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Dynamic restructuring of electrocatalysts in the activation of small molecules: challenges and opportunities

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Electrochemical activation of small molecules plays an essential role in sustainable electrosynthesis, environmental technologies, energy storage and conversion. The dynamic structural changes of catalysts during the course of electrochemical reactions pose challenges in the study of reaction kinetics and the design of potent catalysts. This short review aims to provide a balanced view of *in situ* restructuring of electrocatalysts, including its fundamental thermodynamic origins and how these compare to those in thermal and photocatalysis, and highlighting both the positive and negative impacts of *in situ* restructuring on the electrocatalyst performance. To this end, examples of *in situ* electrocatalyst restructuring within a focused scope of reactions (*i.e.* electrochemical CO₂ reduction, hydrogen evolution, oxygen reduction and evolution, and dinitrogen and nitrate reduction) are used to demonstrate how restructuring can benefit or adversely affect the desired process outcome. Prospects of manipulating *in situ* restructuring towards an energy-efficient and durable electrocatalytic process are discussed. The practicality of pulse electrolysis on an industrial scale is questioned, and the need for genius schemes, such as self-healing catalysis, is emphasized.

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1. Introduction

Stable performance of catalyst (*i.e.* maintaining its activity and selectivity over an extended duration) is a key consideration in chemical processes. In heterogeneous catalysis, the interaction between catalyst surface and adsorbed species (*e.g.* reactants, intermediates, products, *etc.*) and that with the surroundings

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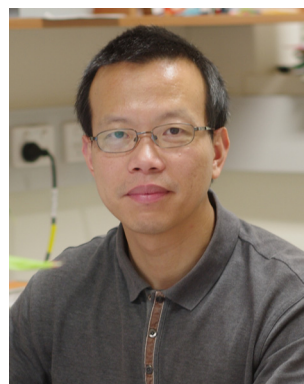
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(e.g. temperature, applied electric potential, radiation, *etc.*) often induce structural transformation of the catalyst during reaction. Such restructuring can be morphological and/or compositional, and the spatial and temporal scales of which can span from nano- to micrometers, and from sub-seconds to hours, respectively.¹ Based on the energy input/output, heterogeneous catalysis can be categorized into thermal-, electro-, and photocatalysis, and the catalyst restructuring involved in each is highly related to the energetics near the catalyst surface.² In thermal catalysis, energy is supplied to the catalyst as heat to produce phonons, and the change in reaction Gibbs free energy from varying reaction conditions is usually less than several tens of milli-eV. Given that reaction enthalpy is a weak function of temperature, a change in temperature by 100 °C for example only results in milli-eV level difference in reaction Gibbs free energy (the exact value depends on the molar entropy change of the reaction of interest). In electro- and photocatalysis, the Gibbs free energy involved is notably larger (e.g. an applied/output voltage of several volts is common in electrocatalysis; while photoexcitation at around 3 eV is frequently seen in semiconductors to generate charge separation in photocatalysis^{3,4}) and therefore is accompanied by pronounced structural change and often deactivation. In addition, the flow of electrons across multiple interfaces is involved in electrocatalysis (*i.e.* electrolyte/catalyst, catalyst/support, support/current collector, *etc.*) and in photocatalysis (*i.e.* metal/dielectric support, *etc.*), where the accumulation charge tends to occur at locations of high surface curvature. Such inhomogeneity in surface charge distribution may produce extremely high local current density⁵ and lead to catalyst restructuring and/or corrosion of other components.⁶

It should be noted that the restructuring of catalyst is dynamic throughout the course of reaction and that the freshly prepared catalyst functions only as a pre-catalyst, as the active sites of the former are most likely different from those during operating reaction conditions.^{1,2} Based on the above, promoters are often incorporated into pre-catalysts to guide the structural transformation towards enhanced catalytic performance⁷ (*i.e.* mass/volume normalized turnover frequency, selectivity towards the target product, and durability). In the Haber–Bosch process, for example, structural promoters such as Al₂O₃ and CaO are incorporated into iron oxides to stabilize the grain boundaries of the latter against sintering.^{8,9} Potassium oxide is used as an electronic promoter in the Haber–Bosch process, which in its active form facilitates the dissociative adsorption of dinitrogen.¹⁰ As another example, in electrochemical CO₂ reduction (ECO₂R), halide ions in the electrolyte^{11–16} are used as promoters to steer the restructuring of copper oxides^{17–22}/halides²³ towards a roughened Cu surface under applied potentials, which results in improved selectivity to multi-carbon products.^{24–26}

While comprehensive reviews focusing on the *in situ* restructuring of electrocatalysts in one specific reaction (e.g. ECO₂R,²⁷ OER,^{28–32} *etc.*) or on characterization techniques that track the species and structural evolution during electrocatalytic reactions^{33,34} are available, works covering the fundamental driving force of restructuring in electrocatalysis over a range of reactions^{35–38} and how it compares with other heterogeneous

catalytic reactions (*i.e.* thermal and photocatalysis)² are relatively few. In this short review, a balanced view of electrocatalyst reconstruction is provided, including its thermodynamic origins and the associated positive and negative effects on catalytic performance. While the aim is not to cover all electrocatalytic reactions involving simple molecules, we focus on the *in situ* restructuring of electrocatalysts during the activation of small molecules (e.g. CO₂, H₂, O₂, N₂ and NO₃[−]) as examples to demonstrate the general applicability of the thermodynamic driving force and highlight the possibility of achieving enhanced catalytic performance through controlled restructuring. The thermodynamic origins of restructuring in electrocatalysis are first introduced and collated with those in thermal and photocatalysis. Next, examples of how *in situ* restructuring adversely impacts the electrocatalytic performance are presented, followed by the opposite cases where it benefits the outcome of electrocatalysis. Finally, perspectives and outlooks on regulated restructuring towards energy-efficient and durable electrocatalytic processes are presented.

2. Origins of restructuring in electrocatalysis

The restructuring of electrocatalysts occurs under reaction conditions to decrease the net free energy of the system. The fact that the state of the electrocatalytic system changes during cell operation (e.g. change in electrode potential, species concentration, exposed surface area, *etc.*) suggests that the driving force for catalyst restructuring also varies throughout the reaction. Origins leading to such dynamic restructuring can be classified into three categories: surface energy reduction, electrode potential, and interaction with an electrolyte and adsorbed species. The following describes how each serves as the driving force for *in situ* structural transformation.

2.1. Surface energy reduction

In a system of particles, the thermodynamic tendency is to lower the energy of the system through the reduction of the surface free energy. This driving force is fundamental and universal, and the effects of which can be observed throughout heterogeneous catalysis (*i.e.* electro-, thermal-, and photocatalysis). Phenomena associated with surface energy reduction include aggregation (assembly of particles with individual boundary maintained),³⁹ coalescence (merge of particles in which individual boundary is lost),⁴⁰ sintering (merge of particles when the temperature is elevated),⁴¹ and Ostwald ripening (dissolution of high-surface-energy sites followed by redeposition onto low-surface-energy sites).^{40,42,43} Since surface energy reduction often results in a decreased catalytically active interface area, it is often considered as a deactivation mode in literature.^{44–46} To keep a focused theme of this work on the restructuring of electrocatalysts, driving forces that are more relevant to electrocatalysis are discussed in detail in the following text.

2.2. Electrode potential

An electrocatalytic reaction involves the transfer of electrons between catalysts and reactants on an electrified surface, and

The interaction of metal catalysts with species present in the electrolyte can lead to a considerable lowering of the reduction potential of the metal, making the dissolution of which more thermodynamically favourable. In copper-catalyzed ECO_2R for example, some of the reaction products (*i.e.* adsorbed CO and oxalate) can form stable complexes with cuprous ions and promote dissolution-related surface reconstruction, such as Ostwald ripening.^{43,66} Studies on gas-solid interfaces have shown that specific adsorption (*e.g.* CO on Cu) lowers the formation energy of adatoms, especially on step edges and kinks.^{67–71} Such



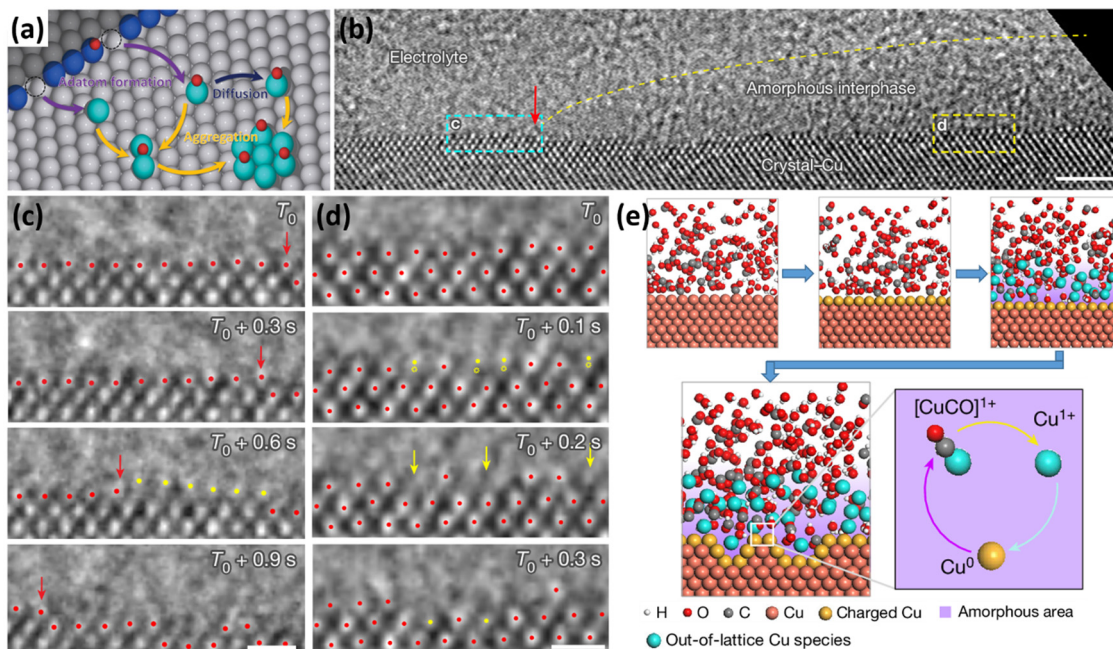


Fig. 2 Adsorbate-mediated surface reconstruction. (a) Schematic of adsorbate-decorated adatom formation, diffusion and migration on the catalyst particle surface. (b) *In situ* liquid-cell TEM image showing the amorphous interphase between the electrolyte and crystalline Cu. Scale bar, 2 nm. (c) and (d) Time-resolved magnified TEM images of regions highlighted in (b). Yellow dots and arrows signify the disappearance of Cu atoms from the crystalline phase. Scale bar 5 Å. (e) Schematic illustration of the restructuring process at the amorphous interphase. Figures adapted with permission from ref. 67 ((a)). Copyright 2023. American Association for the Advancement of Science; and ref. 82 ((b)–(e)). Copyright 2024. Springer Nature.

adsorbate-decorated adatoms have notably increased surface mobility, and tend to form nanoclusters (Fig. 2a) which function as highly active sites for thermo-catalytic reactions such as CO oxidation and water-gas shift,^{67,68,72,73} methanol synthesis,^{69,74} ammonia synthesis/oxidation,^{75,76} and Fischer-Tropsch synthesis.⁷⁶ In electrocatalytic reactions, adsorbate-promoted atom mobility on the catalyst surface is also observed in HER^{77,78} and ECO₂R,^{79–81} as evidenced by the *in situ* formation of undercoordinated sites similar to those reported in thermos-catalytic studies. Direct observation of adsorbate-induced highly mobile Cu surface has been achieved *via in situ* liquid-cell transmission electron microscopy (TEM), and the former is visualized as an amorphous fluid-like layer flowing across the crystalline Cu surface (Fig. 2b–e).⁸² For metal alloy catalysts, the interaction with species present in the electrolyte may lead to segregation, the separation of the originally uniform phase into multiple domains of different compositions. For example, CuAg alloy catalyst during ECO₂R may phase-separate into a core-shell structure with a Cu-rich surface^{80,83} due to stronger binding energy of CO on Cu than that on Ag.⁸⁴

In many instances, the effects of the electrode potential and adsorbate/electrolyte species are intertwined, and both contribute to the restructuring of catalysts. In ECO₂R, the reversible generation/disappearance of Cu nanoclusters from nitrogen-coordinated Cu single-atom catalysts with respect to applied potential has been observed *via in situ* X-ray absorption spectroscopy (XAS).^{85–87} While the formation of clusters from single-atom sites is induced by adsorbate-promoted mobility (*i.e.* *H–Cu⁸⁸ and CO–Cu⁸⁹) under applied potential, the redispersion of clusters back to nitrogen-coordinated single-atoms is

facilitated by hydroxyl radicals produced from the reaction between water molecules and bicarbonate anions near cathode at open-circuit potential.^{88,90} In OER, the strongly oxidizing electrode potential transforms metal nanoparticle pre-catalyst into oxides, and the lattice oxygen mechanism suggests that oxygen atoms in the metal oxide crystal are constantly ejected as O₂ gas, and replenished from adsorbed hydroxide anions.^{91–96} In this case, the effects of adsorbed hydroxide and electrode potential on OER catalyst restructuring are intertwined and both contribute to the lattice oxygen mechanism.

3. Impacts of *in situ* catalyst restructuring on electrocatalytic performance

In the previous section, we see that the restructuring of electrocatalysts depends on multiple (coupled) factors and that the structural change of the catalyst is dynamic throughout the course of the reaction. The impact of restructuring can be beneficial or unfavourable to the catalyzed process, depending on the targeted outcome. The following text discusses the negative and positive impacts of *in situ* catalyst restructuring, using reports on ORR, OER, ECO₂R, HER, and nitrogen electro-redox reactions as examples.

3.1. Negative impacts

In situ restructuring of electrocatalysts often results in diminished activity and/or selectivity on an industrially-relevant time

scale, if not on a laboratory time scale. Therefore, control strategies towards mitigated or regulated restructuring are at the focal point of electrocatalysis research. In the following, cases where restructured electrocatalysts deliver decreased activity and/or selectivity are discussed.

Electrocatalysts operating under high electrode potentials (e.g. OER and ORR catalysts) are prone to metal dissolution. In general, leaching of metal in the cell may lead to deactivation in two folds. One is the loss of electronic and geometric effects beneficial to the activity enhancement, and the other relates to the adverse effects of leached metals on other cell components (i.e. deposition on a low-potential electrode,⁹⁷ deposition within the membrane electrolyte,^{98,99} Fenton reaction that promotes membrane degradation,¹⁰⁰ etc.). In PtM (M is a less noble metal than Pt) ORR catalysts, the outcome of *in situ* restructuring depends on the interplay of M dissolution and Pt surface diffusion,⁵⁵ and is strongly potential dependent, as evidenced by several *in situ* characterization techniques on PtNi ORR catalyst.⁵⁶ At the normal operating potential range of proton exchange membrane fuel cell (PEMFC) cathode, 0.6–1.0 V vs. reversible hydrogen electrode (RHE), PtNi particles maintain their structure (probed *via in situ* electrochemical atomic force microscopy) despite pronounced leaching of Ni content, as verified *via* on-line inductively coupled plasma mass spectrometry. However, at extremely high potentials of 1.3–1.5 V vs. RHE, which occur transiently during the start-up and shut down of the PEMFC, significant coalescence was observed as the *in situ* grazing-incidence small-angle X-ray scattering data suggested a notably increased particle diameter, standard deviation of the particle diameter, and minimum interparticle distance, while the volume fraction of Pt nanoparticles decreases.⁵⁶ Upon metal leaching, the ensuing change in the catalyst particle size (i.e. wider particle size distribution) and the roughened surface with high-surface-energy sites exposed favour Ostwald ripening.¹⁰¹ The effects of leaching are observed in PEMFC cathode as increased catalyst particle size for Pt and PtM (M = Co, Ni) catalysts,^{102,103} as hollow Pt shells for Pt@Pd core-shell catalysts,¹⁰⁴ as the appearance of a Pt^{-98,105} or Pd-band⁹⁹ in the membrane.

Segregation is a common issue in electrocatalysis, where the near-surface composition of a synthesized pre-catalyst is altered *via* nanoscale rearrangement of constituent atoms into different phases under electrochemical conditions. Aside from electrode potential and possible adsorbate that change dynamically during the reaction, the influence of ambient oxygen on catalyst segregation can be a critical factor for the stability of alloy catalysts according to density functional theory (DFT) calculations, and therefore should also be included as a design consideration.¹⁰⁶ While catalyst segregation can be readily regulated in thermal catalysis through activation or regeneration under a selected reducing atmosphere,^{107–112} reliable control of segregation in electrocatalysis can be challenging due partly to the increased system complexity.¹⁰⁶ When aiming to direct an electrocatalyst towards targeted phase(s) (e.g. solid-solution, intermetallic, core-shell, etc.) through the applied potential for example, factors such as the electrolyte pH, possible adsorbates, and the electrochemical

window of the solvent are coupled to the electrode potential and impact the outcome of segregation. In ECO₂R, segregation usually deactivates alloy catalysts through the removal of sites for C–C coupling,¹¹³ loss of targeted electronic interaction,^{80,114} or coverage of ECO₂R-inactive metal on the surface.¹¹⁵ For example, X-ray absorption fine-structure spectroscopy (XAFS) was used to track the evolution of oxidation state and coordination environment of constituents in CuZn catalyst during ECO₂R, and it was discovered that phase-segregated Cu–ZnO promotes methane production, while solid solution CuZn formed after prolonged operation suffers from pronounced HER.¹¹⁴ As another example, through *in situ* nuclear resonant inelastic X-ray scattering and XAFS, it was observed that iron atoms in CuFe alloy segregate to the surface during ECO₂R due to the stronger adsorption energy to CO intermediate, resulting in an enhanced HER.¹¹⁵

The restructuring of the catalyst in ECO₂R is specific with respect to the product–metal pair, and the combined effects of multiple processes eventually lead to deactivation of the catalyst.^{44–46} In Cu-catalyzed ECO₂R for example, the reaction intermediate/product of *CO (adsorbed intermediate) and oxalate can interact strongly with Cu, and stabilize cuprous (Cu⁺) cation in the solution phase, therefore exacerbating dissolution-related structural transformation.^{43,66,116} The structural evolution of Cu nanoparticles in ECO₂R generally follows a chronological order of cathodic corrosion, aggregation and coalescence, surface roughening and smoothening, resulting from dissolution–deposition, adatom migration, etc.¹¹⁷ Some of these processes are captured nicely using *in situ* liquid-cell TEM, such as cathodic corrosion,^{117–119} adsorbate-induced atomic migration⁸² and segregation,⁸⁰ Ostwald ripening⁴³ and coalescence (Fig. 3).¹¹⁷ Cu-based catalysts may initially experience a period of activation (i.e. increasing selectivity for multi-carbon products with respect to time) due to the exposure of high-index crystal facets from cathodic corrosion and adsorbate-induced formation of nanoclusters. At a time scale relevant to industrial applications, however, the activity towards the target product decreases as Ostwald ripening and coalescence gradually take effects, as shown in Fig. 3.¹¹⁷

In electrochemical ammonia synthesis from dinitrogen^{120,121} or nitrate,^{122–125} HER is a major side-reaction similar to the case of ECO₂R. *In situ* restructuring during ammonia synthesis may lead to increased selectivity towards HER, especially under highly cathodic overpotentials.^{123,126} Manipulation of the morphology of pre-catalyst has been shown to enhance the electrochemical dinitrogen reduction reaction (e-NRR) through suppressing HER^{127,128} and enhanced adsorption of dinitrogen on the catalyst surface.¹²⁹ It should be noted that the identification of restructuring during e-NRR can be quite challenging, as the background/artefact of the dominant HER often masks the structural evolution due solely to e-NRR.¹³⁰ In electrochemical dinitrogen oxidation reaction (N₂OR) to nitrate, activation of dinitrogen and suppression of parasitic OER are the two major challenges in catalyst design.¹³¹ In this case, *in situ* restructuring of N₂OR catalyst towards a defect-rich oxide/oxyhydroxide is undesirable,^{132–134} as such amorphous layers favor OER.¹³⁵ For example, in N₂OR *via* oxygen-vacancy-enriched tin oxide, enhanced faradaic efficiency

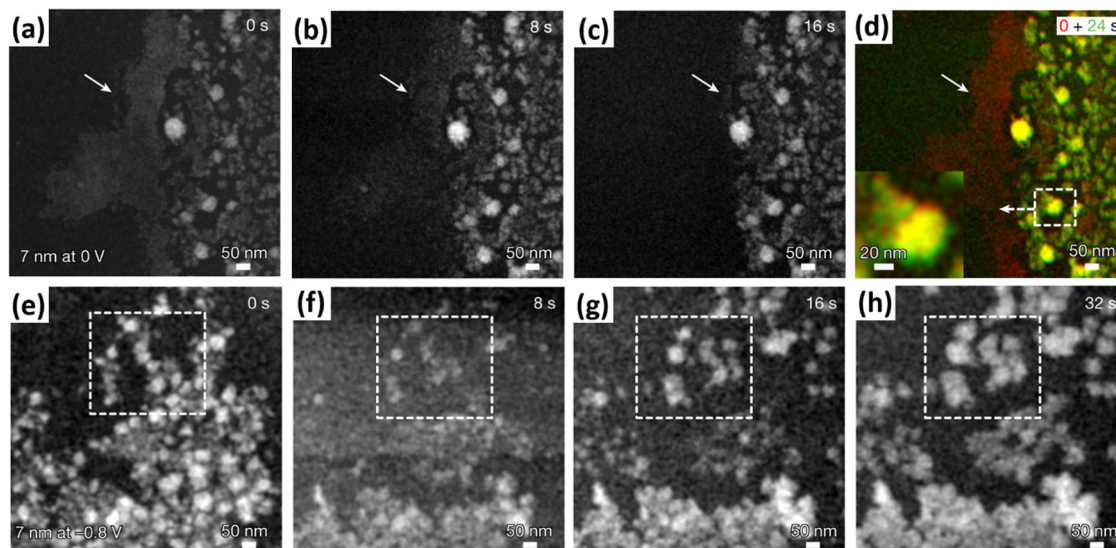


Fig. 3 *In situ* liquid-cell TEM images capturing the time evolution of Cu nanoparticles at different electrode potentials. (a)–(d) at open-circuit potential at time = 0, 8, 16, and 24 seconds. (e)–(h) under -0.8 V vs. RHE at time = 0, 8, 16, and 32 seconds. Figures adapted with permission from ref. 117. Copyright 2023. Springer Nature.

and yield towards nitrate were attributed to decreased activation energy barrier for the activation of $\ast\text{N}_2$ to $\ast\text{N}_2\text{OH}$ through DFT calculations.¹³⁴

Aggregation and coalescence are mechanisms that apply to a system of particles, irrespective of the specific electrochemical reaction. Coalescence usually follows aggregation as the former further reduces the surface energy of the system by eliminating the surface area of the interface, and both lead to a decrease in the number of accessible active sites.¹³⁶ Exemplary cases of proper anchoring of molecular catalyst (*e.g.* cobalt phthalocyanine) on the selected substrate (*e.g.* functionalized carbon nanotube, graphene) against aggregation and coalescence have been demonstrated in ORR^{137,138} and ECO_2R ,^{139–143} where the electronic interaction not only immobilize the catalyst molecule, but also fine-tune its catalytic property. Immobilization of single atom active sites into an extended network (*i.e.* metal–organic frameworks,^{139,144} covalent organic frameworks¹⁴⁵) contributes to increased site density,^{142,143,146,147} but the stability of these frameworks under electrochemical conditions (*i.e.* combined effects of the applied electrode potential and electrolyte pH) remains a challenge for long-term operation.^{148,149} For nanoparticle catalysts, physical confinement through carbon-based support has found some success in delaying the aggregation in the HER,¹⁵⁰ OER,¹⁵¹ ORR^{152,153} and ECO_2R .^{154–156}

3.2. Positive impacts

In instances where the active form generated from pre-catalyst demonstrates favoured catalytic performance (such as improved selectivity towards a specific product, enhanced reaction kinetics, *etc.*) but is rather short-lived, approaches to induce restructuring that leads to the regeneration of desired active form are often implemented. Stabilization of the active form may also be achieved through the design of pre-catalyst and/or pre-treatment methods prior to cell operation. In the following,

instances where electrocatalytic activity and/or selectivity are improved through restructuring are analyzed.

Regulated metal leaching can be used to prepare stable ORR catalysts prior to PEMFC assembly. Potential cycling of PtM alloy catalyst in a selected acidic electrolyte followed by thermal annealing has been shown to produce core–shell structure with a Pt-rich shell (often termed the Pt-skin catalyst) stable against metal leaching under PEMFC relevant conditions.^{53,57,157} For Pt@Pd catalysts, controlled Pd-leaching in the presence of a capping agent allows the rearrangement of Pt atoms in the shell, which is proposed to repair the pinhole defects. The treated Pt@Pd catalyst shows a Pt shell with increased thickness, and in PEMFC tests demonstrates notably improved durability, which is supported by the significantly lowered Pd dissolution rate.¹⁰⁴ Non-precious metal ORR catalysts are promising alternatives to state-of-the-art Pt-based catalysts when operating under neutral or alkaline conditions.^{158,159} Metal leaching is also common in non-precious metal catalysts during ORR, and through rational pre-catalyst design (*i.e.* pairing of a metal cation and a p-block anion), a metastable amorphous layer with enhanced ORR activity can be generated *via in situ* restructuring.^{160,161} The above metal-leaching-induced restructuring of ORR catalysts was mostly studied in rotating disk electrode experiments, and caution should be given that the observed activity enhancement overlooks the possibility of ionomer/membrane poisoning in practical fuel cell test setup.

In HER, catalysts with abundant basal plane active sites have been shown to demonstrate “self-optimizing behaviour”, where stacked catalyst layers become exfoliated and expose more active sites during the course of HER (Fig. 4a–c).¹⁶² Similar to the amorphous surface layer formed through leaching of ORR catalyst component(s) introduced earlier, proper design of HER pre-catalyst leads to a metastable and highly active phase that benefits the electrocatalytic process.^{135,163} For example, vanadium-doped

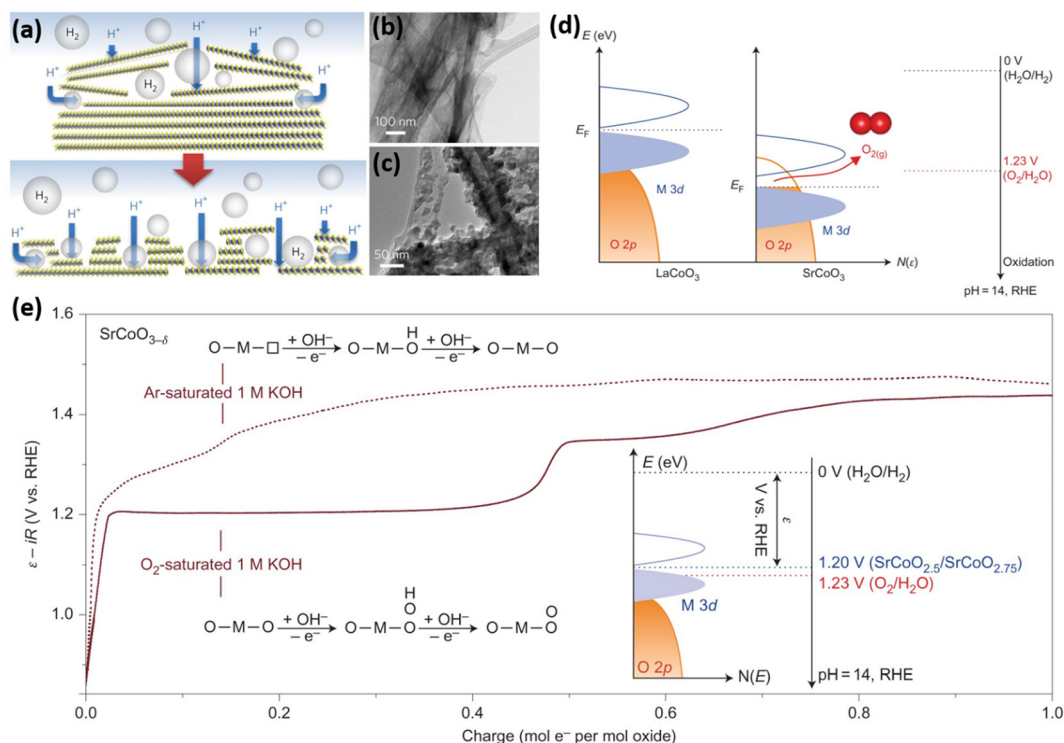


Fig. 4 *In situ* restructuring of electrocatalysts that lead to beneficial catalytic performance. (a) schematic illustration of the “self-optimizing behaviour” of layered TaS₂ catalysts. (b), (c) TEM images of TaS₂ before, and after HER potential cycling. (d) Schematic band diagrams of perovskite oxide LaCoO₃ and SrCoO₃, compared to the redox energy of the O₂/H₂O couple. (e) Galvanostatic charging of SrCoO_{3-δ}, an oxygen-vacancy-rich oxide, in an O₂- and Ar-saturated alkaline electrolyte, demonstrating the effectiveness of the lattice oxygen mechanism in lowering the reaction overpotential. Figures adapted with permission from ref. 162 ((a)–(c)). Copyright 2017. Springer Nature; and ref. 168 ((d) and (e)). Copyright 2017. Springer Nature.

nickel sulfide is restructured to form an amorphous surface layer, which demonstrates superior HER activity relative to the control without V-doping.¹⁶³ Defect engineering through the incorporation of an easily leachable component in the pre-catalyst is another way to facilitate regulated restructuring.¹⁶⁴ In ECO₂R, the stronger binding energy of *CO on defect-rich Cu sites relative to that on low-index Cu crystal facets has been shown to favour the selectivity towards multi-carbon products, through increased surface coverage of *CO and decreased energy barrier for C–C coupling.^{24,165} The use of Cu oxides^{11,18–22,24–26} or chlorides²³ as pre-catalysts facilitates the generation of undercoordinated sites upon *in situ* reduction of Cu under ECO₂R relevant potentials. The rational use of ligand promotes the *in situ* selective faceting of Cu nanocrystals under ECO₂R conditions, and therefore increases the faradaic efficiency towards the targeted product.^{166,167}

In a bottom-up manner, pre-catalysts consisting of atomically dispersed Cu can be directed to form reversibly nanoclusters^{85–88} or irreversibly nanoparticles¹⁶⁹ based on the applied electrode potential and achieve enhanced selectivity towards multi-carbon products. It should be noted that *in situ* generated high-index defects are high-surface-energy sites and that these sites tend to degrade over time *via* modes such as (adsorbate-induced) migration, dissolution, and coalescence.⁴⁴ Pulse electrolysis has been recognised as an effective approach to enhanced selectivity towards multi-carbon products in ECO₂R.^{116,170–172} By periodically bringing the electrode potential to a less negative or even

positive value, undercoordinated sites are regenerated and therefore prolong the service life of the catalyst. It should be noted that the use of pulse electrolysis to generate high-index catalyst surfaces works effectively for metals with low cohesive energy (*e.g.* Cu,^{116,170–173} Ag,¹⁷¹ and Bi¹⁷⁴) because of the high surface atom mobility on these surfaces.^{67,175} The cohesive energy of a metal is the energy required to separate atoms in the crystal into free neutral atoms in vacuum (*i.e.* metal gas),^{175,176} and it serves as an indicator regarding the resistance of the metal against mobility-related structural change (*e.g.* adsorbate-induced adatom formation).^{76,81,177,178} *In situ* generated high-index sites are not thermodynamically favoured, and at a longer time scale, despite the application of periodic potential pulse, the mobile metal atoms tend to migrate towards low-ohmic-resistance sites (*e.g.* contact planes between gas diffusion electrode and current collector)¹⁷⁹ and other low-energy sites to stabilize the system.⁴⁴

The involvement of lattice oxygen in OER on Co-based perovskite has been confirmed *via in situ* ¹⁸O isotope labelling mass spectrometry,¹⁶⁸ and it is expected that increasing the covalency of metal–oxygen bond makes the oxidation of lattice oxygen more thermodynamically favourable.¹⁶⁸ On a theoretical basis, swapping the A site metal of perovskite (ABO₃) to a lower-valent metal (*e.g.* from LaCoO₃ to SrCoO₃) results in a down-shift of Fermi level (Fig. 4d). When the Fermi level crosses the top of the O 2p states and moves below the O₂/H₂O redox energy (1.23 eV), oxidation of lattice oxygen becomes more thermodynamically

favoured than that of water (Fig. 4e).^{168,180} The above explains why OER catalysts with low overpotential are mostly oxides with high valence metals. Such high valence metal sites are intrinsically unstable under ambient conditions, and are therefore often generated *in situ* under applied OER-relevant potential.

The existence of high valence metal sites (*i.e.* Ni^{4+}) during the OER has been confirmed using *in situ* soft XAS,¹⁸¹ and the generation of such sites usually results from dissolution of other constituent metals therefore forming a defect-rich surface layer.^{96,181–187} For example, perovskite hydroxide $\text{CoSn}(\text{OH})_6$ was used as a pre-catalyst, and *in situ* transformed into a highly active OER catalyst *via* electrochemical etching (galvanostatic activation in the reference) of Sn component.¹⁸² As another example, the pre-catalyst of La- and Mn-codoped cobalt spinel was transformed into a surface-defect-rich OER catalyst upon leaching of lanthanum content as La^{3+} .¹⁸³ It is also proposed that the M–O–M motifs (M = Fe, Co, Ni) within the *in situ* formed amorphous layers of metal oxyhydroxide function as the active sites for enhanced OER activity.¹⁸⁸ Under the harsh reaction environment of acidic OER, even iridium suffers from notable dissolution from the pre-catalyst. Through manipulation of the composition of Ir-based perovskite pre-catalysts and dissolution/electrochemical test conditions, it is proposed that the IrO_x amorphous layer formed *in situ* through continuous dissolution/precipitation functions as the true catalyst determining the OER performance.¹⁸⁹

A self-healing electrocatalyst spontaneously regenerates its active sites under the operating conditions (*i.e.* dynamic

equilibrium of multiple reactions).^{190,191} In such a system, therefore, both processes of loss and regeneration of active sites are continuous and dynamic throughout the course of reaction.^{190,191} Distinction should be made between self-healing and self-repairing (Fig. 5a), where in the latter, the regeneration of active sites only occurs when the cell operation is stopped (*e.g.* at open-circuit).^{190,191} Based on the above, the reported on-off electrolysis¹⁹² and the self-assembled metal-organic macrocycle catalyst¹⁹³ in ECO_2R are self-repairing at best. Compared to pulse electrolysis, self-repairing catalysts offer notable merits by removing sophisticated control and continuous power supply. The more desirable self-healing catalysts, however, are yet to be reported for ECO_2R . Self-healing catalysts in OER operate based on parallel dissolution and precipitation of metal oxide clusters (Fig. 5b).¹⁹⁰

Selection of a pre-catalyst metal (*e.g.* Mn, Co, and Ni) cation and solution phase oxyanion (*e.g.* phosphate, methylphosphonate, and borate) pair is crucial to ensure the self-healing feature of the electrocatalytic system. An appropriate cation-oxyanion pair allows dissolved cations to precipitate as oxides/oxyhydroxides, and the size of the latter is regulated *via* metallate capping formed from the reaction between oxyanions and dissolved metal cations.^{190,194} The pre-catalysts of such self-healing OER catalysts usually contain a metal component that upon restructuring serves as a porous conductive support (*e.g.* indium tin oxide,¹⁹⁴ fluorine-doped tin oxide,¹⁹⁵ lead oxide,¹⁹⁶ *etc.*) to ensure facile electronic and ionic conducting pathways. In HER, although not specifically stated as a

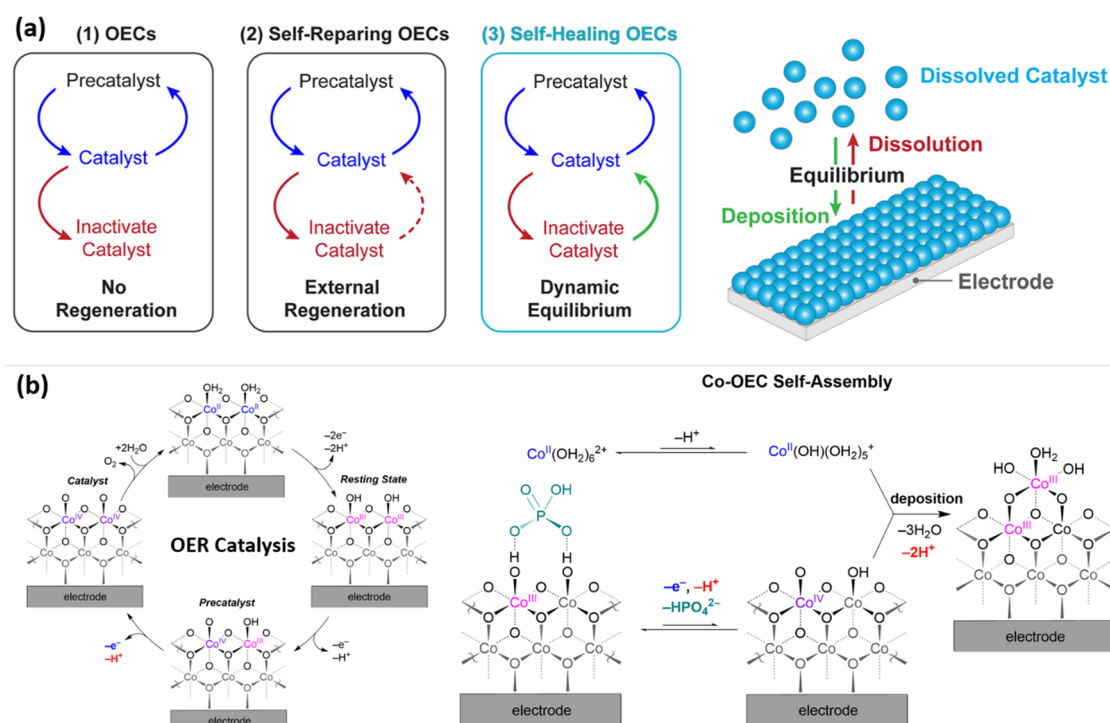


Fig. 5 Comparison between conventional oxygen evolution catalysts (OECs), self-repairing OECs, and self-healing OECs. (a) Summary and schematic illustration of the operating principle of self-healing OECs. (b) Mechanistic schemes of the OER on conventional catalysts (left) versus that on self-healing OECs (Co-OEC assembly, right). Figures adapted with permission from ref. 190. Copyright 2022. Springer Nature.

self-healing system, certain metal alloys also display self-healing properties, where the dissolved molybdenum cations from pre-catalysts polymerize to form polymolybdate which stabilizes the *in situ* generated catalyst with enhanced HER activity.¹⁹⁷ It has been demonstrated that reversible *in situ* restructuring can be achieved, which allows the catalyst to convert between two active forms depending on the operating condition (*i.e.* a bifunctional electrocatalyst).^{198,199} The pre-catalysts of such bifunctional electrocatalysts are usually prepared *via* electrodeposition in pH-buffered oxyanion solution, where the incorporated phosphorus¹⁹⁸ or boron¹⁹⁹ content in the near surface region facilitates the ensuing reversible restructuring. In electrochemical nitrate reduction reaction, amorphous surface layers resulting from *in situ* restructuring are often observed, which deliver improved faradaic efficiencies towards ammonia *via* stabilization of *NOH intermediates^{200,201} and/or suppression of HER,^{202,203} or through improved adsorption to nitrate anions.²⁰⁴

The above two sections have discussed the positive and negative impacts of *in situ* restructuring of catalysts on the outcome of electrochemical process. A tabular comparison summarizing the discussion and examples presented is shown in Table 1.

4. Perspectives and outlook

The fundamental origins and impacts of *in situ* restructuring of catalysts on electrochemical processes have been reviewed. Designs of pre-catalysts and pre-treatment/activation methods have found notable success, but the long-term operational stability of some of these strategies developed in a laboratory scale is questionable when advancing to industrial scales. Design strategies of pre-catalysts (*e.g.* alloying, doping, molecular tuning, size and facet engineering, oxidation state, defect engineering, *etc.*) have been covered in excellent reviews,^{27,28,31,36} and the effectiveness of these approaches rely on controlled/guided restructuring towards the most active and/or selective form of the electrocatalyst. In terms of manipulating restructuring through pre-treatment/activation methods, some of the proposed approaches, such as pulse electrolysis^{179,207} and *in situ* electrochemical dealloying,^{52,55}

still face critical challenges in industrially-relevant setups, due to the impracticality of implementing three-electrode systems and the stability issue related to the leached metals, respectively. We'd like to present four perspectives and outlooks regarding the application of *in situ* restructuring of electrocatalysts in practical industrial settings.

(1) Pulse electrolysis has found success in ECO₂R in regulating active sites to generate targeted products with improved stability and/or selectivity when the restructuring process is reversible under electrochemical conditions. However, it is worth noting that such a technique faces challenges in scaling up towards commercialization. A process that relies on the precise control of the potential of an electrode requires the implementation of a reference electrode (*i.e.* a three-electrode cell). Such a half-cell approach has completely disregarded possible impacts of pulse on the efficiency and stability of counter electrode catalyst, which are equally important in an electrochemical process. Therefore, in large-scale industrial electrochemical processes, the long-term use of reference electrodes throughout the operation is very rare if not non-existent. Instead, constant cell voltage or current is the most practiced mode of operation due to its simplicity and practicality. In the Hall-Héroult electrochemical process for aluminium production for example, constant voltage electrolysis is maintained by adjusting the electrolyte resistance (*i.e.* distance between the anode and cathode).²⁰⁸ In chlor-alkali electrolysis, a constant current is applied and the cell voltage is monitored, which serves as an indicator for reactant (*i.e.* brine solution) flowrate adjustment to keep the operation at the highest energy efficiency.^{209,210}

(2) Approaches to inducing *in situ* restructuring of electrocatalysts towards a more active/selective form and stabilizing them for a prolonged period of time under practical conditions (including transient operation such as start-up and shut-down) are essential to the development of energy-efficient and durable electrochemical processes. Revisiting the concept of promoter discussed at the beginning of this article, the introduction of appropriate species into the electrolyte together with the pre-catalyst to form a catalytic system has shown substantial promise in the OER (*e.g.* phosphate-Co¹⁹⁴), HER

Table 1 Summary of positive and negative impacts of catalyst restructuring on example electrocatalytic reactions

Electrocatalytic reaction	Example catalyst	Restructuring event	Negative impact	Positive impact
ORR	PtM (M = Co, Ni, Cu, Se, <i>etc.</i>)	Metal leaching	Dissolved metal cations poison the ionomer and membrane in fuel cells. ^{98,99} Fenton-like reaction leading to membrane degradation ¹⁰⁰	Under the right conditions, the resulting Pt-rich shell offers higher specific activity ^{53,57,157}
OER	Metal oxides	Metal leaching	Loss of active sites. Corrosion and amorphous layer formation compromise the mechanical integrity of the electrode ^{29,30,32}	Under the right combination of electrolyte and (mixed) metal oxide catalyst, self-healing can be achieved with high activity and stability ^{190,194,196}
ECO ₂ R	Cu-based particles	Formation of an amorphous surface layer	At long time scales, undercoordinated sites are consumed through Ostwald ripening and other processes, eventually leading to decreased activity and selectivity ^{43,66,117}	At short time scales, the generated under-coordinated sites improve the selectivity towards multi-carbon products ^{20,205}
HER	Transition metal chalcogenides	Formation of the restructured surface layer	Prolonged operation favors the formation of highly crystalline MoS ₂ domains, or inactive oxides/oxyhydroxides on the surface, which deactivates the catalyst ²⁰⁶	<i>In situ</i> formation of an amorphous layer exposes highly active sites ^{162,206}

Highlight

(polymolybdate-Ni¹⁹⁷), ECO₂R (imidazolium-based-ionic-liquid-Ag,²¹¹ functionalized-iron-porphine-Cu²¹²), and e-NRR (LiClO₄-Cu²¹³). The fact that even the state-of-the-art Haber-Bosch process relies on the addition of a promoter suggests that this approach towards regulated restructuring deserves more research attention in electrocatalysis.

(3) The concept of self-healing catalysts, where highly active/selective sites are generated, consumed upon reaction, and renewed constantly, provides prospects for an energy-efficient and durable process. Considering that efficient and stable OER has been achieved under harsh conditions (*e.g.* 80 °C and pH = 1) through a self-healing catalyst,¹⁹⁶ the next step towards commercialization should be the improvement in impurity tolerance of the catalyst system, and insights can be obtained from seawater electrolysis.^{214,215} How self-healing can be realized for reactions other than OER and HER, which will require appropriate selection and pairing of solution phase species and catalyst metal components, is still an area rarely explored.

(4) In order to develop more reliable control of *in situ* restructuring of electrocatalysts to our advantage, advances in characterization techniques on electrochemical interfaces and a rigorous understanding of electrokinetics and other potential activity/selectivity descriptors beyond adsorption energy²¹⁶ should propel the field greatly. Advances in the above areas will allow us greater access to the *in situ* restructuring of more complex electrocatalytic reactions, such as electrosynthesis of ammonia through co-reduction of dinitrogen^{217–219} or nitrate^{220,221} with CO₂. The formation of the C–N bond requires the atomic-scale proximity of intrinsically different sites (*i.e.* strong *N₂ or *NOH binding *vs.* strong *CO₂ binding), which poses challenges in catalyst synthesis. The greatly increased number of possible intermediates and side reactions further complicates the *in situ* restructuring scenario. Considering the fact that the catalyst restructuring in the e-NRR is still masked by the dominant competing HER, a breakthrough in characterization techniques is required to elucidate the structural evolution attributed to the electrochemical C–N coupling from CO₂ and N₂.

In summary, the dynamic nature of electrocatalyst surface has introduced both challenges and opportunities to the industrial applications of electrochemical processes. *In situ* restructuring impacts negatively the electrocatalytic outcome when the evolved stable form of the catalyst during operation is of low activity and/or selectivity, or when other device components become poisoned or failed in the course of restructuring. Positive impacts may also be observed on restructured electrocatalysts if the stable form delivers improved activity and/or selectivity than the pre-catalysts. The authors hope that this review article will inspire researchers to advance electrochemical technologies and to ensure access to affordable, reliable and sustainable energy for all.

Data availability

No primary research results, software or code have been included and no new data were generated or analysed as part of this review.

Conflicts of interest

There are no conflicts to declare.

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