



Cite this: *Green Chem.*, 2024, **26**, 9176

## Sustainable iron production *via* highly efficient low-temperature electrolysis of 3D conductive colloidal electrodes†

Panya Thanwisai,<sup>‡a</sup> Zeyi Yao,<sup>‡a</sup> Muntasir Shahabuddin,<sup>b</sup> Jiahui Hou,<sup>id</sup> <sup>a</sup> Jinzhao Fu,<sup>a</sup> Adam C. Powell IV<sup>id</sup> <sup>a</sup> and Yan Wang<sup>id</sup> <sup>\*a</sup>

Towards decarbonizing the carbothermic reduction of iron and steelmaking, which produces around 5% of global CO<sub>2</sub> emissions, we herein propose a low-temperature electrolysis (100 °C) with 3D electrically-ionically conductive colloidal Fe<sub>2</sub>O<sub>3</sub> electrodes as a novel and sustainable alternative. With the designed electrodes that offer a 3D conductive network to facilitate the electrochemical reduction of Fe<sub>2</sub>O<sub>3</sub> at such a low temperature, high-purity Fe powder (>95%) can be produced with high current efficiency (>95%) and no direct CO<sub>2</sub> emission. In addition to Fe, we also demonstrate the production of metal and alloy powders such as Cu, Ag, and an FeNi alloy using the proposed method. A techno-economic assessment of the process is performed to evaluate industrial feasibility as well as CO<sub>2</sub> emission analysis. Altogether, this alternative process is green, environmentally friendly, and energy efficient, showing great potential for revolutionizing the conventional process that has had a significant environmental impact for decades.

Received 6th February 2024,

Accepted 4th July 2024

DOI: 10.1039/d4gc00698d

rsc.li/greenchem

## Introduction

Currently, iron (Fe) is manufactured by carbothermic reduction in which iron oxide ores (Fe<sub>2</sub>O<sub>3</sub>) are reduced by carbon coke at a high temperature of >2000 °C in a blast furnace using the blast furnace/basic oxygen furnace route (BF-BOF) and the electric arc furnace route (EAF).<sup>1</sup> In accordance with the reduction reaction shown in eqn (1), liquid crude Fe is produced while CO<sub>2</sub> is also emitted as a by-product. Moreover, the use of fossil fuels to generate such a high-temperature environment, coke production, and other energy-intensive processes related to iron and steelmaking further contribute to carbon emissions.<sup>2</sup> As reported in the Energy Agency and EDGAR 4.3 databases, approximately 2 tons of CO<sub>2</sub> are emitted per ton of crude Fe produced, accounting for 5% of global CO<sub>2</sub> emissions,<sup>3</sup> which are considered some of the most difficult emissions to eliminate. With the goal of net-zero carbon emissions from iron and steelmaking, radical

and transformational technologies for cleaner Fe production are therefore urgently required. In recent years, several alternatives have been extensively utilized to produce Fe with limited direct carbon emissions such as molten oxide electrolysis (MOE),<sup>4–13</sup> hydrogen flash smelting (HFS),<sup>14–17</sup> and low-temperature electrolysis (LTE).<sup>2,18–26</sup> Among these, the LTE method has attracted much attention due to its intriguing advantages. For example, LTE is conducted at a significantly lower temperature (~100 °C) compared to the carbothermic reduction (>2000 °C), MOE (>500 °C), and HFS processes (>1000 °C). Unlike the MOE process, it does not require a stable anode for such a high-temperature operation and avoids the use of H<sub>2</sub> as a reducing agent, which is cost-prohibitive for the commercialization of the HFS process. These benefits endow the LTE process with less energy-consumptive, simpler, and less expensive iron manufacturing, which has great potential for industrialization.

In fact, LTE for iron production towards zero CO<sub>2</sub> emission has been examined for many years.<sup>5,17,18</sup> Generally, different Fe<sub>2</sub>O<sub>3</sub> electrodes such as Fe<sub>2</sub>O<sub>3</sub> ores, Fe<sub>2</sub>O<sub>3</sub> pellets, or Fe<sub>2</sub>O<sub>3</sub> particles suspended in a highly concentrated alkaline solution electrolyte (50 wt% NaOH) are reduced to metallic Fe by applying electricity to the electrochemical cells. The targeted Fe product is produced at the cathode; meanwhile, O<sub>2</sub> gas is solely generated at the anode without any CO<sub>2</sub> emission. The typical cathodic and anodic reactions are shown in eqn (2) and (3).

<sup>a</sup>Department of Mechanical and Materials Engineering, Worcester Polytechnic Institute, Worcester, MA, 01609, USA. E-mail: yanwang@wpi.edu

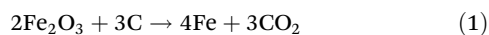
<sup>b</sup>Department of Chemical Engineering, Worcester Polytechnic Institute, Worcester, MA, 01609, USA

† Electronic supplementary information (ESI) available. See DOI: <https://doi.org/10.1039/d4gc00698d>

‡ These authors contributed equally to this work.

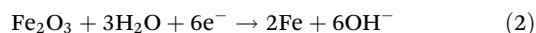


Carbothermic reduction reaction at 2000 °C:

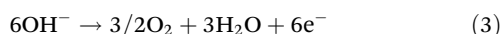


Electrolysis reaction at ~100 °C:

Cathode:



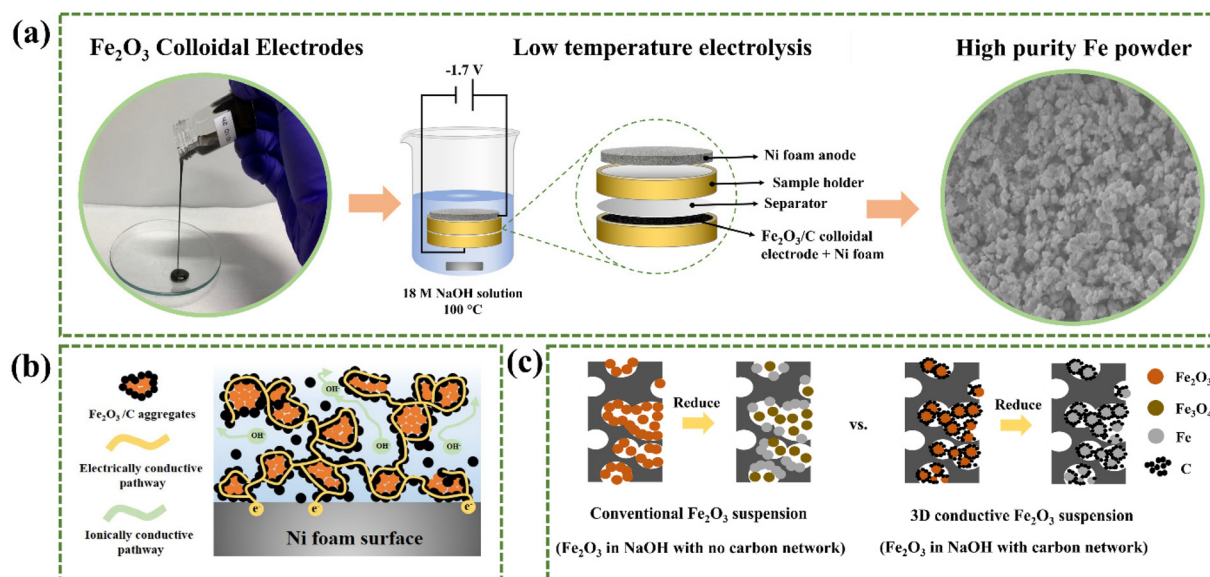
Anode:



Nevertheless, there are some challenges associated with the LTE designs that prevent them from being adopted on a large scale. Firstly,  $\text{Fe}_2\text{O}_3$  intrinsically possesses low electrical conductivity, and thus, charge transfer during the electroreduction and the electrochemical reaction rate are limited, resulting in low energy efficiency. Moreover, palletization and high-temperature sintering steps lead to excessive energy usage and complexity in large-scale production. Secondly, in a system of  $\text{Fe}_2\text{O}_3$  particles suspended in an alkaline electrolyte,  $\text{Fe}_2\text{O}_3$  particles need to diffuse to the cathode substrate surface to be involved in the electrochemical reaction. As a result, the conductive areas are limited by the substrate; meanwhile, the sluggish diffusion of  $\text{Fe}_2\text{O}_3$  impedes the fast reaction rate.

Herein, we report a novel and sustainable method of Fe production *via* low-temperature electrolysis of electrically-ionically conductive  $\text{Fe}_2\text{O}_3$ /carbon (C) colloidal electrodes with porous Ni foam substrates. The proposed LTE process is depicted in Fig. 1a in which the flowable  $\text{Fe}_2\text{O}_3$ /C colloids are electrolyzed at a low temperature of 100 °C with a constant cell voltage of -1.7 V in a 50 wt% NaOH electrolyte solution. The final product is high-purity Fe powder while only  $\text{O}_2$  gas is generated as a by-product, which is collectible. In our LTE design, the colloidal

electrodes contain  $\text{Fe}_2\text{O}_3$ /C composite powders suspended in a highly concentrated NaOH solution, which is different from the reported  $\text{Fe}_2\text{O}_3$  suspension systems. Here, C acts as an electrically conductive network improving the electrical conductivity of  $\text{Fe}_2\text{O}_3$ , while the NaOH solution serves as an ionic conductive network facilitating ion diffusion during the electrochemical reaction. Thus, a 3D conductive percolation network is formed, as shown in Fig. 1b. Fig. 1c depicts the reduction mechanism of suspensions of  $\text{Fe}_2\text{O}_3$  particles in NaOH solution with and without the C conductive network. In the conventional  $\text{Fe}_2\text{O}_3$  suspension (with no C),  $\text{Fe}_2\text{O}_3$  particles need to diffuse to the surface of the Ni foam current collector to be reduced. Due to their sluggish diffusivity in NaOH and intrinsically poor electrical conductivity, most  $\text{Fe}_2\text{O}_3$  particles are reduced to  $\text{Fe}_3\text{O}_4$  with some Fe depositing on Ni foam surfaces. In contrast, in the designed  $\text{Fe}_2\text{O}_3$  suspension with C,  $\text{Fe}_2\text{O}_3$  particles can be directly reduced to Fe without diffusion owing to the formation of the C conductive network. Furthermore, C on  $\text{Fe}_2\text{O}_3$  particles also serves as a conductive medium, so  $\text{Fe}_2\text{O}_3$  particles do not directly come into contact with the Ni foam surface, alleviating the deposition of Fe powder on the electrode surface. This unique function in turn improves production yield and facilitates product collection. More importantly, as the colloidal electrode is flowable, it can potentially be used in a flow electrolysis design that allows continuous production and facilitates product collection and separation steps. Altogether, utilizing the LTE of  $\text{Fe}_2\text{O}_3$  colloidal electrodes can resolve the aforementioned limitations of the LTE process. In addition, it is worth mentioning that the electrolysis design can also be applied to produce other metal and alloy powders such as Cu, Ag, and an FeNi alloy and shows great potential for use as an alternative method of metal/alloy powder production.



**Fig. 1** (a) Schematic illustration of the low-temperature electrolysis of  $\text{Fe}_2\text{O}_3$  colloidal electrodes. (b) Illustration of an electronically and ionically conductive network of  $\text{Fe}_2\text{O}_3$  colloidal electrodes. (c) Illustration showing the electrochemical reduction of  $\text{Fe}_2\text{O}_3$  colloidal electrodes with and without C networks on a Ni foam substrate.



## Results and discussion

### Formation of Fe<sub>2</sub>O<sub>3</sub>/C colloidal electrodes

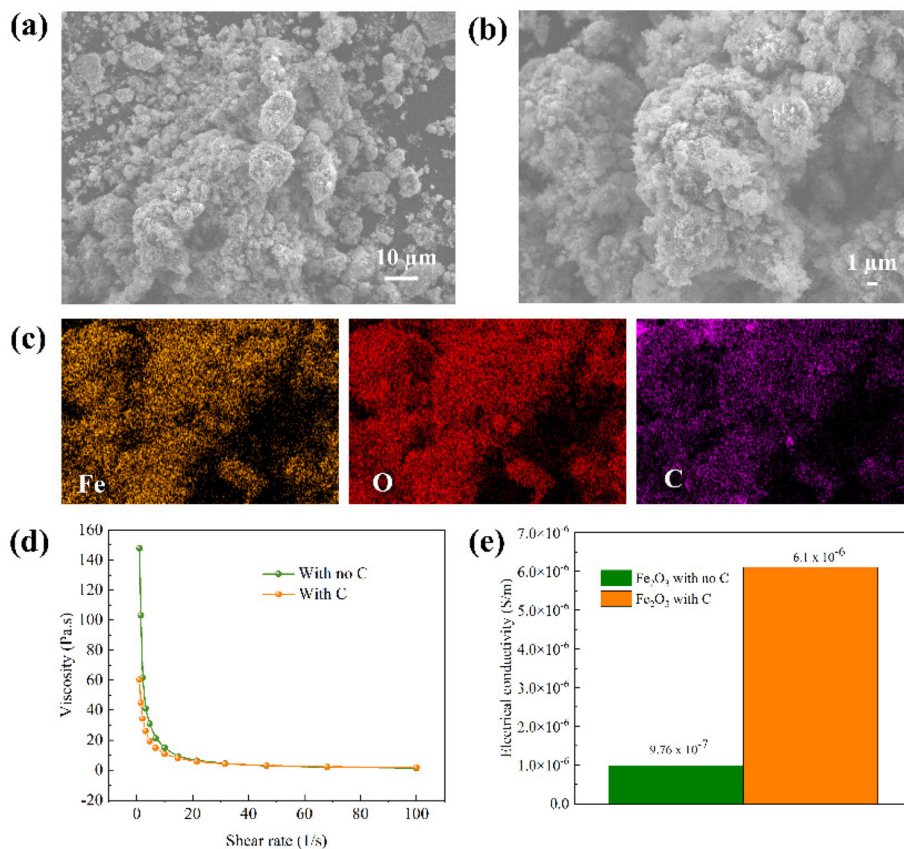
Prior to the electrochemical reduction process, Fe<sub>2</sub>O<sub>3</sub> colloidal electrodes were prepared as described in the experimental details in the ESI.† Fig. 2a and b show the morphologies of Fe<sub>2</sub>O<sub>3</sub>/C aggregates with particle sizes ranging from 1 μm to >10 μm, revealed by scanning electron microscopy (SEM). The corresponding elemental mappings of the aggregates obtained from energy dispersive X-ray spectroscopy (EDS) in Fig. 2c show a uniform distribution of C powders on Fe<sub>2</sub>O<sub>3</sub> particles confirming the successful formation of Fe<sub>2</sub>O<sub>3</sub>/C aggregates. It is worth noting that the structure is necessary for the reduction reaction since the formation of the Fe<sub>2</sub>O<sub>3</sub>/C network sufficiently provides electrically conductive pathways to the colloidal electrodes, which helps increase the electrical conductivity of Fe<sub>2</sub>O<sub>3</sub>. The BET surface areas of Fe<sub>2</sub>O<sub>3</sub> and Fe<sub>2</sub>O<sub>3</sub>/C aggregates are reported in Table S1.† C nanopowders provide extra reactive surface areas, facilitating the reduction reaction. In addition to the electrically conductive network provided by C powders, the added NaOH solution imparts ionic conductivity to the colloidal electrode. Hence, a 3D conductive Fe<sub>2</sub>O<sub>3</sub> percolation network was fabricated. Moreover, organic and inorganic

additives were added to the colloids to aid in suppressing H<sub>2</sub> evolution and promoting the reduction reaction, according to our previous findings.<sup>2,26,27</sup> It should be noted that the Fe<sub>2</sub>O<sub>3</sub>/C colloids still maintain good flowability, as reflected by the trivial change in viscosity compared to the colloid with no carbon added, as can be seen from the viscosity test in Fig. 2d. The slight decrease in the viscosity of the colloid with C results from larger sizes of aggregates compared to Fe<sub>2</sub>O<sub>3</sub> nanopowders, indicating that the colloidal electrode design can be applied in a flow electrolysis system, facilitating continuous production and ease of product collection. In addition, the electrical conductivity of the Fe<sub>2</sub>O<sub>3</sub>/C slurry was greatly improved due to the formation of the conductive carbon network, as can also be seen in Fig. 2e. The testing details are described in the ESI and Fig. S1.†

### Electrolysis of Fe<sub>2</sub>O<sub>3</sub>/C colloidal electrodes

In the electrochemical reduction of the Fe<sub>2</sub>O<sub>3</sub> colloidal electrode, a negative voltage of 1.7 V was applied to the two-electrode electrolysis cell, and the reaction was prolonged until reaching the theoretical capacity calculated based on Faraday's law, as shown in eqn (S1) in the ESI.†

In the electrolysis experiments, we used porous Ni foam sheets as a cathode substrate and an anode electrode. We



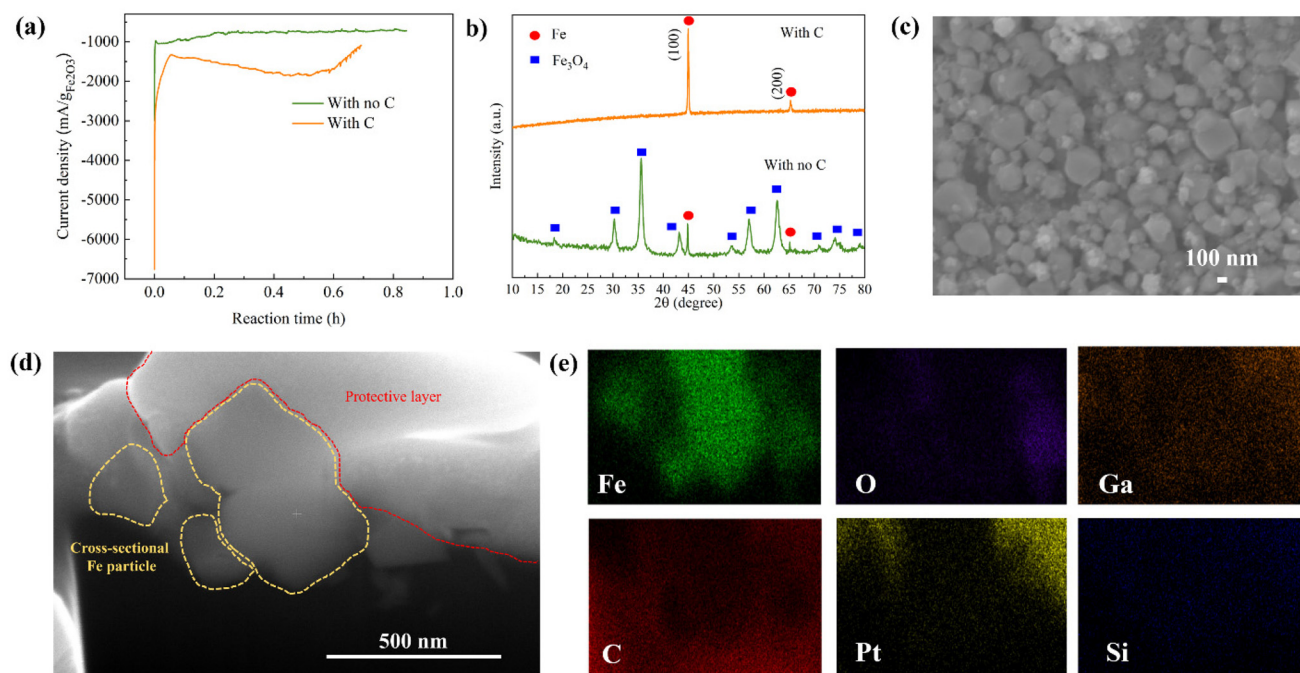
**Fig. 2** (a and b) SEM images of Fe<sub>2</sub>O<sub>3</sub>/C micro-aggregates formed by ball milling at different magnifications. (c) EDS mappings of the prepared aggregates. (d) Viscosity test and (e) electrical conductivity of Fe<sub>2</sub>O<sub>3</sub> colloidal electrodes with and without C.



demonstrated that the utilization of 3D porous Ni foam as a substrate can improve the electrolysis efficiency and Fe purity over using 2D Ti foil as a cathode substrate and Pt foil as an anode, as reported in our previous works.<sup>2,26</sup> This is because the 3D porous structure of Ni foam can sufficiently distribute charge for reducing  $\text{Fe}_2\text{O}_3$  to Fe effectively, resulting in a higher current and a shorter reaction time than those of 2D conductive areas of Ti foil, as can be seen in Fig. S2a.† A cartoon showing the different functions of Ti foil and Ni foam as substrates is illustrated in Fig. S2b.† More importantly, Ni foam is much cheaper than both Ti foil and noble-metallic Pt foil and is more feasible for large-scale and industrial production.

Fig. 3a shows the relationship between the reduction current and reaction time of  $\text{Fe}_2\text{O}_3$  colloidal electrodes with and without C. Of note, the current produced from bare Ni foam is relatively small compared to that from Ni foam with the colloids (Fig. S2c†), contributing to negligible current. At a glance, there are main reduction kinetics observed during the electrolysis reaction that can be used to predict the  $\text{Fe}_2\text{O}_3$  reduction mechanisms as follows.<sup>2</sup> In the first 5 min of the reaction, there is a rapid electrochemical reaction at the  $\text{Fe}_2\text{O}_3$ /electrolyte interface resulting in the production of a high current, similarly observed in both colloidal electrodes. During 20 min of the reaction, in the colloid without C,  $\text{Fe}_2\text{O}_3$  particles are gradually reduced to  $\text{Fe}_3\text{O}_4$  and Fe. Then, after 20 min, the current plateau can be observed implying the sluggish reduction of  $\text{Fe}_3\text{O}_4$  accompanied by  $\text{H}_2$  evolution until the

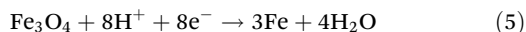
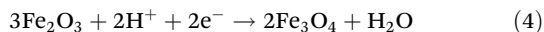
end of the reaction. In contrast, after 5 min of the reaction in the colloidal electrode with C, there is a continuous increase in the current until 36 min of the reaction implying that  $\text{Fe}_2\text{O}_3$  is continuously reduced to Fe throughout the reaction period. In the final 4 min of the reaction, the current decreases, indicative of the end of the reaction. It is noticeable that the current produced by the electrolysis of the  $\text{Fe}_2\text{O}_3/\text{C}$  colloid is higher than that of the colloid without C for the entire reaction period. In addition, the reaction time is shorter, which takes around 40 min to complete the reaction corresponding to  $1\times$  the theoretical capacity applied, while the colloid with no C takes 55 min. This enhancement benefits from the designed colloidal electrode that provides electrically conductive pathways for rapid charge transfer between  $\text{Fe}_2\text{O}_3$  particles and Ni foam substrate surfaces during the electrochemical reduction. The X-ray powder diffraction (XRD) patterns shown in Fig. 3b reveal the resulting products obtained from electrolyzing the colloidal electrodes with and without C. For the conventional  $\text{Fe}_2\text{O}_3$  electrode, the majority of the electrolyzed product is  $\text{Fe}_3\text{O}_4$  with a small amount of Fe. According to peak intensity analysis, the purity of Fe is only 6% while that of  $\text{Fe}_3\text{O}_4$  is 94%. Calculated based on the capacity applied and the purity of produced Fe, the electrolysis efficiency of the electrode without C is around 16%. It was reported that  $\text{Fe}_3\text{O}_4$  is the intermediate phase of  $\text{Fe}_2\text{O}_3$  reduction according to eqn (4) and (5).<sup>26</sup> This intermediate phase is sluggish for the electrochemical reaction to be further reduced to Fe.<sup>2</sup> Hence, it is difficult to reduce all  $\text{Fe}_2\text{O}_3$  to Fe in the conventional colloid that has poor electrical



**Fig. 3** (a) Electrolysis current vs. reaction time plot and (b) XRD patterns of the electrolyzed product for  $\text{Fe}_2\text{O}_3$  colloidal electrodes with and without C. (c) SEM image of electrolyzed Fe after magnetic separation. (d) Cross-sectional FIB-SEM image and (e) EDS mappings of electrolyzed Fe particles.



conductivity, bringing about low purity of Fe and low current efficiency in this process.



In sharp contrast to the conventional suspension, the electrolyzed product of  $\text{Fe}_2\text{O}_3/\text{C}$  colloidal electrodes shows almost no  $\text{Fe}_3\text{O}_4$  phases according to the XRD pattern shown in Fig. 3b. Over 95% of Fe can be obtained with an insignificant amount of  $\text{Fe}_3\text{O}_4$ . This small amount of impurity may come from unreacted  $\text{Fe}_3\text{O}_4$  remaining on the wall of the sample holder made of polypropylene (a non-conductive material), which lacks the coverage of the conductive properties. Of note, the high-purity Fe powder can be reproduced, as shown in Fig. S3.† According to such a high purity of Fe, the calculated current efficiency is 95.6% which is higher than those of other electrolysis methods reported in Table S2,† to the best of our knowledge. The high purity of Fe and high current efficiency stem from the effectiveness of the LTE process with a 3D conductive colloidal electrode design. Compared to those reported LTE and MOE processes, our approach provides comparable or even higher current efficiency and allows bypassing the use of energy-consuming steps, high temperature, and complicated processes leading to more energy and cost savings.

It is worth noting that the presence of the  $\text{Fe}_3\text{O}_4$  intermediate phase suggests that the electroreduction mechanism of most  $\text{Fe}_2\text{O}_3$  suspended particles involves the solid-state reduction of  $\text{Fe}_2\text{O}_3$  particles to  $\text{Fe}_3\text{O}_4$  and then Fe.<sup>20,22,26</sup> In addition, it was found that there are some Fe particles deposited on the Ni foam surface, as shown in Fig. S4a and b.† The deposited Fe particles show a dendritic morphology. Owing to the absence of C layers on  $\text{Fe}_2\text{O}_3$  particles, the electrodeposited Fe is more obvious in the conventional  $\text{Fe}_2\text{O}_3$  colloidal electrodes. Conversely, C powders, forming a conductive layer on  $\text{Fe}_2\text{O}_3$  particles, promote the solid-state reduction of  $\text{Fe}_2\text{O}_3$  particles, resulting in less deposited Fe on the Ni foam surface. Hence, the formation of Fe in the colloidal electrode design involves dominant solid-state  $\text{Fe}_2\text{O}_3$  electrolysis. It is also worth mentioning that, in the practical production of Fe, the deposited Fe on Ni foam can be problematic as it can lead to Fe mass loss. Possible solutions to prevent the deposition and quantification of Fe deposition on Ni foam as well as comments on the issues are provided in Table S3.† Hence, it is suggested that technological advancements in preventing Fe deposition on such a metal porous substrate as well as Fe product separation from the substrate are also needed to improve this technology. Moreover, concerning the reusability of Ni foam, it is shown that Ni foam can be reused without any effects on the resistance or purity of Fe, as seen in Fig. S5a and b.†

### Characterization of electrolyzed Fe powders

After the electrolysis, the electrolyzed Fe was subjected to a magnetic separation step to further enhance the purity and dispose of C remnants, as described in the ESI.† XRD, SEM/

EDS, and focused ion beam scanning electron microscopy (FIB-SEM) for cross-sectional images were also utilized to further characterize the electrolyzed Fe powder before and after separation. Fig. S6a† shows the SEM/EDS mappings of electrolyzed Fe before separation. It can be observed that the Fe particles were covered by C powder and the signal of C from EDS mapping is relatively high. After the magnetic separation, the amount of C was greatly reduced, as reflected by the low signal of C in the EDS mappings (Fig. S6b†), indicating the effective magnetic separation method. The high purity of the obtained Fe powders is also confirmed by inductively coupled plasma optical emission spectroscopy (ICP-OES) (Table S4†). The XRD result of separated carbon is shown in Fig. S6c,† indicating the mixture of nanosized carbon powder and unreacted  $\text{Fe}_2\text{O}_3$  and  $\text{Fe}_3\text{O}_4$ . It should be noted that the carbon powder can possibly be reused after an appropriate separation process, and those iron oxides can also be reduced in further electrolysis reactions. A photograph of separated C powder and Fe powder is also shown in Fig. S6d.† In accordance with the SEM image in Fig. 3c, the Fe particles separated from C powder are of spherical-like nanosizes with an average particle size of around 200 nm. To further investigate the elemental compositions inside the electrolyzed Fe particles, cross-sectional FIB-SEM with line-scanning elemental mapping was accomplished. Fig. 3d illustrates the cross-sectional SEM image of the electrolyzed Fe particles of approximately 200 nm. The cut Fe particles are shown by yellow-dashed areas while the area marked with a red dashed line is a protective layer used in the FIB-SEM process. EDS mapping was conducted to reveal the elemental compositions inside the bulk Fe particles. As shown in Fig. 3e and Fig. S7a,† the signal of Fe is strong throughout the bulk particle with a negligible O signal, confirming that  $\text{Fe}_2\text{O}_3$  is reduced to Fe completely. It should be noted that C, Pt, Ga, and Si signals are from the background and the protective layer. Moreover, no S and Na signals that are from the  $\text{Na}_2\text{S}$  additive and NaOH electrolyte can be detected inside the bulk Fe particle. The EDS mapping is consistent with the line-scanning elemental mapping shown in Fig. S7b† in which the high Fe signal is consistent throughout the whole particle. These confirm the successful reduction of  $\text{Fe}_2\text{O}_3$  to Fe through the proposed LTE of the colloidal electrode.

In addition to nano-sized Fe, we also demonstrated that the method can be applied with a micro-sized  $\text{Fe}_2\text{O}_3$  precursor. The LTE of micro-sized  $\text{Fe}_2\text{O}_3$  provides high-purity Fe powder (>90%) with high current efficiency (>90%) (Fig. S8†). Interestingly, the morphology of Fe from the micro-sized  $\text{Fe}_2\text{O}_3$  source is different from electrolyzed Fe produced by using nano-sized  $\text{Fe}_2\text{O}_3$  as a precursor. Prism-like Fe particles were obtained, as revealed in Fig. S8c.† The morphology is similar to a needle-like or dendritic crystal of Fe grown on a Ni grid, as reported by Lopes *et al.*<sup>28</sup> This suggests that using different sizes of  $\text{Fe}_2\text{O}_3$  can produce Fe powders with different morphologies. However, the purity of electrolyzed Fe from micro-sized  $\text{Fe}_2\text{O}_3$  is slightly lower than that obtained using nano-sized  $\text{Fe}_2\text{O}_3$  sources. This is due to the difference in the par-



ticle sizes of  $\text{Fe}_2\text{O}_3$  and nano-C powder leading to non-homogeneous mixing, as can be observed from the phase separation in the  $\text{Fe}_2\text{O}_3/\text{C}$  suspension shown in Fig. S9a.† In contrast, in Fig. S9b,† the mixture is more homogeneous for the nanosized  $\text{Fe}_2\text{O}_3/\text{C}$  slurry due to their similar particle sizes. It should be noted that the morphology of Fe can alter its physical and chemical properties resulting in the utilization of Fe in a wide range of applications. Therefore, this illustrates that our LTE process can produce Fe with different morphologies by modifying the size of the  $\text{Fe}_2\text{O}_3$  inputs, which is an alternative way to produce nano-Fe or micro-Fe.

### Other metal/alloy powder production

Impressively, in addition to Fe powder production, the proposed LTE with the colloidal electrode design can also be applied to produce other metal/alloy powders such as Ag, Cu, and FeNi alloy powders, as shown in Fig. 4a–c and Fig. S10.† The experimental details of each are described in the ESI. According to the XRD pattern and SEM image of electrolyzed Ag shown in Fig. 4a, Ag can be produced without any detectable impurity signals by electrolyzing  $\text{AgO}/\text{NaOH}$  colloidal electrodes without the addition of C. The ease of electrolyzing  $\text{AgO}$  stems from the excellent electrical conductivity of Ag, hence facilitating such an electrochemical reduction process.  $\text{CuO}$  reduction was also conducted using the LTE method. The preparation of  $\text{CuO}/\text{C}$  aggregates and colloidal electrodes

was identical to iron production. The XRD pattern in Fig. 4b shows that 87% Cu can be obtained through the electrolysis process. It was found that the electrochemical reduction involves the reduction of  $\text{CuO}$  to the  $\text{Cu}_2\text{O}$  intermediate phase and then Cu. This was similarly observed in  $\text{CuO}$  reduction in KCl media.<sup>29,30</sup> In addition to single metal powders, bi-metallic FeNi alloy powders can be produced by the electrolysis of  $\text{NiFe}_2\text{O}_4$  for the first time. Due to the higher electron transfer involved in the reduction reaction, the concentration of the NaOH electrolyte was increased to 65 wt% and the optimized theoretical capacity required is 4 times. As shown in the XRD pattern (Fig. 4c), roughly 78% of FeNi alloy phases can be obtained from the LTE process. Interestingly, the FeNi alloy produced from this LTE method possesses two different phases, BCC-FeNi (Fe-rich phase) and FCC-FeNi (Fe-rich phase). These two phases of FeNi were also observed in the reduction of  $\text{NiFe}_2\text{O}_4$  involving  $\text{H}_2$  reduction at  $>1000^\circ\text{C}$ .<sup>31,32</sup> The SEM image in Fig. 4c shows that cubic-like FeNi particles are produced. Moreover, based on thermodynamic analysis, not only for the production of Fe, Ag, Cu, and the FeNi alloy, but the LTE process can also be applied to produce the elements highlighted in green in Fig. 4d as well as other metal alloy powders. In order to obtain higher purity and current efficiency, nonetheless, electrode fabrications and electrolysis conditions of these metals and alloys need to be optimized.

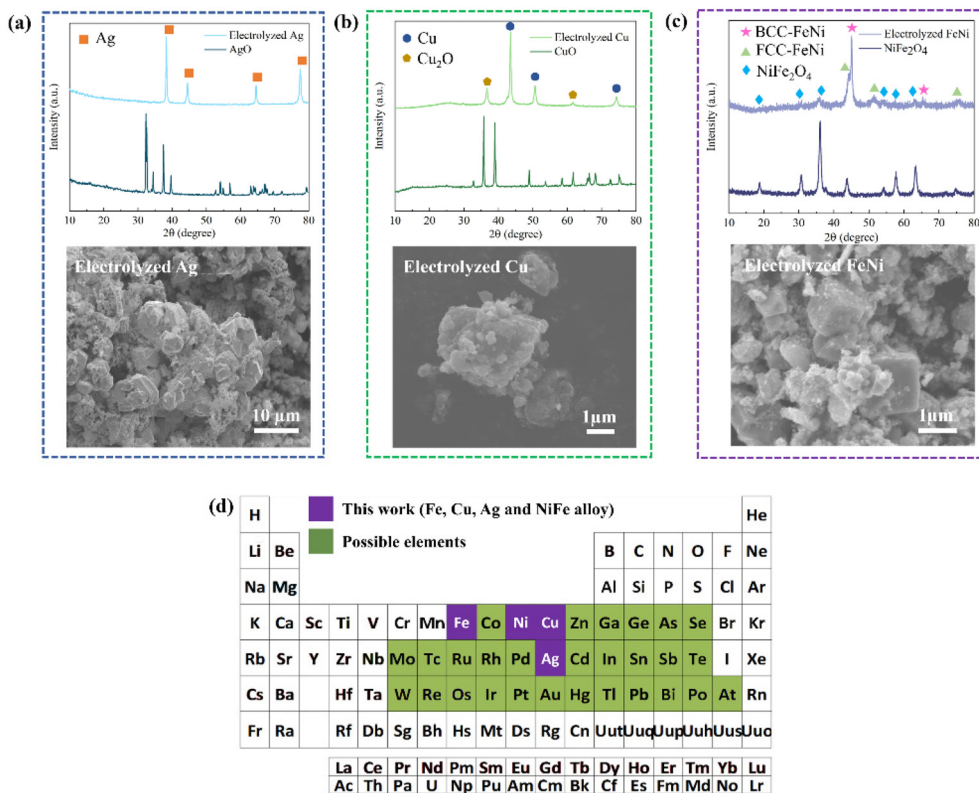


Fig. 4 XRD patterns and SEM images of electrolyzed products using the proposed electrolysis process: (a) Ag, (b) Cu, and (c) FeNi alloy. (d) Possible elements that can be produced by low-temperature electrolysis, based on thermodynamics analysis.



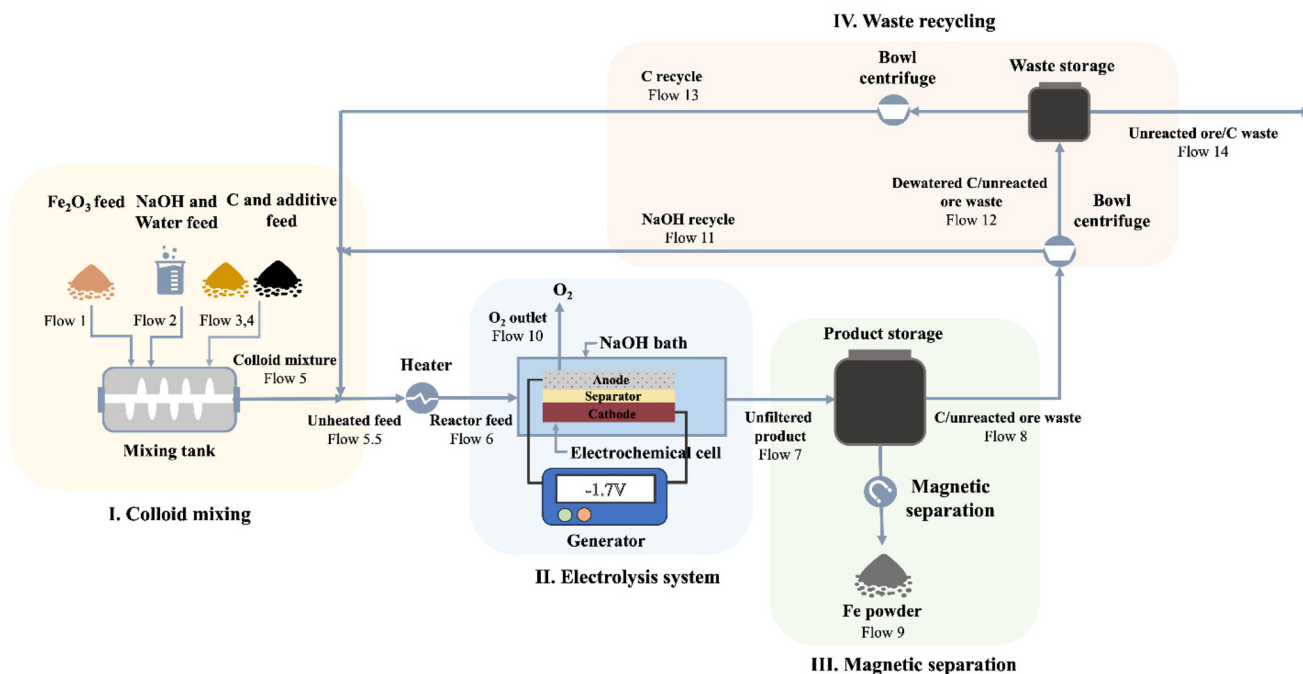


Fig. 5 Schematic illustration showing the flow diagram of iron production *via* the LTE method.

### Techno-economic, energy and CO<sub>2</sub> emission analyses

Inspired by the successful production of Fe *via* LTE on the laboratory scale, the process shows promising potential to be scaled up. Also, we propose a design of closed-loop production of the LTE process. The diagram illustrating the designed electrolysis process is shown in Fig. 5. Overall, the flow process of proposed Fe production consists of four major parts: (I) colloidal mixing, (II) electrolysis system, (III) magnetic separation of electrolyzed iron, and (IV) waste recycling and reuse. In the first part, iron ore powders, C powders, NaOH, water and additives are fed into the colloid mixing tank followed by feeding the colloidal mixture to the electrochemical cell. The electrochemical reduction of the colloidal mixture takes place in the second part. The O<sub>2</sub> by-product in the scaled process is fed out of the process, which can be stored for further utilization. After the electrolysis reaction, the products comprising electrolyzed Fe powders, C powders, NaOH solution and unreacted oxides are fed out from the electrochemical cell for magnetic separation in the third part, where Fe powders will be separated from other components through a magnetic separator. Thereafter, in the final part, bowl centrifuges are used to separate NaOH solution and unreacted powders. NaOH solution and C powders will be recycled and unreacted remnants will be fed out.

To evaluate the economic value of the process, we performed a techno-economic assessment of the LTE process of Fe production. The economic modelling of Fe production *via* the LTE process developed by Shahabuddin *et al.* was adopted to estimate the costs of the process in this work.<sup>33</sup> We adopt the study's process scale of 100 000 tons per year of iron oxide

to best leverage economies of scale. The base case scenario used in the analysis is based on the current experimental results in this work, provided in Table S5.† The product cost breakdown is shown in Fig. 6a, and the details are summarized in Table S6.† Considering variable operating costs (VOC), it appears that the cost of iron oxide ore makes up the largest portion of all the costs accounting for 48% as the expenditure of high-Fe<sub>2</sub>O<sub>3</sub>-content feedstock has a significant cost in comparison with lower value waste feeds. Meanwhile, the price of electricity also occupies a large proportion, which accounts for 31%. This suggests that the cost of the Fe product produced by the electricity-based process is highly dependent on the costs of iron oxide ore and electricity. As the price of iron ore varies with the Fe<sub>2</sub>O<sub>3</sub> content of the sources, it is the most sensitive parameter to determine the cost of Fe. On one hand, using a high-Fe<sub>2</sub>O<sub>3</sub>-content feedstock provides high quality Fe powder in spite of its high cost. On the other hand, there may be a tradeoff between the feedstock cost and purity of Fe powders, if using low-Fe<sub>2</sub>O<sub>3</sub> content ores. In addition, the effects of electrochemically active/inactive impurities on colloid compositions and electrochemical reduction are supposed to be considered for low-grade ore feedstocks. This suggests that, alternatively, utilizing secondary sources that contain a high Fe<sub>2</sub>O<sub>3</sub> content such as Cu tailings or red mud can be a promising remedy to lower the cost of feedstock. Electricity prices can potentially be lowered by managing the operating hours. Other variable costs such as additives, NaOH and C black contribute to only 7% of the product cost since these components can be recycled in the closed-loop process. However, the efficacy of the recycling process may influence the cost of these compositions. Hence, technological advancements in C and



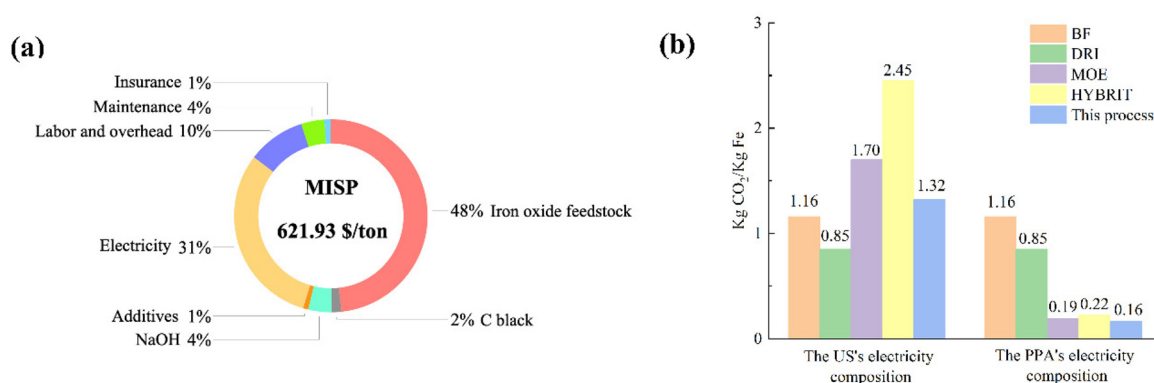


Fig. 6 (a) Cost breakdown with MISP. (b) CO<sub>2</sub> emission of the proposed LTE process compared to other technologies.

NaOH recycling are still needed to achieve the highest efficacy since there is not yet a commercially available carbon recycling process. An appropriate product storage system such as an inert N<sub>2</sub> gas or airtight system is supposed to be considered for such large-scale production to prevent fine Fe powder from undesired exposure. In addition, fixed operating costs (FOC) composed of insurance, maintenance, and labor/overhead account for 15% of the production cost.

The respective minimum iron selling price (MISP) or the levelized cost is calculated to be 621.93 \$ per ton, based on the base case scenario. The price produced by this LTE is comparable to that of hydrogen-based steel production, ranging from 582.18 \$ per ton to 722 \$ per ton.<sup>34,35</sup> Seemingly, the price of Fe powder produced *via* this process is higher than the market prices of bulk pig iron, which are in the range of \$500 to \$600.<sup>33</sup> Although the price of electrolyzed Fe powder is higher than that of the bulk iron produced by conventional pathways, high purity Fe powder with predictable particle sizes and morphologies could be suitable for markets of additive manufacturing and powder metallurgy.<sup>33,36</sup>

In terms of energy utilization, the proposed LTE process has an energy loss through cell leads of only 0.104 kW h per kg of Fe produced, which can be determined *via* the Wiedemann–Franz law using eqn (S10) in the ESI.† The LTE has 9-times lower energy loss through cell leads compared to the high-temperature MOE process, which is also an alternative to iron production with no direct CO<sub>2</sub>.<sup>33</sup> In addition, the LTE does not require a startup heating process like the MOE process. The energy requirement in this developed process is calculated to be 3.19 kW h per kg of Fe produced, which is lower than that of our previously reported LTE of red mud sources (4.76 kW h per kg of Fe produced) and 4.16 kW h per kg of Fe produced for the MOE.<sup>33</sup> It should be noted that the energy requirement of the process in this work is based on utilizing higher Fe<sub>2</sub>O<sub>3</sub> contents, higher electrolysis efficiency, and higher separation performance, resulting in less energy consumption, compared to the LTE of red mud colloidal electrodes.

CO<sub>2</sub> emission analysis of this technology is also performed by comparison with other current steelmaking technologies such as Fe production using a blast furnace (BF), direct reduction of iron (DRI) using natural gas or H<sub>2</sub> gas, molten

oxide electrolysis (MOE) and H<sub>2</sub> reduction (HYBRIT). The analysis is performed by analyzing the emissions associated with material production and electricity sources (Tables S7 and S8†). The base case scenarios for this analysis are based on a constant operation hour with two different electricity conditions: the reported US's electricity mix and power purchasing agreement (PPA). The US's electricity source is composed of 39.8% natural gas, 19.5% coal, 18.2% nuclear, 10.2% wind, 6.3% hydroelectric, 3.4% solar, 1.3% biomass, 0.9% petroleum, and 0.4% geothermal sources.<sup>37</sup> The PPA's electricity is based on 100% electricity from renewable sources that are 50% wind and 50% solar.<sup>33</sup> The estimated CO<sub>2</sub> emissions from BF and DRI are around 1.16 and 0.85 kg CO<sub>2</sub> per kg Fe, respectively.<sup>33,38,39</sup> According to Fig. 6b, considering the utilization of a conventional electricity mixture, the electricity-dependent processes (the proposed process, MOE and HYBRIT) emit a slightly larger amount of CO<sub>2</sub> compared to the blast furnace and DRI processes. It is worth noting that, however, further purification of pig iron and utilization of fossil fuels in the blast furnace can emit additional CO<sub>2</sub>, which may result in a higher emission rate in the conventional process. When using the PPA's electricity, all the alternatives see a significant reduction in CO<sub>2</sub> emission, which is relatively lower than those of the BF and DRI processes. The proposed LTE technology shows the least CO<sub>2</sub> emission, 0.16 kg CO<sub>2</sub> per kg Fe. It should be noted that the emissions from MOE and HYBRIT are estimated using only direct CO<sub>2</sub> emission and electricity usage in the two processes, while CO<sub>2</sub> emissions from other productions such as molten salts and hydrogen sources are not included. Hence, the emissions from the two alternatives could possibly be higher. This analysis suggests that the proposed LTE for Fe production combined with utilizing clean electricity is more environmentally friendly compared to other processes.

## Conclusions

In summary, we have demonstrated that the LTE process with a 3D electrically–ionically conductive electrode design can be successfully used to produce high-purity Fe powder (>95%) with high current efficiency (>95%) at a low temperature of



100 °C with no carbon emissions. The utilization of C conductive networks and 3D porous conductive Ni foam as a substrate in this novel LTE process can facilitate the fast reaction rate by increasing the reactive areas and evenly distributing charges on the substrate for the Fe<sub>2</sub>O<sub>3</sub> reduction process. It was also found that the morphology and particle sizes of electrolyzed Fe rely on the sizes of the initial Fe<sub>2</sub>O<sub>3</sub> precursors. The economic analysis of the process reveals that the price of the Fe product highly depends on the costs of Fe<sub>2</sub>O<sub>3</sub> feedstock and electricity. The calculated MISP is 621.93 \$ per ton which is comparable to the prices of steels produced by the hydrogen-based method. Moreover, CO<sub>2</sub> emission analysis reveals that the process of utilizing clean electricity from renewable sources emits only 0.16 kg CO<sub>2</sub> per kg Fe produced, which is much lower than the emissions from the conventional and alternative processes. In addition to Fe, we also demonstrated that this LTE can be used to produce high-purity Ag, Cu, and FeNi alloy powders from their oxides. Altogether, this cleaner and more energy-saving LTE process is a promising technology for metal and alloy production that can potentially be used to replace the conventional process.

## Data availability

The data supporting this article have been included as part of the ESI.†

## Conflicts of interest

Parts of the experimental results are under a patent application.

## Acknowledgements

This work is financially supported by the U.S. Army Research Laboratory through their award #W911NF-22-2-0040. We gratefully appreciate the aid from Prof. Qi Wen at the Department of Physics, Worcester Polytechnic Institute, to conduct the viscosity test.

## References

- U. D. O. T. Interior, *Minerals Yearbook, 2007, V. 3, Area Reports, International, Asia and the Pacific*, Government Printing Office, 2010.
- Q. Wang, Y. Zhu, Q. Wu, E. Gratz and Y. Wang, *RSC Adv.*, 2015, **5**, 5501–5507.
- S. J. Davis, N. S. Lewis, M. Shaner, S. Aggarwal, D. Arent, I. L. Azevedo, S. M. Benson, T. Bradley, J. Brouwer, Y. M. Chiang, C. T. M. Clack, A. Cohen, S. Doig, J. Edmonds, P. Fennell, C. B. Field, B. Hannegan, B. M. Hodge, M. I. Hoffert, E. Ingersoll, P. Jaramillo, K. S. Lackner, K. J. Mach, M. Mastrandrea, J. Ogden, P. F. Peterson, D. L. Sanchez, D. Sperling, J. Stagner, J. E. Trancik, C. J. Yang and K. Caldeira, *Science*, 2018, **360**, eaas9793.
- D. Wang, A. J. Gmitter and D. R. Sadoway, *J. Electrochem. Soc.*, 2011, **158**, E51.
- D. R. Sadoway, *J. Mater. Res.*, 1995, **10**, 487–492.
- H. Kim, J. Paramore, A. Allamore and D. R. Sadoway, *J. Electrochem. Soc.*, 2011, **158**, E101.
- H. Kim, J. D. Paramore, A. Allamore and D. R. Sadoway, *ECS Trans.*, 2010, **33**, 219.
- A. Allamore, L. Yin and D. R. Sadoway, *Nature*, 2013, **497**, 353–356.
- J. Wiencke, H. Lavelaine, P.-J. Panteix, C. Petitjean and C. Rapin, *J. Appl. Electrochem.*, 2018, **48**, 115–126.
- A. Cox and D. J. Fray, *J. Appl. Electrochem.*, 2008, **38**, 1401–1407.
- D. Tian, H. Jiao, J. Xiao, M. Wang and S. Jiao, *J. Alloys Compd.*, 2018, **769**, 977–982.
- D. Tang, H. Yin, W. Xiao, H. Zhu, X. Mao and D. Wang, *J. Electroanal. Chem.*, 2013, **689**, 109–116.
- H. Yin, D. Tang, H. Zhu, Y. Zhang and D. Wang, *Electrochem. Commun.*, 2011, **13**, 1521–1524.
- H. Wang and H. Sohn, *Metall. Mater. Trans. B*, 2013, **44**, 133–145.
- H. K. Pinegar, M. S. Moats and H. Y. Sohn, *Steel Res. Int.*, 2011, **82**, 951–963.
- M. Choi and H. Sohn, *Ironmaking Steelmaking*, 2010, **37**, 81–88.
- H. Sohn, M. E. Choi, Y. Zhang and J. E. Ramos, *Ironmaking Steelmaking*, 2009, **6**, 158–165.
- A. Allamore, H. Lavelaine, G. Valentin, J. Birat and F. Lapique, *J. Electrochem. Soc.*, 2007, **154**, E187.
- A. Allamore, H. Lavelaine, G. Valentin, J. Birat and F. Lapique, *J. Electrochem. Soc.*, 2008, **155**, E125.
- A. Allamore, H. Lavelaine, G. Valentin, J. Birat, P. Delcroix and F. Lapique, *Electrochim. Acta*, 2010, **55**, 4007–4013.
- B. Yuan and G. M. Haarberg, *ECS Trans.*, 2009, **16**, 31.
- Y. A. Ivanova, J. Monteiro, L. Teixeira, N. Vitorino, A. Kovalevsky and J. Frade, *Mater. Des.*, 2017, **122**, 307–314.
- V. Feynerol, H. Lavelaine, P. Marlier, M.-N. Pons and F. Lapique, *J. Appl. Electrochem.*, 2017, **47**, 1339–1350.
- J. Monteiro, Y. A. Ivanova, A. Kovalevsky, D. Ivanou and J. Frade, *Electrochim. Acta*, 2016, **193**, 284–292.
- M. Tokushige, O. E. Kongstein and G. M. Haarberg, *ECS Trans.*, 2013, **50**, 103.
- Q. Wang, B. Fu and Y. Wang, *J. Electrochem. Soc.*, 2017, **164**, E428–E433.
- Q. Wang and Y. Wang, *ACS Appl. Mater. Interfaces*, 2016, **8**, 10334–10342.
- D. V. Lopes, A. Kovalevsky, M. Quina and J. Frade, *J. Electrochem. Soc.*, 2020, **167**, 102508.
- Q. Wang and Y. Wang, *J. Electrochem. Soc.*, 2018, **165**, A2439–A2445.
- Y. Y. Su and M. Marek, *J. Electrochem. Soc.*, 1994, **141**, 940.
- D. Yu, M. Zhu, T. A. Utigard and M. Barati, *Miner. Eng.*, 2013, **54**, 32–38.
- M. Bahgat, M.-K. Paek and J.-J. Pak, *Mater. Trans.*, 2007, **48**, 3132–3139.
- M. Shahabuddin, A. C. Powell IV and Y. Wang, *J. Sustain. Metall.*, 2022, **8**, 900–912.



- 34 A. Bhaskar, R. Abhishek, M. Assadi and H. N. Somehesaraei, *J. Cleaner Prod.*, 2022, **350**, 131339.
- 35 F. Rosner, D. Papadias, K. Brooks, K. Yoro, R. Ahluwalia, T. Autrey and H. Breunig, *Energy Environ. Sci.*, 2023, **16**, 4121–4134.
- 36 A. Simchi, *Metall. Mater. Trans. B*, 2004, **35**, 937–948.
- 37 EIA, Electricity in the United States, <https://www.eia.gov/energyexplained/electricity/electricity-in-the-us.php>, (accessed 1/27, 2024).
- 38 P. Renzulli, B. Notarnicola, G. Tassielli, G. Arcese and R. Di Capua, *Sustainability*, 2016, **8**, 719.
- 39 C. Ramakgala and G. Danha, *Procedia Manuf.*, 2019, **35**, 242–245.

