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# The microstructure and protective properties of electroplating zinc films on NdFeB from a chloride-free nonaqueous bath†

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The traditional aqueous electroplating of zinc film causes significant corrosion of NdFeB during the electroplating process, which is accompanied by hydrogen evolution reactions. In this study, electroplating zinc film is carried out from a chloride-free nonaqueous bath using zinc acetate ( $\text{Zn}(\text{OAc})_2$ ) as the main salt, sodium acetate ( $\text{NaOAc}$ ) as the conducting salt, and ethylene glycol (EG) as the solvent. The electrochemical properties of the EG bath with  $\text{Zn}(\text{OAc})_2$  and  $\text{NaOAc}$  are characterized by means of cyclic voltammetry (CV) and linear sweep voltammetry (LSV) together with a Hull cell test on brass. The results of the experiment show that the  $\text{Zn}(\text{OAc})_2$  concentration, current density, and temperature significantly impact the deposition behavior of zinc. Moreover, the open circuit potential (OCP) test and scanning electron microscopy (SEM) results demonstrated that the corrosion of NdFeB in the EG bath containing 0.7 M  $\text{Zn}(\text{OAc})_2$  and  $\text{NaOAc}$  is effectively inhibited compared to when using the traditional aqueous zinc plating bath. A dense zinc film with a metallic appearance is successfully deposited on the NdFeB surface from the EG bath containing 0.7 M  $\text{Zn}(\text{OAc})_2$  and  $\text{NaOAc}$  at  $6 \text{ mA cm}^{-2}$  and  $60 \text{ }^\circ\text{C}$ . Comparative experiments demonstrate that the as-deposited Zn film exhibits superior protective performance and exerts less damage to NdFeB compared to the aqueous electroplating film.

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## 1. Introduction

Permanent magnetic materials are widely utilized in various industries and daily life, including in electric, electronic, and electromechanical devices. Sintered NdFeB is particularly favored as the leading commercial permanent magnet due to its numerous advantages.<sup>1</sup> In particular, NdFeB is often used in demanding corrosive environments such as marine and industrial settings involving acids.<sup>2,3</sup> However, due to the high reactivity of Nd and Fe and the relatively loose structure of sintered NdFeB, corrosion susceptibility is a significant issue, resulting in premature function failure.<sup>4–6</sup> Therefore, protective measures need to be implemented to mitigate corrosion effects on these magnets.<sup>7–11</sup> Presently, the primary approach to protecting NdFeB from corrosion involves utilizing various coating materials.<sup>12–14</sup> Metal coatings, such as Ni,<sup>15–18</sup> Ni–P,<sup>19,20</sup> Ni–Cu,<sup>21,22</sup> Zn,<sup>23–26</sup> are the most popular choices in the industry. So far, aqueous electroplating is still the most widely used method of metal coating deposition,<sup>27–30</sup> although physical vapor deposition,<sup>31–33</sup> chemical vapor deposition,<sup>4</sup> thermal spraying,<sup>34</sup> and other technologies have also developed. Unfortunately,

NdFeB is prone to corrosion during the aqueous electroplating process due to exposure to the electrolytic bath solution. Furthermore, the unavoidable electrolysis of water during the process introduces hydrogen embrittlement, which can adversely affect the mechanical and magnetic properties of the magnet. Consequently, the use of nonaqueous electrolytes in nonaqueous electroplating has been explored as a potential solution for overcoming these drawbacks.<sup>35</sup> A nonaqueous bath can minimize secondary reactions, and high-quality films may be obtained, making it an effective alternative approach.<sup>36</sup>

In the past few decades, the most extensively studied nonaqueous systems used for electroplating include ionic liquids (ILs) and deep eutectic solvents (DESs).<sup>37</sup> In the former system, the organic solvent used also acts as an electrolyte, while in the latter one, the hydrogen bond donor (HBD) is mixed with the hydrogen bond acceptor (HBA) (such as quaternary ammonium cation) at an appropriate molar ratio to form a conductive eutectic solution. DESs are currently being considered as potential alternatives to traditional electroplating solutions and have even been implemented at industrial scales in some cases.<sup>38,39</sup> However, it is essential to note that high concentrations of chloride ions in chloride-based DES baths can create an aggressive environment for the substrate. Therefore, in future research, it is necessary to investigate the elimination or substitution of choline chloride, especially when dealing with active substrates like NdFeB.<sup>40</sup> A recent study by Panzeri *et al.* successfully electroplated a high-purity zinc film

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using a chloride-free nonaqueous solution consisting of ethylene glycol, acetate salt, and precursor salt.<sup>41</sup> Furthermore, their previous research findings indicate that the resulting film deposits exhibited significantly better corrosion performance than those obtained from a chloride-based DES due to a less aggressive/corrosive environment.

In this study, the primary objective is to develop a chloride-free nonaqueous bath that is both efficient and environmentally friendly for the protection of NdFeB magnets. The composition of the bath is based on a combination of ethylene glycol and acetate salts, which presents a promising alternative to traditional chloride-based solutions. A series of experiments are conducted to determine the optimal parameters for the bath, carefully controlling and analyzing factors such as bath temperature, deposition time, current density, and concentration of acetate salts. Additionally, scanning electron microscopy (SEM), Tafel curves, open circuit potential (OCP), and salt spray testing are carried out to assess the surface morphology and corrosion resistance of zinc films. This chloride-free nonaqueous bath offers a practical and environmentally friendly alternative for NdFeB protection and contributes to advancing sustainable and eco-conscious manufacturing processes.

## 2. Experimental

### 2.1. Chemicals

Ethylene glycol, zinc acetate, sodium acetate, and potassium acetate (Shanghai Aladdin Bio-Chem Technology Co., Ltd) are used as received. Where ethylene glycol is the hydrogen-bonding donor, zinc acetate is the hydrogen bond acceptor for zinc electroplating, and sodium acetate is used to improve the conductivity of the electroplating bath. NdFeB rod and plate are provided by Anhui Dadixiong New Materials Co., Ltd.

### 2.2. Electroplating Zn films

The NdFeB and brass rod with a diameter of 1 cm used in the experiment is cut, welded with Cu wire for electrical connections, and installed into the epoxy resin with one active flat surface. Successive grades of abrasive papers up to 1000 grit are employed on electrodes and plates, copiously rinsing with distilled water and anhydrous ethanol, and finally drying under nitrogen flow. The Hull cell test is conducted using a conventional two-electrodes cell with a volume of 273 ml. The cathode is comprised of a brass plate measuring  $10 \times 6.5$  cm. The current is set at  $0.5 \text{ A dm}^{-2}$ , and the test duration is 10 minutes, with a temperature of  $60 \text{ }^\circ\text{C}$ . In the bath solution, the concentration of zinc acetate is varied at 0.1 M, 0.3 M, 0.5 M, and 0.7 M, while the ratio of conductive salt sodium acetate to zinc acetate is maintained at 1 : 1, and is labeled as 0.1M-EG, 0.3M-EG, 0.5M-EG, and 0.7M-EG bath, respectively. The zinc film is electro-deposited onto NdFeB plates using a galvanostatic method for characterization.

### 2.3. Electrochemical tests

Electrochemical experiments are conducted using an RST 5200 electrochemical workstation from Zhengzhou Shiruishi

Instrument Technology Co., Ltd. The experimental setup consisted of a three-electrode system: a platinum plate ( $1 \times 1$  cm) served as the counter electrode, a nonaqueous  $\text{Ag}^+/\text{AgCl}$  electrode acted as the reference electrode, and a working electrode. The linear sweep voltammetry test is performed in the 0.7M-EG bath as the temperature varies from  $30 \text{ }^\circ\text{C}$  to  $60 \text{ }^\circ\text{C}$ . The scan range extended from the open circuit potential to the negative direction, with a voltage window of 0 to 4 V and a scanning rate of  $0.02 \text{ V s}^{-1}$ . Different bath solutions are employed at a constant temperature of  $60 \text{ }^\circ\text{C}$  for cyclic voltammetry testing. The scan started from the open circuit potential and went to  $-2 \text{ V}$  in the negative direction, then returned to the open circuit potential at a scanning rate of  $0.001 \text{ V s}^{-1}$ . The timing current test involved applying a voltage within the  $-1.9$  to  $-1.92 \text{ V}$  range, with step increases of  $-0.01 \text{ V}$  for one second. Tafel curves are obtained by scanning from  $-0.02 \text{ V}$  to  $+0.25 \text{ V}$  relative to OCP, with a scan rate of  $0.0005 \text{ V s}^{-1}$ .

### 2.4. Characterization

The surface morphologies of the Zn films are examined using scanning electron microscopy (SEM; FEI Quanta 250 FEG, USA). The chemical composition and elemental mapping of the Zn films are detected using energy-dispersive X-ray (EDX) spectroscopy. The crystal features of the deposited Zn films are characterized using an X-ray diffractometer (XRD; Bruker D8 Advance Davinci, Germany). XPS spectra are collected using an AXIS ULTRA DLD X-ray photoelectron spectrometer with an Al-anode. The binding energies are referenced to the binding energy of the C 1s line, which is set at  $285.0 \text{ eV}$ . The bonding strength between the zinc film and the NdFeB substrate is tested by using an electronic controlled universal testing machine (PY-880, CN). Using glue as a binder to connect the coating with the tie rod, and the tension is applied until the coating and the NdFeB substrate are completely separated.

## 3. Results and discussion

Using acetate salts implies that the anion species in the solution has a larger ionic radius than the chloride usually found in DESs. Consequently, the low conductivity provided by the anion species must be compensated by increasing the amount of metal precursor salt and potentially by incorporating a supporting electrolyte like sodium acetate and potassium acetate, both of which contain the acetate anion. As noted by Panzeri *et al.*,<sup>41</sup> zinc acetate ( $\text{Zn}(\text{OAc})_2$ ) exhibits a solubility of no more than  $0.75 \text{ M}$  in ethylene glycol (EG) at  $30 \text{ }^\circ\text{C}$ . If the salt is further dissolved, it may form a white precipitate (ZnO). The cyclic voltammetry (CV) of the NaOAc-EG bath without  $0.7 \text{ M}$   $\text{Zn}(\text{OAc})_2$ , as depicted in Fig. 1a, does not exhibit a pronounced cathode peak within the electrochemical window of  $-2$  to  $0 \text{ V}$ . This suggests that there are no notable side cathodic reactions leading to the degradation of NaOAc and EG, indicating high stability of the NaOAc-EG bath. Despite the absence of significant secondary reactions, a small amount of hydrogen is also anticipated at lower overpotentials due to the presence of protons in the solution. Fig. 1a also indicates the onset of zinc



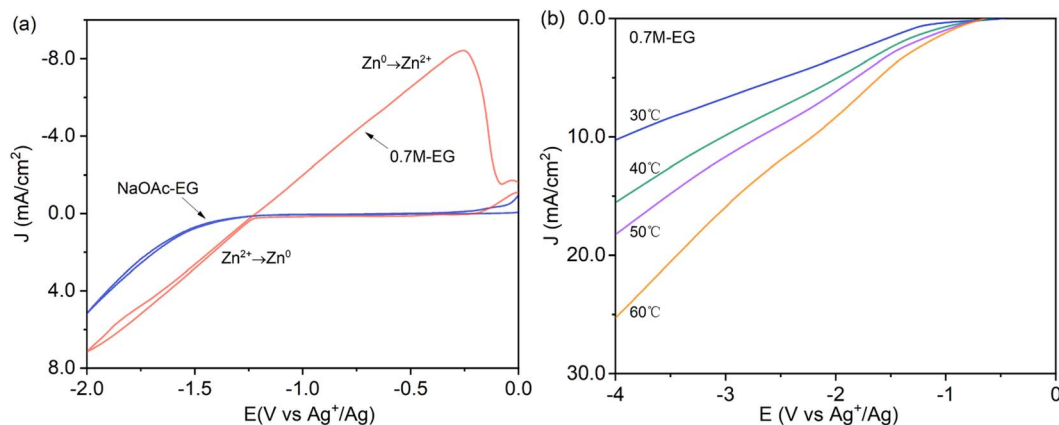


Fig. 1 (a) The cyclic voltammetry of the NaOAc-EG and 0.7M-EG bath ( $1 \text{ mV s}^{-1}$ ,  $60 \text{ }^\circ\text{C}$ ) and (b) linear sweep voltammetry of the 0.7M-EG bath at different temperatures ( $1 \text{ mV s}^{-1}$ ).

electrodeposition ( $\text{Zn}^{2+} \rightarrow \text{Zn}^0$ ) at  $-1.25 \text{ V vs. Ag}^+/\text{Ag}$  for the 0.7M-EG bath, corresponding to the sudden increase in the cathodic current. The observed linear relationship between cathodic potential and current density indicates that the electroplating processes in the 0.7M-EG bath are under kinetic control. To further investigate, linear sweep voltammetry (LSV) is carried out on the brass electrode in the 0.7M-EG bath at different temperatures with a lower cathodic limit ( $4 \text{ V vs. Ag}^+/\text{Ag}$ ). Fig. 1b illustrates that the current density in the 0.7M-EG bath increases as the bath temperature rises. This behavior is attributed to the higher diffusion rate of ions and the reduced viscosity of EG at higher temperatures, resulting in a higher current density. Notably, understanding this correlation between temperature and current density is crucial for optimizing the performance of these baths.

The current density experiment is conducted in a 267 ml Hull cell, using a current of 0.5 A for electroplating for 10 minutes, with a cathode brass sheet of  $10 \times 6.5 \text{ cm}$ . The distance from the near end of the cathode plate is expressed in  $X$ , in cm. The relationship between distance and current density is as follows:

$$J_K = I \times (5.10 - 5.24 \times \log X), \quad (1)$$

wherein  $I$  is the current used in the experiment, and the range of  $X$  is between 0.635–8.255 cm.

Fig. 2 depicts photographs of the Hull cell experiment conducted in various electroplating baths, in which different concentrations of  $\text{Zn}(\text{OAc})_2$  and NaOAc at  $60 \text{ }^\circ\text{C}$ . As illustrated in Fig. 2, the substrate is clearly visible at the distal end after

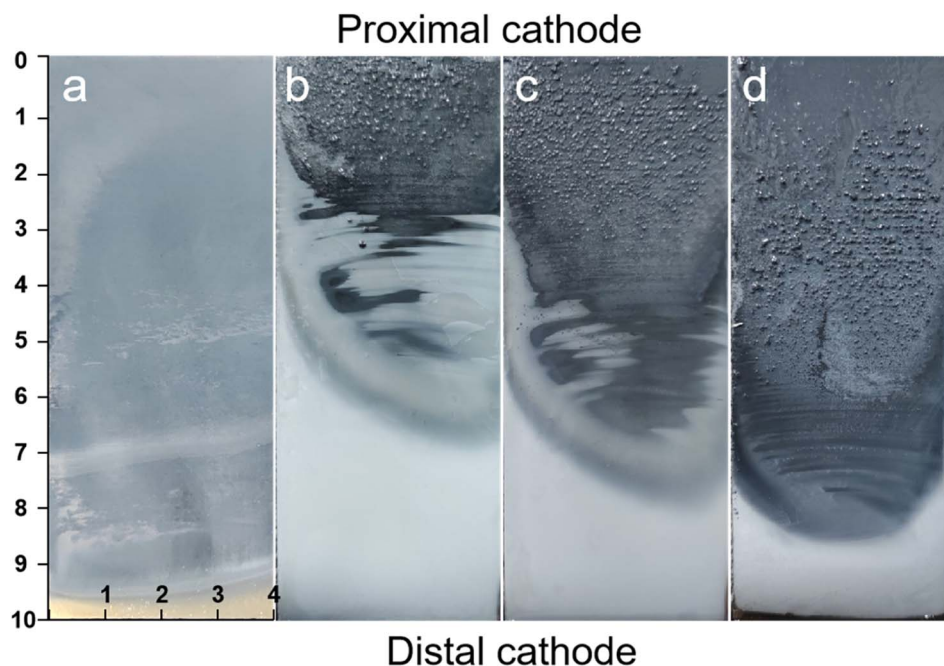


Fig. 2 Photo of Hull cell experiment in the different electroplating bath at  $60 \text{ }^\circ\text{C}$ : (a) 0.1M-EG, (b) 0.3M-EG, (c) 0.5M-EG, and (d) 0.7M-EG.



electroplating for 10 minutes in the 0.1M-EG bath. This is attributed to the low concentration of zinc salt in the bath, as well as the small current density. The corresponding images reveal distinct variations in appearance after electroplating for 10 minutes in  $\text{Zn}(\text{OAc})_2$ -NaOAc-EG baths with concentrations of 0.3 M, 0.5 M, and 0.7 M, respectively. Notably, metallic zinc films are observed at the distal cathode area, while the zinc films in the proximal cathode region appear black and contain bubbles. Furthermore, the bright area expands with an increase in both zinc salt and conductive salt concentrations.

Fig. S1(ESI†) presents the SEM surface morphology of Zn film at different distances from the proximal cathode electroplating from the 0.1M-EG bath. It can be observed that the zinc film is incomplete and consists of dispersed, extremely fine zinc particles. When the concentration of  $\text{Zn}(\text{OAc})_2$  and NaOAc is increased to 0.3 M, compact films with a hexagonal microstructure are obtained through electrodeposition in the current density range of  $1.8$ – $3.3 \text{ mA cm}^{-2}$  (see Fig. S2a†). In Fig. S2b–d,† incomplete zinc films composed of zinc particles are presented, indicating the increased significance of secondary reactions in film

morphology when the current density exceeds  $3.3 \text{ mA cm}^{-2}$ . The SEM morphology differences in the bright area compared to other areas can explain the macroscopic differences in the corresponding regions. As shown in Fig. S3,† a further increase in the  $\text{Zn}(\text{OAc})_2$  and NaOAc concentration to 0.5 M results in zinc films with different shapes and orientations at different current densities. Compact films like  $\langle 002 \rangle$ ,  $\langle 004 \rangle$  with multilayer units parallel to the substrate are obtained when the deposition current density is in the range of  $1.8$ – $5 \text{ mA cm}^{-2}$ . However, zinc films obtained at a deposition current density of  $5$ – $10 \text{ mA cm}^{-2}$  exhibit a textured microstructure. Upon comparison (seen Fig. 3), it can be observed that zinc films obtained from the 0.7M-EG bath display a finer nanoscale multi-level structure than those obtained from a 0.5 M bath.

Based on the Hull cell experiment results, two zinc films are obtained through galvanostatic deposition at two different current densities for 30 min:  $3 \text{ mA cm}^{-2}$  in the 0.5M-EG bath and  $6 \text{ mA cm}^{-2}$  in the 0.7M-EG bath. These films are then analyzed using XRD (see Fig. 4). The diffractograms revealed a significant orientation along the  $\langle 002 \rangle$  direction for the former

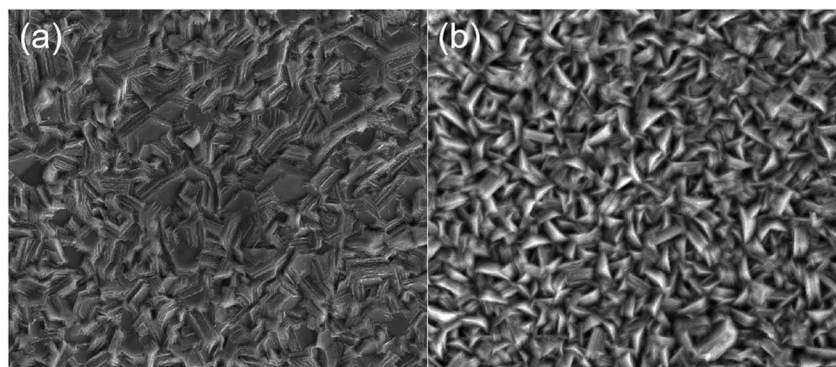


Fig. 3 SEM surface morphology of Zn film from the proximal cathode at different distances from the proximal cathode on brass (a) 7–8 cm from the 0.5M-EG bath and (b) 5–6 cm from 0.7M-EG bath.

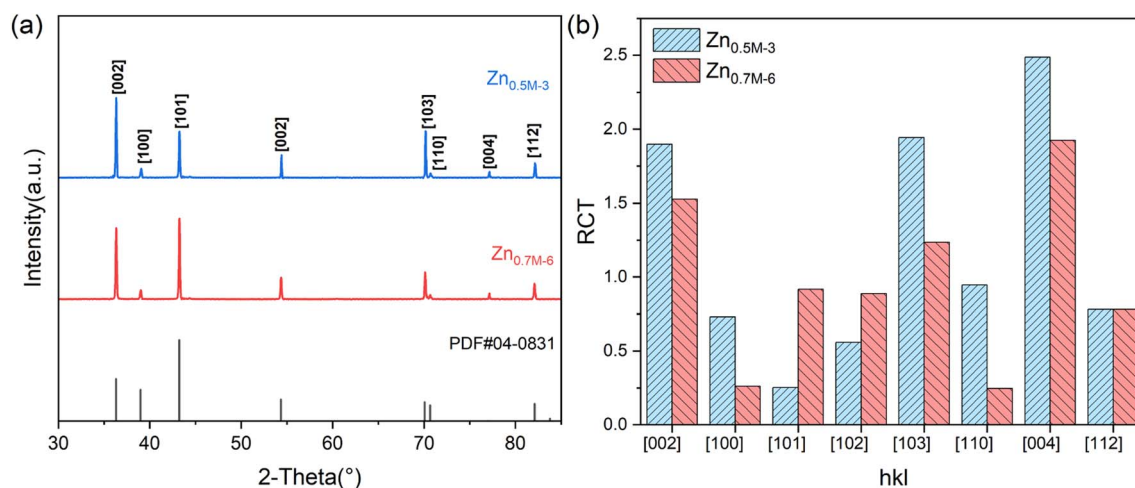


Fig. 4 (a) XRD spectra of zinc films from the galvanostatic deposition at  $3 \text{ mA cm}^{-2}$  in the 0.5M-EG bath for 30 min ( $\text{Zn}_{0.5\text{M}-3}$ ) and the galvanostatic deposition at  $6 \text{ mA cm}^{-2}$  in the 0.70.5M-EG bath for 30 min ( $\text{Zn}_{0.7\text{M}-6}$ ). (b) The relative texture coefficient is calculated from the peak intensity of XRD spectra and the standard relative diffraction intensity of the JCPDS 04-0831.



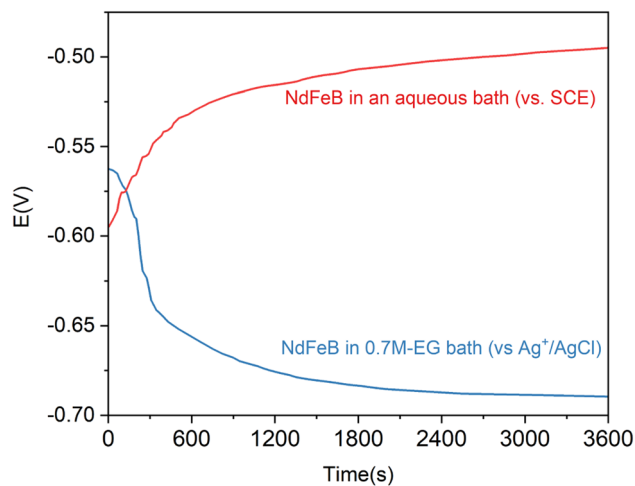


Fig. 5 The OCP curves of NdFeB electrodes in an aqueous alkaline zinc plating bath and the 0.7M-EG bath.

film, while the latter film showed a significant orientation along the  $\langle 101 \rangle$  direction. The SEM surface morphology of the former film also shows identifiable hexagonal cells on the basal surface, consistent with a previous report.<sup>41</sup> To provide a more precise indication of the microstructural orientation, the relative texture coefficient (RTC) is calculated using the following eqn (2):

$$RTC_{hkl} = \frac{I_{hkl}}{I_{0\ hkl}} \frac{n}{\sum_{i=1}^n (I_{hkl}/I_{0\ hkl})} \quad (2)$$

where the  $I_{hkl}$  is the relative diffraction intensity of a given plane  $\langle hkl \rangle$  of the deposited Zn film,  $I_{0\ hkl}$  is the standard diffraction intensity for the JCPDS 04-0831. The value of  $RTC_{hkl}$  represents the texture coefficient, which quantifies the preferred orientation of the deposited Zn film on the  $(hkl)$  crystal plane. Therefore, a higher value of  $RTC_{hkl}$  indicates a stronger preferred orientation, meaning that more grains in the Zn film grow along the  $(hkl)$  crystal plane. The calculation result of  $Zn_{0.5M-3}$  on brass shows the coexistence between  $\langle 002 \rangle$ ,  $\langle 004 \rangle$ , and  $\langle 103 \rangle$  orientations in accordance with the micrographs showing the presence of the basal plane (hexagonal shape) slightly tilted with

respect to the orthogonal direction. However, the orientation of the  $Zn_{0.7M-6}$  in these directions is weaker than that of  $Zn_{0.5M-3}$  and has a stronger orientation along  $\langle 101 \rangle$  and  $\langle 102 \rangle$  directions.

Fig. 5 displays the OCP curves for the NdFeB electrode in an aqueous alkaline zinc plating bath<sup>42</sup> and the 0.7M-EG bath. The OCP curves for the NdFeB electrodes in these two baths demonstrate distinct trends. In the aqueous bath, the OCP value sharply increases with time and then tends to stabilize. This observation suggests that the active component of the NdFeB electrode undergoes a corrosion reaction in the aqueous bath. Conversely, in the 0.7M-EG bath, the OCP value decreases rapidly with time and then stabilizes. This behavior may be attributed to the adsorption of EG and  $Zn^{2+}$  complex molecules on the NdFeB electrode, which form a double layer and lead to a change in potential. In order to visually understand the changes that occur during this process, the morphology of the NdFeB magnets is observed through BSE imaging (see Fig. 6). The white areas in the image indicate the Nd-rich phase. The surface of the NdFeB undergoes significant changes after immersing in these two baths for 30 min. In the aqueous bath, corrosion is more severe at the grain boundaries, as the white area nearly disappears, and the main phase grains are accentuated in some regions. Conversely, there is almost no significant corrosion after immersing in the 0.7M-EG bath. Since the current density between the OPC and the initial deposition potential is very small, the electrode is hardly corroded. Considering that these corrosion changes can negatively impact the performance of NdFeB, it is clear that electroplating a zinc film in the EG bath is superior to doing so in the aqueous bath.

Fig. 7 depicts the cyclic voltammetry curves of NdFeB electrodes in different EG baths. The results indicate a significant difference between the initial concentration of 0.1 M and the concentrations of 0.3 M and 0.5 M. However, there is minimal variation between 0.5 M and 0.7 M, likely due to the similarity in the concentrations of free  $Zn^{2+}$  and  $Na^+$  in EG, which are close to their saturation points. At a concentration of 0.1 M, only one region of reduction peaks ( $C_2$ ) is observed at approximately  $-1.89$  V. When the concentration increases to 0.3 M, one reduction peaks appear at around  $-1.84$  ( $C_2$ ) V. Subsequently, at a concentration of 0.5 M, two reduction peaks are observed at approximately  $-1.22$  V ( $C_1$ ),  $-1.84$  V ( $C_2$ ) and one oxidation

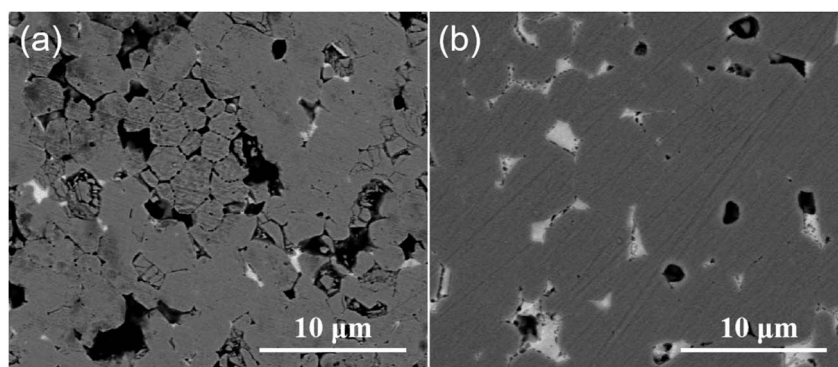


Fig. 6 BSE image of NdFeB after immersing in (a) an aqueous alkaline zinc plating bath and (b) the 0.7M-EG bath for 30 min.



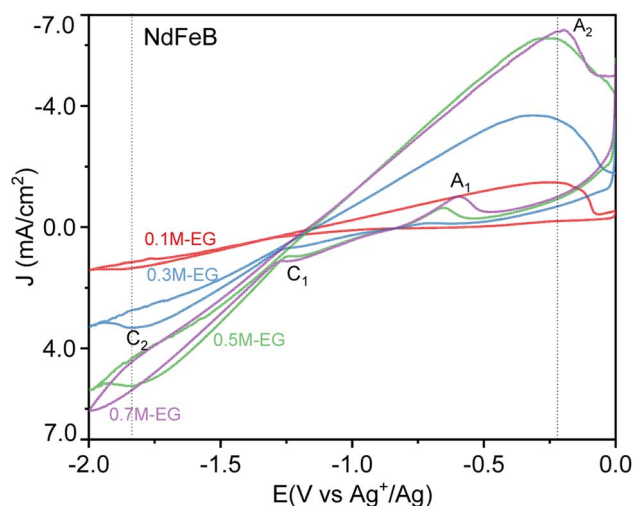


Fig. 7 The cyclic voltammograms of NdFeB electrodes in the 0.1M-EG, 0.3M-EG, 0.5M-EG, and 0.7M-EG baths ( $1 \text{ mV s}^{-1}$ ,  $60^\circ \text{C}$ ).

peak at around  $-0.65 \text{ V}$  ( $A_1$ ). Finally, at a concentration of  $0.7 \text{ M}$ , two reduction peaks are observed at around  $-0.48 \text{ V}$  and  $-1.25 \text{ V}$  ( $C_1$ ). These reduction peaks could be attributed to the redox of the Nd and Fe elements.  $A_1$  and  $C_1$  are the redox peaks of the matrix, respectively, and  $C_2$  and  $A_2$  are the oxidation and

reduction peaks of  $\text{Zn}^{2+}$ . In addition, Guilin Xiang *et al.* also observed the reduction peak of Nd around  $-1.25 \text{ V}$  in the cyclic voltammogram curve of Nd.<sup>43</sup> The low conductivity at low concentrations makes the electromigration process very slow, resulting in almost no redox peaks of the substrate, and the peak values of redox peaks are positively correlated with conductivity, and due to the increase of concentration,  $\text{Zn}^{2+}$  is no longer controlled by diffusion in the electrodeposition process, resulting in the disappearance of  $\text{Zn}^{2+}$  reduction peaks and diffusion plateaus at  $0.7 \text{ M}$  concentrations.

The reduction peak potentials of  $0.5 \text{ M}$  and  $0.7 \text{ M}$  are selected for further investigation and experimentation with the Zn reduction processes. The chronoamperometry technique can be utilized to understand the mechanisms of nucleation and growth rates during electrodeposition. According to the literature review,<sup>44</sup> the Schariker and Hills models explain the nucleation process, specifically the three-dimensional (3D) instantaneous and asymptotic mechanisms under diffusion control. Eqn (3) and (4) present the mathematical expressions of these models in dimensionless form, which determine the nucleation 3D instantaneous mechanism and asymptotic mechanism, respectively.

In both equations,  $I$  is the current density at a particular time  $t$ ,  $I_m$  is the maximum current density, and  $t_m$  is the time obtained at the maximum current peak to perform  $I$ .

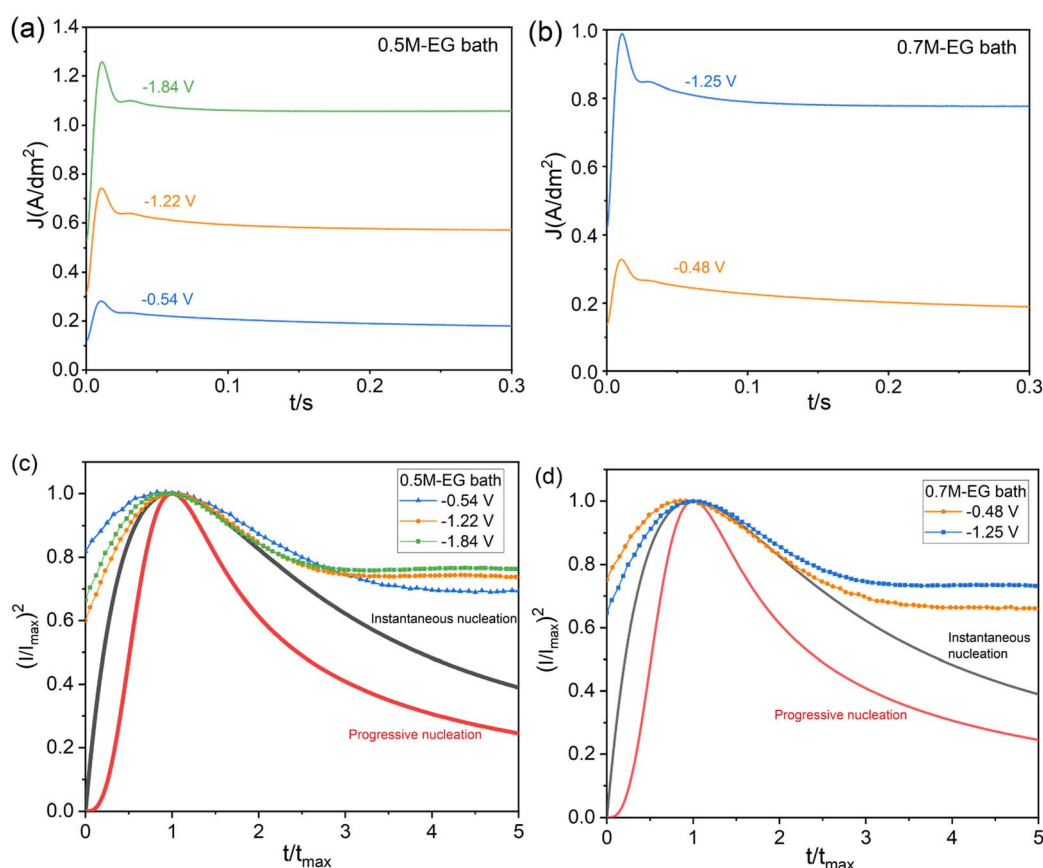


Fig. 8 The variation of current density with deposition time at different deposition potentials (a) in the 0.5M-EG bath and (b) in the 0.7M-EG bath ( $60^\circ \text{C}$ , vs.  $\text{Ag}^+/\text{AgCl}$ ). The fitting results of  $(I/I_{\text{max}})^2$  vs.  $t/t_{\text{max}}$  (c) the 0.5M-EG bath and (d) the 0.7M-EG bath.



Instantaneous:

$$(I/I_{\max})^2 = [1.9542/(t/t_{\max})]\{1 - \exp[-1.2564(t/t_{\max})]\}^2 \quad (3)$$

Progressive:

$$(I/I_{\max})^2 = [1.2254/(t/t_{\max})]\{1 - \exp[-2.3367(t/t_{\max})^2]\}^2 \quad (4)$$

Fig. 8 depicts a plot of  $(I/I_{\max})^2$  vs.  $(t/t_{\max})$  to illustrate the growth of Zn from the 0.5M-EG and 0.7M-EG bath at 60 °C. The plot shows the theoretical patterns for 3D instantaneous and progressive nucleation. Initially, there is a dramatic increase in current when the overpotential is applied, which can be attributed to double-layer charging. In the next stage, the current reaches its maximum ( $I_m$ ), indicating the formation and growth of Zn particles on the NdFeB substrate. Subsequently, the current decays due to limitations imposed by diffusion processes. A comparison of the nucleation modes in each system, as shown in Fig. 8, reveals that the nucleation mechanism for Zn growth from the 0.7M-EG bath aligns more closely with the expected 3D instantaneous nucleation. This finding is consistent with previous research on Zn deposition. Furthermore, the observation of timing current curves at different potentials reveals that an increase in overpotential leads to a corresponding increase in  $t_{\max}$ . This indicates inhibition of nucleation, which may be related to the adsorption of EG molecules at high overpotentials.

The timing-current curve is processed to validate the experimental data, following Schariker's theory. The  $J - t^{1/2}$  function is used to characterize the rising region of the curve, while the falling region is characterized using the  $J - t^{-1/2}$  function. This analysis results in Fig. 9 reveal that the curve does not exhibit a linear correlation and deviates from linearity during the initial and subsequent stages. This finding indicates that the electrodeposition of Zn on NdFeB is governed by a three-dimensional instantaneous nucleation mechanism controlled by electrochemistry and diffusion rather than diffusion alone. The nucleation process plays a crucial role in shaping the structure and morphology of the film, while the growth process after nucleation further influences these characteristics. Specifically, the nucleation and growth processes of electrodeposition significantly impact the final surface morphology of the coating. Electrodeposition can manifest as island-like or layered growth depending on the nucleation processes.

Furthermore, based on the morphology observed during the initial growth stage of the deposited film, the nucleation process can be classified into three modes:<sup>43</sup> Volmer-Weber (V-W), Frank-van der Merwe (F-M), and Stranski-Krastanov (S-K). In the V-W mode, deposition initiates with island-like nucleation and gradually progresses to form a complete thin film. The F-M mode occurs when there is lattice matching between the deposited thin film and the substrate. In this mode, metal ions are adsorbed on the electrode surface after reduction, migrate to the active point, and form a continuous spread of base atoms, resulting in single atomic layer growth of the thin film. The S-K mode can be understood as a transitional or intermediate state between the aforementioned deposition modes. The energy difference between the deposition and base atoms in this mode lies between the V-W and S-K modes.

Fig. 10 illustrates the nucleation and growth of zinc films as observed through SEM. Fig. 10a and d demonstrate the formation of a thin zinc layer within 5 s, aligning with the pattern of instantaneous nucleation. After 15 s, the surface is nearly entirely covered, indicating that nucleation and growth are considerably faster in the 0.7M-EG bath than in the 0.5M-EG one. This rapid growth can be attributed to the high concentration and current density, resulting in a higher diffusion coefficient. After 60 seconds, Fig. 10c and f show a specific crystal plane orientation, with the growth in the 0.7 M bath appearing denser and more uniform, showcasing complete coverage. Notably, the EDS of the Zn deposits revealed the presence of zinc and some oxides (see Fig. S5†). These oxides may have resulted from the oxidation of zinc or the substrate after the deposition process due to exposure to air. The SEM images at various time points suggest that the nucleation and growth observed here follow the F-M growth mode.

Fig. 11 illustrates the cross-section morphology and EDS maps of the deposited zinc films on NdFeB, which are obtained through 30 minutes of electroplating from the 0.7M-EG at 6 mA  $\text{cm}^{-2}$  ( $\text{Zn}_{0.7\text{M-6}}$ ) and from the 0.5M-EG bath at 3 mA  $\text{cm}^{-2}$  ( $\text{Zn}_{0.5\text{M-3}}$ ). As shown corresponding images in Fig. 11, the deposited  $\text{Zn}_{0.5\text{M-3}}$  film on NdFeB is characterized by multiple holes, posing a challenge to its corrosion resistance. Furthermore, a small amount of Fe within the film is discernible, along with the existence of Fe in the NdFeB matrix. It can be inferred that the newly reduced Zn displaces the Fe element within the matrix

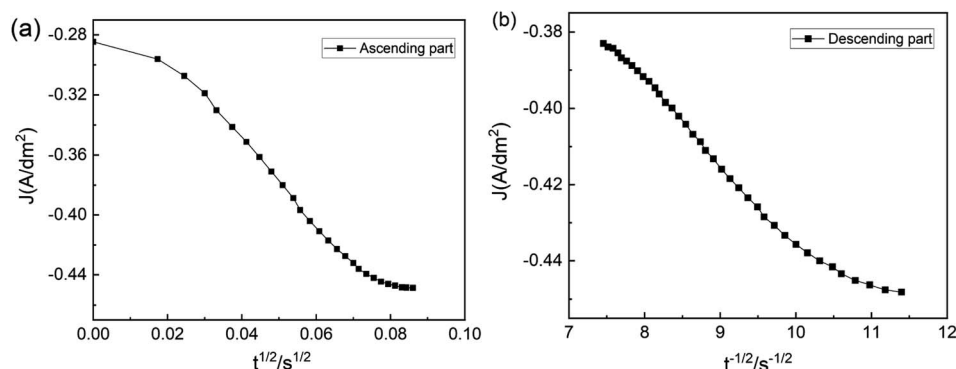


Fig. 9 The timing-current curves of the 0.7M-EG bath (a) ascending part and (b) descending part.



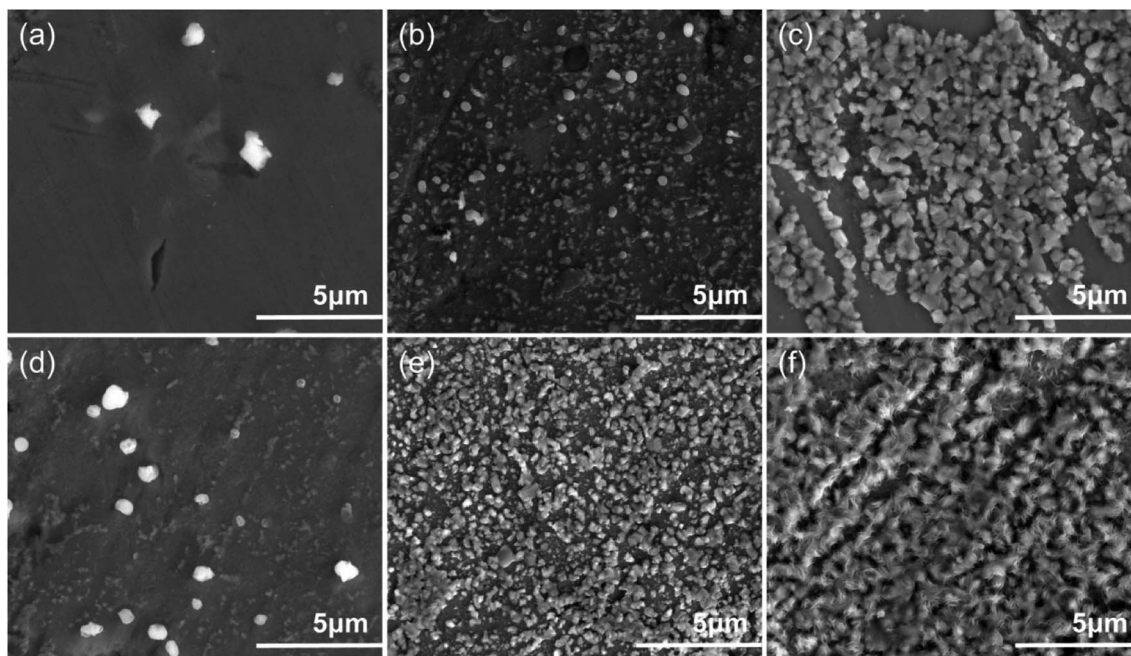


Fig. 10 The SEM morphology of the deposited Zn film on NdFeB at different times: (a) 5 s, (b) 15 s, (c) 60 s from the 0.5M-EG ( $3 \text{ mA cm}^{-2}$ ,  $60^\circ \text{C}$ ) and (d) 5 s, (e) 15 s, (f) 60 s from the 0.7M-EG ( $6 \text{ mA cm}^{-2}$ ,  $60^\circ \text{C}$ ).

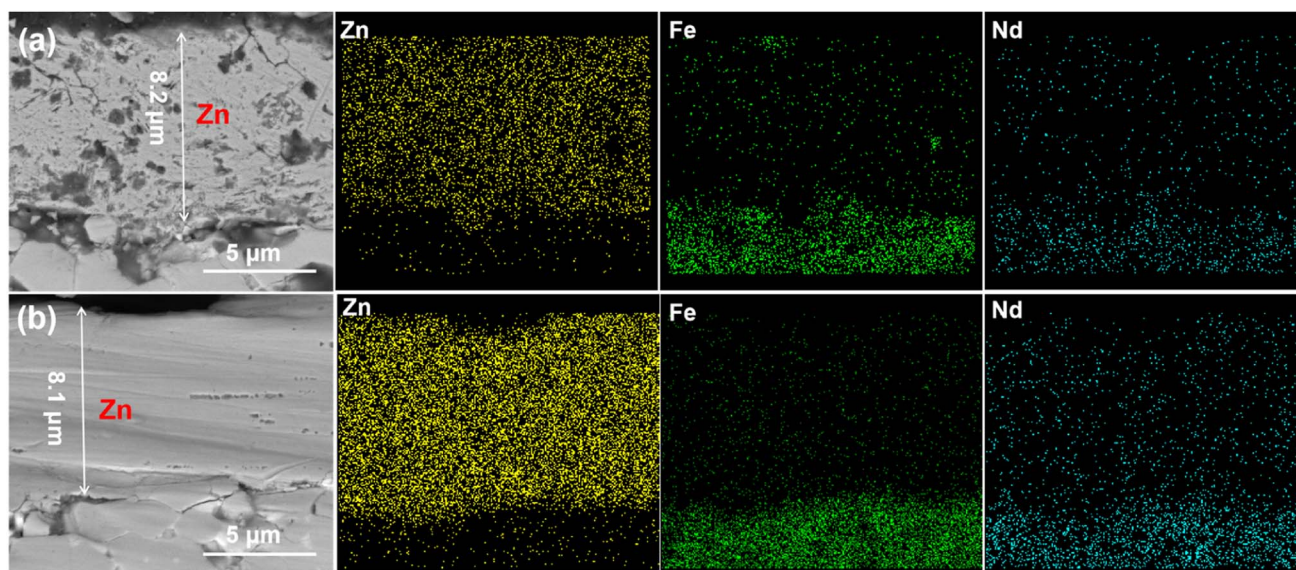


Fig. 11 The cross-section and EDS spectra of the zinc coating (a)  $\text{Zn}_{0.5\text{M}-3}$  (from the 0.5M-EG bath at  $2 \text{ mA cm}^{-2}$ , 60 min,  $60^\circ \text{C}$ ) and (b)  $\text{Zn}_{0.7\text{M}-6}$  (from the 0.7M-EG bath at  $6 \text{ mA cm}^{-2}$ , 30 min,  $60^\circ \text{C}$ ).

during the initial nucleation stage. This inference aligns with the findings from previous cyclic voltammetry tests. The initial crystal nucleus experiences continuous generation and dissolution due to the displacement effect, forming two closely positioned reduction peaks during the negative scanning process. Encouragingly, the deposited  $\text{Zn}_{0.7\text{M}-6}$  film exhibits higher density and uniformity. It is worth noting that the adhesion of the zinc film, which is deposited from the EG bath, on NdFeB is significantly higher compared to the film deposited from the

aqueous bath. Specifically, the  $\text{Zn}_{0.7\text{M}-6}$  film on NdFeB demonstrates an average bonding strength of approximately 18.5 MPa, while the zinc film deposited from the aqueous solution bath only achieves an average bonding strength of 11.2 MPa.

Fig. 12 shows the OCP curves of these as-prepared two Zn films on NdFeB in 3.5 wt% NaCl solution. It can be observed that the OCP value of  $\text{Zn}_{0.7\text{M}-6}$  is consistently higher than that of  $\text{Zn}_{0.5\text{M}-3}$ . Analyzing the OCP curve of  $\text{Zn}_{0.7\text{M}-6}$ , it is seen that the potential initially drops from  $-1.01 \text{ V}$  to  $-1.0 \text{ V}$  over the first



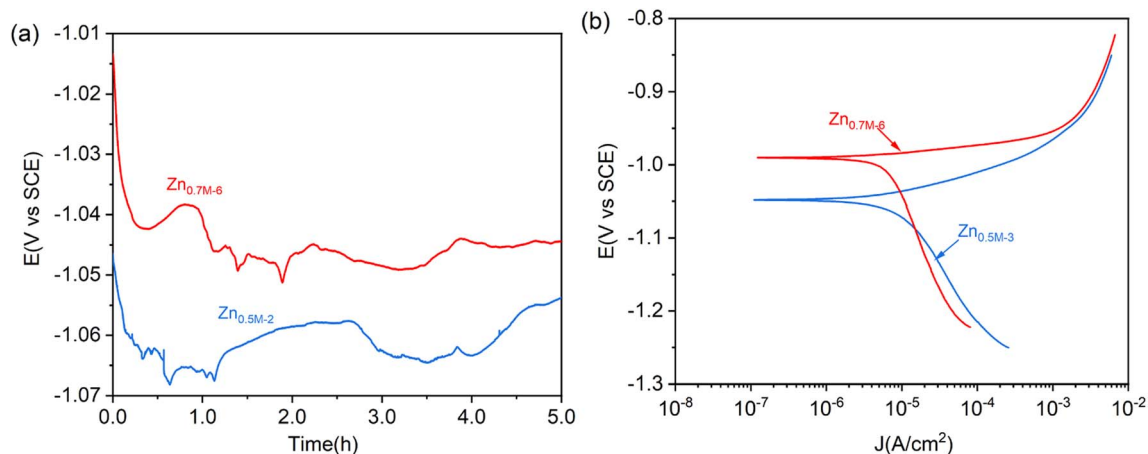


Fig. 12 (a) OCP curves and (b) Tafel curves of the Zn<sub>0.5M-3</sub> and Zn<sub>0.7M-6</sub> covered NdFeB in 3.5 wt% NaCl solution.

20 min. This drop may be attributed to the destruction of the oxide film on the surface of the Zn film. As the immersion time reaches 50 min, the potential moves positively to  $-1.04$  V, indicating the formation of corrosion products such as hydroxides. Subsequently, the potential drops and then plateaus as the corrosion products transform into more stable insoluble chlorides. Comparison between Zn<sub>0.7M-6</sub> and Zn<sub>0.5M-3</sub> reveals a lower OCP value for Zn<sub>0.5M-3</sub>. The potential value of Zn<sub>0.5M-3</sub> decreases from  $-1.05$  V to  $-1.07$  V during the initial stage of oxide film dissolution. This difference in potential can be attributed to numerous holes and gaps in the structure, as suggested by the cross-sectional SEM. These structural defects make it easier for corrosion products to dislodge, rendering them ineffective in hindering further corrosion.

Tafel curves are also carried out to compare the corrosion behavior of these as-prepared two zinc films (see Fig. 13). The Tafel curve gives the corrosion potential value of  $-1.04$  V for Zn<sub>0.5M-3</sub> film, which is lower than that of  $-0.99$  V for Zn<sub>0.7M-6</sub> film, in line with the OCP test. The corrosion current densities are  $I_{\text{corr}} = 5.8 \times 10^{-6}$  A cm<sup>-2</sup> and  $I_{\text{corr}} = 5.03 \times 10^{-6}$  A cm<sup>-2</sup>,

respectively. The difference in corrosion potential between these two films may be due to the differences in surface microstructure, crystal orientation, and grain size. Moreover, the current density of the anode and cathode branches of the Zn<sub>0.7M-6</sub> film is slightly lower than that of Zn<sub>0.5M-3</sub> film, which may be attributed to the more compact film on the surface of Zn<sub>0.7M-6</sub> film. As a result, the corrosive medium cannot enter the inside of the zinc coating. Secondly, due to its dense structure, the corrosion products on the surface are not easy to fall off, which can effectively hinder the corrosion process.

Fig. 13 shows the optical and SEM images of NdFeB covered with Zn<sub>0.7M-6</sub> and Zn<sub>0.5M-3</sub> film after immersion in a 3.5 wt% NaCl solution for 12 hours. As shown in the figure, the Zn<sub>0.7M-6</sub> film on NdFeB maintains a distinct metallic color, albeit slightly darker, implying its superior integrity and absence of discernible defects. Conversely, the Zn<sub>0.5M-3</sub> immersion exhibits evident red rust after the same time period, indicating that the corrosive medium has breached the Zn film and caused corrosion of the NdFeB substrate.

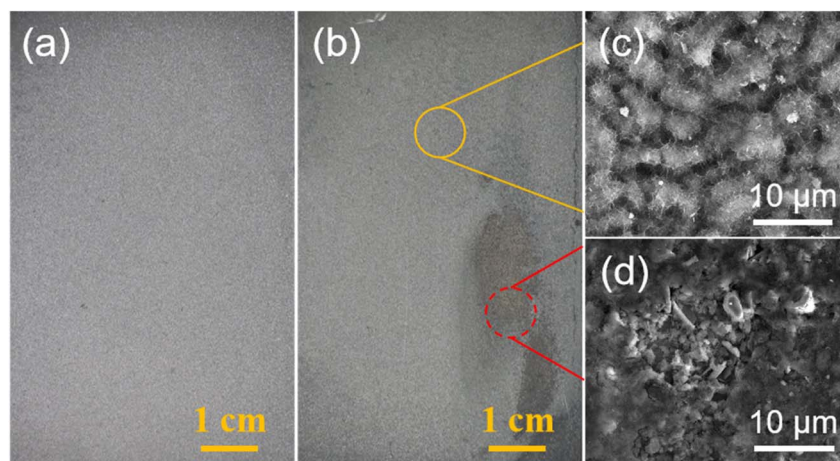


Fig. 13 Photos of NdFeB with (a) Zn<sub>0.7M-6</sub> and (b) Zn<sub>0.5M-3</sub> after immersion in a 3.5 wt% NaCl solution for 12 hours. (c) and (d) SEM surface morphology in corresponding regions of (b).

## 4. Conclusion

The high-quality zinc film is successfully electroplated on NdFeB from a chloride-free nonaqueous bath using  $\text{Zn}(\text{OAc})_2$  as the primary salt, NaOAc as the conductive salt, and EG as the solvent. In comparison to the traditional alkaline plating bath, the corrosion caused by this electroplating bath on NdFeB is virtually negligible. The results of the experiments demonstrate that the concentration of  $\text{Zn}(\text{OAc})_2$ , current density, and temperature have a significant impact on the deposition behavior of zinc. The optimal conditions for Zn deposition are as follows: an EG bath consisting of 0.7 M  $\text{Zn}(\text{OAc})_2$  and NaOAc, at a temperature of 60 °C, with a current density of 6 mA dm<sup>-2</sup>. The optimized zinc film exhibits a distinct metallic appearance, and the SEM cross-section reveals that the film is dense and exhibits good adhesion to NdFeB.

## Conflicts of interest

There are no conflicts to declare.

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