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# Removal of toxic hexavalent chromium *via* graphene oxide nanoparticles: study of kinetics, isotherms, and thermodynamics

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In this study, graphene oxide (GO) was prepared by the Hummers' method from graphite material. The adsorption potential of GO-200 nm for the removal of Cr(vi) ions was investigated. Fourier transform infrared (FTIR) spectroscopy was used to analyze Cr(vi) before and after adsorption. The adsorption isotherm was fitted by the Langmuir model and the maximum adsorption capacity of the GO was 41.27 mg g<sup>-1</sup> at 25 °C. Thermodynamic parameters ( $\Delta G^\circ$ ), ( $\Delta H^\circ$ ), and ( $\Delta S^\circ$ ) were calculated and exhibited as +2.63 kJ mol<sup>-1</sup> K<sup>-1</sup>, +4.30 kJ mol<sup>-1</sup> K<sup>-1</sup>, and +5.56 kJ mol<sup>-1</sup> K<sup>-1</sup> at 30 mg L<sup>-1</sup> of Cr(vi) solution, respectively.

## Introduction

Heavy metal pollution is a major concern of aquatic ecosystems worldwide, even at low levels of exposure. For instance, copper, zinc, cadmium, lead, mercury, arsenic, and chromium metal ions are highly toxic to living organisms due to their persistence, bioaccumulation, non-biodegradability, and environmental stability.<sup>1</sup> Chromium is commonly found in the environment in Cr(III) and Cr(VI) oxidation states, which have quite different chemical properties. Cr(III) is chemically converted to Cr(VI) by redox reaction under certain conditions. Cr(VI) is considered a carcinogenic and mutagenic material.<sup>2</sup> Several methods have been applied to remove Cr(VI) from aqueous solutions. Among these methods, adsorption is the most promising and effective method for Cr(VI) removal due to its simplicity, cost-effectiveness, applicability for the industry and being eco-friendly.<sup>3</sup>

In this regard, various adsorbents such as biological materials, chitosan, industrial wastes, zeolites, dendrimers, biochar, imprinted materials and activated carbon have been proposed to remove hexavalent chromium Cr(VI) from the water<sup>4-7</sup> ecosystem. Recently, GO nanoparticles have been introduced as nano-adsorbents, which have drawn additional attention due to their properties such as extremely high surface area and adsorption

site, tunable morphology, and much lower intra-particle diffusion distance. These materials do not require high operation and maintenance costs.<sup>2,4,5</sup> Nanomaterials such as GO are effective in the removal of heavy metals from wastewater, and they are a viable alternative to conventional adsorbents. Among other advantages, GO has received considerable attention due to its unique chemical and physical properties such as hydrophilicity and stability in solution. The abundant oxygen groups such as -OH, -COOH and -C=O distributed on their surfaces imparted during the oxidation of graphite. GO nanoparticles are successfully prepared in our chemical lab<sup>8</sup> for using as an adsorbent for the removal of hexavalent chromium Cr(VI) from an aqueous solution.

In this work, the adsorptive removal of Cr(VI) metal ions using GO as an adsorbent under different experimental conditions was elucidated. Scheme 1 exhibits the proposed mechanism of reduction of hexavalent Cr to trivalent in acidic conditions. The mechanism for the removal of Cr(VI) using GO includes adsorption through electrostatic attractions,<sup>9</sup> reduction of Cr(VI) to Cr(III),<sup>10</sup> and a probable coordination between chromium ions and ligands.

## Materials and methods

### Preparation of graphite oxide

Graphite oxide was produced from natural graphite using the modified Hummers' method.<sup>8,11-13</sup> In Scheme 2, 1.0 g graphite was ground with 50.0 g of NaCl for a few minutes to exfoliate the graphite particles and reduce their dimensions. The ground graphite was added to warm water and collected using filter paper by suction filtration. The dried graphite was mixed with 20 mL H<sub>2</sub>SO<sub>4</sub> overnight, and the obtained solution was stirred in an ice bath for 45 min and 3 g KMnO<sub>4</sub> was slowly added as an oxidizing material. After the complete addition of the oxidizer, the mixture was stirred for 30 min at 35 °C, the temperature was

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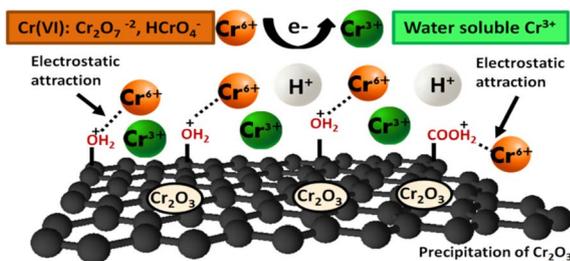
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Scheme 1 Proposed mechanism for Cr(vi) removal by GO in an acidic environment.

raised up to 50 °C for 45 min. Thereafter, 46 mL of distilled water was added gradually to the solution and the solution was kept stirring for 45 min at 98 °C. Subsequently, 140 mL distilled water and 10 mL of 3% H<sub>2</sub>O<sub>2</sub> were added to the mixture.

The collected sample was filtered and washed three times with 5% HCl and distilled water to remove any of the side products. Finally, the graphite oxide powder was obtained after drying in a vacuum at 30 °C for 24 h.

### Synthesis of GO-200 nm

After purification of graphite oxide by centrifugation, the GO-200 nm nanoparticles were prepared according to our previous protocol.<sup>8</sup> Subsequently, 1.0 mg mL<sup>-1</sup> of graphite oxide was sonicated in an ultra-sonication bath under controlled conditions (Scheme 2b).

### Batch adsorption experiments

The batch adsorption experiments were used to study the effect of pH at the range 2.0 to 7.0, mass of adsorbate (1, 5, 10, 20, 40, 60, 100 and 140 mg), time (1, 20, 40, 80, 160, and 240 min),

temperature in the range of 25–55 °C, and Cr(vi) initial concentration (30, 50, 100, 200, 300, 400 and 500 mg L<sup>-1</sup>). Further experiments were performed to characterize the adsorption kinetics, isotherms, and thermodynamics at the optimum values of pH and mass of graphene oxide. Chromium(vi) stock solution (1000 ppm) was prepared by dissolving 0.283 g of potassium dichromate (K<sub>2</sub>Cr<sub>2</sub>O<sub>7</sub>) in 100 mL distilled water. Analytical solutions were prepared from the stock solution by using a dilution factor. The adsorption experiments were performed in 25 mL flasks containing 20 mL of a series of Cr(vi) solutions. The pH of the solution was adjusted to 3.0 and 2 g L<sup>-1</sup> of graphene oxide material was added. The mixture was sonicated to homogenize the mixture.

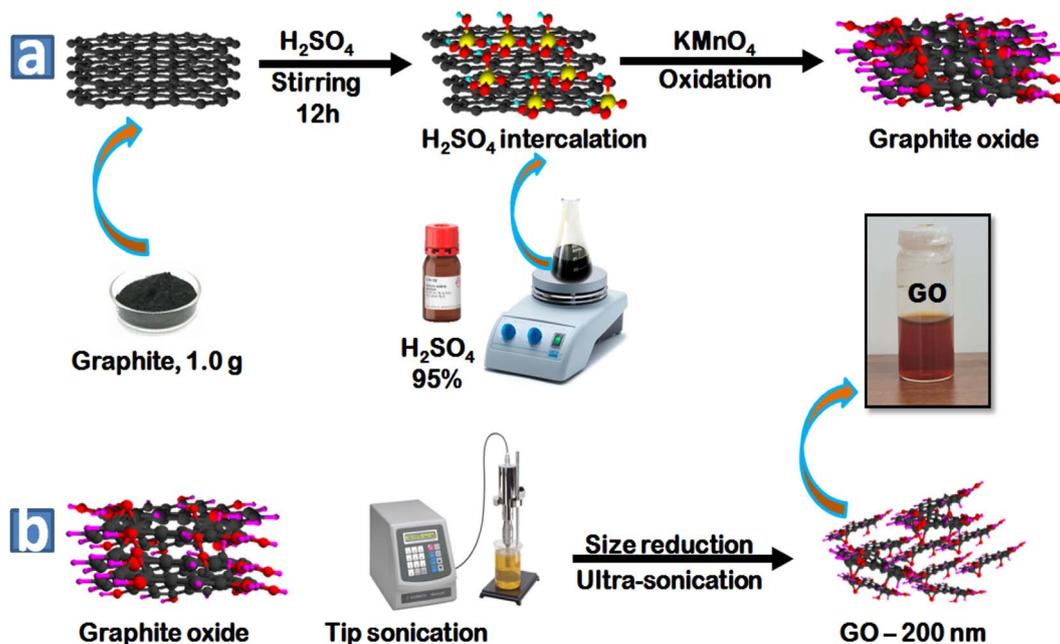
After 24 h of incubation, the mixture was filtered using a syringe filter nylon with pore size (0.45 μm) and stored at 4 °C. The residual total chromium concentration (Cr(vi) + Cr(III)) was analysed by atomic adsorption spectroscopy, while the residual Cr(vi) was analysed using a UV-visible spectrophotometer which was assessed by 1,5-diphenylcarbazide method, the absorbance of the red-violet coloured solution was obtained from the reaction after 10 min at 540 nm.<sup>14</sup> The adsorption capacity [ $q_e$  (mg g<sup>-1</sup>)] and percentage removal efficiency of Cr(vi) were calculated using eqn (1) and (2):<sup>15</sup>

$$q_e = \frac{(C_i - C_e)V}{m} \quad (1)$$

$$R = \frac{(C_i - C_e)}{C_i} \times 100\% \quad (2)$$

### Variation parameters

The kinetic study was carried out at different time intervals (1, 20, 40, 80, 160 and 240 min) in separate experiments for 50 and 100 mg L<sup>-1</sup> of Cr(vi) solution. The variation of initial Cr(vi)



Scheme 2 Oxidation of graphite (a) for the preparation of graphite oxide using Hummers' method and (b) size reduction of GO particles under controlled conditions.



concentrations (30, 50, 100, 200, 300, 400 and 500 mg L<sup>-1</sup>) and isotherm models were employed in this study.

## Results and discussion

### Scanning electron microscopy (SEM)

The lateral sizes of the GO particles were elucidated by scanning electron microscopy, as shown in Fig. 1. The as-prepared graphite oxide is presented in panel (a). The GO-200 nm with the reduced size after sonication under controlled conditions is presented in panel (b).

Panel (c) exhibits the statistical analyses of particles deduced from SEM images. According to our literature reports,<sup>8,11,12</sup> the as-prepared GO particles exhibited 450 nm lateral size distribution. The as-prepared GO particles were treated under hard sonication to increase the surface-to-volume ratio. In panel (c), the number of GO particles is approximately 250 to measure the size distribution of samples.

### FTIR spectra of GO and GO-Cr(vi) system

The characteristic peaks of pristine GO-200 nm and GO/Cr(vi) are shown in Fig. 2. As shown in panel (a), the GO revealed the main functional groups distributed on the surface and the edges of GO particles. The peak position of the hydroxyl (-OH) group appears at 3365 cm<sup>-1</sup> stretching vibration, and the carbonyl (C=O) group at 1731 cm<sup>-1</sup>. The carbon-to-carbon double bond (C=C) takes position at 1619 cm<sup>-1</sup>, this functional group represents the sp<sup>2</sup> regime of the 2D graphene layer. The epoxy (C-O) group becomes visible in the lower frequency region at 1400 cm<sup>-1</sup>.<sup>8,16</sup> The FTIR spectrum of GO-Cr(vi) nano-system was performed as shown in Fig. 2b. The GO-Cr(vi) exhibits three band positions at 715, 804 and 890 cm<sup>-1</sup>, which are assigned to Cr=O and Cr-O-Cr bonds, indicating that Cr(vi) was adsorbed on the surface of GO. Furthermore, the normalized peak intensities were reduced in high and low-frequency regions. A subtle shift in the absorption peaks was observed, which was assigned to the perturbation of energy due to the new coordination between the oxygen groups and chromium ions. These bands are usually shifted to lower or higher frequencies.<sup>17,18</sup>

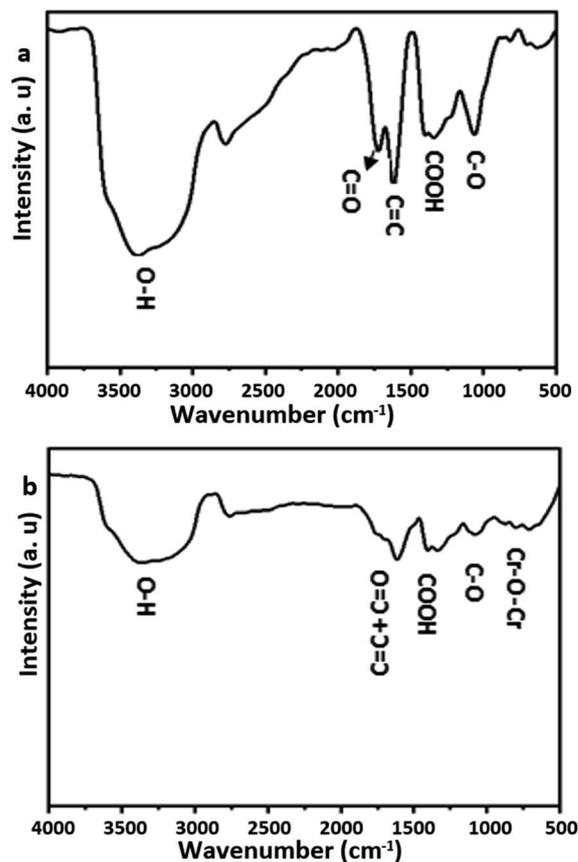


Fig. 2 FTIR spectra of (a) graphene oxide (b) graphene oxide treated Cr(vi).

### Adsorption studies: effect of pH

The pH is a key parameter controlling the Cr(vi) adsorption process. It has a significant effect on the surface charge, binding sites of the adsorbent and metal ion speciation. There are several anionic forms of Cr(vi) existing in the solution, such as CrO<sub>4</sub><sup>2-</sup>, dichromate (Cr<sub>2</sub>O<sub>7</sub><sup>2-</sup>) and hydrogen chromate (HCrO<sub>4</sub><sup>-</sup>). At 2 ≤ pH ≤ 6, it exists in two equilibrium forms of (Cr<sub>2</sub>O<sub>7</sub><sup>2-</sup>) and (HCrO<sub>4</sub><sup>-</sup>), however, chromate anion (CrO<sub>4</sub><sup>2-</sup>) predominates under alkaline conditions.<sup>15</sup> The initial

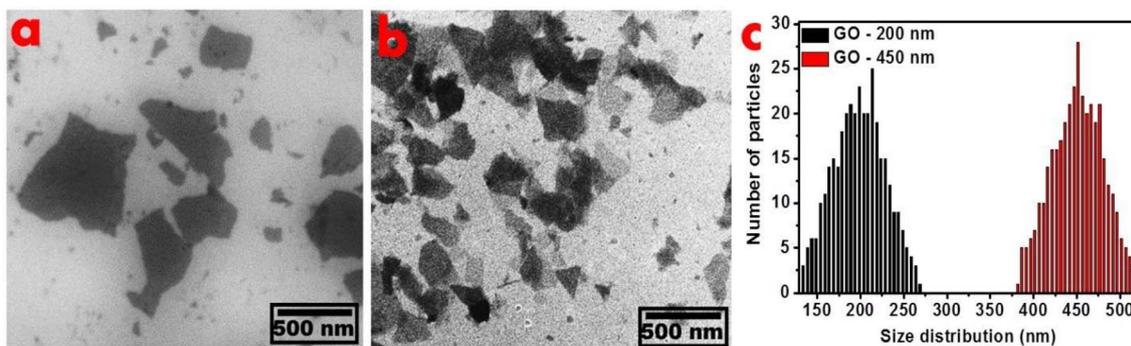


Fig. 1 SEM images of (a) GO-450 nm and (b) GO-200 nm and (c) is the average width (nm) of GO particles deduced from the SEM image, the size distribution of GO-450 is ±35 nm, GO-200 is ±20 nm.



concentration of chromium ions is  $50 \text{ mg L}^{-1}$  with 2 h of contact time and  $25 \text{ }^\circ\text{C}$ .

### Percent removal and adsorption capacity

Fig. 3 reveals the percent removal and adsorption capacity ( $q_e$ ) of Cr(vi) adsorbed onto the basal plane of GO particles as a function of pH. The result indicated that the pH between 3 to 4 has the highest percentage removal of the total chromium and Cr(vi). Cr(vi) is partially reduced to Cr(III) by the reductive surface hydroxyl groups on the surfaces of GO.<sup>10</sup> This reaction catalyzed by electrons might be caused by the electrons on the carbocyclic six-membered ring of GO.<sup>17</sup> The resulting Cr(III) is either released back into the solution at lower pH in the form of water-soluble Cr(III) species or precipitated as  $\text{Cr}_2\text{O}_3$  to achieve the performance of adsorption.<sup>10</sup>

### Kinetic studies

**Contact time.** Generally, the removal of chromium ions increases as the contact time increases until the equilibrium is reached. Once the equilibrium is reached, the adsorption process of metal ions becomes constant. At the beginning of the adsorption process, a large number of active sites are available for the adsorbate and the process proceeds very fast, however, as the active sites are filled, the adsorption proceeds slowly until the equilibrium is reached.<sup>9</sup>

Fig. 4 summarizes the effect of the contact time on the percent removal and adsorption capacity of chromium ions by GO nanoparticles. The percentage removal was increased during the first 80 min, and then it reached a plateau at equilibrium.

**Kinetic models of adsorption.** The Pseudo-first order, pseudo-second order, intra-particle diffusion and Elovich kinetic models have been investigated in this study. These models explain the mechanisms that control the adsorption processes. The following linear forms expressed the pseudo-first-order (eqn (3)),<sup>15</sup> pseudo-second-order (eqn (4)), intra-particle diffusion model (eqn (5)), and Elovich kinetic model in (eqn (6)).<sup>19</sup>

$$\log(q_e - q_t) = \log q_e - \frac{k_1 t}{2.303} \quad (3)$$

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e} \quad (4)$$

$$q_t = k_p t^{\left(\frac{1}{2}\right)} + C \quad (5)$$

$$q_t = \frac{1}{\beta} \ln(\alpha\beta) + \frac{1}{\beta} \ln(t) \quad (6)$$

where  $q_e$  and  $q_t$  are the adsorption capacities ( $\text{mg g}^{-1}$ ) at equilibrium and at a time ( $t$ ) respectively,  $k_2$  is the rate constant of second-order adsorption ( $\text{g mg}^{-1} \text{ min}^{-1}$ ),  $k_1$  is the pseudo-first-

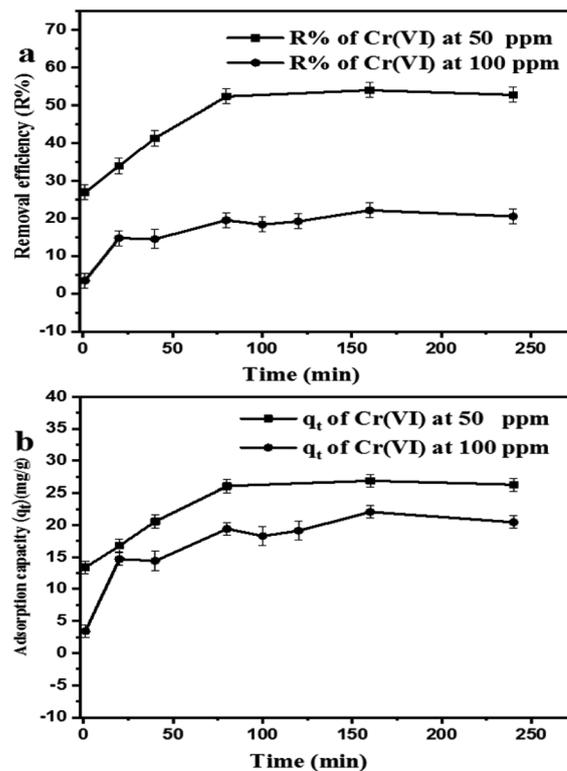


Fig. 4 Effect of the contact time on (a) percentage removal efficiency (R%) and (b) adsorption capacity ( $q_t$ ) of Cr(vi).

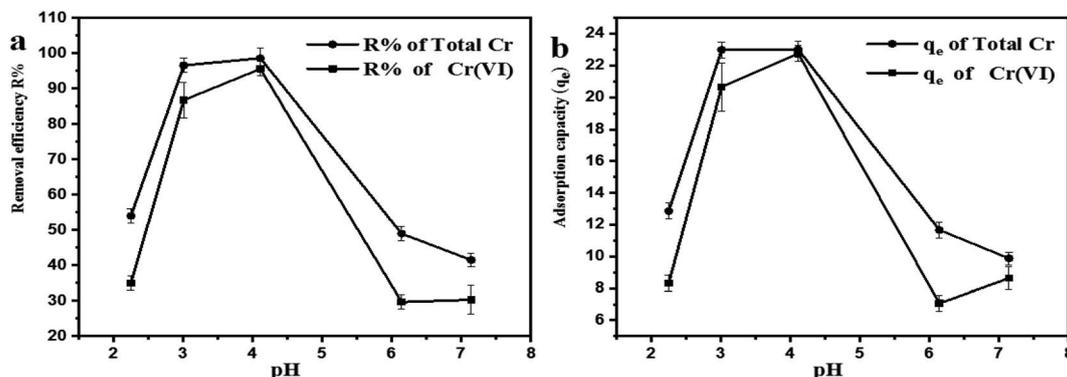


Fig. 3 Effect of adjusted pH on (a) percentage removal and (b) adsorption capacity ( $q_e$ ).



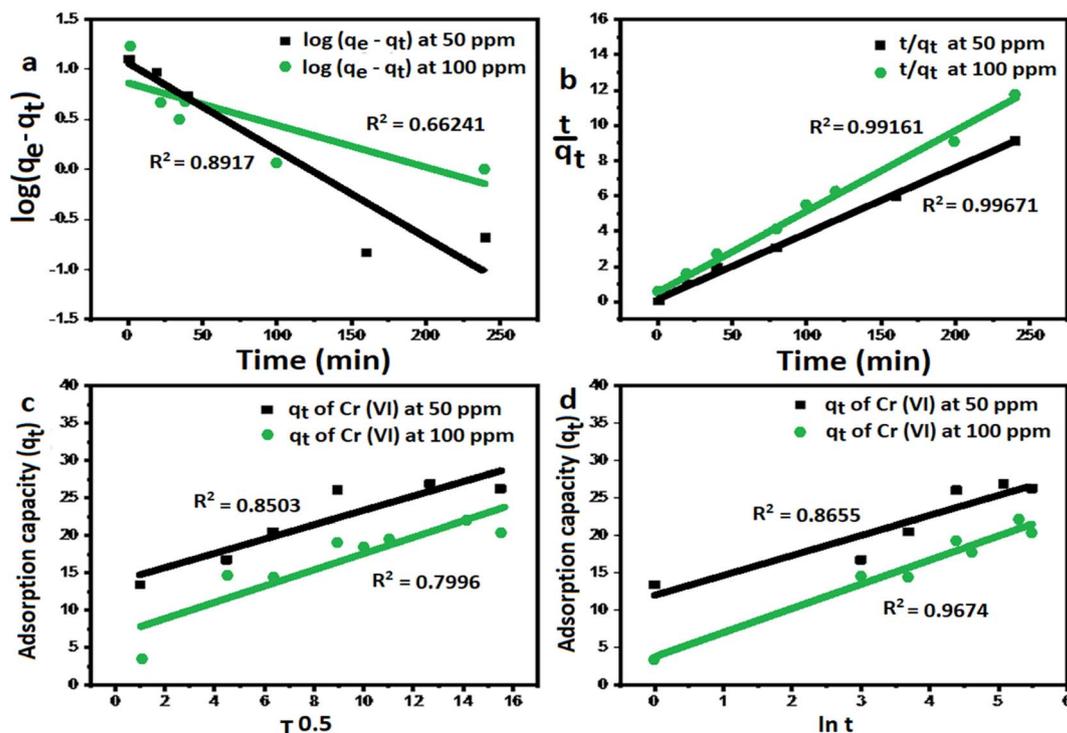


Fig. 5 The kinetic models of Cr(vi) adsorption using GO-200 nm. (a) Pseudo first order model, (b) pseudo-second order model, (c) intra-particle diffusion model, and (d) Elovich kinetic model.

order rate constant ( $\text{min}^{-1}$ ),  $k_p$  is the rate constant of intra-particle diffusion ( $\text{mg g}^{-1} \text{min}^{-1/2}$ ),  $C$  is the intercept represents the thickness of the boundary layer,  $\alpha$  is the initial adsorption rate ( $\text{mg min}^{-1}$ ),  $\beta$  is the extent of surface coverage and activated energy ( $\text{g mg}^{-1}$ ).

Fig. 5a shows the pseudo-first-order model with linear regression correlation coefficient ( $R^2$ ) and describes the kinetics of Cr(vi) adsorption onto GO nanoparticles. The results support the assumption that adsorption is chemisorption and related to valence forces through the sharing or exchange of electrons between the GO and Cr(vi).<sup>15,19</sup>

The rate constant of the pseudo-first-order kinetic was found to be decreased with increasing initial Cr(vi) concentration,<sup>17</sup>

indicating that the adsorption of Cr(vi) onto GO would be faster at a lower initial concentration.

Fig. 5b exhibits a linear relation with high correlation coefficient for 50 and 100 ppm, which reflects a very strong correlation between the parameters and a good fitting of the experimental data with pseudo second order kinetic model, this is supported by the agreement between the theoretical values and the experimental values and data are listed in Table 1.

**Adsorption isotherm models.** Among various adsorption isotherms, Langmuir, Freundlich and Temkin models were applied in this study to understand the adsorption behaviour of Cr(vi) ions by GO particles, which is observed in Fig. 6. The linear forms of Langmuir, Freundlich, and Temkin are expressed in eqn (7)–(9), respectively.

Table 1 The kinetic models with different correlation coefficients at 50, 100  $\text{mg L}^{-1}$

Conc. ( $\text{mg L}^{-1}$ )	Pseudo second-order model				Pseudo first-order model			
	$R^2$	$q_e$ (exp)	$q_e$ (cal)	$k_2$	$R^2$	$q_e$ (exp)	$q_e$ (cal)	$k_1$
50	0.9967	26.06	27.38	$4.96 \times 10^{-3}$	0.8917	26.06	11.195	0.0197
100	0.9916	19.39	21.97	$3.55 \times 10^{-3}$	0.6624	19.39	7.391	0.0098
Conc. ( $\text{mg L}^{-1}$ )	Intra-particle model			Elovich model				
	$R^2$	$k_p$	$C$	$R^2$	$\alpha$	$\beta$		
50	0.8503	0.960	13.66	0.9674	245.4	0.375		
100	0.7996	1.086	6.79	0.8655	10.19	0.308		



$$\frac{C_e}{q_e} = \frac{1}{bQ_{\max}} + \frac{C_e}{Q_{\max}} \quad (7)$$

$$\log q_e = \log k_f + \frac{1}{n} \log C_e \quad (8)$$

$$q_e = B_T \ln k_T + B_T \ln C_e \quad (9)$$

where  $C_e$  refers to the equilibrium concentration of the remaining solute in the solution ( $\text{mg L}^{-1}$ ),  $q_e$  is the amount of solute adsorbed per unit mass of the adsorbent at equilibrium ( $\text{mg g}^{-1}$ ),  $Q_{\max}$  is the amount of adsorbate per unit mass of the adsorbent at complete monolayer coverage ( $\text{mmol g}^{-1}$ ),  $b$  is a Langmuir constant. The variables ( $n$ ) and ( $k_f$ ) are Freundlich constants that are related to the adsorption intensity and adsorption capacity, respectively,  $1/n$  represents the heterogeneity factor. The  $B_T$  is the constant related to the heat of sorption ( $\text{J mol}^{-1}$ ), and  $k_T$  is the Temkin isotherm constant. Fig. 6 indicates that the adsorption of  $\text{Cr}(\text{vi})$  ions by GO is well described by Langmuir isotherm parameters that are listed in Table 2. The calculated  $Q_{\max}$  is  $41.27 \text{ mg g}^{-1}$  for the adsorption by GO.

The nature of the adsorption was addressed depending on the values of the dimensionless constant of Langmuir isotherm the dimensional constant known as the equilibrium parameter,  $R_L$  of Langmuir isotherm, and its value calculated from eqn (10):

$$R_L = \frac{1}{1 + bC_i} \quad (10)$$

where  $b$  is a Langmuir constant and  $C_i$  is the initial concentration. The value of  $R_L$  indicates the nature of the adsorption process.  $R_L > 1$ ,  $R_L = 1$ ,  $0 < R_L < 1$ , and  $R_L = 0$  for unfavourable adsorption, linear adsorption, favorable adsorption, and irreversible adsorption, respectively.<sup>15</sup> From this data, the parameter that show the  $R_L$  values for the removal of  $\text{Cr}(\text{vi})$  ranged from 0.197 to 0.620 for GO. These values indicate favorable adsorption process for the GO. From the Freundlich isotherm model, the calculated value for  $(1/n)$  of adsorption  $\text{Cr}(\text{vi})$  is less than 1, this refers to a heterogamous surface with minimum interactions between the adsorbent ions.

**Thermodynamic parameter for adsorption process.** The Gibbs free energy ( $\Delta G^\circ$ ), entropy ( $\Delta S^\circ$ ), and the enthalpy process

Table 2 Isotherm models parameters for adsorption of  $\text{Cr}(\text{vi})$  by GO

Isotherm models	$R^2$	Parameters
Langmuir	0.9217	$Q_{\max} = 41.27 \text{ mg g}^{-1}$ $b = 0.02035 \text{ mg}^{-1}$
Temkin	0.8970	$B_T = 8.226$ $k_T = 0.254$
Freundlich	0.9200	$\frac{1}{n} = 0.449$ $k_f = 3.27$

( $\Delta H^\circ$ ) were calculated using the following van't Hoff eqn (11)–(13):

$$k_c = \frac{q_e}{C_e} \quad (11)$$

$$\Delta G^\circ = -RT \ln k_c \quad (12)$$

$$\ln k_c = \frac{\Delta S^\circ}{R} - \frac{\Delta H^\circ}{RT} \quad (13)$$

where  $k_c$  is the equilibrium constant calculated as the surface and solution metal distribution. Adsorption enthalpy and entropy were calculated from eqn (11) and the plot curve of  $\ln k_c$  versus  $1/T$ , the values are presented in Table 3. The positive value of adsorption enthalpy shows that the process is endothermic, and its magnitude implies that the adsorption of  $\text{Cr}(\text{vi})$  on GO is chemical adsorption.<sup>4,16</sup> An increase in the equilibrium constant ( $k_c$ ) with the increase in the temperature also indicates an increase in the amount of the adsorbent metal ions.<sup>20</sup>

Furthermore, the positive value of the adsorption entropy suggested increased randomness at the adsorbent-solution interface.<sup>4,19</sup> The  $\Delta G^\circ$  can be calculated from eqn (14):

$$\Delta G^\circ = \Delta H^\circ - T\Delta S^\circ \quad (14)$$

which means the reaction is non-spontaneous at optimized conditions.

Table 3 Thermodynamic parameters for the adsorption of  $\text{Cr}(\text{vi})$  onto GO-200 nm

$T$ (K)	$1/T$	$k_c$	$\ln k_c$	$\Delta G^\circ$	$\Delta H^\circ$	$\Delta S^\circ$
298	$3.355 \times 10^{-3}$	0.345	-1.062	2.631	4.30	5.56
318	$3.144 \times 10^{-3}$	0.377	-0.973	2.572		
328	$3.048 \times 10^{-3}$	0.407	-0.898	2.448		

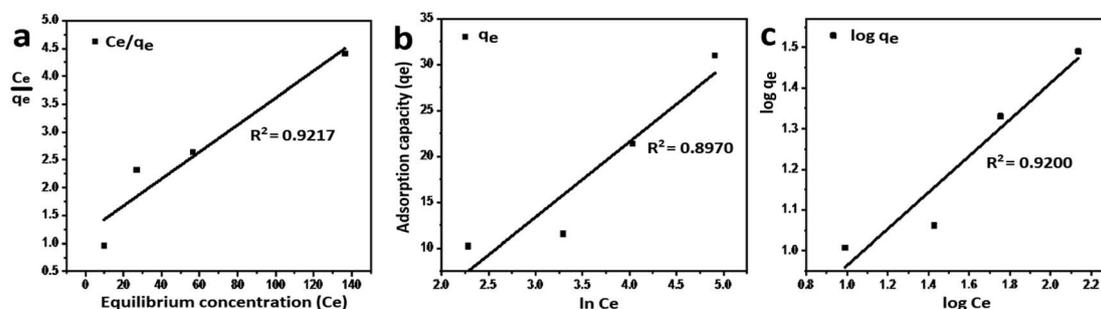


Fig. 6 Equilibrium studies of  $\text{Cr}(\text{vi})$  adsorption by GO, (a) Langmuir isotherm model, (b) Temkin isotherm model, and (c) Freundlich isotherm model.



## Conclusions

In this study, the preparation of GO-200 nm for the removal of Cr(VI) under different experimental conditions was elucidated. The FTIR spectroscopy showed oxidation of graphite to GO and confirmed the formation of GO particles and GO/Cr(VI) interaction. Furthermore, the experimental results showed that the pseudo-second-order model and Langmuir isotherm model fitted well with the adsorption data. The thermodynamic parameter ( $\Delta G^\circ$ ) indicated that the adsorption process is nonspontaneous.

## Data availability

We confirm that some of findings in this paper are available as part of master thesis of the first author Mrs Zohor Khdoor at Hebron University, Faculty of Graduate Studies, Chemistry Department. Here is the link: <https://dspace.hebron.edu/jspui/bitstream/123456789/921>.

## Conflicts of interest

The authors declare that no competing interests.

## Acknowledgements

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## References

- 1 K. Yang, *et al.*, A novel method for removing heavy metals from composting system: the combination of functional bacteria and adsorbent materials, *Bioresour. Technol.*, 2019, **293**, 122095.
- 2 J. Bayuo, K. B. Pelig-Ba and M. A. Abukari, Adsorptive removal of chromium(VI) from aqueous solution unto groundnut shell, *Appl. Water Sci.*, 2019, **9**, 107.
- 3 M. N. Siddiqui, *et al.*, Using functionalized asphaltene as effective adsorbents for the removal of chromium and lead metal ions from aqueous solution, *Environ. Res.*, 2022, **204**, 104.
- 4 S. Li, *et al.*, Magnetic Ion-Imprinted Materials for Selective Adsorption of Cr(VI): Adsorption Behavior and Mechanism Study, *Molecules*, 2024, **29**, 1952.
- 5 W. Y. Zhang, *et al.*, A recoverable magnetic surface ion-imprinted polymer based on graphene oxide for fast and selective adsorption of Ni(II) from aqueous solution: experimental and DFT calculations, *New J. Chem.*, 2022, **47**, 1197–1208.
- 6 C. Jung, *et al.*, Hexavalent chromium removal by various adsorbents: powdered activated carbon, chitosan, and single/multi-walled carbon nanotubes, *Sep. Purif. Technol.*, 2013, **106**, 63–71.
- 7 A. Awasthi, P. Jadhao and K. Kumari, Clay nano-adsorbent: structures, applications and mechanism for water treatment, *SN Appl. Sci.*, 2019, **1**, 1076.
- 8 M. Atawneh, *et al.*, The cross-talk between lateral sheet dimensions of pristine graphene oxide nanoparticles and Ni<sup>2+</sup> adsorption, *RSC Adv.*, 2021, **11**, 11388–11397.
- 9 A. I. A. Sherlala, A. A. A. Raman, M. M. Bello and A. Asghar, A review of the applications of organo-functionalized magnetic graphene oxide nanocomposites for heavy metal adsorption, *Chemosphere*, 2018, **193**, 1004–1017.
- 10 L. Li, *et al.*, Adsorbent for chromium removal based on graphene oxide functionalized with magnetic cyclodextrin-chitosan, *Colloids Surf., B*, 2013, **107**, 76–83.
- 11 S. Makharza, *et al.*, Size-Dependent Nanographene Oxide as a Platform for Efficient Carboplatin Release, *J. Mater. Chem. B*, 2013, **1**, 6107–6114.
- 12 S. Makharza, *et al.*, Graphene oxide - gelatin nanohybrids as functional tools for enhanced carboplatin activity in neuroblastoma cells, *Pharm. Res.*, 2015, **32**, 2132–2143.
- 13 T. Rattana, *et al.*, Preparation and characterization of graphene oxide nanosheets, *Procedia Eng.*, 2012, **32**, 759–764.
- 14 J. M. Eckert, R. J. Judd, P. A. Lay and A. D. Symons, Response of chromium(V) to the diphenylcarbazine spectrophotometric method for the determination of chromium(VI), *Anal. Chim. Acta*, 1991, **255**, 31–33.
- 15 M. Shaban, M. R. Abukhadra, M. Rabia, Y. A. Elkader and M. R. Abd El-Halim, Investigation the adsorption properties of graphene oxide and polyaniline nano/micro structures for efficient removal of toxic Cr(VI) contaminants from aqueous solutions; kinetic and equilibrium studies, *Rend. Lincei. Sci. Fis. Nat.*, 2018, **29**, 141–154.
- 16 S. Chowdhury and R. Balasubramanian, Recent advances in the use of graphene-family nanoadsorbents for removal of toxic pollutants from wastewater, *Adv. Colloid Interface Sci.*, 2014, **204**, 35–56.
- 17 C. He, *et al.*, Effective removal of Cr(VI) from aqueous solution by 3-aminopropyltriethoxysilane-functionalized graphene oxide, *Colloids Surf., A*, 2017, **520**, 448–458.
- 18 L. Anah and N. Astrini, Influence of pH on Cr(VI) ions removal from aqueous solutions using carboxymethyl cellulose-based hydrogel as adsorbent, *IOP Conf. Ser. Earth Environ. Sci.*, 2017, **60**, 012010.
- 19 A. Nasrollahpour, S. E. Moradi and J. Khodaveisi, Effective removal of hexavalent chromium from aqueous solutions using ionic liquid modified graphene oxide sorbent, *Chem. Biochem. Eng. Q.*, 2017, **31**, 325–334.
- 20 M. Uysal and I. Ar, Removal of Cr(VI) from industrial wastewaters by adsorption. Part I: determination of optimum conditions, *J. Hazard. Mater.*, 2007, **149**, 482–491.

