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Dual-function additive enables a self-regulatory mechanism to balance cathode–anode interface demands in Zn||MnO₂ batteries†

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The poor reversibility of the zinc (Zn) anodes and the irreversible deposition/dissolution of Mn²⁺/MnO₂ significantly impede the commercialization of Zn–Mn aqueous batteries (ZMABs). In reducing the difference between the desired interfacial reaction environments of the cathode and anode, we found that they face the same problem of interference—the generation of irreversible corrosion products. Herein, we have introduced a novel self-regulatory mechanism. This mechanism involves the addition of sodium dihydrogen phosphate, which shifts from passive protection to active regulation. It effectively captures OH[−] ions, prevents corrosion product formation, and facilitates the *in situ* generation of a solid electrolyte interface (SEI) film. This modification also homogenizes Zn ion flow and improves the reversibility of Zn plating and stripping. Furthermore, a stable and slightly acidic environment has been established to stabilize the pH at the cathodic interface, mitigate corrosion product formation, and enhance the reversible deposition and dissolution of Mn²⁺/MnO₂. With the optimal electrolyte, Zn||Zn symmetric cells demonstrate stable operation for over 3000 hours at 1 mA cm^{−2}, 1 mA h cm^{−2}. Additionally, the Zn||Cu cells maintain high reversibility after 1000 cycles, achieving an average coulombic efficiency (CE) of 99.76%. The assembled Zn||MnO₂ full cells exhibit exceptional cycling stability and rate performance. This work adopts the approach of seeking common ground and emphasizing the balance of cathode and anode interfacial requirements, which represents a new and significant insight for design of ZMABs with high reversibility and high cyclability.

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1 Introduction

Aqueous Zn-ion batteries (AZIBs) are among the most promising candidates for energy storage systems, favored for their high safety, high volumetric energy density (5855 mA h cm^{−3}), low redox potential (Zn/Zn²⁺ at −0.76 V vs. SHE), and environmental friendliness.^{1–3} MnO₂ is extensively used as a cathode material for AZIBs due to its theoretical specific capacity, high redox potential, abundant resources, and low toxicity.^{4–6} Nevertheless, the differing interface requirements between manganese-based cathodes and Zn anodes limit its application.

One significant challenge is the poor reversibility of the Zn anode, which hinders the development of AZIBs.⁷ During the Zn plating/stripping process, massive electrons/ions accumulate at the interface, leading to polarization potential fluctuations and disordered diffusion, resulting in rampant Zn dendrite growth. Therefore, regulating the spatial electric field distribution and homogenizing Zn ion flow are critical for achieving uniform Zn deposition.^{8–10} Additionally, parasitic hydrogen evolution reactions (HER) produce excess OH[−], leading to the formation of insulating Zn₄(OH)₆SO₄·xH₂O byproducts (ZHS). These byproducts cause non-homogeneous Zn²⁺ flux and electric fields at the interface,^{11,12} further disrupting electrodeposition and leading to irreversible imbalances. The phase transition and dissolution of manganese oxides, as well as side reactions between the electrode and electrolyte, also hinder commercialization.¹³ The abundance of OH[−] ions from the manganese dissolution reaction increases the local pH, promoting rapid formation of byproducts at the cathodic interface.^{14,15} Moreover, the poor electrical and ionic conductivity of these byproducts significantly limits charge transfer. Consequently, Mn²⁺ generated during the discharge process diffuses irreversibly into the electrolyte and does not return to the cathode surface during charging, resulting in capacity degradation through irreversible

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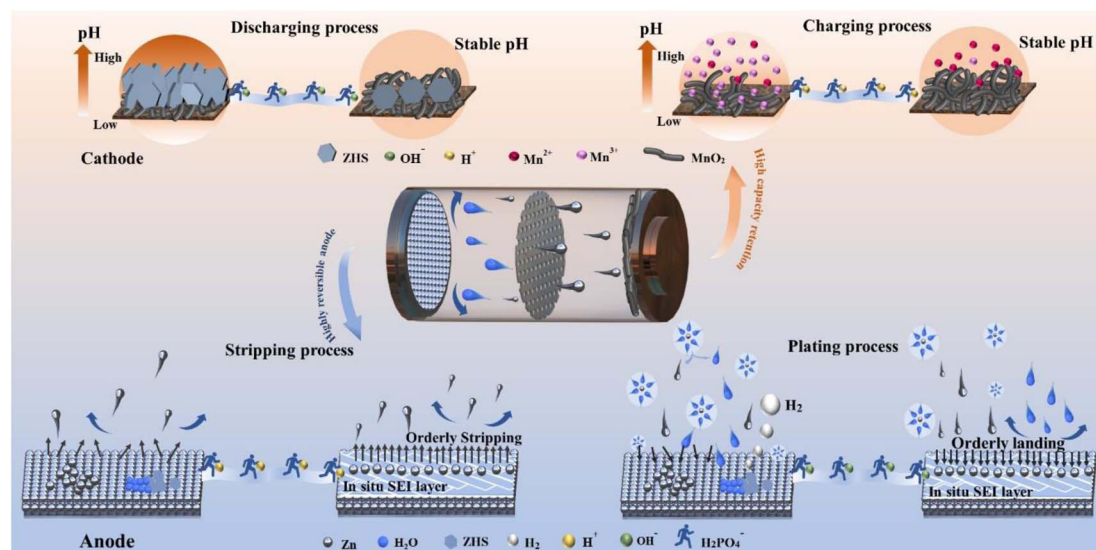
$\text{Mn}^{2+}/\text{MnO}_2$ deposition/dissolution reactions at the manganese cathode.^{16,17}

The pivotal determinant of high performance in Zn–manganese batteries lies in the reversibility of both cathode and anode processes. Any imbalance in either component sets off an irreversible chain reaction. Yet, concurrently, we've noted significant disparities and even contradictions in the desired interfacial reaction environments of the cathode and anode during charging and discharging. The recognized energy storage mechanisms of ZMABs can be categorized into (1) H^+ and/or Zn^{2+} dominated insertion/deinsertion, and (2) deposition/dissolution type electrolytic reactions ($\text{Mn}^{2+} \rightarrow \text{Mn}^{n+}$, $2 < n \leq 4$).^{18,19} Numerous studies have underscored the influence of pH changes on the deposition/dissolution of $\text{Mn}^{2+}/\text{MnO}_2$.^{20,21} In a 2 M ZnSO_4 solution, the former necessitates proton capture to prevent excessive formation of unutilized Mn^{3+} , while the latter requires proton provision, otherwise, creating a conducive environment for ZHS generation due to insufficient proton concentration and the formation of MnOOH and M_xMnO_2 .^{19,22,23} Hence, coordinating these processes assumes paramount importance. Fluctuations in pH not only dramatically affect the reversibility of $\text{Mn}^{2+}/\text{MnO}_2$ deposition/dissolution but also severely impact the stability of the anode interface. Zn ion deposition, coupled with persistent HER, exacerbates the elevated local OH^- concentration. These reactions can further alter the local pH and reduce the reversibility of Zn/Zn^{2+} by forming inactive solid byproducts like Zn oxides or hydroxides.^{24,25} Achieving a stable and moderately acidic environment is thus crucial for balancing efficient battery operation.

In response, numerous studies have employed decoupled electrolyte systems to segregate the operating conditions of the MnO_2 cathode and the Zn anode within a single cell, enhancing the operating voltage window and significantly improving battery life.^{26–28} However, these systems require costly ion-

selective membranes to prevent cross-mixing during cycling and are rarely used in smaller devices due to the stringent manufacturing processes.²⁹ Alternative strategies include constructing anhydrous or water-poor environments^{30–34} and using electrolyte additives that have been available to regulate pH to stabilize interfacial environments, or to construct interfacial layers to inhibit parasitic reactions on Zn metals with remarkable success.^{35–39} These approaches have predominantly focused on suppressing undesirable phenomena at the Zn anode while often neglecting cathodic chemistry. Therefore, in the process of meeting the interface requirements of the anode and cathode in a normal system, the discussion of interface compatibility and its dynamic self-regulation mechanism is also a relatively unexplored and neglected area.

To address the simultaneous interfacial challenges faced by both the cathode and anode—particularly the generation of irreversible corrosion products—we have developed a self-regulatory mechanism by incorporating a small amount of sodium dihydrogen phosphate (NaH_2PO_4 , denoted as SDP). This additive not only neutralizes OH^- ions generated during hydrogen precipitation but also forms a protective $\text{Zn}_3(\text{PO}_4)_2 \cdot 4\text{H}_2\text{O}$ (ZnPO) layer *in situ*, shielding the Zn anode from further corrosive damage. Simultaneously, the generated ZnPO film can homogenize the Zn ion flow and buffer the concentration polarization caused by localized over-consumption of Zn ions. Unlike other phosphate additives, SDP actively stabilizes pH on the cathode side, capturing excess OH^- ions, slowing down inert byproduct formation, promoting reversible $\text{Mn}^{2+}/\text{MnO}_2$ processes, and stabilizing pH fluctuations during cycling (Scheme 1). Specifically, Zn||Zn symmetric cells can operate stably for over 3000 hours at 1 mA cm^{-2} , 1 mA h cm^{-2} . The deep cycle stability exceeds 180 hours (DOD = 50%, which is 5 times that of the base electrolyte.) The Zn||Cu cell exhibits high reversibility after 1000 cycles, with an average coulombic Efficiency (CE) of 99.76%, and the assembled Zn|| MnO_2 full cell



Scheme 1 Schematic illustration of the regulation behavior of the SDP additive on the cathode and anode bilateral interface synchronously.

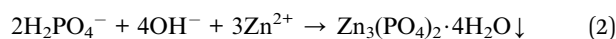
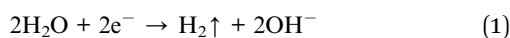


delivers excellent cycling stability and multiplicity performance. This “self-regulation” strategy significantly enhances the reversibility of Zn anode plating/stripping and $\text{Mn}^{2+}/\text{MnO}_2$ deposition/dissolution, providing a novel approach to developing highly reversible aqueous metal batteries with practical applications.

2 Results and discussion

2.1. Stabilization of pH and inhibition of ZHS

The continuous HER on the anode exacerbates the fluctuation of H^+ concentration and leads to the increase of local OH^- concentration (Fig. 1a). SDP counters this by binding to OH^- ions through its buffering effect and *in situ* forms a solid electrolyte interface (SEI) film. This film specifically adsorbs onto the surface of the Zn foil, creating a protective layer that effectively inhibits the HER, mitigates electrochemical corrosion, and slows the formation of inert ZHS. The dynamic SEI adsorption layer provides steric hindrance, blocking active corrosion sites and limiting the random two-dimensional diffusion of Zn^{2+} ions (Fig. 1b). The *in situ* formation mechanism of the SEI film can be described as follows:



In situ pH monitoring in a $\text{Zn}||\text{Zn}$ symmetric cell reveals that the pH in 2 M ZnSO_4 (base electrolyte, BE) gradually increases during discharge and remains relatively unchanged during charging (Fig. 1c). To ensure consistency between the initial pH values of the BE and SDP-modified Zn electrolyte (SDP-BE), 0.05 mol sulfuric acid (S-BE) was used for calibration. Despite this, the pH with SDP addition remains more stable, highlighting its effectiveness in trapping elevated local OH^- concentrations resulting from HER, thus stabilizing the interfacial pH and inhibiting corrosion product formation. This effect is corroborated by X-ray diffraction (XRD) patterns (Fig. 1d, and e), where a pronounced diffraction peak at 8.5° , corresponding to ZHS (PDF:44-0673),⁴⁰ was observed in BE over several cycles. Furthermore, a $\text{Zn}||\text{Zn}$ symmetric cell was assembled and left to rest for 12 hours for *in situ* electrochemical impedance spectroscopy (EIS) testing. The initial reduction in charge transfer resistance (R_{ct}) over the first nine cycles is attributed to the dissolution of loosely attached electrolyte and oxide layers, which exposes previously covered active sites.⁴¹ Beyond the tenth cycle, R_{ct} values for the BE increase (Fig. 1g), while the SDP-BE maintains a steady state (Fig. 1h). This difference arises because ZHS continuously forms on the Zn surface during the cycling process, post the stripping of the pre-attached layers. ZHS covers the active sites, obstructing ion transport pathways and degrading cycling performance. This passive and constrained mechanism leads to the continuous accumulation of ZHS and electrolyte depletion.^{42,43} In contrast, the addition of SDP results in the formation of an *in situ* ZnPO interfacial layer, which homogenizes Zn ion flow and

neutralizes the local pH increase, effectively suppressing the generation of ZHS at the source and maintaining a stable interfacial environment.

2.2. Mechanism and effects of *in situ* membrane formation

The formation of ZnPO in the self-regulatory mechanism is triggered by an increase in pH, and in order to investigate the membrane-forming mechanism, the electron probe X-ray micro analyzer (EPMA) was conducted on the copper surface during Zn deposition. The EPMA results reveal a uniform distribution of Zn, O, and P across the Zn surface (Fig. S5),[†] confirming the homogeneous formation of the ZnPO layer. X-ray photoelectron spectroscopy (XPS) analysis of the SDP-BE confirmed the presence of P–O bond in phosphate anions (PO_4^{3-}) represented by characteristic peaks at 133.4 eV (P 2p), and the characteristic peak of the Zn 2p_{3/2} peak at 1022.2 eV, corresponding to the formation of an abundant Zn^{2+} in ZnPO (Fig. 2c and d).^{44–46} Transmission electron microscope (TEM) and elemental mapping support the formation of a P, O and Zn rich SEI layer on the surface (Fig. 2a and b).

Further investigations into the dynamic reversibility of the ZnPO layer were conducted using *ex situ* EPMA (site-specific labeling technique) to analyze elemental content and distribution on the Cu foil during Zn deposition and stripping (Fig. 2e and f). Initially, the content of Zn and P during discharge was recorded at 150 and 6.2, respectively. After charging, these values decreased to 4.2 for Zn and 6.0 for P, suggesting a partial dynamic stripping of the ZnPO film concurrent with Zn stripping. *In situ* electro-chemical quartz crystal microbalance (EQCM) coupled with chronopotentiometry (CP) was used to monitor the mass change of the working electrode during the Zn plating/stripping processes (Fig. S6).[†] Based on previous validation, the 10 ng difference in mass left on the crystal sheet compared to the sample without SDP additive can be attributed to the ZnPO film (Fig. S7).[†] Fig. 2i illustrates the mass efficiency and mass change over ten cycles. It can be seen that after the first cycle, the deposited/stripped mass decreases and the mass efficiency is close to 100%, suggesting that ZnPO film induces reversible Zn deposition/stripping while stabilising pH fluctuations, and the ZnPO film is then in a steady and reversible state.

This is confirmed by the findings of white light interferometry comparing the anode surfaces for different numbers of cycles (Fig. 3a and b), where it is observed that the ZnPO film is being generated during the initial cycles and the surface of the SDP-BE became more uniform as the cycle progressed, comparing with the surface of the BE sample showing inhomogeneous adherence at 10 cycles. The cross-sectional SEM images after 10 cycles show a homogeneous ZnPO interfacial layer on the Zn surface, contrasting with the irregular ZHS coverage observed on the BE surface (Fig. 3c, and S8[†]). Dynamic contact angle tests conducted over 15 minutes demonstrated that the SDP-Zn electrolyte wets the Zn plate more rapidly than the BE, enhancing electrode/electrolyte contact and accelerating Zn ion migration kinetics (Fig. 3d).⁴⁷ Assessing the initial deposition, the surface roughness (S_a) of BE was 0.249 μm ,



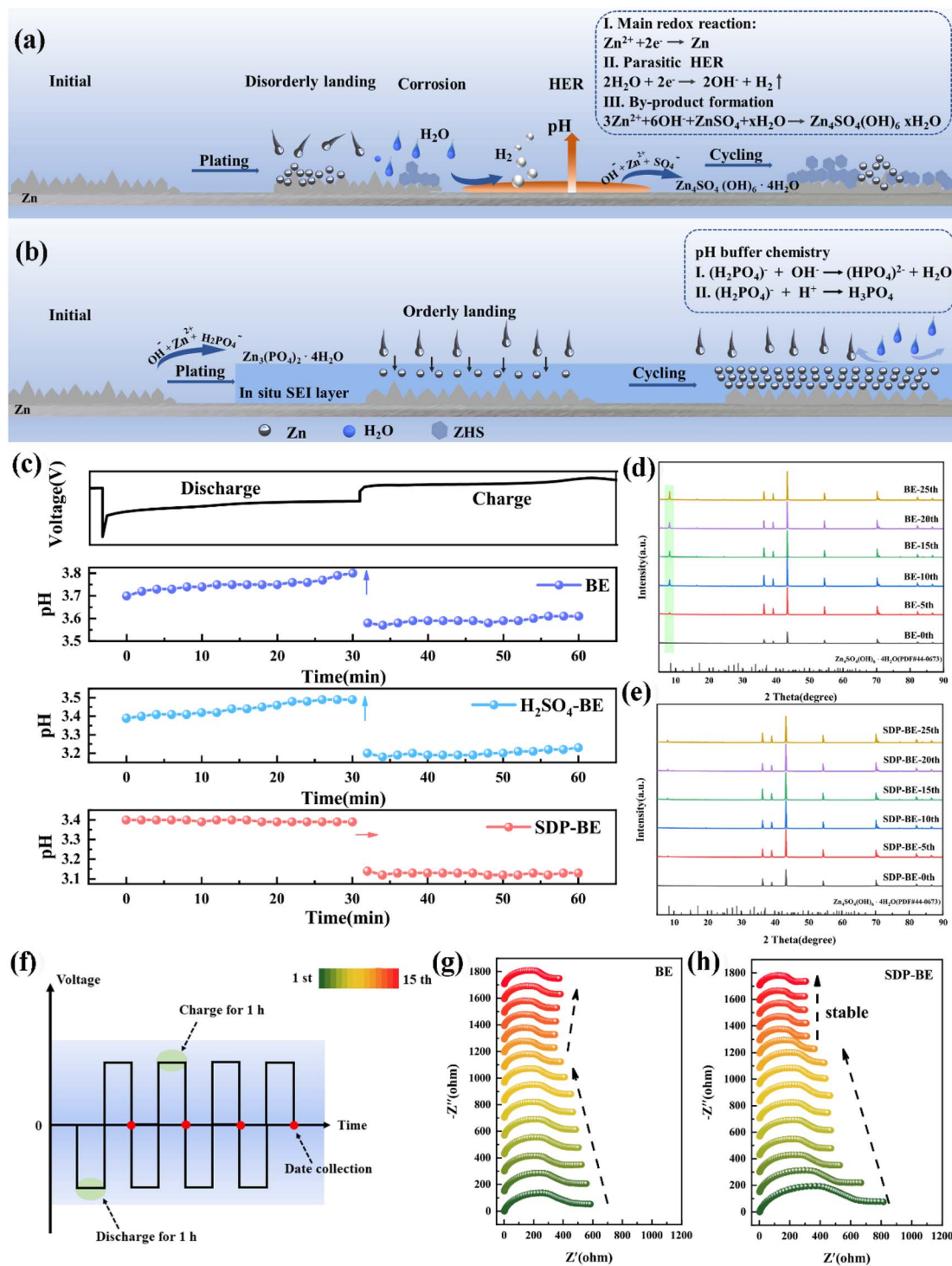


Fig. 1 Schematic illustration of electrochemical behavior at Zn/electrolyte interface. (a) Without SDP additives. (b) With SDP additives. (c) *In situ* pH monitoring in discharge and charge. XRD patterns of Zn electrodes at different number of cycles. (d) Without SDP additives. (e) With SDP additives. *In situ* impedance spectrum of Zn||Zn batteries in different electrolytes. (f) Charging and discharging schematic. (g) Without SDP additives. (h) With SDP additives.

significantly higher than that of SDP-BE (Fig. 3e, and f). The uniform Zn ion flow and inhibition of corrosion products by the ZnPO layer contribute to a smooth and flat surface morphology observed over 1 to 50 cycles. In contrast, significant Zn dendrites and interspersed corrosion products were noted on

the BE surface at both the initial and 50th cycle. Cross-sectional analysis revealed a loose and porous deposit approximately 89 μm thick on the BE surface, likely comprising a mix of corrosion products and inactive Zn (Fig. 3g, and h). The *in situ* formed ZnPO film by SDP-BE shields the Zn anode from corrosive

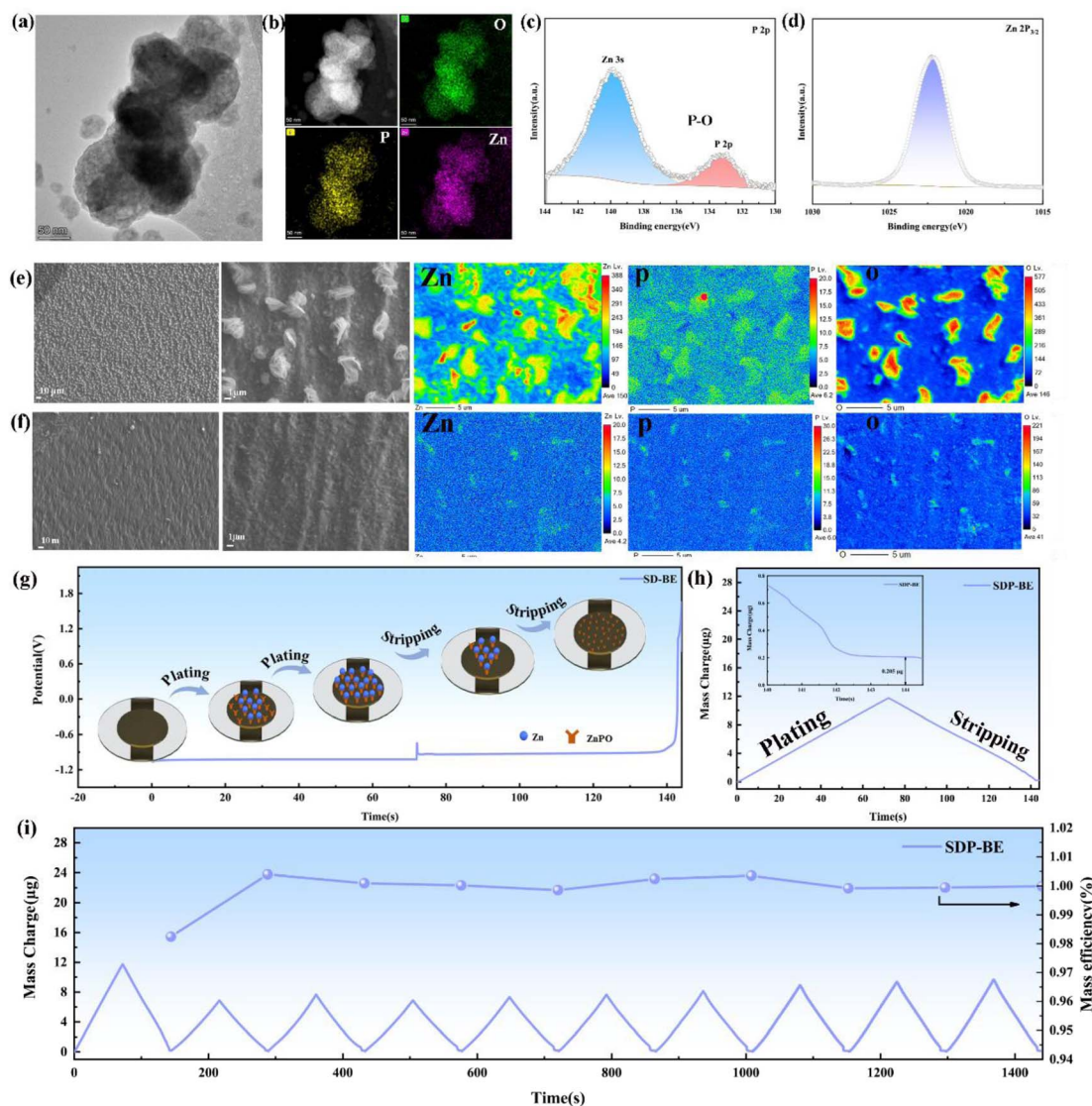


Fig. 2 (a) TEM image. (b) HADDF-STEM image and elemental mappings of ZnPO. XPS spectrum of Zn electrode in the electrolytes with SDP. (c) P 2p, (d) Zn 2p. SEM image and corresponding EPMA elemental mappings of Cu electrode in different states at 5 mA cm^{-2} , 1 mA h cm^{-2} . (e) Upon completion of Zn deposition. (f) Upon completion of Zn stripping. (g) Schematic diagram of an EQCM coupled with CP to track the plating/stripping process at 5 mA cm^{-2} . (h) Mass change in the first circle of the SDP-BE. (i) The mass efficiency and mass change over ten cycles.

media, reducing thermodynamic instability at the anode-electrolyte interface. Specifically, the addition of SDP lowered the corrosion current from 4.649×10^{-3} to $3.208 \times 10^{-3} \text{ A cm}^{-2}$ and increased the corrosion potential from -0.995 V to -0.988 V in the Tafel test, and the hydrogen precipitation potential increased from 122 mV to 132 mV in the linear sweep voltammetry test at a current density of -20 mA cm^{-2} (Fig. S11).†

To further explore how the ZnPO interfacial layer promotes uniform Zn deposition, density functional theory (DFT) calculations were conducted. These calculations demonstrate that the adsorption energy of Zn ions on the ZnPO surface is significantly higher at -2.93 eV compared to -0.31 eV on the Zn(002) surface (Fig. 4a, and b). This suggests that ZnPO acts as a zincophilic site, preferentially capturing Zn ions and promoting homogeneous Zn galvanization under electric field

influence. Moreover, theoretical simulations were performed to compare the migration energy barriers for Zn ions in ZnPO and ZHS. The results indicate that the migration energy barrier in ZnPO is much lower (0.32 eV) compared to 1.85 eV in ZHS (Fig. 4c–e), demonstrating that the ZnPO layer facilitates the rapid migration of Zn ions and immobilization by deposition. Combined with SEM images of bare Zn cross sections (Fig. 4f, and g), the COMSOL simulation results show that the addition of SDP can homogenize the local electric field and Zn ion concentration distribution for uniform galvanization (Fig. 4h, and i). Fig. 4j highlights the comparative analysis of Zn dendrite formation on BE and SDP-BE surfaces. Over time, Zn dendrites on the BE surface become progressively larger under a current density of 5 mA cm^{-2} . In stark contrast, the SDP-BE exhibits flatter and more uniform Zn deposition under the same operational conditions.



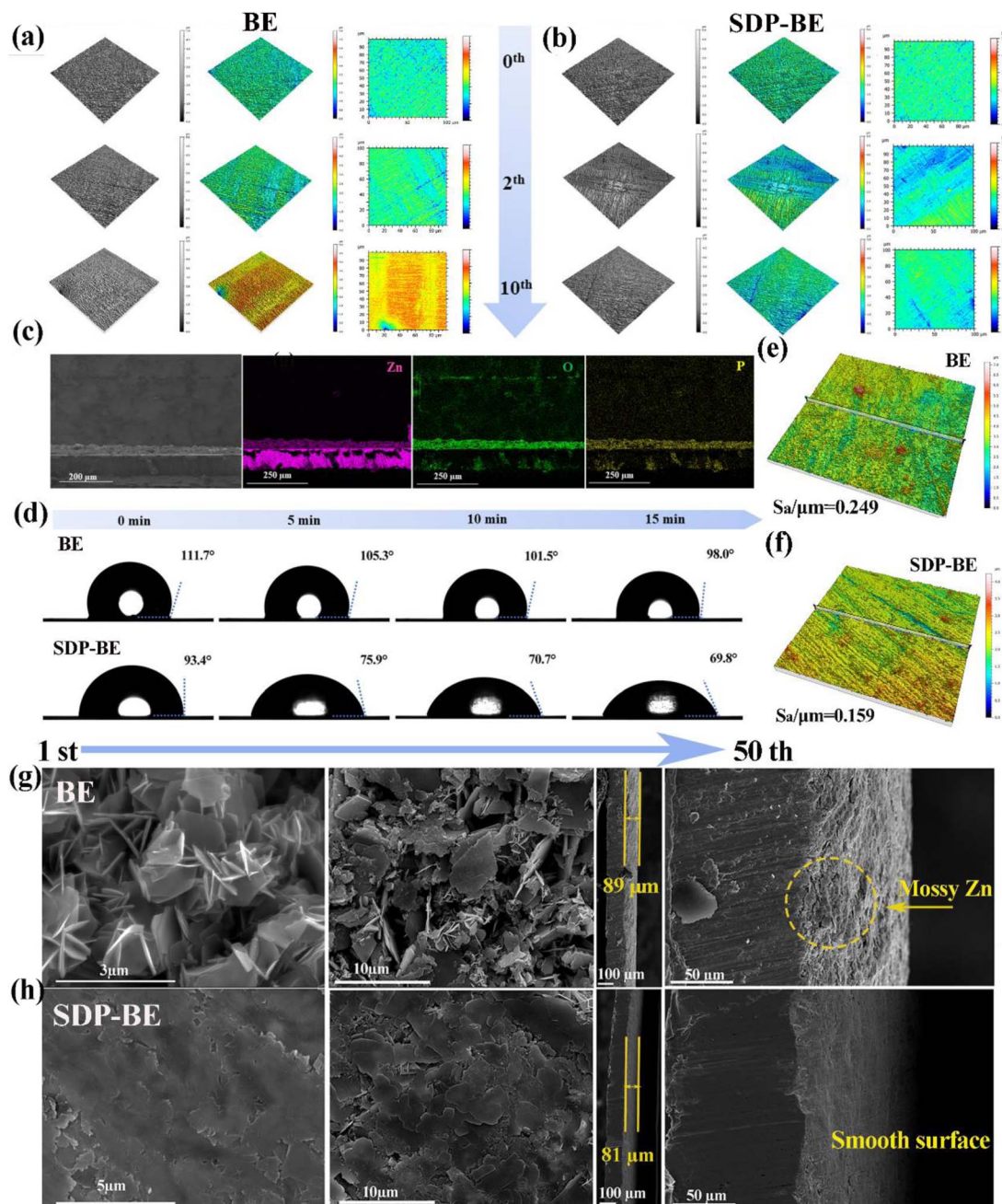


Fig. 3 White light interferometer images at different number of cycles. (a) Without SDP additives. (b) With SDP additives. (c) Cross-section SEM image and corresponding EDS elemental mappings of Zn electrode at 1 mA cm^{-2} , 1 mA h cm^{-2} after 10 cycles. (d) Dynamic contact angles of different solutions on Zn plates. 3D white light interferometer images of Zn electrode in different solutions after Zn deposition. (e) Without SDP additives. (f) With SDP additives. SEM images of planar surfaces and cross sections for 1 and 50 cycles at 5 mA cm^{-2} , 1 mA h cm^{-2} . (g) Without SDP additives. (h) With SDP additives.

2.3. Induced Zn ordered plating/stripping and electrochemical properties

To explore the mechanism behind the SDP-BE induced reversible plating/stripping of Zn, *ex situ* white light interferometry was employed to monitor the morphological evolution of Zn plating/stripping at a current density of 5 mA cm^{-2} (Fig. 5a-c). At stage II, the bare Zn||Cu surface exhibits an inhomogeneous distribution of Zn, with pronounced localized aggregation

evident by stage III. This aggregation persists through the stripping phases (stages IV and V), leaving the Cu surface highly aggregated and inhomogeneous, which undermines the stability of subsequent Zn plating/stripping cycles. In contrast, the SDP-Zn||Cu surface maintains a uniform Zn deposition across the entire interface, and the Cu foil surface remains relatively flat even after stripping is completed in stages IV and V. These observations confirm that the SDP additive

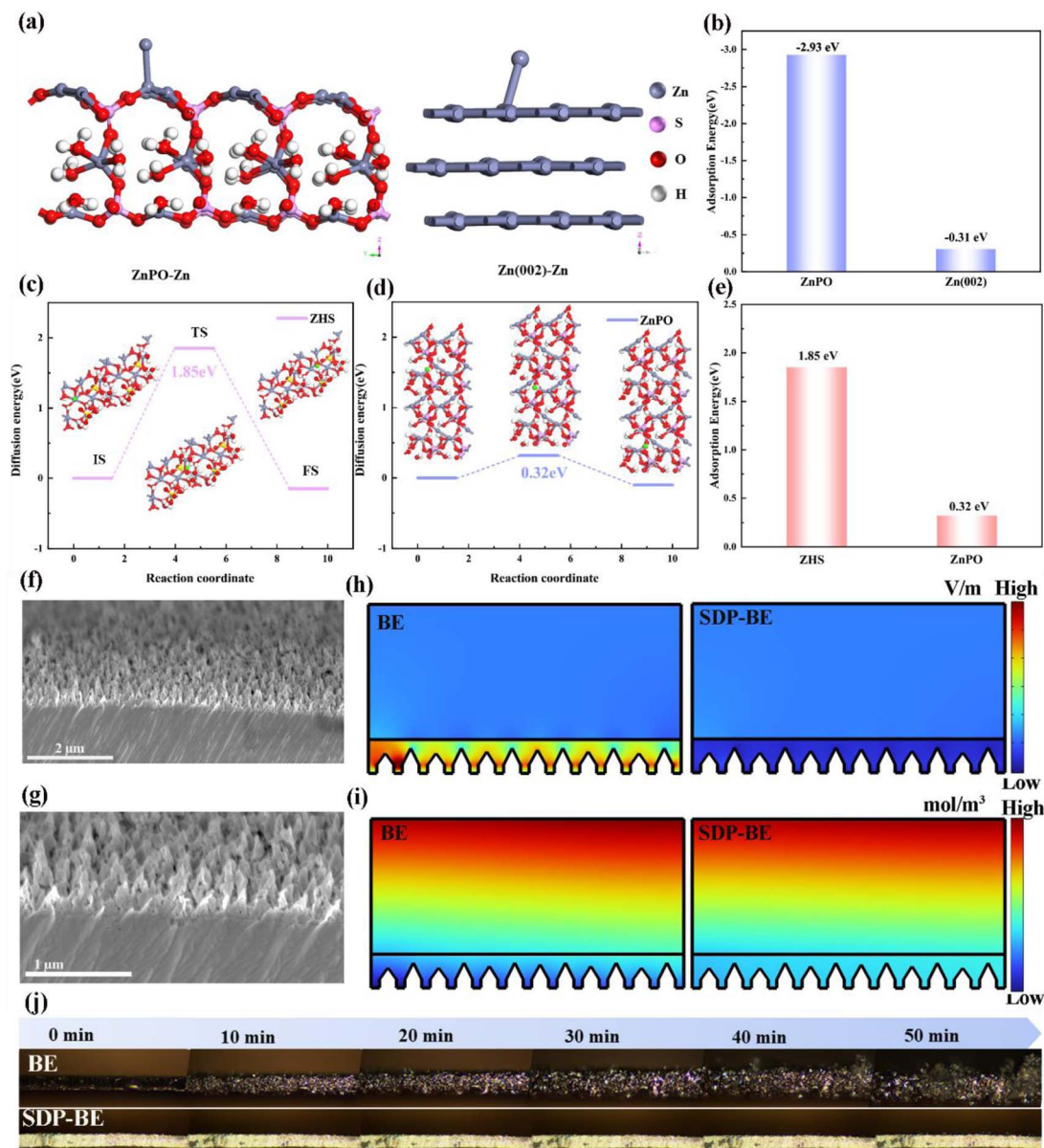


Fig. 4 (a) Adsorption models of Zn on bare Zn and ZnPO. (b) Adsorption energies of Zn on bare Zn and ZnPO. (c) Schematic diagram of Zn migration in the ZHS. (d) Schematic diagram of Zn migration in the ZnPO. (e) Zn-migration energy barrier on different surfaces. (f) SEM image of the cross section of bare Zn. (g) Enlarged view of the cross-sectional SEM image of bare Zn. (h) Simulated electric field distributions on Zn plate in different electrolytes. (i) Simulated Zn ion concentration distributions on Zn plate in different electrolytes. (j) *In situ* optical microscopy visualization of Zn plating on in different electrolytes.

significantly enhances the reversibility of plating/stripping in the Zn||Cu cell.

The CA test in Fig. 5d offers further insights into the Zn ion diffusion dynamics during deposition. The current density on the bare Zn surface continues to rise monotonically at 100 seconds, indicative of uncontrolled two-dimensional (2D) diffusion. Conversely, the *in situ* generated ZnPO buffer layer on the Zn surface curtails the rampant nucleation of Zn, thereby restricting the stochastic 2D diffusion of Zn^{2+} ions and mitigating the “tip effect”. The uncontrolled growth observed on the bare Zn is further highlighted by aggregation phenomena in the

three-dimensional (3D) plot (Fig. S12),[†] which contributes to a gradual increase in nucleation resistance. In contrast, SDP-Zn results in more uniform deposition on the Zn foil surfaces, which significantly improves their electrochemical performance by stabilizing diffusion dynamics and reducing nucleation barriers.

Specifically, the SDP-Zn||Cu asymmetric cell demonstrates a stable voltage profile up to 1500 cycles with an average CE of 99.76% at 2 mA cm^{-2} , 1 mA h cm^{-2} (Fig. 5e). In contrast, the voltage profile of the BE progressively increases with each cycle, indicating degradation (Fig. S13).[†] Similarly, the assembled



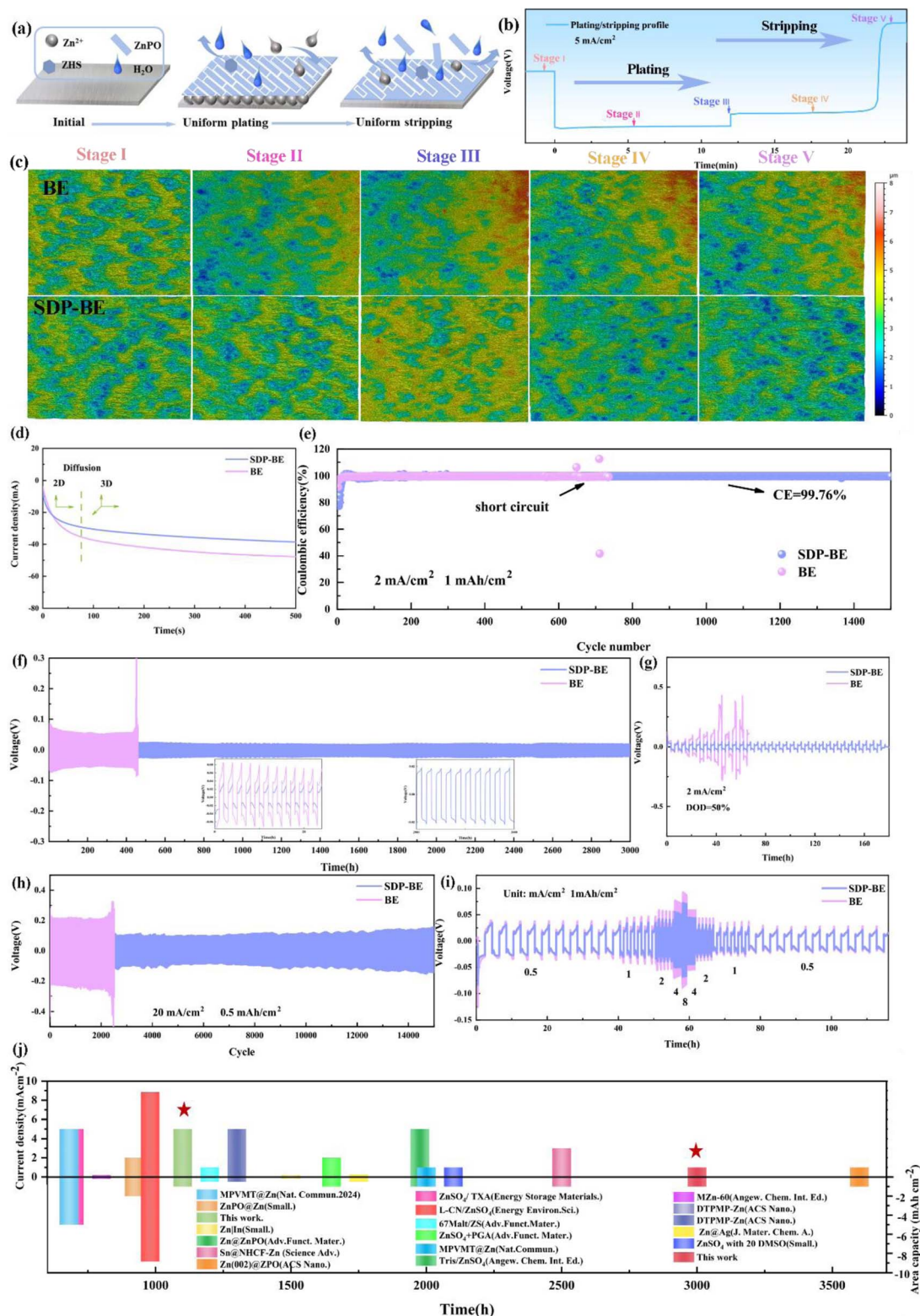


Fig. 5 (a) Schematic diagram of SDP additive induced uniform plating/stripping of Zn. (b) Plating/stripping curves for Zn||Cu cells. (c) Corresponding 3D white light interferometer images of Zn electrode in different solutions. Electrochemical testing of different solutions with and without SDP additive. (d) Chronoamperograms (CAs) curves. (e) coulombic efficiencies of the Zn plating/stripping of Cu||Zn cell. (f) Cycling performance of Zn||Zn symmetric Zn cells at 1.0 mA cm⁻² and 1.0 mA h cm⁻². (g) 2.0 mA cm⁻² and 20 μm thick Zn foil. (h) And 20.0 mA cm⁻² and 0.5 mA h cm⁻². (i) The rate performance at various current densities of Zn||Zn symmetric cells. (j) The comparison of cyclic reversibility between this work and previous reports.

Zn||Zn symmetric cell using SDP shows remarkable stability, sustaining 3000 hours of cycling at 1 mA cm^{-2} , 1 mA h cm^{-2} , significantly surpassing the endurance of the bare Zn||Zn cell (Fig. 5f). Increasing the current to 5 mA cm^{-2} , the SDP-Zn can be cycled stably for 1200 h, while the bare Zn has a sharp rise in polarization voltage after 200 h, leading to cell failure (Fig. S14).† The same phenomenon occurs when the current is 20 mA cm^{-2} and the capacity is 0.5 mA h cm^{-2} (Fig. 5g). In the extreme case, SDP-BE records stable cycling up to 180 h when DOD_{Zn} is increased to 50%, in contrast to BE, which fails after 50 h due to a sudden drop in voltage (Fig. 5h). Furthermore, Fig. 5i illustrates that the overpotential in the SDP-BE symmetric cell remains consistently low and stable across all tested current densities, contrasting sharply with the higher overpotentials observed in the BE. These improvements in

electrochemical performance validate that the SEI film generated by the self-regulatory Mechanism significantly enhances the reversibility of Zn plating/stripping reactions. Additionally, comparisons with findings from other studies highlight substantial benefits provided by SDP, affirming its superior performance (Fig. 5j).

2.4. Suppression of side reactions and full cell performance

To assess the practicality of SDP additives, $\alpha\text{-MnO}_2$ was employed as the cathode material in full cells (Fig. S15 and S16).† The SDP-Zn|| MnO_2 full cell demonstrates higher peak currents in cyclic voltammetry (CV) curves compared to the Zn|| MnO_2 cell, indicating enhanced reaction kinetics (Fig. 6a). The evaluation of the EIS tests further quantifies this enhancement, where the R_{ct} of the Zn|| $\alpha\text{-MnO}_2$ cell is approximately double that of the SDP-

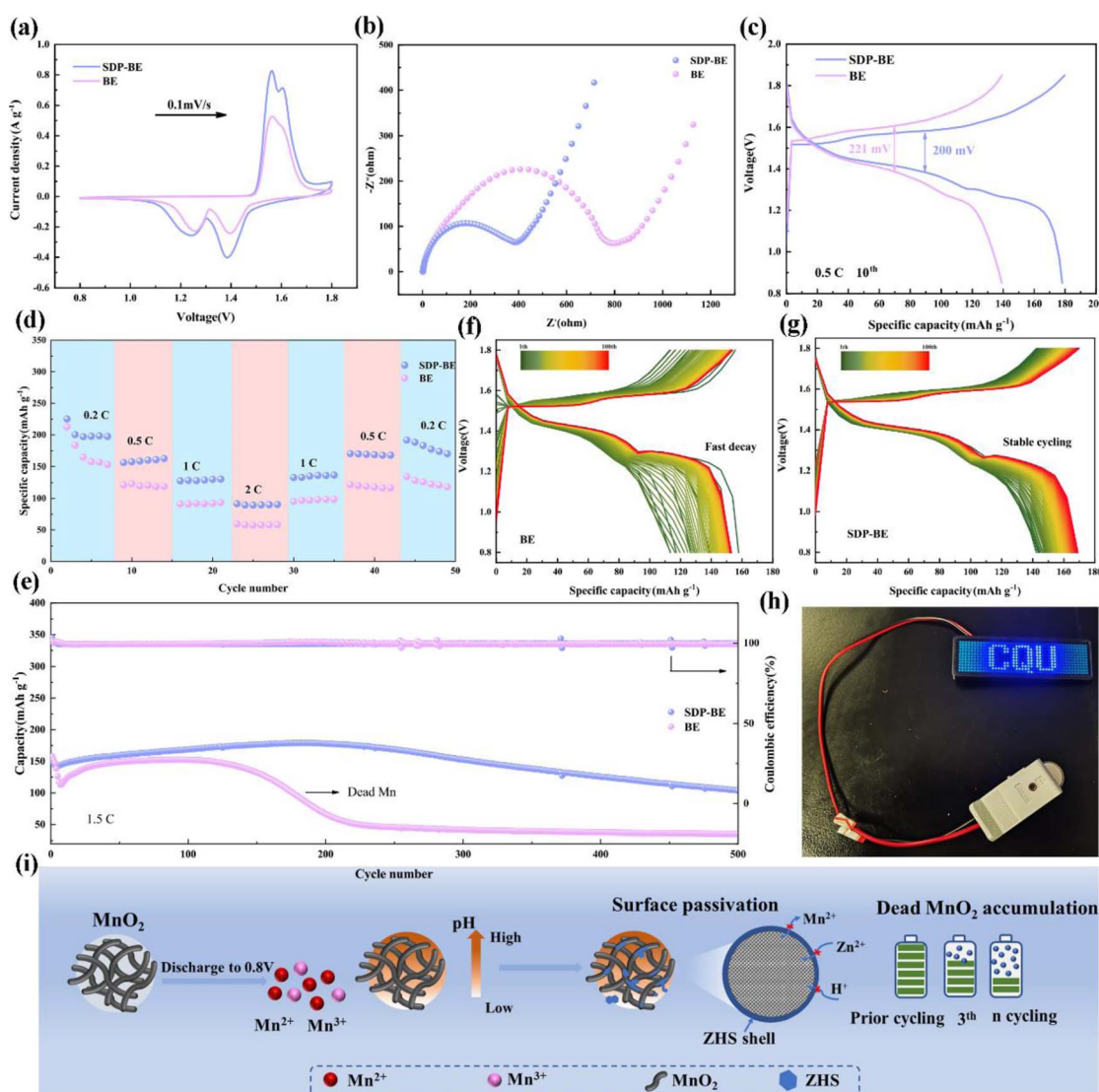


Fig. 6 Electrochemical performance of Zn|| MnO_2 full cell with and without SDP additive. (a) CV curves. (b) Nyquist plots. (c) Galvanostatic charge/discharge of Zn|| MnO_2 batteries at 0.5C. (d) Rate performance. (e) Long-term cycling performance at 1.5C. (f) The corresponding charge/discharge voltage–capacity profiles at different cycle without SDP additive. (g) The corresponding charge/discharge voltage–capacity profiles at different cycle with SDP additive. (h) A picture of three-connected Zn|| MnO_2 full cell with SDP additive lighting up a LED display screen. (i) Schematic diagram of the full battery without SDP additive.



Zn||MnO₂ cell, suggesting faster electron mobility in the latter (Fig. 6b). Additionally, the SDP-Zn||MnO₂ cathode exhibits a significantly reduced potential gap ($\Delta E = 200$ mV) between the charge and discharge plateaus compared to the Zn||MnO₂ cathode, indicating lower polarization (Fig. 6c). The practical application is further demonstrated as connecting three SDP-BE cells in series successfully powers an LED (Fig. 6h). Regarding

rate capability, the SDP-Zn||MnO₂ full cell achieves a capacity recovery of 93%, significantly higher than the 77% observed with the standard Zn||MnO₂ when returning to a rate of 0.2C (Fig. 6d). At varying rates, the full cell with bare Zn shows markedly lower capacities than the SDP-Zn||MnO₂ (Fig. S17).† In a long cycling test at a rate of 1.5C, the Zn|| α -MnO₂ retains only 27.1% of its initial capacity after 300 cycles, whereas the SDP-Zn||MnO₂

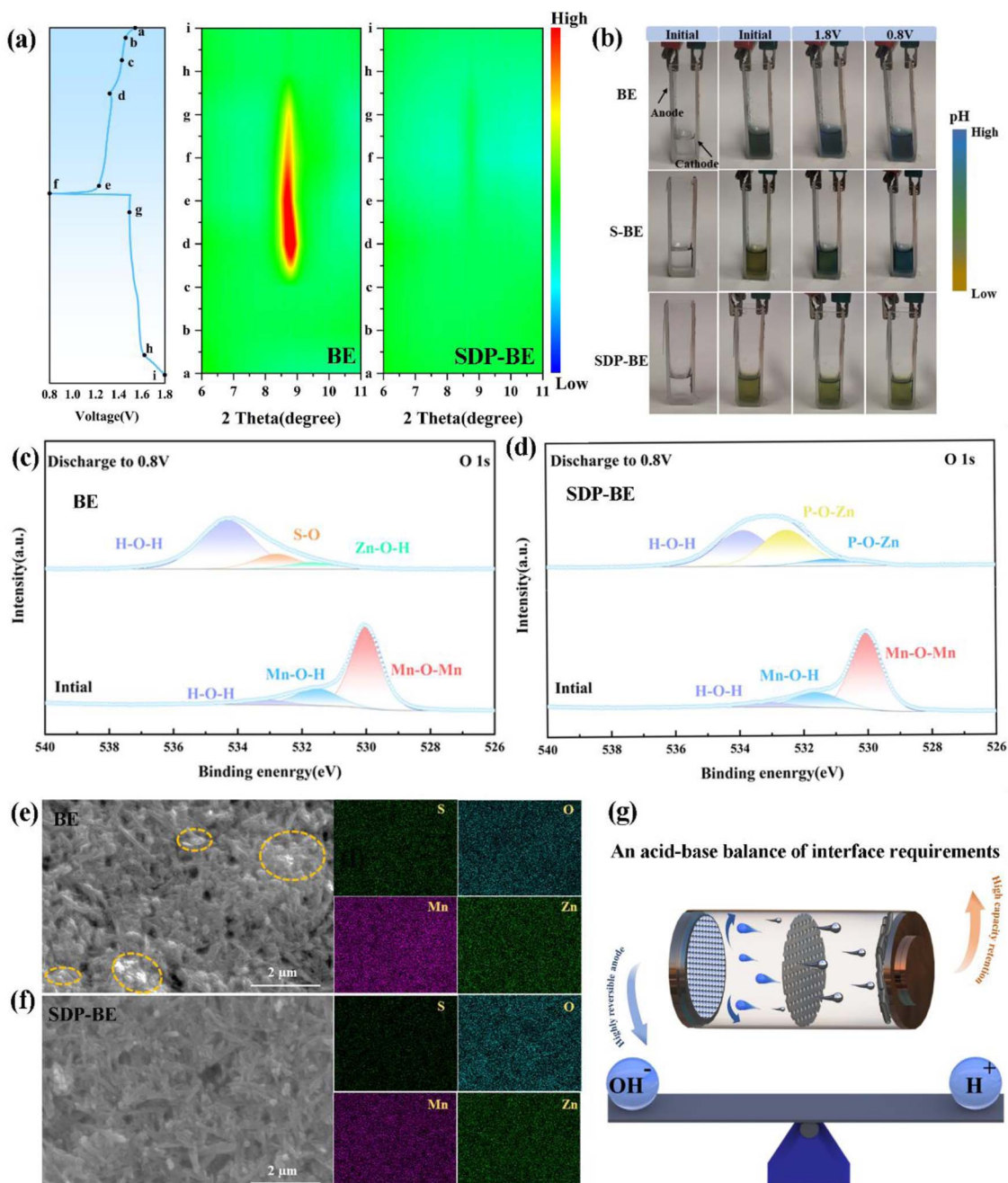


Fig. 7 (a) The galvanostatic charge/discharge curves and *ex situ* XRD patterns of the α -MnO₂ electrode during the initial first cycles, including GCD curves, XRD patterns of BE and SDP-BE sample. (b) Digital images depicting the transparent Zn||MnO₂ full cell in different solutions at various stages of full charge/discharge after activation. (c) XPS spectra of pristine MnO₂ electrode and the electrode discharged to 0.8 V without SDP additive. (d) XPS spectra of pristine MnO₂ electrode and electrode discharged to 0.8 V with SDP additive. (e) SEM image and corresponding EDS elemental mappings of MnO₂ electrode without SDP additive at 1.5C. (f) SEM image and corresponding EDS elemental mappings of MnO₂ electrode with SDP additive at 1.5C. (g) Schematic diagram of a full cell requiring acid-base balance.

maintains 68.7% capacity over 500 cycles (Fig. 6e), as further supported by the corresponding voltage profiles (Fig. 6f, and g). This pattern persists even at a higher rate of 2C (Fig. S18),[†] underscoring the instability and irreversible properties of manganese-based cathodes in BE electrolyte. The rapid capacity decay in the BE solution is primarily attributed to the abundant OH^- produced by the manganese dissolution reaction, which elevates the local pH and promotes swift formation of ZHS at the cathode interface. The poor electrical and ionic conductivity of ZHS significantly hinders charge transfer. Particularly, Mn^{2+} generated during discharge diffuses irreversibly into the electrolyte, driven by ionic concentration gradients, and fails to return to the cathode surface during subsequent charging,^{48,49} exacerbating capacity decay (Fig. 6i).

To investigate the rapid capacity decline in the $\text{BE}||\text{MnO}_2$ system, *ex situ* XRD was employed to analyze MnO_2 at different stages of the charging and discharging process. As shown in Fig. 7a, a pronounced increase in the diffraction peak at 8.5° occurs as the discharge progresses, corresponding to the formation of ZHS (PDF:44-0673).⁴⁰ Additionally, the pH stability of the BE electrolyte during the charge-discharge cycles is problematic, as illustrated by a transparent electrolytic Zn-Mn cell (Fig. 7b). The initial color of the electrolyte is deep green, which changes to blue after charging and discharging process. To minimize the starting pH error with SDP, 0.05 M H_2SO_4 (S-BE) is added, and the results remain the same. In contrast, the SDP-BE electrolyte in the transparent cell maintains a stable pH throughout the cycling, attributed to the dynamic and reversible neutralization of OH^- and H^+ by SDP.

XPS was conducted to detect changes in the chemical state of $\sigma\text{-MnO}_2$. As depicted in Fig. 7c, the O 1s spectra identify peaks at 529.98, 531.55, and 533.12 eV, corresponding to Mn-O-Mn, Mn-O-H, and H-O-H bonds in pristine MnO_2 nanosheets. After the 1st discharge, new peaks at 531.60, 532.40, and 533.70 eV appear, indicative of Zn-O-H, S-O, and H-O-H bonds of ZHS.⁵⁰⁻⁵² For the SDP-BE, peaks corresponding to P-O-Zn in $\text{Zn}(\text{H}_2\text{PO}_4)_2/\text{ZnHPO}_4$ (531.12 eV), $\text{Zn}_3(\text{PO}_4)_2$ (532.51 eV), and crystal water (533.86 eV) are identified (Fig. 7d).⁵³⁻⁵⁵ Substantial corrosion product accumulation is observed on the blank sample after one cycle (Fig. 7e), with the situation worsening after three cycles (Fig. S20).[†] In stark contrast, the SDP-BE surface exhibits none of these detrimental effects (Fig. 7f). These results further demonstrate the accumulation of irreversible ZHS on the cathode surface of the BE sample during the discharge process, exacerbating as the cycles continue. It is well known that maintaining the pH of the electrolyte at a weakly acidic level facilitates the maintenance of the charge storage mechanism based on the $\text{Zn}^{2+}/\text{H}^+$ intercalation, which is essential for reversible and stable battery operation. Therefore, a stable acid-base environment is essential for promoting efficient battery performance, as indicated by the ability of SDP to maintain such a balance (Fig. 7g).

3 Conclusion

This study adopts the approach of seeking common ground while reserving differences and emphasizing the balance of

cathode and anode interfacial requirements, leading to significantly improved cycling stability in Zn-manganese batteries. Besides, we have carried out systematic experiments and theoretical calculations to reveal how the self-regulatory mechanism balances the difference in cathode and anode interfacial demands, and the excellent electrochemical performances obtained proved to be effective in enhancing the cycling stability of Zn-manganese batteries. This enhancement is primarily attributed to the addition of SDP, which forms a ZnPO interfacial layer *in situ* on the Zn anode. This layer is uniformly distributed across the Zn surface, creating a homogeneous electric field and Zn ion flow that facilitates uniform Zn plating and stripping. Crucially, SDP actively captures the abundant OH^- ions produced by the manganese dissolution reaction, thereby preventing the formation of ZHS and promoting the reversible deposition/dissolution of $\text{Mn}^{2+}/\text{MnO}_2$. Thanks to these advantages, $\text{Zn}||\text{Zn}$ symmetric cells have demonstrated stable operation for over 3000 hours at 1 mA cm^{-2} , 1 mA h cm^{-2} . The $\text{Zn}||\text{Cu}$ cell exhibits high reversibility after 1000 cycles, with an average CE of 99.76%, and the assembled $\text{Zn}||\text{MnO}_2$ full cell delivers excellent cycling stability and multiplicity performance. This self-regulatory strategy represents a novel and effective method for homogenizing Zn^{2+} flux and enhancing the plating/stripping reversibility, marking a significant advancement in the development of practical, highly reversible aqueous Zn ion batteries. The implications of this work are profound for the future of ZMABs, providing a foundation for their practical application in energy storage systems.

Data availability

The data that supporting the findings of this study are available within the article and its ESI,[†] or from the corresponding author on reasonable request.

Author contributions

Q. C., X. Z., Y. Z., and B. X. directed the project. Y. H. performed the main experimental works. F. W., L. Y., and L. L. participate in some of experimental works. Q. Y., C. Z., and J. H. provided some constructive suggestions for the experiment. All the authors discussed the experimental results.

Conflicts of interest

The authors declare no conflict of interest.

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