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# A cyanide-free synthesis of nitriles exploiting flow chemistry†

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## Introduction

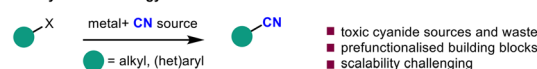
Nitriles are versatile structural motifs and ubiquitous in the pharmaceutical industry. Replacing a carbonyl group with a nitrile group in a drug molecule can lead to an improved absorption, distribution, metabolism, and excretion (ADME) profile making them a key asset in early-stage drug development.<sup>1</sup> Nitriles are also convenient handles in API intermediates as they can be readily converted to other functional groups such as carboxylic acids, ketones, amines, amides, esters, and aldehydes.<sup>2</sup> Typically, nitriles are synthesised from an alkyl or aryl halide and a metal cyanide (*e.g.*, Sandmeyer cyanation,<sup>3</sup> Rosenmund-von Braun reaction,<sup>4</sup> and Kolbe nitrile synthesis) (Scheme 1, top)<sup>5</sup> or alternatively *via* the hydrocyanation of alkenes or ammoxidation reactions.<sup>6–8</sup> However, synthesising nitriles in this way can present challenges on a manufacturing scale due to the use and associated release of highly toxic cyanide waste products.

Various approaches have been taken to develop methodologies which circumvent this issue, including the use of masked nitrile transfer reagents,<sup>9,15</sup> biocatalysis<sup>10,11</sup> and continuous flow chemistry.<sup>12–15</sup> To date, none have been as attractive and robust as the van Leusen reaction, which was first reported in 1977, and is frequently used in the total synthesis of medicinal compounds.<sup>16–19</sup> The reaction relies on ketones reacting with TosMIC

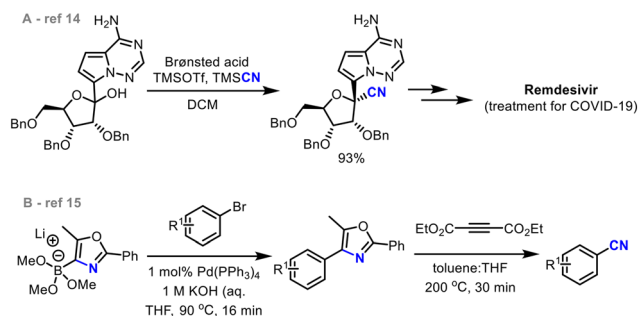
(*p*-tosylmethyl isocyanide),<sup>20</sup> a nitrile transfer reagent, which prevents the inadvertent release of cyanide side products *via* a mechanistic sequence involving ring formation and subsequent ring-opening. To the best of our knowledge, no broad-scope optimisation work has been reported on the reaction since its first publication almost 50 years ago. As the van Leusen reaction is a safe way to synthesise nitriles, we aimed to improve the efficiency and increase the

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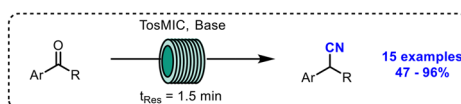
### General cyanation strategy:



### Continuous flow cyanations:



### This work:



**Scheme 1** Overview of different batch and flow-based cyanation processes. A: A large-scale continuous flow cyanation process towards Remdesivir. B: A cyanide-free cyanation in batch mode using an oxazole-based masked nitrile source.

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understanding of the reported conditions by transferring the reaction into a continuous flow process.

Over the past two decades, continuous flow technology has been gaining momentum as a manufacturing tool of the future. There are several advantages associated with performing chemical reactions in continuous flow mode, including better heat and mass transfer, improved reproducibility, and better scalability.<sup>21</sup> This technology platform is particularly attractive to industry as it allows for the synthesis of compounds 'on tap' in a fast, safe, and efficient manner.<sup>22</sup> A number of recent literature reports utilise flow technology for cyanation reactions, including in the derivatisation of amines.<sup>12,13</sup> In 2020, Vieira *et al.* reported a large-scale continuous flow cyanation process towards Remdesivir, an antiviral drug used for the treatment of COVID-19 (Scheme 1A).<sup>14</sup> A mechanistically insightful report by Sharma *et al.* detailed a cyanide-free cyanation for the derivatisation of  $sp^2$  and  $sp$  carbons *via* an oxazole-based masked nitrile source (Scheme 1B).<sup>15</sup> However, a cyanide-free continuous flow synthesis of nitriles *via* the van Leusen reaction is unreported in the literature despite its significant advantages.

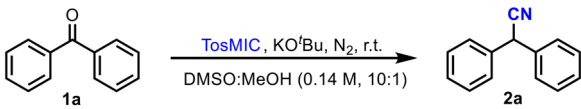
## Results & discussion

### Initial exploration in batch mode

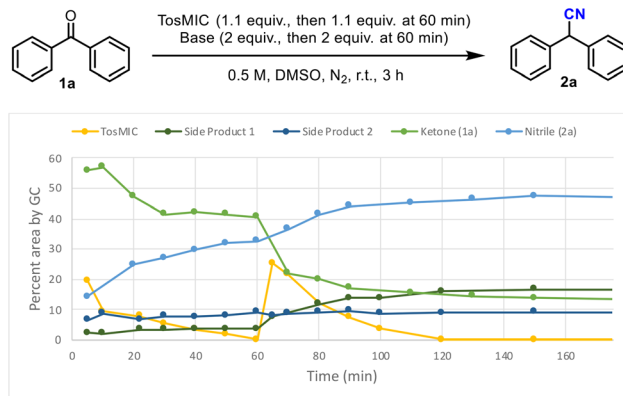
Initial exploratory work on the reaction was carried out using traditional batch methods. Employing benzophenone as the model substrate and van Leusen's reported conditions as a baseline reaction, the following parameters were screened: reaction time, temperature, and reagent addition. The results of this screen are detailed in Table 1.

Firstly, conditions similar to those reported by van Leusen were replicated on a smaller scale (1 mmol) and it was found that a shorter reaction time of 2 h gave 63% conversion to the nitrile product **2a** (Table 1, entry 1) compared with a 69% yield reported by van Leusen for the same reaction after 17 h. Additional portions of TosMIC (1.3 equiv.) and  $KO^tBu$  (2 equiv.) were added after 1 h which gave a significantly improved conversion of 91% after 4 h (Table 1, entry 2).

**Table 1** Batch studies for the formation of nitrile **2a**

				
Entry	TosMIC (equiv.)	$KO^tBu$ (equiv.)	Reaction time (h)	$^1H$ -NMR yield <b>2a</b> <sup>a</sup>
1	1.3	3.0	2	63%
2	1.3 + 1.0 <sup>b</sup>	1.0 + 2.0 <sup>b</sup>	4	91%
3	1.3 + 1.0 <sup>b</sup>	1.0 + 2.0 <sup>b</sup>	3	63%
4 <sup>c</sup>	1.1 + 1.0 <sup>b</sup>	1.0 + 2.0 <sup>b</sup>	4	93%

<sup>a</sup> Using 1,3,5-trimethoxybenzene as internal standard. <sup>b</sup> Addition after 60 min. <sup>c</sup> Gradient used: r.t. for 1 h, then 30 °C for 30 min, then 50 °C for 30 min, then 70 °C for 30 min, then 90 °C for 30 min.



**Scheme 2** Reaction monitoring *via* GC analysis.

Gradually increasing the reaction temperature by 20 °C every 30 min did not show any improvement on the reaction conversion (Table 1, entry 3). The most efficient conditions for the batch process are shown in entry 4 which give high conversion whilst limiting the excess of TosMIC reagent used. To understand the positive effect of adding further aliquots of TosMIC and base, a kinetic study was carried out in which the amount of each component was monitored by GC analysis over a period of 3 h (Scheme 2).

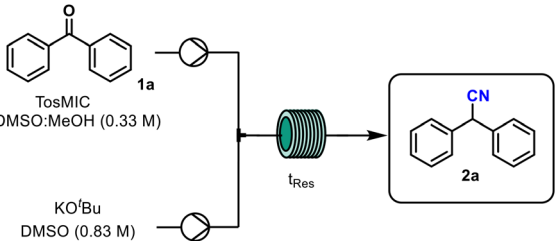
The rate of nitrile formation was initially high but then levelled off after 50 min. There was no TosMIC left in the reaction after 60 minutes despite an excess of 1.1 equiv. being used. A second addition of TosMIC and  $KO^tBu$  at this point led to an increased amount of nitrile product **2a** before leveling off at 90 min. Two new peaks were observed by GC analysis (side products 1 & 2 (Scheme 2)), possibly resulting from a degradation pathway, or a competing pathway involving TosMIC. At this stage it was hoped that a continuous flow setup would enable a quicker reaction due to better mass transfer. Additionally, with the knowledge of competing reactant decomposition in batch mode, we anticipated that spatiotemporal processing in flow mode might be advantageous as the propagating reaction mixture is separated from the feed streams containing base and TosMIC.

### Transfer to continuous flow

Initial efforts in transferring the batch-based van Leusen reaction into continuous flow continued with the use of  $KO^tBu$  as the base. Table 2 details the results of optimising the reaction with a focus on investigating the stoichiometry of TosMIC as well as the residence time when using either normal PFA coils (perfluoroalkoxy, 10 mL volume) or modified coils containing static mixing elements (PFA, 22.4 mL, see ESI† for details).

Variation of the residence time indicated that 20 min was preferable to shorter and longer residence times (entries 1–3, Table 2). Following this, the amount of TosMIC was varied from 1.2 equivalents (entries 4 and 5),

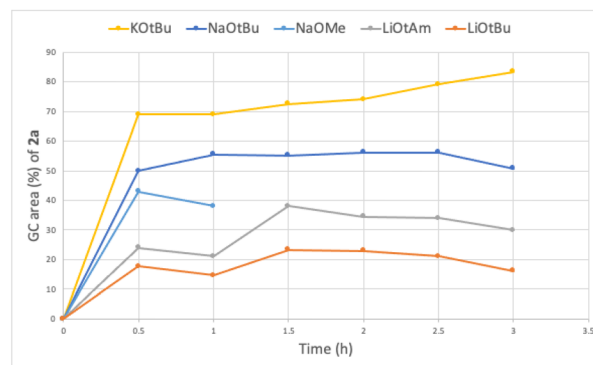
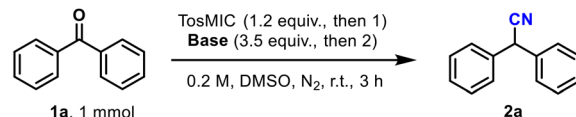


**Table 2** Initial continuous flow optimisation study using KO<sup>t</sup>Bu


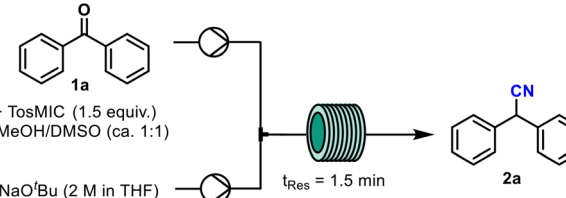
Entry	TosMIC (equiv.)	Flow rate (mL min <sup>-1</sup> )	<i>t</i> <sub>Res</sub> (min)	<sup>1</sup> H-NMR yield 2a <sup>a</sup>
1 <sup>b</sup>	1.2	0.5	15	21
2 <sup>b</sup>	1.2	0.5	20	31
3 <sup>b</sup>	1.2	0.5	40	23
4 <sup>b</sup>	1.4	0.5	20	12
5 <sup>b</sup>	1.05	0.5	20	19
6 <sup>b,d</sup>	1.2	0.5	20	18
7 <sup>c</sup>	1.2	0.56	20	33
8 <sup>c</sup>	1.2	1.12	20	46
9 <sup>c,e</sup>	1.2	1.12	20	52
10 <sup>c,e</sup>	1.2	1.68	20	50

Reactions performed at 1 mmol scale. <sup>a</sup> Determined by <sup>1</sup>H-NMR, using 1,3,5-trimethoxybenzene as an internal standard. <sup>b</sup> Standard PFA coil (10 mL). <sup>c</sup> Static mixer coil (22.4 mL). <sup>d</sup> Reaction performed at 50 °C. <sup>e</sup> Overall concentration 0.37 M.

however, no improvement in reaction conversion was observed. Increasing the reaction temperature to 50 °C resulted in a lower reaction conversion, similar to what was observed in batch mode (entry 6). To study the effect of mixing on the reaction, the initially used standard 10 mL PFA coil was replaced with a bespoke static mixer coil (see ESI† for images). Although the diameter of this static mixer coil is wider, increased mixing is typically achieved *via* the screw-like internal structure. First, a 20 min residence time (0.56 mL min<sup>-1</sup> flow rate) in the static mixer coil caused only a negligible improvement in conversion to 33% (entry 7). However, increasing the flow rate while maintaining a 20 min residence time caused the most significant increase in reaction conversion to 46% (entry 8). When this was coupled with an increase of the reaction concentration to 0.37 M (from 0.27 M) further improvement to 52% was noted (entry 9). Increasing the flow rate further and therefore reducing the residence time to 15 min resulted in a slight decrease in the reaction conversion (entry 10). From this study it was clear that mixing is a key parameter for this reaction, however, due to the poor solubility of KO<sup>t</sup>Bu in DMSO, the concentration of the reaction mixture could not be increased and thus further improvements in product yield were not possible. Several other mixing strategies were tried (see ESI† for details), but none offered an improvement on the best results detailed above (entry 9). Given the low productivity of these optimised conditions and the limitations in scaling this initial flow process, several other metal alkoxide bases were tried in the reaction (Fig. 1).

**Fig. 1** Evaluation of different alkoxide bases in batch.

This comparative study identified NaOMe as well as NaO<sup>t</sup>Bu as promising alternatives for this reaction. The reaction with NaOMe was stopped after just 1 h as previous experiments revealed that the GC % area of the nitrile product is highest at 0.5 h despite a second addition of reagents at 1 h. As NaOMe (commercial solution in MeOH, 25% w/v) is readily available at low cost, and has the best atom economy, the reaction was initially studied in continuous flow mode with this base. The optimised conditions however, led to low yields and a very poor substrate scope (see ESI† for details). Therefore, efforts turned to using commercially available solutions of NaO<sup>t</sup>Bu (2 M in THF) and the following optimisation employed design of experiment (DOE) strategies (Table 3).

**Table 3** Results from DOE optimisation study with NaO<sup>t</sup>Bu (2 M in THF)


Entry	TosMIC (equiv.)	NaO <sup>t</sup> Bu (equiv.)	<sup>1</sup> H-NMR yield <sup>a</sup>
1	1.0	2.0	37
2	2.5	3.5	56
3	3.0	4.0	61
4	3.5	4.0	61
5	1.75	5.0	62
6	2.0	6.0	65
7	3.25	5.0	66
8	2.5	6.5	72
9	2.0	4.0	72
10	2.5	5.0	73
11	3.0	6.0	75

<sup>a</sup> Determined by <sup>1</sup>H-NMR using 1,3,5-trimethoxybenzene as internal standard. Full DOE results available in ESI†.



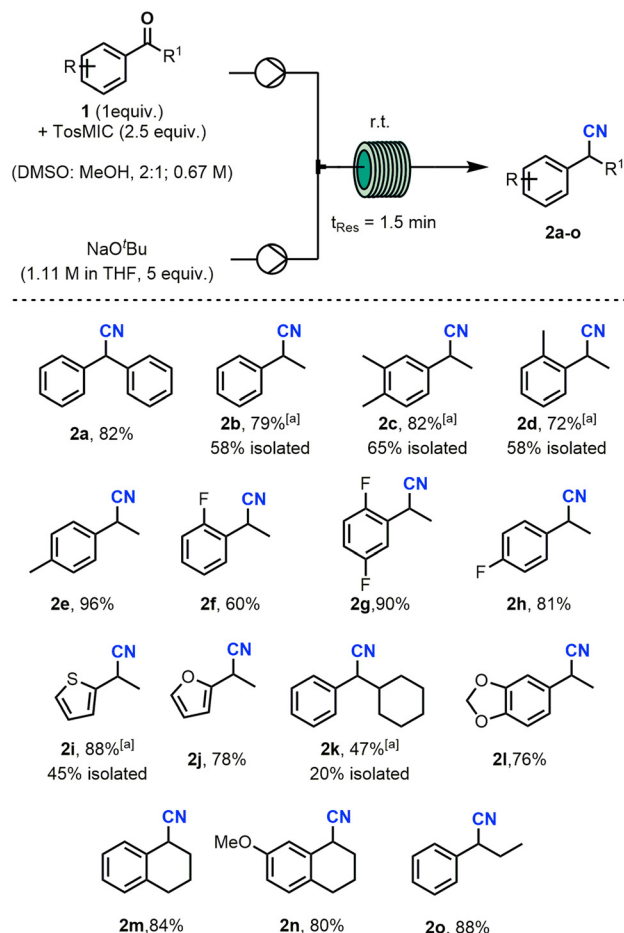


Fig. 2 Optimised continuous flow setup and exploration of substrate scope. A list of unsuccessful substrates are included in the ESI.†  
<sup>[a]</sup>Determined by <sup>1</sup>H-NMR using 1,3,5-trimethoxybenzene as an internal standard. All nitriles were collected under steady state conditions.

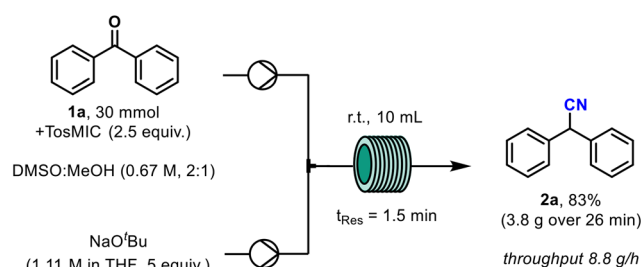
Two DOE studies (central composite design) were carried out. The first with lower limit 1, upper limit 3 equiv. of TosMIC and lower limit 2, upper limit 6 equiv. of NaO<sup>t</sup>Bu (entries 1–6). A consecutive DOE study followed with more refined limits: lower limit 2, upper limit 3 equiv. of TosMIC and lower limit 4, upper limit 6 equiv. of NaO<sup>t</sup>Bu (entries 7–11). As shown in Table 3, the highest yielding results were found when using a 1:2 ratio of TosMIC:NaO<sup>t</sup>Bu (entries 9–11). The stoichiometry from entry 10 was used for further optimisation studies, however, the stoichiometry detailed in entry 9 would be more appropriate for an industrial-scale process due to the potential cost savings of using less reagents in the face of a slightly reduced yield (1%). Further optimisation was carried out on the residence time, solvent, and amount of MeOH used in the reaction (see ESI† for results). Fig. 2 details the optimised conditions for the reaction along with the substrate scope that was explored. For this study the reaction output was collected under steady state conditions. A range of acetophenones were first subjected to the optimised conditions. Both electron-donating and electron-withdrawing

groups on the aryl ring were well tolerated, with compound **2e** being synthesised in 96% yield. Compound **2f** which has a fluorine in the 2-position of the ring was the lowest yielding of this study but still resulted in 60% yield. The phenyl group was replaced with heteroaromatic systems including a thiophene and furan ring which gave 88% and 78% yield respectively (**2i**, **2j**). The cyclohexyl phenyl ketone was relatively low yielding (47%) compared with the other substrates (**2k**). A piperonyl system was well tolerated in the reaction and gave 76% yield of product. Lastly, selected  $\alpha$ -tetralone substrates gave the corresponding nitriles in excellent yields (**2m**, **2n**) as did propiophenone (**2o**).

When the model benzophenone reaction was then scaled to 30 mmol the yield of the reaction was reproduced from the earlier small-scale tests producing 3.8 g of the desired nitrile within 26 minutes, which is equivalent to a throughput of 8.8 g h<sup>-1</sup> (Scheme 3).

In relation to the competing reactivity of TosMIC, under continuous flow conditions only one distinct side product was observed and subsequently isolated. Based on NMR analysis this material was initially thought to be 4-tosylimidazole (**5**) which is believed to result from dimerisation of TosMIC followed by loss of the tosyl-CH<sub>2</sub> group under basic conditions.<sup>23,24</sup> However, an older report by Bull suggests that by using a ratio of 1:2 TosMIC:base, the formation of the dimer (**4**) can be prevented due to an absence of neutral TosMIC (**3**).<sup>25</sup> This might explain why the highest yielding reactions from the DOE study (Table 3) were found to be along an axis which represents a 1:2 ratio of TosMIC to base. As our scale-up studies generated sufficient quantities of this side-product we were able to exploit single crystal X-ray diffraction analysis which revealed the structure of this compound to be 4-tosyloxazole (**9**) instead. Earlier reports by both van Leusen<sup>26</sup> and Schöllkopf<sup>27</sup> propose a mechanistic rationale for the formation of **9**, however, its significance in the overall mechanism appears to have been overlooked due the absence of definitive structural data (Scheme 4).

In the mechanistic proposal shown below, intermediate **6** results from initial condensation between ketone and TosMIC followed by hydration of the isonitrile group (Scheme 4). This species (**6**) then abstracts a proton from MeOH and subsequently undergoes transfer of its formyl group to a deprotonated molecule of TosMIC. This leads to

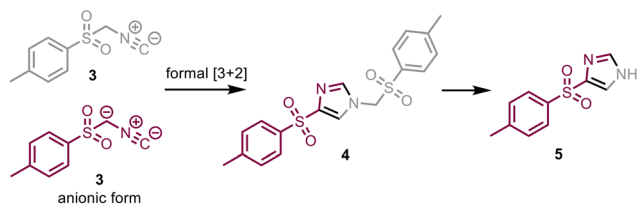


Scheme 3 Reaction scalability demonstrated on 30 mmol scale.

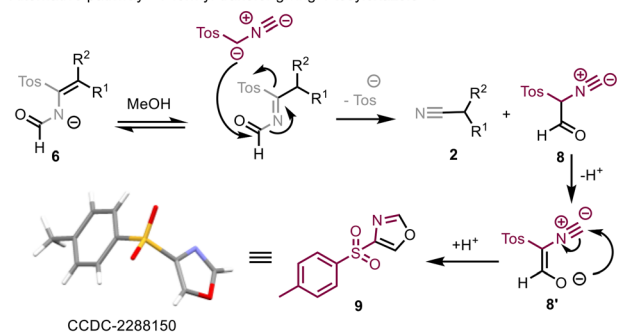




Plausible pathway for formation of **5** via dimerisation of TosMIC:



Alternative pathway via formyl-transfer giving 4-tosyloxazole **9**:



**Scheme 4** Proposed pathways for the formation of 4-tosylimidazole (**5**) and 4-tosyloxazole (**9**) from competing reaction pathways involving TosMIC. This route is secondary to that proposed by van Leusen for the formation of the nitrile product **2**.<sup>16</sup>

the formation of the desired nitrile product (**2**) as well as formyl species **8** that cyclises to give the aromatic 4-tosyloxazole **9**. Crucially, this proposal accounts for the high yields observed in the reaction despite the formation of significant amounts of 4-tosyloxazole (**9**) which forms due to additional TosMIC reagent being available. Bull<sup>25</sup> and van Leusen<sup>26</sup> suggest that minimising the amount of MeOH used in the reaction may limit the formation of **9**, however, our experiments did not corroborate this hypothesis.

## Conclusions

In conclusion, we have developed a fast and straightforward continuous flow process for the formation of aryl nitriles from ketones and TosMIC in the presence of alkoxide bases. Screening different bases ultimately identified NaO<sup>t</sup>Bu (2 M in THF) as the best choice in terms of solubility and product yield. The overall process is attractive as it does not require the handling of cyanide or any related reagents. Furthermore, the scalability of the flow method and its high throughput (8.8 g h<sup>-1</sup>) make this continuous van Leusen reaction an appealing strategy for future industrial applications. Systematic variation of the reaction parameters thereby yielded additional mechanistic insights. Importantly, the isolation and characterisation of a tosyloxazole side-product was accomplished whose formation accounts for the competitive consumption of the TosMIC reagent under the reaction conditions. This study is expected to generate renewed interest in the underutilised van Leusen nitrile synthesis and its use in accessing nitrile-containing organic building blocks *via* a safe and readily scalable process.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

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