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# Fluorinated vs. non-fluorinated tetrahedral Tri<sup>4</sup>Tri<sup>4</sup> porous organic cages for H<sub>2</sub>, CO<sub>2</sub>, and CH<sub>4</sub> adsorption†

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**We present the synthesis of two porous complementary tetrahedral Tri<sup>4</sup>Tri<sup>4</sup> imine cages, exhibiting Brunauer–Emmett–Teller (BET) surface areas of 591 m<sup>2</sup> g<sup>-1</sup> and 753 m<sup>2</sup> g<sup>-1</sup>, suitable for the adsorption of H<sub>2</sub>, CO<sub>2</sub>, and CH<sub>4</sub>. Comparisons in terms of crystallinity, thermal stability, porosity, and selectivity highlight the promising properties of fluorinated and non-fluorinated porous organic cages as functional materials.**

Harnessing the power of organic synthesis in combination with subcomponent self-assembly of small and rigid building blocks into larger assemblies under thermodynamic control gives facile access to novel materials by molecular design.<sup>1</sup> Besides metal-organic frameworks (MOFs) and covalent organic frameworks (COFs), porous organic cages (POCs) are an emerging class of porous materials that are self-assembled in solution before precipitation as solid materials.<sup>2</sup> These discrete, three-dimensional molecular assemblies differ from networks by enabling straightforward solution-phase processing and analysis while also allowing post-synthetic transformations that can modify the scaffolds with atomic precision.<sup>2,3</sup> Dynamic covalent chemistry, particularly imine bond condensation<sup>4</sup> and boronate ester formation,<sup>2a,b,e</sup> among others,<sup>2e</sup> can be employed to access POCs. In comparison to imine cages, the rigidity of boronate ester linkages is beneficial for the synthesis of large shape-persistent cages,<sup>2d-f</sup> as shown by Mastalerz and co-workers, who reported a giant boronate ester cage with cuboctahedral symmetry exhibiting an extraordinarily

high surface area of S<sub>BET</sub> = 3758 m<sup>2</sup> g<sup>-1</sup> already in 2014, comparable to those observed for extended networks like MOFs and COFs.<sup>5</sup> The group of Beuerle recently reported the first water-stable boronate ester cage,<sup>6</sup> stable under ambient conditions with a well-defined microporous solid state structure (S<sub>BET</sub> = 2534 m<sup>2</sup> g<sup>-1</sup>), paving the way for further applications of dynamic covalent boronate ester materials.<sup>7</sup> In addition, the use of computational crystal structure prediction,<sup>8</sup> along with computational design in supramolecular synthesis at both the molecular level and in the solid state,<sup>9</sup> has been key to obtaining a complex, shape-persistent [4[2+3]+6] cage by reversible nucleophilic aromatic substitution.<sup>10</sup> From the various accessible cage structures, the class of Tri<sup>4</sup>Tri<sup>4</sup> cages surprisingly remains largely underrepresented. Despite their tetrahedral structure enabling the formation of three-dimensional pores, only a few porous cages have been reported to date.<sup>9,11a-c,12</sup>

Herein, we present the synthesis of two highly porous Tri<sup>4</sup>Tri<sup>4</sup> imine cages, **Et<sup>4</sup>H<sup>4</sup>** and **Et<sup>4</sup>F<sup>4</sup>**. When reacting the pre-organised 1,3,5-tris(aminomethyl)-2,4,6-triethylbenzene (**Et**) with the non-fluorinated trialdehyde (**H**) and the analogous highly fluorinated trialdehyde (**F**), **Et<sup>4</sup>H<sup>4</sup>** and **Et<sup>4</sup>F<sup>4</sup>** form, respectively, opening up the possibility to investigate the influence of fluorinated units in porous organic materials (Fig. 1a). Heating the building blocks in a chloroform/methanol (3 : 1) mixture at 60 °C without stirring results in the growth of cube-like crystals on the walls of the reaction vessel. Repeated solvent exchange against *n*-pentane and drying of the crystals in air gives **Et<sup>4</sup>H<sup>4</sup>** in 84% and **Et<sup>4</sup>F<sup>4</sup>** in 45% yield as colourless crystals (Fig. S9–S14, ESI†). The <sup>1</sup>H NMR analysis of the redissolved crystals shows sharp signals, indicating the clean formation of both cages (Fig. 1b). Furthermore, <sup>19</sup>F NMR analysis of **Et<sup>4</sup>F<sup>4</sup>** reveals only one broad signal for the two independent aromatic fluorine atoms (Fig. S44, ESI†). Size determination using <sup>1</sup>H DOSY experiments gives solvodynamic radii of *r*<sub>solv</sub> = 1.04 nm (*D* = 3.98 × 10<sup>-10</sup> m<sup>2</sup> s<sup>-1</sup> in CDCl<sub>3</sub>) for **Et<sup>4</sup>H<sup>4</sup>** and *r*<sub>solv</sub> = 1.24 nm (*D* = 3.35 × 10<sup>-10</sup> m<sup>2</sup> s<sup>-1</sup> in CDCl<sub>3</sub>) for **Et<sup>4</sup>F<sup>4</sup>**, respectively (Fig. S1–S4, ESI†). Crystals suitable for single-crystal X-ray diffraction (SC-XRD) analysis can be obtained directly from the reaction mixture and reveal the cubic space groups *F*43c for **Et<sup>4</sup>H<sup>4</sup>**

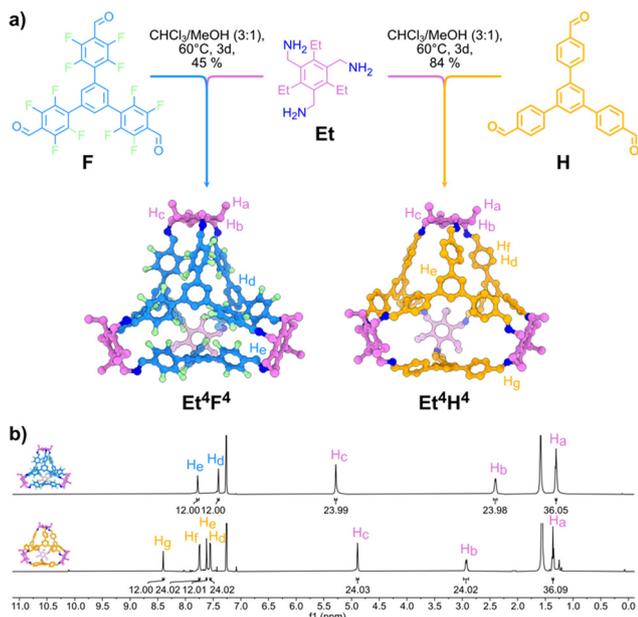
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† Electronic supplementary information (ESI) available: Experimental details, spectroscopic data, gas sorption data, crystallographic data. CCDC 2388131 and 2388132. For ESI and crystallographic data in CIF or other electronic format see DOI: <https://doi.org/10.1039/d4cc05277c>





**Fig. 1** (a) Synthesis of crystalline  $\text{Et}^4\text{F}^4$  and  $\text{Et}^4\text{H}^4$  by combining **H** and **F** with 1.20 eq. **Et**, respectively; (b)  $^1\text{H}$  NMR spectra of  $\text{Et}^4\text{F}^4$  and  $\text{Et}^4\text{H}^4$  recorded in  $\text{CDCl}_3$  at 25 °C.

and  $\text{Fd}_3$  for  $\text{Et}^4\text{F}^4$ .  $\text{Et}^4\text{F}^4$  assembles in a face-to-face arrangement with centroid-to-centroid distances of 4.5 Å for the fluorinated tetraphenyl panels packing loosely and C–H...F contacts between the inner fluorine and the hydrogen of the phenyl core of a neighbouring cage's panel with a distance of 3.1 Å, resulting in interconnected windows and a three-dimensional pore network (Fig. S6, ESI<sup>†</sup>). Additional vertex-to-vertex arrangements of **Et** from four separate cages lead to isolated extrinsic pores that are inaccessible. In contrast,  $\text{Et}^4\text{H}^4$  packs in a close window-to-window arrangement but also exhibits an extensively connected three-dimensional pore network. Powder X-ray diffraction (PXRD) analysis of dried cage crystals shows sharp diffraction for  $\text{Et}^4\text{F}^4$ , revealing a partly crystalline material before and after all gas sorption experiments (Fig. 2a). Whereas the PXRD analysis of  $\text{Et}^4\text{H}^4$  shows broad diffraction, indicating the formation of a largely amorphous material upon activation (Fig. 2a). Additional thermogravimetric analysis shows a high thermal stability for both materials, with decomposition temperatures of 348 °C for  $\text{Et}^4\text{F}^4$  and 352 °C for  $\text{Et}^4\text{H}^4$ , respectively (Fig. S21 and S22, ESI<sup>†</sup>).  $\text{Et}^4\text{F}^4$ 's seemingly more robust networked cages and high thermal stability are most likely the result of several stabilising weak interactions between the fluorinated and (non-)fluorinated parts of the cages in the highly symmetric lattice.<sup>13</sup> Jiang *et al.* outlined the improved crystallinity of fluorine-containing systems due to self-complementary electronic interactions between fluorinated and non-fluorinated counterparts.<sup>14,15</sup> The pore sizes of  $\text{Et}^4\text{H}^4$  range from 5.6 Å to 11.7 Å, derived from the SC-XRD data. Analogues are the diameters 3.4 Å and 6.4 Å for  $\text{Et}^4\text{F}^4$ , respectively. Non-local density functional theory (NLDFT) and grand canonical Monte Carlo (GCMC) calculations based on the  $\text{N}_2$  sorption isotherms at 77 K also show the smaller pore size of  $\text{Et}^4\text{F}^4$  with a narrow pore size distribution around 5.8 Å (Fig. S29,

ESI<sup>†</sup>). Contrarily, the pore size distribution of  $\text{Et}^4\text{H}^4$  shows a broader maximum for micropores around 14 Å and some mesopores with pore diameters between 20 Å and 80 Å, which are larger than the cage compounds themselves (Fig. S26, ESI<sup>†</sup>), indicating cracks and a subsequent loss of crystallinity. This suggests that the solvent exchange and subsequent drying of the crystals obtained from the reaction mixture, in contrast to  $\text{Et}^4\text{F}^4$ , leads to a loss of crystallinity for  $\text{Et}^4\text{H}^4$ . The observed porosity of  $\text{Et}^4\text{H}^4$ , however, is suggested to be caused by the cage's large voids in the amorphous material. The pore widths of both cages and the kinetic diameters of  $\text{H}_2$  (2.89 Å),  $\text{CO}_2$  (3.30 Å), and  $\text{CH}_4$  (3.80 Å) indicate that both should be suitable for the adsorption of these gases.<sup>16</sup> Therefore, the dried crystals were activated by heating under dynamic vacuum overnight, at 80 °C for  $\text{Et}^4\text{F}^4$  and at 140 °C for  $\text{Et}^4\text{H}^4$ . Between the measurements, both samples were recycled by heating to 80 °C for two hours *in vacuo*. The obtained specific surface areas (SA) of 591  $\text{m}^2 \text{g}^{-1}$  and 753  $\text{m}^2 \text{g}^{-1}$  for  $\text{Et}^4\text{F}^4$  and  $\text{Et}^4\text{H}^4$ , respectively, determined by the BET method, are comparable to the  $\text{Tri}^4\text{Di}^6$  cage **CC3** ( $S_{\text{BET}} = 624 \text{ m}^2 \text{g}^{-1}$ ) and a  $\text{Tri}^2\text{Di}^3$  *exo*-functionalised salicylimine cage ( $S_{\text{BET}} = 744 \text{ m}^2 \text{g}^{-1}$ ) of similar sizes.<sup>17,18</sup> To the best of our knowledge,  $\text{Et}^4\text{F}^4$  and  $\text{Et}^4\text{H}^4$  exhibit among the largest specific surface areas reported for tetrahedral  $\text{Tri}^4\text{Tri}^4$  cages.  $\text{Et}^4\text{F}^4$  is additionally the largest fluorinated  $\text{Tri}^4\text{Tri}^4$  imine cage, surpassing cage **FC1** ( $S_{\text{BET}} = 536 \text{ m}^2 \text{g}^{-1}$ ) previously published by our group.<sup>12</sup> The pore volume of both cages was determined from the  $\text{N}_2$  sorption isotherms at 77 K by GCMC as well as NLDFT calculations, revealing a total pore volume of 0.39  $\text{cm}^3 \text{g}^{-1}$  and a micropore volume of 0.21  $\text{cm}^3 \text{g}^{-1}$  for  $\text{Et}^4\text{F}^4$  and 0.59  $\text{cm}^3 \text{g}^{-1}$  and 0.24  $\text{cm}^3 \text{g}^{-1}$  for  $\text{Et}^4\text{H}^4$ , respectively. The  $\text{Et}^4\text{H}^4$  cage adsorbs 14.5  $\text{mmol g}^{-1}$  (28.9 wt%) of  $\text{N}_2$  at 77 K and 0.95 $p/p_0$  (Fig. 2c), as beyond this relative pressure,  $\text{N}_2$  condensation inside the pore network can be observed, which is often not considered. This is comparable to the adsorption performance of the substituted  $\text{Tri}^4\text{Di}^6$  cages reported by Mastalerz *et al.*, which also remain porous in their amorphous state while exhibiting specific surface areas ranging from 690 to 727  $\text{m}^2 \text{g}^{-1}$ , with  $\text{N}_2$  uptake values between 17.4 and 21.4  $\text{mmol g}^{-1}$  at 77 K and 0.95 $p/p_0$  bar.<sup>19</sup> The  $\text{N}_2$  sorption isotherm of  $\text{Et}^4\text{H}^4$  can be classified as a combination of type-Ib (low  $p/p_0$  for the microporous region) and a type-II isotherm (higher  $p/p_0$ , macroporous multi-layer region) with a wide H4 hysteresis loop.<sup>20</sup>  $\text{Et}^4\text{F}^4$  exhibits a higher gas uptake of 10.1  $\text{mmol g}^{-1}$  (22.0 wt%)  $\text{N}_2$  at 77 K and 0.95 $p/p_0$  (Fig. 2c), compared to the slightly larger **CC3** (8.2  $\text{mmol g}^{-1}$ , 18.6 wt%, 1 bar).<sup>17</sup> The  $\text{N}_2$  adsorption isotherm can again be described as a combination of a type-I and type-II isotherm with a H4 hysteresis loop. Noteworthy is the step in the H4 hysteresis loop at 0.5 $p/p_0$ , more clearly seen in  $\text{Et}^4\text{F}^4$  than in  $\text{Et}^4\text{H}^4$ , which we assign to two types of bottle-neck pores in combination with framework reconstruction.<sup>20</sup> Exhibiting a hydrogen uptake of 6.1  $\text{mmol g}^{-1}$  (1.2 wt%),  $\text{Et}^4\text{H}^4$  adsorbs more  $\text{H}_2$  at 77 K and 1 bar than the almost twice as large  $\text{Tri}^4\text{Di}^6$  *tert*-butyl substituted adamantoid cage ( $S_{\text{BET}} = 1377 \text{ m}^2 \text{g}^{-1}$ , 5.6  $\text{mmol g}^{-1}$ ) and is also comparable to the smaller sized **CC2** ( $S_{\text{BET}} = 533 \text{ m}^2 \text{g}^{-1}$ , 5.9  $\text{mmol g}^{-1}$ ) and **CC3** ( $S_{\text{BET}} = 624 \text{ m}^2 \text{g}^{-1}$ , 5.0  $\text{mmol g}^{-1}$ ) POCs reported.<sup>17,21</sup> We further measured an adsorption of 3.0  $\text{mmol g}^{-1}$  (11.8 wt%) for



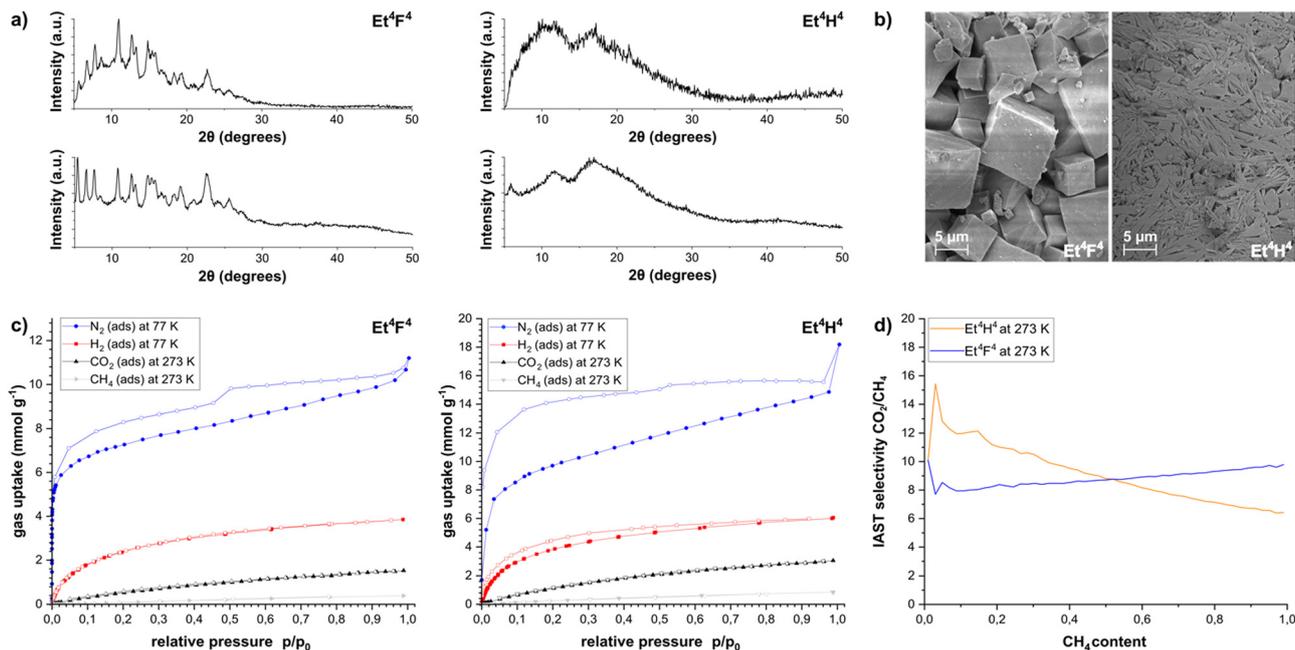


Fig. 2 (a) Powder X-ray diffraction (PXRD) patterns before (bottom) and after (top) sorption experiments of  $\text{Et}^4\text{F}^4$  (left) and  $\text{Et}^4\text{H}^4$  (right); (b) true to scale cutouts from scanning electron microscope (SEM) images of  $\text{Et}^4\text{F}^4$  (left) and  $\text{Et}^4\text{H}^4$  (right), scanning voltage 5 kV; (c) gas adsorption (filled) and desorption (hollow) overview of  $\text{Et}^4\text{F}^4$  (left) and  $\text{Et}^4\text{H}^4$  (right); (d) ideal adsorbed solution theory (IAST) selectivity curves of  $\text{Et}^4\text{F}^4$  (orange) and  $\text{Et}^4\text{H}^4$  (blue) for varying gas compositions of  $\text{CO}_2/\text{CH}_4$  (1 bar total pressure, 273 K).

$\text{CO}_2$  at 273 K and 1 bar. This value is again well comparable with the cages mentioned above showing  $\text{CO}_2$  uptakes of  $2.7 \text{ mmol g}^{-1}$  (11.8 wt%),  $3.0 \text{ mmol g}^{-1}$  (11.7 wt%), and  $2.5 \text{ mmol g}^{-1}$  (9.9 wt%), respectively.<sup>17,22</sup> For  $\text{CH}_4$ , we measured a low gas uptake at 273 K and 1 bar of  $0.8 \text{ mmol g}^{-1}$  (1.3 wt%) compared to **CC2** ( $1.1 \text{ mmol g}^{-1}$ , 1.7 wt%) and **CC3** ( $1.5 \text{ mmol g}^{-1}$ , 2.3 wt%), resulting in a higher selectivity of 10.3:1 (w/w) for  $\text{CO}_2$  over  $\text{CH}_4$ , which is well comparable to the selectivity of 10:1 (w/w) for the adamantoid cage by Mastalerz *et al.*<sup>17,21</sup> The measured gas adsorptions of the highly fluorinated  $\text{Et}^4\text{F}^4$  are much lower than for the non-fluorinated  $\text{Et}^4\text{H}^4$ .  $\text{Et}^4\text{F}^4$  adsorbs at 1 bar  $3.9 \text{ mmol g}^{-1}$  (0.8 wt%)  $\text{H}_2$  (77 K),  $1.5 \text{ mmol g}^{-1}$  (6.3 wt%)  $\text{CO}_2$  (273 K), and  $0.4 \text{ mmol g}^{-1}$  (0.6 wt%)  $\text{CH}_4$  (273 K). The smaller, previously reported cage **FC1** exhibits higher adsorption properties for  $\text{H}_2$  ( $7.5 \text{ mmol g}^{-1}$  and 1.5 wt%) and  $\text{CO}_2$  ( $4.2 \text{ mmol g}^{-1}$  and 19.0 wt%) than both here reported cages.<sup>12</sup> To date, **FC1** is the cage with the highest  $\text{CO}_2$  uptake ever reported for POCs.<sup>10</sup> When calculating the gas uptake for a porous material in moles of gas per gramme material, the molecular weight and density of the material are not taken into account. This entails that smaller cages, such as **FC1** ( $1309 \text{ g mol}^{-1}$ ), frequently display higher gas uptakes since there are essentially more cage molecules with specific surface area per gramme of material available. To evaluate the quantitative uptake, we also calculated the gas uptake in moles of gas per mole of cage and volume of adsorbed gas per volume of the cage (Tables S3–S5, ESI<sup>†</sup>). For  $\text{CO}_2$ , we calculated gas uptakes of  $5.5 \text{ mol mol}^{-1}$  for **FC1** and  $4.9 \text{ mol mol}^{-1}$  together with  $7.1 \text{ mol mol}^{-1}$  for  $\text{Et}^4\text{F}^4$  and  $\text{Et}^4\text{H}^4$ , respectively. In this regard,  $\text{Et}^4\text{H}^4$  is the superior adsorbent material in direct comparison to **FC1**. With increasing pore sizes, the number of adsorbed gas molecules that directly interact with

the surface area becomes less, and therefore higher relative pressure is needed for the pore filling through multilayer adsorption by adsorbate–adsorbate interactions to achieve a higher gas uptake. However, besides adsorption capacity, selectivity is arguably another critical property of a porous material for industrial applications such as gas purification.<sup>23</sup> Natural gas, primarily composed of  $\text{CH}_4$ , is a crucial energy source that is often contaminated with over 40%  $\text{N}_2$  and  $\text{CO}_2$ , which must be removed before combustion.<sup>24</sup> Therefore, we calculated the ideal adsorbed solution theory (IAST) selectivity for  $\text{CO}_2$  over  $\text{CH}_4$ , based on the sorption isotherms at 273 K and 1 bar (Fig. 2d). For a 1:1  $\text{CO}_2:\text{CH}_4$  composition, both cages exhibit nearly the same selectivity (8.80 and 8.71 for  $\text{Et}^4\text{H}^4$  and  $\text{Et}^4\text{F}^4$ , respectively). With decreasing  $\text{CO}_2$  content, the selectivity of the non-fluorinated cage decreases to 6.6 at 95%  $\text{CH}_4$  in the gas composition, whereas the selectivity of the fluorinated cage increases to 9.7 for the identical composition (Fig. 2d). In addition to the recent studies of our group, Miljanić *et al.* reported the higher selectivity of fluorinated covalent triazine frameworks to  $\text{CO}_2$  in a  $\text{CH}_4$ -enriched composition and the higher  $\text{CO}_2$ -philicity of fluorine-containing materials, resulting from attractive quadrupole interactions.<sup>12,13b</sup> The better selectivity of  $\text{Et}^4\text{F}^4$ , especially in  $\text{CH}_4$ -enriched compositions ( $\geq 60\%$ ), shows the potential for the application of fluorinated materials in the purification of gases.

In conclusion, we presented the successful synthesis and characterisation of two new porous  $\text{Tri}^4\text{Tri}^4$  imine cages,  $\text{Et}^4\text{H}^4$  and the highly fluorinated  $\text{Et}^4\text{F}^4$ . To the best of our knowledge, both cages are among the largest shape-persistent cages within this topology.<sup>11a–c,12</sup> We further investigated the influence of the incorporation of highly fluorinated building blocks into



porous materials in terms of retention of crystallinity, thermal stability, porosity, selectivity, and reusability. The fluorinated  $\text{Et}^4\text{F}^4$  shows a much higher retention of the crystallinity, whereas  $\text{Et}^4\text{H}^4$  was obtained as an amorphous material upon solvent removal. Both materials exhibit high thermal stability of approximately 350 °C and gas adsorption measurements further demonstrated that both cages are highly porous with BET surface areas of 591 m<sup>2</sup> g<sup>-1</sup> ( $\text{Et}^4\text{F}^4$ ) and 753 m<sup>2</sup> g<sup>-1</sup> ( $\text{Et}^4\text{H}^4$ ), which are accessible for the uptake of H<sub>2</sub> and CO<sub>2</sub>, simultaneously showing a low affinity towards CH<sub>4</sub>. At 273 K and 1 bar, both cages nearly exhibit the same IAST selectivity for CO<sub>2</sub> over CH<sub>4</sub> for a 1 : 1 composition of the gases of 8.8 and 8.7 for  $\text{Et}^4\text{H}^4$  and  $\text{Et}^4\text{F}^4$ , respectively. For compositions with decreasing amounts of CO<sub>2</sub>, the selectivity for CO<sub>2</sub> of the non-fluorinated cage decreases, whereas the selectivity of the fluorinated cage increases, demonstrating the advantages of fluorine-containing building blocks in materials for gas purification. Unveiling significant relationships between the structural and electronic differences of fluorinated and non-fluorinated building blocks, offering new ways to tailor highly selective porous organic architectures for advanced functional materials.

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## Data availability

The data supporting this article have been included as part of the ESI.† Crystallographic data for has been deposited at the CCDC under 2388131 ( $\text{Et}^4\text{F}^4$ ) and 2388132 ( $\text{Et}^4\text{H}^4$ ) and can be obtained from <https://www.ccdc.cam.ac.uk/structures/>.

## Conflicts of interest

There are no conflicts to declare.

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