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## Synthesis of amine derivatives from furoin and furil over a Ru/Al<sub>2</sub>O<sub>3</sub> catalyst†

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The direct/reductive amination of carbohydrate-based furoin and furil with NH<sub>3</sub>/H<sub>2</sub> was investigated to access amine derivatives. In the sole presence of NH<sub>3</sub>, cyclic amines, *i.e.* 2,3,5,6-tetra(furan-2-yl)pyrazine and 2,2'-bipyridine-3,3'-diol, were generated as the main products from furoin and furil, respectively. Over Ru/Al<sub>2</sub>O<sub>3</sub> under NH<sub>3</sub>/H<sub>2</sub>, 2-amino-1,2-di(furan-2-yl)ethan-1-ol (*i.e.* alcohol-amine) was generated as the main product with 47% yield at 140 °C for 2 h starting from furoin. The catalyst could be recycled for at least three consecutive runs. An alcohol-imine was the main intermediate that underwent tautomerization to alcohol-enamine/keto-amine leading to cyclic by-products by self-condensation. DFT calculations, complementing the experimental observations, provided detailed molecular-level insight into the reactivity of the alcohol-imine intermediate. Its preferential adsorption on Ru centers *via* the NH group, with the OH group pointing away from the surface, was found to direct its hydrogenation towards the alcohol-amine as main product. By combining Ru/Al<sub>2</sub>O<sub>3</sub> and a silica-anchored N-heterocyclic carbene (NHC) catalyst, the alcohol-amine could be accessed with 42% overall yield in a single reactor.

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## Introduction

Furfural (FF) is a cheap commercial platform molecule (1.0–1.2€ per kg) that can be prepared at a large scale by dehydration of carbohydrates (>200 kT per year).<sup>1</sup> FF can be used as a building block for accessing a variety of products and intermediates.<sup>1c,2</sup> In particular, FF can be converted into amines by reductive amination, which are valuable intermediates to manufacture polymers, surfactants, biologically active molecules and pharmaceuticals (*e.g.*, furosemide).<sup>3</sup> The synthesis of furfurylamines can be conducted from FF and 5-hydroxymethylfurfural (HMF) by direct/reductive amination over homogeneous and heterogeneous catalysts.<sup>4</sup> Also, secondary and tertiary tetrahydrofurfurylamines can be

accessed with high yield (>90%) from FF over Pd/Al<sub>2</sub>O<sub>3</sub> at room temperature and 1 bar H<sub>2</sub>.<sup>5</sup>

An upgrading process of FF comprises C–C bond coupling and amination. In this view, it is desirable to design multistep processes with a high degree of intensification and high activity/selectivity to the desired amines. One-pot reactions have been reported for the synthesis of furan- and THF-derived amines combining an aldol condensation reaction of FF with ketones, followed by reductive amination with NH<sub>3</sub> and H<sub>2</sub>, over a mixture of Amberlyst-26 (A26) and Ru/C or Pd/Al<sub>2</sub>O<sub>3</sub> catalysts.<sup>6</sup> For example, using Pd/Al<sub>2</sub>O<sub>3</sub> as a catalyst and H<sub>2</sub> (2.0 MPa) as a reductant, 98% overall yield of THF-amine was achieved at 120 °C after 20 h.<sup>6b</sup>

Benzoin condensation is a C–C coupling reaction that can promote the self-condensation of aldehydes using nucleophiles such as cyanides or N-heterocyclic carbenes (NHC) as catalysts.<sup>7</sup> FF and HMF can self-condense towards 5,5'-dihydroxymethylfuroin (DHMF) derivatives using NHC organocatalysts.<sup>8</sup> The reaction mechanism operates *via* umpolung condensation as proposed by Breslow.<sup>9</sup> In particular, benz-imidazolium (bim) salts with one/two long-chain aliphatic substituents at the N-atoms in the imidazole ring are active catalysts for the reaction.<sup>10</sup> Bim catalysts have been supported over silica and polymers with controlled mesoporosity, affording recyclable heterogeneous catalysts.<sup>11</sup> In the presence of a base (*e.g.*, 1,8-diazabicyclo[5.4.0]undec-7-ene, DBU), supported bim catalysts can catalyze the self-condensation of FF into furoin with 96–99% yield over three

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consecutive runs. Sequential reactions have been developed encompassing furoin derivatives targeting the synthesis of branched alkanes. Furoin/furil intermediates derived from FF can be hydrogenated towards THF-derivatives and subjected to ring opening by hydrodeoxygenation over  $\text{Pd/C} + \text{La}(\text{OTf})_3/\text{Eu}(\text{OTf})_3$  catalysts, accessing  $\text{C}_{10}\text{--C}_{12}$  diesel fuels.<sup>8b,12</sup> Furoin/furil intermediates have also been employed to prepare  $\text{C}_{12}$  biofuels by subsequent esterification and etherification reactions.<sup>13</sup>

Herein we investigated the direct/reductive amination of furoin and furil with  $\text{NH}_3/\text{H}_2$  over 5%  $\text{Ru}/\text{Al}_2\text{O}_3$ . DFT calculations were implemented to rationalize the nature and stability of surface species on  $\text{Ru}(0001)$  in the presence of adsorbed  $\text{NH}_3$  and ad-H, as well as the formation of 2-amino-1,2-di(furan-2-yl)ethan-1-ol (*i.e.* alcohol-amine) as main product and the alcohol-imine and its tautomers leading to cyclic by-products. We also engineered a single-reactor tandem process by combining silica-supported bim to catalyze benzoin condensation (C-C coupling), and 5%  $\text{Ru}/\text{Al}_2\text{O}_3$  to catalyze reductive amination, to access furoin alcohol-amine starting from FF.

## Results and discussion

### Catalyst-free conversion of furoin/furil under $\text{NH}_3$

Furoin was first reacted with both  $\text{NH}_3$  and ammonium acetate as an  $\text{NH}_3$  surrogate in *N,N*-dimethylformamide (DMF). 2,3,5,6-Tetra(furan-2-yl)pyrazine is generated as the main product at a temperature higher than 130 °C (Scheme 1), which is in accordance with an earlier report.<sup>14</sup> The yield is about 15–18% at full furoin conversion by reacting furoin at 140 °C for 4 h, using 0.06 g of furoin, 6 mL of DMF and 1 g of ammonium acetate (or 0.22 g  $\text{NH}_3$ ). A myriad of minor products are generated with low yield (<5%), including 2-amino-1,2-di(furan-2-yl)ethan-1-ol. The easier operation and higher solubility of ammonium acetate as a masked  $\text{NH}_3$  reagent compared to gas  $\text{NH}_3$  prompted us to use this reagent in the forthcoming experiments.

We next explored the effect of the operation variables on the yield of 2,3,5,6-tetra(furan-2-yl)pyrazine at 140 °C for 4 h. Among the solvents tested, DMF, THF and 2-methyl-THF afford a yield of 18–21% (Table S1†). The reaction does not proceed in water most likely due to the poor solubility of furoin. We further studied the effect of the temperature using THF for 3 h reaction while keeping the other reaction conditions unchanged (Table S2†). The yield of 2,3,5,6-tetra(furan-2-yl)pyrazine increases monotonously in the range of 130–160 °C up to 30% at full conversion. The highest yield

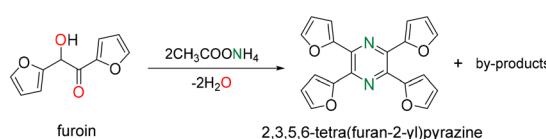
(30%) occurs for an ammonium acetate loading above 0.1 g at 160 °C in THF (Table S3†). The yield of 2,3,5,6-tetra(furan-2-yl)pyrazine reaches 44% at 160 °C for 3 h using dry THF and dry ammonium acetate (Table S4†).

A possible reaction mechanism for 2,3,5,6-tetra(furan-2-yl)pyrazine formation by reaction of furoin with ammonium acetate/ $\text{NH}_3$  is depicted in Scheme 2. The first step consists of the nucleophilic attack of  $\text{NH}_3$  to the carbonyl group of furoin to generate an alcohol-imine intermediate with concomitant release of one water molecule. This intermediate can undergo tautomerization to alcohol-enamine/keto-amine by-products ( $m/z = 191$ ) that can be hardly distinguished by GC-MS. The self-condensation of the keto-amine, followed by dehydrogenation, results in 2,3,5,6-tetra(furan-2-yl)pyrazine.

Next, we reacted furil with  $\text{NH}_3$  in DMF. 2,2'-Bipyridine-3,3'-diol is generated as the main product with a yield of 22% at 170 °C after 4 h at full furil conversion (Scheme 3, Table S5†). A variety of by-products are generated with low yield (<5%), including 2-amino-1,2-di(furan-2-yl)ethan-1-ol and 1,2-di(furan-2-yl)ethane-1,2-diamine (*i.e.* diamine). The yield of 2,2'-bipyridine-3,3'-diol increases to 36% at 180 °C, but decreases further to 24% at 200 °C (Table S6†). This observation suggests partial product/substrate decomposition at higher temperature. The formation of 2,2'-bipyridine-3,3'-diol can be rationalized on the basis of the mechanism depicted in Scheme 4. Furil reacts fast with  $\text{NH}_3$  generating a diimine intermediate. This intermediate is unstable and may be easily activated by a proton in solution favoring ring activation and intramolecular rearrangement leading to pyridine rings. The diimine intermediate can also suffer from reversible polymerization, as earlier observed for diformylfuran upon exposure to  $\text{NH}_3$ .<sup>15</sup>

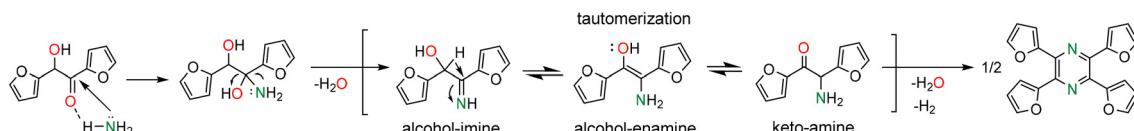
### Furoin and furil amination in the presence of a catalyst

With the results above, we studied the reductive amination of furoin and furil with  $\text{NH}_3$  and  $\text{H}_2$ . The catalytic tests were first conducted using furoin at 80 °C and 100 °C in DMF over 5%  $\text{Pd}/\text{Al}_2\text{O}_3$  and 5%  $\text{Ru}/\text{Al}_2\text{O}_3$  catalysts (Fig. S1† and 1).  $\text{Pd}/\text{Al}_2\text{O}_3$  provides a broad distribution of products, especially at lower temperature (Fig. 1A). In contrast, the alcohol-amine is formed as the main product over  $\text{Ru}/\text{Al}_2\text{O}_3$  (Fig. 1B), as confirmed by GC-MS and  $^1\text{H}$  NMR (presence of two doublets centered at 4.7 ppm and 5.4 ppm) (Fig. S2†). The alcohol-imine and its possible tautomers (keto-amine, alcohol-enamine), and the keto-imine, appear as the main by-products. The detection of the keto-imine suggests the formation of furil from furoin dehydrogenation along the reaction despite the presence of  $\text{H}_2$  in the reaction medium. Indeed, we confirmed that furil can be generated at room temperature under neat conditions (*i.e.* without  $\text{NH}_3/\text{H}_2$ ) (Fig. 1C). Additional peaks are observed at higher temperature (not shown) that can be attributed to cyclic by-products, especially 2,3,5,6-tetra(furan-2-yl)pyrazine, and minor formation of oligomers.



**Scheme 1** Catalyst-free furoin amination with  $\text{NH}_3/\text{ammonium acetate}$ .





**Scheme 2** Proposed mechanism for 2,3,5,6-tetra(furan-2-yl)pyrazine formation from the reaction of furoin with ammonium acetate/NH<sub>3</sub>.

We measured the yield of alcohol-amine from furoin amination over 5% Pd/Al<sub>2</sub>O<sub>3</sub>, 5% Ru/Al<sub>2</sub>O<sub>3</sub>, 5% Rh/Al<sub>2</sub>O<sub>3</sub> and 5% Pt/Al<sub>2</sub>O<sub>3</sub>, at 160 °C for 2 h (Table 1). The first three catalysts exhibit poor yield (up to 28%) (entries 1–3), whereas the yield over 5% Ru/Al<sub>2</sub>O<sub>3</sub> is the highest (40%) (entry 7) at full furoin conversion. The yield of alcohol-amine is poorly affected by the Ru loading (entries 4–6) and the type of support (*i.e.* alumina, silica, carbon) at the same Ru loading (5 wt%) (entries 7–9). The alcohol-imine and its tautomers are generated as the main by-products, as well as 2,3,5,6-tetra(furan-2-yl)pyrazine (not quantified).

The yield of alcohol-amine increases with the temperature in the range of 80–140 °C at 4.0 MPa H<sub>2</sub> pressure with a maximum value of 47%, but decreases slightly further to 40% at 160 °C that we attribute to the formation of oligomers (Fig. 2). The yield of alcohol-amine also increases with the H<sub>2</sub> pressure in the range of 0.5–4.0 MPa at constant temperature (160 °C) and keeps unchanged beyond 4.0 MPa (Fig. 3). The alcohol-imine (and possible tautomers) is generated as the main by-product, which can be further hydrogenated to the alcohol-amine product and generate 2,3,5,6-tetra(furan-2-yl)pyrazine and oligomers that were not quantified. However, the keto-imine, which is generated at 80 and 100 °C, vanishes at higher temperature. The catalyst is robust under reaction conditions, and can be reused for three consecutive catalytic runs with a yield of alcohol-amine in the range of 40–45% (Fig. 4).

We also studied the reductive amination of furil with NH<sub>3</sub> and H<sub>2</sub> over Ru/Al<sub>2</sub>O<sub>3</sub>. As in the case of furoin, the alcohol-amine is generated as the main product with 34% yield together with the diimine and 2,2'-bipyridine-3,3'-diol as the main by-products, as well as oligomers. Diamines are generated with less than 5% yield.

### Understanding furoin amination over 5% Ru/Al<sub>2</sub>O<sub>3</sub>

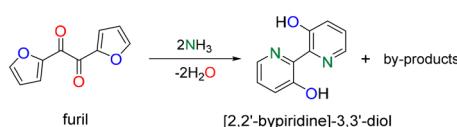
The results above point out the preferential formation of the alcohol-amine product over Ru/Al<sub>2</sub>O<sub>3</sub> at 140 °C and 2.0 MPa H<sub>2</sub> pressure starting from furoin, with ketone-amine/alcohol-imine being the main intermediates. To rationalize the formation of the alcohol-amine and cyclic by-products,

we computed the adsorption configurations and energies of the reactants (furoin, furil), end products (alcohol-amine, diamine) and possible intermediates (alcohol-imine + tautomers, diimine). The calculations were carried out both on a bare reduced Ru(0001) surface and on a reduced Ru(0001) surface covered with NH<sub>3</sub> and ad-H, at the DFT-PBE level (see the ESI† for computational details).

Table 2 lists the adsorption energies for the optimized configurations of the reactants, products and intermediates on bare and ad-H/NH<sub>3</sub>-covered Ru(0001). For adsorbed furoin (entries 1–4), four configurations were probed on the bare Ru(0001) interacting *via* (Scheme 5): i) C=O group, ii) OH group, iii) both C=O and OH groups, and iv) furan rings. The most stable configuration, *i.e.* iii), corresponds to a bidentate binding mode with C=O showing the shortest Ru–O distance. The adsorption energy on bare Ru(0001) (−156 kJ mol<sup>−1</sup>) (entry 4) is almost twice the sum of the energies for monodentate adsorption *via* C=O (i) and OH (ii) groups, *i.e.* −59 and −37 kJ mol<sup>−1</sup>, respectively (entries 1–2). No stable configuration occurs *via* furan rings as inferred from the positive adsorption energy (+14 kJ mol<sup>−1</sup>) (entry 3).

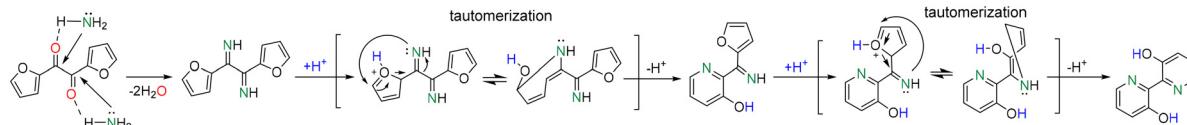
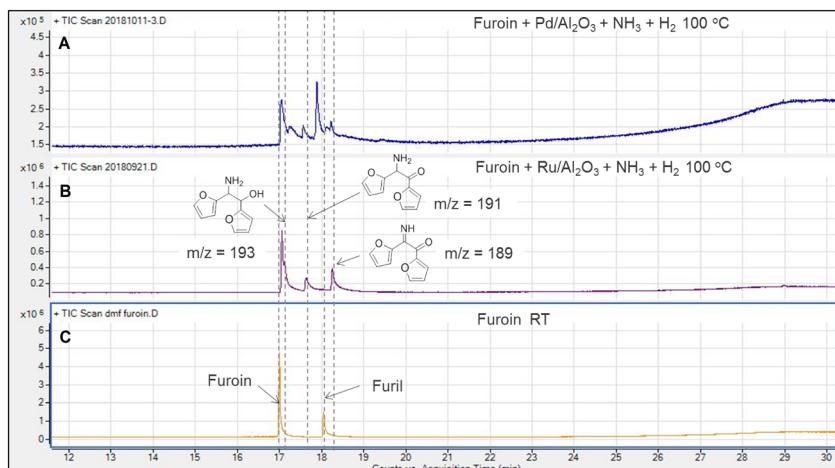
Few studies describe the atomistic details of H<sub>2</sub> and NH<sub>3</sub> co-adsorption on Ru(0001).<sup>16</sup> H<sub>2</sub> and NH<sub>3</sub> are known to occupy different sites on the Ru(0001) surface, so that ad-H atoms can influence the adsorption pattern of NH<sub>3</sub> on Ru(0001).<sup>16</sup> Since ad-H atoms occupy mainly fcc sites,<sup>17</sup> we simulated the dissociative H<sub>2</sub> chemisorption on fcc sites and NH<sub>3</sub> adsorption on adjacent top sites. First, we simulated a full monolayer of ad-H on fcc sites without NH<sub>3</sub> (Scheme 5a1). The adsorption energy is −111 kJ mol<sup>−1</sup> and keeps unchanged when implicit solvation by DMF is included (−112 kJ mol<sup>−1</sup>). Next, we simulated NH<sub>3</sub> chemisorption on only 25% of available top sites to take into account steric constraints (Scheme 5a2). Also, we assumed that no NH<sub>3</sub> dissociation occurs at the reaction temperature (up to 160 °C) given its high activation energy (>100 kJ mol<sup>−1</sup>),<sup>18</sup> and that adsorbed NH<sub>3</sub> is known to keep undissociated in the presence of ad-H species below 170 °C.<sup>17,19</sup> The adsorption energy of NH<sub>3</sub> is −75 kJ mol<sup>−1</sup> with a limited stabilizing effect of DMF (−5 kJ mol<sup>−1</sup>), which agrees well with an earlier report.<sup>20</sup> The average N–Ru distance is 2.2 Å that is similar to the distance measured for diamine and diimine derivatives. We also computed H<sub>2</sub> and NH<sub>3</sub> co-adsorption on Ru(0001) (Scheme 5a3). After geometry optimization, half of ad-H atoms move to neighboring hcp sites with a hexagonal arrangement around each adsorbed NH<sub>3</sub> molecule. The adsorption energy is −101 kJ mol<sup>−1</sup> (−104 kJ mol<sup>−1</sup> in DMF).

Using the optimized NH<sub>3</sub>- and ad-H-covered Ru(0001) surface, we simulated the adsorption of furoin/furil, products



**Scheme 3** Catalyst-free furil amination with NH<sub>3</sub>.



Scheme 4 Possible mechanism for 2,2'-bipyridine-3,3'-diol formation from the reaction of furil with NH<sub>3</sub>.Fig. 1 Representative GC plots for furoin amination with NH<sub>3</sub> and H<sub>2</sub> over (A) 5% Pd/Al<sub>2</sub>O<sub>3</sub>, (B) 5% Ru/Al<sub>2</sub>O<sub>3</sub>, and (C) neat conditions (RT) with neither NH<sub>3</sub> nor H<sub>2</sub>. Reaction conditions: furoin (0.12 g, 0.625 mmol), catalyst (24 mg), NH<sub>3</sub> (0.7 g), DMF (2 g), 100 °C, 4.0 MPa H<sub>2</sub>, 2 h. The catalysts were pre-reduced at 200 °C before the reaction.

and intermediates, and recomputed the adsorption energies (Scheme 5b–g, Table 2). As a rule, although the adsorption energies can show variations when different NH<sub>3</sub> and ad-H coverages are considered, the primary effect on the relative stability of the different species and their orientation is expected to be poorly affected.<sup>21</sup> With these considerations, all adsorption energies are lower on the NH<sub>3</sub>- and ad-H-covered Ru(0001) surface than on bare Ru(0001). However, the relative stability between furoin, diamine and diimine is preserved. Furil exhibits stronger adsorption than furoin ( $-107 \text{ kJ mol}^{-1}$  vs.  $-74 \text{ kJ mol}^{-1}$ , compare entries 5 and 4),

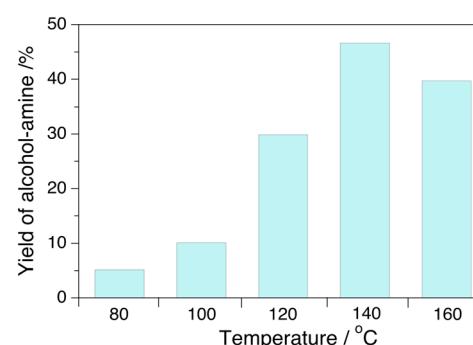
since the C=O–Ru interaction is kept when NH<sub>3</sub> covers the surface (Scheme 5e). In contrast, in the case of furoin, NH<sub>3</sub> bridges the interaction between the OH group and the Ru(0001) surface *via* H-bonding (Scheme 5b), resulting in lower stability.

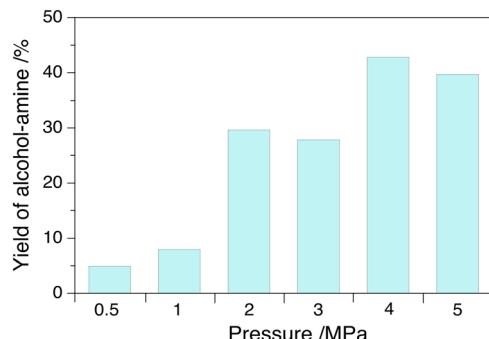
We also investigated the relative stability of the alcohol-imine and its two tautomers on Ru(0001) in the presence of adsorbed NH<sub>3</sub> and ad-H species. The alcohol-imine interacts preferentially with Ru(0001) *via* the NH group (Scheme 5g), but the adsorption energy is lower compared to the value on

Table 1 Survey of catalysts for the reductive amination of furoin with NH<sub>3</sub> and H<sub>2</sub><sup>a</sup>

Entry	Catalyst	Yield of alcohol–amine (%)
0	—	0
1	5% Pd/Al <sub>2</sub> O <sub>3</sub>	28
2	5% Rh/Al <sub>2</sub> O <sub>3</sub>	10
3	5% Pt/Al <sub>2</sub> O <sub>3</sub>	14
4	0.1% Ru/Al <sub>2</sub> O <sub>3</sub>	30
5	1% Ru/Al <sub>2</sub> O <sub>3</sub>	35
6	2% Ru/Al <sub>2</sub> O <sub>3</sub>	40
7	5% Ru/Al <sub>2</sub> O <sub>3</sub> (6.7 nm <sup>b</sup> )	40
8	5% Ru/SiO <sub>2</sub>	35
9	5% Ru/C (2.8 nm <sup>b</sup> )	40

<sup>a</sup> Reaction conditions: furoin (60 mg), NH<sub>3</sub> (0.45 g), % Ru/Al<sub>2</sub>O<sub>3</sub> (12 mg), DMF (2 mL), 160 °C, 2 h, H<sub>2</sub> (2.0 MPa). The catalyst was pre-reduced at 200 °C before the reaction. <sup>b</sup> Average particle size of Ru nanoparticles measured by HR-TEM.

Fig. 2 Effect of temperature on furoin amination with NH<sub>3</sub>/H<sub>2</sub> over 5% Ru/Al<sub>2</sub>O<sub>3</sub>. Reaction conditions: furoin (60 mg), NH<sub>3</sub> (0.45 g), 5% Ru/Al<sub>2</sub>O<sub>3</sub> (12 mg), DMF (2 mL), 2 h, 2.0 MPa H<sub>2</sub>, catalyst pre-reduced at 200 °C before the reaction. The furoin conversion was complete in all experiments. Alcohol-imine tautomers and 2,3,5,6-tetra(furan-2-yl)pyrazine were generated as the main by-products (not quantified).



**Fig. 3** Effect of  $\text{H}_2$  pressure on furoin amination with  $\text{NH}_3/\text{H}_2$  over 5%  $\text{Ru}/\text{Al}_2\text{O}_3$ . Reaction conditions: furoin (60 mg),  $\text{NH}_3$  (0.45 g), 5%  $\text{Ru}/\text{Al}_2\text{O}_3$  (12 mg), DMF (2 mL), 160 °C, 2 h, catalyst pre-reduced at 200 °C before the reaction. The furoin conversion was complete in all experiments. Alcohol-imine tautomers and 2,3,5,6-tetra(furan-2-yl)pyrazine were generated as the main by-products (not quantified).

the bare surface ( $-31$  vs.  $-92$   $\text{kJ mol}^{-1}$ , entry 9) due to steric hindrance. The alcohol-imine is  $-19$   $\text{kJ mol}^{-1}$  more stable than the alcohol-enamine and  $-8$   $\text{kJ mol}^{-1}$  more stable than the keto-amine tautomer over  $\text{NH}_3$  and ad-H-covered  $\text{Ru}(0001)$  (entries 10–11) (see also Fig. S3†). This relative stability opposes that observed in bulk solution, where the keto-enamine is the most stable tautomer being  $45$   $\text{kJ mol}^{-1}$  more stable than the alcohol-imine and  $27$   $\text{kJ mol}^{-1}$  less stable than the keto-amine.

This body of results points out that the alcohol-imine is a likely intermediate responsible for the formation of the alcohol-amine over  $\text{Ru}(0001)$ . The weak adsorption of the alcohol-imine and its tautomers over  $\text{Ru}(0001)$  can favor their desorption from the catalyst and the further formation of 2,3,5,6-tetra(furan-2-yl)pyrazine among other cyclic by-products in bulk solution competing with the alcohol-amine proceeding over the catalyst. Besides, preferential interaction of NH or  $\text{NH}_2$  groups of the alcohol-imine and keto-amine, respectively, on  $\text{Ru}(0001)$  discourages the formation of the diimine and amine-imine intermediates, and in turn hinders diamine formation. This selectivity shortcoming has also

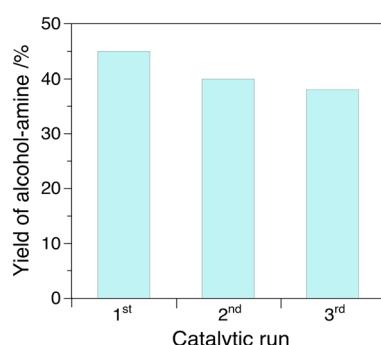
**Table 2** Energy of adsorption ( $\Delta E_{\text{ads}}$ ,  $\text{kJ mol}^{-1}$ ) of reactants, products and intermediates for the most stable configurations on bare  $\text{Ru}(0001)$  and the effect of coverage by  $\text{NH}_3$  and ad-H

Entry	Molecule	Interacting groups	$\Delta E_{\text{ads}} @ \text{bare Ru}(0001)$	$\Delta E_{\text{ads}} @ \text{ad-H and NH}_3 \text{ Ru}(0001)$
1	Furoin	C=O	-59	—
2	Furoin	OH	-37	—
3	Furoin	Furan rings	+14	—
4	Furoin	C=O + OH	-156	-74
5	Furil	C=O +	-115	-107
		C=O		
6	Alcohol-amine	NH <sub>2</sub>	-189	-36
7	Diamine	NH <sub>2</sub>	-91	-24
8	Diimine	NH + NH	-252	-185
9	Alcohol-imine	NH	-92	-31
10	Alcohol-enamine	NH <sub>2</sub>	-45	-12
11	Keto-amine	NH <sub>2</sub>	-67	-23

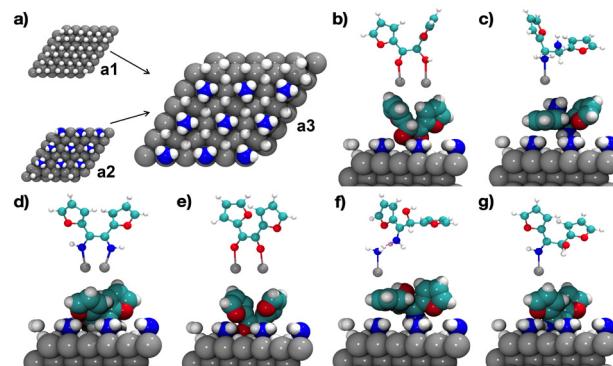
been observed in the amination of isosorbide with  $\text{NH}_3$  and  $\text{H}_2$ , where the *exo*-OH group exhibits much lower reactivity than the *endo*-OH group, resulting in the formation of amino-alcohols with different stereochemistry as the main products with small amounts of diamines.<sup>18</sup>

### Single-reactor tandem benzoin condensation + reductive amination process

With the results above, we investigated the credentials of a tandem reaction for the synthesis of the alcohol-amine starting from FF by combining supported bim-silica<sup>11d</sup> and  $\text{Ru}/\text{Al}_2\text{O}_3$  catalysts in a single reactor (Scheme 6). In this test, both catalysts were loaded in the reactor together with DMF, FF and DBU to activate bim. First, the benzoin condensation reaction was carried out at 30 °C for 20 h. Subsequently,  $\text{NH}_3$  and  $\text{H}_2$  were added, and the amination reaction was carried out at 140 °C for 2 h. The results clearly show the formation of the alcohol-amine product (Fig. 5) with 42% overall yield.

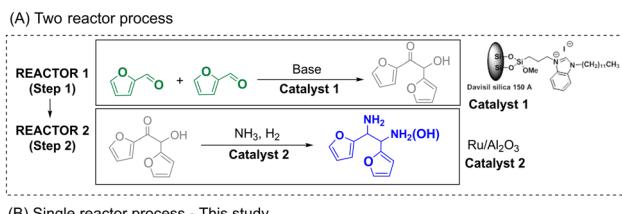


**Fig. 4** Catalyst recycling and reuse for experiments carried out over 5%  $\text{Ru}/\text{Al}_2\text{O}_3$ . Reaction conditions: 60 mg furoin, 0.45 g  $\text{NH}_3$ , 0.012 g 5%  $\text{Ru}/\text{Al}_2\text{O}_3$ , 2 mL DMF, 2 h, 4.0 MPa  $\text{H}_2$ , catalyst pre-reduced at 200 °C before the reaction.

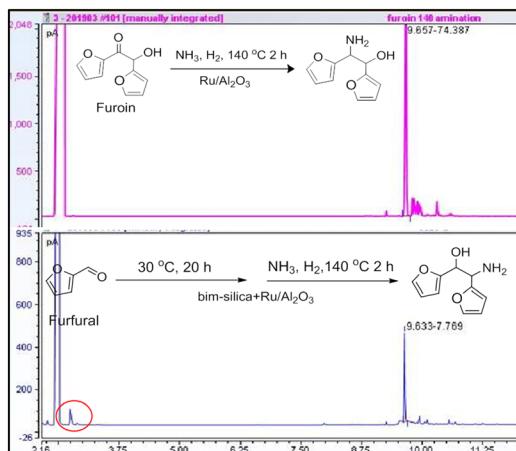


**Scheme 5** (a) Single  $\text{H}_2$  and  $\text{NH}_3$  coverage and co-coverage on  $\text{Ru}(0001)$  (a1–a3), and most stable surface configurations for (b) furoin, (c) diamine, (d) diimine, (e) furil, (f) alcohol-amine and (g) alcohol-imine, represented both as balls-and-stick representations of the interactions.





**Scheme 6** Two-reactor vs. single reactor tandem process for the synthesis of hydrogenated derivatives from FF.



**Fig. 5** Representative GC plots of the reaction system after the amination reaction of furoin with  $\text{NH}_3$  and  $\text{H}_2$  over (top)  $\text{Ru}/\text{Al}_2\text{O}_3$  and (bottom) bim-silica +  $\text{Ru}/\text{Al}_2\text{O}_3$  in the single-reactor tandem process. Reaction conditions: (top) furoin (0.12 g), 0.625 mmol, catalyst (24 mg), DMF (2 g),  $\text{NH}_3$  (0.7 g), 140 °C, 4.0 MPa  $\text{H}_2$ , 2 h, catalyst pre-reduced at 200 °C; (bottom) (1) benzoin condensation: FF (0.096 g, 1 mmol), DBU (26 mg, 0.17 mmol), bim-silica (0.16 g), catalyst (24 mg), DMF (2 g), 30 °C, 20 h, 5%  $\text{Ru}/\text{Al}_2\text{O}_3$  catalyst pre-reduced at 200 °C; (2) reductive amination: 0.7 g  $\text{NH}_3$ , 4.0 MPa  $\text{H}_2$ , 140 °C, 2 h.

To assess the stability of bim-silica in the presence of  $\text{NH}_3$  and  $\text{H}_2$ , the catalyst was extracted from the reaction system after the tandem reaction, washed with HCl and DMF and retested in the benzoin condensation of FF. The catalyst was found to be fully active (see the chromatogram in Fig. S4†), pointing out that the bim moiety is not detached from the support during the tandem reaction. TG analyses on the fresh and spent bim-silica catalysts confirm the stability of bim-silica during the tandem reaction (Fig. S5†).

## Conclusions

Along this study, we studied the direct/reductive amination of furoin and furil with  $\text{NH}_3$  and  $\text{H}_2$ . Without a catalyst, furoin reacts with either  $\text{NH}_3$  or ammonium acetate to generate 2,3,5,6-tetra(furan-2-yl)pyrazine with 39% yield. Furil also reacts with  $\text{NH}_3$  to generate 2,2'-bipyridine-3,3'-diol with 44% yield. When  $\text{Ru}/\text{Al}_2\text{O}_3$  and  $\text{H}_2$  were added to the reaction

system, furoin and furil generated 2-amino-1,2-di(furan-2-yl)ethan-1-ol (alcohol-amine) as the main product with 47% and 34% yield, respectively, at 140 °C for 2 h. DFT simulations underscored the significance of the unique adsorption orientation of these intermediates on  $\text{Ru}/\text{Al}_2\text{O}_3$ , with the NH group in proximity to Ru centers and the OH group oriented away from the surface. This orientation, as revealed by our computational analysis, plays a pivotal role in guiding the reaction towards the formation of alcohol-amine, corroborating the experimentally observed product distribution. The alcohol-imine exhibits weak adsorption on ad-H/ $\text{NH}_3$ -covered Ru, allowing the formation of 2,3,5,6-tetra(furan-2-yl)pyrazine in solution competing with alcohol-amine formation on Ru. By combining  $\text{Ru}/\text{Al}_2\text{O}_3$  and a silica-anchored N-hetero-cyclic carbene (NHC) catalyst, 2-amino-1,2-di(furan-2-yl)ethan-1-ol could be accessed with 42% overall yield in a single reactor.

## Author contributions

LG: experimental data acquisition, data curation, formal analysis, writing original draft; MDP & MC: DFT calculation, data curation, formal analysis, writing original draft; FJ: investigation, formal analysis, supervision; RR: formal analysis, visualization; MPT: conceptualization, funding acquisition, resources, supervision, validation, visualization, writing – review & editing.

## Conflicts of interest

There are no conflicts to declare.

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