





Cite this: *Chem. Commun.*, 2025, 61, 4038

Received 26th December 2024,
Accepted 10th February 2025

DOI: 10.1039/d4cc06745b

rsc.li/chemcomm

Selective hydrogenation of nitrocyclohexane to cyclohexanone oxime over a $\text{Cu}_{12}\text{Ag}_{17}(\text{SR})_{12}(\text{PPh}_3)_4$ cluster catalyst†

Jinzhi Lu, Danyun Yao, Shisi Tang, Xiao Cai, Weiping Ding  and Yan Zhu  *

Atomically precise metal cluster catalysts with crystallographically solved structures have been documented to be promising alternatives to tackle the challenge of selective hydrogenation of organics into high value products. Here we report that a $\text{Cu}_{12}\text{Ag}_{17}(\text{SR})_{12}(\text{PPh}_3)_4$ (SR = 1,3-benzenedithiol) cluster as a heterogeneous catalyst can achieve a highly catalytic selectivity of cyclohexanone oxime in catalytic hydrogenation of nitrocyclohexane, due to the unique synergy in the bimetallic cluster.

It is of paramount importance to develop sustainable green chemical processes to replace traditional chemical processes. Cyclohexanone oxime (CHO) is a key intermediate in the generation of caprolactam, which is an important precursor in the production of nylon fibers, engineering plastics and plastic films.^{1,2} Currently, the industrial production of CHO mainly relies on the reaction of cyclohexanone (CHone) and hydroxylamine salt, while the process has many problems such as low atomic utilization, high energy consumption and serious environmental pollution.^{3,4} Therefore, there is an urgent requirement to develop green, environmentally friendly and efficient technologies for CHO production. The direct reduction of nitrocyclohexane (NCH) to CHO has attracted extensive research due to its high atom economy, easy operation and environmental friendliness.^{5–7} The difficulties of this above technology include the design of high-performance catalysts and the resolution of the contradiction between the conversion of the reactants and the selectivity of the target products.⁴ Initially, the hydrogenation of NCH to CHO was dominated by noble metal catalysts, while the high price of noble metals and the scarcity of raw materials limit the industrialization.^{8,9} Consequently, non-noble metals like Cu and Ni are preferred.^{3,10} For example, Liu *et al.* synthesized MOF-derived Ni@C catalysts containing rich defects, in which

strong metal-support interaction between the defect-rich carbon and Ni was demonstrated to enhance the dispersion of Ni nanoparticles and create electron-deficient Ni sites, thereby attenuating the adsorption of CHO and leading to high selectivity for CHO.² Furthermore, the addition of a second metal has also been utilized to modulate the electronic and chemical properties of the metals to improve their activities. Luo *et al.* prepared a series of activated carbon supported bimetallic Ni-based catalysts, in which the supported CuNi catalyst exhibited highly catalytic performances, since the Cu could effectively improve the reduction of nickel oxides and the dispersion of nickel, and finally CuNi could effectively activate the N–O bond in NCH and facilitate the desorption of CHO as compared with Ni.¹¹ What's more, N doping was utilized to improve the basic properties of the catalysts, which in turn led to an enhanced activity.⁶ Besides, the ethylenediamine (EDA)-modified Pt/ In_2O_3 catalyst gave rise to 100% selectivity in EDA solvent.⁹ However, 100% CHO selectivity has not yet been attained by non-Pt-group metal catalysts.

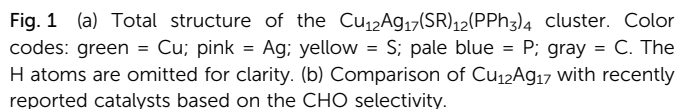
Atomically precise metal clusters with exact atomic numbers and crystal structures have been demonstrated to be remarkable in understanding fundamental catalysis, exhibiting unique catalytic performances in many selective hydrogenation reactions.^{12–16} These metal clusters with small sizes are typically different from conventional metal nanoparticles or metal complex catalysts and they have been demonstrated to tackle the challenge of selective hydrogenation processes into high value products.^{17–19} For example, $\text{Au}_{36}(\text{SR})_{24}$ cluster catalysed the hydrogenation of nitrobenzene in low sulfuric acid content medium to produce exclusively *p*-aminophenol.¹⁹ In this work, we utilized a $\text{Cu}_{12}\text{Ag}_{17}(\text{SR})_{12}(\text{PPh}_3)_4$ (SR = 1,3-benzenedithiol; PPh_3 = triphenylphosphine) cluster to catalyse the hydrogenation of NCH to CHO.

The $\text{Cu}_{12}\text{Ag}_{17}(\text{SR})_{12}(\text{PPh}_3)_4$ cluster, denoted as $\text{Cu}_{12}\text{Ag}_{17}$, was synthesized based on the previously reported method and its atomic-pattern structure is displayed in Fig. 1a.^{20,21} The total structure of $\text{Cu}_{12}\text{Ag}_{17}$ is composed of an Ag_{13} icosahedral kernel, four $\text{Cu}_3(\text{SR})_3$ units and four AgPPh_3 units. In the $\text{Cu}_3(\text{SR})_3$ units, one S atom in each bidentate ligand is attached to a Cu

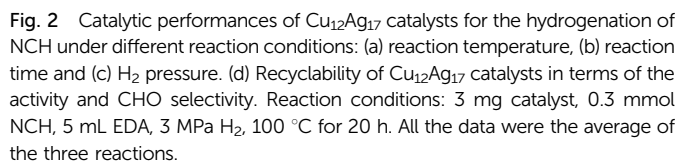
State Key Laboratory of Coordination Chemistry, Key Laboratory of Mesoscopic Chemistry of Ministry of Education, School of Chemistry and Chemical Engineering, Nanjing University, Nanjing 210093, China. E-mail: zhuyan@nju.edu.cn

† Electronic supplementary information (ESI) available. See DOI: <https://doi.org/10.1039/d4cc06745b>



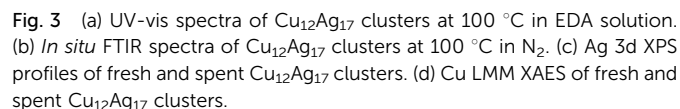


The hydrogenation process of NCH to CHO mainly involves the hydrogenation of NCH, removing one molecule of H₂O to produce nitrosocyclohexane (NSCH), and transferring the α -H to produce CHO. We first explored the catalytic performances of Cu₁₂Ag₁₇ cluster catalysts for the hydrogenation of NCH performed in various solvents. It was found that CHO could give rise to a \sim 100% selectivity of CHO in the EDA solvent (Fig. S1, ESI[†]). CHone was generally obtained by hydrolysis of CHO, suggesting that EDA can promote the oximization and inhibit the hydrolysis of CHO.⁹ Moreover, as shown in Fig. 2a–c, Cu₁₂Ag₁₇ always exhibited \sim 100% selectivity for CHO product performed in a series of reaction conditions, including the reaction temperature, reaction time and hydrogen pressure. This is the first time that \sim 100% selectivity of CHO has been achieved on non-Pt-group metal catalysts (Fig. 1b and



We next investigated the potential reaction mechanism to reveal the reasons for highly selective hydrogenation of NCH to CHO over the $\text{Cu}_{12}\text{Ag}_{17}$ cluster catalyst. The UV-vis spectrum of the spent cluster catalyst showed that the peak at 365 nm disappeared and the peak at 441 nm shifted to 447 nm (Fig. S2, ESI[†]), compared to that of fresh clusters. The spent catalyst after the catalytic reaction was washed several times with methanol to obtain spent $\text{Cu}_{12}\text{Ag}_{17}$ washed catalyst. For the sample washed, its UV-vis spectrum showed that the peak at 365 nm appeared and the peak at 447 nm shifted to 443 nm (Fig. S2, ESI[†]). These observations showed that the $\text{Cu}_{12}\text{Ag}_{17}$ clusters were robust during the reaction. Furthermore, the UV-vis spectra of $\text{Cu}_{12}\text{Ag}_{17}$ clusters in EDA solvent over time were carried out, which suggested that, as shown in Fig. 3a, the interaction of EDA and the cluster possibly led to changes in the difference of UV-vis spectra between fresh and spent catalysts. Time-resolved *in situ* infrared Fourier transform (FTIR) spectra of $\text{Cu}_{12}\text{Ag}_{17}$ clusters performed in a gas-solid-phase reaction cell at 100 °C were also carried out, which showed that the $\text{Cu}_{12}\text{Ag}_{17}$ clusters had an excellent structure stability (Fig. 3b).

Notably, EDA was adsorbed onto the surface of the Cu₁₂Ag₁₇ catalyst during the reaction, which was confirmed by FTIR studies. Deduced from the FTIR spectra of fresh Cu₁₂Ag₁₇ and spent Cu₁₂Ag₁₇ catalysts, as shown in Fig. S3 (ESI[†]), the band at



1597 cm^{-1} assigned to NH_2 bending vibration appeared on the spent $\text{Cu}_{12}\text{Ag}_{17}$ sample,²² suggesting that EDA was adsorbed on the catalyst after the reaction. The N 1s XPS data showed that there were N-containing species from the reaction system adsorbed on the spent catalyst (Fig. S4, ESI†). It was noteworthy that the band at 1434 cm^{-1} assigned to the stretching vibration of triphenylphosphine ligand of the $\text{Cu}_{12}\text{Ag}_{17}$ catalyst almost disappeared after the reaction (Fig. S3b, ESI†),²³ while the peak of P 2p was almost invisible on the X-ray photoelectron spectra (XPS) of the spent $\text{Cu}_{12}\text{Ag}_{17}$ catalyst (Fig. S5, ESI†). These results suggested that PPh_3 was detached from the catalyst during the reaction. Since Ag sites were exposed after the PPh_3 ligands were removed from the cluster, it was likely that EDA adsorbed onto the Ag sites. There was no significant change in the binding energy of Ag 3d of the spent $\text{Cu}_{12}\text{Ag}_{17}$ catalyst, compared to the fresh sample (Fig. 3c), implying that the Ag sites might be coordinated by ligands or EDA.²⁴ It was reported that the N adsorption onto the catalyst surface might enhance the Lewis basicity of the catalyst, thereby promoting CHO synthesis.⁶ For the Cu LMM XAES (X-ray induced Auger electron spectra) of the catalysts (Fig. 3d), the broad peaks were divided into two peaks located at around 917.10 eV and 914.31 eV, which were assigned to Cu^0 and Cu^+ species, respectively.²⁵ There was a slight increase in Cu^0 species on the spent $\text{Cu}_{12}\text{Ag}_{17}$ catalyst, as listed in Table S2 (ESI†), compared to the fresh one.

The formation of CHO by α -H transfer on NSCH and the formation of cyclohexylamine by hydrogenation of NSCH are the two competing pathways during NCH hydrogenation.³ *In situ* FTIR spectra of the NCH hydrogenation over the $\text{Cu}_{12}\text{Ag}_{17}$ cluster catalyst with 3 MPa H_2 for 60 min *via* a gas-solid-phase reaction cell are shown in Fig. 4a and b. The bands at 1374 and 1545 cm^{-1} were assigned to the asymmetric stretching vibration of the NO_2 group of nitrocyclohexane, which were blue-shifted after 60 min of the reaction, indicating that the nitrocyclohexane adsorbed onto the cluster catalyst was being converted (Fig. 4d).³ As the reaction proceeded, the bands of nitrocyclohexane gradually weakened and a new small peak appeared at 1690 cm^{-1} belonging to the $\text{C}=\text{N}$ stretching vibration of the oxime, suggesting that the CHO was produced (Fig. 4a and b).^{3,26} It was noted that cyclohexylamine and cyclohexanone can be condensed to form condensation by-products, while IR signals from the condensation species were not detected, ruling out the generation of condensation by-products.^{2,10} In addition, no other by-products were detected. The results confirmed that the $\text{Cu}_{12}\text{Ag}_{17}$ catalyst was able to adsorb and activate NCH and promoted the isomerization of NSCH, which led to an excellent selectivity of CHO. The *in situ* FTIR spectra for the interaction of the $\text{Cu}_{12}\text{Ag}_{17}$ catalyst with H_2 at room temperature are shown in Fig. 4c, where a peak assigned to a Cu-H signal at 1044 cm^{-1} appeared and gradually intensified with the increase of the contact time with H_2 .²⁷ The peak remained visible after 30 min of N_2 purging, suggesting that the Cu atoms of the $\text{Cu}_{12}\text{Ag}_{17}$ catalyst served as the active sites for H_2 adsorption and activation. This could possibly account for more Cu^0 species on the catalyst after the reaction (Table S2, ESI†). Therefore, the Cu sites in $\text{Cu}_{12}\text{Ag}_{17}$ were responsible for the activation of hydrogen, while the adsorption of EDA on the Ag

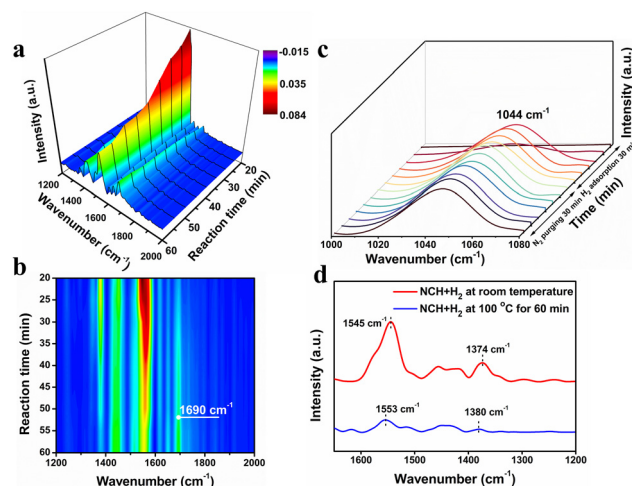


Fig. 4 (a) and (b) Time-resolved *in situ* FTIR spectra of the intermediates and products formed on $\text{Cu}_{12}\text{Ag}_{17}$ clusters for NCH hydrogenation with 3 MPa H_2 at 100 °C. (c) FTIR spectra collected in the $\text{Cu}_{12}\text{Ag}_{17}$ clusters with H_2 at room temperature and then N_2 purging for 30 min. (d) FTIR spectra of NCH with H_2 at room temperature and NCH with H_2 at 100 °C for 60 min on the $\text{Cu}_{12}\text{Ag}_{17}$ clusters, respectively.

sites promoted the conversion of NCH, constituting a two-site synergy of Cu and Ag in this bimetallic cluster.

In summary, we report that an atomically precise $\text{Cu}_{12}\text{Ag}_{17}(\text{SR})_{12}(\text{PPh}_3)_4$ cluster as a heterogeneous catalyst can exhibit an excellent catalytic performance in the hydrogenation of NCH to yield CHO, which can be comparable to the high-performance Pt-group metal catalysts. The high selectivity of CHO from the hydrogenation of NCH is mainly attributed to the unique synergy in this $\text{Cu}_{12}\text{Ag}_{17}(\text{SR})_{12}(\text{PPh}_3)_4$ cluster, in which the Ag sites might bind with the EDA molecules and the Cu sites may be responsible for the adsorption and activation of hydrogen. This work can provide a distinct insight into catalytic hydrogenation of atomically precise cluster catalysts, which is different from conventional metal nanoparticles. Atomically precise metal catalysts are promising alternatives to tackle the challenge of selective hydrogenation processes into high value products.

We acknowledge financial support from the National Natural Science Foundation of China (22125202, 92461312, U24A20487, 92361201) and the Natural Science Foundation of Jiangsu Province (BK20220033).

Data availability

The data supporting this article have been included as part of the ESI.†

Conflicts of interest

There are no conflicts to declare.

Notes and references

- 1 P. Serna, M. Lopez-Haro, J. Calvino and A. Corma, *J. Catal.*, 2009, 263, 328–334.



- 2 P. Yuan, X. Liao, H. Cui, F. Hao, W. Xiong, H. Luo, Y. Lv and P. Liu, *ACS Catal.*, 2023, **13**, 3224–3241.
- 3 Y. Zhang, X. Liao, H. Cui, H. Luo, Y. Lv and P. Liu, *J. Colloid Interface Sci.*, 2024, **678**, 353–365.
- 4 E. Kowalewski and A. Srebrowata, *Catal. Sci. Technol.*, 2022, **12**, 5478–5487.
- 5 F. Yao, S. Liu, H. Cui, Y. Lv, Y. Zhang, P. Liu, F. Hao, W. Xiong and H. Luo, *ACS Sustainable Chem. Eng.*, 2021, **9**, 3300–3315.
- 6 P. Yuan, X. Liao, H. Cui, F. Hao, W. Xiong, H. Luo, P. Liu and Y. Lv, *Chem. Eng. J.*, 2023, **455**, 115824.
- 7 Q. Zhang, J. Dong, Y. Liu, Y. Cao, H. He and Y. Wang, *Chem. Commun.*, 2017, **53**, 2930–2933.
- 8 M. Liqiu, L. Xing, L. Guang, Y. Dulin, Y. Kui and L. He, *Chem. Ind. Eng. Prog.*, 2009, **28**, 1024–1026.
- 9 Q. Wu, W. Zhou, H. Shen, R. Qin, Q. Hong, X. Yi and N. Zheng, *CCS Chem.*, 2023, **5**, 1215–1224.
- 10 Y. Zhang, X. Liao, H. Cui, H. Luo, Y. Lv and P. Liu, *ACS Sustainable Chem. Eng.*, 2024, **12**, 595–609.
- 11 F. Yao, S. Liu, H. Cui, Y. Lv, Y. Zhang, P. Liu, F. Hao, W. Xiong and H. Luo, *ACS Sustainable Chem. Eng.*, 2021, **9**, 3300–3315.
- 12 J. Dong, J. Robinson, Z. Gao and L. Wang, *J. Am. Chem. Soc.*, 2022, **144**, 12501–12509.
- 13 C. Liu, H. Abroshan, C. Yan, G. Li and M. Haruta, *ACS Catal.*, 2016, **6**, 92–99.
- 14 G. Li, D. Jiang, S. Kumar, Y. Chen and R. Jin, *ACS Catal.*, 2014, **4**, 2463–2469.
- 15 G. Li, C. Zeng and R. Jin, *J. Am. Chem. Soc.*, 2014, **136**, 3673–3679.
- 16 G. Li and R. Jin, *J. Am. Chem. Soc.*, 2014, **136**, 11347–11354.
- 17 T. Song, Z. Yao, G. Li, X. Cai, X. Liu, Y. Wang, W. Ding and Y. Zhu, *ACS Catal.*, 2023, **13**, 10878–10886.
- 18 D. Yang, W. Pei, S. Zhou, J. Zhao, W. Ding and Y. Zhu, *Angew. Chem., Int. Ed.*, 2020, **59**, 1919–1924.
- 19 J. Lu, K. Tang, G. Qi, C. Juan, J. Xu, Z. Cai, D. Li, X. Cai, X. Liu, M. Chen, W. Ding and Y. Zhu, *Chem. Sci.*, 2024, **15**, 15617–15624.
- 20 X. Kang, H. Abroshan, S. Wang and M. Zhu, *Inorg. Chem.*, 2019, **58**, 11000–11009.
- 21 G. Li, J. Hou, X. Lei, D. Li, E. Yu, W. Hu, X. Cai, X. Liu, M. Chen and Y. Zhu, *Angew. Chem., Int. Ed.*, 2023, **62**, e202216735.
- 22 S. Korpayev, C. Kavakli, S. Colak and A. Kavakli, *Cellulose*, 2018, **25**, 813–828.
- 23 X. Cai, W. Hu, S. Xu, D. Yang, M. Chen, M. Shu, R. Si, W. Ding and Y. Zhu, *J. Am. Chem. Soc.*, 2020, **142**, 4141–4153.
- 24 G. Chen, C. Xu, X. Huang, J. Ye, L. Gu, G. Li, Z. Tang, B. Wu, H. Yang, Z. Zhao, Z. Zhou, G. Fu and N. Zheng, *Nat. Mater.*, 2016, **15**, 564–569.
- 25 J. Pang, M. Zheng, C. Wang, X. Yang, H. Liu, X. Liu, J. Sun, Y. Wang and T. Zhang, *ACS Catal.*, 2020, **10**, 13624–13629.
- 26 S. Ramalingam, M. Karabacak, S. Periandy, N. Puviarasan and D. Tanuja, *Spectrochim. Acta, Part A*, 2012, **96**, 207–220.
- 27 C. Lousada, R. Fernandes, N. Tarakina and I. Soroka, *Dalton Trans.*, 2017, **46**, 6533–6543.

