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Enhancing continuous-flow reactions *via* compression-molding of solid catalysts and dilutants in packed-bed systems†

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In this study, we present an improved packed-bed system designed for continuous-flow reactions using platinum (Pt)-black powder and silica gel (SiO_2). The Pt-leaching from the reaction column is suppressed *via* compression-molding of the Pt and SiO_2 . Scanning electron microscopy results and particle-size distribution analysis demonstrate that crushed and downsized SiO_2 is effective in suppressing outflow. Furthermore, we successfully conducted a scaled-up experiment of the flow reaction using a large column, achieving excellent productivity.

Introduction

The continuous-flow (CF) method represents a novel technology that offers several advantages over traditional batch methods. These benefits encompass ease of scalability, enhanced safety, and improved environmental friendliness.^{1–5} In particular, the development of packed-bed flow methods utilizing columns filled with solid catalysts is in high demand.^{6–10} Fine powder catalysts (metal-on-support catalyst, polymer, *etc.*) which are used for the packed-bed flow method are generally premixed with a solid dilutant, such as Celite, silica gel (SiO_2), or metal oxide. This precautionary measure prevents the clogging of the reaction column and the increment of the reaction pressure. We also developed various CF reactions employing the reaction column packed with premixed solid catalysts and dilutants.^{11–13}

Recently, the CF-oxidation of alcohols using hydrogen peroxide (H_2O_2) was developed in a reaction column.¹⁴ This column was packed with platinum (Pt)-black powder and SiO_2 , and equipped with a Teflon column filter. Since H_2O_2 and oxygen gas are a clean oxidant that forms water after oxidation,¹⁵ this flow oxidation is remarkable in terms of environmental friendliness. As part of our efforts to scale up the process, we conducted a preliminary experiment using a large column (inner diameter (ID): 10 mm and length (L): 100 mm). In the previous work we employed a small reaction column (ID: 5 mm, L: 100 mm) in conjunction with *tert*-amyl alcohol (*t*-amylOH) as the solvent. Initially, the substrate and water were simultaneously introduced into the prepared reaction column

packed with Pt-black and SiO_2 before transitioning to the substrate solution and H_2O_2 . For the scaled-up experiment involving a large reaction column (ID: 10 mm, L: 100 mm), only water was introduced into the column before the reaction to avoid the risk of Pt-ignition. Unfortunately, the treatment of the column with water led to the undesired leaching of Pt-black from the reaction column. Based on this result, it was determined that stable operation for scaled-up experiments is infeasible owing to the risk of catalyst leaching and clogging of the column. Our analysis suggests that the leaching occurred due to the void space within the reaction column, which resulted from the disparity in particle size difference between the Pt powder and SiO_2 . Substituting other solid dilutants, such as aluminum oxide and magnesium oxide, for controlling the leaching was not suitable due to the resulting decrease in catalyst reactivities.¹⁴ Consequently, we initiated an investigation into a method for suppressing the leaching of Pt-black powder from the reaction column by diluting it with SiO_2 . The void space can be reduced by packing the column with a catalyst in which Pt is supported on silica. However, with the supported catalyst, Pt is slightly oxidized by silica, which reduces its reactivity.¹⁴ Thus, a method is needed to pack the column without void spaces while maintaining Pt-black in its zero-valency state.

Results and discussion

EDX analysis for the Pt content in the column after the reaction

To confirm the composition of the catalyst in the column before and after the CF-oxidation of alcohols, we performed energy-dispersive X-ray spectroscopy (EDX) for the Pt content in the reaction column (Table 1). Initially, the 0.42 wt% Pt-black powder (particle size: 2–20 μm) and SiO_2 were premixed and

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packed into a glass reaction column (ID: 10 mm, L: 100 mm). The columns were installed in a flow reactor (EYELA, MCR-1000). Following the introduction of only water into the column, the flow reactor was heated to 90 °C, and a 2.0 wt% H₂O₂ aqueous solution and a benzyl alcohol (**1**) solution in *t*-amylOH were pumped to the reaction column at a flow rate of 0.4 mL min⁻¹ for 24 h. Subsequently, the column was cooled to room temperature and rinsed with *t*-amylOH and water. The catalysts were then removed from the column and dried *in vacuo*. Detailed information on the reaction setup and procedures are provided in the ESI.† The Pt content in the column before and after the flow reaction was measured *via* EDX at four different locations (Table 1). When employing the reaction column packed with Pt-black powder and Wakogel C-200 (75–150 µm), the Pt content in the column significantly decreased from 0.42% to 0.07–0.26% after the reaction (entry 1). Notably, the Pt in the column at the inlet side (parts A and B) leached 1.2–2.2 times faster than at the outlet side (parts C and D) considering the ratio of reduction for Pt amount. Afterward, the reaction column was packed with Pt and 60-spherical SiO₂ (SiO₂-60-S, Kanto Chemical Co. Inc.), which has a smaller particle size (40–50 µm) than Wakogel C-200 (entry 2). The leaching of Pt from the reaction column was improved compared with that of Wakogel C-200, although some Pt flowed out even when using SiO₂-60-S.

Compression-molding (CM) is a forming method that provides a desired-shaped powder using a mold with optional pressure.^{16,17} Consequently, we envisaged that Pt could adhere to the solid dilutant, and by employing CM, the void space within Pt and the solid dilutant could be minimized. Premixed Pt and SiO₂-60-S were pressed using a press machine (RIKEN KIKI Co. Ltd., CDM-5PA) and mold (AS ONE CORPORATION, mold for heat press machine φ14) under a pressure of 20 MPa for 2 h. After CM, the resulting cylindrical-shaped solid was crushed, filtrated through a 300 µm-filter, and then packed into the reaction column. Importantly, the amount of Pt remained

unchanged after the reaction within the prepared column (entry 3). Thus, the leaching of Pt during the reaction can be suppressed by CM. On the other hand, using the reaction column that SiO₂-60-S was compression-molded alone and then mixed with Pt, the Pt content decreased after the reaction (entry 4). Therefore, CM of Pt and SiO₂-60-S together was effective for the Pt leaching.

SEM and EDX analysis for catalysts

Scanning electron microscopy (SEM) and EDX mapping of the catalysts were performed to evaluate the impact of CM on Pt and SiO₂-60-S (Fig. 1). At first, SiO₂-60-S exhibited a spherical morphology before CM (Fig. 1(a)); however, after CM, these spherical SiO₂-60-S were crushed (Fig. 1(b)). In the EDX mapping images, SiO₂-60-S appeared orange while Pt was blue (Fig. 1(c) and (d)). These images reveal that a portion of the Pt

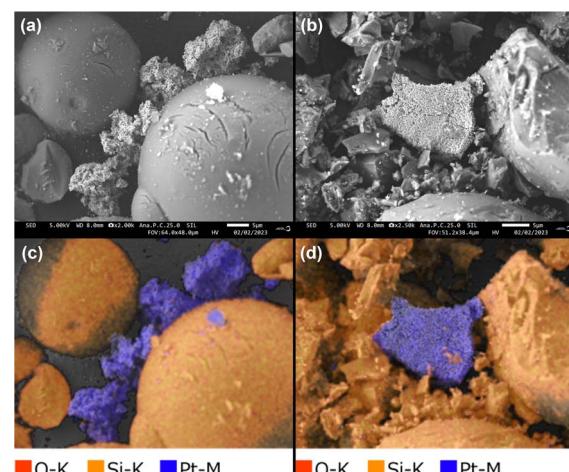
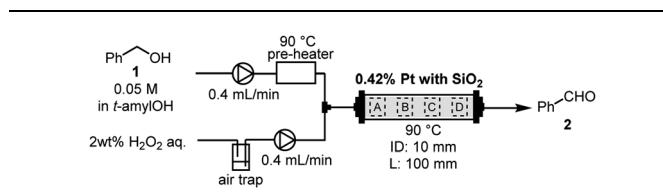


Fig. 1 (a) A scanning electron microscopy (SEM) image of premixed Pt and SiO₂-60-S. (b) A SEM image of compression-molded Pt and SiO₂-60-S. (c) Energy-dispersive X-ray spectroscopy (EDX) mapping of premixed Pt and SiO₂-60-S. (d) EDX mapping of compression-molded Pt and SiO₂-60-S.

Table 1 Energy-dispersive X-ray spectroscopy (EDX) analysis of Pt in the reaction column before and after the continuous-flow (CF) oxidation reaction



Entry	SiO ₂	EDX analysis of the Pt rate (%)			
		A	B	C	D
1	Wakogel C-200	0.07	0.07	0.12	0.26
2	SiO ₂ -60-S	0.32	0.27	0.38	0.31
3 ^a	SiO ₂ -60-S	0.42	0.43	0.42	0.42
4 ^b	SiO ₂ -60-S	0.37	0.26	0.36	0.37

^a Compression-molded Pt with SiO₂-60-S was used. ^b SiO₂-60-S was compression-molded alone and then mixed with Pt.

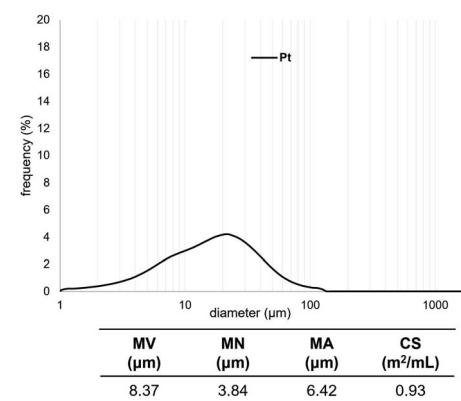


Fig. 2 Particle size distributions of Pt. MV: mean volume diameter, MN: mean number diameter, MA: mean area diameter, CS: specific surface area.



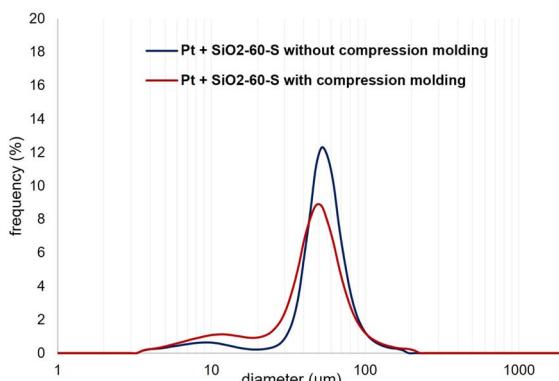


Fig. 3 Particle size distributions of Pt and SiO_2 -60-S without and with compression-molding (CM).

powder was attached to SiO_2 -60-S. Furthermore, we confirmed the void volume of the reaction column packed with Pt and SiO_2 -60-S. The void volume of the reaction column without CM was 6.36 mL, while that with CM was 4.72 mL. Detailed results were provided in the ESI.† The presence of crushed SiO_2 -60-S contributed to a reduction in void space. Consequently, it is evident that the adhesion between Pt and SiO_2 -60-S, coupled with the smaller void space, effectively suppressed the leaching of Pt powder.

Particle-size distribution of catalysts

We measured the particle-size distribution of the SiO_2 -60-S and/or Pt-black powder with and without CM (Fig. 2 and 3). In Fig. 2, the particle-size distribution of only Pt was assessed, revealing particles (derived from Pt) with diameters of approximately 10 μm . Fig. 3 clearly illustrates the differences in the size distribution between SiO_2 -60-S and Pt without CM (the peaks of around 10 μm and 50 μm). Conversely, the difference in particle size SiO_2 -60-S and Pt with CM was small. The particle-size distributions of only SiO_2 -60-S with and without CM are

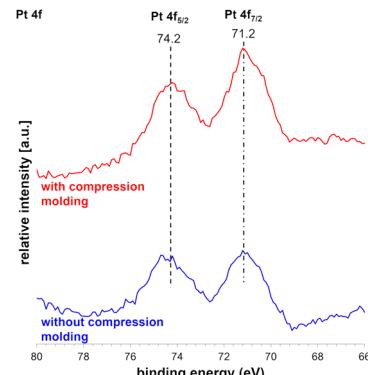


Fig. 4 XPS analysis of Pt and SiO_2 -60-S with and without CM.

provided in the ESI.† Based on the SEM results and particle-size distribution, we concluded that the crushed- and downsized- SiO_2 -60-S effectively suppressed Pt flow from the reaction column during the reaction.

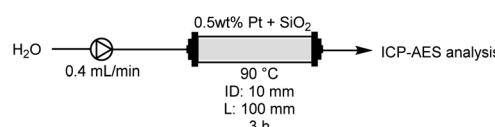
ICP-AES analysis of Pt with/without CM for the CF reaction

We analysed the Pt content after introducing water for 3 h using inductively coupled plasma atomic emission spectroscopy (ICP-AES), with the results shown in Table 2. The analysis employed a flow reactor equipped with a reaction column (ID: 10 mm, L: 100 mm) and a flow reactor (EYELA, MCR-1000). Water was pumped into the reaction column packed with Pt and SiO_2 -60-S at 0.4 mL min^{-1} for 3 h. The solutions that passed through the column for 3 h were subjected to ICP-AES analysis (ESI†). ICP-AES analysis without CM indicated that 0.48 mg (2.66%) of Pt flowed out from the reaction column packed with 17.95 mg of Pt (entry 1). In contrast, when using a column packed with compression-molded catalysts, the rate of Pt leaching from the column considerably reduced to 0.13% (entry 2). This clearly demonstrates the effectiveness of CM of Pt and SiO_2 -60-S in suppressing the flow of Pt powder from the column. The reproducibility of the leaching tests was described in ESI.†

XPS analysis of Pt with/without CM

X-ray photoelectron spectroscopy (XPS) was performed with and without CM of Pt with SiO_2 -60-S catalysts (Fig. 4). The peaks at

Table 2 Inductively coupled plasma atomic emission spectroscopy (ICP-AES) analysis of Pt with/without CM for the CF reaction



ICP-AES analysis of Pt

Entry	CM	Amount of Pt packed in the column	Amount of Pt flowing out	Rate of Pt flowing out from column
1	Without	17.95 mg	0.48 mg	2.66%
2	With	21.20 mg	0.03 mg	0.13%



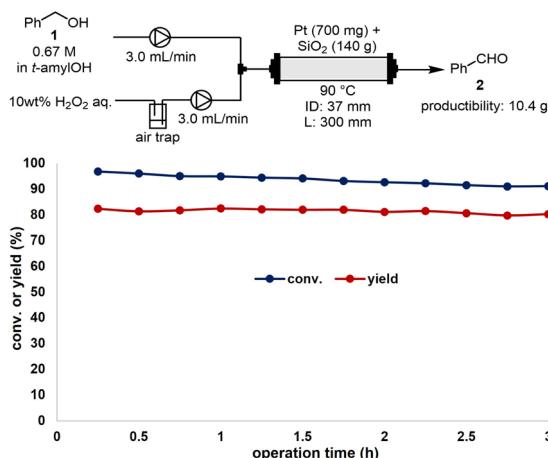


Fig. 5 The scale-up experiment for the CF-oxidation reaction.

71.2 and 74.2 represent the binding energies (BEs) of the CM catalysts, which are ascribed to Pt 4f_{7/2} and Pt 4f_{5/2}, respectively. These values of the Pt 4f peaks were close to 70.9 and 74.2 eV, which were assigned to the BEs of the bulk Pt metal, and the observed peaks corresponded to Pt(0).^{18,19} This indicates that whether compression-molded or not, there was no change in the Pt 4f_{7/2} and Pt 4f_{5/2} peaks, affirming the preservation of Pt(0) even after CM.

Scale-up experiment for the CF-oxidation using compression-molded Pt and SiO₂-60-S

Finally, we conducted a 10 g-scale-up experiment at the laboratory scale for the CF-oxidation reaction of benzyl alcohol (1) to benzaldehyde (2) using compression-molded Pt and SiO₂-60-S (Fig. 5). A stainless-steel (SUS) reaction column (ID: 37 mm, L: 300 mm) and flow reactor (EYELA, HCR-1000) were employed for the bench-scale reaction. The mesh size of the SUS column filter (EYELA, SUS laminated metal filter) was 10 µm. To scale up the CM experiment, a press machine (RIKEN KIKI Co. Ltd., CDM-5PA) and mold (Labonect, LD-3025, φ30 mm × 25 mm) were utilized. Premixed Pt and SiO₂-60-S were pressed at 40 MPa for 2 h to obtain the compression-molded catalysts. A solution of 1 in *t*-amylOH (0.67 M) and 10 wt% of an aqueous H₂O₂ solution were introduced at a flow rate of 3.0 mL min⁻¹ into the reaction column and heated to 90 °C. The yield of 2 was maintained at over 80%, with its productivity being 10.4 g h⁻¹. In comparison, a previous study reported a productivity of 0.7 g h⁻¹ for 2.¹⁴ Thus, a significant fifteen-fold scale-up of the reaction was achieved through the use of a large column (ID: 37 mm, L: 300 mm).

Conclusions

We have successfully developed an improved packed-bed system for CF-oxidation reactions. This system employs a compression-molded Pt-black catalyst and SiO₂-60-S to effectively suppress Pt leaching from the column during reactions. Stable flow oxidation was conducted by utilizing CM. According to the SEM and particle-size distribution results, the crushed-

and downsized-SiO₂-60-S was effective in avoiding Pt leaching. Furthermore, we scaled up the CF-oxidation of benzyl alcohol to benzaldehyde using compression-molded Pt and SiO₂-60-S. This scale-up was performed, resulting in a final productivity of 10.4 g h⁻¹ for benzaldehyde. We believe that our CM method for solid catalysts and dilutants holds great promise for small-to-large-scale experiments of CF reactions because it effectively prevents catalyst leaching from the reaction columns.

Conflicts of interest

There are no conflicts to declare.

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