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## A municipal wastewater treatment plant “drinking beer” for reduction of cost and carbon emission

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In wastewater treatment plants (WWTPs), external carbon sources are often required due to low C/N influent. However, the use of external carbon sources can increase treatment costs and cause large carbon emissions. Beer wastewater, which contains a substantial amount of carbon, is often treated separately in China, consuming significant energy and cost. However, most studies using beer wastewater as an external carbon source are still on a laboratory scale. To address this issue, this study proposes using beer wastewater as an external carbon source in an actual WWTP to reduce operating costs and carbon emissions while achieving a win-win situation. The denitrification rate of beer wastewater was found to be higher ( $0.075 \text{ g}_{\text{NO}_3^--\text{N}}/\text{g}_{\text{MLVSS}} \text{ d}$ ) than that of sodium acetate ( $0.072 \text{ g}_{\text{NO}_3^--\text{N}}/\text{g}_{\text{MLVSS}} \text{ d}$ ), resulting in improved treatment efficiency of the WWTP. Specifically, COD,  $\text{BOD}_5$ , TN,  $\text{NH}_4^+-\text{N}$  and TP increased by 3.4%, 1.6%, 10.8%, 1.1%, and 1.7%, respectively. Additionally, the treatment cost and carbon emission per 10 000 tons of wastewater treated were reduced by 537.31 yuan and 2.27 t  $\text{CO}_2$ , respectively. These results indicate that beer wastewater has significant utilization potential and provide a reference for using different types of production wastewater in WWTPs. This study's findings demonstrate the feasibility of implementing this approach in an actual WWTP setting.

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## 1 Introduction

In recent years, the Chinese government has placed great emphasis on improving the capacity and number of urban wastewater treatment plants (WWTPs) in the country.<sup>1</sup> However, despite this progress, the operational performance and energy efficiency of most WWTPs in China still lag behind those of developed countries.<sup>2</sup> To ensure sustainable and stable operation of WWTPs, it is crucial to find ways to improve their performance and reduce energy consumption.<sup>3</sup> Additionally, given that carbon emissions from China's wastewater treatment account for 1–2% of the total social carbon emissions,<sup>4</sup> reducing carbon emissions from WWTPs has become a pressing concern, especially in light of China's carbon peaking and carbon neutrality goals.

One key issue that WWTPs in China face is the need for an external carbon source due to low carbon nitrogen ratio (C/N) influent, particularly in the southern regions of the country, and this is closely related to denitrification efficiency.<sup>5–7</sup> Despite efforts to conserve carbon sources by not setting up primary sedimentation tanks, insufficient carbon sources remain

a significant challenge. Thus, it is crucial to reduce the use of external carbon sources and improve their utilization rate. To address this issue, researchers have explored denitrification of wastewater under low C/N ratio conditions.<sup>8,9</sup> However, increasing the nitrate cycle rate has been found to have limited impact on improving denitrification efficiency under such circumstances.<sup>10</sup> Some researchers have proposed new processes and optimized existing ones. For example, step feed,<sup>11</sup> simultaneous nitrification and denitrification (SND),<sup>12</sup> and endogenous denitrification (ED)<sup>13</sup> technologies have been developed, which have improved the utilization efficiency of carbon sources in influent, resulting in improved denitrification rates.<sup>14</sup> Autotrophic denitrification using iron and hydrogen as electron donors and inorganic carbon source has also been studied.<sup>15,16</sup> However, these new process is not yet widely applicable in WWTPs due to technological limitations. Despite ongoing efforts to develop new methods, adding an external carbon source remains a common approach to improving the nitrogen removal rate in WWTPs.

The most commonly used external carbon source in China's WWTPs is commercial carbon source, particularly sodium acetate (NaAC) and glucose (GLU).<sup>17</sup> However, such sources have several drawbacks, including hidden safety risks and high costs. Different types of commercial carbon source also result in varying nitrogen removal rates.<sup>18</sup> Moreover, the need for supporting facilities such as measurement and management further increases the operation and management cost.<sup>19</sup>

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Methanol, another external carbon source, poses safety risks due to its flammability, necessitating additional safety measures during transportation and storage.<sup>20</sup> Researchers have explored alternative sources of external carbon, such as biodegradable polymers (BDPs) and natural materials based on cellulose, to reduce costs and increase environmental friendliness. However, BDPs are more expensive,<sup>6,21</sup> and methane is susceptible to oxygen concentrations.<sup>22</sup> Although natural cellulose-based sources have been studied as potential alternatives,<sup>23</sup> the initial and saturated carbon release rates vary significantly, and the effect after addition is unstable, making them unsuitable for widespread application.<sup>24</sup> Therefore, a low-cost, high-performance, and environmentally friendly external carbon source is necessary. Production wastewater may be a satisfactory alternative to commercial carbon sources. Further research is needed to determine the feasibility and effectiveness of production wastewater as an external carbon source in WWTPs, but it holds promise as a potential solution to the challenges associated with existing external carbon sources.

Studies on using production effluents, such as beer effluents, as external carbon sources have mostly been conducted on a laboratory scale. Na *et al.* explored the influence of the dosage of beer wastewater on nitrogen and phosphorus removal in a laboratory-scale AAO reactor,<sup>25</sup> and Mielcarek *et al.* explored the influence of beer wastewater on microorganisms in a laboratory-scale anaerobic sequencing batch reactor.<sup>26</sup> However, laboratory scale experiments have their limitations, such as the inability to simulate the change of water quality and quantity in the actual WWTP, the actual situation of the operation method cannot be applied, and the cost accounting and carbon emission accounting cannot be carried out. The production wastewater containing carbon produced in the process of agricultural products and food production has high organic concentration and good biodegradability.<sup>8</sup> Quan *et al.* used hydrolyzed molasses (the percentage of biodegradable substrates was 47.5%) and methanol as external carbon source in sequencing batch reactor (SBR) to treated urban wastewater, and the nitrogen removal rate was  $91.6 \pm 1.6\%$ , which was better than methanol ( $85.3 \pm 2.0\%$ ).<sup>27</sup> Fernandez Nava *et al.* achieved the denitrification of wastewater with nitrate content of  $2500 \text{ mg L}^{-1}$  by using sugar, beverage and dairy plant wastewater as the only external carbon source in SBR.<sup>28</sup> Studies have shown that carbon-containing industrial wastewater can be used as an external carbon source for WWTPs and has great potential for practical use. However, relevant policies in China limit its practical application, which also leads to less research on the practical application of production wastewater in WWTPs.<sup>29</sup>

In recent years, China has implemented environmental protection policies that require industrial wastewater to be treated to meet specific standards before it is transferred to WWTPs *via* sewage pipes. However, some industrial wastewater, which contains high concentrations of organic matter, has high biodegradability, low toxicity, and few side effects, also undergoes pretreatment before being transferred to WWTPs. This pretreatment process reduces the influent C/N ratio of WWTPs, which wastes a significant amount of available carbon

sources and increases treatment costs for both industrial enterprises and WWTPs. To address this issue, the Ministry of Ecology and Environment and the State Administration for Market Regulation of China issued an amendment to the Discharge Standard of Pollutants for Beer Industry (GB 19821-2005) in December 2020.<sup>30</sup> This amendment clarified that the wastewater of alcohol enterprises, including beer wastewater, can be used as a high-quality external carbon source for WWTPs. This can promote the stable operation of WWTPs and reduce their operating costs and carbon emissions. However, despite this policy change, there are still limited reports on the practical application of beer wastewater as an external carbon source in actual WWTPs. In light of this, it is important to investigate the potential of beer wastewater as an external carbon source and assess its economic and environmental impact when used in WWTPs. This knowledge can help inform future policies that encourage the use of production wastewater as a carbon source in WWTPs.

This paper proposes a system that uses beer wastewater as an external carbon source and applies it to an actual WWTP to reduce the operating costs and carbon emissions of the WWTP. The study analyzes the data of the WWTP in 2017 (before adding beer wastewater) and 2021 (after adding beer wastewater) to investigate the change in treatment effect before and after using beer wastewater as an external carbon source, the denitrification rate of activated sludge in beer wastewater as a carbon source, the economic cost analysis of the system, and carbon emission changes of beer wastewater as an external carbon source. Based on these analyses, it is predicted that production wastewater (wastewater with high carbon content that can be used as an additional carbon source, such as sugar wastewater, wine wastewater and vinegar wastewater) will be widely used as a carbon source in WWTPs in the future.

## 2. Materials and methods

### 2.1 Overview of wastewater treatment plant and adding method of beer wastewater

The WWTP in Huzhou City, Zhejiang Province, China, was commissioned in February 2002 and has a designed capacity of treating  $40\,000 \text{ m}^3$  of wastewater per day, with industrial and domestic wastewater accounting for 40% and 60%, respectively. The WWTP employs an anaerobic-anoxic-oxic (AAO) process, as depicted in Fig. 1. In China, due to the low C/N ratio of influent, an initial sedimentation tank is generally not employed to prevent the loss of particulate organic matter and increase the content of influent organic matter. However, the WWTP still faces the challenge of insufficient influent carbon source and needs to add an external carbon source.

The yeast plant uses brewery wastewater to produce yeast. After precipitation, the sediment from the beer wastewater is used as a raw material for yeast production, and the upper beer wastewater becomes the production wastewater. According to the Discharge Standard of Pollutants for Beer Industry (GB 19821-2005) in China, the yeast plant is required to treat the production wastewater by itself or outsource it to relevant companies to make it meet the discharge standard before it can



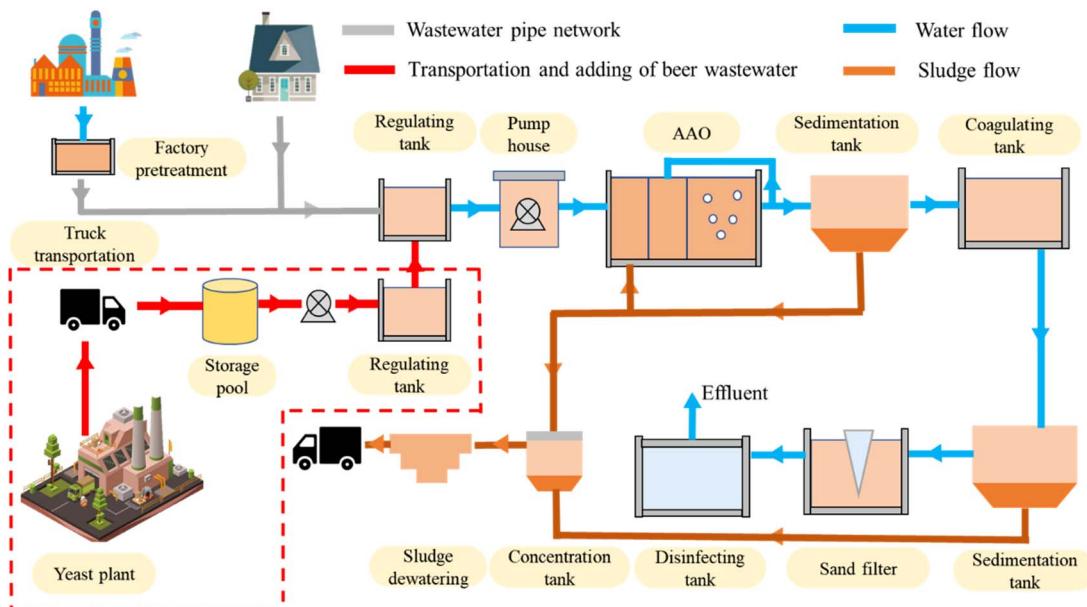


Fig. 1 Main process flow of the wastewater treatment plant, and the transportation and adding method of beer wastewater.

Table 1 Main water quality parameters of beer wastewater

Water quality parameters	Concentration (mg L <sup>-1</sup> ) or range
COD	134 570–208 789
BOD <sub>5</sub> /COD	0.76 ± 0.08
TN	1056–2195
NH <sub>4</sub> <sup>+</sup> -N	400–786
TP	371–1301
pH	4.37–4.64

be discharged into the sewage pipe network. However, this approach can be expensive. The water quality of the beer wastewater, including pH, chemical oxygen demand (COD), biochemical oxygen demand (BOD<sub>5</sub>), total nitrogen (TN), ammonia nitrogen (NH<sub>4</sub><sup>+</sup>-N), and total phosphorus (TP), is summarized in Table 1.

To reduce costs and promote a win-win situation, the WWTP has entered into a partnership with the yeast plant, using the beer wastewater as an external carbon source. The transportation and dosing method of the beer wastewater to the WWTP is illustrated in the red dotted line in Fig. 1. The production wastewater is transported by truck from the yeast plant to the WWTP and stored in a storage tank. Because the influent carbon source decreases at night, the beer wastewater is transported to the regulating tank by pump at night and added to the influent regulating tank through the overflow. The dosage is approximately one ton of beer wastewater per ten thousand tons of wastewater, which translates to a beer wastewater to water intake ratio of approximately 1 : 10 000. Therefore, pH adjustment and pretreatment are not required. Moreover, to prevent TN in beer wastewater from affecting

denitrification, the beer wastewater is mixed with influent water.

## 2.2 Analysis method

The influent water sample of the WWTP was taken from the influent water of the wastewater pipe network into the regulating tank, and the effluent water sample was taken from the effluent water of the disinfection tank. The parameters COD, BOD<sub>5</sub>, NH<sub>4</sub><sup>+</sup>-N, NO<sub>3</sub><sup>-</sup>-N, TP, TN, mixed liquid suspension (MLSS) and mixed liquid volatile suspension (MLVSS) were measured according to standard methods.<sup>31</sup> Dissolved oxygen, pH and temperature were measured using a German WTW Multi 3420.

## 2.3 Method of measuring denitrification rate

Three sets of reactors (R1, R2 and R3) were set up to compare denitrification rate when NaAC and beer wastewater were used as carbon source. Sludge is taken from the biochemical tank of the WWTP, and prior to the experiment, the sludge was aerated for 3 h to consume the residual and internal carbon source, and then nitrogen blowing to remove oxygen. Sludge volume in reactors was 500 ml, and MLSS and MLVSS of the sludge were 3941 and 2068 mg L<sup>-1</sup>, respectively. Electromagnetic agitator stirring to ensure adequate reaction during the experiment. NaNO<sub>3</sub> was added to the three reactors to ensure that the initial nitrate nitrogen concentration was 30 mg L<sup>-1</sup>, R1 and R2 were added with NaAC solution (2 ml, 100 000 mg L<sup>-1</sup>), beer wastewater (2 ml), respectively, and R3 added pure water (2 ml) as the blank group. Experiments were run for two hours, respectively on 0, 1, 3, 5, 10, 15, 20, 30, 40, 60, 90 and 120 minutes in R1, R2 and R3 extracted the same volume water samples to measure the concentration of NO<sub>3</sub><sup>-</sup>-N.



## 2.4 Carbon emission calculation

The carbon emissions from the beer wastewater treatment station (BWTS) and the WWTP were calculated according to the Technical Specification for Low-carbon Operation Evaluation of Sewage Treatment Plant (T/CAEPI 49-2022) (in Chinese).<sup>32</sup> The emission of CH<sub>4</sub> generated in the direct emission process are calculated according to formula (1).

$$m_{\text{CH}_4} = \frac{Q \times (\text{COD}_{\text{in}} - \text{COD}_{\text{out}})}{1000} \times \text{EF}_{\text{COD}} \quad (1)$$

where  $Q$  is the daily influent of the WWTP (m<sup>3</sup>); COD<sub>in</sub> is the average daily influent COD<sub>cr</sub> concentration of the WWTP (mg L<sup>-1</sup>); COD<sub>out</sub> is the average daily effluent COD<sub>cr</sub> concentration of WWTP (mg L<sup>-1</sup>); EF<sub>COD</sub> is the CH<sub>4</sub> emission factor in the treatment process (kg CH<sub>4</sub>/kg COD), and the emission factor of AO process is 0.0078, the emission factor of AAO process is 0.002.<sup>33</sup>

The emission of N<sub>2</sub>O generated in the direct emission process were calculated in a similar way to COD, through formula (2).

$$m_{\text{N}_2\text{O}} = \frac{Q \times (\text{TN}_{\text{in}} - \text{TN}_{\text{out}})}{1000} \times \text{EF}_{\text{N}_2\text{O}} \quad (2)$$

where  $Q$  is the daily influent water of WWTP (m<sup>3</sup>); TN<sub>in</sub> is the average daily influent nitrogen concentration of the WWTP (mg L<sup>-1</sup>); TN<sub>out</sub> is the average daily effluent nitrogen concentration of WWTP (mg L<sup>-1</sup>); EF<sub>N<sub>2</sub>O</sub> is the N<sub>2</sub>O emission factor in the treatment process (kg CH<sub>4</sub>/kg COD), and the emission factor of AO process is 0.001, the emission factor of AAO process is 0.0014.<sup>33</sup>

The carbon emission from indirect emission process mainly includes the emission from chemicals and electricity consumption. It is calculated using formula (3).

$$M = \sum_{g=1}^m (f_g \times M_g) \quad (3)$$

where  $M$  is chemicals consumption of CO<sub>2</sub> emission equivalent, kg CO<sub>2</sub>;  $f_g$  the CO<sub>2</sub> emission factor of the  $g$ th commercial carbon source (kg CO<sub>2</sub>/kg), and the emission factor of GLU and NaAC is 1.6, the emission factor of PAC is 1.62, and the emission factor of PAM is 1.5;<sup>34</sup>  $M_g$  is the mass of the  $g$ th chemical used (kg).

Indirect emissions from truck transport cannot be ignored. According to the Standard for Carbon Emission Calculation of Urban Sewage Treatment and Sludge Treatment and Disposal Project (T/CABEE 040-2022) (in Chinese),<sup>35</sup> the carbon emissions generated by the transportation part are based on formula (4). It is known that the distance to transport the wastewater from the yeast plant to the WWTP is 2.6 km, and the carrying vehicle is heavy diesel truck (with a load of 30 t), each carrying 20 t wastewater, 40 times a year.

$$C_{\text{wc}} = \sum_{i=1}^n (C_i \times \text{CL}_i \times C_{\text{y}}F_i) \quad (4)$$

where  $C_{\text{wc}}$  is the WWTP average daily consumption of CO<sub>2</sub> emissions, kg CO<sub>2</sub>;  $C_i$  is the average daily consumption of material  $i$  (t per day); CL<sub>i</sub> is transportation distance of material  $i$  (km);  $C_{\text{y}}F_i$  is carbon emissions factor of transport material  $i$ , and the value of heavy diesel truck (30 t load) is 0.078 (kg CO<sub>2</sub>/km t).

Wastewater can produce CH<sub>4</sub> emissions in sewage pipe network, which are often ignored in carbon emissions accounting. And this part is calculated according to formula (5).

$$C_{\text{CH}_4} = 6 \times 10^{-5} \times 1.05^{(T-20)} \times \gamma \times \frac{A}{V} \times \text{HRT} + 0.0015 \quad (5)$$

where  $C_{\text{CH}_4}$  is the release amount of CH<sub>4</sub> per unit volume of sewage pipe network (kg CH<sub>4</sub>/m<sup>3</sup>);  $\gamma$  is the release rate relative to CH<sub>4</sub>, and the value is 5.24 × 10<sup>-5</sup> kg (m<sup>-2</sup> h<sup>-1</sup>);  $A/V$  is the surface area to volume ratio in the pipeline (m<sup>-1</sup>); HRT is the residence time of the WWTP in the sewage pipe network (h).

## 3. Results and discussion

### 3.1 Performance of the system

The effects of adding beer wastewater on the pollutant treatment efficiency of the WWTP were investigated. The treatment efficiency of COD, BOD, TP, TN, and NH<sub>4</sub><sup>+</sup>-N before and after adding beer wastewater is shown in Fig. 2. Monthly data was obtained by averaging the influent and effluent data for the whole month. The influent data of the WWTP in 2021 was the original influent data before mixing beer wastewater. As shown in Fig. 2(a), the influent COD exhibited a noticeable seasonal fluctuation, with a decrease starting in July and rising again during winter. Similarly, the influent BOD, TP, TN, and NH<sub>4</sub><sup>+</sup>-N exhibited a decreasing trend in July and began to rise during winter (Fig. 2(b)–(d)). These seasonal trends were attributed to various factors, including seasonal and holiday events, such as the Spring Festival, which affect both residents' activities and factory production. In addition, Zhang *et al.* highlighted that the influent characteristics of WWTPs in China vary depending on the region and season.<sup>36</sup>

In Fig. 2(a), the influent COD concentration before and after adding beer wastewater was 250.5 ± 37.8 (in 2017) and 218.8 ± 9.7 mg L<sup>-1</sup> (in 2021), and the effluent COD concentration was 23.2 ± 6.6 and 13.1 ± 1.4 mg L<sup>-1</sup>, reaching the average removal rate of 90.6% and 94.0%, respectively. The removal efficiency of COD is obviously improved. Of the same change, the average removal rate of BOD, TP, TN and NH<sub>4</sub><sup>+</sup>-N (Fig. 2(b)–(d)) increased from 96.6, 93.1, 70.1 and 98.2% to 98.2, 94.8, 80.9 and 99.3%. In addition, the effluent concentration of TP, TN and NH<sub>4</sub><sup>+</sup>-N decreased from 0.2 ± 0.1, 8.8 ± 2.0 and 0.5 ± 1.1 mg L<sup>-1</sup> to 0.1 ± 0.03, 5.2 ± 1.5 and 0.2 ± 0.1 mg L<sup>-1</sup>, which is an impressive improvement. Previous studies have demonstrated that carbon-rich wastewater, such as kitchen waste and agricultural food waste, can improve nitrogen and phosphorus removal.<sup>37,38</sup> In conclusion, when the beer wastewater was used as an external carbon source in the WWTP, the treatment effect is significantly improved.

### 3.2 Denitrification rate

To investigate the denitrification effect of beer wastewater as carbon source, the denitrification rates of NaAC (R1) and beer wastewater (R2) as carbon source were measured respectively,



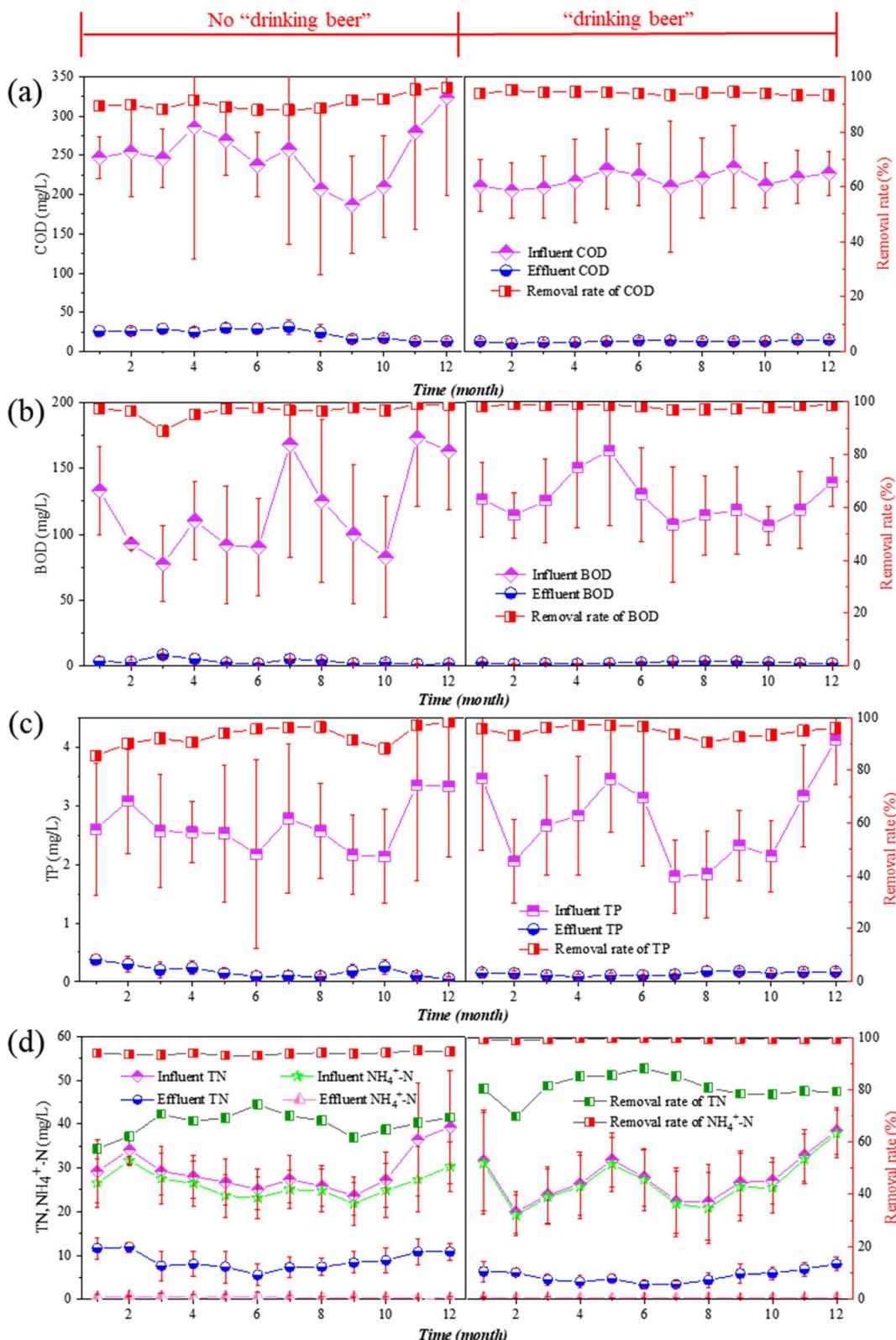


Fig. 2 The variations of (a) COD; (b) BOD; (c) TP; (d) TN and  $\text{NH}_4^+ \text{-N}$  before (2017) and after (2021) adding beer wastewater.

and the results were shown in Fig. 3. The  $\text{NO}_3^- \text{-N}$  concentration in the blank group (R3) remained stable over time, indicating that the experiment was not affected by residual carbon source

and internal carbon source, as shown in Fig. 3. Conversely, the  $\text{NO}_3^- \text{-N}$  concentration in R1 and R2 presents a linear transformation over time, and the linear fitting equation is shown in

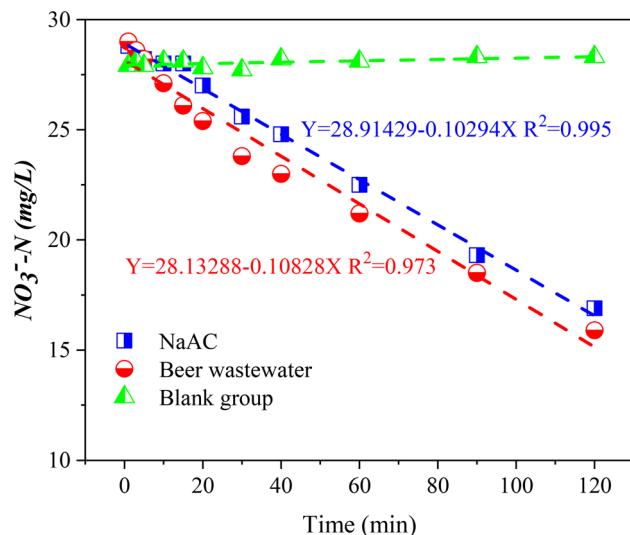


Fig. 3 Denitrification rate of activated sludge with sodium acetate and beer wastewater as carbon source.

the Fig. 3. The slope of R2 was smaller than that of R1, indicating that the  $\text{NO}_3^-$ -N degradation rate is faster when beer wastewater is used as carbon source. The denitrification rates of R1 and R2 are  $(0.072 \text{ and } 0.075 \text{ g}_{\text{NO}_3^--\text{N}}/\text{g}_{\text{MLVSS}} \text{ d})$ , respectively, after calculation. The results showed that the denitrification rate with beer wastewater as carbon source was slightly higher than that with sodium acetate as carbon source, which is consistent with previous research.<sup>39</sup> In previous studies, Ali Mahmoud *et al.* used fermentation filtrates such as oil and whey powder, methanol and acetate (control) as carbon source respectively to conduct denitrification experiments, and the results showed that the specific denitrification rates of all fermentation liquids were higher than those of methanol and acetate.<sup>40</sup> Moreover, Eunji Kim *et al.* found that food waste recycling wastewater, as an external carbon source, could conduct efficient and stable denitrification.<sup>9</sup> These studies imply that high-carbon production effluents may have higher denitrification rates than commercial carbon source. In conclusion, beer wastewater as a carbon source is superior to NaAC in denitrification rate.

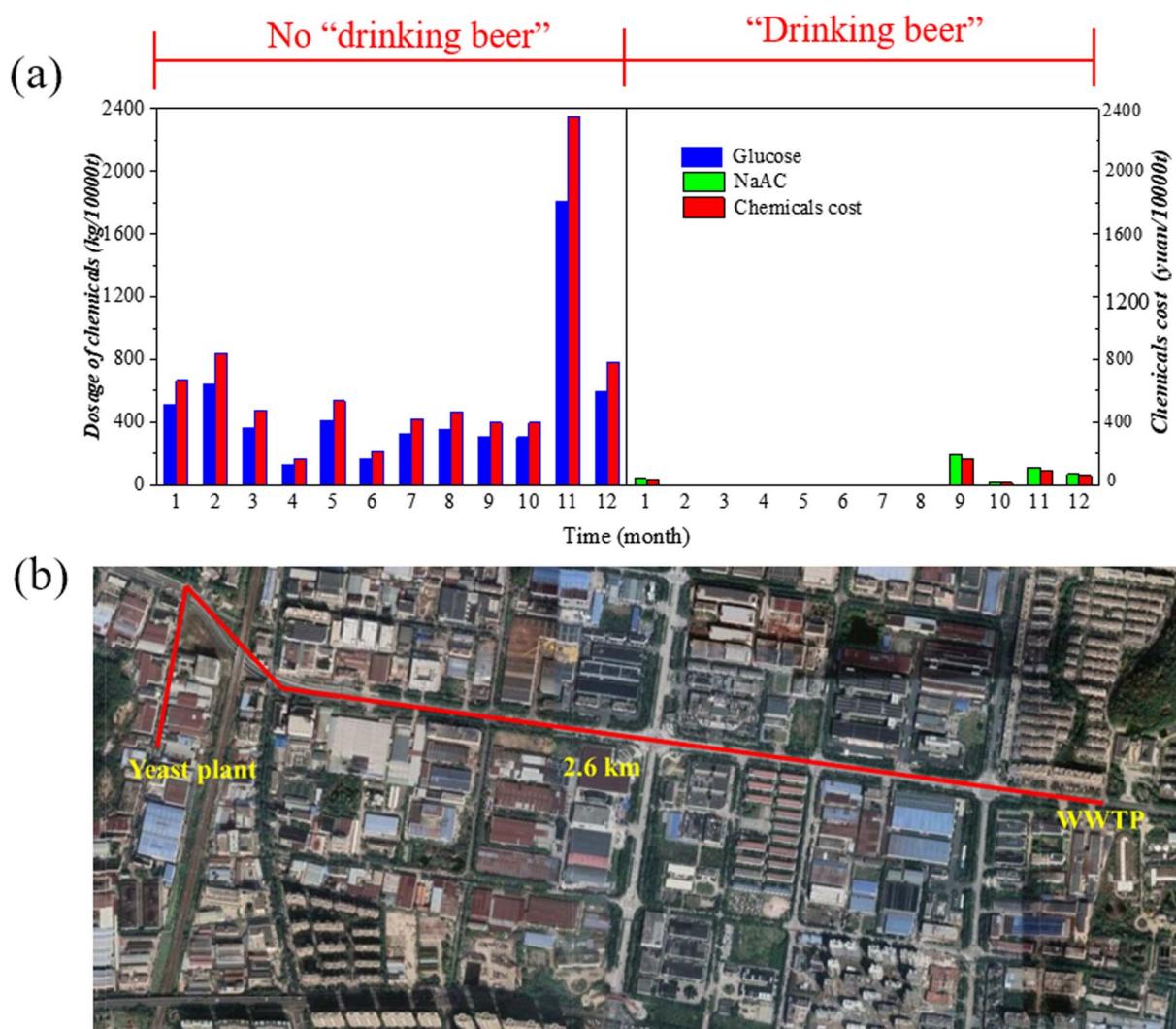


Fig. 4 Changes in costs: (a) consumption and expenditure of commercial carbon source; (b) transportation route and distance.



### 3.3 Cost of system

In order to assess the cost reduction resulting from the use of beer wastewater as a carbon source, three major factors were analysed, including the cost of commercial carbon sources at the wastewater treatment plant (WWTP), original processing cost of the yeast plant, and transportation cost of beer wastewater.

Fig. 4(a) displays the average amount and cost of external carbon source used per 10 000 tons of water treated per month before and after using beer wastewater as carbon source in the WWTP. The commercial carbon source used in the WWTP were GLU and NaAC, with GLU used before the application of beer wastewater and NaAC used in emergencies after the application of beer wastewater, mainly due to the reasons caused by the resumption of factory work after holidays or the cleaning of factory equipment. The fluctuations in chemicals usage were related to change in influent water quality. The average dosage of GLU per 10 000 tons of water treated before using beer wastewater was  $493.21 \pm 441.70$  kg, while the average amount of NaAC per 10 000 tons of water treated after using beer wastewater was  $35.68 \pm 61.32$  kg. This suggests that the amount of chemical usage significantly decreased after the application of beer wastewater as an additional carbon source.

The market price for GLU and NaAC are 1300 and 850 yuan per ton respectively. The total annual cost of carbon sources was 1 078 428 yuan before using beer wastewater, and it decreased to 48 501 yuan after using beer wastewater. Because the yeast plant and the wastewater treatment plant cooperate is a win-win situation, the yeast plant saves the cost of treating the wastewater, and the sewage plant saves the cost of buying commercial carbon sources. Therefore, the beer wastewater is provided free by the yeast plant to the wastewater plant, and the wastewater plant does not charge the yeast plant for treating the wastewater. Consequently, the commercial carbon source cost of the WWTP decreased from 641.17 yuan to 103.86 yuan per 10 000 tons of water treated, representing an 83.8% decrease, and the annual savings amounted to 1 029 927 yuan.

Fig. 4(b) illustrates the transportation route and distance of yeast plant wastewater, which is transported by truck from the

yeast plant to the WWTP. As a result, the total amount of wastewater transported by the yeast plant to the WWTP throughout the year is about 800 tons, with each transportation volume being 20 tons at a cost of 200 yuan per transportation. The total transportation cost of yeast wastewater is 8000 yuan, and the cost is 10 yuan per ton. The cost of the yeast plant's own treatment, including investment in wastewater treatment facilities and depreciation charges of 12.50 yuan per ton and running costs of 4 yuan per ton, is approximately 16.50 yuan per ton. Thus, the wastewater treatment cost of the yeast plant decreased by 6.50 yuan per ton.

In conclusion, the application of beer wastewater as a carbon source has significant economic advantages due to the reduced cost of commercial carbon sources at the WWTP and the decreased transportation cost of yeast wastewater. The total cost was reduced by 543.81 yuan, demonstrating the economic feasibility of utilizing beer wastewater as a carbon source.

### 3.4 Carbon emission

It is necessary to calculate the carbon emissions of WWTP, which can directly show the emission reduction results.<sup>41</sup> A study was conducted to assess the changes in carbon emissions before and after the use of beer wastewater as an external carbon source in the WWTP (Fig. 5).

In 2017, prior to the implementation of beer wastewater as an external carbon source, the carbon emissions included direct emissions of  $\text{CH}_4$  and  $\text{N}_2\text{O}$  from the biological wastewater treatment system (BWTS) (data on chemicals and electricity consumption in treating beer wastewater were obtained from a brewery in Qingdao, China), indirect emissions from chemical and electricity consumption,  $\text{CH}_4$  emissions from pipeline transportation of the wastewater, direct emissions of  $\text{CH}_4$  and  $\text{N}_2\text{O}$  from the WWTP, and indirect emissions from chemical and electricity consumption. In contrast, in 2021, after the implementation of beer wastewater as an external carbon source, the carbon emissions included those from trucking the beer wastewater and direct and indirect emissions from the WWTP.

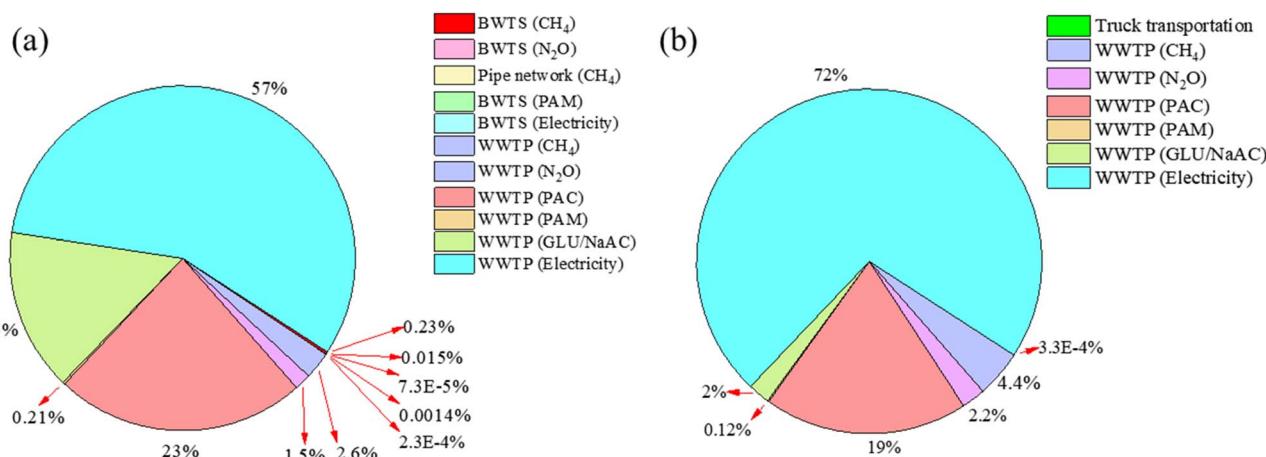


Fig. 5 Carbon emissions (a) no "drinking beer"; (b) "drinking beer".



Table 2 Comparison of carbon emission

Carbon emission classification		2017		2021	
		Annual (kg CO <sub>2</sub> )	Proportion (%)	Annual (kg CO <sub>2</sub> )	Proportion (%)
Beer wastewater treatment station	Direct	CH <sub>4</sub>	20 363.62	0.23	—
		N <sub>2</sub> O	185.08	0.0021	—
	Indirect	PAM	9.61	0.00011	—
		Electricity	1950.47	0.022	—
Pipe network	—	CH <sub>4</sub>	30.25	0.00035	—
Truck transportation	—	—	—	14.60	0.00033
Wastewater treatment plant	Direct	CH <sub>4</sub>	224 569.80	2.57	199 063.86
		N <sub>2</sub> O	134 769.77	1.54	99 622.48
	Indirect	PAC	2 048 045.00	23.47	855 651.60
		PAM	18 226.50	0.21	5362.50
		GLU/NaAC	1 327 296.00	15.21	91 296.00
Total		Electricity	4 959 441.07	56.83	3 234 500.75
			8 734 886.66		4 484 511.66

According to Table 2, the total annual carbon emissions from the BWTS and WWTP were 8734.89 t CO<sub>2</sub> in 2017. However, after the implementation of beer wastewater as an external carbon source, the total annual carbon emissions decreased to 4484.51 t CO<sub>2</sub> in 2021, which reflects a reduction of 51.3%. Notably, the total emissions decreased by 4250.38 t CO<sub>2</sub>, which was largely attributed to the reduced use of chemicals in the WWTP.<sup>5</sup> Specifically, the use of an external carbon source in the WWTP reduced the carbon emissions caused by it from 15.21% to 2.04%. This resulted in a reduction of 1236 t CO<sub>2</sub>, which accounted for 29.1% of the total reduction.

The carbon emissions from electricity consumption increased from 56.8% to 72.1% of the total carbon emissions, mainly because of the reduction in total carbon emissions. However, the total carbon emissions from electricity consumption decreased by 1 724 941 t CO<sub>2</sub>, and this was related to equipment upgrades at the WWTP. In 2017, the total carbon

emissions from the BWTS were 22 508.8 tons, primarily due to CH<sub>4</sub> emissions from the treatment process (90.5%). In contrast, in 2021, the WWTP still produced carbon emissions for beer wastewater treatment, but it reduced the use of chemicals, which greatly reduced the carbon emissions from chemical use. The increase in carbon emissions from truck transportation was only 0.0146 t CO<sub>2</sub>.

The total amount of water treated in 2017 and 2021 was 17 643 300 tons and 16 735 190 tons, respectively. This difference accounted for the higher direct carbon emissions from the WWTP in 2017 compared to those in 2021. Furthermore, it can be determined that the carbon emissions per 10 000 tons of water treated by the WWTP decreased from 4.95 t CO<sub>2</sub>/10,000 t in 2017 to 2.68 t CO<sub>2</sub>/10 000 t in 2021. This represents a reduction of 2.27 t CO<sub>2</sub>/10 000 t, or 45.8%.

In conclusion, the implementation of beer wastewater as an external carbon source in the WWTP significantly reduced the

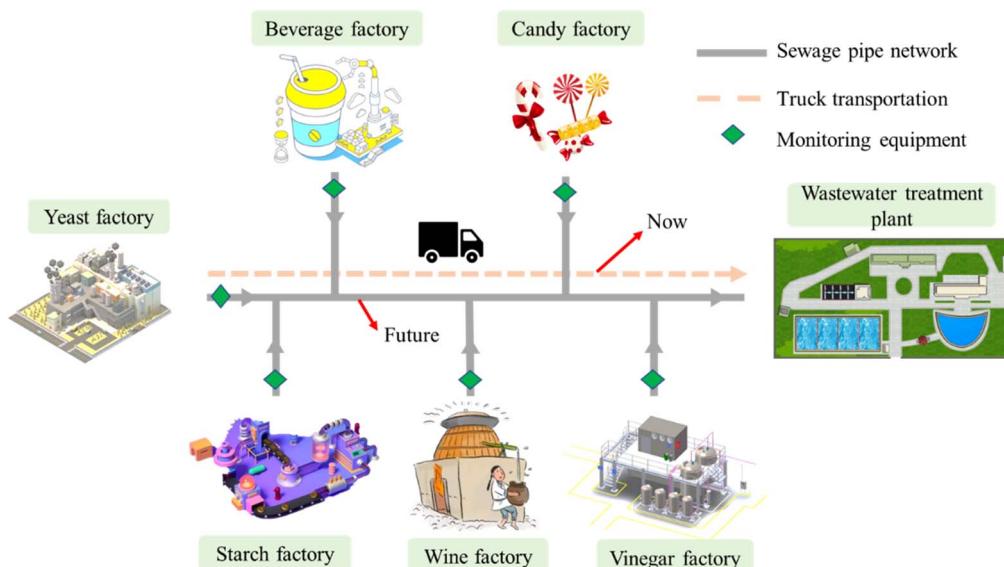


Fig. 6 Vision of the future.



use of chemicals and carbon emissions. The findings of this study suggest that this practice can serve as a promising method for reducing carbon emissions in WWTPs.

### 3.5 Vision of the future

Fig. 6 illustrates that production wastewater, including beer wastewater, can serve as an additional carbon source in WWTPs. Various types of production wastewater, such as sugar wastewater, brewing wastewater, and vinegar wastewater, have been proven to be applicable as an additional carbon source in laboratory-scale studies, as demonstrated by Fernandez-Navar *et al.*, who proved that sugar factory wastewater, beverage factory wastewater and dairy factory wastewater can be used as additional carbon source for WWTPs.<sup>28</sup> Tang *et al.* also showed that food wastewater could be used as an additional carbon source for WWTPs.<sup>37</sup> In addition, the cost of transporting beer wastewater will increase dramatically with the increase of distance, and the cheapest and most efficient solution is to use the current drainage network, which will be the future direction.

The Amendment to Discharge Standard of Pollutants for Beer Industry, recently issued by China, indicates that China is beginning to recognize the significant value of beer wastewater as an additional carbon source for WWTPs. As regulations improve, production wastewater that can be used will be discharged directly into the sewage pipe network without pretreatment and under monitored conditions, leading to an increasing availability of production wastewater for WWTPs.

## 4. Conclusions

Previous studies on using beer wastewater as an external carbon source have primarily focused on laboratory-scale experiments, with limited research on its application in actual wastewater treatment plants. Additionally, there has been little examination of the costs and carbon emissions associated with this approach.

In this study, a method of applying beer wastewater to an actual WWTP was proposed, the treatment efficiency, carbon emission, cost and denitrification rate using beer wastewater as an external carbon source are analyzed. The results showed that the treatment efficiency of COD, BOD, TN,  $\text{NH}_4^+ \text{-N}$  and TP increased by 3.4, 1.6, 10.8, 1.1 and 1.7%, respectively. Additionally, this approach reduces treatment cost and carbon emission by more than 1 million yuan and 4250.38 t  $\text{CO}_2$  per year, respectively. Furthermore, the denitrification rate of beer wastewater as carbon source is 0.075  $\text{g}_{\text{NO}_3^- \text{-N}} / \text{g}_{\text{MLVSS}}$  d, slightly faster than NaAC (0.072  $\text{g}_{\text{NO}_3^- \text{-N}} / \text{g}_{\text{MLVSS}}$  d).

In conclusion, beer wastewater has significant potential as a carbon source for wastewater treatment, leading to improved treatment efficiency and substantial economic and environmental benefits. In the future, the development and utilization of production wastewater is likely to become an important trend. Therefore, policies should be developed that implement different treatment methods for different type of wastewater, avoiding one-size-fits-all policies, in order to promote the

rational use and redistribution of resources. Such efforts will contribute to China's carbon peak and carbon-neutral goals and further reduce the costs of WWTP treatment. In addition, the effects of beer wastewater on aeration rate, excess sludge production and microbial community in WWTPs need to be further explored.

## Conflicts of interest

There are no conflicts to declare.

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