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## Rethinking nitrate reduction: redirecting electrochemical efforts from ammonia to nitrogen for realistic environmental impacts†

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The excessive use of nitrate in agriculture and industry poses a significant threat to human health and ecosystems. To effectively manage the nitrogen cycle (N-cycle) in nature and to deal with nitrate pollution in wastewater, various electrochemical approaches have been developed to convert nitrate into N-products. Recent research works have focused their efforts on electrochemical nitrate reduction ( $e\text{NO}_3\text{R}$ ) to ammonia ( $\text{NH}_3$ ) as "an alternative approach to the Haber–Bosch process" while reducing the environmental impacts. However, when considering challenges due to the low concentration of nitrate in wastes and difficulties in extracting as-synthesized  $\text{NH}_3$  and comparing this scale with the scale of current  $\text{NH}_3$  and nitrate production, such an  $e\text{NO}_3\text{R}$  to  $\text{NH}_3$  approach at the largest possible scale, even without examining its economic viability and overall environmental implications, will have an insignificant impact. Therefore, we recommend that rational implementation approaches for nitrate treatment should involve converting nitrate ions at low concentrations into nitrogen ( $\text{N}_2$ ) gas or recycling them at high concentrations to produce other nitrate chemicals or fertilizers.

### Broader context

With the growing world population and increasing human activities, nitrate pollution in water bodies has caused severe health and environmental issues. To provide clean drinking water and balance the nitrogen cycle (N-cycle) in nature, numerous research efforts have focused on removing nitrate from wastewater using electrochemical approaches. Several recent studies have claimed that converting waste nitrate into ammonia ( $\text{NH}_3$ ) with high catalytic performance provides an alternative approach to the Haber–Bosch process. Unfortunately, such a "waste-to-wealth" conversion will likely have insignificant impacts and should be considered an unnecessary distraction. To deliver realistic environmental impacts, our analysis deems that the low-concentration nitrate in wastewater should be directly converted into harmless  $\text{N}_2$  gas through electrochemical reactions, and for the case of high concentrations, nitrate ions should be recycled and purified to generate nitrate chemicals or fertilizers.

## Background

Ammonia ( $\text{NH}_3$ ), as one of the most important chemicals, plays a vital role, particularly in the production of fertilizers for agriculture that feeds the world population.<sup>1–3</sup> The global production of  $\text{NH}_3$  reaches over 180 million tonnes (Mt) per year with a market value of ~US\$75 billion.<sup>4–6</sup> This massive amount of  $\text{NH}_3$  is produced through the conventional Haber–Bosch process, accounting for 1–2% of the world's energy demand and contributing to 1–1.5% of

annual anthropogenic  $\text{CO}_2$  emissions.<sup>7,8</sup> Around 75% of  $\text{NH}_3$  is utilized in the agricultural sector for the production of fertilizers and synthesis of nitric acid ( $\text{HNO}_3$ ), another critical industrial feedstock for manufacturing fertilizers.<sup>9</sup> The remaining ~25% is employed in plastics, explosives, food and synthetic fibers manufacturing industries.<sup>10</sup> In particular, almost 100% of nitric acid production relies on the energy-intensive Ostwald process:  $\text{NH}_3$  oxidation at high temperatures (600–900 °C) and pressure (410–1000 kPa).<sup>1,11,12</sup> The global production of nitric acid totals approximately 60 Mt per year, with a market value of around US\$30 billion, of which about 70% is exploited to produce ammonium nitrate ( $\text{NH}_4\text{NO}_3$ ) as a modern agricultural fertilizer.<sup>11,13</sup> Moreover, about 13% of nitric acid is used for organic oxidation reactions, which also constitute a vital intermediate for organic nitrations. The remaining nitric acid is consumed for the synthesis of other materials and chemical processes. This signifies the essential roles of large nitric acid production and its utilization in fertilizer

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Table 1 Various types of nitrate-polluted wastewater and criteria for drinking water

Type of wastewater	pH	N-species	Nitrate concentration (N-mg L <sup>-1</sup> )
Polluted groundwater <sup>19</sup>	Unknown	NO <sub>3</sub> <sup>-</sup> , NO <sub>2</sub> <sup>-</sup> , NH <sub>4</sub> <sup>+</sup>	12–18
Textile wastewater <sup>20</sup>	7	NO <sub>3</sub> <sup>-</sup>	104
Industrial wastewater <sup>21</sup>	7.9	NO <sub>3</sub> <sup>-</sup> , NH <sub>4</sub> <sup>+</sup>	582.4
Low-level nuclear wastewater <sup>22</sup>	Alkaline	NO <sub>3</sub> <sup>-</sup> , NO <sub>2</sub> <sup>-</sup> , Ru(NO(NO <sub>2</sub> ) <sub>4</sub> (OH)) <sup>2-</sup>	27 300
Drinking water <sup>18</sup>	6.5–8.5	NO <sub>3</sub> <sup>-</sup> , NO <sub>2</sub> <sup>-</sup> , NH <sub>4</sub> <sup>+</sup>	<10

industries. Furthermore, the escalating global population and economic activities will continue to increase the demand for nitric acid production in the future. Its excessive use for agricultural purposes and the improper disposal of industrial wastes, however, can lead to health and environmental issues.

Nitrate contamination in drinking water (NO<sub>3</sub><sup>-</sup> > 10 N-mg L<sup>-1</sup>) mainly results from agricultural and industrial activities and has health impacts, such as causing methemoglobinemia, cancer, and thyroid problems.<sup>14–17</sup> In addition, the rising NO<sub>3</sub><sup>-</sup> concentration can disrupt the natural N-cycle by releasing reactive nitrogen species into the environment. Table 1 lists the concentrations of nitrate in various types of contaminated wastewater.<sup>16</sup> Concerning public health, the World Health Organization (WHO) recommends maximum contaminant levels of 10, 0.03, and 0.4 N-mg L<sup>-1</sup>, respectively, for NO<sub>3</sub><sup>-</sup>, NO<sub>2</sub><sup>-</sup>, and NH<sub>4</sub><sup>+</sup> in drinking water.<sup>18</sup>

## Electrochemical NO<sub>3</sub><sup>-</sup> Reduction (eNO<sub>3</sub>R) to NH<sub>3</sub>

### Impractical potential

To address nitrate pollution in wastewater and mitigate the natural N-cycle imbalance, a growing number of studies have been reported on the electrochemical NO<sub>3</sub><sup>-</sup> reduction to NH<sub>3</sub> (Fig. 1), with strong catalytic performances achieved, including a current density as high as ~1 A cm<sup>-2</sup> and ~100% faradaic efficiencies.<sup>23–25</sup> Some reports have even asserted that electrochemical NO<sub>3</sub><sup>-</sup> reduction to NH<sub>3</sub> under ambient conditions utilizing nitrate wastes as feedstock could be an alternative to

the conventional Haber–Bosch process.<sup>26–29</sup> Although significant progress has been made in the electrochemical conversion of NO<sub>3</sub><sup>-</sup> to NH<sub>3</sub> in terms of current densities and faradaic efficiencies, the feasibility of large-scale NH<sub>3</sub> production remains highly questionable due to the insufficient concentration and low capacity of nitrates feedstock in real wastewater. Taking the widespread fertilizer ammonium nitrate as an example, about 17% of nitrate ions would leach to the groundwater as nitrate contaminants annually.<sup>30</sup> Even if those nitrate contaminants can be successfully converted to NH<sub>3</sub> with 100% selectivity using an electrochemical approach, the estimated amount of ammonia produced would only be about 2 Mt year<sup>-1</sup>. Such a “waste-to-wealth” conversion approach is insignificant compared to the NH<sub>3</sub> production accomplished using the conventional Haber–Bosch process, even without considering the energy needs for NO<sub>3</sub><sup>-</sup> collection and reduction, and NH<sub>3</sub> separation, purification, and compression, and a significant amount of the NH<sub>3</sub> produced would be oxidized for the nitric acid production.

### Unintentional environmental challenges

In another area of research that focuses on adopting environmentally friendly approaches to address nitrate contaminants in wastewater, various technologies such as reverse osmosis, bacterial denitrification, and ion exchange are currently being employed on a commercial scale.<sup>31</sup> However, those technologies are expensive and require harsh reaction conditions. In contrast, electrochemical reduction of nitrate to ammonia powered by renewable electricity would seem to be a more sustainable method for treating wastewater than existing commercial technologies,<sup>32,33</sup> but, unfortunately, may not be economically viable despite the reported high selectivity and efficiency of NO<sub>3</sub><sup>-</sup>-to-NH<sub>3</sub> conversion due to the resulting low concentration of NH<sub>3</sub>.<sup>34</sup> Moreover, any NH<sub>3</sub> not completely isolated would itself be a more serious contaminant than NO<sub>3</sub><sup>-</sup> in wastewater.

## Conclusion and outlook

In summary, electrochemical NO<sub>3</sub><sup>-</sup> reduction to NH<sub>3</sub> may show some scientific merits, but when considering practical and industrial implementations, this process will likely play an insignificant role in either NO<sub>3</sub><sup>-</sup> contaminants removal or NH<sub>3</sub> production.<sup>35,36</sup> When dealing with NO<sub>3</sub><sup>-</sup> contaminants in real wastewater, NO<sub>3</sub><sup>-</sup> should not be converted to NH<sub>3</sub> at any concentration range: at high concentrations, NO<sub>3</sub><sup>-</sup> is a more valuable feedstock (as it has to be produced from NH<sub>3</sub>), with the

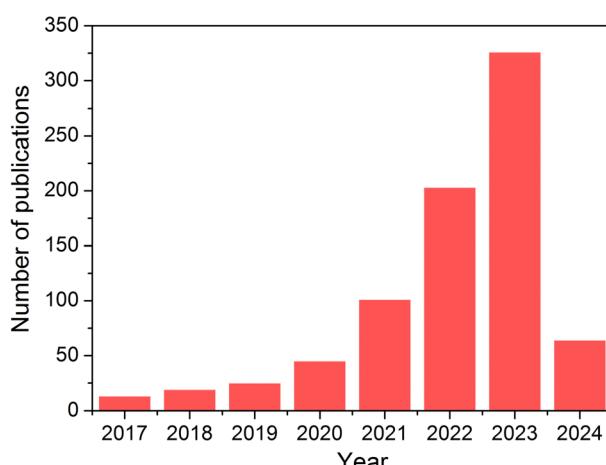


Fig. 1 Number of publications per year on “electrochemical nitrate reduction to ammonia.” Source: Web of Science on Mar. 29, 2024.



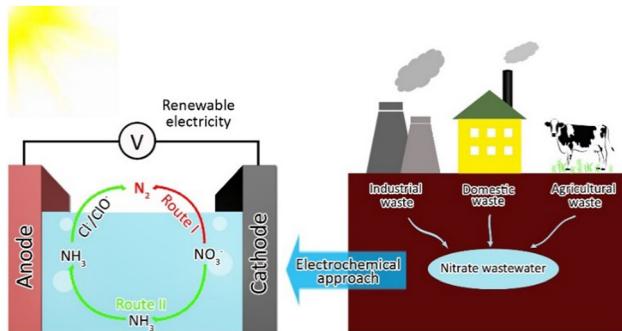
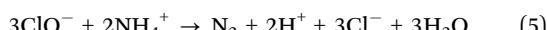
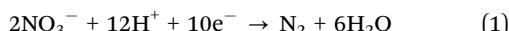


Fig. 2 Schematic diagram of electrochemical reduction of nitrate to nitrogen gas for wastewater denitrification.

production costs and energy consumption of  $\text{NH}_3$  using the electrochemical  $\text{NO}_3^-$  reduction process being 2.04 times higher than those of the Haber–Bosch process (the detailed calculation is provided in Table S1, ESI†);<sup>37</sup> at low concentrations,  $\text{NH}_3$  produced from reducing  $\text{NO}_3^-$  becomes a more serious contaminant. For a more feasible and meaningful N-cycle to address nitrate pollution issues, following directions are recommended.

### I. $\text{NO}_3^-$ reduction to $\text{N}_2$

In wastewater denitrification, instead of focusing on converting  $\text{NO}_3^-$  to  $\text{NH}_3$ , directly converting low-concentration nitrate (10–1 000 N-mg  $\text{L}^{-1}$ ) into harmless  $\text{N}_2$  gas through electrocatalysis powered by renewable electricity would be more practical (Route I, Fig. 2 and eqn (1)).<sup>38,39</sup> Alternatively,  $\text{NO}_3^-$  can be converted into  $\text{NH}_3$  first on the cathode side, followed by the oxidation of  $\text{NH}_3$  at the anode side to produce  $\text{N}_2$  with the assistance of chloride ions in wastewater (Route II, Fig. 2, and eqn (2)–(5)),<sup>40,41</sup> and in this way, risks induced by the potential byproducts of the  $\text{eNO}_3\text{R}$  process, such as  $\text{ClO}_3^-$ , trichloromethane, bromodichloromethane, or dibromochloromethane, are mitigated or avoided.<sup>42,43</sup> Such a route can also be applied for removing  $\text{NH}_3/\text{NH}_4^+$  from wastewater.



### II. $\text{NO}_3^-$ recovery

In the case of wastewater containing nitrate at high concentrations (above 1 000 N-mg  $\text{L}^{-1}$ ), a more pragmatic approach can be recycling and purifying nitrate salts to produce  $\text{NO}_3^-$  chemicals or fertilizers rather than converting them into  $\text{NH}_3$ .<sup>44,45</sup>

### III. Coupling with $\text{CO}_2$ reduction for value-added N-fertilizers

Value-added N-fertilizers might be generated or co-produced during the removal of nitrate from wastewater. For instance,

urea can be produced by coupling  $\text{NO}_3^-$  reduction with  $\text{CO}_2$  reduction.<sup>46,47</sup> An electrochemical approach has been recently reported for recovering  $\text{NH}_3/\text{NH}_4^+$  from manure wastewater and co-producing  $\text{NH}_4^+$ -rich fertilizer.<sup>48</sup> These technologies, however, are still in their early stages. Investigations of larger-scale implementation, improvement of energy efficiencies, and economic viability optimization will be needed to create meaningful impacts.

## Conflicts of interest

There are no conflicts to declare.

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## References

- 1 J. G. Chen, R. M. Crooks, L. C. Seefeldt, K. L. Bren, R. M. Bullock, M. Y. Dahrenbourg, P. L. Holland, B. Hoffman, M. J. Janik, A. K. Jones, M. G. Kanatzidis, P. King, K. M. Lancaster, S. V. Lymar, P. Pfromm, W. F. Schneider and R. R. Schrock, *Science*, 2018, **360**, eaar6611.
- 2 C. Smith, A. K. Hill and L. Torrente-Murciano, *Energy Environ. Sci.*, 2020, **13**, 331–344.
- 3 S. Chatterjee, R. K. Parsapur and K.-W. Huang, *ACS Energy Lett.*, 2021, **6**, 4390–4394.
- 4 Global Data, Global Ammonia Industry Outlook to 2025 – Capacity and Capital Expenditure Forecasts with Details of All Active and Planned Plants, 2021.
- 5 U.S. Geological Survey, Mineral commodity summaries 2023: U.S. Geological Survey, Reston, VA, 2023, p. 210, DOI: [10.3133/mcs2023](https://doi.org/10.3133/mcs2023).
- 6 G. Schnitkey, Fertilizer prices higher for 2019 crop, farmdoc daily, Department of Agricultural and Consumer Economics, UIUC, 2018. <https://farmdocdaily.illinois.edu/2018/09/fertilizerprices-higher-for-2019-crop.html>.
- 7 J. Nørskov and J. Chen, *Sustainable Ammonia Synthesis*, U.S. Department of Energy, Dulles, VA, 2016.
- 8 F. Jiao and B. Xu, *Adv. Mater.*, 2019, **31**, e1805173.
- 9 D. Erdemir and I. Dincer, *Int. J. Energy Res.*, 2020, **45**, 4827–4834.
- 10 International Energy Agency (IEA), *Ammonia Technology Roadmap*, IEA, Paris, 2021.
- 11 ChemAnalyst, *Nitric Acid Market Analysis*, 2023, <https://www.chemanalyst.com/industry-report/nitric-acid-market-615>.
- 12 C. A. Grande, K. A. Andreassen, J. H. Cavka, D. Waller, O.-A. Lorentsen, H. Øien, H.-J. Zander, S. Poulston, S. García and D. Modeshia, *Ind. Eng. Chem. Res.*, 2018, **57**, 10180–10186.
- 13 M. C. E. Groves, “*Nitric Acid*,” in *Kirk-Othmer Encyclopedia of Chemical Technology*, John Wiley & Sons, 5th edn, 2020,



<https://doi.org/10.1002/0471238961.1409201803120118.a01>. pub3.

14 Q. Hu, Y. Qin, X. Wang, Z. Wang, X. Huang, H. Zheng, K. Gao, H. Yang, P. Zhang, M. Shao and C. He, *Energy Environ. Sci.*, 2021, **14**, 4989–4997.

15 D. Chen, S. Zhang, D. Yin, W. Li, X. Bu, Q. Quan, Z. Lai, W. Wang, Y. Meng, C. Liu, S. Yip, F. R. Chen, C. Zhi and J. C. Ho, *Adv. Energy Mater.*, 2022, **13**, 2203201.

16 P. H. van Langevelde, I. Katsounaros and M. T. M. Koper, *Joule*, 2021, **5**, 290–294.

17 S. Shukla and A. Saxena, *Handbook of Environmental Materials Management*, Springer, 2018, pp. 1–21, [https://doi.org/10.1007/978-3-319-58538-3\\_20-1](https://doi.org/10.1007/978-3-319-58538-3_20-1).

18 WHO, *Guidelines for drinking-water quality: incorporating the first and second addenda*, 4th edn, 2022.

19 E. Abascal, L. Gomez-Coma, I. Ortiz and A. Ortiz, *Sci. Total Environ.*, 2022, **810**, 152233.

20 L. Su, K. Li, H. Zhang, M. Fan, D. Ying, T. Sun, Y. Wang and J. Jia, *Water Res.*, 2017, **120**, 1–11.

21 R. Chauhan and V. C. Srivastava, *Chem. Eng. J.*, 2020, **386**, 122065.

22 I. Katsounaros, M. Dortsiou and G. Kyriacou, *J. Hazard. Mater.*, 2009, **171**, 323–327.

23 L. Mi, Q. Huo, J. Cao, X. Chen, H. Yang, Q. Hu and C. He, *Adv. Energy Mater.*, 2022, **12**, 2202247.

24 S. Li, D. Han, G. Jiang, Z. Han, H. Lu, J. Gao, X. Wang, Y. Wang, C. Geng, Z. Weng and Q.-H. Yang, *ACS Appl. Energy Mater.*, 2023, **6**, 5067–5073.

25 Z. Xu, L. Wan, Y. Liao, M. Pang, Q. Xu, P. Wang and B. Wang, *Nat. Commun.*, 2023, **14**, 1619.

26 F. Lv, M. Sun, Y. Hu, J. Xu, W. Huang, N. Han, B. Huang and Y. Li, *Energy Environ. Sci.*, 2023, **16**, 201–209.

27 N. Zhou, Z. Wang, N. Zhang, D. Bao, H. Zhong and X. Zhang, *ACS Catal.*, 2023, **13**, 7529–7537.

28 X. Li, X. He, J. Yao, K. Dong, L. Hu, J. Chen, L. Zhang, X. Fan, Z. Cai, S. Sun, D. Zheng, M. S. Hamdy, Q. Liu, Y. Luo, Y. Liao and X. Sun, *ChemSusChem*, 2023, e202300505.

29 J. Li, H. Liu, F. Du, L. Liu, Y. Gu, C. Li, C. Guo and H. Wang, *Chem. Eng. J.*, 2023, **471**, 144488.

30 K. Guillard and K. L. Kopp, *J. Environ. Qual.*, 2004, **33**, 1822–1827.

31 M. Duca and M. T. M. Koper, *Energy Environ. Sci.*, 2012, **5**, 9726.

32 Y. Liu, M. Chen, X. Zhao, H. Zhang, Y. Zhao and Y. Zhou, *Chem. Eng. J.*, 2023, **475**, 146176.

33 Y. Wang, W. Zhou, R. Jia, Y. Yu and B. Zhang, *Angew. Chem., Int. Ed.*, 2020, **59**, 5350–5354.

34 *Nat. Catal.*, 2022, **5**, 1071–1072.

35 S. Garcia-Segura, M. Lanzarini-Lopes, K. Hristovski and P. Westerhoff, *Appl. Catal., B*, 2018, **236**, 546–568.

36 Z. Wu, Y. Song, Y. Liu, W. Luo, W. Li and J. Yang, *Chem. Catal.*, 2023, **3**, 100786.

37 H. Jiang, G. F. Chen, O. Savateev, J. Xue, L. X. Ding, Z. Liang, M. Antonietti and H. Wang, *Angew. Chem., Int. Ed.*, 2023, **62**, e202218717.

38 H. Zhang, C. Wang, H. Luo, J. Chen, M. Kuang and J. Yang, *Angew. Chem., Int. Ed.*, 2023, **62**, e202217071.

39 J. Lim, Y. Chen, D. A. Cullen, S. W. Lee, T. P. Senftle and M. C. Hatzell, *ACS Catal.*, 2022, **13**, 87–98.

40 H. Luo, S. Li, Z. Wu, Y. Liu, W. Luo, W. Li, D. Zhang, J. Chen and J. Yang, *Adv. Mater.*, 2023, e2304695.

41 X. Zhao, K. Zhao, X. Quan, S. Chen, H. Yu, Z. Zhang, J. Niu and S. Zhang, *Chem. Eng. J.*, 2021, **415**, 128958.

42 L. Su, D. Han, G. Zhu, H. Xu, W. Luo, L. Wang, W. Jiang, A. Dong and J. Yang, *Nano Lett.*, 2019, **19**, 5423–5430.

43 F. Zhang, J. Luo, J. Chen, H. Luo, M. Jiang, C. Yang, H. Zhang, J. Chen, A. Dong and J. Yang, *Angew. Chem., Int. Ed.*, 2023, **62**, e202310383.

44 J. Kim, M.-J. Hwang, S.-J. Lee, W. Noh, J. M. Kwon, J. S. Choi and C.-M. Kang, *Bioresour. Technol.*, 2016, **205**, 269–273.

45 R. Mohammadi, D. L. Ramasamy and M. Sillanpää, *Desalination*, 2021, **498**, 114726.

46 Y. Luo, K. Xie, P. Ou, C. Lavallais, T. Peng, Z. Chen, Z. Zhang, N. Wang, X.-Y. Li, I. Grigioni, B. Liu, D. Sinton, J. B. Dunn and E. H. Sargent, *Nat. Catal.*, 2023, **6**, 939–948.

47 C. Lv, L. Zhong, H. Liu, Z. Fang, C. Yan, M. Chen, Y. Kong, C. Lee, D. Liu, S. Li, J. Liu, L. Song, G. Chen, Q. Yan and G. Yu, *Nat. Sustainability*, 2021, **4**, 868–876.

48 R. Wang, K. Yang, C. Wong, H. Aguirre-Villegas, R. Larson, F. Brushett, M. Qin and S. Jin, *Nat. Sustainability*, 2024, DOI: [10.1038/s41893-023-01252-z](https://doi.org/10.1038/s41893-023-01252-z).

