

Cite this: *Mater. Adv.*, 2024, 5, 1940

## Fabrication and preliminary testing of patterned silver cathodes for proton conducting IT-SOFCs†

Md Shariful Islam Sozal,<sup>id</sup><sup>a</sup> Wenhao Li,<sup>a</sup> Suprabha Das,<sup>a</sup> Borzooye Jafarizadeh,<sup>a</sup> Azmal Huda Chowdhury,<sup>a</sup> Chunlei Wang<sup>b</sup> and Zhe Cheng<sup>\*a</sup>

Dense silver (Ag) cathodes with defined triple phase boundary (TPB between the interface of electrolyte, electrode, and gas) lengths ( $L_{\text{TPB}}$ ) and electrode areas ( $A_{\text{ELT}}$ ) were fabricated by photolithography and E-beam evaporation over a proton conducting  $\text{BaZr}_{0.4}\text{Ce}_{0.4}\text{Y}_{0.1}\text{Yb}_{0.1}\text{O}_{3-\delta}$  (BZCYb4411) electrolyte. A bi-layer lift-off resist method appears to be more versatile than a single layer lift-off resist method for successful patterned cathode fabrication. The electrochemical behaviors of the patterned Ag cathodes over the BZCYb4411 electrolyte were tested by electrochemical impedance spectroscopy (EIS) at different temperatures in atmospheres with different concentrations of  $\text{O}_2$  and  $\text{H}_2\text{O}$ . The results were processed using Distribution of Relaxation Times (DRT) and reaction order analyses and also fitted to equivalent circuits. The directions for future work on patterned electrodes with different  $L_{\text{TPB}}$  and  $A_{\text{ELT}}$  and theoretical calculations to gain further insights into the kinetics and mechanism of the cathode oxygen reduction reaction (ORR) over proton conducting electrolytes are pointed out.

Received 3rd October 2023,  
Accepted 5th January 2024

DOI: 10.1039/d3ma00793f

rsc.li/materials-advances

## Introduction

Solid oxide fuel cells (SOFCs) have been extensively researched for a variety of applications including portable or stationary power generation and transportation.<sup>1–5</sup> The commercialization of conventional SOFCs faces a notable obstacle due to the required high operating temperature – typically  $\sim 700\text{--}1000\text{ }^\circ\text{C}$ . The high operating temperature results in prolonged start-up time and difficulties in ensuring the compatibility and durability of the materials used in the system, leading to a higher than ideal degradation rate.<sup>5,6</sup> To address this challenge, extensive research is currently being conducted on intermediate temperature ( $400\text{--}600\text{ }^\circ\text{C}$ ) solid oxide fuel cells (IT-SOFCs), especially proton conducting (PC) IT SOFCs due to the high ionic conductivities of proton conducting ceramic (PCC) electrolytes at intermediate temperatures.<sup>7–11</sup>

However, when the operating temperature drops, the oxygen reduction reaction (ORR) at the cathode becomes more critical to the efficient functioning of SOFCs. This is due to sluggish ORR kinetics at intermediate temperatures. The cathode reaction processes for oxygen ion conducting SOFCs and proton conducting SOFCs follow different pathways. The cathode ORR

process for conventional SOFCs based on oxygen ion (*i.e.*,  $\text{O}^{2-}$  or  $\text{V}_\text{O}^\bullet$ ) conducting electrolytes would proceed *via* the pathway of oxygen vacancies.<sup>12,13</sup>



The ORR for oxygen ion conducting SOFCs includes elementary steps such as oxygen adsorption, oxygen dissociation, charge transfer, and mass transfer of oxide ions into the bulk of the electrolyte.<sup>12,13</sup> The mechanism of the ORR *via* the oxygen vacancy pathway has been extensively studied using various approaches, including the use of cells with patterned electrodes over oxygen ion conducting electrolytes. In comparison, the cathode ORR process for proton conducting SOFCs would proceed *via* a different pathway, as described below:<sup>12,13</sup>



which involves protons (or protonated oxygen,  $((\text{OH})_o^\bullet)$  and water). The ORR of proton conducting SOFCs involves even more elementary steps including oxygen adsorption, oxygen dissociation, surface diffusion, charge transfer, mass transfer of protons into the bulk of the electrolyte, and water formation and desorption.<sup>12–15</sup> A previous study conducted by He *et al.* analysed the reaction order of the ORR of proton conducting SOFCs (*i.e.*, dependence of the reaction rate on atmospheres such as  $p\text{O}_2$  and  $p\text{H}_2\text{O}$ ) by hypothesizing eight elemental steps,<sup>14</sup> while the study conducted by Grimaud *et al.* assumed 6 elemental steps.<sup>15</sup> However, despite numerous studies, there

<sup>a</sup> Department of Mechanical and Materials Engineering, Florida International University, Miami, FL, 33174, USA. E-mail: zhcheng@fiu.edu

<sup>b</sup> Department of Mechanical and Aerospace Engineering, University of Miami, Miami, FL, 33146, USA

† Electronic supplementary information (ESI) available. See DOI: <https://doi.org/10.1039/d3ma00793f>



are still aspects of the ORR mechanism of proton conducting SOFCs that remain uncertain.

On the other hand, a classical approach for understanding electrode reactions, including the ORR, was offered by dense patterned electrodes as mentioned.<sup>16–29</sup> The utilization of patterned electrodes enables precise control of both the length of the triple phase boundary (TPB) and the area of the electrode, linking electrode geometry with reaction kinetics. Significant research has been carried out on the electrode reaction mechanism in conventional oxygen ion conducting SOFCs utilizing patterned electrodes made of noble metals such as platinum (Pt) or silver (Ag).<sup>16,19–21,23,26–28</sup> Previous studies showed that for Pt, ORR kinetics was correlated with the length of the TPB.<sup>20,23,27,28</sup> In contrast, Ag is less expensive and has a higher electronic conductivity than Pt. One study showed that an SOFC with a patterned Ag cathode exhibited comparable performance to that with the Pt cathode with an identical design.<sup>21</sup> Another study showed that the rate-limiting step of the Ag cathode reaction for oxygen ion conducting SOFCs is the bulk diffusion through the Ag electrode at 70–900 °C.<sup>16</sup> A subsequent study reported that at 350–550 °C, dissociative oxygen adsorption/reduction might be the rate limiting steps of the Ag cathode reaction for oxygen ion conducting SOFCs.<sup>30</sup>

However, for proton conducting IT-SOFCs, despite their recent development, there is no study carried out utilizing the patterned electrode approach except for the study conducted by Haile *et al.*<sup>31</sup> who used  $\text{PrBa}_{0.5}\text{Sr}_{0.5}\text{Co}_{1.5}\text{Fe}_{0.5}\text{O}_{5+\delta}$ , a PBSCF mixed conducting cathode. It is expected that a simpler patterned Ag electrode over a proton conducting electrolyte will be very valuable to help identify the reaction site (*i.e.*, at the TPB or cathode surface) and clarify if the proton conducting ceramic electrolyte plays any electro-catalytic role in the ORR reaction. Therefore, this study aims to fabricate patterned Ag cathodes on a proton conductive  $\text{BaZr}_{0.4}\text{Ce}_{0.4}\text{Y}_{0.1}\text{Yb}_{0.1}\text{O}_{3-\delta}$  (BZCYYb4411) electrolyte. Preliminary testing of the patterned electrode cells has been carried out showing the effects of moisture ( $\text{H}_2\text{O}$ ) and oxygen ( $\text{O}_2$ ) concentration on measured electrochemical behaviors. The implications of the preliminary study and the directions for subsequent research have also been discussed.

## Experimental

### Powder synthesis, sintering, and polishing

In this study, BZCYYb4411 proton conducting ceramic electrolyte and  $\text{PrNi}_{0.5}\text{Co}_{0.5}\text{O}_{3-\delta}$  (PNC, as the counter electrode) powders were synthesized using the Pechini method,<sup>32</sup> and the details have been described previously.<sup>32</sup> To fabricate the proton conducting electrolyte pellet, 0.4 g of BZCYYb4411 powder containing 0.5 wt% NiO as a sintering aid was pressed using a 13 mm die with a pressure of ~300 MPa. The green pellet was sintered at 1550 °C for 10 h in air under protective conditions, as previously described.<sup>32</sup> Subsequently, BZCYYb4411 pellets were subjected to grinding on both surfaces using silicon carbide abrasive papers of varying grit numbers from 600 to 1200. Finally, the samples underwent a polishing procedure using

diamond suspensions of 1, 0.1, and 0.05  $\mu\text{m}$  in succession. The thickness of the polished BZCYYb4411 pellet is ~0.5 mm.

### Photolithography for fabrication of patterned Ag electrodes

Photolithography is a microfabrication technique that uses a photomask to transfer a pre-defined pattern onto a substrate surface through a series of steps. It is widely used in integrated circuit (IC) and sensor fabrication. In the past two decades, photolithography was also used in the fabrication of patterned electrodes for oxygen ion-conducting SOFCs.<sup>16,18,19,22–25,27–29,33–36</sup> However, most previous studies did not provide adequate details of the fabrication process, making the reproduction and further fine-tuning of the patterned electrode difficult. Meanwhile, as stated, there have been no studies on the fabrication of patterned electrodes over proton conducting electrolytes except for the study conducted by Haile *et al.*<sup>31</sup> Therefore, a comprehensive description of the techniques and procedures used for the fabrication of patterned Ag electrodes over the BZCYYb4411 electrolyte is given below in detail.

First, a blank photomask was purchased from Nano film and it consisted of three layers: a top surface layer of a positive photoresist, followed by a layer of chromium and a glass substrate, which is transparent to UV light. The desired pattern for the mask was designed using the LayoutEditor software (free version, 20230301) and subsequently transferred onto the mask by exposing the photoresist layer using a laser mask writer ( $\mu\text{PG}$  101, a wavelength of 405 nm), as illustrated in Fig. 1(a). The laser power used for exposure was 4.8 mW. Following the exposure, the mask was developed using a developer solution (AZ400K (15% potassium borate/85% water):water = 1:4 by volume) to remove the laser-exposed positive photoresist, which resulted in openings in the photoresist layer exposing the chromium layer according to the designed pattern. The exposed chromium was subsequently etched away by immersing the mask in Chromium Etch 1020 AC (containing nitric acid, ceric ammonium nitrate, water; exact concentration is unknown as this is a commercial product) for 3 min, and the pattern was transferred onto the glass. Finally, the remaining photoresist was removed through reactive ion etching by oxygen plasma, thus completing the fabrication of the mask as shown in Fig. 1.

After the photomask is patterned, the subsequent step involves transferring the pattern onto the substrate coated with a photoresist layer. The photoresist comes in two forms, positive or negative. A positive photoresist, upon UV light exposure, undergoes molecular chain breakage and becomes more soluble in the developer solution.<sup>35,37</sup> As a result, after development, the regions exposed to UV light undergo material removal/dissolution, leaving the unexposed regions intact and insoluble in the developer solution. In comparison, a negative photoresist, upon UV light exposure, experiences polymerization and becomes insoluble in the developer solution. Thus, after development, the regions exposed to UV light remain on the substrate.<sup>35,37</sup> Due to the disparity in light dosage between the top and bottom layers, with the top layer experiencing a higher dose, positive photoresists tend to produce overcut profiles (*i.e.*, the opening at the photoresist top surface is wider



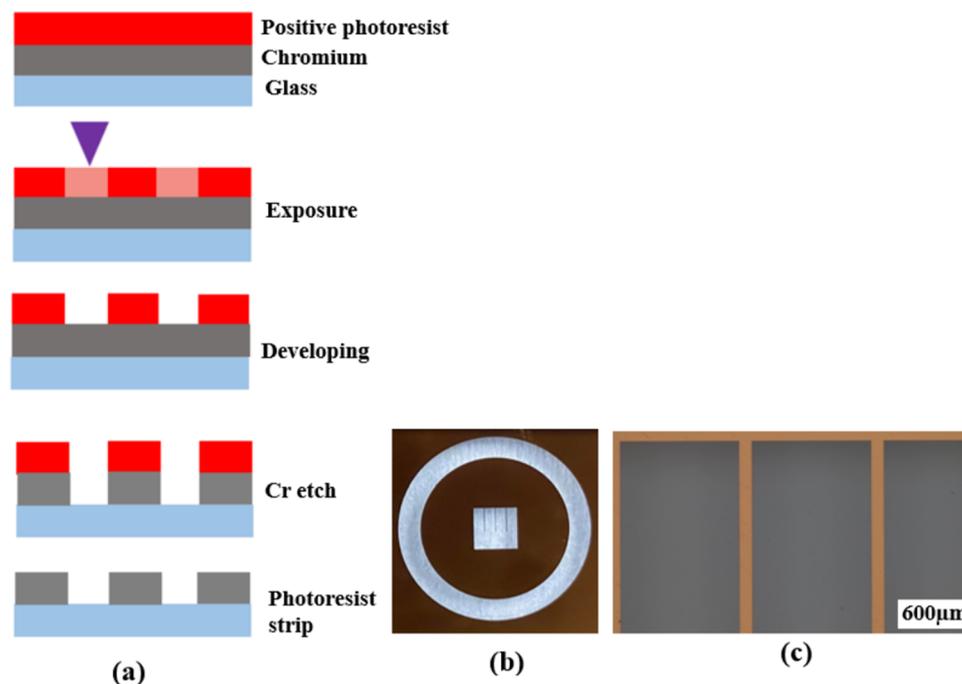


Fig. 1 (a) Schematic representation of the fabrication process of the photomask, (b) photograph of the final photomask, (c) and the microscopic image of the photomask, showing the fine features and patterns.

than at the bottom or near the substrate), while negative photoresists tend to produce undercut profiles (*i.e.*, the opening at the photoresist top surface is narrower than at the bottom or near the substrate),<sup>38,39</sup> after the development process, as depicted in Fig. 2(a) and (b).

Because of the difference in the sidewall profile, the lift-off process (*i.e.*, the removal of the residual photoresist after metal

deposition) is easier when using a negative photoresist than when using a positive photoresist, as the negative photoresist prevents the metal from accumulating on the walls of the resist after deposition.<sup>39</sup> However, a negative photoresist often has lower resolution compared to a positive photoresist. This is because for the negative photoresist, the developer solution tends to infiltrate both the UV-exposed and unexposed areas,

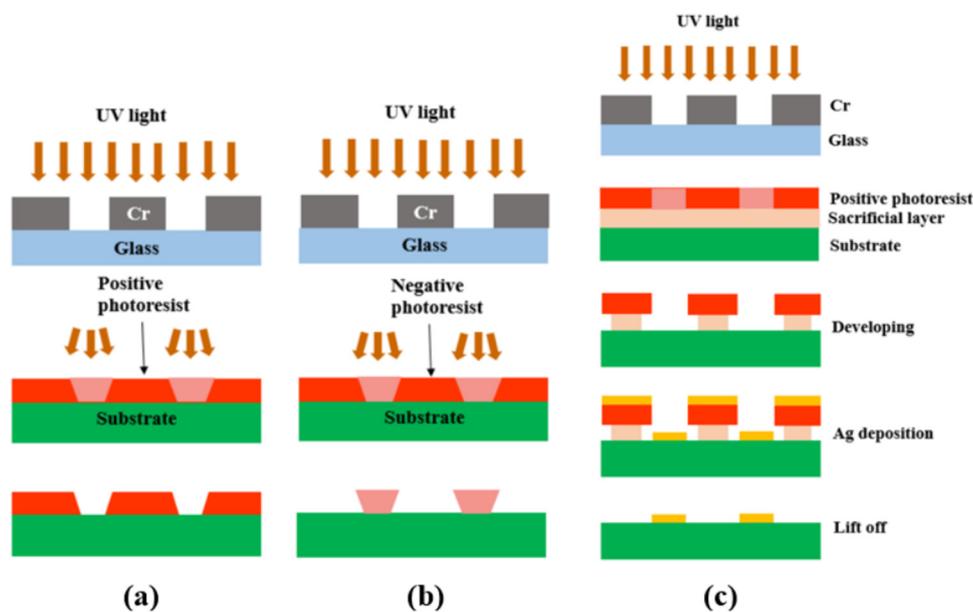


Fig. 2 Schematic showing (a) the overcut profile formed in a positive photoresist, with wider opening at the photoresist top surface than at the bottom or near the substrate,<sup>39</sup> (b) the undercut profile formed in a negative photoresist, with narrower opening at the photoresist top surface than at the bottom or near the substrate,<sup>39</sup> and (c) the photolithography process using a bilayer resist system.



which results in reduced resolution or pattern distortion.<sup>40–42</sup> On the contrary, a positive photoresist is capable of maintaining its high-resolution pattern unless it is overdeveloped (by being left in the developer solution longer than necessary). Therefore, in this study, a positive photoresist was chosen.

To achieve effective lift-off in photolithography with a positive photoresist, the use of a bilayer resist system composed of a bottom sacrificial layer and a top imaging photoresist layer was found to be crucial in this study.<sup>35,43</sup> Although the sacrificial layer lacks photo-reactivity, it creates undercut during development due to its *higher* dissolution rate than the top imaging photoresist layer. This enables the successful removal of the resists after Ag electrode deposition, as demonstrated in Fig. 2(c). Without this bilayer approach, the lift-off process is challenging due to accumulation of the metal on the walls of the resist after deposition. Therefore, in this study, patterned Ag electrodes were fabricated over BZCYYb4411 electrolyte substrates using photolithography with a bilayer resist system.

Prior to the photolithography process, polished BZCYYb4411 substrates underwent cleaning with IPA, acetone, and DI water, followed by a dehydration bake at 170 °C for 10 min to improve the adhesion of the resist with the substrate. LOR 3B, a sacrificial layer, was spin-coated onto the cleaned substrates using the following parameters: 500 rpm for 10 s, 1000 rpm for 10 s, 1500 rpm for 10 s, and 2000 rpm for 120 s. Subsequently, the sacrificial layer underwent a soft bake process at 141 °C for 90 s to eliminate the solvent and improve its adhesion to the substrate. Then, AZ1518, a positive photoresist, was spin-coated over the LOR 3B sacrificial layer on the BZCYYb4411 substrate, using the same spinning parameters. Afterward, the photoresist underwent a soft bake process at 110 °C for 90 s to eliminate solvents and improve its adhesion to the sacrificial layer. Subsequently, the substrates were exposed to UV light of 150 mJ cm<sup>-2</sup> to form the pattern. The photoresist was developed in AZ400K developer solution to form the pattern in the photoresist layer (as well as the bottom sacrificial layer, with undercut) over the electrolyte (see Fig. 3 for photos), which was necessary for subsequent Ag electrode deposition.

In microfabrication, metals are deposited commonly by two techniques: E-beam evaporation and sputtering. In E-beam evaporation, metal deposition is unidirectional as the mean free path of metal atoms is longer than the distance

between the substrate and the target due to high vacuum ( $\sim 10^{-7}$  Torr).<sup>35,37,39</sup> This results in minimal sidewall deposition and effective lift-off. In sputtering, the lower vacuum ( $\sim 10^{-3}$  Torr) causes a shorter mean free path, leading to non-unidirectional deposition with more sidewall coverage and challenges in lift-off.<sup>35,37,39</sup> In this study, an  $\sim 75$  nm thick Ag layer was deposited onto the BZCYYb4411 substrates by E-beam evaporation (base pressure:  $5 \times 10^{-6}$  Torr, soak-1 power: 12%, rise-1 time: 5 min, soak-1 time: 30 s; soak-2 power: 14%, rise-2 time: 10 s, and soak-2 time: 30 s). Finally, the lift-off of the remaining photoresist was carried out using Remover PG (*N*-methyl pyrrolidone) at  $\sim 70$  °C. Microstructural analysis and the EDS line scan of the patterned Ag electrodes over the BZCYYb4411 electrolyte substrate were done using a scanning electron microscope (SEM JEOL JSM-F100) equipped with an energy dispersive X-ray spectrometer (EDS).

### Electrochemical cell fabrication and test

In this study, electrochemical cells with patterned Ag working electrodes were fabricated using PNC as the counter electrode. To fabricate cells, fritless Ag paste was first brush painted on the contact pad of the patterned Ag electrode over the BZCYYb4411 electrolyte and dried. PNC slurry was then brushed onto the opposite side of the electrolyte, as previously discussed, to form the PNC counter electrode, followed by the application of Ag paste over the PNC electrode for current collection.<sup>32</sup> The cell then underwent heat treatment at 600 °C for 2 h in simulated air (ultra-zero grade, Airgas, <5 ppm H<sub>2</sub>O and CO<sub>2</sub> by volume).

Following the heat treatment at 600 °C for 2 h, electrochemical impedance spectroscopy (EIS) tests were conducted using a potentiostat (Gamry Interface 1000) without any DC bias in a frequency range of 10<sup>6</sup> to 10<sup>-2</sup> Hz at 400 to 600 °C. The AC amplitude used was 0.1 mA. The effect of oxygen partial pressure was tested by varying the flow rate of pure O<sub>2</sub> *versus* pure N<sub>2</sub> using mass flow controllers to achieve *p*O<sub>2</sub> values of 0.1, 0.2, 0.5, and 1 atm, while the effect of H<sub>2</sub>O was tested by passing the simulated air through a water bubbler at room temperature and 66 °C to achieve *p*H<sub>2</sub>O values of  $\sim 0.03$  and  $\sim 0.26$  atm, respectively. Each time the atmosphere was changed, and there was a typical delay of 2.5 h before the electrochemical measurements could be taken. (Such a delay was based on our previous experiments, which showed that the impedance stabilized after a similar time. On the other hand, from the gas flow point of view, this delay was also reasonable because the total flow rate was maintained at 40 cc min<sup>-1</sup>. Over 2.5 h, the total flow volume is 6000 cc, which is much larger than the test chamber volume of  $\sim 100$  cc (2.5 cm ID, 20 cm long).)

## Results and discussion

### Fabricated patterned electrode cell

Fig. 4(a) and (b) show the LayoutEditor design and a photograph, respectively, of a patterned Ag electrode fabricated over

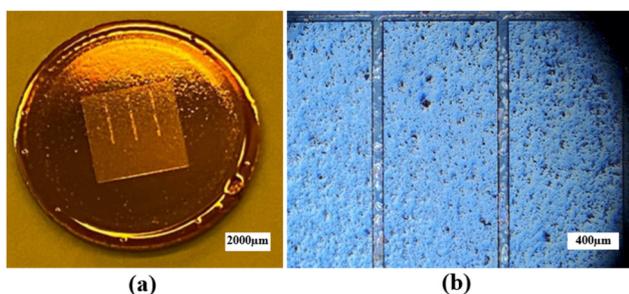


Fig. 3 (a) Photograph and (b) optical microscopic image of the BZCYYb4411 electrolyte substrate covered by a patterned photoresist after development.



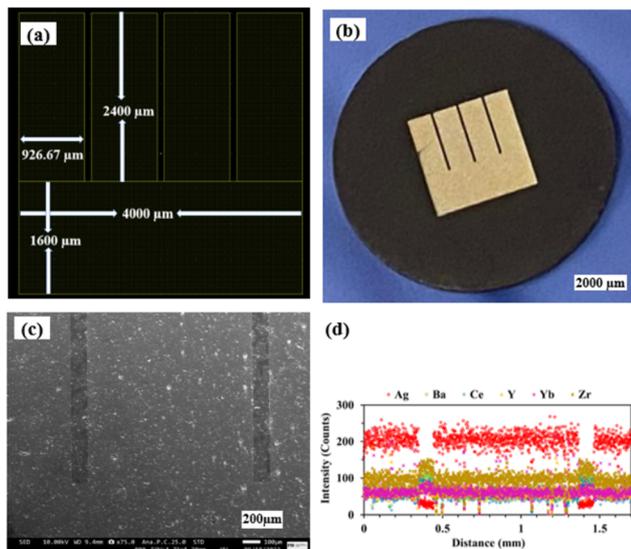


Fig. 4 (a) The LayoutEditor design, (b) photograph, (c) SEM micrograph, and (d) EDS line scan of the patterned Ag electrode over the BZCYYb4411 electrolyte substrate.

the BZCYYb4411 proton conducting electrolyte. The pattern has 4 long fingers and a wide busbar for current collection. The designed TPB length ( $L_{TPB}$ ) and the electrode area ( $A_{ELT}$ ) were 30.4 mm and 15.3 mm<sup>2</sup>, respectively. Fig. 4(c) and (d) show the corresponding SEM micrograph and EDS line scan, respectively, of such a sample. The silver electrode is reasonably dense considering its thickness of only  $\sim 75$  nm.

### Preliminary electrochemical test of a patterned Ag electrode cell

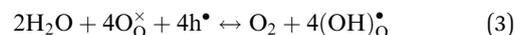
Fig. 5 shows the impedance spectra of a patterned silver electrode cell with the PNC counter electrode in simulated air ( $< 5$  ppm H<sub>2</sub>O and CO<sub>2</sub> by volume, according to Airgas) as well as humidified air with  $p_{H_2O}$  values of 0.03 and 0.26 atm at 600–450 °C. A previous study conducted by the authors<sup>32</sup> has shown that a porous PNC cathode over the same proton conducting electrolyte has a much lower interfacial resistance (about one tenth), which, as a first approximation, allows us to neglect the contribution of the PNC counter electrode in the current patterned Ag electrode cell.

On the other hand, in comparison with simulated air, the addition of 0.03 atm H<sub>2</sub>O resulted in the reduction of ohmic resistance ( $R_O$ , the high frequency intercept in the impedance spectra), indicating higher bulk conductivity, particularly at temperatures of 600 and 550 °C. This is attributed to the hydration of the BZCYYb4411 electrolyte and formation of protons (OH)<sub>O</sub><sup>•</sup> from oxygen vacancies, leading to higher ionic conductivity.<sup>9,32</sup> As  $p_{H_2O}$  further increased to 0.26 atm, there was almost no further change in  $R_O$ , indicating the saturation of hydration at 0.03 atm.

The electrode interfacial process can roughly be separated into two parts: a high-frequency resistance corresponding to the high frequency (HF) loops ( $\sim 10^6$  to  $10^4$  Hz) and a mid-to-low frequency (MF-LF) resistance corresponding to multiple,

partially overlapping loops in the mid to low frequency ( $\sim 10^4$  to  $10^{-3}$  Hz) range. With the introduction of 0.03 atm moisture, the HF loops of the EIS decreased at all temperatures from 600 to 450 °C. With increase of  $p_{H_2O}$  to 0.26 atm, the HF loops decreased further, especially at a lower temperature of 500 °C or 450 °C. It is natural to expect that, in a simulated air atmosphere with very little moisture, the ORR would proceed *via* the oxygen vacancy pathway (eqn (1)), while after the introduction of moisture and full hydration of the proton-conducting electrolyte, the ORR would proceed *via* the proton pathway (eqn (2)). It is hypothesized that the charge transfer step, as often believed to be represented by the HF loops in the EIS, might be intrinsically faster for the proton route than the oxygen vacancy route. Such a hypothesis is consistent with earlier observations of depressed HF loops with increasing  $p_{H_2O}$  for the BSCF cathode over the proton conducting electrolyte.<sup>12</sup>

On the other hand, with the introduction of moisture, the total apparent electrode interfacial resistance,  $R_{ai}$  (*i.e.*, the direct difference between the high and low frequency intercepts on the impedance spectra) actually increased significantly, primarily due to the large expansion of the mid-to-low frequency MF-LF loops, and the increase was more significant when the moisture content was higher (0.26 atm. *vs.* 0.03 atm.). One possible explanation for such an observation is related to the reduced shorting effect based on the defect reaction involving electron holes (h<sup>•</sup>) and protonic defects



where an increase in  $p_{H_2O}$  will shift the reaction to the right and reduce electron hole concentration, decreasing electronic leakage through the electrolyte.<sup>44</sup> Previous studies have shown that electronic leakage through proton conducting electrolytes, such as Y-doped BaCeO<sub>3</sub> and BaZr<sub>x</sub>Ce<sub>1-x</sub>O<sub>3</sub>, causes the apparent interfacial resistance  $R_{ai}$  to be smaller than the actual values, particularly at high temperatures and high  $p_{O_2}$ .<sup>45,46</sup> As a result, reduced electronic leakage due to moisture introduction and hydration of the electrolyte would cause  $R_{ai}$  to increase, even though the electrode kinetics might remain largely the same.<sup>44,45</sup> Another possibility is that, since the MF-LF loops in EIS are commonly associated with O<sub>2</sub> adsorption and dissociation processes,<sup>12,13</sup> their observed increase may be attributed to the blockage of surface reaction sites by adsorbed H<sub>2</sub>O molecules – in this case, near the TPB between the Ag electrode and the BZCYYb4411 electrolyte, which reduces the active sites for O<sub>2</sub> adsorption and dissociation. Which of the two explanations plays the dominant role needs to be investigated in the future. It is worth mentioning that the Warburg-like behavior is observed at lower temperatures of 500 and 450 °C under different atmospheric conditions, as well as at a higher temperature of 550 °C with a higher  $p_{H_2O}$  content of 0.26 atm. Warburg lines are often associated with diffusion (*i.e.*, mass transport) limitations. At lower operating temperature (*e.g.*, 450 °C) or with higher  $p_{H_2O}$  content (*e.g.*,  $p_{H_2O} = 0.26$  atm.), it is hypothesized that the availability of oxygen atoms becomes limited, possibly resulting from slower oxygen dissociation or surface diffusion (*e.g.*, to the TPB), which results



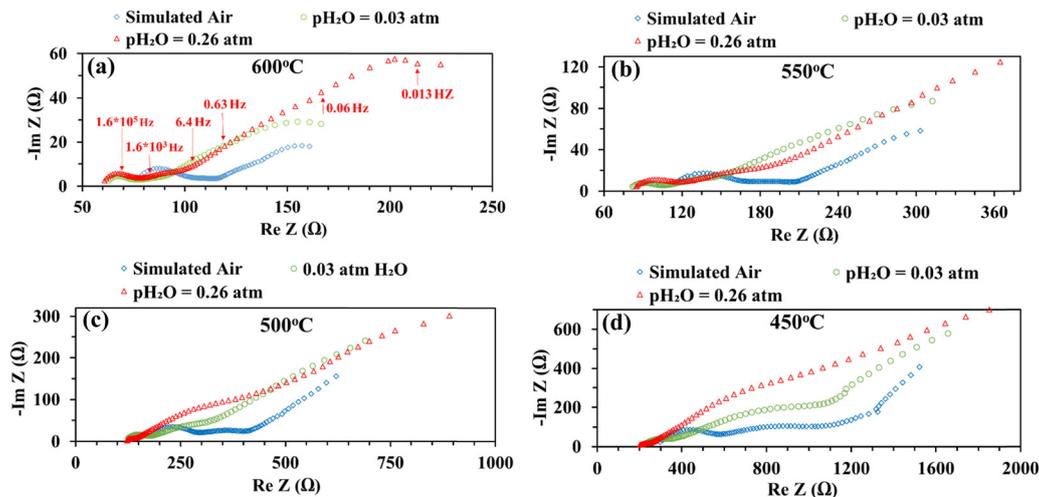


Fig. 5 Plots of EIS for an electrochemical cell with a patterned Ag working electrode over the BZCYYb4411 proton conducting electrolyte and the PNC counter electrode in simulated air and at various  $\text{pH}_2\text{O}$  levels of 0.03 and 0.26 atm at (a) 600, (b) 550, (c) 500, and (d) 450 °C, respectively.

in the Warburg-like behavior. Of course, additional studies, especially computational modeling, are needed to test such a hypothesis.

The impedance spectra are further analyzed using the Distribution of Relaxation Times (DRT) method,<sup>47–54</sup> as shown in Fig. 6. Multiple peaks (7+) are observed across different frequency ranges. Consistent observation (*i.e.*, multiple processes for the electrode reaction) is obtained by fitting the EIS data to the equivalent circuit using the ZView software. ESI,† Fig. S1 shows the fittings for the EIS plot at 550 °C in simulated air with water addition at  $\text{pH}_2\text{O} = 0.03 \text{ atm}$ , considering 4, 6, 7, and 8 RC circuits. It appears that 8 RC circuits provide the best fit, while 4 RC gives the worst fitting. ESI,† Fig. S3 shows the fittings for the EIS plot in simulated air with water addition at  $\text{pH}_2\text{O} = 0.03 \text{ atm}$  and at 600–450 °C. The fitted equivalent circuits turn out to contain 8–9 RC circuits in series. Such a number of RC elements seem to be high but still reasonable given the DRT plots in Fig. 6 showing 7+ peaks. The high number is also possible due to the complex nature of the 4-electron ORR process and the many elemental steps that may be involved, as suggested in earlier studies.<sup>14,15</sup>

On the other hand, there are still significant uncertainties in fittings. In addition, linking the elemental steps of the electrode reaction with the different peaks in DRT or the semi-circles in EIS is difficult due to the complex nature of the ORR process. In fact, with the limited information currently available, it is impossible at this stage. Therefore, both experiments and theoretical modeling are currently underway to deepen the understanding of the cathode ORR processes for proton conducting SOFCs.

Nevertheless, Fig. 7(a) shows electrode interfacial conductance,  $1/R_{\text{ai}}$ , normalized by the TPB length *vs.* inverse of temperature (*i.e.*,  $1/T$ ) for the patterned Ag electrode over the BZCYYb4411 proton conducting electrolyte in simulated air and in air with  $\text{pH}_2\text{O}$  values of 0.03 and 0.26 atm at 600–450 °C. For comparison, data from previous studies conducted

by Herle *et al.*<sup>16</sup> and Huang *et al.*<sup>30</sup> on patterned Ag electrodes in air over a conventional oxygen ion conducting yttria-stabilized zirconia (YSZ) electrolyte are also plotted. Despite the many differences between the current study and the one conducted by Herle *et al.*,<sup>16</sup> *i.e.*, silver pattern geometry, electrolyte type (BZCYYb4411 proton conducting electrolyte *vs.* YSZ oxygen ion conducting electrolyte), and testing temperature, the measured interfacial conductance ( $1/R_{\text{ai}}$ ) normalized by the TPB length appears to roughly follow the same trend for silver electrodes. In contrast, Huang *et al.*<sup>30</sup> showed better activity of the patterned Ag electrode on YSZ from 550 °C down to 450 °C. Additionally, the activation energy determined in the current study is 0.93–0.98 eV, much lower than those proposed by Herle *et al.*<sup>16</sup> (1.19 eV) and Huang *et al.*<sup>30</sup> (1.65 eV) for patterned Ag electrodes over an oxygen ion conducting YSZ electrolyte. This suggests the potentially better activity of the patterned Ag electrode at a temperature below 450 °C over the proton conducting BZCYYb4411 electrolyte than the YSZ electrolyte. A further study is needed to verify this.

To gain additional insights into the reaction process including possible rate limiting steps, reaction order analysis is often carried out.<sup>14,15,55–60</sup> Such an analysis may provide information regarding the influence of different reactants' activity, such as the partial pressures of oxygen ( $p_{\text{O}_2}$ ) and water vapor ( $\text{pH}_2\text{O}$ ), on the rate of the ORR. According to the literature, the overall reaction rate or the inverse of electrode apparent interfacial resistance depends on oxygen and water vapor pressure:  $1/R_{\text{ai}} \propto (p_{\text{O}_2})^n \cdot (\text{pH}_2\text{O})^m$ , where  $n$  and  $m$  are the reaction orders of  $p_{\text{O}_2}$  and  $\text{pH}_2\text{O}$ , respectively. The cathode reaction involves several fundamental steps for proton conducting SOFCs: (1) oxygen adsorption, (2) oxygen dissociation, (3) charge transfer (multiple steps, actually), (4) water formation, and (5) desorption of water.<sup>14,15</sup> By plotting  $1/R_{\text{ai}}$  against  $p_{\text{O}_2}$  or  $\text{pH}_2\text{O}$  (both on the logarithmic scale), the reaction order (the  $n$  or  $m$  value) might be obtained from the fitted slope of the plot. Fig. 7(b) shows plots of  $\log(1/(R_{\text{ai}} \times L_{\text{TPB}}))$  *vs.*  $\log(\text{pH}_2\text{O})$  for the patterned Ag



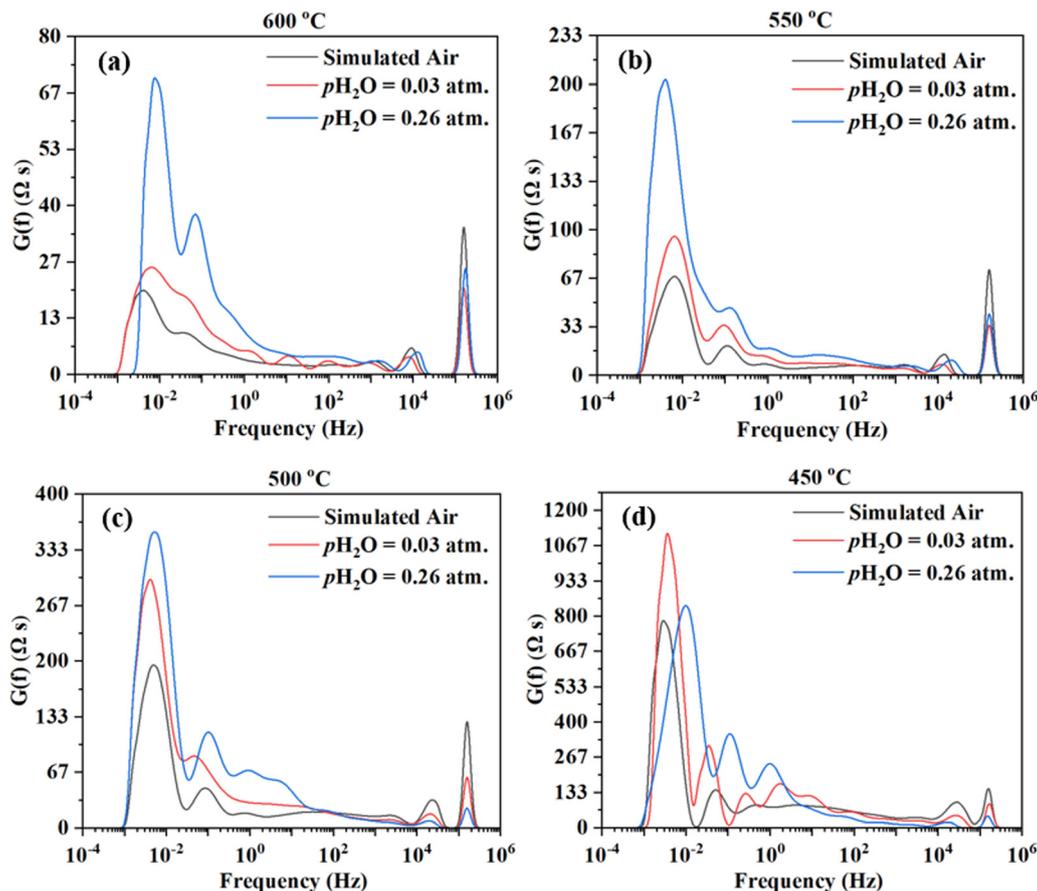


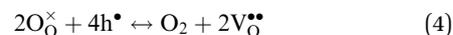
Fig. 6 Distribution of relaxation times (DRT) curves from the impedance spectra of an electrochemical cell with the patterned Ag working electrode, the BZCYYb4411 proton conducting electrolyte, and the PNC counter electrode in simulated air (< 5 ppm  $\text{H}_2\text{O}$  and  $\text{CO}_2$  according to Airgas) and with added  $p_{\text{H}_2\text{O}}$  at 0.03 and 0.26 atm and at (a) 600, (b) 550, (c) 500, and (d) 450 °C, respectively.

cathode at different temperatures from 600 to 450 °C. The obtained reaction order with respect to  $p_{\text{H}_2\text{O}}$ ,  $m$ , is  $-0.14$  to  $-0.22$ . These values fall outside the range of  $m$  (0.5–1) modeled in previous studies. On the other hand, these values are very close to the value ( $-0.21$ ) obtained for the  $\text{La}_{0.6}\text{Sr}_{0.4}\text{Co}_{0.2}\text{Fe}_{0.8}\text{O}_{3-\delta}$  (LSCF) cathode over the  $\text{BaCe}_{0.9}\text{Y}_{0.1}\text{O}_{3-\delta}$  (BCY10) proton conducting electrolyte at 600 °C.<sup>15</sup> Whether such consistency is pure co-incidence given the difference in electrode and electrolyte materials or the two cells are indeed limited by the same fundamental process (e.g., the electronic leakage effect in the proton conducting electrolyte) needs to be studied in the future.

Fig. 8 shows the impedance spectra of the patterned Ag electrode cell at various  $p_{\text{O}_2}$  (0.1, 0.2, 0.5, and 1 atm) at 600–450 °C. The bulk or ohmic resistance decreases with increasing temperature, which is expected for solid oxide fuel cells. The primary factor contributing to the observed drop in ohmic resistance with increasing temperature is the higher mobility of the charge carriers (oxygen vacancies or protons, if water is present) at higher temperature. It is also expected that the cell's ohmic resistance will be independent of the electrode's architecture, whether porous or dense, but should decrease with temperature. This was indeed observed in the current study: the

area corrected ohmic resistance of the patterned Ag electrode cell matched very well with our earlier study using a porous electrode over the same  $\text{BaZr}_{0.4}\text{Ce}_{0.4}\text{Y}_{0.1}\text{Yb}_{0.1}\text{O}_{3-\delta}$  (BZCYYb4411) electrolyte.<sup>32</sup>

On the other hand, at 600 and 550 °C, ohmic resistance  $R_{\text{O}}$  increased as  $p_{\text{O}_2}$  decreased from 1 to 0.1 atm, which was attributed to the decrease in the electronic conduction (or leakage) of the BZCYYb4411 electrolyte resulting from a drop in  $p_{\text{O}_2}$ : based on the defect reaction involving oxygen vacancies and electron holes:



a drop in  $p_{\text{O}_2}$  would shift the reaction to the right and reduce electron hole concentration. At 500 and 450 °C, there is almost no change in  $R_{\text{O}}$ . This is likely because hole conduction is significantly less at lower temperature for electrolytes that display electronic leakage (e.g., acceptor-doped  $\text{CeO}_2$  and  $\text{BaCeO}_3$ ).<sup>46</sup> (In comparison, previous studies have shown that a small change in  $p_{\text{O}_2}$  has no obvious effect on  $R_{\text{O}}$  for the oxygen ion-conducting YSZ electrolyte, as the electronic conduction in YSZ is negligible under similar conditions.<sup>28,61</sup>)

Meanwhile, with reduced  $p_{\text{O}_2}$ , there is an increase in total apparent electrode interfacial resistance  $R_{\text{ai}}$ . Such a behavior



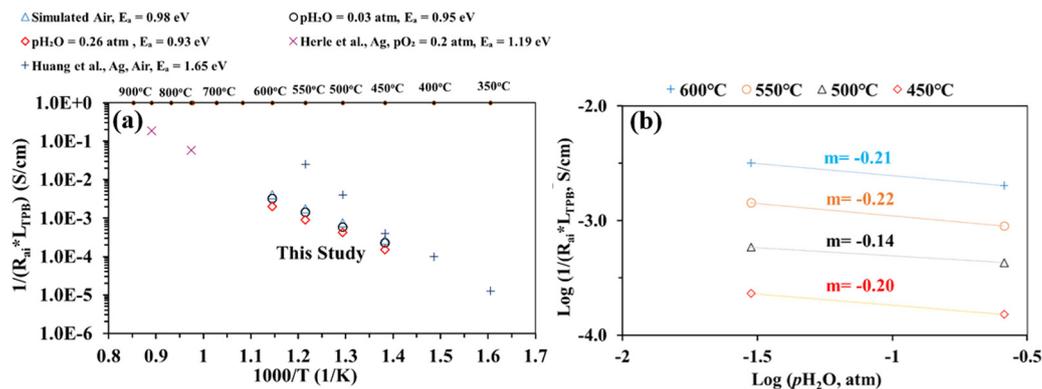


Fig. 7 (a) Plot of inverse of  $R_{ai}$  normalized by the TPB length versus inverse temperature for the patterned Ag electrode cell over the BZCYYb4411 proton conducting electrolyte in simulated air and in air with  $p_{H_2O}$  values of 0.03 and 0.26 atm at 600–450 °C. The results obtained from previous studies conducted by Herle *et al.*<sup>16</sup> and Huang *et al.*<sup>30</sup> on patterned Ag electrodes, all in air over the oxygen ion conducting yttria-stabilized zirconia (YSZ) electrolyte are also shown for comparison. (b) Inverse of  $R_{ai}$  normalized by the TPB length vs.  $p_{H_2O}$  plot, both on the logarithmic scale, showing the fitted reaction order  $m$  with respect to  $p_{H_2O}$  for the patterned Ag cathode over the BZCYYb4411 electrolyte at 600–450 °C.

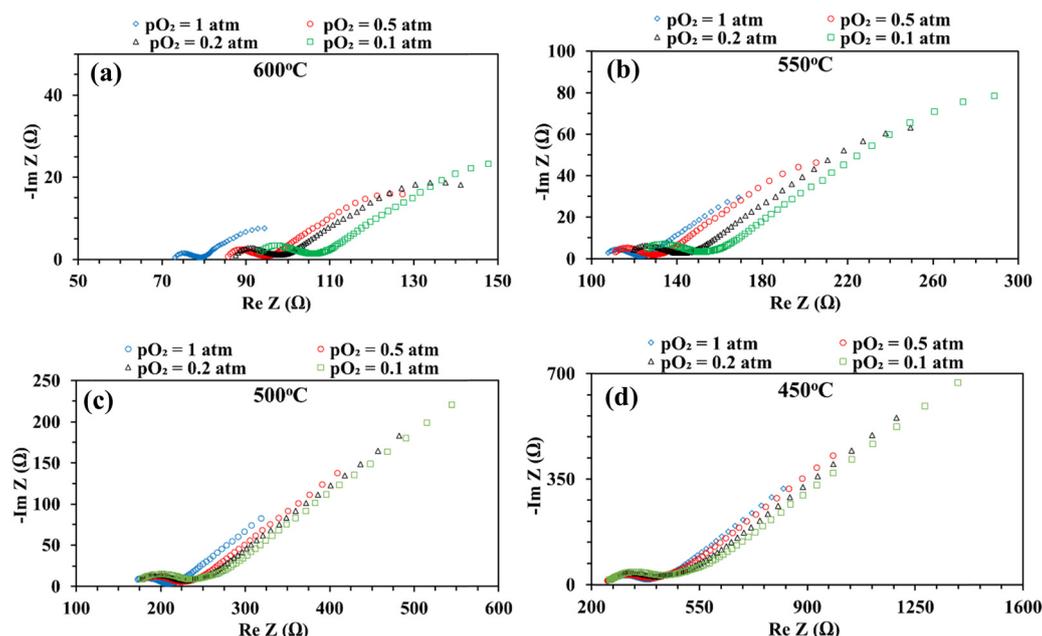


Fig. 8 Electrochemical impedance spectra (EIS) of an electrochemical cell with the patterned Ag working electrode and the PNC counter electrode in an  $O_2$ – $N_2$  mixture with  $p_{O_2}$  values of 1, 0.5, 0.2, and 0.1 atm at (a) 600, (b) 550, (c) 500, and (d) 450 °C, respectively.

(increase of  $R_{ai}$  with reduced  $p_{O_2}$ ) is consistent with a porous Ag cathode symmetrical cell over the  $BaZr_{0.1}Ce_{0.7}Y_{0.1}Yb_{0.1}O_{3-\delta}$  (BZCYYb1711) proton conducting electrolyte<sup>13</sup> and is expected to result from the slowdown of oxygen gas phase transport, surface adsorption, and dissociation with lower oxygen concentration. In addition, the reduced electronic leakage, due to shifting of reaction (4) to the right with lower  $p_{O_2}$ , especially at higher temperatures such as 600 and 550 °C, is also expected to contribute to the increase in  $R_{ai}$ .<sup>62</sup> Interestingly, at elevated temperatures such as 600 and 550 °C, there appears to be a continuation of the EIS loop at the low frequency end towards the real axis. The exact reason is not clear. One possibility is that the ORR elemental steps such as  $O_2$  dissociative

adsorption may be much faster at these temperatures than those at a lower temperature (*i.e.*, 450 °C). This might enable the presence of surface active species even under very low frequency conditions (near DC conditions) and the continuation of the EIS loop towards the real axis instead of the Warburg-like behavior seen at lower temperatures such as 450 °C.

Fig. 9 shows the DRT curves of impedance spectra shown in Fig. 8. Similar to the testing in simulated air (see Fig. 6), multiple peaks (7+) are also observed across the frequency range. Like before, the EIS† Fig. S2 shows the fittings for the EIS plot at 550 °C in a dry 20%  $O_2$ –80%  $N_2$  mixture (*i.e.*,  $p_{O_2} = 0.2$  atm.), considering 4, 5, 6, and 8 RC circuits. In this case,



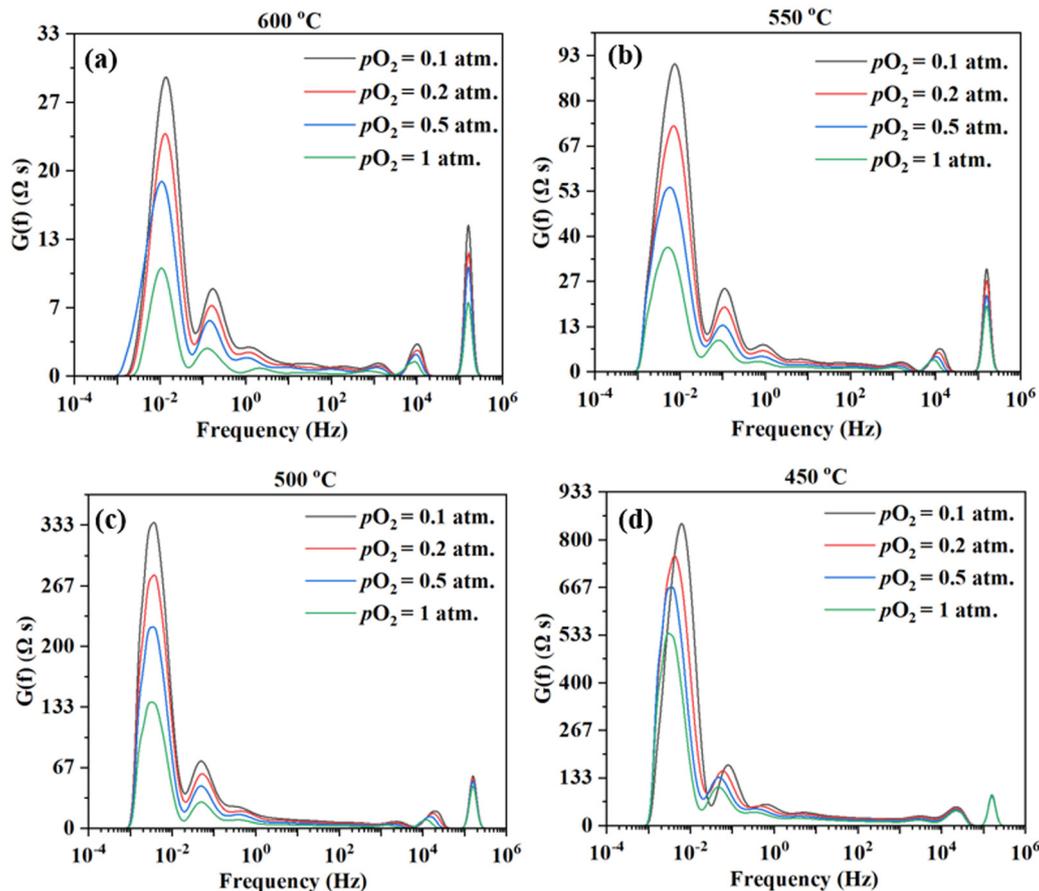


Fig. 9 Distribution of Relaxation Times (DRT) curves of the impedance spectra of an electrochemical cell with the patterned Ag working electrode and the PNC counter electrode in an  $O_2-N_2$  mixture with  $pO_2$  values of 0.1, 0.2, 0.5, and 1 atm at (a) 600, (b) 550, (c) 500, and (d) 450 °C, respectively.

6 RC circuits seem to be enough to give a reasonable fit, while the fitting with 4 RC gives unsatisfactory results. ESI,† Fig. S4 shows the fittings for the EIS plot in a dry 20%  $O_2$ -80%  $N_2$  mixture (*i.e.*,  $pO_2 = 0.2$  atm) at 600–450 °C. The fitted equivalent circuits turn out to contain 6–8 RC circuits in series. As explained before, such a high number of peaks are probably due to the complex nature of the 4-electron ORR process involving many elemental steps.

Fig. 10 shows the inverse of  $R_{ai}$  normalized by the TPB length *vs.*  $pO_2$  plot, both on the logarithmic scale for the patterned Ag electrode cell over the BZCYb4411 proton conducting electrolyte in this study at 600–450 °C in comparison to the dense Ag electrode reported by Herle *et al.* at 753 °C<sup>16</sup> and by Huang *et al.*<sup>30</sup> at 450 °C, all over the conventional YSZ electrolyte. For the current dense patterned Ag electrode over the proton conducting electrolyte,  $1/R_{ai}$  increases with increasing  $pO_2$  at all temperatures from 600 to 450 °C, with roughly the same slope, indicating the same rate-controlling mechanism. The fitted slope  $n$  is in the range of 0.39–0.47, which indicates that the ORR process on the Ag electrode over the BZCYb4411 proton conducting electrolyte is likely controlled by both oxygen dissociation ( $n = 0.5$ ) and charge transfer ( $n = 0.25$ ), according to an earlier study conducted by Grimaud *et al.*<sup>15</sup> A further study is needed to confirm this.

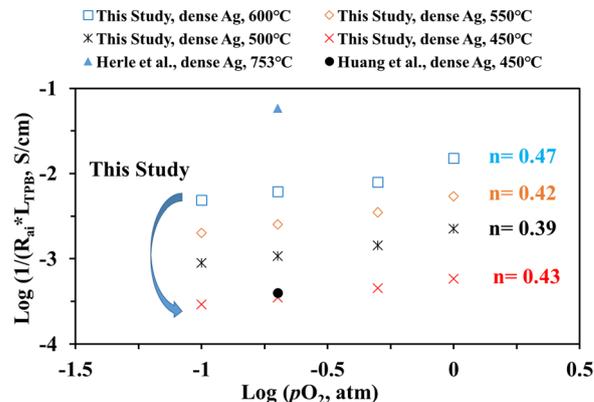


Fig. 10 (a) Plot of  $\log(1/(R_{ai} \times L_{TPB}))$  *vs.*  $\log(pO_2)$  for the dense patterned Ag electrode over the proton conducting BZCYb4411 electrolyte in this study. Data for the dense patterned Ag electrode over the YSZ electrolyte reported by Herle *et al.*<sup>16</sup> at 753 °C and Huang *et al.*<sup>30</sup> at 450 °C are also shown for comparison.

In addition to the studies discussed above, new experiments are currently underway involving the fabrication of dense patterned Ag electrodes with different TPB lengths and electrode contact areas to clarify the relationship between geometric parameters (*e.g.*,  $L_{TPB}$ ) and electrode kinetics for the



ORR over the proton conducting electrolyte. The reference electrode will also be added to the patterned electrode cell to get polarization curves. More systematic studies with respect to atmospheres and bias conditions will also be carried out. Additionally, patterned Ag electrodes with the same electrode geometry will be fabricated over both proton conducting and oxygen ion conducting electrolytes with comparable total ionic conductivities (e.g., BZCYYb4411 and GDC at  $\sim 450$  °C in simulated air). This will provide another way to examine the roles of proton conducting electrolytes in the critical ORR versus conventional oxygen conducting electrolytes. Last but not least, theoretical calculations using both the density functional theory (DFT) method and electrochemical modeling based on the finite element method (FEM) will be conducted to reveal the cathode ORR reaction mechanism, including all the elemental steps for proton conducting SOFCs.

## Conclusion

In this study, patterned Ag cathodes were successfully fabricated on the BZCYYb4411 proton conducting electrolyte by photolithography and E-beam evaporation. Electrochemical cells with the fabricated patterned Ag working electrode and PNC counter electrode were tested by electrochemical impedance spectroscopy. The results for the Ag metal cathode over the proton conducting electrolyte, with the introduction of moisture into air, show that both ohmic resistance and EIS high frequency loops decrease, representing bulk hydration and a change in the reaction pathway from oxygen ions to protons, while the mid-to-low frequency loops increase, possibly due to either water adsorption blocking O<sub>2</sub> adsorption/dissociation and diffusion to the TPB or reduced electronic leakage through the electrolyte. In addition, decreasing  $pO_2$  also appears to slow down the cathode process in a way similar to the moisture effect. The reaction order in terms of interfacial conductance is estimated to be in the range of  $-0.14$  to  $-0.22$  for moisture and  $0.39$  to  $0.47$  for oxygen. Analysis of the EIS data by both the DRT analysis and fitting to equivalent circuits suggests multiple elemental steps reflecting the complex nature of the cathode ORR reaction, especially when water and protons are involved. Future work, involving both experiments and theoretical calculations (e.g., by finite element electrochemical modeling and DFT calculations), will focus on revealing the effects of patterned electrode geometry on electrode kinetics and the fundamental mechanism (especially the pathway) of the ORR in proton conducting IT-SOFCs.

## Author contributions

Md Shariful Islam Sozal: methodology, investigation, data curation, writing – original draft; Wenhao Li: methodology; Suprabha Das: methodology; Borzooye Jafarizadeh: methodology; Azmal Huda Chowdhury: methodology; Chunlei Wang: methodology; and Zhe Cheng: conceptualization, funding, supervision, writing – reviewing and editing.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

This research is supported by the National Science Foundation (award no. DMR-1848305). The use of facilities at the FIU Advanced Materials Engineering Research Institute (AMERI) and Dr John T. Macdonald Foundation Biomedical Nanotechnology Institute (BioNIUM) Nanofabrication Facility of University of Miami is acknowledged. The Dissertation Acquisition Fellowship (DEA) from FIU is also acknowledged for its valuable support.

## References

- 1 N. Q. Minh, Ceramic Fuel Cells, *J. Am. Ceram. Soc.*, 1993, **76**, 563–588.
- 2 S. C. Singhal, Solid oxide fuel cells for stationary, mobile, and military applications, *Solid State Ionics*, 2002, **152–153**, 405–410.
- 3 C. Lu, S. An, W. L. Worrell, J. M. Vohs and R. J. Gorte, Development of intermediate-temperature solid oxide fuel cells for direct utilization of hydrocarbon fuels, *Solid State Ionics*, 2004, **175**, 47–50.
- 4 P. Singh and N. Q. Minh, Solid oxide fuel cells: Technology status, *Int. J. Appl. Ceram. Technol.*, 2004, **1**, 5–15.
- 5 E. Wachsman and K. Lee, Lowering the Temperature of Solid Oxide Fuel Cells, *Science*, 2011, **334**, 935–940.
- 6 M. Singh, D. Zappa and E. Comini, Solid oxide fuel cell: Decade of progress, future perspectives and challenges, *Int. J. Hydrogen Energy*, 2021, **46**, 27643–27674.
- 7 Y. Yamazaki, R. Hernandez-Sanchez and S. M. Haile, High total proton conductivity in large-grained yttrium-doped barium zirconate, *Chem. Mater.*, 2009, **21**, 2755–2762.
- 8 Y. Guo, Y. Lin, R. Ran and Z. Shao, Zirconium doping effect on the performance of proton-conducting BaZr<sub>y</sub>Ce<sub>0.8–y</sub>Y<sub>0.2</sub>O<sub>3–δ</sub> ( $0.0 \leq y \leq 0.8$ ) for fuel cell applications, *J. Power Sources*, 2009, **193**, 400–407.
- 9 L. Yang, *et al.*, Enhanced Sulfur and Coking Tolerance of a Mixed Ion Conductor for SOFCs: BaZr<sub>0.1</sub>Ce<sub>0.7</sub>Y<sub>0.2–x</sub>Yb<sub>x</sub>O<sub>3–δ</sub>, *Science*, 2009, **326**, 126–129.
- 10 H. An, *et al.*, A  $5 \times 5$  cm<sup>2</sup> protonic ceramic fuel cell with a power density of  $1.3$  W cm<sup>–2</sup> at  $600$  °C, *Nat. Energy*, 2018, **3**, 870–875.
- 11 C. Duan, J. Huang, N. Sullivan and R. O’Hayre, Proton-conducting oxides for energy conversion and storage, *Appl. Phys. Rev.*, 2020, **7**, 011314.
- 12 S. Sun and Z. Cheng, Effects of H<sub>2</sub>O and CO<sub>2</sub> on Electrochemical Behaviors of BSCF Cathode for Proton Conducting IT-SOFC Effects of H<sub>2</sub>O and CO<sub>2</sub> on Electrochemical Behaviors of BSCF Cathode for Proton Conducting IT-SOFC, *J. Electrochem. Soc.*, 2017, **164**, F81–F88.
- 13 S. Sun and Z. Cheng, Electrochemical Behaviors for Ag, LSCF and BSCF as Oxygen Electrodes for Proton Conducting



- IT-SOFC Electrochemical Behaviors for Ag, LSCF and BSCF as Oxygen Electrodes for Proton Conducting IT-SOFC, *J. Electrochem. Soc.*, 2017, **164**, F3104–F3113.
- 14 F. He, T. Wu, R. Peng and C. Xia, Cathode reaction models and performance analysis of  $\text{Sm}_{0.5}\text{Sr}_{0.5}\text{CoO}_{3-\delta}$ - $\text{BaCe}_{0.8}\text{Sm}_{0.2}\text{O}_{3-\delta}$  composite cathode for solid oxide fuel cells with proton conducting electrolyte, *J. Power Sources*, 2009, **194**, 263–268.
- 15 A. Grimaud, *et al.*, Hydration Properties and Rate Determining Steps of the Oxygen Reduction Reaction of Perovskite-Related Oxides as H<sup>+</sup>-SOFC Cathodes, *J. Electrochem. Soc.*, 2012, **159**, 683–694.
- 16 J. Van Herle and A. J. McEvoy, Oxygen diffusion through silver cathodes for solid oxide fuel cells, *J. Phys. Chem. Solids*, 1994, **55**, 339–347.
- 17 V. Brichzin, J. Fleig, H. U. Habermeier and J. Maier, Geometry Dependence of Cathode Polarization in Solid Oxide Fuel Cells Investigated by Defined Sr-Doped  $\text{LaMnO}_3$  Microelectrodes, *Electrochem. Solid-State Lett.*, 2000, **3**, 403–406.
- 18 J. Fleig, H. R. Kim, J. Jamnik and J. Maier, Oxygen Reduction Kinetics of Lanthanum Manganite (LSM) Model Cathodes: Partial Pressure Dependence and Rate-Limiting Steps, *Fuel Cells*, 2008, **8**, 330–337.
- 19 A. K. Opitz and J. Fleig, Investigation of O<sub>2</sub> reduction on Pt/YSZ by means of thin film microelectrodes: The geometry dependence of the electrode impedance, *Solid State Ionics*, 2010, **181**, 684–693.
- 20 Y. B. Kim, *et al.*, Nanopore Patterned Pt Array Electrodes for Triple Phase Boundary Study in Low Temperature SOFC, *J. Electrochem. Soc.*, 2010, **157**, B1269–B1274.
- 21 J. H. Shim, *et al.*, Patterned Silver Nanomesh Cathode for Low-Temperature Solid Oxide Fuel Cells, *J. Electrochem. Soc.*, 2012, **159**, B541–B545.
- 22 V. Brichzin, J. Fleig, H. U. Habermeier, G. Cristiani and J. Maier, The geometry dependence of the polarization resistance of Sr-doped  $\text{LaMnO}_3$  microelectrodes on yttria-stabilized zirconia, *Solid State Ionics*, 2002, **152–153**, 499–507.
- 23 J. L. Hertz and H. L. Tuller, Electrochemical Characterization of Thin Films for a Micro-Solid Oxide Fuel Cell, *J. Electroceramics*, 2004, **13**, 663–668.
- 24 E. Koep, D. S. Mebane, R. Das, C. Compson and M. Liu, Characteristic thickness for a dense  $\text{La}_{0.8}\text{Sr}_{0.2}\text{MnO}_3$  electrode, *Electrochem. Solid-State Lett.*, 2005, **8**, A592–A595.
- 25 J. Fleig, *et al.*, Thin Film Microelectrodes in SOFC Electrode Research, *Fuel Cells*, 2006, **6**, 284–292.
- 26 J.-H. Wang, M. Liu and M. C. Lin, Oxygen reduction reactions in the SOFC cathode of  $\text{Ag/CeO}_2$ , *Solid State Ionics*, 2006, **177**, 939–947.
- 27 J. L. Hertz and H. L. Tuller, Measurement and finite element modeling of triple phase boundary-related current constriction in YSZ, *Solid State Ionics*, 2007, **178**, 915–923.
- 28 S. Koc, G. J. La O', T. Golfopoulos and Y. Shao-Horn, Impedance Spectroscopy Studies of Oxygen Reduction Reaction on Thin Film Platinum Microelectrodes Supported on YSZ, *ECS Trans.*, 2007, **7**, 1271–1277.
- 29 F. S. Baumann, *et al.*, Quantitative Comparison of Mixed Conducting SOFC Cathode Materials by Means of Thin Film Model Electrodes, *J. Electrochem. Soc.*, 2007, **154**, B931–B941.
- 30 H. Huang, T. Holme and F. B. Prinz, Oxygen Reduction Characteristics on Ag, Pt, and Ag–Pt Alloys in Low Temperature SOFCs, *ECS Trans.*, 2007, **3**, 31–40.
- 31 S. Choi, *et al.*, Exceptional power density and stability at intermediate temperatures in protonic ceramic fuel cells, *Nat. Energy*, 2018, **3**, 202–210.
- 32 M. S. I. Sozal, *et al.*, Electrical, thermal, and H<sub>2</sub>O and CO<sub>2</sub> poisoning behaviors of  $\text{PrNi}_{0.5}\text{Co}_{0.5}\text{O}_{3-\delta}$  electrode for intermediate temperature protonic ceramic electrochemical cells, *Int. J. Hydrogen Energy*, 2022, **47**, 21817–21827.
- 33 A. Bieberle, L. P. Meier and L. J. Gauckler, The Electrochemistry of Ni Pattern Anodes Used as Solid Oxide Fuel Cell Model Electrodes, *J. Electrochem. Soc.*, 2001, **148**, A646–A656.
- 34 A. Ehn, *et al.*, Electrochemical Investigation of Nickel Pattern Electrodes in H<sub>2</sub>/H<sub>2</sub>O and CO/CO<sub>2</sub> Atmospheres, *J. Electrochem. Soc.*, 2010, **157**, B1588–B1596.
- 35 W. Yao and E. Croiset, Ni/YSZ pattern anodes fabrication and their microstructure and electrochemical behavior changes in H<sub>2</sub>-H<sub>2</sub>O environments, *J. Power Sources*, 2013, **226**, 162–172.
- 36 W. Li, Y. Shi, Y. Luo, Y. Wang and N. Cai, Carbon deposition on patterned nickel/yttria stabilized zirconia electrodes for solid oxide fuel cell/solid oxide electrolysis cell modes, *J. Power Sources*, 2015, **276**, 26–31.
- 37 O. Cherry, *Fabrication of an Atom Chip for Rydberg Atom-Metal Surface Interaction Studies*, Master thesis, Univ. Waterloo, Waterloo, Canada, 2007.
- 38 R. Zaouk, B. Y. Park and M. J. Madou, Introduction to Microfabrication Techniques, *Methods Mol. Biol.*, 2010, **321**, 5–15.
- 39 G. Marin, *Inclined lithography and photoresist optimization for fabrication of 3D mesh structures*, Master thesis, Aalto Univ., 74, 2014.
- 40 J. M. Shaw, J. D. Gelorme, N. C. LaBianca, W. E. Conley and S. J. Holmes, Negative photoresists for optical lithography, *IBM J. Res. Dev.*, 1997, **41**, 81–94.
- 41 H. S. Lee and J. B. Yoon, A simple and effective lift-off with positive photoresist, *J. Micromech. Microeng.*, 2005, **15**, 2136–2140.
- 42 R. A. Lawson, L. M. Tolbert, T. R. Younkin and C. L. Henderson, Negative-tone molecular resists based on cationic polymerization, *Adv. Resist Mater. Process. Technol.*, 2009, **XXVI** 7273, 72733E1.
- 43 E. Koep, C. Compson, M. Liu and Z. Zhou, A photolithographic process for investigation of electrode reaction sites in solid oxide fuel cells, *Solid State Ionics*, 2005, **176**, 1–8.
- 44 D. Poetzsch, R. Merkle and J. Maier, Investigation of oxygen exchange kinetics in proton-conducting ceramic fuel cells: Effect of electronic leakage current using symmetric cells, *J. Power Sources*, 2013, **242**, 784–789.
- 45 R. Strandbakke, *et al.*, Gd- and Pr-based double perovskite cobaltites as oxygen electrodes for proton ceramic fuel cells and electrolyser cells, *Solid State Ionics*, 2015, **278**, 120–132.



- 46 F. J. A. Loureiro, *et al.*,  $\text{La}_4\text{Ni}_3\text{O}_{10\pm\delta}$ - $\text{BaCe}_{0.9}\text{Y}_{0.1}\text{O}_{3-\delta}$  cathodes for proton ceramic fuel cells; short-circuiting analysis using  $\text{BaCe}_{0.9}\text{Y}_{0.1}\text{O}_{3-\delta}$  symmetric cells, *Int. J. Hydrogen Energy*, 2021, **46**, 13594–13605.
- 47 H. Schichlein, *et al.* System Identification: A New Modelling Approach for SOFC Single Cells. in Proceedings of The Electrochemical Society vol. 1999–19 1069–1077 (1999).
- 48 T. Ramos, K. Thydén and M. Mogensen, Electrochemical Characterisation of Ni/(Sc)YSZ Electrodes, in *ECS Transactions*, ed. T. Ramos, 2010, vol. 28, pp.123–139.
- 49 M. Saccoccio, T. H. Wan, C. Chen and F. Ciucci, Optimal regularization in distribution of relaxation times applied to electrochemical impedance spectroscopy: Ridge and Lasso regression methods – A theoretical and experimental Study, *Electrochim. Acta*, 2014, **147**, 470–482.
- 50 B. A. Boukamp and A. Rolle, Analysis and Application of Distribution of Relaxation Times in Solid State Ionics, *Solid State Ionics*, 2017, **302**, 12–18.
- 51 E. Ivers-Tiffée and A. Weber, Evaluation of electrochemical impedance spectra by the distribution of relaxation times, *J. Ceram. Soc. Jpn.*, 2017, **125**, 193–201.
- 52 B. A. Boukamp and A. Rolle, Use of a distribution function of relaxation times (DFRT) in impedance analysis of SOFC electrodes, *Solid State Ionics*, 2018, **314**, 103–111.
- 53 J. Hong, A. Bhardwaj, H. Bae, I. Kim and S.-J. Song, Electrochemical Impedance Analysis of SOFC with Transmission Line Model Using Distribution of Relaxation Times (DRT), *J. Electrochem. Soc.*, 2020, **167**, 114504.
- 54 A. Zare, H. Salari, A. Babaei, H. Abdoli and H. Aslannejad, Electrochemical evaluation of  $\text{Sr}_2\text{Fe}_{1.5}\text{Mo}_{0.5}\text{O}_{6-\delta}/\text{Ce}_{0.9}\text{Gd}_{0.1}\text{O}_{1.95}$  cathode of SOFCs by EIS and DRT analysis, *J. Electroanal. Chem.*, 2023, **936**, 1–8.
- 55 J. Sasaki, J. Mizusaki, S. Yamauchi and K. Fueki, Studies on Electrode Processes of Stabilized Zirconia Cell System by Complex Impedance Method, *Bull. Chem. Soc. Jpn.*, 1981, **54**, 1688–1692.
- 56 H. Uchida, S. Tanaka and H. Iwahara, Polarization at Pt electrodes of a fuel cell with a high temperature-type proton conductive solid electrolyte, *J. Appl. Electrochem.*, 1985, **15**, 93–97.
- 57 N. Li, *et al.*, Characterization of  $\text{GdBaCo}_2\text{O}_{5+\delta}$  cathode for IT-SOFCs, *J. Alloys Compd.*, 2008, **454**, 274–279.
- 58 R. Peng, T. Wu, W. Liu, X. Liu and G. Meng, Cathode processes and materials for solid oxide fuel cells with proton conductors as electrolytes, *J. Mater. Chem.*, 2010, **20**, 6218–6225.
- 59 C. Zhang and H. Zhao, A novel cobalt-free cathode material for proton-conducting solid oxide fuel cells, *J. Mater. Chem.*, 2012, **22**, 18387–18394.
- 60 Z. Wang, *et al.*, A high performance cathode for proton conducting solid oxide fuel cells, *J. Mater. Chem. A*, 2015, **3**, 8405–8412.
- 61 R. Radhakrishnan, A. V. Virkar and S. C. Singhal, Estimation of Charge-Transfer Resistivity of Pt Cathode on YSZ Electrolyte Using Patterned Electrodes, *J. Electrochem. Soc.*, 2005, **152**, A927–A936.
- 62 M. Liu and H. Hu, Effect of Interfacial Resistance on Determination of Transport Properties of Mixed-Conducting Electrolytes, *J. Electrochem. Soc.*, 1996, **143**, L109–L112.

