# **Catalysis<br>Science & Technology** Technology (SS)

## PAPER

Cite this: Catal. Sci. Technol., 2024, 14, 3407

Received 20th March 2024, Accepted 6th May 2024

DOI: 10.1039/d4cy00373j

rsc.li/catalysis

### 1 Introduction

Selective catalytic reduction of nitrogen oxides  $(NO<sub>x</sub>)$  with  $NH<sub>3</sub>$  as a reducing agent (NH<sub>3</sub>-SCR) is a leading technology for diesel exhaust emission control.  $NH<sub>3</sub>-SCR$  involves the reduction of NO<sub>x</sub> to N<sub>2</sub> and H<sub>2</sub>O in the presence of NH<sub>3</sub> and  $O_2$ .<sup>1-3</sup> In the last two decades, Cu-exchanged zeolites with a chabazite structure (Cu–CHA) have emerged as the preferred catalysts thanks to their high activity, selectivity and high tolerance to sulfur oxides.3–<sup>5</sup> Zeolites are alumino-silicates composed of tetrahedral units of  $SiO<sub>4</sub>$  and  $AlO<sub>4</sub>$ .<sup>6</sup> The tetrahedral units are in CHA arranged to form 4-, 6-, and 8-membered rings. The presence of Al creates a negative charge that is balanced by a proton or in the case of Cu–CHA, Cu ions. One general issue with zeolite-based catalysts is deactivation due to dealumination when the catalyst material is exposed to water vapor at high temperatures (>850 K for

 $b$  Umicore Denmark ApS, DK 2970 Horsholm, Denmark

## Mechanism for Cu-enhanced hydrothermal stability of Cu–CHA for  $NH<sub>3</sub>$ -SCR $\dagger$

Shivangi Singh, \*ab Ton V. W. Janssens **D** b and Henrik Grönbeck **D** \*a

Exposure of acidic zeolite-based catalysts to water at high temperatures generally leads to deactivation due to dealumination. In Cu–CHA zeolite, which is a preferred catalyst for the selective catalytic reduction of NO by NH<sub>3</sub> (NH<sub>3</sub>-SCR), the acidic protons in the zeolite are partially exchanged by Cu ions. The presence of Cu has been measured to reduce the rate of dealumination, thus stabilizing the catalyst. To understand the stabilizing effect of Cu, density functional theory calculations, ab initio thermodynamics and microkinetic modeling are used to compare the reaction mechanism for the dealumination of H–CHA to Cu–CHA. For H–CHA, we find that dealumination leads to the formation of mobile Al(OH)<sub>3</sub>H<sub>2</sub>O (extraframework aluminum) species, whereas for Cu–CHA, formation of framework bound Cu–Al species is thermodynamically preferred over Al(OH)<sub>3</sub>H<sub>2</sub>O, which results in the increased stability of Cu-CHA. The formation of mobile Al(OH)<sub>3</sub>H<sub>2</sub>O in Cu–CHA is, moreover, associated with a high energy barrier. The phase diagrams show the formation of Al(OH)<sub>3</sub>H<sub>2</sub>O and Al<sub>2</sub>O<sub>3</sub> from H–CHA and that high temperatures favor the formation of Al<sub>2</sub>O<sub>3</sub>. For Cu–CHA, high temperatures lead to the formation of CuO and Al<sub>2</sub>O<sub>3</sub>, which is favored over Al(OH)<sub>3</sub>H<sub>2</sub>O + CuO. The microkinetic model shows that the formation of Al(OH)<sub>3</sub>H<sub>2</sub>O in the presence of water starts at 380 K and 800 K in H–CHA and Cu–CHA, respectively. Additionally, the time evolution of the Al(OH)<sub>3</sub>H<sub>2</sub>O coverage at 923 K reveals that the process of dealumination is significantly faster for H–CHA as compared to Cu–CHA, which is in accordance with the measured increased stability. **PAPER**<br> **(a)** Checkforundates<br>
Case of the contract and the contract of the method intervention of the MCH and Stability of Cu-CHA for NH<sub>3</sub>-SCR†<br>
The method case is the contract and the contract of the second contract a

Cu–CHA7 ). Dealumination refers to the removal of aluminum from the zeolite framework, resulting in structural changes that adversely affect the catalytic activity, leading to catalyst degradation.<sup>8,9</sup>

The exhaust stream of diesel engines contains typically 2– 9% water. The interaction of water with aluminum in the zeolite framework results in sequential breakage of the Al–O bonds and ultimately to the formation of silanol groups and extra-framework aluminum.<sup>10,11</sup> Extra-framework aluminum in HCHA has been measured to contain different forms of aluminum oxide  $(AI_2O_3)$ , together with tetrahedral, pentagonal and octahedral coordinated aluminum ions.<sup>12,13</sup> Octahedrally coordinated Al ions  $(A(OH)_3(H_2O)_3)$  are unstable above 395 K and converts to tetrahedrally coordinated aluminum  $(AI(OH)_3H_2O)^{12}$  A recent infrared spectroscopy study has indicated the formation of hydroxylated aluminum oxide clusters during the steaming process.<sup>14</sup> Solid-state nuclear magnetic resonance measurements show a reduction in tetrahedrally coordinated framework aluminum upon water exposure, indicating dealumination. Dealumination is associated with a decrease in the number of Brønsted acid sites, which has been measured with infrared spectroscopy and temperature-programmed desorption.<sup>14-16</sup>

Atomic scale computational studies have primarily focused on the dealumination mechanism in H–CHA. The

<sup>&</sup>lt;sup>a</sup> Department of Physics, Competence Centre for Catalysis, Chalmers University of Technology, Sweden. E-mail: shivangi.singh@chalmers.se, ghj@chalmers.se; Tel: +46 3177 22963

<sup>†</sup> Electronic supplementary information (ESI) available: Results for dealumination with SAR = 35, thermodynamic results with a hybrid functional, hydrolysis barriers for different Al-distributions, and DFT optimized atomic structures. See DOI: <https://doi.org/10.1039/d4cy00373j>

initial stage of dealumination involves water adsorbing on aluminum, yielding a pentahedral or distorted tetrahedral Al atom. Following this, the first Al–O hydrolysis step occurs through the dissociation of a water molecule. The sequential addition of water molecules results in extra-framework aluminum.17–<sup>19</sup> Monte Carlo simulations for H–CHA under steam conditions (725 K, 1 bar) predict that more than three water molecules are present per unit cell and the collective action of more than one water molecule has been found to decrease the energy barrier for dealumination.<sup>20</sup> Dealumination is usually associated with high temperature although NH<sub>4</sub>-Y zeolite dealuminates already at  $450-500$  K.<sup>15</sup>

The protons in H–CHA can be replaced with Cu ions, which at high temperatures predominately are present in the  $Cu<sup>2+</sup>$  oxidation state as  $Z_2Cu$  (where Z represents the anionic Al site in the zeolite framework).<sup>9</sup> Copper is in the  $Z_2$ configuration located in the plane of a 6-membered ring, balancing the negative charge of two aluminum sites. Cu– CHA has demonstrated a higher resistance to dealumination than H–CHA when exposed to water vapor at high temperatures. Early XRD measurements have shown that the zeolite structure of  $NH_4$ -CHA breaks down at 850-900 K, whereas Cu–CHA remains stable up to  $1100-1150$  K.<sup>21</sup> Moreover, Kwak et al. observed that the  $NO<sub>x</sub>$  conversion over Cu–CHA was only weakly affected by hydrothermal aging at 800 °C for 16 hours, which was consistent with minor changes in the solid state Al-NMR spectra between fresh and aged samples.<sup>22</sup>

Linking hydrothermal deactivation of Cu–CHA with atomic-scale reactions is complex because of the possibility of many simultaneous processes and products.<sup>23</sup> The processes include (1) dealumination as for H–CHA, (2) the formation of copper oxide (CuO) species, (3) the agglomeration of Cu–Al species into copper aluminate (CuAl<sub>2</sub>-O4) and (4) complete collapse of the zeolite framework. Previous studies have reported the formation of a Cu–Al phase in a hydrothermally aged Cu-ZSM-5 zeolite and the clustering of Cu-Al species in Cu-CHA zeolite.<sup>23,24</sup> The major product depends on the Cu/Al ratio; samples with a high Cu content show  $CuO<sub>x</sub>$  cluster formation and conversion of ZCuOH to  $CuO_x$ .<sup>25</sup>

Numerous experimental studies have been performed to elucidate the kinetics of dealumination. Masuda et al. studied the dealumination in MFI-type zeolite and measured the reaction order with respect to steam partial pressure to be 1.5 at 1 bar and 773 K.<sup>11</sup> Furthermore, the apparent activation energy of dealumination in HZSM-5 has been measured to be about 1.1 eV at a water pressure of 5 kPa and 873 K.<sup>8</sup> In a recent study, density functional theory (DFT) calculations and microkinetic modeling were used to investigate the dealumination of H–CHA, allowing for a detailed understanding of the measured reaction kinetics.<sup>20</sup> Previous studies have primarily focused on the dealumination mechanism in H–CHA and HZSM-5 zeolites. An atomic-level understanding explaining how copper stabilizes the zeolite framework in Cu–CHA and why

dealumination in Cu–CHA is delayed compared to  $H/NH_4$ – CHA is still lacking. Here, we use DFT calculations to compare the dealumination mechanisms in H–CHA and Cu– CHA and elucidate the enhanced hydrothermal stability of Cu–CHA. The study is performed in three steps. First, the potential energy landscapes for dealumination of H–CHA and Cu–CHA are calculated to identify the reaction pathway and analyze the reaction barriers. Second, phase diagrams are constructed to investigate the thermodynamic stability of different reaction products resulting from dealumination under different temperature and pressure conditions. Third, a DFT-informed microkinetic model is constructed to simulate the evolution of extra-framework alumina as a function of temperature and water pressure. We find that the formation of extra-framework aluminum species is faster for H–CHA as compared to Cu–CHA, which is related to higher barriers for hydrolysis in Cu–CHA. An additional reason for the increased stability of Cu–CHA is the preferential formation of framework bound Cu–Al species instead of mobile Al(OH)3H2O. Our work provides a material-based description of the hydrothermal stability of Cu–CHA catalysts for NH<sub>3</sub>-SCR. **Paper** Catalysis Science & Technical sings on Catalysis Science & Technology<br>
nitriductions in educations in the set and the set and the set are the dealer<br>
nature and the set are the set and the set are the dealer in th

### 2 Computational methods

### 2.1 Electronic structure calculations

Spin-polarized density functional theory (DFT) calculations are performed with the Vienna ab initio simulation package (VASP).26–<sup>29</sup> The interaction between the valence and core electrons is described by the plane augmented wave (PAW) method, and the Kohn–Sham orbitals are expanded with plane waves using an energy cutoff of 480 eV. $30,31$  The number of electrons treated in the valence is  $Cu(11)$ ,  $Si(4)$ ,  $Al(3)$ ,  $O(6)$ , and H(1). The Perdew–Burke–Ernzerhof (PBE) exchange–correlation functional is used together with a Grimme-D3 correction, which accounts for the van der Waals interactions. $32-34$ Moreover, a Hubbard-U correction of 6 eV is applied to enforce the localization of 3d electrons in  $Cu^{35,36}$  The chosen treatment of the electronic interactions is evaluated by comparative calculations using the hybrid functional HSE06.37,38 The relative stability of the considered solid phases is found to depend weakly on the functional, see the ESI.† The electronic structure is considered to be converged when the change of electronic energy and Kohn–Sham eigenvalues between two iterations is smaller than  $1 \times 10^{-6}$  eV.

Structures are optimized with the conjugate gradient method. Geometries are considered to be converged when the largest force is smaller than 0.05 eV Å<sup>-1</sup>. Only the gamma point was used to sample the Brillouin zone. Transition states are located using the climbing image nudge elastic band (NEB) method<sup>39-41</sup> with a spring constant of 5.0 eV  $\AA^{-1}$ . Transition states are confirmed by vibrational analysis using the finite difference method. Born–Oppenheimer ab initio molecular dynamics (AIMD) with a time step of 1 fs is employed to explore and identify the minimum energy structure of CHA in a canonical (NVT) ensemble at 300 K.

### Catalysis Science & Technology Paper

The temperature of the simulation is controlled using a Nosé-Hoover thermostat<sup>42,43</sup> and the masses of the H atoms are set to 3 amu to allow for a large time step.

The chabazite structure is modeled with a hexagonal unit cell, which includes 36 tetrahedrally coordinated silicon atoms (T-sites). Calculations are performed with the experimental lattice parameters of  $a = b = 13.8$  Å,  $c = 15.0$  Å,  $\alpha = \beta = 90.0^{\circ}$ , and  $\gamma = 120.0^{\circ}$ . H-CHA is modeled with either one or two aluminum (Al) in a 6-membered ring. Thus, the considered Si/Al ratios are 35 and 17. The two models are denoted as 1H–CHA and 2H–CHA, respectively. The results for 1H–CHA are reported in the ESI.† Catalysis Science & Technology<br>
The temperature of the simulation is controlled using a<br>
Note-Hiremetr berms on the First article is article. The article is licensed under the simulation of the first<br>
or the Hiremetr berm

#### 2.2 Evaluation of entropy

The rate constant includes both enthalpy and entropy changes. Evaluation of entropies for species in confined volumes, such as zeolites, is generally challenging.<sup>44,45</sup> The entropy of a gas phase water molecule is given by:

$$
Sgas = Sgastrans + Sgasrot + Sgasvib
$$
 (1)

where  $S_{\text{trans}}^{\text{gas}}, S_{\text{rot}}^{\text{gas}},$  and  $S_{\text{vib}}^{\text{gas}}$  are the translational, rotational, and vibrational entropies, respectively. To account for the entropy loss when water enters the zeolite cage, the translational and rotational entropy of the water inside the cage is taken to be two-thirds of gas-phase water.<sup>44</sup> The same approach is used for  $Al(OH)_{3}H_{2}O$  and water adsorbed on a Brønsted acid site within a zeolite. Thus, the entropy is given by:

$$
S = S_{\rm vib}^{\rm Zeo} + \frac{2}{3} \left( S_{\rm trans}^{\rm gas} + S_{\rm rot}^{\rm gas} \right) \tag{2}
$$

The entropy contribution is evaluated as frustrated vibrations for other intermediates, which are a part of the zeolite framework and exhibit strongly restricted motion.

#### 2.3 Evaluation of phase diagrams

To study the temperature-dependent relative stability of extraframework aluminum species and alumina, Gibbs free energies at 50 mbar pressure (water) are determined for the optimized zeolite structure. The enthalpy is approximated by the zero-point corrected electronic energy, neglecting the  $pV$ term. This approximation is based on the assumption that the pressure–volume work is small compared to the electronic energy contributions, which is reasonable as the volume and pressure do not change in the reaction. The entropy contributions from the lattice vibration for the zeolite and the considered bulk phases are calculated using the PHONOPY code.<sup>46</sup> The Gibbs free energy ( $\Delta G$ ) for the formation of extra-framework aluminum species and alumina is calculated according to:<sup>47</sup>

$$
\Delta G(T, p) = G_{\text{Si}_{34}\text{AlO}_{72}\text{H}_{5}}(T) + G_{\text{Al(OH)}_{3}\text{H}_{2}\text{O}}(T, p) - G_{\text{Si}_{34}\text{Al}_{2}\text{O}_{72}\text{H}_{2}}(T) - 4\mu_{\text{H}_{2}\text{O}}(T, p)
$$
\n(3)

$$
\Delta G(T, p) = G_{\text{Si}_{34}\text{O}_{72}\text{H}_8}(T) + 2G_{\text{Al(OH)}_3\text{H}_2\text{O}}(T, p) + G_{\text{CuO}}(T) - G_{\text{Si}_{34}\text{Al}_2\text{O}_{72}\text{Cu}_1}(T) - 9\mu_{\text{H}_2\text{O}} \tag{4}
$$

$$
\Delta G(T, p) = G_{\text{Si}_{34}\text{AlO}_{72}\text{H}_5}(T) + \frac{1}{2} G_{\text{Al}_2\text{O}_3}(T) - G_{\text{Si}_{34}\text{Al}_2\text{O}_{72}\text{H}_2}(T) \tag{5}
$$

$$
-\frac{3}{2} \mu_{\text{H}_2\text{O}}(T, p)
$$

$$
\Delta G(T, p) = G_{\text{Si}_{34}\text{O}_{72}\text{H}_{8}}(T) + G_{\text{Al}_{2}\text{O}_{3}}(T) + G_{\text{CuO}}(T) - G_{\text{Si}_{34}\text{Al}_{2}\text{O}_{72}\text{Cu}_{1}}(T) - 4\mu_{\text{H}_{2}\text{O}}(T, p) \tag{6}
$$

with  $G_{\text{Si}_{34} \text{Al}_{2}\text{O}_{72} \text{H}_{2}}$  being 2H–CHA,  $G_{\text{Si}_{34} \text{AlO}_{72} \text{H}_{5}}$  being dealuminated 2H–CHA with four Si–OH groups,  $G_{\text{Si}_{34}\text{Al}_{2}\text{O}_{72}\text{Cu}_{1}}$ being Z<sub>2</sub>Cu,  $G_{\text{Si}_{34}\text{O}_7\text{H}_8}$  being dealuminated Z<sub>2</sub>Cu with with four Si-OH groups,  $G_{\text{Al(OH)}_3\text{H}_2\text{O}}$  being extra-framework aluminum species,  $G_{\text{Al},\text{O}_2}$  being alumina, and  $G_{\text{CuO}}$  being copper oxide.  $\mu_{\text{H}_2O}$  is the chemical potential of water.

#### 2.4 Microkinetic model

The microkinetic model is based on the mean-field approach, which assumes that the system is homogeneous and that species are randomly distributed. The time evolution of the surface coverages is obtained by solving a set of ordinary differential equations.<sup>48</sup>

$$
\frac{\mathrm{d}\theta_j}{\mathrm{d}t} = \sum_i \nu_{ij} r_i \tag{7}
$$

where  $\theta_i$  is the fractional coverage of species j,  $v_{ii}$  is the stoichiometric coefficient of species  $j$  in the elementary reaction  $i$ , and  $r_i$  is the rate of  $i$ -th elementary reaction. SciPy is used to numerically solve the differential equations. The solver uses the backward differentiation formula (BDF) method and integrates the differential equations.

The rate constant for the adsorption of water on the Brønsted acid site is estimated using collision theory:<sup>48</sup>

$$
k_{\rm ads} = \frac{P_{\rm water} s_0 A}{\sqrt{2\pi m k_{\rm b} T}} \tag{8}
$$

where  $P$  is the pressure of the water,  $s_0$  is the sticking coefficient, which is considered to be one in this case, A is the area of the 8-membered ring,  $m$  is the mass of water,  $k<sub>b</sub>$ is the Boltzmann constant and  $T$  is the temperature. Thermodynamic consistency is ensured by calculating the desorption rate constant from  $k_{ads}$  and the equilibrium constant:

$$
k_{\text{des}} = \frac{k_{\text{ads}}}{K_{\text{eq}}} \tag{9}
$$

The rate constants for the surface reactions are calculated with transition state theory.<sup>49</sup> Transition state theory is based on two important assumptions: (1) the product is formed via an activated complex (transition state) through a loose vibration, and (2) the transition state and the reactants of the elementary steps are in quasi-equilibrium. The second

assumption implies that the transition state has a finite lifetime, and during this time, the reactant molecules have an opportunity to proceed toward the formation of products or revert to the reactants. The rate constant is in the transition state theory given by:

$$
k = \frac{k_{\rm b}T}{h} \exp\left(\frac{\Delta S^{\dagger}}{R}\right) \exp\left(-\frac{\Delta H^{\dagger}}{RT}\right) \approx \frac{k_{\rm b}T}{h} \exp\left(\frac{\Delta S^{\dagger}}{R}\right) \exp\left(-\frac{\Delta E^{\dagger}}{RT}\right) \tag{10}
$$

where  $\Delta H^{\dagger}$  and  $\Delta S^{\dagger}$  are the enthalpy and entropy change for the formation of the transition state from the reactants. As  $pV$  does not change along the reaction path,  $H^{\dagger}$  is approximated by  $\Delta E$  (the zero-point corrected barrier of the elementary step).

### 3 Results and discussion

#### 3.1 Potential energy landscapes

The considered dealumination pathway is based on the mechanism proposed by Silaghi et  $al.^{19}$  The complete dealumination requires a minimum of four water molecules and consists of four hydrolysis steps in which the breaking of the Al–O bonds takes place. The reaction scheme for hydrolysis of the first Al–O bond is shown in Fig. 1. The hydrolysis process starts with (II) adsorption on the Brønsted acid site, which has the highest adsorption energy, (III) diffusion of the water molecule to the aluminum site, (TS-I) initiation of hydrolysis of the Al–O–Si bond, and (IV) breaking of the Al–O–Si bond. The hydrolysis of the remaining three Al–O bonds occurs in a similar fashion leading to the formation of an  $Al(OH)_{3}H_{2}O$  species and a socalled silanol nest (four hydrogen bonded Si–OH groups).

3.1.1 Dealumination mechanism of 2H–CHA. 2H–CHA consists of two aluminum atoms in a 6-membered ring, charge balanced by two protons resulting in two Brønsted acid sites. The Si/Al ratio is, in this case, 17. The potential energy landscape for the dealumination of 2H–CHA is shown in Fig. 2 with the corresponding structures in Fig. 3. The first H2O adsorbs with an adsorption energy of −0.97 eV at the Brønsted acid site and subsequently diffuses to adsorb on the Al site where it dissociates with a barrier of 0.85 eV. Following the first water molecule, the second water molecule adsorbs at a neighboring proton site with an adsorption energy of −0.84 eV. Like the first water molecule, it diffuses to the Al site where it dissociates. This step has a barrier of 0.74 eV. The third water molecule adsorbs at yet another Brønsted acid site with an adsorption energy of −0.75 eV.



Fig. 1 Reaction scheme for hydrolysis of the first Al–O bond in 2H– CHA.



Fig. 2 Potential energy landscape for dealumination of 2H–CHA.

Through the subsequent diffusion, it binds to the Al site and dissociates. This step has a barrier of 0.66 eV. The fourth water molecule adsorbs with an adsorption energy of −0.95 eV and forms extra-framework aluminum species in the form of Al $(OH)_{3}H_{2}O$  with a barrier of 0.88 eV. The formation of extra-framework aluminum is exothermic by −1.49 eV. The first and the last steps in the energy landscape have the highest barriers, whereas the third step has the lowest barrier. However, the effective barrier, taking the need for diffusion before hydrolysis into account, is highest for the first step (1.25 eV) and lowest for the last step (0.88 eV). The potential energy landscape for dealumination of H–CHA with an Si/Al ratio of 35 (1H–CHA) is reported in the ESI.† The main difference with respect to 2H–CHA is the last hydrolysis step, which for 1H–CHA has a barrier of only 0.09 eV. **Catalysis Science Article** and the transition state has a finite<br>
inform, and done published on present in the resument in the case of the same of t

3.1.2 Dealumination mechanism of Cu–CHA (Z2Cu). The dealumination pathway for Cu–CHA is similar to that for 2H– CHA. In  $Z_2Cu$ ,  $Cu^{2+}$  is located in the plane of the



Fig. 3 Intermediates for dealumination of 2H–CHA. Atomic color codes: Cu (bronze), Si (yellow), Al (pink), O (red), and H (white).



Fig. 4 Reaction scheme for hydrolysis of the first Al–O bond in Cu– **CHA** 

6-membered ring, balancing the negative charge of two aluminum ions. The reaction scheme for hydrolysis of the first Al–O bond is shown in Fig. 4. The hydrolysis of the first Al–O bond in the Cu–CHA consists of the following steps: (II) adsorption of water on the lowest energy site, which is the copper site, (III) diffusion of the water molecule to the aluminum site, (TS-I) initiation of hydrolysis of the Al–O–Si bond, and (IV) breaking of the Al–O–Si bond. Complete dealumination takes places after four hydrolysis steps and leads to either an  $Al(OH)_{3}H_{2}O$  or a Cu–Al species.

The energy landscape for the dealumination process of Cu–CHA is shown in Fig. 5 with the corresponding structures in Fig. 6. The first water molecule adsorbs on the copper site with an adsorption energy of −0.90 eV and dissociates over the copper site with an energy barrier of 1.33 eV. The second water molecule adsorbs at the copper site with an adsorption energy of −1.20 eV. Subsequently, water diffuses to the aluminum site where it dissociates. This step involves a barrier of 0.66 eV. The third water molecule adsorbs at the aluminum site with an adsorption energy of −0.68 eV, where it dissociates forming IX. Finally, the fourth water molecule adsorbs at the copper site with an adsorption energy of −0.40 eV. After diffusion to the aluminum site, either an extraframework aluminum species  $(AI(OH)_{3}H_{2}O)$  or a copperaluminum species is formed. The barrier to form the extraframework aluminum species is higher than that to form the framework-bound copper–aluminum species, 1.54 eV as compared to 0.72 eV. Both reaction products are exothermic with respect to  $Z_2$ Cu and water in the gas phase. However, the formation of structure XII (with  $Al(OH)_{3}H_{2}O$ ) is endothermic with respect to structure X, whereas structure XI (with the Cu–Al species) is exothermic with respect to structure X. The barriers for hydrolysis of the Al–O bonds in



Fig. 5 Potential energy landscape for dealumination of Cu–CHA.





Cu–CHA are higher than those for the 2H–CHA case. The third hydrolysis step has the highest barrier being 1.88 eV.

### 3.2 Thermodynamic stability

Before discussing the kinetics of the dealumination reaction for 2H–CHA and Cu–CHA, it is interesting to examine the thermodynamic stability of the products formed during dealumination. Previous studies have established that exposing zeolites to steam at high temperatures leads to the formation of  $Al_2O_3$  and  $Al(OH)_3H_2O^{14,50}$  The phase diagrams for the reactions at different temperatures have been constructed considering a fixed water partial pressure of 50 mbar. The reactions of interest are:

$$
Si34Al2O72H2 + \frac{3}{2}H2O = Si34AlO72H5 + \frac{1}{2}Al2O3
$$
  
(Pristine 2H-CHA) (Dealuminated 2H-CHA) (11)

$$
Si34Al2O72H2 + 4H2O \rightleftharpoons Si34AlO72H5 + Al(OH)3H2O
$$
\n(Pristine 2H–CHA) (Dealuminated 2H–CHA) (12)

$$
Si34Al2O72Cu1 + 4H2O \rightleftharpoons Si34O72H8 + Al2O3 + CuO(Pristine Cu-CHA) (Dealuminated Cu-CHA) (13)
$$

Fig. 7 shows the formation of  $Al(OH)_{3}H_{2}O$  and  $Al_{2}O_{3}$  from 2H–CHA and Cu–CHA, respectively. The phase diagram shows that the free energy of the formation of  $Al(OH)_{2}H_{2}O$  is endothermic after 350 K, which is in agreement with a previous report by Nielsen *et al.*<sup>51</sup> The formation of Al(OH)<sub>3</sub>-H2O is endothermic already at 335 K in the case of Cu–CHA.  $Al(OH)_{3}H_{2}O$  will eventually form bulk phases and the formation of the aluminum oxide is found to be endothermic above 510 K for 2H–CHA, whereas the formation of aluminum oxide and copper oxide is endothermic above 840 K for Cu– CHA. The reason that the formation of dealumination products is endothermic at elevated temperatures is connected to the considerable loss of entropy during hydrolysis of gas-phase water. The entropy contribution to the free energy of a water molecule at 1000 K is ∼2.4 eV.



Fig. 7 Phase diagram showing the stability of extra-framework aluminum species, aluminum oxide and copper oxide in 2H–CHA and Cu–CHA.

### Paper Catalysis Science & Technology

The relative thermodynamic stability could be affected by the choice of the exchange–correlation functional. To ensure the accuracy of the results, we compared the results of the  $PBE + U + D3$  calculations with calculations using a hybrid functional (HSE06 + D3), see the ESI. $\dagger$  The enthalpy change between the functionals differs only by 0.15 eV for eqn (13). The relatively small discrepancy suggests that the phase diagrams with the PBE  $+ U + D3$  approach have a reasonable accuracy. The phase diagrams suggest that the thermodynamics of dealumination, in principle, does not require high temperatures. The high temperature could instead be needed for kinetic reasons, which have motivated us to construct a microkinetic model for the dealumination of 2H–CHA and Cu–CHA.

#### 3.3 Microkinetic modeling of dealumination

A microkinetic model for dealumination in 2H–CHA and Cu– CHA has been constructed to investigate kinetic limitations. A microkinetic model provides a possibility to examine dominant species as a function of time and temperature. Additionally, it assists in identifying which elementary steps influence the kinetics of the overall dealumination mechanism. In the microkinetic model, some intermediates have been omitted for simplicity and a state of "gas-phase" water inside the zeolite cage has been added. The state with gas-phase water is added to simplify the handling of entropy changes. The entropy for the gas-phase water state in the zeolite is evaluated according to eqn (2). The entropy of other intermediate states is determined within the harmonic approximation treating rotations and translations as frustrated vibrations. The last elementary step in both reaction paths is considered to be irreversible. Treating the last step as irreversible effectively accounts for a large entropy barrier adding an Al ion from an extra-framework aluminum species to the zeolite framework. The elementary steps involved in the dealumination of 2H–CHA and Cu–CHA are described in Table 1. **Catalysis Science & Technique (Satalysis Science & Technique)**<br>
(Pissine Cu-CTA) (Dealuminaal Cu-CTA) the characteristic interesting compared the creative of the creative of the creative of the creative of the creative o

> The microkinetic analysis is performed at a water partial pressure of 50 mbar. The temperature-dependent coverages are shown in Fig. 8(A) for 2H–CHA after  $10<sup>7</sup>$  seconds. The surface is predominantly occupied by species II below 380 K, which refers to the state where one water molecule is adsorbed on the Brønsted acid site. This is a consequence of the strong adsorption of water on the Brønsted acid site (−0.73 eV). The fraction of species II decreases with increasing temperature, while the fraction of extra-framework aluminum species reaches unity. The switch in the dominant surface species occurs at about 380 K.

> The temperature-dependent fraction of surface species for Cu–CHA is shown in Fig.  $8(B)$  after  $10<sup>7</sup>$  seconds. The dominant surface species is II below 600 K, IV at intermediate temperatures and extra-framework aluminum in the high-temperature limit. The low-temperature preference for II is a consequence of the relatively high adsorption energies (−1.19 eV). Similarly, the presence of IV is related to

**Table 1** Energy ( $\Delta E^{\ddagger}$ ) and entropy ( $\Delta S^{\ddagger}$ ) contributions of the elementary reaction considered in the dealumination process. Energy and entropy are given in eV and J mol $^{-1}$  K $^{-1}$ , respectively.  $\Delta \mathsf{S}^{\ddagger}$  is given at standard state

No.	Elementary step	$E_{\rm f}^{\ddag}$	$E_{\rm D}^{\ddag}$	$S_{\rm f}^{\ddag}$	$S_{\rm b}^{\ddag}$
$2H-CHA$					
r1	I-H <sub>2</sub> O (cage) $=$ II	$-0.73$	0.73	$-95.86$	95.86
r2	$II = IV$	1.25	0.51	$-1.30$	$-3.06$
r3	$IV + H2O = V$	$-0.84$	0.84	$-105.59$	105.59
r4	$V \approx VII$	1.18	0.37	6.58	2.98
r5	$VII + H_2O = VIII$	$-0.75$	0.75	$-100.17$	100.17
r <sub>6</sub>	$VIII = X$	1.04	0.35	$-0.18$	$-18.77$
r7	$X + H_2O = XI$	$-0.95$	0.95	$-111.56$	111.56
r8	$XI \rightarrow XIII$	0.92	0.62	3.49	$-10.72$
$Cu-CHA$					
r9	$I-H_2O$ (cage) $=$ II	$-0.67$	0.67	$-77.04$	77.04
r10	$II \Rightarrow III$	1.33	0.84	$-31.09$	$-8.01$
r11	$III + H2O = IV$	$-1.19$	1.19	$-99.77$	99.77
r12	$IV = VI$	1.16	0.52	$-5.02$	$-2.10$
r13	$VI + H2O = VII$	$-0.68$	0.68	$-96.70$	96.70
r14	$VII = VIII$	1.88	1.63	3.61	8.25
r15	VIII + $H_2O = IX$	$-0.40$	0.40	$-81.85$	81.85
r16	$IX \rightarrow XII$	1.73	0.31	$-10.16$	0.87

the high adsorption energies and high barriers for continuing the reaction. The appearance of the extraframework aluminum species becomes noticeable at 900 K, indicating that the formation of extra-framework aluminum is favored only at high temperatures.

To facilitate the comparison between the two systems, we study the time dependence of the extra-framework aluminum formation at 923.15 K, Fig. 8(C). Specifically, we find that the



Fig. 8 Coverage of the different species as a function of temperature calculated at an integration time of  $10^7$  seconds for (A) 2H–CHA and (B) Cu–CHA. (C) Coverage of the extra-framework aluminum species (EFALs) as a function of time at 923 K for 2H–CHA (low barrier and high barrier are shown with blue and grey lines, respectively) and Cu–CHA (shown in red), and (D) relationship between the barrier and the energy difference between the final and initial states for the first Al–O(H) bond breaking. Black and red dots represent H–CHA with SARs of 17 and 35, respectively.

coverage of extra-framework aluminum species in 2H–CHA becomes appreciable after 0.003 seconds, whereas the corresponding time is  $10^8$  seconds (3 years) for Cu–CHA. The comparison shows that the process of dealumination in Cu– CHA is slow as compared to 2H–CHA and that the presence of copper in the zeolite significantly influences the dealumination reaction.

The kinetics of the dealumination for 2H–CHA is largely determined by the first barrier. This is corroborated by a sensitivity analysis where the barrier for the different reactions is changed while keeping the thermodynamics fixed. Increasing the different barriers by 0.2 eV, we find that the evolution of the surface species is mainly dependent on the first hydrolysis step. Knowing that the first barrier mainly determines the kinetics for 2H–CHA, it is interesting to investigate the dependence of this barrier on the Al distribution. We calculated the barrier for the first hydrolysis step for 8 different Al configurations (see the ESI† for details). We find that the barrier is lowest (0.85 eV) when the Al atoms are placed on opposite sides of a 6-membered ring (two Si atoms apart). Higher barriers are calculated for configurations with one Al atom in the 6-membered ring and the other Al atom in an 8-membered ring with the highest barrier being 1.23 eV. The hydrolysis step is in these cases performed on the Brønsted site connected to the Al in the 6-membered ring. With the calculations for different Al distributions, we are able to establish a relationship, which shows the barrier of the reaction as a function of the difference in energy between the final and initial states of the reaction. The results are shown in Fig. 8(D). Catalysis Science & Technology<br>
Task Computer Science & Technology<br>
Task Computer Science Computer Science Computer Science Commons are the science of the common Access Article<br>
2021. The commons are the science of the co

As the Al distribution can result in a wide range of hydrolysis barriers, we simulate the evolution of the extra framework aluminum for different barriers. In Fig. 8(C), we show the time dependence of the extra framework aluminum formation at 923.15 K for the highest and lowest barriers associated with the first hydrolysis step. For the highest barrier (1.23 eV), we find that the formation of extraframework aluminum becomes appreciable only after a duration of 0.3 seconds, which is a noticeable delay in the formation of extra-framework aluminum as compared to the case with the lowest barrier (0.85 eV). The delay demonstrates that the Al distribution clearly affects the rate of dealumination.

The reaction orders and apparent activation energies for dealumination in 2H–CHA and Cu–CHA were calculated to further characterize the kinetics of the dealumination. The reaction order was determined at the initial rise of the reaction rate curve, ensuring that the coverage of extraframework aluminum is low. The reaction order for 2H–CHA was calculated to be 1.6 at a temperature of 295 K and in a pressure range between 50 mbar and 55 mbar, which is fairly close to the experimentally determined reaction order of 1.5 (at 773 K and in a pressure range between 10 mbar and 1 bar).<sup>11</sup> The apparent activation energy of 2H-CHA was calculated to be 1.2 eV at a pressure of 50 mbar within a temperature range of 290 to 305 K. The apparent activation

energy can largely be related to the first adsorption energy and first dealumination barrier. The calculated apparent activation energy is close to the experimental value of 1.09 eV reported by Sano et al. at 50 mbar and temperatures between 740 and 1000 K.<sup>8</sup> The reaction order and apparent activation energy for Cu–CHA were calculated to be 4.7 (analyzed at 50– 55 mbar and 820 K) and 2.6 eV (analyzed at 785–920 K at 50 mbar), respectively. The high apparent activation energy for Cu–CHA is related to the third reaction barrier together with the low barrier for the reversed second hydrolysis step, making IV the dominant species at intermediate temperatures (Fig. 8B).

### 4 Conclusion

Using density functional theory calculations in combination with *ab initio* thermodynamics and microkinetic modeling, we have investigated the dealumination mechanism in H– CHA and Cu–CHA. We find that the introduction of copper into the zeolite structure increases the barriers for dealumination compared to the H–CHA. Thus, the rate of dealumination is decreased in the presence of Cu. With Cu, some of the extra-framework Al species in the zeolite form bonds with the copper ions, resulting in Cu-bound Al species. The formation of copper-bound aluminum species is thermodynamically favorable compared to the formation of  $Al(OH)_{3}H_{2}O$  species. The reversibility of the formation of the Cu-bound Al species is an additional reason for a decreased rate of dealumination in the presence of Cu. We find that the formation of  $Al_2O_3$  or  $Al_2O_3$  + CuO is thermodynamically preferred with respect to the formation of extra-framework aluminum at high temperatures. The microkinetic model revealed a clear temperature difference in the onset of dealumination for H–CHA and Cu–CHA. In the case of H– CHA, the barrier for the first hydrolysis step was calculated for different Al distributions. The Al distribution was found to clearly affect the barrier, with a difference of ∼0.4 eV between the lowest and highest barriers. Our results rationalize the higher hydrothermal stability of Cu–CHA as compared to H–CHA and show that careful steering of the Al distribution is one route for increased hydrothermal stability. **Catalysis Science** Catalysis Science Articles. The control of the model on the control of the contro

### Conflicts of interest

There are no conflicts to declare.

### Acknowledgements

We acknowledge support from the European Union's Horizon 2020 Research and Innovation Programme under the Marie Sklodowska-Curie grant agreement no. 955839 (CHASS). Additional support from the Swedish Energy Agency (47110-1) is acknowledged. The calculations have been performed at C3SE (Göteborg) and NSC (Linköping) through a NAISS grant. The Competence Centre for Catalysis (KCK) is hosted by Chalmers University of Technology and financially supported by the Swedish Energy Agency (52689-1) and the member

companies Johnson Matthey, Perstorp, Powercell, Preem, Scania CV, Umicore and Volvo Group.

### Notes and references

- 1 A. M. Beale, F. Gao, I. Lezcano-Gonzalez, C. H. Peden and J. Szanyi, Chem. Soc. Rev., 2015, 44, 7371–7405.
- 2 R. K. Srivastava, W. Neuffer, D. Grano, S. Khan, J. Staudt and W. Jozewicz, Environ. Prog., 2005, 24, 181–197.
- 3 F. Gao, J. H. Kwak, J. Szanyi and C. H. Peden, Top. Catal., 2013, 56, 1441–1459.
- 4 J. H. Kwak, R. G. Tonkyn, D. H. Kim, J. Szanyi and C. H. Peden, J. Catal., 2010, 275, 187–190.
- 5 S. J. Schmieg, S. H. Oh, C. H. Kim, D. B. Brown, J. H. Lee, C. H. Peden and D. H. Kim, Catal. Today, 2012, 184, 252–261.
- 6 R. E. Morris and P. Nachtigall et al., Zeolites in catalysis: properties and applications, Royal Society of Chemistry, 2017.
- 7 F. Gao and J. Szanyi, Appl. Catal., A, 2018, 560, 185–194.
- 8 T. Sano, H. Ikeya, T. Kasuno, Z. Wang, Y. Kawakami and K. Soga, Zeolites, 1997, 19, 80–86.
- 9 J. Luo, F. Gao, K. Kamasamudram, N. Currier, C. H. Peden and A. Yezerets, J. Catal., 2017, 348, 291–299.
- 10 S. M. Campbell, D. M. Bibby, J. M. Coddington, R. F. Howe and R. H. Meinhold, J. Catal., 1996, 161, 338–349.
- 11 T. Masuda, Y. Fujikata, S. R. Mukai and K. Hashimoto, Appl. Catal., A, 1998, 172, 73–83.
- 12 J. A. van Bokhoven, A. M. Van der Eerden and D. C. Koningsberger, J. Am. Chem. Soc., 2003, 125, 7435–7442.
- 13 D. L. Bhering, A. Ramírez-Solís and C. J. Mota, J. Phys. Chem. B, 2003, 107, 4342–4347.
- 14 K. Khivantsev, N. R. Jaegers, L. Kovarik, M. A. Derewinski, J.-H. Kwak and J. Szanyi, Molecules, 2022, 27, 2352.
- 15 G. Agostini, C. Lamberti, L. Palin, M. Milanesio, N. Danilina, B. Xu, M. Janousch and J. A. Van Bokhoven, *J. Am. Chem.* Soc., 2010, 132, 667–678.
- 16 Y. Xi, C. Su, N. A. Ottinger and Z. G. Liu, Appl. Catal., B, 2021, 284, 119749.
- 17 S. Malola, S. Svelle, F. L. Bleken and O. Swang, Angew. Chem., Int. Ed., 2012, 51, 652–655.
- 18 K. Stanciakova, B. Ensing, F. Goltl, R. E. Bulo and B. M. Weckhuysen, ACS Catal., 2019, 9, 5119–5135.
- 19 M.-C. Silaghi, C. Chizallet, J. Sauer and P. Raybaud, J. Catal., 2016, 339, 242–255.
- 20 M. Nielsen, A. Hafreager, R. Y. Brogaard, K. De Wispelaere, H. Falsig, P. Beato, V. Van Speybroeck and S. Svelle, Catal. Sci. Technol., 2019, 9, 3721–3725.
- 21 D. W. Fickel and R. F. Lobo, J. Phys. Chem. C, 2010, 114, 1633–1640.
- 22 J. H. Kwak, D. Tran, S. D. Burton, J. Szanyi, J. H. Lee and C. H. Peden, J. Catal., 2012, 287, 203–209.
- 23 J. E. Schmidt, R. Oord, W. Guo, J. D. Poplawsky and B. M. Weckhuysen, Nat. Commun., 2017, 8, 1666.
- 24 P. N. Vennestrøm, T. V. Janssens, A. Kustov, M. Grill, A. Puig-Molina, L. F. Lundegaard, R. R. Tiruvalam, P. Concepción and A. Corma, J. Catal., 2014, 309, 477–490.

## Catalysis Science & Technology Paper

- 25 J. Song, Y. Wang, E. D. Walter, N. M. Washton, D. Mei, L. Kovarik, M. H. Engelhard, S. Prodinger, Y. Wang and C. H. Peden, et al., ACS Catal., 2017, 7, 8214–8227.
- 26 G. Kresse and J. Hafner, Phys. Rev. B: Condens. Matter Mater. Phys., 1993, 48, 13115.
- 27 G. Kresse and J. Hafner, Phys. Rev. B: Condens. Matter Mater. Phys., 1994, 49, 14251.
- 28 G. Kresse and J. Furthmüller, Comput. Mater. Sci., 1996, 6, 15-50.
- 29 G. Kresse and J. Furthmüller, Phys. Rev. B: Condens. Matter Mater. Phys., 1996, 54, 11169.
- 30 P. E. Blöchl, Phys. Rev. B: Condens. Matter Mater. Phys., 1994, 50, 17953.
- 31 G. Kresse and D. Joubert, Phys. Rev. B: Condens. Matter Mater. Phys., 1999, 59, 1758.
- 32 J. P. Perdew, K. Burke and M. Ernzerhof, Phys. Rev. Lett., 1996, 77, 3865.
- 33 S. Grimme, J. Antony, S. Ehrlich and H. Krieg, J. Chem. Phys., 2010, 132, year.
- 34 S. Grimme, S. Ehrlich and L. Goerigk, J. Comput. Chem., 2011, 32, 1456–1465.
- 35 L. Chen, T. V. Janssens and H. Grönbeck, Phys. Chem. Chem. Phys., 2019, 21, 10923-10930.
- 36 L. Y. Isseroff and E. A. Carter, Phys. Rev. B: Condens. Matter Mater. Phys., 2012, 85, 235142.
- 37 J. Heyd, G. E. Scuseria and M. Ernzerhof, J. Chem. Phys., 2003, 118, 8207–8215.
- 38 J. Heyd and G. E. Scuseria, J. Chem. Phys., 2004, 121, 1187–1192.
- 39 G. Mills, H. Jónsson and G. K. Schenter, Surf. Sci., 1995, 324, 305–337.
- 40 H. Jónsson, G. Mills and K. W. Jacobsen, Classical and quantum dynamics in condensed phase simulations, World Scientific, 1998, pp. 385–404.
- 41 G. Henkelman and H. Jónsson, J. Chem. Phys., 2000, 113, 9978–9985.
- 42 S. Nosé, J. Chem. Phys., 1984, 81, 511–519.
- 43 S. Nosé, Mol. Phys., 1984, 52, 255–268.
- 44 M. Jørgensen, L. Chen and H. Gronbeck, J. Phys. Chem. C, 2018, 122, 20351–20357.
- 45 G. Piccini, M. Alessio, J. Sauer, Y. Zhi, Y. Liu, R. Kolvenbach, A. Jentys and J. A. Lercher, J. Phys. Chem. C, 2015, 119, 6128–6137.
- 46 A. Togo and I. Tanaka, Scr. Mater., 2015, 108, 1–5.
- 47 J. Rogal and K. Reuter, Ab initio atomistic thermodynamics for surfaces: A primer, in Experiment, Modeling and Simulation of Gas-Surface Interactions for Reactive Flows in Hypersonic Flights, Educational Notes RTO-EN-AVT-142, Paper 2, France: RTO, Neuilly-sur Seine, 2006, pp. 2-1–2-18. Catalysis Science & Technology<br>
25 J. Song, Y. Wang, E. D. Walter, N. M. Wahlon, D. Mci, L. 39 G. Milk, H. Jonsson, and G. K. Schenter, Surf, Sci., 1998, 23<br>
Newton, M. K. Fryderion, S. Prodieson, State Brownloade (C. H.
	- 48 I. Chorkendorff and J. W. Niemantsverdriet, Concepts of modern catalysis and kinetics, John Wiley & Sons, 2017.
	- 49 H. Eyring, Chem. Rev., 1935, 17, 65–77.
	- 50 R. Simancas, A. Chokkalingam, S. P. Elangovan, Z. Liu, T. Sano, K. Iyoki, T. Wakihara and T. Okubo, Chem. Sci., 2021, 12, 7677–7695.
	- 51 M. Nielsen, R. Y. Brogaard, H. Falsig, P. Beato, O. Swang and S. Svelle, ACS Catal., 2015, 5, 7131–7139.