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Multi-functional perovskite oxide $\text{Pr}_{0.6}\text{Sr}_{0.4}\text{Mn}_{0.2}\text{Fe}_{0.7}\text{Ni}_{0.1}\text{O}_{3-\delta}$ as an efficient quasi-symmetric electrode for solid oxide fuel/electrolysis cells†

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Solid oxide cells (SOCs) have recently gained attention as an efficient energy conversion system for a smart-grid that can resolve the intermittency of renewable energy. In particular, a symmetric configuration of the electrode has been developed to minimize fabrication cost and relieve compatibility issues. In this work, PSMFN ($\text{Pr}_{0.6}\text{Sr}_{0.4}\text{Mn}_{0.2}\text{Fe}_{0.7}\text{Ni}_{0.1}\text{O}_{3-\delta}$) was developed and evaluated as a quasi-symmetric electrode for a solid oxide cell (Q-SSOC). A solid oxide cell fashioned with PSMFN–GDC ($\text{Ce}_{0.9}\text{Gd}_{0.1}\text{O}_2$) exhibited an electrochemical performance of 0.702 W cm^{-2} for H_2 -SOFC and 1.02 A cm^{-2} at a voltage of 1.5 V for CO_2 -SOEC at 800 °C. The physiochemical and electrochemical properties of PSMFN were investigated to elaborate this notable electrochemical performance of PSMFN–GDC. X-ray diffraction (XRD), microscopic analyses, and X-ray absorption near edge structure (XANES) indicated the occurrence of an exsolution of Fe–Ni alloy nanoparticles (NPs) along with a phase transition from the perovskite to the Ruddlesden–Popper structure. In addition, X-ray photoelectron spectroscopy (XPS) was utilized to elucidate the change in surface oxygen vacancies of the reduced PSMFN form. Furthermore, electrical conductivities and area specific resistances under an air atmosphere were measured to investigate the activities of PSMFN towards oxygen electrode reactions. From these analyses, PSMFN can provide numerous active sites both for electrode reactions with oxygen as well as fuel, which make it a promising quasi-symmetric electrode for an SOC.

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Introduction

Solid oxide cells (SOCs), which can be operated under both modes of a galvanic cell (*e.g.*, solid oxide fuel cells, SOFCs) and an electrolytic cell (*e.g.*, solid oxide electrolysis cells, SOECs), can play a key technological role in resolving the intermittency issue of renewable energies and relieving global warming by the greenhouse gas effect.^{1–6} Moreover, various types of fuel, even carbon-containing gas, can be converted into electricity with lower emission of greenhouse gas,^{7–9} while superfluous energy produced during the night-time from renewable energy sources can be stored in forms of chemical energy; for instance,

converting carbon dioxide (CO_2) into carbon monoxide (CO).^{10,11} The high-temperature operation, where heat demand is largely diminished, gives a high theoretical thermodynamic efficiency and fast electrode kinetics compared to other electrochemical systems.

In an SOC configuration, materials for the fuel electrode and air electrode, which are separated by a gastight solid electrolyte, should have sufficient electrical conductivity over a wide range of $p\text{O}_2$ and catalytic activity towards several reactions, including the hydrogen oxidation reaction (HOR), CO_2 reduction reaction (CO_2RR) for a fuel electrode and the oxygen reduction reaction (ORR), and the oxygen evolution reaction (OER) for an air electrode. Nowadays, symmetric SOCs (SSOCs), which adopt an identical electrode material for anode and cathode, have been developed with advantages over conventional SOCs, such as simplified preparation procedure, low cost in fabrication, and well-matched thermo-chemical compatibility.^{12,13} Irvine's group has suggested the concept of a symmetric configuration in an SOFC, and demonstrated the versatility of a redox-stable $(\text{La}_{0.75}\text{Sr}_{0.25})\text{Cr}_{0.5}\text{Mn}_{0.5}\text{O}_{3-\delta}$ electrode for the operation of a hydrogen/hydrocarbon fuel cell (FC) and a water electrolysis cell (EC).¹⁴ Indeed, the electrode material of an SSOC should be

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electrochemically active under both a reducing and an oxidizing gas atmosphere. Recently, a quasi-symmetric configuration has been studied for solid oxide cells (Q-SSOCs), where two similar electrode materials are optimally combined to further enhance the electrochemical performance of SSOCs.^{15,16} This configuration can also be obtained *via* a follow-up process after electrode fabrication, such as annealing in a reducing atmosphere.^{17,18}

A perovskite oxide (ABO_3) can be employed as the effective electrode material for an SOC since it has mixed ionic and electronic conducting (MIEC) and redox-stable properties depending on its versatile combinations of A/B cations. For most perovskite oxides, the component of the B-site cations is closely correlated with the electronic and catalytic properties of the parent oxides. For example, Fe-based perovskite oxide, where the redox pair of $\text{Fe}^{3+}/\text{Fe}^{4+}$ plays a critical role in its electrocatalytic activity, has been studied as an electrode material for SOCs.^{19–21} However, use of this perovskite oxide could lead to inferior electrochemical performance compared with a conventional Ni-based electrode. Recently, the exsolution method has been applied to enhance the electrochemical performance of perovskite oxide materials because evenly distributed metal or alloy nanoparticles (NPs) could be formed *in situ* on the surface during the reduction process with easy control over the size of the NPs.^{22–24} Nevertheless, the exsolution method has a limitation on the amounts of NPs, since excessive amounts of exsolved NPs on the surface leave a large amount of B-site vacancies inside the lattice, leading to stability issues for the crystal structure. To overcome this limitation, tuning the A-site deficiency of the host oxide has been demonstrated as an effective way to increase the amount of exsolved NPs and to facilitate the exsolution of less reducible cations.²⁵ On the other hand, several perovskite oxides have been reported to be transformed into a layered perovskite oxide such as a Ruddlesden–Popper (RP) oxide and this transition can induce a large number of NPs to be exsolved according to its stoichiometry.^{26–28} A phase transformation concurrent with the exsolution process can occur due to different vacancy formation behaviors on the AO layer and the BO_2 layer. H. Kim *et al.* demonstrated a DFT calculation to estimate the $G_{\text{Vf-O}}$ (Gibbs free energy of oxygen vacancy formation) on the AO and BO_2 layers of $\text{Pr}_{0.5}\text{Sr}_{0.5}\text{TO}_{3-\delta}$ (T: Mn, Fe, Co, Ni) and revealed that positive oxygen vacancy formation on the AO layer and negative formation on the BO_2 layer can lead to a complete phase transformation from single perovskite oxide to Ruddlesden–Popper oxide, where Mn and Fe are used as B-site components.²⁹

Herein, we designed a novel perovskite oxide, $\text{Pr}_{0.6}\text{Sr}_{0.4}\text{Mn}_{0.2}\text{Fe}_{0.7}\text{Ni}_{0.1}\text{O}_{3-\delta}$ (PSMFN), as an efficient electrode material for a quasi-symmetric SOC and evaluated it as an efficient electrode material for HOR, CO_2RR , ORR, and OER in an SOC. Especially under fuel conditions, *in situ* reconstructed PSMFN, which is composed of a Ruddlesden–Popper oxide (R.P. PSMFN) with Ni–Fe alloy NPs decorated on the surface has been applied to the fuel electrode of a Q-SSOC. Exsolved metal NPs have shown high catalytic activity towards both HOR in SOFC mode and CO_2RR in SOEC mode.^{29,30,31} In addition, Ni doping on ferrite oxide can induce the formation of an Ni–Fe alloy, which can drastically enhance the electrochemical performance of the oxide. Furthermore, several studies have demonstrated that ferrite-based

perovskite oxides have shown catalytic activity against OER/ORR as good as that of cobalt-based perovskite oxide.^{32–34} X-ray diffraction (XRD) and microscopic analyses were conducted to investigate the occurrence of exsolution. Electrochemical analyses, such as X-ray absorption fine structure (XAFS), X-ray photoelectron spectroscopy (XPS), and electrochemical impedance spectroscopy (EIS) were performed to elucidate the electrochemical performance of PSMFN for Q-SSOC.

Experimental section

Catalyst preparation

PSMFN was synthesized by a modified sol–gel method, as described below: stoichiometric amounts of metal nitrate precursors, $\text{Pr}(\text{NO}_3)_3 \cdot 6\text{H}_2\text{O}$ (Sigma-Aldrich, 99.9%), $\text{Sr}(\text{NO}_3)_2$ (Sigma-Aldrich, 99.0%), $\text{Mn}(\text{NO}_3)_2 \cdot 4\text{H}_2\text{O}$ (Alfa Aesar, 98%), $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$ (Sigma-Aldrich, 98%), $\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ (Samchun, 98%), were prepared and dissolved in DI water. Chelating agents, citric acid (Daejung, anhydrous) and ethylenediaminetetraacetic acid (Sigma-Aldrich), were also dissolved in the above solution, followed by adjusting the pH of the solution to 8. After that, the precursor solution was heated on a hot plate at 90 °C with vigorous stirring until the solution became a brown gel. The gelled solution was then pre-heated at 200 °C for 1 h and pulverized to get a fully dehydrated and fine powder. The final product was obtained by calcination at 1000 °C for 5 h.

Cell fabrication

An electrolyte-supported symmetric solid oxide cell was prepared for an electrochemical performance test. A button-shaped LSGM ($\text{La}_{0.8}\text{Sr}_{0.2}\text{Ga}_{0.8}\text{Mg}_{0.2}\text{O}_{3-\delta}$, fuel cell material) electrolyte pellet was fabricated by a dry-pressing method. The pressed pellet was sintered twice in an air atmosphere at 1200 °C for 3 h and 1450 °C for 15 h. The sintered electrolyte pellet has a diameter of 17 mm with a thickness of 230 μm without any secondary phase observed in the XRD pattern (Fig. S1†). The as-prepared PSMFN was ball milled by a planetary mixer with an ion conducting material, GDC ($\text{Ce}_{0.9}\text{Gd}_{0.1}\text{O}_2$, UHSA Anan Kasei), in a weight ratio of 6 : 4 at 400 rpm for 1 h. The obtained powder was mixed with an organic binder (6% ethyl cellulose in α -terpineol solution) in a weight ratio of 1 : 1.1 and pasted on both sides of the electrolyte pellet by a screen-printing method, followed by calcination at 1000 °C for 1 h. The fabricated porous electrode has an area of 0.283 cm^2 with a thickness of 20 nm, and is strongly attached onto the surface of the electrolyte (Fig. S2†). A bar-shaped pellet with dimensions of $3.5 \times 1.6 \times 19$ mm was dry-pressed and sintered at 1350 °C for 10 h for the measurement of electrical conductivity.

Physicochemical characterization

X-ray diffraction (XRD) analysis was conducted to investigate the crystal structure of the prepared PSMFN, reduced PSMFN and PSMFN–GDC composite using a Rigaku Ultima IV with 40 kV, 30 mA conditions within the 2θ range of 20–80°. Field-emission scanning electron microscopy (FE-SEM, S-4800, HITACHI) and mini-SEM (SNE-4000M, SEC) were employed to



examine the surface morphology of the electrode catalyst and cross-sectional image of the fabricated solid oxide cell. Transmission electron microscopy (TEM, JEM-2200FS, JEOL) and electron energy loss spectroscopy (EELS) were also utilized to investigate the microstructure and elemental distribution of the exsolved metal NPs at 200 kV. X-ray absorption fine structure (XAFS) was conducted to inspect the electronic structure and estimated oxidation states of the transition metal cations on the 7D beamline of Pohang Accelerator Laboratory (PLS-II). X-ray absorption near edge structure (XANES) was analyzed using Athena software. X-ray photoelectron spectroscopy (XPS) was adopted to examine the surface oxygen species of the electrode catalysts using high-performance XPS (K-Alpha XPS system, Thermo Scientific). H₂-temperature programmed reduction (H₂-TPR) was carried out to investigate the reduction behavior of the prepared electrode catalyst. 40 mg of PSMFN was analyzed by a flow-type reactor (AutoChem II Chemisorption Analyzer, Micromeritics) under a 4% H₂/Ar atmosphere at a flow rate of 50 mL min⁻¹ in a temperature range from 100 °C to 800 °C.

Electrochemical measurements

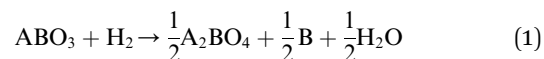
The electrical conductivities of PSMFN were measured using a four-probe method under air, 20% H₂/N₂, and 30% CO/CO₂ at a total flow rate of 30 mL min⁻¹ in the temperature range from 550 to 800 °C. Pt wire and Ag paste were used to connect the four probes. The electrochemical performance of a PSMFN–GDC symmetric cell was evaluated under both FC and EC operation. 100% H₂ and air were fed into each fuel and oxygen electrode side, respectively, and 30% CO/CO₂ was flowed into the fuel side, while the oxygen electrode was exposed to ambient air conditions. The total flow rate of the feed gas was 50 mL min⁻¹. The electrolyte-supported button cell was mounted on an alumina tube using ceramic adhesive (552-VFG, AREMCO) as a sealant and Ag paste and wire was used as a current collector. Before the cell test, the fuel electrode had been previously annealed in a 100% H₂ atmosphere for 0.5 h to induce the exsolution process of PSMFN. Electrochemical impedance spectroscopy (EIS, MP2, ZiveLab) was utilized to measure the ohmic and polarization resistance of the symmetric cell under OCV and applied voltage conditions with a voltage amplitude of 28.3 mV in the frequency range of 100 MHz to 10 mHz. Further distribution of relaxation times (DRT) analysis was performed with the MATLAB DRTtools developed by Ciucci *et al.*³⁵ A half-cell test of the symmetric cell was conducted to estimate the HOR and ORR activities of the PSMFN–GDC electrode in air and a 100% H₂ atmosphere. Both sides of the electrodes were exposed to the same gas atmosphere and EIS profiles were obtained under OCV conditions. Product analysis of CO₂ electrolysis was carried out to calculate the CO production rate and the Faraday efficiency was determined by gas chromatography (Agilent, 7890B).

Results and discussion

Structural and microscopic analyses

Fig. 1(a) depicts the reduction process of PSMFN, which has been developed and utilized as a quasi-symmetric electrode in

this study. A single perovskite oxide, PSMFN, which can be denoted by the SrFeO_{2.97} (PDF #40-0905) phase in XRD analysis (Fig. 1(b)), is transformed into the R.P. phase of SrPrFeO₄ (PDF #32-1237), which will now be denoted as R.P. PSMFN, during an annealing process under a 20% H₂/N₂ atmosphere at 800 °C for 10 h. Simultaneously, newly formed signals at 2θ values of 43.6°, 57.8°, and 74.7° are detected in the XRD patterns and identified as an alloy phase of Fe_{0.64}Ni_{0.36} (PDF #47-1405). The above reduction behavior can be expressed with the equation:



According to the above equation, a large amount of B-site metal cations can be exsolved to a separate metal phase due to the difference in stoichiometry between the two phases along with the phase transition. The stray peaks, mainly located at around 32° and marked by blue circles in Fig. 1b, could be assigned to the Pr_{0.96}Mn_{0.982}O₃ (PDF #85-2203) phase, which is known to be decomposed into Pr₂O₃ and MnO under a reduction atmosphere. On the other hand, an ionic conducting material, GDC, was mixed with PSMFN to enlarge the triple phase boundaries (TPBs) for the electrode reaction. Fig. 1(c) suggests that PSMFN and GDC represented good material compatibility under electrode sintering conditions, which were calcination at 1000 °C for 1 h in ambient air, by revealing no additional phase formation between those two materials after sintering.

Microscopic analyses of reduced PSMFN were conducted to further verify the formation of an alloy phase. The TEM image and corresponding EELS mapping of reduced PSMFN (Fig. 1(d) and (e)) show that the newly formed Fe–Ni alloy NPs are present with spherical shape with a diameter of ~30 nm, and are evenly distributed and deeply socketed onto the surface of the oxide. Meanwhile, polycrystallinity of the support oxide was observed, which might be due to the widespread phase reconstruction during the *in situ* exsolution process, as shown in the HR-TEM image (Fig. S3†). Small peaks from Pr₂O₃ were found in the XRD analysis of reduced PSMFN and the Pr₂O₃ seemed to be delocalized in the vicinity of Fe–Ni alloy particles, as can be seen in the Pr mapping in Fig. 1f. Similar behavior for the segregation of A-site cations during the exsolution process has been reported; for example, BaO islands appeared near the exsolved Ni nanoparticles on a BCZYb support oxide.³⁶ In this work, Pr₂O₃ segregation might take place due to the intrinsic high-valence state of praseodymium (Pr³⁺/Pr⁴⁺). From the XRD and microscopic analyses, it was clearly observed that the as-prepared PSMFN undergoes a phase transition from single perovskite oxide to R.P. oxide with newly exsolved Fe–Ni alloy nanoparticles on the surface of the oxide.

XANES analysis

In a perovskite-type oxide, the oxidation state of the B-site cation plays an important role in charge transfer and catalytic activity against an electrochemical reaction, where Bⁿ⁺–O–B⁽ⁿ⁻¹⁾⁺ is usually known as the charge transfer pathway.³⁷ The relatively low catalytic activity of perovskite oxides can be



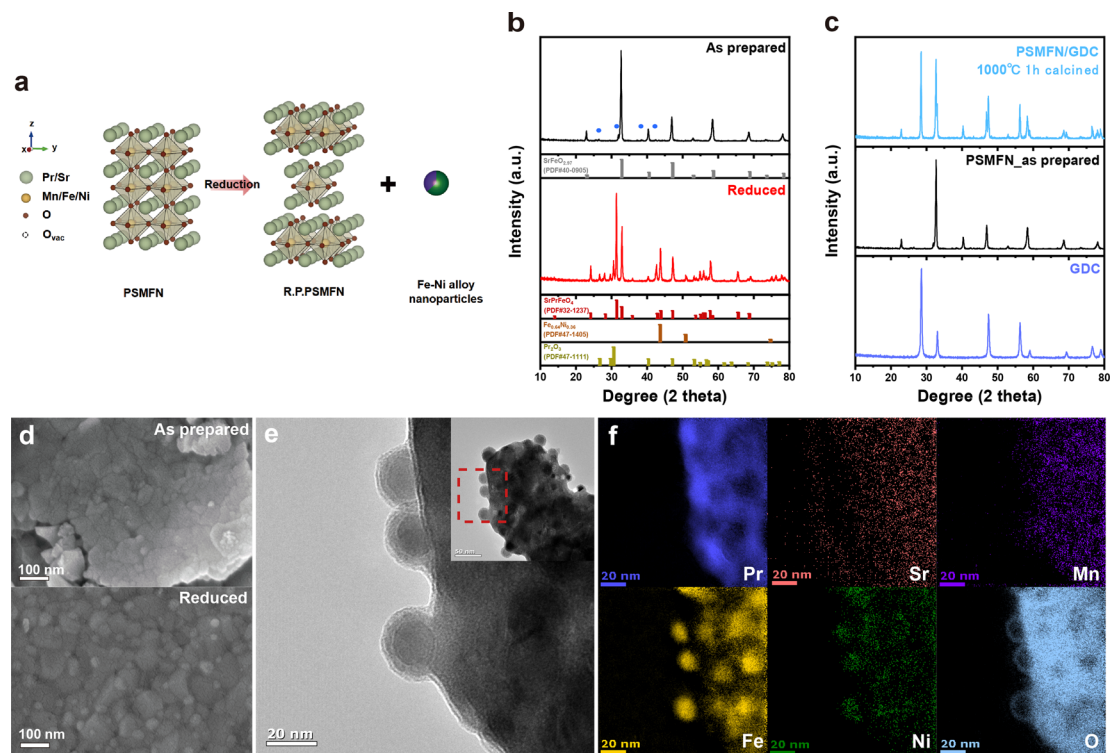


Fig. 1 Structural and microscopic analyses of PSMFN. (a) Schematic diagram of the exsolution process with concurrent phase transformation from perovskite to Ruddlesden–Popper oxide. (b) XRD patterns of the as-prepared and reduced PSMFN with corresponding PDF standard patterns and of (c) the PSMFN–GDC mixture annealed at 1000 °C for 1 h. (d) SEM images of as-prepared and reduced PSMFN. (e) Magnified TEM image of reduced PSMFN (red box with dashed line) and (f) corresponding EELS mappings at the Pr L-edge, Sr L-edge, Mn K-edge, Fe K-edge, Ni K-edge and O K-edge, respectively.

ascribed to the AO termination of the perovskite oxide surface, due to its larger ionic radius compared to the B-site cation.^{38,39}

In this context, exsolution can be another strategy to expose the B-site cations to the surface, further reducing these cations to the metal or alloy NPs. Therefore, the oxidation states of B-site cations should be investigated to assess the electrochemical properties of their prepared catalysts. For a 3d or 4d transition metal, the absorption edge shape and position in XANES spectra are highly dependent on the electronic structure of the species, where electron excitation from the s orbital to the p orbital occurs by X-ray absorption.⁴⁰ In other words, the main absorption edge position of the transition metal is highly sensitive to the oxidation states of the metal species. To estimate the change in oxidation states of the B-site cations, X-ray absorption near edge spectra (XANES) of PSMFN and reduced PSMFN at the Fe K-edge and Ni K-edge were obtained and analysed (Fig. 2(a) and (c)). Based on the obtained 1st-derivative curves of the normalized XANES spectra (Fig. S4†), the energies of the edge positions and oxidation states of the reference oxide are interpolated to estimate the oxidation states of Fe and Ni species for the as-prepared and reduced PSMFN. In the as-prepared PSMFN, the average oxidation state of Fe cations is calculated to be 3.75+, which represents mixed states of Fe³⁺ and Fe⁴⁺ in the perovskite lattice (Fig. 2(b)). After reduction in an H₂ atmosphere, two edge positions of the XANES spectra at the Fe K-edge were simultaneously observed at 7112 and

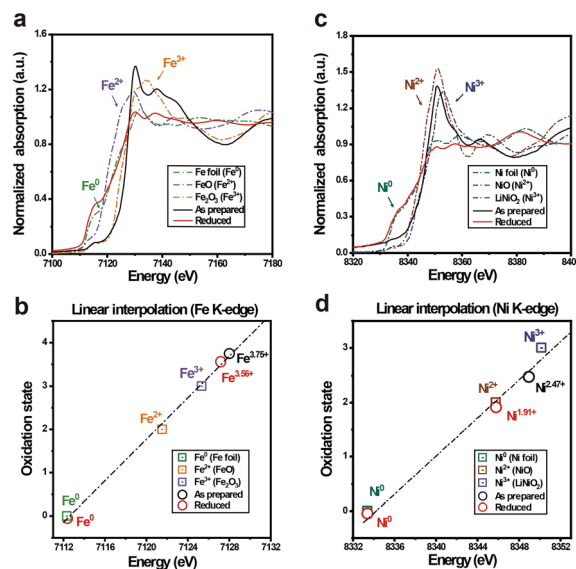
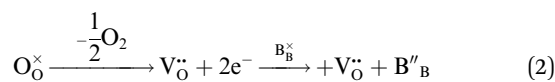


Fig. 2 Edge energy analyses for the oxidation states of transition metal ions in PSMFN. Normalized X-ray absorption near edge spectra of PSMFN, reduced PSMFN and reference oxide at (a) the Fe K-edge, (c) the Ni K-edge. Corresponding linear interpolations of edge positions for PSMFN, reduced PSMFN and reference oxides at (b) the Fe K-edge, (d) the Ni K-edge.



7127 eV, which can be assigned to the edge energy of the Fe⁰ phase and Fe^{3.56+} in the lattice, respectively. These results imply that the exsolution of Fe species took place successfully in agreement with the microstructural analyses, and the Fe species are also present in a mixed state of Fe³⁺/Fe⁴⁺ in the R.P. phase. Similar behavior is also observed for Ni species; the oxidation state of Ni species in the as-prepared PSMFN, 2.47+, is reduced with an emerging state of Ni⁰ in the reduced PSMFN sample. Notably, Ni species seems to remain in the lattice structure of R.P. PSMFN with an observed oxidation state of 1.91+ in its XANES spectra. In a low oxygen partial pressure (*p*O₂), all the oxygen atoms of the perovskite oxide can be released and neutral oxygen vacancies, which are composed of positively charged oxygen vacancies and two electrons, can be produced. This neutral oxygen vacancy reduces the neighboring cation, especially a transition metal cation in the B site of perovskite oxide, as expressed by eqn (2) below using Kröger-Vink notation:^{41,42}



For the material characteristics of PSMFN, oxygen vacancy concentration increases up to a critical point, where the perovskite structure cannot tolerate the large amounts of defects, and phase reconstruction and exsolution of Fe and Ni cations occur simultaneously. As a consequence, metallic Fe⁰ and Ni⁰ phases were observed with a reduced lattice oxidation state of B-site cations in the R.P. PSMFN.

Redox behavior and electrical properties

The redox behavior of PSMFN was further investigated with the H₂-TPR profiles obtained in a 4% H₂/Ar atmosphere. As featured in Fig. 3(a), the TPR profile of PSMFN has three significant peaks, one is located at *ca.* 250 °C, another is at *ca.* 350 °C and the third is at *ca.* 700 °C. As mentioned in the above section, a reducing atmosphere under the condition of a low oxygen partial pressure can create oxygen vacancies with the reduction of neighboring transition metal cations in B sites. The first

reduction peak near 250 °C can be attributed to the reduction processes of Mn⁴⁺ and Fe⁴⁺ to Mn³⁺ and Fe³⁺, whereas the other peak positioned at about 350 °C could be assigned to the reduction processes of Mn³⁺, Fe³⁺, and Ni³⁺ to Mn²⁺, Fe²⁺, and Ni²⁺.^{43–45} When the temperature is raised to over 600 °C, further reduction causes the formation of a large amount of oxygen vacancies, which can destabilize the perovskite lattice and thus induce exsolution of the Fe–Ni alloy with a concurrent phase transition to a Ruddlesden–Popper structure, resulting in a large H₂O peak in the TPR profile.

Even if phase reconstruction occurred to rebalance the unstable perovskite structure with high oxygen vacancy concentration, large amounts of oxygen vacancies can still remain on the lattice after the exsolution process is complete. Fig. 3(b) represents the electronic structure of O 1s in the XPS spectra of the as-prepared and reduced PSMFN samples. The O 1s spectrum of a typical perovskite oxide usually shows three characteristic peaks; one located near a binding energy of 529 eV is related to lattice oxygen species, another positioned at ~531 eV is attributed to surface-adsorbed species such as –OH groups and O₂, and the other one at the highest binding energy is correlated with adsorbed H₂O species.^{46,47} For lattice oxygen species, a slight increase in binding energy in the reduced PSMFN could be associated with varied electronic structures within the lattice oxygen (O₂[–]). More importantly, the ratio of surface-adsorbed species to lattice oxygen greatly increased in the reduced sample and the amount of surface-adsorbed species is directly connected with the adsorption sites of oxygen-containing gas molecules, thus indicating oxygen vacancies on the surface of the oxides. Therefore, the XPS spectra of O 1s exhibited an increased number of oxygen vacancy species over the reduced PSMFN even after the phase reconstruction had occurred. This large number of created oxygen vacancies could also contribute to the superior fuel electrode kinetics in both operations of the SOC.

The electrical conductivities of PSMFN were also measured by the 4-probe method under the operating conditions of a quasi-symmetric electrode in an SOC in the temperature range from 550 °C to 800 °C with air, H₂, and CO₂ atmospheres, respectively (Fig. 3(c)). In the air atmosphere, the electrical

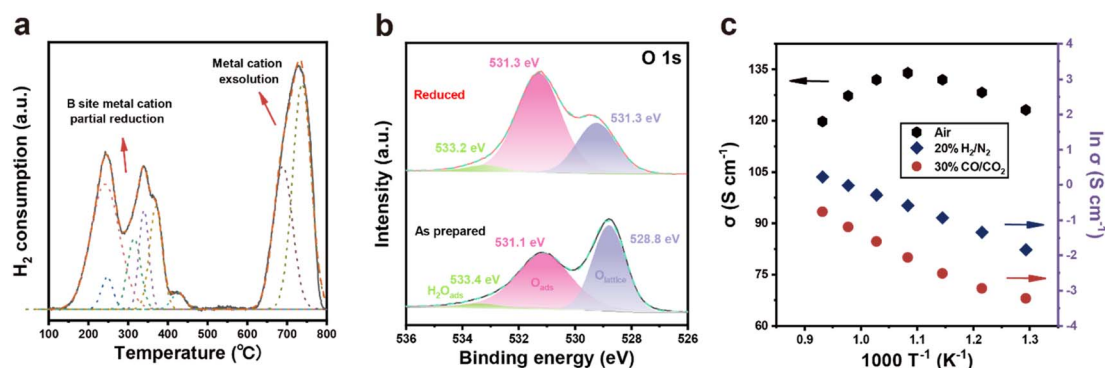


Fig. 3 Redox behavior and electrical properties of PSMFN. (a) H₂-TPR profile of PSMFN under 4% H₂/Ar atmosphere at temperatures from 100 °C to 800 °C with a ramping rate of 5 °C min^{–1}. (b) O 1s XPS spectra of PSMFN and reduced PSMFN. (c) Electrical properties of PSMFN under air (left axis), 20% H₂/N₂, and 30% CO/CO₂ atmosphere (right axis) in a temperature range from 550 °C to 800 °C.



conductivity of PSMFN increased with temperature until it reached a maximum value at 650 °C, then decreased at temperatures higher than 800 °C, indicating that the electrical conducting behavior of the PSMFN has transformed from semi-conducting to metallic behavior. Such a transition of conduction behavior is typically observed for a perovskite-related mixed conductor governed by a small polaron hopping mechanism.^{48,49} Ferrite perovskite oxide, represented by LaFeO_3 , shows p-type conduction behavior where small polaron hopping is thermally activated below ~ 600 °C via the $\text{Fe}^{3+}\text{-O-Fe}^{4+}$ bond pathway. As the temperature rises further, however, a substantially increased number of oxygen vacancies disturbs the three-dimensional Fe–O–Fe network, resulting in decreased electrical conductivity.^{30,50} In other words, the creation of electrons induced by oxygen vacancy formation (eqn (2)), diminishes the main charge carriers, *i.e.*, holes, of ferrite oxide by a recombination process and reduces the redox pairs by facilitating the conversion of Fe^{4+} to Fe^{3+} . As shown in Fig. 3(c), the electrical conductivity of PSMFN is 120 S cm^{-1} at 800 °C, which is still a little bit larger than the threshold for application to an air electrode of an SOFC (100 S cm^{-1}).⁵¹ Before measuring the electrical conductivity of PSMFN under 20% H_2/N_2 and 30% CO/CO_2 atmospheres, an annealing process under 20% H_2/N_2 for 0.5 h was carried out in order to induce exsolution and phase transition. Under both atmospheric conditions, the electrical

conductivities are significantly lower than that under the air atmosphere. These lower conductivities are also associated with p-type conduction; a low oxygen partial pressure leads to a substantial loss of lattice oxygen species through liberation, decreasing the charge carriers and electrical conductivities of PSMFN. Specifically, under the H_2/N_2 atmosphere, the reduced PSMFN has a conductivity value of 1.66 S cm^{-1} , which is comparable with those of reported symmetrical electrode catalysts, such as $(\text{La}_{0.75}\text{Sr}_{0.25})_{0.9}\text{Cr}_{0.5}\text{Mn}_{0.45}\text{Ru}_{0.05}\text{O}_{3-\delta}$ (1.6 S cm^{-1} at 800 °C),⁵⁰ and $\text{La}_{0.5}\text{Sr}_{0.5}\text{Fe}_{0.9}\text{Mo}_{0.1}\text{O}_{3-\delta}$ (1.1 S cm^{-1} at 850 °C).⁵²

Performance evaluation on SOFC mode

Due to its high electrical conductivity under an air atmosphere and large amounts of TPBs attained by *in situ* exsolution of Fe–Ni alloy NPs with phase reconstruction, it is demonstrated that PSMFN can be simultaneously employed as both fuel and air electrodes. Therefore, an LSGM-based PSMFN–GDC quasi-symmetric cell was evaluated under fuel cell operating conditions, as shown in Fig. 4. Symmetric half-cell tests under air and H_2 atmospheres were conducted to measure the ORR/OER and HOR activities of PSMFN–GDC. For HOR activity, both sides of the symmetric cell were treated under 100% H_2 for 0.5 h to induce the exsolution and phase transition of PSMFN–GDC. Fig. 4(a) shows the temperature dependency of area specific

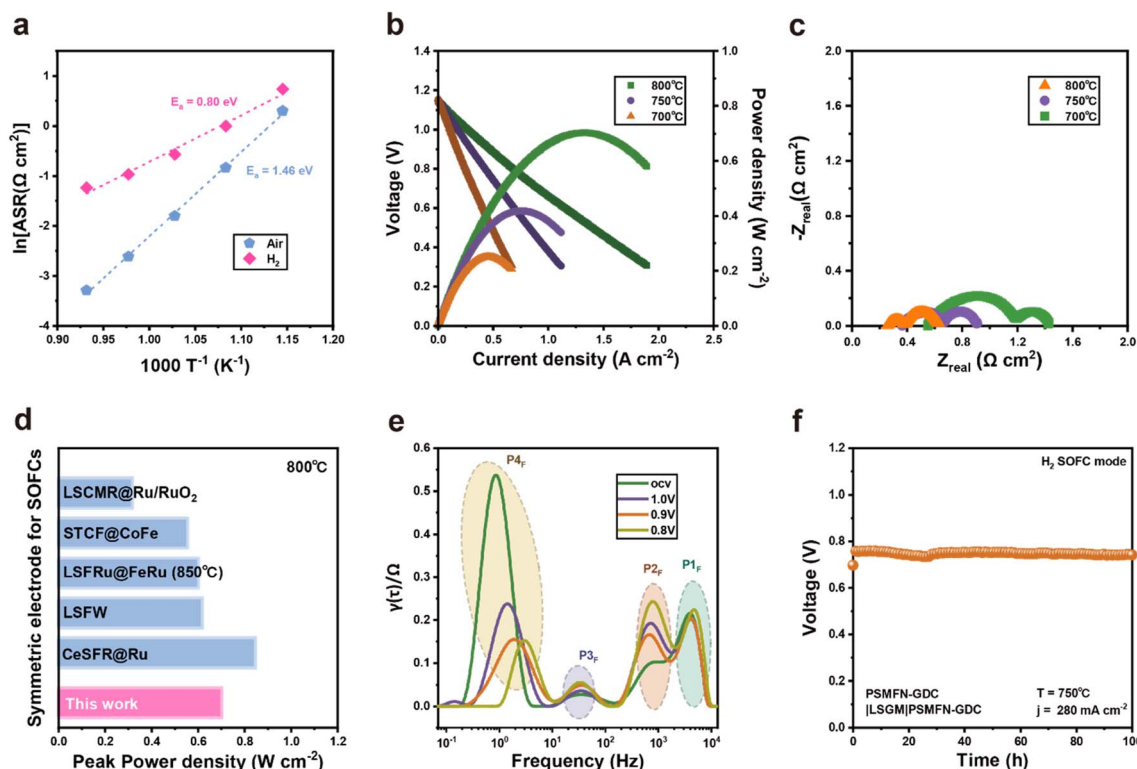


Fig. 4 Electrochemical performances of PSMFN in quasi-symmetric SOFC mode with a configuration of PSMFN–GDC|LSGM|PSMFN–GDC. (a) Arrhenius plots for the area specific resistances of a PSMFN–GDC electrode in 100% H_2 and air atmospheres. (b) I – V – P plots of a PSMFN–GDC quasi-symmetric cell under 100% H_2 fuel conditions and corresponding (c) Nyquist plots under OCV conditions at temperatures of 800 °C, 750 °C, and 700 °C. (d) Peak power density comparison with other symmetric SOFC electrodes in 100% H_2 . (e) DRT plots of the PSMFN–GDC cell at OCV and applied voltage conditions for SOFC operation at 800 °C. (f) Long-term test of the PSMFN–GDC cell under constant current operation of 280 mA cm^{-2} at 750 °C.



resistance (ASR) and the calculated activation energy of the PSMFN-GDC electrode. In the Arrhenius plot, the ASR of PSMFN-GDC shows nearly linear correlation with temperature, which indicates thermally activated electrode kinetics in fuel cell conditions. In particular, the ASR value of PSMFN-GDC at 800 °C is $0.0371 \Omega \text{ cm}^2$, which is significantly lower than that of $\text{Sr}_2\text{Fe}_{1.5}\text{Mo}_{0.5}\text{O}_{6-\delta}$ ($0.24 \Omega \text{ cm}^2$)⁵³ and comparable with a typical double perovskite $(\text{Pr,Ba})_{0.95}(\text{Fe}_{0.95}\text{W}_{0.05})_2\text{O}_{5+\delta}$ ($0.0307 \Omega \text{ cm}^2$),⁵⁴ demonstrating the validity and superiority of ferrite oxide as an oxygen electrode. For HOR activity, the PSMFN-GDC exhibited an ASR of $0.290 \Omega \text{ cm}^2$ at 800 °C with an activation energy of 0.80 eV. These electrodes show a lower ASR value and activation energy against HOR compared to similar ferrite-oxide-based electrodes, such as $\text{Pr}_{0.4}\text{Sr}_{0.6}\text{Fe}_{0.875}\text{Mo}_{0.125}\text{O}_{3-\delta}$ ($1.6 \Omega \text{ cm}^2$, 0.95 eV),⁵⁵ which might be attributed to the fast ion transport kinetics of the transformed Ruddlesden-Popper structure, the large number of oxygen vacancies created and exsolved alloy NPs. The performance of the PSMFN-GDC symmetric cell was evaluated under an FC mode with dry H_2 flow in a fuel electrode and air flow in an oxygen electrode in Fig. 4(b) with the corresponding EIS profiles given in Fig. 4(c). Prior reduction before the performance test was also conducted in the same way as for the half-cell test. These electrodes exhibited peak power densities (PPD) of 0.702, 0.428, and 0.250 W cm^{-2} with corresponding polarization resistances of 0.370, 0.542, and $0.876 \Omega \text{ cm}^2$ under OCV at 800, 750, and 700 °C, respectively. The impressive PPD at 800 °C is comparable with other reported

electrodes adopted in symmetric SOFC operation, as shown in Fig. 4(d). To further investigate the elemental electrode process under the FC mode, EIS data under applied voltage were analyzed using distribution of relaxation time (DRT), as shown in Fig. 4(e). In the DRT plots, the area of each peak directly represents the polarization resistance of the electrode sub-process occurring in the characteristic frequency region. Under all applied voltage conditions, the DRT plots showed four peaks, which are labelled P1_F (10^3 to 10^4 Hz), P2_F (10^2 to 10^3 Hz), P3_F (10^0 to 10^2 Hz), and P4_F (10^{-1} to 10^0 Hz). According to previous study, the P1_F , P2_F , and P3_F peaks represent fuel electrode kinetics, where the P1_F is attributed to charge transport and the others reflect oxygen-transport-related processes in the fuel electrode.⁵⁶ On the other hand, the P4_F process is related mainly to the cathodic reaction, *i.e.*, ORR. Under OCV conditions, the cathodic reaction (P4_F) makes a larger contribution to overall polarization compared with P1_F , P2_F , and P3_F , indicating sluggish ORR in FC operation. In addition, while oxygen-transport-related processes, P1_F and P3_F , show negligible change in voltage, charge transfer kinetics, represented by P2_F and P4_F , could exhibit great dependency on voltage. In particular, cathodic polarization is greatly reduced with an applied voltage compared to polarization of the fuel electrode. A relatively low contribution from fuel electrode kinetics to overall polarization could be ascribed to enhanced fuel electrode kinetics by *in situ* exsolution and sluggish ORR kinetics in SOFC. A long-term stability test was conducted under a constant

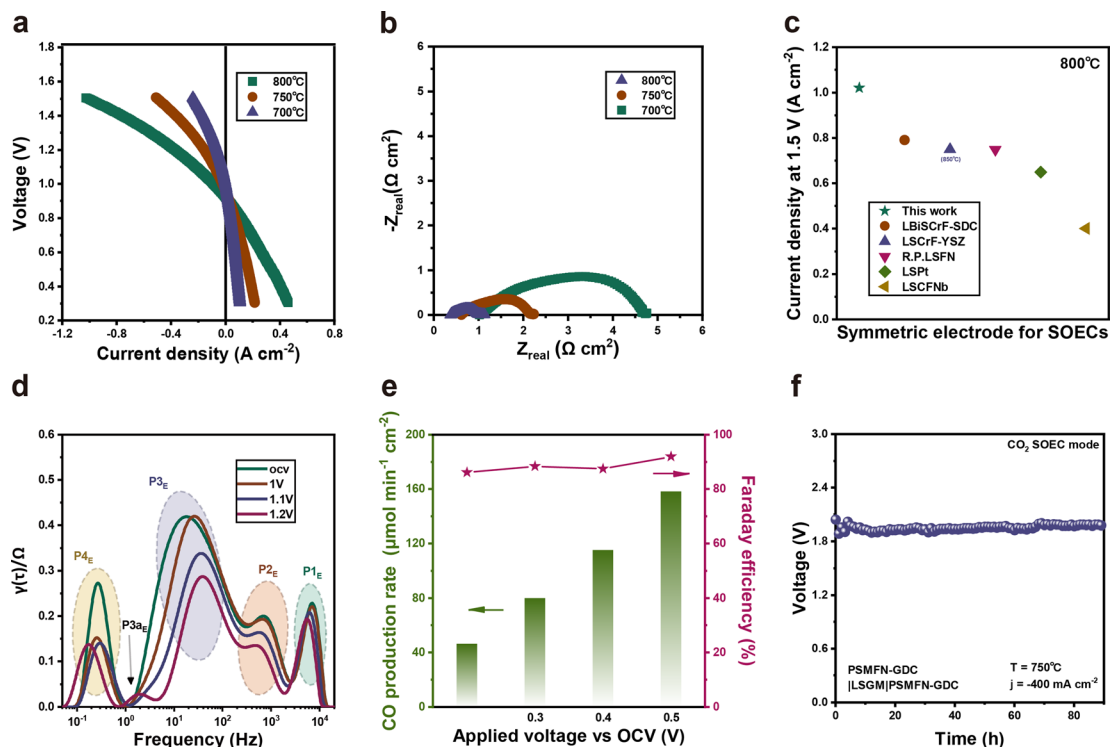


Fig. 5 PSMFN-GDC quasi-symmetric cell for CO_2 electrolysis performance evaluation. (a) I - V plots of PSMFN-GDC cell for CO_2 electrolysis under 30% CO/CO_2 and (b) Nyquist plots under OCV at 800 °C to 700 °C. (c) CO_2 electrolysis performance comparison with other symmetric SOEC electrodes. (d) DRT analyses of PSMFN-GDC cell under applied voltage conditions for CO_2 electrolysis at 800 °C. (e) Production rates of CO and corresponding Faraday efficiencies under applied voltage of 0.2–0.5 V vs. OCV at 800 °C. (f) Long-term stability test under constant current density of 280 mA cm^{-2} at 750 °C.



current density of 280 mA cm^{-2} at $750 \text{ }^\circ\text{C}$ for 100 h, where no significant voltage decay was observed, indicating the robustness of PSMFN-GDC as a symmetric electrode for SOFC (Fig. 4(f)).

Performance evaluation on SOEC mode

The electrochemical performance of the PSMFN-GDC electrode was also evaluated under an EC mode for CO_2 electrolysis (Fig. 5). The symmetric cell demonstrated notable current densities of -1.02 , -0.508 , and -0.240 A cm^{-2} at a voltage of 1.5 V at 800, 750 and 700 $^\circ\text{C}$, respectively (Fig. 5(a)). The EIS profiles in Fig. 5(b) also exhibit corresponding polarization resistances under OCV conditions, which are 0.752, 1.616, and $3.71 \text{ } \Omega \text{ cm}^2$ at each temperature. The current density values of the PSMFN-GDC symmetric cell against CO_2 electrolysis at 800 $^\circ\text{C}$ is much higher than for previously studied symmetric electrode catalysts, as summarized and listed in Fig. 5(c). DRT analysis of the EIS plots was also conducted to elucidate the electrode process of CO_2 electrolysis in SOEC. As shown in Fig. 5(d), the DRT plots present four elemental processes of oxygen ion transportation between electrolyte and electrode ($\text{P}_{1\text{E}}$), OER ($\text{P}_{2\text{E}}$), CO_2 adsorption ($\text{P}_{3\text{E}}$), and dissociation of carbonate intermediates on the cathode surface ($\text{P}_{4\text{E}}$).^{10,57} In particular, the $\text{P}_{3\text{E}}$ process made the majority of the contribution to total polarization resistance, indicating that CO_2 adsorption could be the rate-limiting step for CO_2 electrolysis in the SOEC system, in agreement with previous studies. Also, apart from the $\text{P}_{1\text{E}}$ process, three elemental processes were accelerated by applying a voltage, especially for the $\text{P}_{3\text{E}}$ process. Notably, the shoulder peak beside $\text{P}_{3\text{E}}$ ($\text{P}_{3\text{aE}}$) emerged under a high imposed voltage of 1.2 V, where this peak can be caused by a finite Warburg effect that is indicative of gas diffusion and surface processes.⁵⁸ Outlet gas analysis of CO_2 electrolysis leads to a CO production rate of $158 \text{ } \mu\text{mol cm}^{-2} \text{ min}^{-1}$ with a high Faraday efficiency of 91% at 0.5 V vs. OCV, as demonstrated in Fig. 5(e). A long-term test under a constant current density of 0.39 A cm^{-2} also demonstrated the voltage profile with a decay rate of 0.621 mV h^{-1} , indicating the stable behavior of the PSMFN-GDC symmetric electrode for CO_2 electrolysis under the EC mode.

Conclusions

In this work, PSMFN was prepared and evaluated as an efficient electrode material for Q-SSOCs. A fabricated PSMFN-GDC quasi-symmetric cell exhibited a peak power density of 0.702 W cm^{-2} under an H_2 -fed FC mode and current density of 1.02 A cm^{-2} at a voltage of 1.5 V under CO_2 electrolysis EC mode at $800 \text{ }^\circ\text{C}$. The physiochemical and electrochemical properties of PSMFN were investigated to support the electrochemical performance of a PSMFN-GDC electrode in symmetric application. Under a fuel atmosphere, PSMFN was successfully phase-transformed from single perovskite to an R.P. structure along with a simultaneous exsolution process to produce large amounts of Fe-Ni NPs. These *in situ* exsolved Fe-Ni alloy NPs were thoroughly characterized by microscopic analyses and the

great number of surface oxygen vacancies produced were examined by O 1s XPS. Furthermore, a suitable electrical conductivity of 120 S cm^{-1} and significantly low area specific resistance of $0.0371 \text{ } \Omega \text{ cm}^2$ in an air atmosphere can ensure sufficient activity towards ORR and OER. Therefore, the quasi-symmetric application of a PSMFN electrode on SOC could be a promising strategy for an efficient energy conversion system.

Author contributions

Choi J.: investigation, synthesis, formal analysis, writing – original draft, visualization. Jang D., Kim M., Ha J.: data curation. Ahn H.: writing, visualization – review & editing. Kim W. B.: project administration, supervision, conceptualization, writing – review & editing.

Conflicts of interest

There are no conflicts to declare.

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References

- 1 R. Murphy, Y. Zhou, L. Zhang, L. Soule, W. Zhang, Y. Chen and M. Liu, *Adv. Funct. Mater.*, 2020, **30**, 2002265.
- 2 W. Zhang, Y. Zhou, E. Liu, Y. Ding, Z. Luo, T. Li, N. Kane, B. Zhao, Y. Niu, Y. Liu and M. Liu, *Appl. Catal., B*, 2021, **299**, 120631.
- 3 M. A. Laguna-Bercero, *J. Power Sources*, 2012, **203**, 4–16.
- 4 J. C. Ruiz-Morales, D. Marrero-López, J. Canales-Vázquez and J. T. S. Irvine, *RSC Adv.*, 2011, **1**, 1403–1414.
- 5 A. Brisse, J. Schefold and M. Zahid, *Int. J. Hydrogen Energy*, 2008, **33**, 5375–5382.
- 6 O. A. Marina, L. R. Pederson, M. C. Williams, G. W. Coffey, K. D. Meinhardt, C. D. Nguyen and E. C. Thomsen, *J. Electrochem. Soc.*, 2007, **154**, B452.
- 7 Y. Chen, B. deGlee, Y. Tang, Z. Wang, B. Zhao, Y. Wei, L. Zhang, S. Yoo, K. Pei, J. H. Kim, Y. Ding, P. Hu, F. F. Tao and M. Liu, *Nat. Energy*, 2018, **3**, 1042–1050.
- 8 W. Zhang, X. Hu, Y. Zhou, Z. Luo, G. Nam, Y. Ding, T. Li, Z. Liu, Y. Ahn, N. Kane, W. Wang, J. Hou, D. Spradling and M. Liu, *Adv. Energy Mater.*, 2022, **12**, 2202928.
- 9 S. Park, J. M. Vohs and R. J. Gorte, *Nature*, 2000, **404**, 265–267.



- 10 S. Lee, M. Kim, K. T. Lee, J. T. S. Irvine and T. H. Shin, *Adv. Energy Mater.*, 2021, **11**, 2202928.
- 11 K. T. Bae, I. Jeong, A. Akromjon, H. N. Im and K. T. Lee, *Chem. Eng. J.*, 2023, **472**, 145015.
- 12 B. Niu, C. Lu, W. Yi, S. Luo, X. Li, X. Zhong, X. Zhao and B. Xu, *Appl. Catal., B*, 2020, **270**, 118842.
- 13 Q. Liu, X. Dong, G. Xiao, F. Zhao and F. Chen, *Adv. Mater.*, 2010, **22**, 5478–5482.
- 14 D. M. Bastidas, S. Tao and J. T. S. Irvine, *J. Mater. Chem.*, 2006, **16**, 1603–1605.
- 15 K. Zheng, J. Lach, P. Czaja, M. Gogacz, P. Czach, A. Brzozakos, P. Winiarz and J. Luo, *J. Power Sources*, 2023, **587**, 233707.
- 16 Y. Zhang, X. Zhang, J. Ni and C. Ni, *ACS Appl. Mater. Interfaces*, 2023, **15**, 3974–3984.
- 17 P. Li, Y. Xuan, B. Jiang, S. Zhang and C. Xia, *Electrochem. Commun.*, 2022, **134**, 107188.
- 18 Y. Chen, Z. Cheng, Y. Yang, Q. Gu, D. Tian, X. Lu, W. Yu and B. Lin, *J. Power Sources*, 2016, **310**, 109–117.
- 19 B. Li, S. He, J. Li, X. Yue, J. T. S. Irvine, D. Xie, J. Ni and C. Ni, *ACS Catal.*, 2020, **10**, 14398–14409.
- 20 A. P. Panunzi, L. Duranti, I. Luisetto, N. Lisi, M. Marelli and E. Di Bartolomeo, *Chem. Eng. J.*, 2023, **471**, 144448.
- 21 B. Zhang, Y. Wan, Z. Hua, K. Tang and C. Xia, *ACS Appl. Energy Mater.*, 2021, **4**, 8401–8409.
- 22 O. Kwon, S. Sengodan, K. Kim, G. Kim, H. Y. Jeong, J. Shin, Y. W. Ju, J. W. Han and G. Kim, *Nat. Commun.*, 2017, **8**, 15967.
- 23 Y. Gao, D. Chen, M. Saccoccio, Z. Lu and F. Ciucci, *Nano Energy*, 2016, **27**, 499–508.
- 24 D. Neagu, T. S. Oh, D. N. Miller, H. Ménard, S. M. Bukhari, S. R. Gamble, R. J. Gorte, J. M. Vohs and J. T. S. Irvine, *Nat. Commun.*, 2015, **6**, 8120.
- 25 D. Neagu, G. Tsekouras, D. N. Miller, H. Ménard and J. T. S. Irvine, *Nat. Chem.*, 2013, **5**, 916–923.
- 26 M. Qin, Y. Xiao, H. Yang, T. Tan, Z. Wang, X. Fan and C. Yang, *Appl. Catal., B*, 2021, **299**, 120613.
- 27 J. Choi, M. Kim, S. K. Kang, J. Kim, J. Ha, H. H. Shin, T. Park and W. B. Kim, *ACS Sustain. Chem. Eng.*, 2022, **10**, 7595–7602.
- 28 J. Choi, S. Park, H. Han, M. Kim, M. Park, J. Han and W. B. Kim, *J. Mater. Chem. A*, 2021, **9**, 8740–8748.
- 29 H. Kim, C. Lim, O. Kwon, J. Oh, M. T. Curnan, H. Y. Jeong, S. Choi, J. W. Han and G. Kim, *Nat. Commun.*, 2021, **12**, 6814.
- 30 M. Marasi, L. Duranti, I. Luisetto, E. Fabbri, S. Licocchia and E. Di Bartolomeo, *J. Power Sources*, 2023, **555**, 232399.
- 31 Y. F. Sun, Y. Q. Zhang, J. Chen, J. H. Li, Y. T. Zhu, Y. M. Zeng, B. S. Amirkhiz, J. Li, B. Hua and J. L. Luo, *Nano Lett.*, 2016, **16**, 5303–5309.
- 32 M. Chen, S. Paulson, W. H. Kan, V. Thangadurai and V. Birss, *J. Mater. Chem. A*, 2015, **3**, 22614–22626.
- 33 N. A. Baharuddin, N. A. M. N. Aman, A. Muchtar, M. R. Somalu, A. A. Samat and M. I. Aznam, *Ceram. Int.*, 2019, **45**, 12903–12909.
- 34 H. Choi, A. Fuller, J. Davis, C. Wielgus and U. S. Ozkan, *Appl. Catal., B*, 2012, **127**, 336–341.
- 35 T. H. Wan, M. Saccoccio, C. Chen and F. Ciucci, *Electrochim. Acta*, 2015, **184**, 483–499.
- 36 Y. Song, W. Wang, L. Ge, X. Xu, Z. Zhang, P. S. B. Julião, W. Zhou and Z. Shao, *Adv. Sci.*, 2017, **4**, 1700337.
- 37 J. Mizusaki, *Solid State Ionics*, 1992, **52**, 79–91.
- 38 X. Xi, X. W. Wang, Y. Fan, Q. Wang, Y. Lu, J. Li, L. Shao, J. L. Luo and X. Z. Fu, *J. Power Sources*, 2021, **482**, 228981.
- 39 J. Druce, H. Téllez, M. Burriel, M. D. Sharp, L. J. Fawcett, S. N. Cook, D. S. McPhail, T. Ishihara, H. H. Brongersma and J. A. Kilner, *Energy Environ. Sci.*, 2014, **7**, 3593–3599.
- 40 H. Sun and W. Zhou, *Energy Fuels*, 2021, **35**, 5716–5737.
- 41 A. B. Muñoz-García, A. M. Ritzmann, M. Pavone, J. A. Keith and E. A. Carter, *Acc. Chem. Res.*, 2014, **47**, 3340–3348.
- 42 R. B. Wexler, G. S. Gautam, E. B. Stechel and E. A. Carter, *J. Am. Chem. Soc.*, 2021, **143**, 13212–13227.
- 43 K. Zhao, A. Zheng, H. Li, F. He, Z. Huang, G. Wei, Y. Shen and Z. Zhao, *Appl. Catal., B*, 2017, **219**, 672–682.
- 44 S. Shah, M. Xu, X. Pan and K. L. Gilliard-Abdulaziz, *ACS Appl. Nano Mater.*, 2021, **4**, 8626–8636.
- 45 F. He, J. Chen, S. Liu, Z. Huang, G. Wei, G. Wang, Y. Cao and K. Zhao, *Int. J. Hydrogen Energy*, 2019, **44**, 10265–10276.
- 46 B. Yang, J. Bian, L. Wang, J. Wang, Y. Du, Z. Wang, C. Wu and Y. Yang, *Phys. Chem. Chem. Phys.*, 2019, **21**, 11697–11704.
- 47 T. J. Frankcombe and Y. Liu, *Chem. Mater.*, 2023, **35**, 5468–5474.
- 48 M. Chen, S. Paulson, V. Thangadurai and V. Birss, *ECS Trans.*, 2012, **45**, 343–348.
- 49 J. Mizusaki, J. Tabuchi, T. Matsuura, S. Yamauchi and K. Fueki, *J. Electrochem. Soc.*, 1989, **136**, 2082.
- 50 L. Bian, C. Liu, S. Li, J. Peng, X. Li, L. Guan, Y. Liu, J. H. Peng, S. An and X. Song, *Int. J. Hydrogen Energy*, 2020, **45**, 19813–19822.
- 51 A. P. Panunzi, L. Duranti, I. Luisetto, N. Lisi, M. Marelli and E. Di Bartolomeo, *Chem. Eng. J.*, 2023, **471**, 144448.
- 52 J. Wang, J. Zhou, J. Yang, D. Neagu, L. Fu, Z. Lian, T. H. Shin and K. Wu, *Adv. Mater. Interfaces*, 2020, **7**, 2000828.
- 53 Q. Liu, X. Dong, G. Xiao, F. Zhao and F. Chen, *Adv. Mater.*, 2010, **22**, 5478–5482.
- 54 B. Zhang, Y. Wan, Z. Hua, K. Tang and C. Xia, *ACS Appl. Energy Mater.*, 2021, **4**, 8401–8409.
- 55 D. Zhang, K. Zhang, T. He, N. Yu, Y. Zhao, Y. Wang and T. Liu, *Int. J. Hydrogen Energy*, 2020, **45**, 21825–21835.
- 56 S. M. Choi, H. An, K. J. Yoon, B. K. Kim, H. W. Lee, J. W. Son, H. Kim, D. Shin, H. I. Ji and J. H. Lee, *Appl. Energy*, 2019, **233–234**, 29–36.
- 57 X. Zhang, Y. Song, F. Guan, Y. Zhou, H. Lv, G. Wang and X. Bao, *J. Catal.*, 2018, **359**, 8–16.
- 58 I. D. Unachukwu, V. Vibhu, J. Uecker, I. C. Vinke, R. A. Eichel and L. G. J. B. de Haart, *J. CO₂ Util.*, 2023, **69**, 102423.

