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# The effect of air on oxidation decomposition of uranium-containing cationic exchange resins in $\text{Li}_2\text{CO}_3\text{--Na}_2\text{CO}_3\text{--K}_2\text{CO}_3$ molten-salt system

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With the development of nuclear energy, spent cationic exchange resins after purification of radioactive wastewater must be treated. Molten-salt oxidation (MSO) can minimize the disposal content of resins and capture  $\text{SO}_2$ . In this work, the decomposition of uranium-containing resins in carbonate molten salt in  $\text{N}_2$  and air atmospheres was investigated. Compared to  $\text{N}_2$  atmosphere, the content of  $\text{SO}_2$  released from the decomposition of resins was relatively low at 386–454 °C in an air atmosphere. The SEM morphology indicated that the presence of air facilitated the decomposition of the resin cross-linked structure. The decomposition efficiency of resins in an air atmosphere was 82.6% at 800 °C. The XRD analysis revealed that uranium compounds had the reaction paths of  $\text{UO}_3 \rightarrow \text{UO}_{2.92} \rightarrow \text{U}_3\text{O}_8$  and  $\text{UO}_3 \rightarrow \text{K}_2\text{U}_2\text{O}_7 \rightarrow \text{K}_2\text{UO}_4$  in the carbonate melt, and sulfur elements in resins were fixed in the form of  $\text{K}_3\text{Na}(\text{SO}_4)_2$ . The XPS result illustrated that peroxide and superoxide ions accelerated the conversion of sulfone sulfur to thiophene sulfur and further oxidized to  $\text{CO}_2$  and  $\text{SO}_2$ . Besides, the ion bond formed by uranyl ions on the sulfonic acid group was decomposed at high temperature. Finally, the decomposition of uranium-containing resins in the carbonate melt in an air atmosphere was explained. This study provided more theoretical guidance and technical support for the industrial treatment of uranium-containing resins.

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## 1. Introduction

Currently, ion exchange resins (IERS) are widely applied for the separation and purification of radioactive wastewater. When their capacity reaches saturation, waste resins are replaced by fresh resins. A large number of waste resins are produced in nuclear energy units.<sup>1</sup> For example, the actual annual output of waste resins of two units of the Daya Bay nuclear power plant was 4–13  $\text{m}^3$  per year, and the average annual output of waste resins of the two units of the Qinshan No. 2 nuclear power plant from 2002 to 2016 reached 46  $\text{m}^3$  per year.<sup>2</sup>

After replacement, spent resins undergo chemical degradation and radiation decomposition, which can release hazardous substances into the environment. To reduce the risks of waste resins to the environment and humans, proper disposal of waste resins is required. The general treatment methods include curing method, incineration method, *etc.*<sup>3</sup> Traditional curing methods are cement curing, asphalt curing and polymer curing.<sup>4–8</sup> These are some advantages about these ways, such as a simple process, mature technology, low investment and

operating costs, and stable properties of the obtained cured products. However, the volume reduction ratio after the curing of waste resins is low, and the degradation or swelling of waste resins is unfavorable for the long-term storage of cured products.<sup>9</sup> The advantages of treating waste resins by incineration mainly contain a high weight loss rate and a volume reduction rate. The heat generated during the treatment process can be recovered. However, the treatment of waste resins with this technology makes radionuclides volatilize and releases large amounts of sulfur oxides, thereby polluting the environment.<sup>10–12</sup> Therefore, it is critical to propose a safe and efficient method for the disposal of waste resins.

Molten-salt oxidation (MSO) is an efficient, flame-free thermal process that captures  $\text{SO}_2$  and minimizes the disposal content of wastes through oxidation destruction.<sup>13–16</sup> Most importantly, this technology can be applied for the retention of radionuclides in molten salt. Our group investigated the destruction process of resins using the ternary eutectic carbonate ( $\text{Li}_2\text{CO}_3\text{--Na}_2\text{CO}_3\text{--K}_2\text{CO}_3$ ), and demonstrated that this molten salt system was an effective medium to process resins at low temperatures, thereby reducing the volatilization of radionuclides.<sup>17</sup> Antonetti *et al.*<sup>18</sup> conducted pyrolysis experiments on cation exchange resins (CERs) doped with cobalt and cesium and demonstrated that the presence of Co and Cs on the resin inhibited the transfer of sulfur to the gas phase while accelerating the degradation of volatile carbon compounds. Yang

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*et al.*<sup>19</sup> investigated the volatilization of Cd, Co, Ce, Cs, Pb, and Sr doped with different contents of resins in binary eutectic carbonate ( $K_2CO_3$ – $Na_2CO_3$ ) at 710 °C. The results showed that the retention rate of each metal reached 99.5 wt%. In addition, some experiments also explored certain metal impurities (such as unionized and ionized forms) can play a catalytic role in the oxidative cracking of resins.<sup>20–22</sup> Juang *et al.*<sup>23</sup> found that several metal salts containing  $CuO$ ,  $CuSO_4 \cdot 5H_2O$  and  $FeSO_4 \cdot 7H_2O$  had a catalytic effect on the oxidative destruction of cationic resins. This was because the decomposition of functional groups and polymer matrices was enhanced by these salts. Matsuda *et al.*<sup>21</sup> studied the effect of Fe impurities including unionized Fe ( $Fe$ ,  $Fe_2O_3$ ,  $Fe_3O_4$ ) forms and ionized Fe ( $Fe^{3+}$ ) forms on resin oxidation. Ionized Fe ( $Fe^{3+}$ ) forms resulted in considerable increases in reaction rate constant, which indicated that  $Fe^{3+}$  functioned as a catalyst. However, unionized Fe ( $Fe$ ,  $Fe_2O_3$ ,  $Fe_3O_4$ ) had no catalytic effect. In addition, the catalytic effect of other metal impurities (such as  $Pd^{2+}$ ,  $Cu^{2+}$ ,  $Fe^{2+}$ ,  $Al^{3+}$ ,  $Co^{2+}$  and  $Ni^{2+}$ ) on the resin oxidation reaction was also investigated using resins. The experimental analysis revealed that in the case of resins containing  $Pd^{2+}$ ,  $Cu^{2+}$ ,  $Fe^{2+}$  and  $Al^{3+}$ , resins were catalysed and oxidized, and metallic sulfides in molten salt could be rapidly transferred to oxides. Sulfur compound formation was attributed to the functional sulfonic acid group ( $-SO_3H$ ) in the cation exchange resin.<sup>20</sup> When metal compounds were present in sulfur-containing waste, sulfur, as a main environmental pollution source, was fixed in the form of metal sulfides and metal sulfates in the condensed phase during waste treatment, which decreased the output in sulfur compounds (such as  $H_2S$  and  $SO_2$ ).<sup>24–28</sup>

Uranium element is a main radioactive nuclide in nuclear industry wastewater. Based on analysis of the above literature, resins after the purification of uranium-containing wastewater can be also disposed by MSO method and the content of spent resins can be reduced. However, the presence of uranium element could have a certain impact on the decomposition of resins in molten salt. Therefore, it is of great significance to study the oxidation decomposition of uranium-containing cationic exchange resins (CERs). In this study, due to its low melting point, the ternary carbonate ( $Li_2CO_3$ – $Na_2CO_3$ – $K_2CO_3$ ) is chosen as molten salt for the oxidation decomposition of resins. Some experiments on the decomposition of uranium-containing resins and pure resins were conducted under air atmosphere. The characteristics of products after the decomposition of uranium-containing resins and pure resins were analysed, such as the release change of off gas, component of spent salt and structure variation of residues. The experiments focused on investigating the oxidation decomposition of uranium-containing resins in ternary carbonate ( $Li_2CO_3$ – $Na_2CO_3$ – $K_2CO_3$ ) molten-salt system.

## 2. Materials and methods

### 2.1 Materials

Cationic exchange resins (CERs) used in our experiment were insoluble solid granules and had a strong acid form ( $-SO_3-H^+$ ) based on the structure of a styrene-divinylbenzene (ST-DVB)

matrix. Because fresh resins contain impurity ions, hydrochloric acid solution and sodium hydroxide solution were utilized to remove impurities in resins before the experiment. The resins after cleaning were dried to a constant weight in an oven at 105 °C. Through elemental analysis, the contents of C, O, S and H in resins were 38.6 wt%, 43.6 wt%, 12.2 wt% and 5.6 wt%, respectively. In the preparation process of uranium-containing resins, when resins were in contact with the solution containing a certain concentration of uranium element, uranyl ions in solution were adsorbed onto the resin using an ion exchange method. This uranium concentration approximately corresponded to that of spent resin generated from spent fuel reprocessing plant. In the experiment, uranium-containing resins and pure resins after drying were used as raw materials. The molten salt system contained 44 wt%  $Li_2CO_3$ , 30 wt%  $Na_2CO_3$  and 26 wt%  $K_2CO_3$ .

### 2.2 Experimental operation process

Uranium-containing resins was decomposed in molten salt under nitrogen and air atmospheres in a tube furnace. First, carbonates ( $Li_2CO_3$ ,  $Na_2CO_3$  and  $K_2CO_3$ ) were dried to remove moisture in an oven at 200 °C, and  $Li_2CO_3$ ,  $Na_2CO_3$  and  $K_2CO_3$  were evenly mixed by 44 wt%, 30 wt% and 26 wt%, respectively. Second, 2 g of carbonates and 2 g of resins were weighed, respectively. 60 wt% of ternary eutectic carbonates was uniformly mixed with resins and the rest was covered on resins, which could absorb acid gas released from resin decomposition. This mixture was packed in the alundum crucible. The crucible was kept at a certain temperature for 30 min in a furnace and subsequently taken out. The products after resin decomposition were treated to collect waste salt and residues. Residues were washed with deionized water and then be dried to a constant weight in an oven at 105 °C. Waste salt was ground into a powder for further analysis. All experiments were repeated three times. The retention rate of sulfur in spent salt was analysed through the dichromic acid method. The degradation and removal efficiency (DRE) of resins and retention rate of sulfur (SRR) after the decomposition of resins were calculated by formulas (1) and (2).

$$DRE(\%) = \frac{M_{\text{before}} - M_{\text{after}}}{M_{\text{before}}} \times 100\% \quad (1)$$

where  $M_{\text{before}}$  – the mass of resins before decomposition; and  $M_{\text{after}}$  – the mass of resins after decomposition.

$$SRR(\%) = \frac{S_{\text{salt}}}{S_{\text{CERs}}} \times 100\% \quad (2)$$

where  $S_{\text{CERs}}$  – the amount of sulfur in resins before decomposition; and  $S_{\text{salt}}$  – the amount of sulfur in spent salt after decomposition.

### 2.3 Analytical methods

The thermogravimetric analyzer (TGA) was utilized to explore the destruction laws of uranium-containing resins. The temperature was increased from room temperature to 800 °C at 10 °C  $\text{min}^{-1}$  in  $N_2$  or air flow rate of 20 mL  $\text{min}^{-1}$ . On-line gas



mass spectrometer (GM) was applied for the analysis of composition and release variation of gaseous products in the decomposition process of resins. The microscopic morphology of residue after resins destruction was observed by the scanning electron microscope (SEM). Energy dispersive spectrometry (EDS) was conducted to analyse the element composition of residues. The pictures of samples were taken at a magnification of  $\times 50$  and an excitation voltage of 5 kV. The chemical composition of spent salt was analyzed through X-ray diffraction (XRD). The scan degree range ( $2\theta$ ) of sample was from  $5^\circ$  to  $85^\circ$ . The Fourier transform infrared spectrometer (FT-IR) was used to determine the change of functional groups in residues. 2 mg of the sample was mixed with 40 mg of KBr and then pressed into round thin sheets. The thin sheets were measured in the  $400\text{--}4000\text{ cm}^{-1}$  range. The binding energies of sulfur 2p in residues were determined by X-ray photoelectron spectroscopy (XPS). Al K $\alpha$  radiation ( $h\nu = 1486.6\text{ eV}$ ) from a monochromatic X-ray source and a  $500\text{ }\mu\text{m}$  light spot size was utilized. Additionally, according to the experimental results, HSC Chemistry 6.0 thermodynamic software is used to analyse the relevant reactions, and study the Gibbs free energy of reaction between substances, which can verify the accuracy of the experimental results. In the calculation process of reaction Gibbs free energy, the analysis module of reaction equation in the software is mainly used. Before the calculation of Gibbs free energy, the reaction temperature range is set as  $0\text{--}1000^\circ\text{C}$ , and the temperature step is  $100^\circ\text{C}$ . The reaction equation between substances is balanced. Then, the Gibbs free energy of reaction is directly calculated through HSC Chemistry 6.0 thermodynamic software. Eventually, the relationship between Gibbs free energy of reaction and temperature can be obtained.

### 3. Results and discussion

#### 3.1 Thermal destruction of uranium-containing resins

Fig. 1 describes the thermal destruction of uranium-containing resins in the temperature range of  $30\text{--}800^\circ\text{C}$  in  $\text{N}_2$  and air atmospheres. According to the obtained thermogravimetric curve, the derivative thermogravimetric (DTG) curve was fitted and the main temperature destruction range was determined. It was determined that with increasing reaction temperature, the mass remaining efficiencies of uranium-containing resins progressively decreased, irrespective of the environment. Besides, there were three main variation stages in the thermal decomposition process of resins in  $\text{N}_2$  atmosphere, such as  $30\text{--}214^\circ\text{C}$ ,  $214\text{--}375^\circ\text{C}$  and  $375\text{--}800^\circ\text{C}$ , and in air atmosphere, such as  $30\text{--}228^\circ\text{C}$ ,  $228\text{--}436^\circ\text{C}$  and  $436\text{--}800^\circ\text{C}$ , *i.e.*, the decomposition process of resins was different at every stage in  $\text{N}_2$  and air atmospheres.

From Fig. 1, in  $\text{N}_2$  atmosphere, the mass remaining efficiencies of uranium-containing resins gradually decreased with reaction temperature increasing from  $30^\circ\text{C}$  to  $214^\circ\text{C}$  and the weight loss of resins was 18.7% in this temperature range, which was due to the evaporation of water in resins. The maximum weight loss of resins (26.1%) occurs in  $214\text{--}375^\circ\text{C}$ . This change of resin mass corresponded to the destruction of functional groups of sulfonic acid groups ( $-\text{SO}_3\text{H}$ ) in resins.

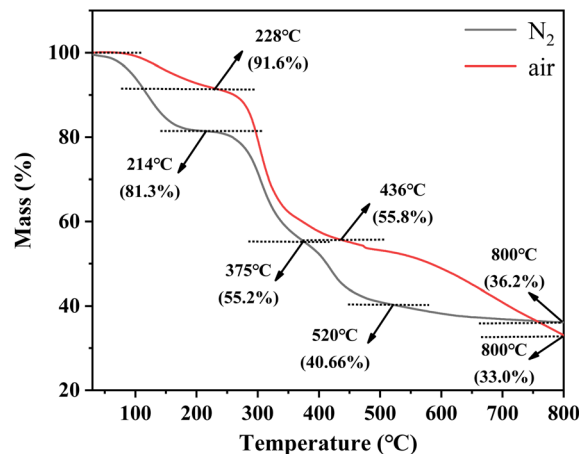


Fig. 1 The thermal characteristics of uranium-containing resins in the temperature range of  $30\text{--}800^\circ\text{C}$  in  $\text{N}_2$  and air atmospheres.

When reaction temperature was increased to  $800^\circ\text{C}$ , the mass remaining efficiencies of uranium-containing resins was decreased to 36.2%, and the weight loss of resins was 15.7%. The result was mainly ascribed to the decomposition of ST-DVB matrix and polymer chains. These results were similar to the conclusion in ref. 23. In addition, compared to  $\text{N}_2$  atmosphere, the mass remaining efficiencies of resins had an obvious decrease in air atmosphere above  $436^\circ\text{C}$ , and reached 33.0% at  $800^\circ\text{C}$ . It meant that the addition of air accelerated and prompted the decomposition of ST-DVB matrix and polymer chains in resins at the third stage.

To study the decomposition of uranium-containing resins in molten salt, some experiments were designed to analyse the content variation of exhaust gas during the decomposition of uranium-containing resins in  $\text{N}_2$  and air atmospheres with increasing temperature, and the results are shown in Fig. 2. From Fig. 2a and b, the release temperatures of  $\text{CH}_4$  and  $\text{C}_2\text{H}_4$  during the decomposition of uranium-containing resins in  $\text{N}_2$  atmosphere were basically the same with those in air atmosphere, and were  $423^\circ\text{C}$  and  $386^\circ\text{C}$ , respectively. However, compared to  $\text{N}_2$  atmosphere, the production of  $\text{CH}_4$  at  $527\text{--}755^\circ\text{C}$  and  $\text{C}_2\text{H}_4$  at  $386\text{--}452^\circ\text{C}$  in air atmosphere obviously decreased. Based on the TG analysis in Fig. 1, the generation of  $\text{CH}_4$  and  $\text{C}_2\text{H}_4$  was due to the cleavage of hydrogen bonds (ST-DVB matrix and polymer chains) during the decomposition of resins in air atmosphere, and the hydrogen bonds in resins were immediately oxidized, resulting in the decrease in  $\text{C}_2\text{H}_4$  release content and the increase in  $\text{CO}_2$  release content (Fig. 2b and c). Besides, the release content of  $\text{CO}_2$  above  $368^\circ\text{C}$  in air atmosphere was significantly more than that in  $\text{N}_2$  atmosphere. Additionally, the release change of  $\text{SO}_2$  during resin decomposition in carbonates in  $\text{N}_2$  and air atmospheres was studied (Fig. 2d). The temperature range of  $\text{SO}_2$  release was  $386\text{--}454^\circ\text{C}$  in  $\text{N}_2$  and air atmospheres. According to the TG analysis in Fig. 1, the production of  $\text{SO}_2$  in air atmosphere corresponded to the decomposition of sulfonic acid groups at  $186\text{--}436^\circ\text{C}$ . The addition of carbonates absorbed the heat around resins and decreased the temperature around resins, which hindered the

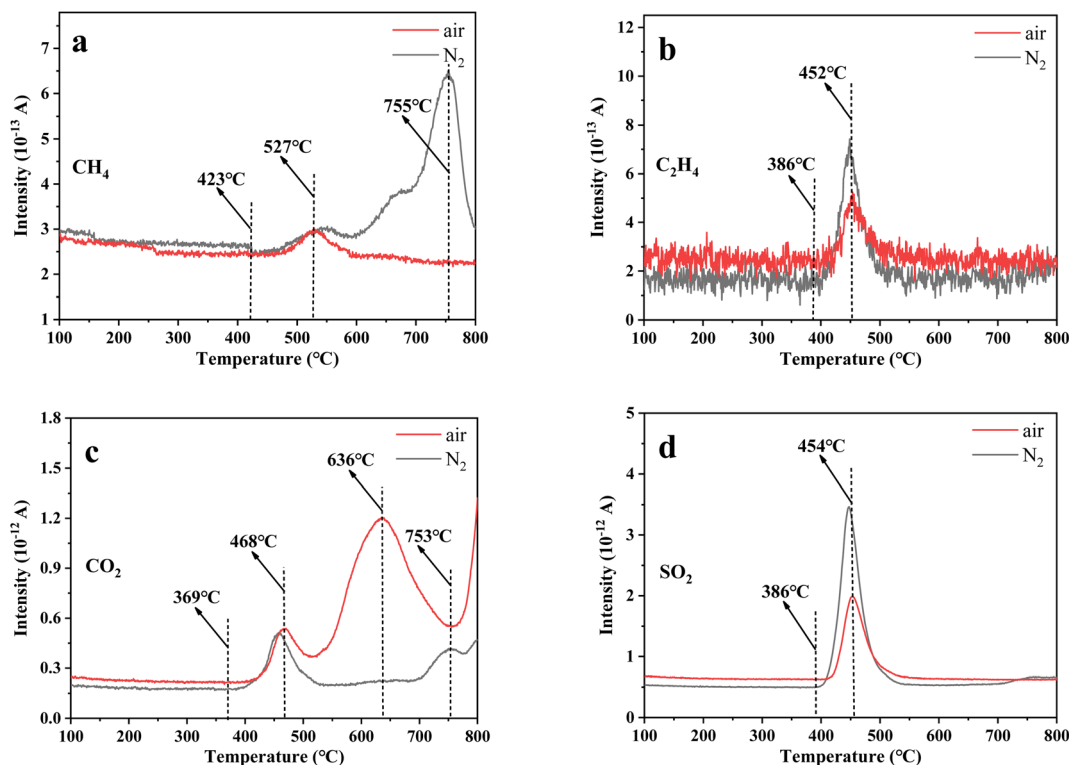


Fig. 2 The release variation of off gas (a)  $\text{CH}_4$ , (b)  $\text{C}_2\text{H}_4$ , (c)  $\text{CO}_2$  and (d)  $\text{SO}_2$  during the decomposition of uranium-containing resins in carbonates with increasing temperature in  $\text{N}_2$  and air atmospheres.

decomposition of sulfonic acid groups. It meant that the decomposition temperature of sulfonic acid groups was increased. Besides, compared to  $\text{N}_2$  atmosphere, the release content of  $\text{SO}_2$  in air atmosphere was comparatively low. It was concluded that more  $\text{SO}_2$  was absorbed by carbonates in air atmosphere.

To further explore the content change of  $\text{SO}_2$  during uranium-containing resin decomposition in carbonates, the HSC Chemistry 6.0 thermodynamic software was applied for the analysis of the thermal characteristics of reaction between  $\text{SO}_2$  and carbonates in  $\text{N}_2$  and air atmospheres. Fig. 3a describes the relationship between reaction temperature and Gibbs free

energy ( $\Delta G$ ) required for the reaction of  $\text{SO}_2$  and carbonates ( $\text{Li}_2\text{CO}_3$ ,  $\text{Na}_2\text{CO}_3$  and  $\text{K}_2\text{CO}_3$ ) in  $\text{N}_2$  atmosphere. From Fig. 3a, it was seen that the Gibbs free energy required for the reaction of  $\text{SO}_2$  and carbonates gradually decreased with increasing reaction temperature and remained negative. The reaction between  $\text{SO}_2$  and carbonates was spontaneous to proceed. Compared to  $\text{N}_2$  atmosphere, the Gibbs free energy required for the reaction of  $\text{SO}_2$  and carbonates was relatively smaller in air atmosphere (Fig. 3b). It was determined that  $\text{SO}_2$  was easily absorbed by carbonates with the addition of air, which proved the decrease in  $\text{SO}_2$  release content at 386–454 °C in air atmosphere (Fig. 2d).

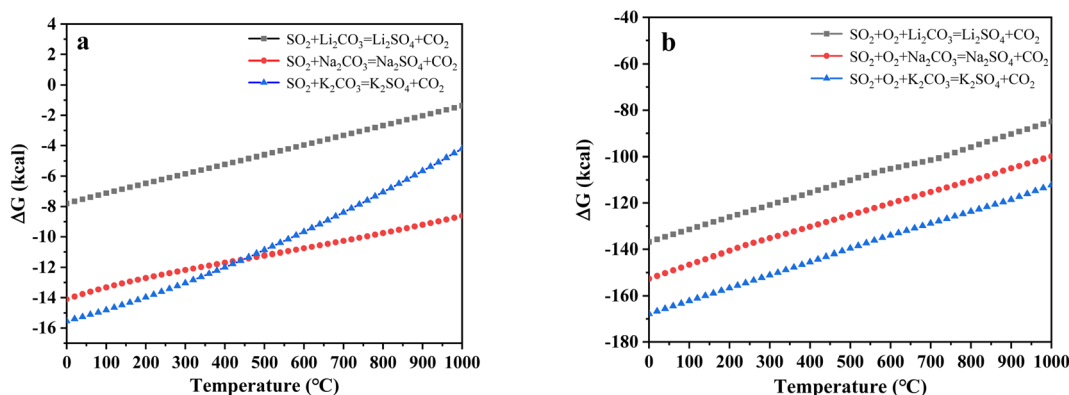


Fig. 3 The relationship between reaction temperature and Gibbs free energy ( $\Delta G$ ) required for the reaction of  $\text{SO}_2$  and carbonates in (a)  $\text{N}_2$  and (b) air atmospheres.



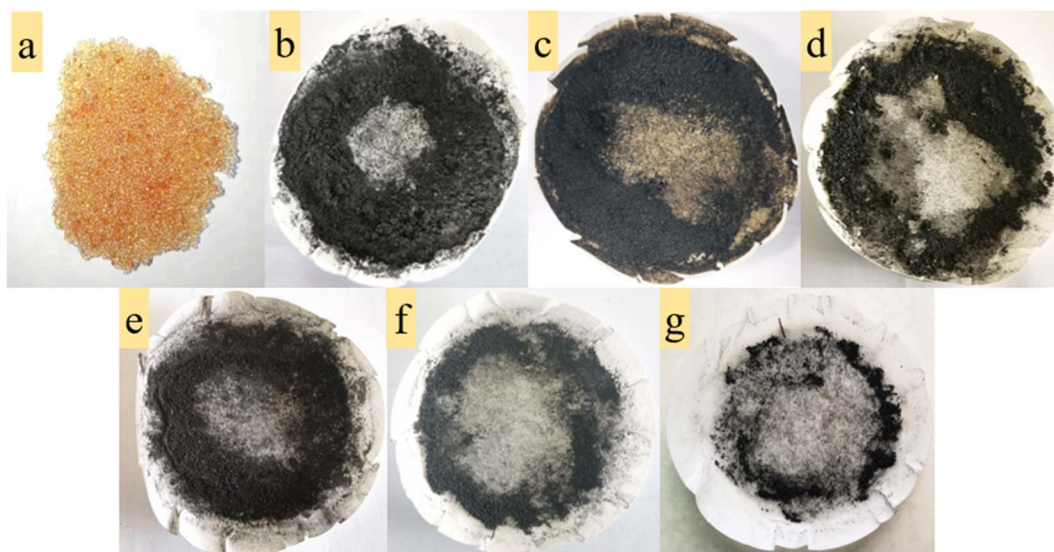


Fig. 4 The images of (a) original resins and product after the decomposition of uranium-containing resins in carbonate molten salt at (b) 460 °C, (c) 640 °C, (d) 720 °C in  $N_2$  atmosphere and at (e) 460 °C, (f) 640 °C, (g) 720 °C in air atmosphere.

### 3.2 The characterization analysis of product

**3.2.1 The morphology analysis of product.** Fig. 4 shows the images of original resins and products after decomposition of uranium-containing resins in carbonate molten salt at different reaction temperatures in  $N_2$  and air atmospheres. The reaction temperature was chosen based on TG results of uranium-containing resins. From Fig. 4a, the color of original resins before destruction in  $N_2$  atmosphere was brown. With increasing reaction temperature, the resins changed from brown to black (Fig. 4b–d) and the remaining mass of residues gradually decreased, which confirmed that the amplify in temperature triggered the decomposition of resins.

From Fig. 4e–g, in contrast to  $N_2$  atmosphere, the remaining mass of residues after resin decomposition in carbonate molten salt in air atmosphere obviously decreased at the same temperature. It meant that the oxidation decomposition of resins was prompted due to the addition of air. Besides, from Fig. 4e and f, with reaction temperature increasing from 460 °C

to 640 °C, the remaining mass of residues had a considerable decrease, which showed that majority of resins were oxidized to  $CO_2$  in air atmosphere. This result was validated by the conclusion in Fig. 2c.

**3.2.2 The decomposition rate of resins and retention rate of sulfur.** The decomposition rate of resins and retention rate of sulfur after the decomposition of uranium-containing resins in carbonate molten salt at different temperatures for 30 min in  $N_2$  and air atmospheres are presented in Fig. 5. From Fig. 5a, when temperature increased from 325 °C to 800 °C, the decomposition rate of resins increased from 37.3% to 54.3% in  $N_2$  atmosphere, and in air atmosphere, that of resins increased from 38.2% to 82.6%. During the decomposition of uranium-containing resins in carbonate molten salt in  $N_2$  and air atmospheres, the increase in temperature prompted the decomposition of resins. Associated with the TG analysis in Fig. 1, the decrease of resin decomposition rate at 325 °C was mainly ascribed to the dehydration of the remaining water and

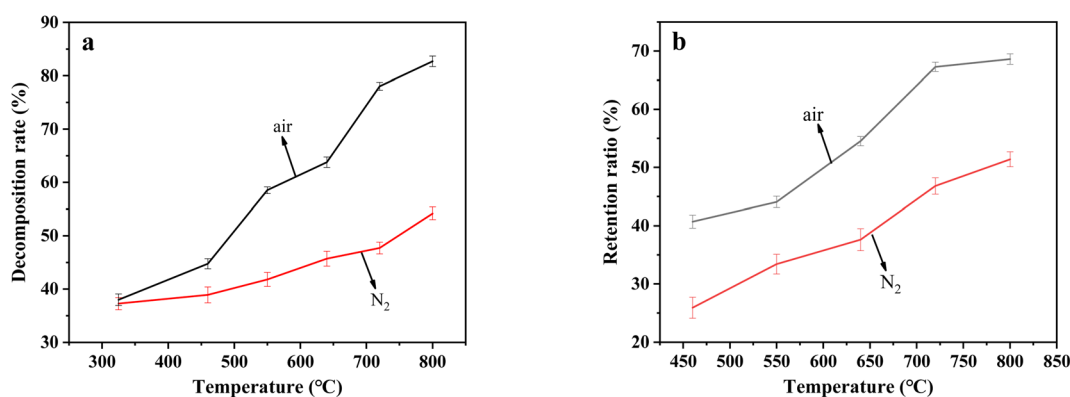


Fig. 5 (a) The decomposition rate of resins and (b) retention rate of sulfur after the decomposition of uranium-containing resins in carbonate molten salt at different temperatures for 30 min in  $N_2$  and air atmospheres.

the decomposition of some sulfonic acid functional groups. Nevertheless, due to the stability of the ion bond formed by uranyl ions on the sulfonic acid group, the sulfonic acid group in uranium-containing resins was difficult to decompose at 325 °C, which resulted in a slightly low decomposition rate of resins. This conclusion was similar to the inhibition of resin pyrolysis with metal ion doping.<sup>29,30</sup> With temperature increasing from 325 °C to 460 °C, the ion bonds on the sulfonic acid group of uranium-containing resins were gradually decomposed, which generated SO<sub>2</sub> (Fig. 2d). Meanwhile, the hydrocarbon structure was destroyed, which released CH<sub>4</sub>, C<sub>2</sub>H<sub>4</sub> and CO<sub>2</sub> (Fig. 2a–c). The production of exhaust gas corresponded to the increase in resin decomposition rate at 325–460 °C. When temperature was increased to 550 °C, the decomposition rate of uranium-containing resins continuously greatly increased. This conclusion was because the ion bonds on the sulfonic acid group of uranium-containing resins were completely destroyed. Besides, the increase in decomposition rate of resins in air atmosphere was larger than that in N<sub>2</sub> atmosphere at 460–550 °C, which meant that the presence of air prompted the oxidation decomposition of ST-DVB matrix and polymer chains in resins and resulted in the release increase in CO<sub>2</sub>. As temperature continuously increased, the decomposition rate of uranium-containing resins gradually increased, and the change curve of resin decomposition rate becomes steeper. Thus, the decomposition rate of resins in air atmosphere was higher than that in N<sub>2</sub> atmosphere, which was consistent with the TG analysis in Fig. 1. Compared to the results of Fig. 1, the decomposition efficiency of resins in molten salt could be lower at the same temperature in Fig. 5. This was because in the thermal property analysis of resin in Fig. 1, resins without carbonate were directly decomposed in air atmosphere, and the cross-linked structure and carbon chain structure of the resin were destroyed, resulting in high weight loss of resins. However, in Fig. 5a, when samples contained carbonate, oxygen in air atmosphere could be first dissolved in molten salt and then,

resins were oxidized and decomposed in molten carbonate. When the reaction temperature increased, more oxygen was dissolved in molten salt, and the oxidation decomposition of resins could be further improved. Therefore, the decomposition efficiency of resins in molten salt could be lower at the same temperature.

From Fig. 5b, when temperature increased from 325 °C to 800 °C, the retention rate of sulfur after the decomposition of resins in carbonate molten salt in N<sub>2</sub> atmosphere gradually increased from 17.7% to 51.4%, while that increased from 40.7% to 68.7% in air atmosphere. Compared to N<sub>2</sub> atmosphere, organic sulfur in resins could be more easily retained by carbonate melt at high temperature in air atmosphere. According to the analytical results in Fig. 5a and b, it was determined that in air atmosphere, large quantities of resins were oxidized and decomposed to SO<sub>2</sub>, which was absorbed by carbonate molten salt and resulted in the substantial increase in sulfur retention rate.

In order to further investigate the decomposition of uranium-containing resins in (Li<sub>2</sub>CO<sub>3</sub>–Na<sub>2</sub>CO<sub>3</sub>–K<sub>2</sub>CO<sub>3</sub>) molten-salt system, the characteristics of products after the decomposition of resins at different reaction temperatures were studied using various analysis methods including SEM-EDS, XRD, FT-IR and XPS.

**3.2.3 Scanning electron microscopy (SEM) analysis.** Fig. 6 describes the SEM morphology of original resins and residues after the decomposition of uranium-containing resins in carbonate molten salt at different temperatures in N<sub>2</sub> atmosphere. In Fig. 6a, resins after decomposition maintained a good spherical structure at 325 °C, since ion bonds on sulfonic acid groups and the cross-linked structure of resins have good thermal stability. At 460 °C, some holes were observed on the shell surface of resins in Fig. 6c, which was ascribed to resins being further destroyed at high temperature. With increasing temperature from 460 °C to 720 °C, more holes on the shell surface of resins were found. However, because the cross-linked

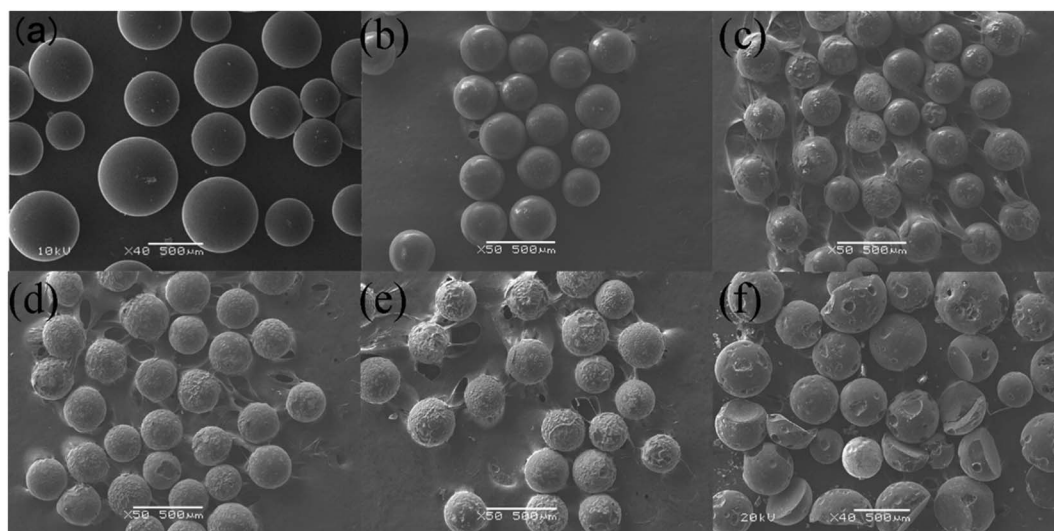


Fig. 6 The SEM morphology of (a) original resins and residues after the decomposition of uranium-containing resins in carbonate molten salt at (b) 325 °C, (c) 460 °C, (d) 550 °C, (e) 640 °C and (f) 720 °C in N<sub>2</sub> atmosphere.



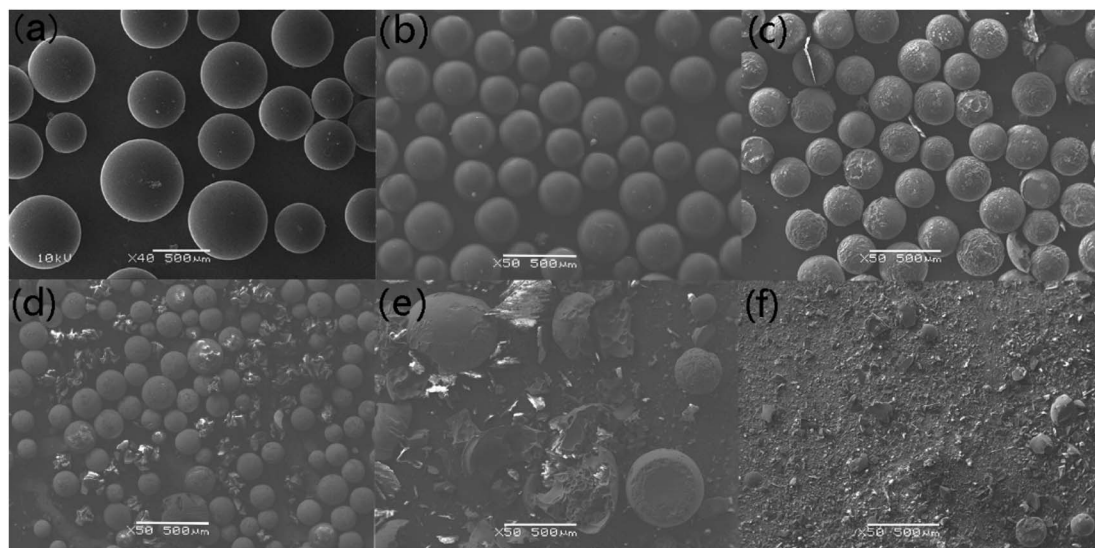


Fig. 7 The SEM morphology of (a) original resins and residues after the decomposition of uranium-containing resins in carbonate molten salt at (b) 325 °C, (c) 460 °C, (d) 550 °C, (e) 640 °C and (f) 720 °C in air atmosphere.

structure of resins had good thermal stability and structural stability, parts of resins could maintain the spherical structure at 720 °C. Besides, some stable organic structures were generated in the resin structure, which made the resin structure difficult to decompose.

Compared to  $N_2$  atmosphere, the SEM morphology of residues after decomposition of uranium-containing resins in carbonate molten salt in air atmosphere showed an obvious change at different temperatures (as shown in Fig. 7). When temperature was increased to 460 °C, the smooth surface of resins became uneven, and more holes appeared on the surface of resins in Fig. 7c, since the hydrocarbon structure of resins was decomposed. With increasing temperature, the spherical structure of parts of resins was destroyed and decomposed in Fig. 7d. Thus, the increase in temperature prompted the decomposition of ion bonds on sulfonic acid groups and resins, which resulted in the cleavage of resin morphology. The conclusion was confirmed by the increase in resins decomposition efficiency in Fig. 5a. Compared to  $N_2$  atmosphere

(Fig. 6e), a majority of resins were destroyed in air atmosphere at 640 °C (Fig. 7e), which implied that the cross-linked structure of resins was further destroyed by air. When temperature was 720 °C, the cross-linked structure of resins was basically completely destroyed in Fig. 7f. Based on the analytical result, the addition of air facilitated the oxidation decomposition of ion bonds on sulfonic acid groups and resin cross-linked structure at high temperature.

**3.2.4 X-ray diffraction (XRD) analysis.** XRD technology was applied for the analysis of chemical components in spent salt after uranium-containing resin decomposition in carbonate molten salt at different temperatures in  $N_2$  and air atmospheres and the results are shown in Fig. 8. It was seen from Fig. 8a that spent salt after the destruction of uranium-containing resins mainly contained sulfates, uranium oxides and alkali metal diuranate. The sulfur element in sulfates was from the sulfonic acid group functional group ( $-SO_3H$ ) in resins. When temperature was 325 °C, sulfates in the form of  $Na_2SO_4$  (PDF card No. 24-1132) and  $UO_2SO_4$  (PDF card No. 24-1378) and uranium

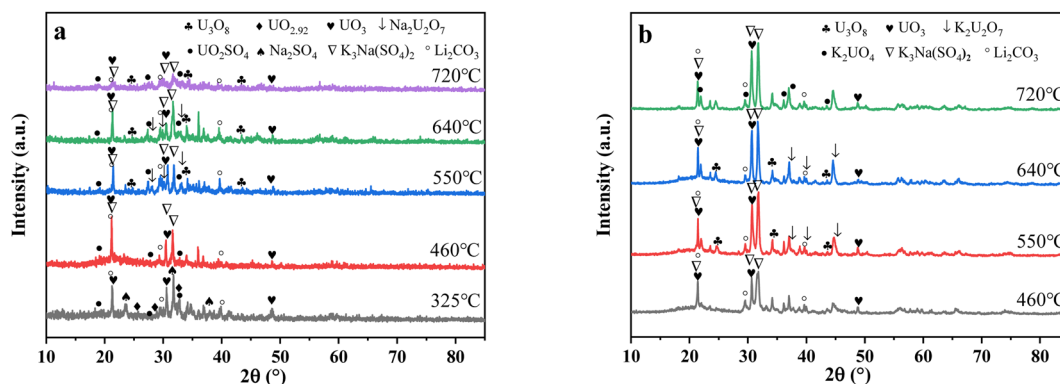


Fig. 8 The XRD patterns of spent salt after the decomposition of uranium-containing resins at different temperatures in carbonate molten salt in (a)  $N_2$  and (b) air atmospheres.

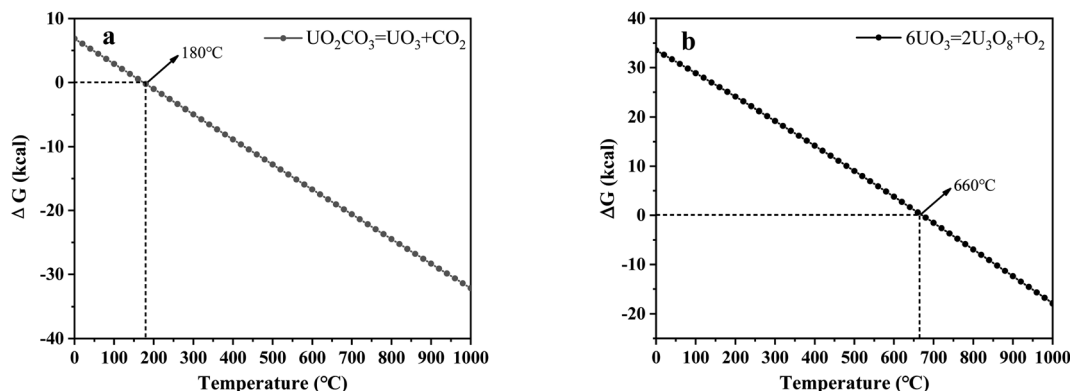


Fig. 9 Analysis of the thermal characteristics of reaction for (a)  $\text{UO}_2\text{CO}_3\text{--UO}_3$  and (b)  $\text{UO}_3\text{--U}_3\text{O}_8$  using the HSC Chemistry 6.0 thermodynamic software.

oxides in the form of  $\text{UO}_3$  (PDF card No. 31-1419) and  $\text{UO}_{2.92}$  (PDF card No. 46-0948) appeared in spent salt. The formation of sulfates was ascribed to the absorption of  $\text{SO}_2$  by carbonates. The reaction between uranyl ions and sulfate ions in molten salt led to the formation of  $\text{UO}_2\text{SO}_4$ .  $\text{UO}_3$  could result from the decomposition of uranyl carbonate at high temperature.<sup>31</sup> The thermal characteristics of the reaction between  $\text{UO}_2\text{CO}_3$  and  $\text{UO}_3$  were studied using the HSC Chemistry 6.0 thermodynamic software, and the result is shown in Fig. 9a. When temperature gradually increased, the Gibbs free energy required for the transformation of  $\text{UO}_2\text{CO}_3$  to  $\text{UO}_3$  gradually decreased and the transformation reaction easily proceeded. Parts of  $\text{UO}_3$  were converted to  $\text{UO}_{2.92}$ . This conversion was used to establish the relationship between the final structures of  $\text{UO}_3$  to  $\text{U}_3\text{O}_8$ .<sup>32,33</sup> With the increase in temperature,  $\text{K}_3\text{Na}(\text{SO}_4)_2$  (PDF card No. 74-1742) was present in spent salt at 460 °C. At 550 °C,  $\text{U}_3\text{O}_8$  (PDF card No. 20-1345) and  $\text{Na}_2\text{U}_2\text{O}_7$  (PDF card No. 12-0106) were found in spent salt. The production of  $\text{Na}_2\text{U}_2\text{O}_7$  was ascribed to the reaction between  $\text{Na}_2\text{CO}_3$  and  $\text{U}_3\text{O}_8$ .<sup>34</sup>  $\text{U}_3\text{O}_8$  was present due to the conversion of  $\text{UO}_3$ .<sup>35</sup> The thermal characteristics of the reaction between  $\text{UO}_3$  and  $\text{U}_3\text{O}_8$  were analysed using the HSC Chemistry 6.0 thermodynamic software (as shown in Fig. 9b). Fig. 9b shows that with increasing temperature, the Gibbs free energy transforming  $\text{UO}_3$  to  $\text{U}_3\text{O}_8$  gradually decreased and the

transformation reaction easily proceeded. In Fig. 8a, as temperature was increased to 720 °C,  $\text{Na}_2\text{U}_2\text{O}_7$  phase essentially disappeared in spent salt, which was due to the decomposition of  $\text{Na}_2\text{U}_2\text{O}_7$ .<sup>36</sup> However,  $\text{K}_3\text{Na}(\text{SO}_4)_2$ ,  $\text{UO}_2\text{SO}_4$  and  $\text{U}_3\text{O}_8$  were still in spent salt. It meant that these compounds had a certain thermal stability at 720 °C. To further explain the stability of  $\text{UO}_2\text{SO}_4$  in carbonate molten salt at 720 °C, the HSC Chemistry 6.0 thermodynamic software was utilized to analyse the thermal characteristics of  $\text{UO}_2\text{SO}_4$ , and the result is shown in Fig. 10. From Fig. 10, the Gibbs free energy transforming  $\text{UO}_2\text{SO}_4$  to  $\text{UO}_3$  was relatively high at 720 °C, which illustrated that the transformation reaction did not easily proceed. In other words,  $\text{UO}_2\text{SO}_4$  remained stable at 720 °C. In addition, the SEM morphology of product after the decomposition of resins in carbonate molten salt at 720 °C was also studied, and the result is shown in Fig. 11. From Fig. 11, it was found that uranium was evenly distributed in spent salt.

From Fig. 8b,  $\text{K}_2\text{U}_2\text{O}_7$  (PDF card No. 13-0081) occurred in spent salt in air atmosphere at 460 °C. The formation of  $\text{K}_2\text{U}_2\text{O}_7$  resulted from the reaction between  $\text{UO}_3$  and  $\text{K}_2\text{CO}_3$  and the formation process is showed in reaction (3).<sup>37</sup> When temperature was 720 °C, a new peak of  $\text{K}_2\text{UO}_4$  was observed in spent salt. Because carbonate was in excess,  $\text{K}_2\text{U}_2\text{O}_7$  reacted with an excess of  $\text{K}_2\text{CO}_3$  to form  $\text{K}_2\text{UO}_4$  and this process is showed in reaction (4).<sup>37</sup> Compared to  $\text{N}_2$  atmosphere (Fig. 8a), the peak intensities of  $\text{K}_3\text{Na}(\text{SO}_4)_2$  obviously strengthened in air atmosphere (Fig. 8b), which meant that more sulfate remained in spent salt. The result was consistent with the high retention rate of sulfur in air atmosphere at 720 °C in Fig. 5b.

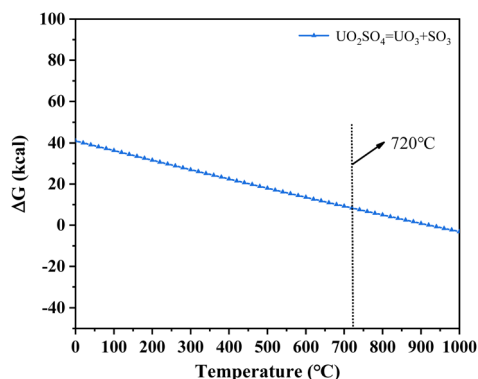


Fig. 10 The thermal characteristics of  $\text{UO}_2\text{SO}_4$  analysed using the HSC Chemistry 6.0 thermodynamic software.

**3.2.5 Fourier transform infrared spectrometer (FT-IR) analysis.** Fig. 12 describes the FT-IR spectrograms of residue after the decomposition of uranium-containing resins at different temperatures in carbonate molten salt in  $\text{N}_2$  and air atmospheres. The peak ( $743\text{ cm}^{-1}$ ) was the characteristic



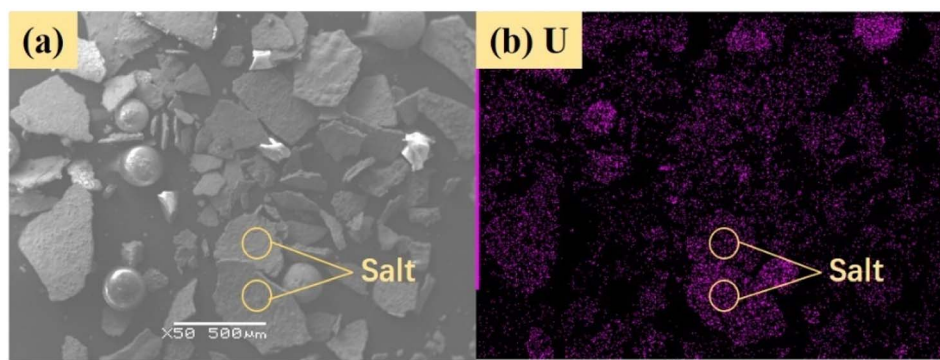


Fig. 11 Images of product at 720 °C: (a) SEM image, (b) uranium element distribution image.

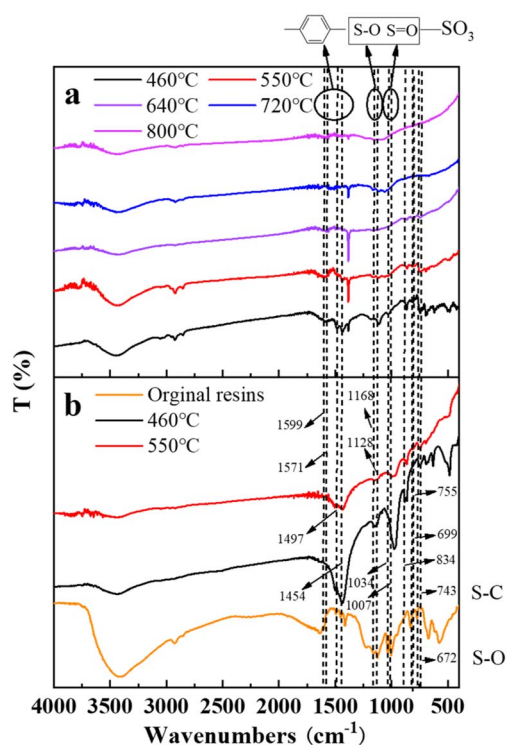


Fig. 12 The FT-IR spectrograms of residue after the decomposition of uranium-containing resins at different temperatures in carbonate molten salt in (a) air and (b)  $N_2$  atmospheres.

absorption of the S–C bond. The peaks ( $699$  and  $755\text{ cm}^{-1}$ ) were ascribed to the twisting and wobbling of the benzene ring.<sup>38,39</sup> The peak ( $834\text{ cm}^{-1}$ ) was due to outside surface bending of C–H in the benzene ring. The peaks ( $1007$  and  $1034\text{ cm}^{-1}$ ) were attributed to the characteristic absorption of the S=O bond in the sulfonic acid group functional group ( $-\text{SO}_3\text{H}$ ), and the peaks ( $672$ ,  $1128$  and  $1168\text{ cm}^{-1}$ ) were the characteristic absorption of the S–O bond.<sup>40,41</sup> The peaks ( $1454$ ,  $1497$ ,  $1571$  and  $1599\text{ cm}^{-1}$ ) corresponded to the C=C stretching of the aromatic benzene ring.<sup>42,43</sup>

In Fig. 12, compared to  $N_2$  atmosphere (Fig. 12b), the peak intensities of the benzene ring and sulfonic acid group functional group ( $-\text{SO}_3\text{H}$ ) after the decomposition of resins in

carbonate molten salt in air atmosphere were relatively weaker at  $460\text{ °C}$  in air atmosphere (Fig. 12a). It was determined that the addition of air prompted the destruction of the benzene ring and sulfonic acid group functional group ( $-\text{SO}_3\text{H}$ ). Associated with the analysis of Fig. 5a, the decomposition efficiency of resins (37.3%) in  $N_2$  atmosphere was slightly higher than that (44.7%) in air atmosphere, which meant that the benzene ring was destructed and could be further converted to other structures. These structures remained good thermal stability. In addition, the ion bond formed by uranyl ions on the sulfonic acid group had a certain thermal stability, which inhibited the decomposition of the sulfonic acid group in residues. When temperature increased from  $550\text{ °C}$  to  $720\text{ °C}$ , the intensity of characteristic peaks of the S–O bond and S–C bond in residues gradually weakened and basically disappeared at  $720\text{ °C}$ , which was ascribed to the oxidation decomposition of the S–O bond and S–C bond in air atmosphere.

**3.2.6 X-ray photoelectron spectrometer (XPS) analysis.** XPS spectroscopy can be further utilized to investigate the change in sulfur speciation and component percentage of sulfur species in residue. According to the binding energy of sulfur compounds, sulfur (2p) spectra was determined using components at the peaks of  $2p_{1/2}$  and  $2p_{3/2}$  with separated energy of  $1.18\text{ eV}$ .<sup>44,45</sup> The fitting result is presented in Fig. 13. From Fig. 13, there were three sulfur compounds existed in residues, such as thiophene sulfur ( $164.1 \pm 0.2\text{ eV}$ ), sulfoxide sulfur ( $165.7 \pm 0.3\text{ eV}$ ) and sulfone sulfur ( $168.0 \pm 0.5\text{ eV}$ ).<sup>46–49</sup> The binding energy gradually increased with the oxidation state of sulfur rising, which was consistent with the experimental result of Urban *et al.*<sup>50</sup>

From Fig. 13a, there were two sulfur species existing in residues at  $460\text{ °C}$ , including thiophene sulfur (89.97%) and sulfone sulfur (10.03%). The formation of thiophene sulfur was ascribed to the condensation reaction of organic sulfide.<sup>51</sup> Whereas, organic sulfide was relatively unstable and easily destroyed at high temperatures,<sup>52</sup> so organic sulfide was not observed in Fig. 13a. When resins were destroyed at  $550\text{ °C}$ , the relative proportion of thiophene sulfur decreased from 89.97% to 85.99% and sulfone sulfur increased from 10.03% to 14.01%. The change in sulfur compounds in residues was due to the transformation of sulfur species.<sup>53</sup> The increase in temperature accelerated the decomposition of parts of thiophene sulfur.



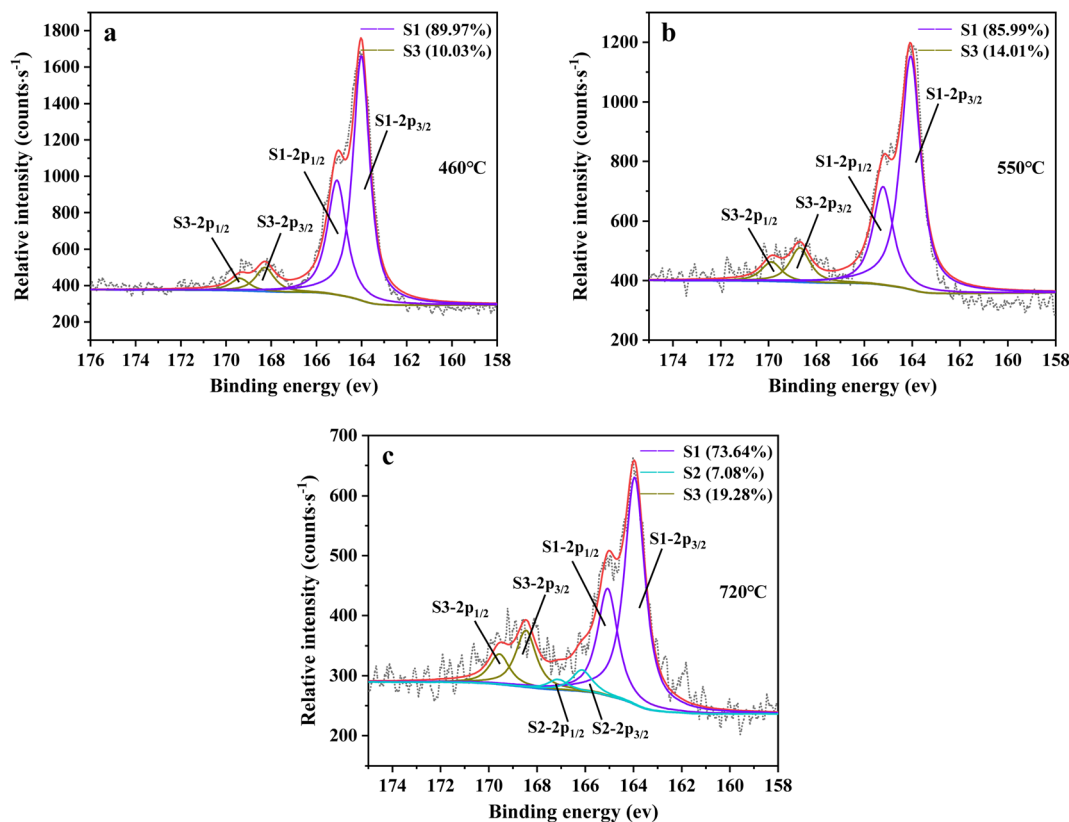
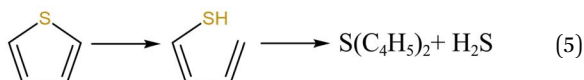


Fig. 13 Sulfur speciation in residue after the decomposition of uranium-containing resins and the spectra of S 2p conducted through the XPS spectrograph analysis (S1: thiophene sulfur, S2: sulfoxide sulfur, S3: sulfone sulfur) at (a) 460 °C, (b) 550 °C and (c) 720 °C in carbonate molten salt in N<sub>2</sub> atmosphere.

This decomposition of thiophene sulfur is shown in reaction (5).



In addition, combined with the component analysis of spent salt (Fig. 8a), parts of UO<sub>3</sub> were converted to U<sub>3</sub>O<sub>8</sub> at 550 °C and this conversion was accompanied by the production of oxygen (as exhibited in Fig. 9b).<sup>31</sup> When temperature was increased to 720 °C, sulfoxide sulfur was found in residues and the relative proportion was 7.08% in Fig. 13c. The relative proportion of sulfone sulfur increased from 14.01% to 19.28%, while that of thiophene sulfur significantly decreased from 85.99% to 73.64%. The increase in relative proportion of sulfone sulfur and sulfoxide sulfur corresponded to the decrease in relative proportion of thiophene sulfur, which was due to the decomposition of thiophene sulfur and the conversion of sulfone sulfur to sulfoxide sulfur. Meanwhile, the release of oxygen gradually increased with increasing temperature and a small amount of oxygen was chemically dissolved in molten salt.<sup>54,55</sup> The solubility of oxygen in carbonate molten salt also resulted in the oxidation of fractional thiophene sulfur and the conversion of some sulfone sulfur to sulfoxide sulfur. This transformation can be expressed in reactions (6)–(8), which was

confirmed by the decrease in thiophene sulfur and the increase in sulfoxide sulfur during the molten salt decomposition of resins.<sup>56</sup> Additionally, the production of CO<sub>2</sub> and SO<sub>2</sub> in these reactions corresponded to the experimental results in Fig. 2c and d.

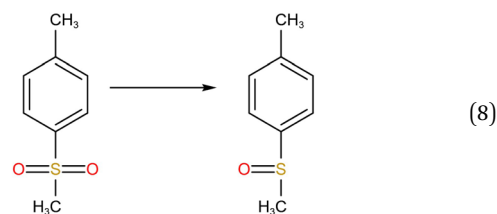
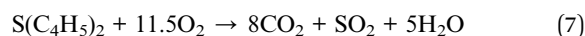
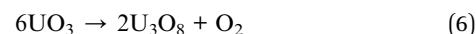


Fig. 14 shows sulfur speciation in residue after the decomposition of uranium-containing resins and the spectra of S 2p conducted through the XPS spectrograph at different temperatures in carbonate molten salt in air atmosphere. In Fig. 14a, there were three sulfur compounds existed in residues at 325 °C, such as thiophene sulfur (25.61%), sulfone sulfur (47.53%) and sulfonic acid sulfur (26.86%). When temperature was 460 °C, the relative proportion of thiophene sulfur after the



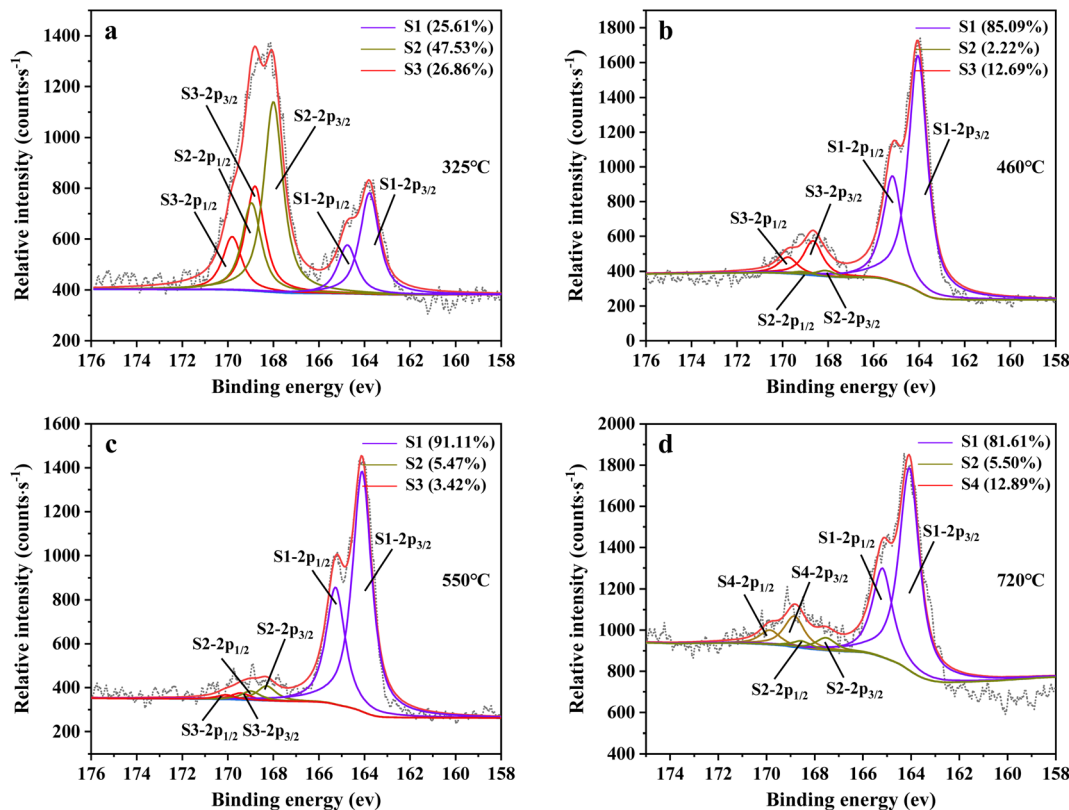


Fig. 14 Sulfur speciation in residue after the decomposition of uranium-containing resins and the spectra of S 2p conducted through the XPS spectrograph analysis (S1: thiophene sulfur, S2: sulfone sulfur, S3: sulfonic acid sulfur, S4: sulfate sulfur) at (a) 325 °C, (b) 460 °C, (c) 550 °C and (d) 720 °C in carbonate molten salt in air atmosphere.

decomposition of resins was increased to 85.09% in Fig. 14b. The increase in the relative proportion for thiophene sulfur was ascribed to the transformation of sulfone sulfur and sulfonic acid sulfur. When temperature was increased to 550 °C, the relative proportion of sulfone sulfur and thiophene sulfur

increased in Fig. 14c. Thus, the relative proportion in formation of sulfone sulfur and thiophene sulfur were more than that in consumption. When temperature was 720 °C, the decrease in relative proportion of thiophene sulfur corresponded to the increase in relative proportion of sulfate sulfur in Fig. 14d. It

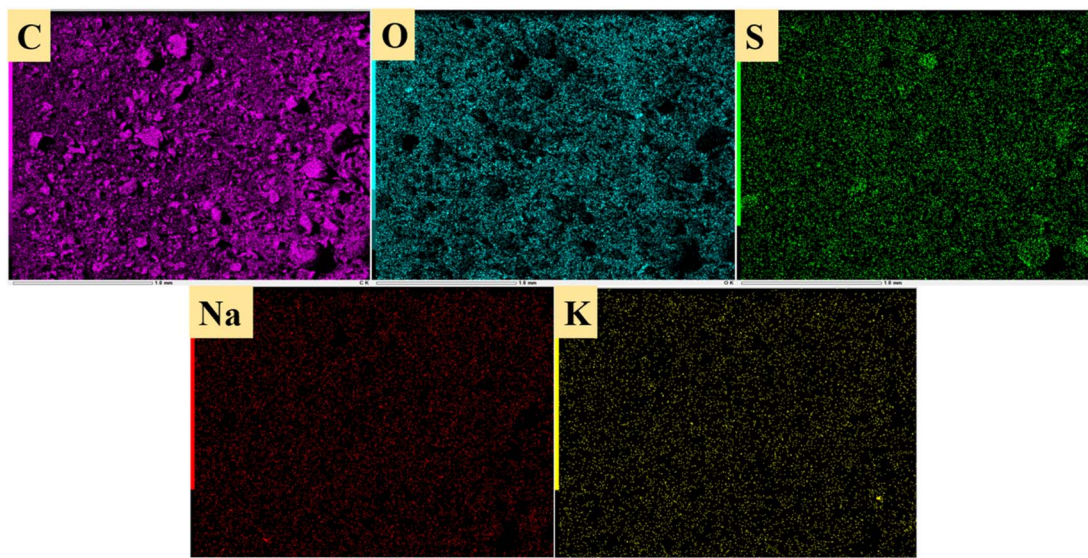


Fig. 15 EDS of residues after resin decomposition at 720 °C for 30 min.

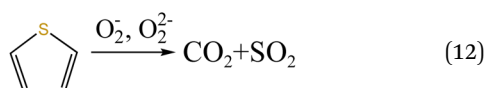
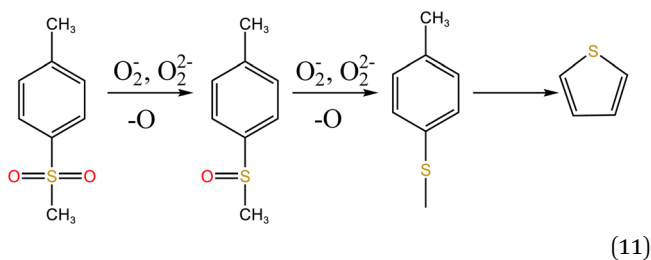
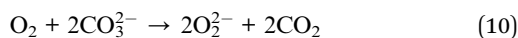
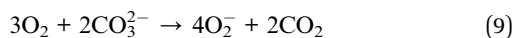
Table 1 The decomposition of uranium-containing resins in carbonate molten salt in air atmosphere

Temperature range	Decomposition process
325–460 °C	<p> <math>\text{H}_3\text{C}-\text{C}_6\text{H}_4-\text{SO}_3\text{H} \rightarrow \text{SO}_2 \xrightarrow{\text{molten salt}} \text{K}_3\text{Na}(\text{SO}_4)_2</math>  <math>\text{CH}_3-\text{C}_6\text{H}_4-\text{SO}_3\text{H} \xrightarrow{\text{O}_2, \text{O}_2^{2-}, -\text{O}} \text{CH}_3-\text{C}_6\text{H}_4-\text{SO}_2\text{H} \xrightarrow{\text{O}_2, \text{O}_2^{2-}, -\text{O}} \text{CH}_3-\text{C}_6\text{H}_4-\text{SO} \xrightarrow{\text{O}_2, \text{O}_2^{2-}, -\text{O}} \text{CH}_3-\text{C}_6\text{H}_4-\text{SH} \rightarrow \text{thiophene} \xrightarrow{\text{O}_2, \text{O}_2^{2-}} \text{CO}_2 + \text{SO}_2</math>  <math>\text{SO}_2 \xrightarrow[\text{O}_2, \text{O}_2^{2-}]{\text{molten salt}} \text{sulfates}</math> </p>
460–550 °C	<p> <math>\text{CH}_3-\text{C}_6\text{H}_4-\text{SO}_3\text{O}-(\text{UO}_2)^{2+}-\text{O}-\text{SO}_3-\text{C}_6\text{H}_4-\text{CH}_3 \xrightarrow{\text{O}_2, \text{O}_2^{2-}, -2\text{O}_2} \text{CH}_3-\text{C}_6\text{H}_4-\text{SO}_2\text{O}-(\text{UO}_2)^{2+}-\text{O}-\text{SO}_3-\text{C}_6\text{H}_4-\text{CH}_3 \xrightarrow{\text{O}_2, \text{O}_2^{2-}, -\text{O}_2} \text{CH}_3-\text{C}_6\text{H}_4-\text{SO}-(\text{UO}_2)^{2+}-\text{O}-\text{SO}_3-\text{C}_6\text{H}_4-\text{CH}_3 \xrightarrow{\text{O}_2, \text{O}_2^{2-}, -\text{O}_2} \text{CH}_3-\text{C}_6\text{H}_4-\text{SH}-(\text{UO}_2)^{2+}-\text{O}-\text{SO}_3-\text{C}_6\text{H}_4-\text{CH}_3 \rightarrow \text{thiophene} \xrightarrow{\text{O}_2, \text{O}_2^{2-}} \text{CO}_2 + \text{SO}_2</math>  <math>(\text{UO}_2)^{2+} \xrightarrow{\text{molten salt}} \text{UO}_2\text{CO}_3 \rightarrow \text{UO}_3</math>  <math>\text{SO}_2 \xrightarrow[\text{O}_2, \text{O}_2^{2-}]{\text{molten salt}} \text{sulfates}</math> </p>
550–720 °C	<p> <math>\text{CH}_3-\text{C}_6\text{H}_4-\text{SO}_3\text{O}-(\text{UO}_2)^{2+}-\text{O}-\text{SO}_3-\text{C}_6\text{H}_4-\text{CH}_3 \xrightarrow{\text{O}_2, \text{O}_2^{2-}, -2\text{O}_2} \text{CH}_3-\text{C}_6\text{H}_4-\text{SO}_2\text{O}-(\text{UO}_2)^{2+}-\text{O}-\text{SO}_3-\text{C}_6\text{H}_4-\text{CH}_3 \xrightarrow{\text{O}_2, \text{O}_2^{2-}, -\text{O}_2} \text{CH}_3-\text{C}_6\text{H}_4-\text{SO}-(\text{UO}_2)^{2+}-\text{O}-\text{SO}_3-\text{C}_6\text{H}_4-\text{CH}_3 \xrightarrow{\text{O}_2, \text{O}_2^{2-}, -\text{O}_2} \text{CH}_3-\text{C}_6\text{H}_4-\text{SH}-(\text{UO}_2)^{2+}-\text{O}-\text{SO}_3-\text{C}_6\text{H}_4-\text{CH}_3 \rightarrow \text{thiophene} \xrightarrow{\text{O}_2, \text{O}_2^{2-}} \text{CO}_2 + \text{SO}_2</math>  <math>(\text{ST-DVB matrix}) + (\text{polymer chains}) \xrightarrow{\text{O}_2, \text{O}_2^{2-}} \text{CO}_2 + \text{SO}_2</math>  <math>\text{SO}_2 \xrightarrow[\text{molten salt}]{\text{O}_2, \text{O}_2^{2-}} \text{sulfates}</math> </p>



was determined that the increase in relative proportion of sulfate sulfur resulted from the oxidation decomposition of thiophene sulfur in residues. The presence of sulfate sulfur could be because alkali metal sulfates in molten salt came into the resin structure, which corresponded to the uniform distribution of elements (Na, K, S and O) in residues in Fig. 15 and was confirmed by the analytical result in Fig. 8b.

To explore the oxidation decomposition of uranium-containing resins in carbonate molten salt in air atmosphere, the characteristics of products after resin decomposition were studied. During the decomposition of resins, SO<sub>2</sub> released from the cleavage of functional sulfonic acid groups was absorbed by carbonates to form sulfate at 325 °C. When temperature was 460 °C, K<sub>3</sub>Na(SO<sub>4</sub>)<sub>2</sub> and UO<sub>3</sub> were observed in spent salt. Compared to N<sub>2</sub> atmosphere, the production temperatures of CH<sub>4</sub>, C<sub>2</sub>H<sub>4</sub>, CO<sub>2</sub> and SO<sub>2</sub> released from the decomposition of resins were essentially unchanged (Fig. 2). The relative proportions of sulfone sulfur (2.22%) in residues in air atmosphere greatly decreased at 460 °C (Fig. 14b). Due to the existence of oxygen in air atmosphere, oxygen was chemically dissolved in molten salt and formed peroxide and superoxide ions, which could accelerate the conversion of sulfone sulfur to thiophene sulfur and generate CO<sub>2</sub> and SO<sub>2</sub> (Fig. 2c and d). This conversion is showed in reactions (9)–(12). However, sulfonic acid sulfur (12.69%) still existed in residues. This could be because parts of uranyl ions in spent salt formed some stable ion bonds with sulfonic acid group in residue structure. These ion bonds were attached to the benzene ring of ST-DVB matrix, which could keep resin structure stable in Fig. 7c.



When temperature was 550 °C, U<sub>3</sub>O<sub>8</sub>, UO<sub>3</sub> and K<sub>2</sub>U<sub>2</sub>O<sub>7</sub> as the main uranium compounds existed in spent salt. The conversion of UO<sub>3</sub> to U<sub>3</sub>O<sub>8</sub> was accompanied by the production of a small amount of oxygen. Besides, these stable ion bonds between uranates and sulfonic acid group were destroyed. Fractional sulfonic acid groups were decomposed, which led to the increase in relative proportion of sulfone sulfur and thiophene sulfur. Associated with the TG analysis of Fig. 1, ST-DVB matrix

and polymer chains in resins was oxidized by peroxide and superoxide ions in molten salt at 550 °C, which resulted in the increase in CO<sub>2</sub> release content (Fig. 2c) and the cleavage of resin structure (Fig. 7d). With the increase of temperature, the release content of CO<sub>2</sub> gradually increased. The uranium compounds essentially unchanged in spent salt at 640 °C. As temperature was 720 °C, UO<sub>3</sub> and K<sub>2</sub>UO<sub>4</sub> was the main uranium compounds in spent salt. A majority of resins were oxidized and decomposed, and ST-DVB matrix and polymer chains were basically completely destroyed, which corresponded to the increase in the decomposition efficiency of resins (Fig. 5a) and the morphology change of residues (Fig. 7f). Meanwhile, thiophene sulfur in residues was further oxidized and decomposed (Fig. 14d). This inference was confirmed by the increase in retention rate of sulfur in molten salt with increasing temperature from 550 °C to 720 °C (Fig. 5b). Because thiophene sulfur had excellent stability, thiophene sulfur still existed in spent salt at 720 °C. Based on these analytical results, the decomposition of uranium-containing resins in molten carbonates in air atmosphere is presented in Table 1.

## 4. Conclusions

In this work, the oxidation decomposition of uranium-containing resins in Li<sub>2</sub>CO<sub>3</sub>–Na<sub>2</sub>CO<sub>3</sub>–K<sub>2</sub>CO<sub>3</sub> molten salt system was investigated at different temperatures in air atmosphere. Based on the experimental analysis, the following conclusions were obtained:

(1) Compared to N<sub>2</sub> atmosphere, the release content of exhaust gas CO<sub>2</sub> released from the destruction of uranium-containing resins in air atmosphere was relatively high above 368 °C, which was because oxygen in the form of peroxide and superoxide ions in molten salt oxidized and decomposed ST-DVB matrix and polymer chains. The decrease in release content of SO<sub>2</sub> at 454 °C was assigned to the absorption of SO<sub>2</sub> by molten salt. The decomposition rate of resins in air atmosphere reached 82.6% at 800 °C in 30 min.

(2) Spent salt after resin decomposition was composed of sulfates and uranium compounds, and the retention rate of organic sulfur in spent salt at 800 °C was 68.7%. Besides, there were the transformation of UO<sub>3</sub> to U<sub>3</sub>O<sub>8</sub> and K<sub>2</sub>U<sub>2</sub>O<sub>7</sub> to K<sub>2</sub>UO<sub>4</sub> occurring in carbonate melt at 325–720 °C.

(3) These sulfur species showed a conversion law during the decomposition of uranium-containing resins in carbonate molten salt in air atmosphere. Peroxide and superoxide ions accelerated the conversion of sulfone sulfur to thiophene sulfur and generated CO<sub>2</sub> and SO<sub>2</sub> at 460 °C. The ion bond formed by uranyl ions on the sulfonic acid group inhibited the decomposition of the sulfonic acid group in residues. With the increase in temperature, sulfonic acid group was converted to sulfone sulfur (–SO<sub>2</sub>–), sulfoxide sulfur (–SO–) and further to thiophene sulfur. Finally, the oxidation decomposition of uranium-containing resins in molten carbonates in air atmosphere was explained.

(4) This work provided more theoretical guidance for the industrial treatment of uranium-containing resins and



technical support for the sustainable development of the nuclear industry.

## Author contributions

Zhi Zhang: data curation, supervision, conceptualization, writing-original draft, writing-reviewing & editing. Yun Xue: methodology, formal analysis, writing-reviewing & editing. Yong-De Yan: conceptualization, resources, investigation, writing-reviewing & editing. Guo-Qiang Li: data curation, supervision, conceptualization. Wen-Da Xu: project advisor, validation, formal analysis, writing-reviewing & editing. Fu-Qiu Ma: supervision, writing-reviewing & editing. Xin Liu: conceptualization, formal analysis, writing-reviewing & editing. Qing-Guo Zhang: conceptualization, formal analysis.

## Conflicts of interest

There are no conflicts to declare.

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## References

- 1 J. L. Wang and Z. Wan, Treatment and disposal of spent radioactive ion-exchange resins produced in the nuclear industry, *Prog. Nucl. Energy*, 2015, **78**, 47–55.
- 2 L. X. Huang, W. X. He and D. G. Chen, Solid radioactive waste management in Daya Bay nuclear power station, *Radiat. Prot.*, 2004, **24**, 211–226.
- 3 K. Kinoshita, M. Hirata and T. Yahata, Treatment of ion-exchange resins by fluidized bed incinerator equipped with copper oxide catalyst fundamental studies, *J. Nucl. Sci. Technol.*, 1991, **28**, 228–238.
- 4 C. M. Jantzen, W. E. Lee and M. I. Ojovan, Radioactive waste conditioning, immobilization, and encapsulation process and technologies: overview and advances, *Radioactive Waste Management and Contaminated Site Clean-Up: Process, Technologies and International Waste Experience*, 2013, pp. 171–272.
- 5 J. F. Li and J. L. Wang, Advances in cement solidification technology for waste radioactive ion exchange resins: A review, *J. Hazard. Mater.*, 2006, **135**, 443–448.
- 6 N. Moriyama, S. Dojiri, S. Emura, T. Sugo and S. Machi, Incorporation of radioactive spent ion exchange resins in plastics, *J. Nucl. Sci. Technol.*, 1975, **12**, 362–369.
- 7 L. Gong, D. H. Du, Li Cheng and Q. X. Zhao, Feasibility study of immobilization of simulated radioactive wastes using unsaturated polyester, *Radiat. Prot.*, 1991, **11**, 352–357.
- 8 X. Fan, M. Q. H. Lin, H. Z. Li, J. L. Tan, Y. H. Chang and L. Liu, A study on immobilization of spent resins with polyester, *At. Energy Sci. Technol.*, 1994, **28**, 348–355.
- 9 Y. J. Huang, H. P. Wang, S. H. Liu and M. C. Hsiao, Pyrolysis kinetics of spent low-level radioactive resin, *Nucl. Technol.*, 2002, **138**, 206–210.
- 10 A. Nezu, K. Moro and T. Watanabe, Thermal plasma treatment of waste ion exchange resins by CO<sub>2</sub> injection, *Thin Solid Films*, 2006, **506**, 432–435.
- 11 M. J. Quina, J. C. M. Bordado and R. M. Quinta-Ferreira, Chemical stabilization of air pollution control residues from municipal solid waste incineration, *J. Hazard. Mater.*, 2010, **179**, 382–392.
- 12 H. C. Yang, Y. J. Cho, H. C. Eun, J. H. Yoo and J. H. Kim, Molten salt oxidation of ion-exchange resins doped with toxic metals and radioactive metal surrogates, *J. Nucl. Sci. Technol.*, 2005, **42**, 123–129.
- 13 P. C. Hsu, K. G. Foster, T. D. Ford, P. H. Wallman, B. E. Watkins, C. O. Pruneda and M. G. Adamson, Treatment of solid wastes with molten salt oxidation, *Waste Manage.*, 2000, **20**, 363–368.
- 14 H. Nasir, P. Kassandra, L. Tristan and A. Tn, Thermal analysis and immobilization of spent ion exchange resin in borosilicate glass, *New J. Glass Ceram.*, 2012, **2**, 111–120.
- 15 H. C. Yang, M. W. Lee, I. H. Yoon, D. Y. Chung and J. K. Moon, Scale-up and optimization of a two-stage molten salt oxidation reactor system for the treatment of cation exchange resins, *Chem. Eng. Res. Des.*, 2013, **91**, 703–712.
- 16 N. Sathi Sasidharan, D. S. Deshingkar and P. K. Wattal, *Vitrification of spent organic ion exchange resins-<sup>137</sup>Cesium volatility during oxidation*, Bhabha Atomic Research Centre, 2006.
- 17 X. Z. Wang, Y. H. Zheng, Y. Xue, Y. D. Yan, F. Q. Ma, M. L. Zhang, H. Y. Bai, Z. Q. Kou and J. P. Liu, Study on the destruction process of cationic exchange resins treated by Li<sub>2</sub>CO<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub>-K<sub>2</sub>CO<sub>3</sub> molten salt, *J. Environ. Chem. Eng.*, 2021, **9**, 105948.
- 18 P. Antonetti, Y. Claire, H. Massit, P. Lessart, C. Pham Van Cang and A. Perichaud, Pyrolysis of cobalt and cesium doped cationic ion-exchange resin, *J. Anal. Appl. Pyrolysis*, 2000, **55**, 81–92.
- 19 H. C. Yang, J. S. Yun, M. J. Kang, J. H. Kim and Y. Kang, Mechanisms and kinetics of cadmium and lead capture by calcined kaolin at high temperatures, *Korean J. Chem. Eng.*, 2001, **18**, 499–505.
- 20 M. Matsuda, K. Funabashi and H. Yusa, Effect of metallic impurities on ion exchange resin oxidation rate, *J. Nucl. Sci. Technol.*, 1985, **22**, 241–243.
- 21 M. Matsuda, K. Funabashi and H. Yusa, Effect of Metallic Impurities on Oxidation Reaction of Ion Exchange Resin, (I) Catalytic Effect of Ionized and Unionized Irons, *J. Nucl. Sci. Technol.*, 1986, **23**, 244–252.
- 22 M. Matsuda, K. Funabashi and H. Yusa, Effect of Metallic Impurities on Oxidation Reaction of Ion Exchange Resin, (II) Comparison of Catalytic Activity between Six Metals, *J. Nucl. Sci. Technol.*, 1986, **23**, 813–818.



- 23 R. S. Juang and T. S. Lee, Oxidative pyrolysis of organic ion exchange resins in the presence of metal oxide catalysts, *J. Hazard. Mater.*, 2002, **92**, 301–314.
- 24 S. H. Yu, C. Zhang, X. P. Zhang, X. Liu, B. Wei, P. Tan, Q. Y. Fang, G. Chen and J. Xia, Release and transformation characteristics of Na/Ca/S compounds of Zhundong coal during combustion/CO<sub>2</sub> gasification, *J. Energy Inst.*, 2020, **93**, 752–765.
- 25 C. Y. Cao, Y. Ren, H. Wang, H. Y. Hu, B. J. Yi, X. Li, L. L. Wang and H. Yao, Insights into the role of CaO addition on the products distribution and sulfur transformation during simulated solar-powered pyrolysis of waste tires, *Fuel*, 2022, **314**, 122795.
- 26 J. R. Lanteigne, J. P. Laviolette and J. Chaouki, Behavior of sulfur during the pyrolysis of tires, *Energy Fuels*, 2015, **29**, 763–774.
- 27 H. Darmstadt, C. Roy and S. Kaliaguine, Inorganic components and sulfur compounds in carbon blacks from vacuum pyrolysis of used tires, *Kautsch. Gummi Kunstst.*, 1994, **47**, 891–895.
- 28 P. R. Westmoreland, J. B. Gibson and D. P. Harrison, Comparative kinetics of high temperature reaction between H<sub>2</sub>S and selected metal oxides, *Environ. Sci. Technol.*, 1977, **11**, 488–491.
- 29 J. Luo, W. R. Hu, Z. L. Suo, Y. B. Wang and Y. K. Zhang, Copyrolysis of spent radioactive ion exchange resin and manganese dioxide: Decrease the decomposition temperatures of functional groups, *J. Hazard. Mater.*, 2021, **418**, 126275.
- 30 H. C. Eun, H. C. Yang, Y. Z. Cho and H. S. Lee, Study on a stable destruction method of radioactive waste ion exchange resins, *J. Radioanal. Nucl. Chem.*, 2009, **281**, 585–590.
- 31 T. R. Griffiths and V. A. Volkovich, A review of the high temperature oxidation of uranium oxides in molten salts and in the solid state to form alkali metal uranates, and their composition and properties, *J. Nucl. Mater.*, 1999, **274**, 229–251.
- 32 A. F. Andresen, The structure of U<sub>3</sub>O<sub>8</sub> determined by neutron diffraction, *Acta Crystallogr., Sect. A: Found. Crystallogr.*, 2010, **211**, 612–614.
- 33 H. R. Hoekstra, S. Siegel, L. H. Fuchs and J. J. Katz, The Uranium-Oxygen System: UO<sub>2.5</sub> to U<sub>3</sub>O<sub>8</sub>, *J. Phys. Chem.*, 1955, **59**, 136–138.
- 34 K. M. Efremova, E. A. Ippolitova, Y. P. Simanov, *et al.*, An investigation of the composition of alkali element uranates obtained by a dry procedure, *Dokl. Akad. Nauk SSSR*, 1959, **124**, 29.
- 35 A. R. Bekeov, V. N. Strekalovskii and V. G. Vlasov, A study of the structure of solid solutions of uranium oxides in the range  $\alpha$ -UO<sub>3</sub>-U<sub>3</sub>O<sub>8</sub>, *J. Struct. Chem.*, 1965, **6**, 64–67.
- 36 E. H. P. Cordfunke and B. O. Loopstra, Sodium uranates: Preparation and thermochemical properties, *J. Inorg. Nucl. Chem.*, 1971, **33**, 2427–2436.
- 37 V. A. Volkovich, T. R. Griffiths, D. J. Fray and R. C. Thied, Solubilities and solubilisation enthalpies of alkali metal uranates(vi) in carbonate melts, *Phys. Chem. Chem. Phys.*, 1999, **1**, 3297–3302.
- 38 P. J. Wibawa, M. A. Agam, H. Nur and H. Saim, Changes in physical properties and molecular structure of polystyrene nanospheres exposed with solar flux, 2010 International Conference on Enabling Science & Nanotechnology, *AIP Conf. Proc.*, 2011, **1341**, 54–61.
- 39 J. Sheng and Y. Z. Wan, Preparation and characterization of TiO<sub>2</sub>/polystyrene core-shell nanospheres via microwave-assisted emulsion polymerization, *Mater. Lett.*, 2008, **62**, 37–40.
- 40 L. J. Koenig, Application of fourier transform infrared spectroscopy to chemical systems, *Appl. Spectrosc.*, 1975, **29**, 293–308.
- 41 R. M. Silverstein, G. C. Bassler and T. C. Morrill, Spectrometric identification of organic compounds, *J. Chem. Educ.*, 2014, 826–827.
- 42 A. Refik and U. Nurseli, Study of the morphological and thermal properties of polystyrene nanocomposites based on modified halloysite nanotubes with styrene-maleic anhydride copolymers, *Mater. Today Commun.*, 2017, **13**, 255–262.
- 43 S. Luciano, M. S. Mariana, L. S. Arxel, A. S. C. Adriana, M. A. Diana, F. M. Rachel and B. Roberto, Synthesis and characterization of styrene-vinyl tetrazole copolymers for their application as a solid electrolyte, *React. Funct. Polym.*, 2021, **167**, 105007.
- 44 L. Wang, P. Z. Zhang and M. Zheng, Study on structural characterization of three Chinese coals of high organic sulphur content using XPS and solid-state NMR spectroscopy, *J. Fuel Chem. Technol.*, 1996, **24**, 539–543.
- 45 M. A. Olivella, J. M. Palacios, A. Vairavamurthy, J. C. Delrio and F. X. C. Delasheras, A study of sulfur functionalities in fossil fuels using destructive-(ASTM and Py-GC-MS) and non-destructive-(SEM-EDX, XANES) and (XPS) techniques, *Fuel*, 2002, **81**, 405–411.
- 46 L. Flandinet, F. Tedjar, V. Ghetta and J. Fouletier, Metals recovering from waste printed circuit boards (WPCBs) using molten salts, *J. Hazard. Mater.*, 2012, **213**, 485–490.
- 47 C. Q. Lin, Y. Chi, Y. Q. Jin, X. G. Jiang, A. Buekens, Q. Zhang and J. Chen, Molten salt oxidation of organic hazardous waste with high salt content, *Waste Manage. Res.*, 2018, **36**, 140–148.
- 48 S. Kelemen, G. George and M. Gorbaty, Direct determination and quantification of sulphur forms in heavy petroleum and coals: 1. The X-ray photoelectron spectroscopy (XPS) approach, *Fuel*, 1990, **69**, 939–944.
- 49 S. R. Kelemen, M. Afeworki, M. L. Gorbaty, M. Sansone, P. J. Kwiatek, C. Walters, H. Freund, M. Siskin, A. E. Bence, D. Curry, M. S. Solum and R. Pugmire, Direct characterization of kerogen kerogen by X-ray and solid-state, *Energy Fuels*, 2007, **21**, 1548–1561.
- 50 N. R. Urban, K. Ernst and S. Bernasconi, Addition of sulfur to organic matter during early diagenesis of lake sediments, *Geochim. Cosmochim. Acta*, 1999, **63**, 837–853.



- 51 J. L. Hou, Y. Ma and S. Y. Li, Transformation of sulfur and nitrogen during Shenmu coal pyrolysis, *Fuel*, 2018, **231**, 134–144.
- 52 H. Y. Hu, Y. Fang and H. Liu, The fate of sulfur during rapid pyrolysis of scrap tires, *Chemosphere*, 2014, **97**, 102–107.
- 53 S. Cheng, Y. Qiao, J. Huang, L. Cao, H. Yang, H. Liu, Y. Yu and M. Xu, Effect of alkali addition on sulfur transformation during low temperature pyrolysis of sewage sludge, *Proc. Combust. Inst.*, 2017, **36**, 2253–2261.
- 54 J. A. Appleby, Solubilities of Oxygen and Carbon Monoxide in Carbonate Melts, *J. Electrochem. Soc.*, 1980, **8**, 1655–1659.
- 55 T. Nishina, Y. Masuda and I. Uchida, Gas solubility and diffusivity of H<sub>2</sub>, CO<sub>2</sub> and O<sub>2</sub> in molten alkali carbonates, *Proc. Int. Symp. Molten Salt Chemistry and Technology*, 1993, 424–435.
- 56 T. Kamo, K. Takaoka, J. Otomo and H. Takahashi, Effect of steam and sodium hydroxide for the production of hydrogen on gasification of dehydrochlorinated poly(vinyl chloride), *Fuel*, 2006, **85**, 1052–1059.

