text{Sr}^{2+}$  removal rate ( $R$ ) by  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$  plotted as the concentration ( $C_e$ ) and  $R^{\text{Sr}}$  of  $\text{Sr}^{2+}$  ions vs. time (min). (d) Distribution coefficient ( $K_d^{\text{Sr}}$ , columns) and removal rate ( $R^{\text{Sr}}$ , line) at various solutions with different initial pH (0.92–12.92).

such as  $\text{K}_{2x}\text{Sn}_{4-x}\text{S}_{8-x}$  ( $x = 0.65\text{--}1$ ) (KTS-3,  $102.00 \text{ mg g}^{-1}$ )<sup>47</sup> and commercial AMP-PAN ( $16 \text{ mg g}^{-1}$ ).<sup>48</sup>

### Adsorption kinetics studies

The rapid capture capability of an adsorption material for radioactive  $\text{Sr}^{2+}$  ions is critical in nuclear emergency management.  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$  demonstrated exceptional adsorption efficiency, achieving a  $\text{Sr}^{2+}$  removal rate of 94.89% within 1 min in neutral aqueous solutions ( $\text{Sr}^{2+}$  concentration: from  $34.04 \text{ mg L}^{-1}$  to  $1.74 \text{ mg L}^{-1}$ , Fig. 2c, Table S7, eqn (S6)). The current compound approached adsorption equilibrium within a 5 min contact period, achieving remarkable  $\text{Sr}^{2+}$  removal efficiency ( $R^{\text{Sr}} = 98.88\%$ ). We systematically investigated the  $\text{Sr}^{2+}$  adsorption mechanism of it using pseudo-first-order and pseudo-second-order kinetic models (Table S8, Fig. S2, eqn (S7) and (S8)).<sup>49</sup> Quantitative analysis demonstrated superior correlation with the pseudo-second-order kinetic model.

### pH effect on adsorption

The pH of aqueous solutions critically governs adsorption processes by mediating proton competition and material stability. To systematically evaluate these effects, the removal performance of  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$  was investigated across a pH range of 0.92–12.92 (Fig. 2d, Table S9, eqn (S9)). The title compound exhibited exceptional adsorption capacities across the pH range of 1.95–8.46, with distribution coefficients ( $K_d^{\text{Sr}}$ ) consistently exceeding  $5 \times 10^3 \text{ mL g}^{-1}$  and  $R^{\text{Sr}}$  above 83.99%, accompanied by a moderate leaching of Zr (Fig. S3a). The leaching rates of Zr of  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$

after being immersed in different acidic (pH of 1.95) or alkaline (pH of 11.87) solutions for 12 h were less than 6.60% (Fig. S3a). At pH 1.95–12.92, the layered anionic architecture of  $[\text{Zr}(\text{PO}_4)\text{F}_2]^{n-}$  is stable, as no phase transition observed by PXRD (Fig. S3b). This indicates that  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$  has relatively wide acid–base stability. Under strongly acidic conditions (pH = 0.92),  $K_d^{\text{Sr}}$  exhibits a substantial reduction to  $4.4 \times 10^2 \text{ mL g}^{-1}$ , possibly attributed to competitive proton exchange, where  $\text{H}^+$  effectively displaces  $\text{Sr}^{2+}$  at  $[(\text{CH}_3)_2\text{NH}_2]^+$  sites. Under extreme acidity, concomitantly partially structural degradation of the anionic layers further diminished the ion-exchange capacity.<sup>30</sup> Subsequently, we employed the pH drift method for analysing the pH dependence of adsorption. The  $\Delta\text{pH}$  ( $= \text{pH}_0 - \text{pH}_f$ ) vs.  $\text{pH}_0$  curve shows the  $\text{pH}_{\text{pzc}}$  value of 5.0 (Fig. S3c). It indicates that the surface of  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$  is positively charged at  $\text{pH} < 5.0$  and negatively charged at  $\text{pH} > 5.0$ . For low pH, the surface of  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$  favours electrostatic attraction of anions, while for high pH, it favours the attraction of cations.

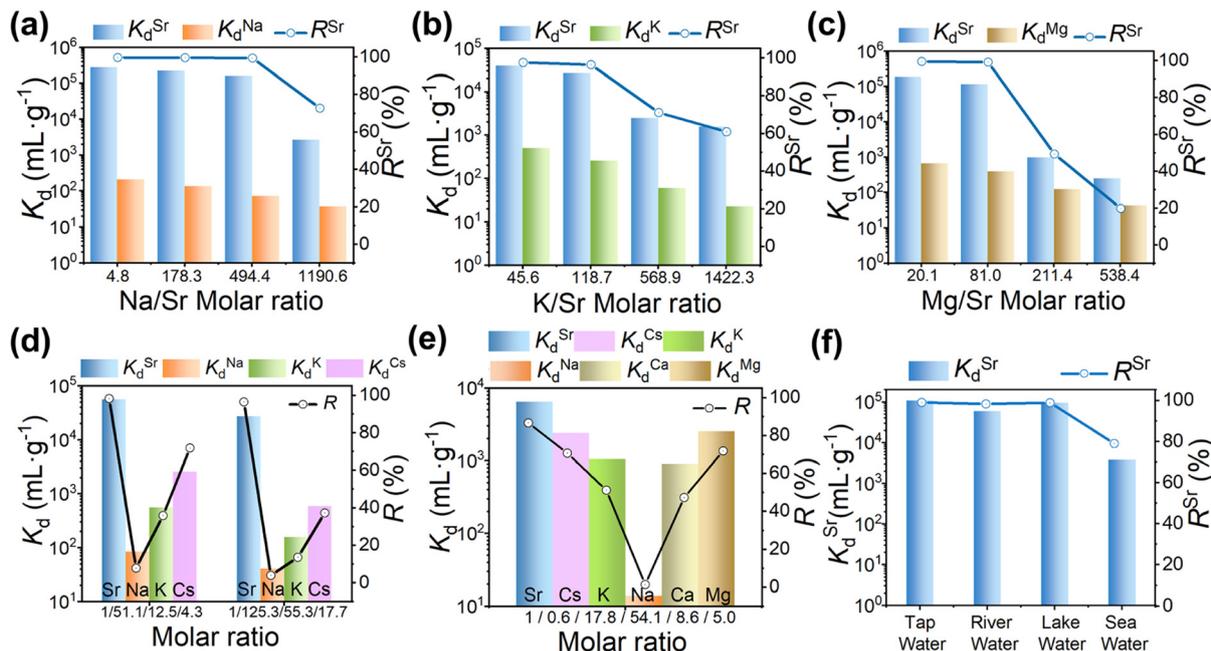
### Competitive adsorption

The presence of high-concentration competing ions ( $\text{Na}^+$ ,  $\text{K}^+$ ,  $\text{Mg}^{2+}$ , and  $\text{Ca}^{2+}$ ) poses significant challenges for selective  $\text{Sr}^{2+}$  removal in nuclear wastewater treatment. Thus, we systematically evaluated the  $\text{Sr}^{2+}$  selectivity of  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$  under competing ions ( $\text{Na}^+$ ,  $\text{K}^+$ ,  $\text{Cs}^+$ ,  $\text{Mg}^{2+}$ , and  $\text{Ca}^{2+}$ ) using separation factor (SF) and distribution coefficient ( $K_d$ ) analyses. Notably, effective SF typically requires values exceeding 100.<sup>50</sup>

Competitive impacts of individual competitive  $\text{Na}^+$ ,  $\text{K}^+$ , and  $\text{Mg}^{2+}$  ions concentrations on  $\text{Sr}^{2+}$  adsorption by  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$  were quantified. At the  $\text{Na}^+/\text{Sr}^{2+}$  molar ratio of 494.4:1, it maintains  $\text{Sr}^{2+}$  removal efficiency of 99.37% ( $K_d^{\text{Sr}} = 1.59 \times 10^5 \text{ mL g}^{-1}$ ,  $\text{SF}_{\text{Sr}/\text{Na}} = 2219.95$ ), confirming excellent  $\text{Na}^+/\text{Sr}^{2+}$  separation (Fig. 3a, Table S10, eqn (S10)). At the  $\text{K}^+/\text{Sr}^{2+}$  molar ratio of 45.6:1,  $K_d^{\text{Sr}}$  reaches  $3.96 \times 10^4 \text{ mL g}^{-1}$  with  $R^{\text{Sr}}$  of 97.54% (Fig. 3b, Table S11). Even under extremely excessive  $\text{K}^+$  ( $C_0^{\text{Sr}} = 5.57 \text{ mg L}^{-1}$ ,  $C_0^{\text{K}} = 294.91 \text{ mg L}^{-1}$ ,  $\text{K}^+/\text{Sr}^{2+}$  molar ratio of 118.7:1),  $K_d^{\text{Sr}}$  reaches  $2.69 \times 10^4 \text{ mL g}^{-1}$  ( $R^{\text{Sr}} = 96.41\%$ ). Notably,  $\text{SF}_{\text{Sr}/\text{K}}$  surpasses 100, confirming exceptional selectivity for  $\text{Sr}^{2+}$  over competing  $\text{K}^+$  ions. At the  $\text{Mg}^{2+}/\text{Sr}^{2+}$  molar ratio of 20.1:1,  $K_d^{\text{Sr}}$  remains  $1.17 \times 10^5 \text{ mL g}^{-1}$  ( $R^{\text{Sr}} = 99.15\%$ ,  $\text{SF}_{\text{Sr}/\text{Mg}} = 299.98$ ), underscoring  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$ 's resilience against the interference of alkaline earth metal ions (Fig. 3c, Table S12). However, when the  $\text{Mg}^{2+}/\text{Sr}^{2+}$  molar ratios are more than 211.4:1, the  $\text{Sr}^{2+}$  removal of the current compound is interfered.<sup>51</sup>

Simultaneously,  $\text{Sr}^{2+}$  selectivity of  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$  was systematically evaluated in mixed  $\text{Na}^+$ ,  $\text{K}^+$ ,  $\text{Cs}^+$ , and  $\text{Sr}^{2+}$  solution and mixed  $\text{Cs}^+$ ,  $\text{K}^+$ ,  $\text{Na}^+$ ,  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$ , and  $\text{Sr}^{2+}$  solution (Fig. 3d and e, Tables S13 and S14), respectively. In the mixed  $\text{Na}^+$ ,  $\text{K}^+$ ,  $\text{Cs}^+$ , and  $\text{Sr}^{2+}$  solution, the material exhibits exceptionally high separation factors ( $\text{SF}_{\text{Sr}/\text{M}} > 100$ ,  $\text{M} = \text{Na}^+$





**Fig. 3** Selectivity performance diagrams of the compound  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$ .  $K_d$  (columns) for  $\text{Sr}^{2+}$ ,  $\text{K}^+$ ,  $\text{Na}^+$ ,  $\text{Mg}^{2+}$  and  $R^{\text{Sr}}$  (line plot) of  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$  at different molar ratios of Na/Sr (a), K/Sr (b), and Mg/Sr (c). (d)  $K_d$  for  $\text{Sr}^{2+}$ ,  $\text{K}^+$ ,  $\text{Na}^+$ ,  $\text{Cs}^+$  and  $R^{\text{Sr}}$  of  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$  in mixed  $\text{Na}^+$ ,  $\text{K}^+$ ,  $\text{Cs}^+$ , and  $\text{Sr}^{2+}$  solution at different molar ratios. (e)  $K_d$  for various metal ions and  $R^{\text{Sr}}$  of  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$  in mixed  $\text{Cs}^+$ ,  $\text{K}^+$ ,  $\text{Na}^+$ ,  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$ , and  $\text{Sr}^{2+}$  solution. (f)  $K_d^{\text{Sr}}$  and  $R^{\text{Sr}}$  of  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$  in tap water, river water, lake river, and sea water.

and  $\text{K}^+$ ) for  $\text{Sr}^{2+}$  under the presence of monovalent competing ions.  $\text{SF}_{\text{Sr}/\text{M}}$  ( $\text{M} = \text{Na}^+$ ,  $\text{K}^+$ ) exceed 668.67 and 173.09 despite the presence of high concentrations for competing ions, whereas  $\text{SF}_{\text{Sr}/\text{Cs}}$  is merely 45.66. Nevertheless, in the mixed  $\text{Cs}^+$ ,  $\text{K}^+$ ,  $\text{Na}^+$ ,  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$ , and  $\text{Sr}^{2+}$  solution, significantly diminished selectivity ( $\text{SF}_{\text{Sr}/\text{M}} < 100$ ,  $\text{M} = \text{K}^+$ ,  $\text{Cs}^+$ ,  $\text{Mg}^{2+}$ , and  $\text{Ca}^{2+}$ ) was observed in monovalent and divalent cation matrices. Remarkably,  $\text{SF}_{\text{Sr}/\text{Na}}$  values still remain elevated (464.99) with concurrent high distribution coefficient ( $K_d^{\text{Sr}} = 6.44 \times 10^3 \text{ mL g}^{-1}$ ) and removal efficiency ( $R^{\text{Sr}} = 86.57\%$ ).

Significantly, further validation in actual aqueous environments including tap water, lake water, river water, and seawater demonstrates consistently high  $R^{\text{Sr}}$  values of 99.09%, 98.34%, 98.97%, and 79.06%, respectively, while  $K_d^{\text{Sr}}$  values exceed  $3.78 \times 10^3 \text{ mL g}^{-1}$  without exception (Fig. 3f, Table S15). The removal rate in actual seawater is higher than that of many reported adsorbents, such as  $\text{K}_2\text{SbPO}_6$  ( $R^{\text{Sr}} = 1.17\%$ )<sup>52</sup> and K-HTNs ( $R^{\text{Sr}} = 35\%$ )<sup>53</sup> at  $m/V = 1 \text{ g L}^{-1}$ . These results unequivocally establish the maintenance of the removal capacity of  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$  in complex contaminated matrices.

### Adsorption and desorption

Reusability serves as a critical performance for ion exchange materials. Remarkably, the Sr-loaded phase  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]\text{-Sr}$  can be efficiently reused through elution with a  $0.5 \text{ mol L}^{-1}$  KCl solution. The sample treated with KCl solution is named  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]\text{-Sr-K}$ . EDS analysis of the eluted material confirms near-complete substitution of

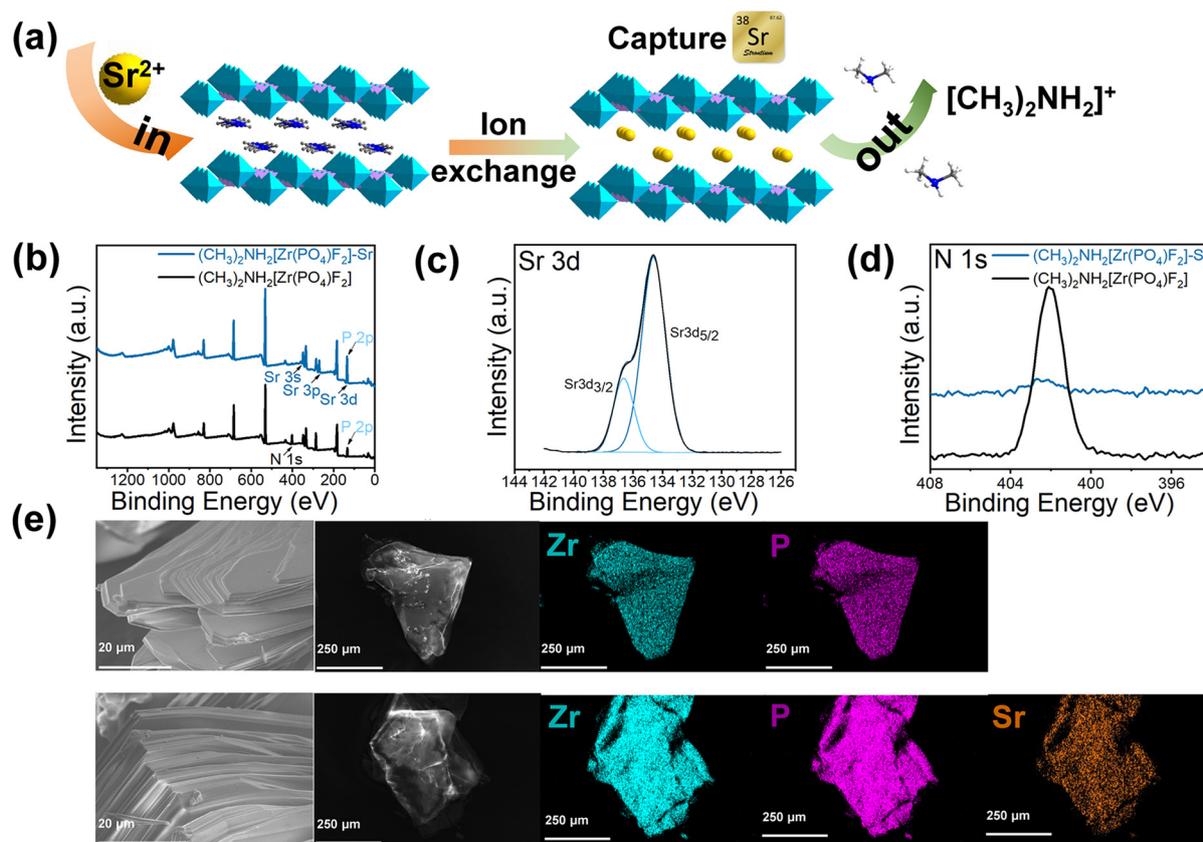
$\text{Sr}^{2+}$  by  $\text{K}^+$  ions (Fig. S4a and b). The eluted material still maintains exceptional  $\text{Sr}^{2+}$  adsorption capacity ( $R^{\text{Sr}} = 93.80\%$ ) over one adsorption–desorption cycle, with high desorption efficiencies ( $E^{\text{Sr}} = 91.47\%$ ) (Table S16, eqn (S11)). Structural integrity preservation is verified through PXRD patterns in cycled samples (Fig. S4c).  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]$  demonstrates reusability capabilities for the sequential capture of  $\text{Sr}^{2+}$  ions in radioactive waste management.

### Adsorption mechanism

PXRD analysis validates no detectable phase transitions observed upon  $\text{Sr}^{2+}$  displacement (Fig. S5). Notably, the (002) diffraction peak of  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]\text{-Sr}$  shifts toward higher Bragg angles ( $\Delta 2\theta = 0.46^\circ$ ) according to the Bragg equation. Corresponding SEM characterization reveals well-defined  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]\text{-Sr}$  crystals exhibiting pristine morphological integrity, evidenced by defect-free planar facets (Fig. S6).

Based on the above evidences, we hypothesized that this follows the ion exchange mechanism, wherein  $[(\text{CH}_3)_2\text{NH}_2]^+$  cations are displaced by  $\text{Sr}^{2+}$  (Fig. 4a). To validate this hypothesis, high-resolution XPS analysis of the pristine and Sr-loaded phases was conducted. All XPS spectra were corrected to the C 1s peak of adventitious carbon at 284.8 eV. XPS spectra reveal Sr 3d and P 2p signals overlap at  $\sim 133.0 \text{ eV}$  in  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)\text{F}_2]\text{-Sr}$  (Fig. 4b),<sup>54</sup> while emergent peaks at 360.0 eV (Sr 3s) and 270.0 eV (Sr 3p) provide unambiguous evidence of strontium integration, accompanied by definitive Sr 3d spectral signatures at





**Fig. 4** Adsorption mechanism diagrams of the compound [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>]. (a) Mechanistic illustration of Sr<sup>2+</sup> exchange within the anionic layers of [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>]. (b) Comparative XPS survey spectra of pristine [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>] (black) and [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>]-Sr (blue). (c) Narrow scan XPS spectrum of Sr 3d of [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>]-Sr. (d) Narrow scan XPS spectra of N 1s in pristine [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>] (black) versus [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>]-Sr (blue). (e) SEM micrographs at magnification of 2.0k, complemented by corresponding elemental distribution profiles of pristine [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>] and [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>]-Sr.

binding energies of 134.6 eV (Sr 3d<sub>5/2</sub>), 136.6 eV (Sr 3d<sub>3/2</sub>) (Fig. 4c). At the same time, N 1s intensity attenuated at 402.1 eV after Sr<sup>2+</sup> capture (Fig. 4d). Collectively, these results confirm that Sr<sup>2+</sup> capture occurs *via* ion exchange between interlamellar [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>]<sup>+</sup> cations and Sr<sup>2+</sup>.

EDS analysis (Fig. S6f) confirmed successful capture of Sr<sup>2+</sup> ions. Elemental mapping reveals a homogeneous distribution of Sr<sup>2+</sup> in [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>]-Sr (Fig. 4e). EA further reveals a concomitant reduction in nitrogen content from 4.83% to 0.43% after Sr<sup>2+</sup> ion exchange (experimental: C 1.50%, H 2.11%, N 0.43%), quantitatively confirming that [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>]<sup>+</sup> ions have been exchanged during ion exchange. Furthermore, the theoretical ion exchange capacity of [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>] for Sr<sup>2+</sup> is calculated as 162.10 mg g<sup>-1</sup> (eqn (S2)), whereas by experimental measurements the adsorption capacity of [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>] for Sr<sup>2+</sup> is 161.48 mg g<sup>-1</sup>. This indicates that the interlamellar [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>]<sup>+</sup> cations are almost completely exchanged by Sr<sup>2+</sup> ions.

In simulated nuclear wastewater containing competing ions (Na<sup>+</sup>, K<sup>+</sup>, Cs<sup>+</sup>, Ca<sup>2+</sup>, and Mg<sup>2+</sup>), (CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>[Zr(PO<sub>4</sub>)F<sub>2</sub>] maintained Sr<sup>2+</sup> removal efficiency. Ion exchange constitutes a stoichiometrically constrained process

wherein charge balance is preserved through equivalent substitution of exchanged cations.<sup>55</sup> The Sr<sup>2+</sup> selectivity of (CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>[Zr(PO<sub>4</sub>)F<sub>2</sub>] may arise from the electrostatic valence-dependency rule: adsorbent affinity scales with cation charge density under constant selectivity coefficients and concentrations of competing cations.<sup>56</sup> Consequently, the [Zr(PO<sub>4</sub>)F<sub>2</sub>]<sup>n-</sup> anionic layers may exhibit preferential binding toward divalent Sr<sup>2+</sup> over monovalent Na<sup>+</sup>/K<sup>+</sup>. This material achieves SF<sub>Sr/Mg</sub> exceeding 100, possibly because the hydrated Sr<sup>2+</sup> diameter (8.24 Å) is smaller than competing cations (Mg<sup>2+</sup>, 8.56 Å).<sup>51</sup>

Thermodynamics of Sr<sup>2+</sup> adsorption on [(CH<sub>3</sub>)<sub>2</sub>NH<sub>2</sub>][Zr(PO<sub>4</sub>)F<sub>2</sub>] was further investigated between 293–353 K (Table S17, Fig. S7). The K<sub>d</sub> values increased with temperature, indicating enhanced adsorption affinity at higher temperatures. The thermodynamic parameters were also calculated using the thermodynamic model (eqn (S13)–(S15)).<sup>57,58</sup> Thermodynamic parameters reveal positive ΔH<sup>0</sup> (29.62 kJ mol<sup>-1</sup>) and ΔS<sup>0</sup> (0.18 kJ mol<sup>-1</sup> K<sup>-1</sup>), confirming an entropy-driven process. Negative ΔG<sup>0</sup> values (-22.10 to -32.55 kJ mol<sup>-1</sup>) demonstrate spontaneous adsorption across the temperature range. The decreasing ΔG<sup>0</sup> with rising temperature further support favourable



adsorption at elevated temperatures. Notably, operational expenditure increases at higher temperatures, necessitating balanced temperature selection.

## Conclusions

Here, a new layered zirconium phosphate fluoride  $[(\text{CH}_3)_2\text{NH}_2][\text{Zr}(\text{PO}_4)_2\text{F}_2]$  was synthesized hydrothermally. This material achieves a maximum  $\text{Sr}^{2+}$  adsorption capacity of  $161.48 \text{ mg g}^{-1}$  (higher than that of many inorganic crystalline adsorbents) and fast kinetics ( $R^{\text{Sr}} = 94.89\%$  within 1 min). It exhibits exceptional pH tolerance (operational range: 1.95–8.46). This material maintains  $\text{Sr}^{2+}$  removal efficiency in the presence of competing  $\text{Cs}^+$ ,  $\text{K}^+$ ,  $\text{Na}^+$ ,  $\text{Ca}^{2+}$ , and  $\text{Mg}^{2+}$  ions. Particularly, it can maintain  $R^{\text{Sr}}$  of 79.06% even in seawater. XPS and thermodynamics confirm that spontaneous  $\text{Sr}^{2+}$  adsorption occurs through ion exchange with interlayered  $[(\text{CH}_3)_2\text{NH}_2]^+$  cations in the current zirconium phosphate fluoride. This work provides a promising adsorbent for capture of radiostrontium in radioactive waste management.

## Author contributions

Z. Y. Chen: data curation, writing – reviewing and editing, validation, formal analysis, investigation, and software. S. Z. Liu: formal analysis and data curation. S. J. Li: formal analysis. Z. H. Chen: formal analysis and visualization. L. Yang: data curation. S. M. Zhang: data curation. H. Y. Sun: funding acquisition, reviewing and editing, supervision, and project administration. M. L. Feng: conceptualization, funding acquisition, review and editing, visualization, supervision, and project administration. X. Y. Huang: review and editing, and project administration. All authors have read and agreed to the published version of the manuscript.

## Conflicts of interest

The authors declare no conflict of interest.

## Data availability

Supplementary information: experimental section (batch adsorption experiments, equations, crystal structures section, and characterization section), and additional tables (Tables S1–S17) and figures (Fig. S1–S7). See DOI: <https://doi.org/10.1039/D5CE00784D>.

CCDC 2466544 contains the supplementary crystallographic data for this paper.<sup>59</sup>

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