


 Cite this: *RSC Adv.*, 2023, **13**, 11472

Strategy for oxygen vacancy enriched CoMn spinel oxide catalyst activated peroxodisulfate for tetracycline degradation: process, mechanism, and toxicity analysis†

 Jingdan Gao, Yonggang Sun,* Ruijia Xiong, Yulong Ma, * Lei Wang, Song Qiao, Juan Zhang, Wenxin Ji and Yuanyuan Li

Antibiotic-like organic pollutants are harmful to aquatic ecosystems and seriously disrupt the ecological balance. Herein, we propose a simple and versatile method to prepare cobalt–manganese oxides with high specific surface area and abundant oxygen vacancies using low-temperature reduction crystallization, which greatly facilitates the adsorption and electron transfer between the catalyst, PDS, and TC, thus accelerating the degradation of tetracycline (TC). Among them, the degradation efficiency of TC in the CoMn₂O₄(C)/PDS system was 99.8% in 60 min and the degradation rate remained above 90% after four cycles. The possible degradation mechanism is also discussed, where Co is the main metal active center of the catalyst and Mn plays an auxiliary catalytic role to promote the generation of reactive radicals in PDS through redox interactions between Co and Mn, where SO₄^{•−} is the main active species for TC degradation. Finally, the possible degradation pathways of TC are proposed and the toxicity of the intermediates is evaluated. Findings from this work will shed light on the rational design of bimetallic oxide catalysts.

 Received 8th February 2023
 Accepted 29th March 2023

DOI: 10.1039/d3ra00852e

rsc.li/rsc-advances

Introduction

As one of the greatest scientific achievements of the 20th century, antibiotics play a key role in the treatment of human and animal diseases.^{1–4} Tetracycline, a typical antibiotic, ranks second in the global production and consumption of antibiotics. It is reported that annually about 210 000 tons of TC is being discharged into the aquatic environment together with wastewater during the last few decades.^{5–9} Due to the excessive and irrational use of antibiotics coupled with the fact that humans and animals can only metabolize a small percentage of tetracycline, almost most of it is excreted directly out of the body through urine. Moreover, some studies have reported that TC has been found in groundwater, surface water, and even drinking water, posing a serious threat to the environment and humans.¹⁰ Therefore, there is an urgent need to find fast, efficient and recyclable methods to remove TC from water.

To date, various methods have been developed to remove TC from water, such as adsorption,¹¹ microbial degradation,¹² membrane bioreactors,¹³ and advanced oxidation processes

(AOPs).¹⁴ Among them, AOPs can produce highly reactive oxygen species (ROS), such as sulfate (SO₄^{•−}), hydroxyl (·OH), singlet oxygen (¹O₂), and superoxide (·O₂^{•−}), which are capable of converting various pollutants, especially the kind that are difficult to degrade, into mostly harmless compounds or even completely mineralized into water, carbon dioxide, and inorganic ions.^{15–21} In recent decades, sulfate radical-based advanced oxidation processes (SR-AOPs) have been increasingly investigated for their excellent performance and prevalence in degrading emerging contaminants. SR-AOPs have many advantages: (a) the redox potential of SO₄^{•−} ($E^0 = 2.5–3.1$ V) is higher than that of ·OH ($E^0 = 1.8–2.7$ V);²² (b) SO₄^{•−} has a longer half-life ($\tau_{1/2} = 30–40$ μs) than ·OH ($\tau_{1/2} < 1$ μs);²³ (c) SO₄^{•−} can remain active over a wide pH range (2.0–8.0);²⁴ (d) SO₄^{•−} exhibits good selectivity and effectiveness due to the transfer of electrons between organic pollutants through unsaturated bonds or aromatic functional groups with π electrons.²⁵ Up to now, persulfate can be activated by various activation methods to produce SO₄^{•−}, including thermal activation,²⁶ UV light,²⁷ ultrasound,²⁸ and transition metals.²⁹ Ömür Gökkuş³⁰ reported that Ru-coated graphite is an inexpensive and effective anode material in the electrochemical oxidation treatment of tetracycline. Ledjeri *et al.*³¹ combined the electro/Fe³⁺/peroxydisulfate (PDS) process with biological treatment for the degradation of tetracycline and found that under optimal conditions, TC could be completely removed

State Key Laboratory of High-efficiency Coal Utilization and Green Chemical Engineering, School of Chemistry and Chemical Engineering, Ningxia University, Yinchuan, 750021, P. R. China. E-mail: cassyg2015@163.com; Yulongma796@sohu.com

† Electronic supplementary information (ESI) available. See DOI: <https://doi.org/10.1039/d3ra00852e>



within 40 min and the mineralization rate was 98% after 3 h of electrolysis. Wang *et al.*³² introduced Fe into nickel-based metal-organic framework materials (FeNi-MOFs) and activated PDS to degrade tetracycline under visible light irradiation. Guo *et al.*³³ prepared Fe-Co/BC catalysts for the activation of PDS to degrade TC. The high activity of Fe-Co/BC is mainly due to the synergistic effect between Fe and Co. Among them, activation using transition metals would be the simplest because it would be the most cost-effective method compared to other methods, especially those based on energy, such as electrolysis, heating, and ultrasound. In transition metal catalysts, the cobalt ion (Co^{2+}) was found to be the most efficient ion for activating PMS/PDS.³⁴ Recent reports have shown that the combination of cobalt oxides with manganese (Mn) can promote redox reactions and improve catalytic performance.^{35–37} Compared to monometallic oxides, bimetallic oxides have higher oxygen reduction activity, stability, and catalytic activity.

In this work, we have successfully prepared three catalysts, $\text{CoMn}_2\text{O}_4(\text{P})$, $\text{CoMn}_2\text{O}_4(\text{S})$, and $\text{CoMn}_2\text{O}_4(\text{C})$ for the activation of PDS to degrade TC using the reduction crystallization method for the first time. The above three catalysts were characterized by various surface analysis techniques, and the effects of reaction temperature, reaction time, and reductant concentration on the degradation of TC were systematically investigated. The possible degradation pathways of TC were inferred from the detection of intermediates by high-performance liquid chromatography-mass spectrometry (HPLC-MS). Finally, the catalytic stability of Co-Mn spinel was evaluated. Our work may provide a valuable reference for the development of more efficient multiphase catalysts for pollutant control applications.

Experimental

Materials

All chemicals used in this study were at least of analytical grade (AR). We used the following chemicals: manganese acetate tetrahydrate ($\text{Mn}(\text{CH}_3\text{COO})_2 \cdot 4\text{H}_2\text{O}$), cobalt chloride hexahydrate ($\text{CoCl}_2 \cdot 6\text{H}_2\text{O}$), potassium permanganate (KMnO_4), sodium borohydride (NaBH_4), sodium hypophosphite (NaH_2PO_2), hydrazine hydrate ($\text{N}_2\text{H}_4 \cdot \text{H}_2\text{O}$), sodium hydroxide (NaOH), methanol (MeOH), *tert*-butanol (TBA), peroxydisulfate (PDS), tetracycline (TC), and 5,5-dimethyl-1-pyrrolidine *N*-oxide (DMPO). Ultrapure water (resistivity $> 18.2 \text{ M}\Omega \text{ cm}^{-1}$) was used to prepare all solutions. All the chemicals were used as received without further purification.

Synthesis of the catalyst

In this work, $\text{CoMn}_2\text{O}_4-\delta$ was synthesized by the reduction crystallization method.

Preparation of amorphous MnO_2 . $\text{Mn}(\text{CH}_3\text{COO})_2$ (100 mL, 0.03 mol L^{-1}) was slowly added to KMnO_4 solution (50 mL, 0.04 mol L^{-1} , $\text{pH} = 12$) at room temperature, and then a brown precipitate of MnO_2 was formed under constant stirring, and the precipitate was filtered and dried overnight, and the dried solid was amorphous MnO_2 nanoparticles.

Preparation of $\text{CoMn}_2\text{O}_4-\delta$. Then in the nanocrystal $\text{CoMn}_2\text{O}_4-\delta$ synthesis, amorphous MnO_2 (0.696 g) and $\text{CoCl}_2 \cdot 6\text{H}_2\text{O}$ (0.952 g) were mixed in 20 mL of water. An excess of the ready-made NaBH_4 solution (NaBH_4 solution dissolved in NaOH solution with $\text{pH} = 11-12$) was added dropwise to the mixture under vigorous magnetic stirring and controlled temperature. The purplish-red solution immediately turned colorless and bubbling violently. The resulting precipitate was collected by centrifugation, washed repeatedly with distilled water to remove residual ions, and dried at $80 \pm 8 \text{ }^\circ\text{C}$ for 12 h. It was recorded as $\text{CoMn}_2\text{O}_4-\delta(\text{P})$. When NaH_2PO_2 and $\text{N}_2\text{H}_4 \cdot \text{H}_2\text{O}$ were used as the reducing agents, the samples were noted as $\text{CoMn}_2\text{O}_4-\delta(\text{C})$ and $\text{CoMn}_2\text{O}_4-\delta(\text{S})$, respectively, and the procedure was the same as described above.

Characterization of catalyst

The identification of the catalyst phase and crystal structure was carried out by X-ray diffraction (XRD, Bruker D8 Advance A25, Germany). The morphological details of the solid products were observed with scanning electron microscopy (SEM, ZEISS Gemini 300, Germany) and transmission electron microscopy (TEM), respectively. The specific surface area and pore structure of different catalysts were analyzed by the Brunauer-Emmett-Teller analyzer (BET, ASAP 2460, USA). Defect analysis was detected using an electron paramagnetic resonance spectrometer (EPR, Bruker A300-10/12, Germany). The chemical composition and chemical state of elements were determined by X-ray photoelectron spectroscopy (XPS, Thermo Scientific K-Alpha, USA). Finally, degradation products were analyzed by the UPLC-MS method to identify the intermediate products of TC degradation.

Experimental procedure and analysis

TC degradation experiments were conducted in 500 mL conical flasks containing 250 mL of TC solution (50 mg L^{-1}) and a certain quantity of the catalyst (0.25 g) at $30 \text{ }^\circ\text{C}$ to maintain the same reacting temperature and mixing rate. All batch experiments were implemented in an air bath shaker at 180 rpm. At a given time interval, 0.5 mL of the reaction solution was taken, and then the TC concentration was detected with a $0.22 \text{ }\mu\text{m}$ cellulose acetate membrane. The concentration of TC was analyzed by high performance liquid chromatography (HPLC, Shimadzu LC-20AT, Japan) with Agilent HC-C18 column ($5 \text{ }\mu\text{m}$, $150 \times 4.6 \text{ mm}$) at $\lambda = 356 \text{ nm}$. The mobile phase was the organic phase (acetonitrile : methanol = 2 : 1, $\nu = 0.28 \text{ mL min}^{-1}$) and the aqueous phase (0.01 M, oxalic acid, $\nu = 0.56 \text{ mL min}^{-1}$) at an isocratic flow rate of 0.84 mL min^{-1} . After a cycle of TC adsorption and degradation, the used catalyst was collected by centrifugation, washed with deionized water, and vacuum dried at $60 \text{ }^\circ\text{C}$.

Results and discussion

Characterization of catalysts

The XRD patterns of the synthesized catalysts are shown in Fig. S1.† Firstly, the strong reducing agent NaBH_4 was selected



as the reducing agent for the screening of each preparation condition, and the corresponding XRD patterns are shown in Fig. S1a–c.† Fig. S1a† shows the preparation of cobalt–manganese spinel by reduction of NaBH_4 at different temperatures, from which it can be seen that the reaction at 20 °C and 40 °C for 15 min did not form the crystalline form corresponding to CoMn_2O_4 spinel. The peaks at 18.1°, 29.3°, 30.9°, 33.3°, 36.1°, 44.2°, 58.4°, 60.9°, and 64.4° are in good agreement with the CoMn_2O_4 standard card (PDF #77-0471) and correspond to (101), (112), (200), (103), (211), (200), (321), (224) and (400) crystal planes,³⁸ indicating that the cobalt–manganese spinel, CoMn_2O_4 was successfully synthesized, and by further increasing the temperature to 80 °C it can be seen that the crystalline strength did not change significantly, laying a certain foundation for the subsequent preparation experiments. Fig. S1b and c,† respectively, show the effect of different concentrations and reaction times of NaBH_4 on the crystalline shape of spinel. It was found that the increase of reducing agent concentration did not have a significant effect on the crystalline strength of spinel; however, the crystalline shape of spinel appeared to be strengthened after 12 h of the reaction, so the subsequent preparation of spinel was performed by extending the reaction time to prepare spinel with better crystalline shape. Fig. S1d† shows the preparation of spinel by reduction with the weak reducing agent NaH_2PO_4 , and it was found that no characteristic peaks of CoMn_2O_4 were formed at different reaction times, temperatures, and reducing agent concentrations. In addition, another reductant $\text{N}_2\text{H}_4 \cdot \text{H}_2\text{O}$ was used for the preparation of spinel.

The preparation process of the catalysts is shown in Fig. 1a. Fig. 1b compares the crystalline shapes of the spinels prepared with different reducing agents, and it can be seen from the XRD that the strongest crystalline shape of the spinels formed by

$\text{N}_2\text{H}_4 \cdot \text{H}_2\text{O}$ under the same conditions, followed by NaBH_4 , and the use of NaH_2PO_4 did not show the corresponding CoMn_2O_4 spinels in the XRD patterns. Also, XRD characterization of the three different spinels was performed again after four uses and no significant change in the crystalline shape occurred (Fig. 1c).

The texture parameters including the BET surface area and pore volume of the prepared catalysts were measured from N_2 physical adsorption–desorption. The N_2 adsorption–desorption isotherms of the three catalysts were typical type IV with long and narrow hysteresis lines at relative pressures (P/P_0) of 0.6 to 1.0, indicating the mesoporous structure (Fig. 1d) and the three catalysts demonstrated H3 type hysteresis loops, indicating the presence of slit-shaped pores. The pore properties including Brunauer–Emmett–Teller (BET) specific surface area, total pore volume, and pore size are summarized in Table S1.† The BET-specific surface area was 79.40, 24.24, and 242.52 $\text{m}^2 \text{g}^{-1}$ and the pore volume was 0.248, 0.098, and 0.694 $\text{cm}^3 \text{g}^{-1}$ for $\text{CoMn}_2\text{O}_4(\text{P})$, $\text{CoMn}_2\text{O}_4(\text{S})$, and $\text{CoMn}_2\text{O}_4(\text{C})$, respectively. This is consistent with the degradation test results of tetracycline, where the larger the specific surface area and the more active sites of the catalyst, the better the degradation effect.

Fig. 1e–g shows the SEM images of $\text{CoMn}_2\text{O}_4(\text{P})$, $\text{CoMn}_2\text{O}_4(\text{S})$ and $\text{CoMn}_2\text{O}_4(\text{C})$. All three catalysts have irregular granular morphology and rough surface of the samples, indicating a high degree of defects that can act as active centers of the catalysts and improve the catalytic performance. The TEM magnification (Fig. S2†) shows that $\text{CoMn}_2\text{O}_4(\text{P})$ and $\text{CoMn}_2\text{O}_4(\text{S})$ possess the tetragonal morphology of spinel with an average size of about 50–100 nm. The TEM of $\text{CoMn}_2\text{O}_4(\text{C})$ shows a lamellar structure.³⁹

Defect characteristics

The oxygen vacancies of the three catalysts were further confirmed using an electron paramagnetic resonance spectrometer (EPR). As shown in Fig. 2a, the signal of $\text{CoMn}_2\text{O}_4(\text{C})$ was the strongest with a g factor of 2.004, indicating the

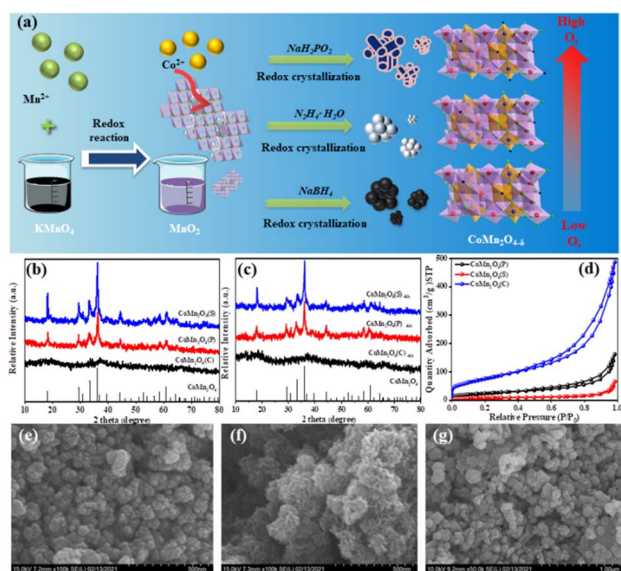


Fig. 1 (a) Schematic diagram of the catalysts preparation process. (b and c) XRD patterns of before and after catalytic oxidation. (d) N_2 isotherms adsorption–desorption curves; (e–g) SEM images of $\text{CoMn}_2\text{O}_4(\text{P})$, $\text{CoMn}_2\text{O}_4(\text{C})$ and $\text{CoMn}_2\text{O}_4(\text{S})$ catalysts.

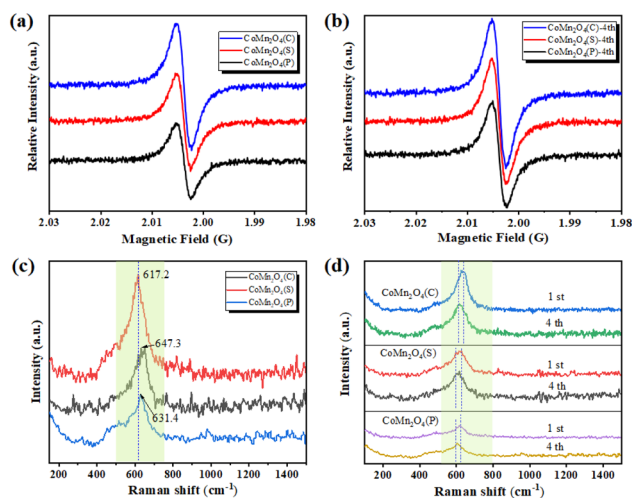


Fig. 2 (a and b) EPR and (c and d) Raman spectra of $\text{CoMn}_2\text{O}_4(\text{P})$, $\text{CoMn}_2\text{O}_4(\text{S})$, and $\text{CoMn}_2\text{O}_4(\text{C})$ before and after use.



abundant oxygen vacancies in $\text{CoMn}_2\text{O}_4(\text{C})$. Sufficient oxygen vacancies could provide more adsorption sites and active sites, exhibiting excellent catalytic performance.⁴⁰ After the catalyst was used 4th for drying, another EPR test was conducted. The test results (Fig. 2b) showed that the defects of the catalysts appeared to increase to some extent after use, which means that the crystalline shape was damaged to some extent during the use, and also this is the reason why the removal rate did not significantly lower during the cyclic experiments of tetracycline catalytic degradation, the crystalline shape was damaged, the defects increased, and the removal effect remained the same.

The Raman spectrum of $\text{CoMn}_2\text{O}_4(\text{C})$ has a significantly higher front intensity at 617.2 cm^{-1} than $\text{CoMn}_2\text{O}_4(\text{S})$ and $\text{CoMn}_2\text{O}_4(\text{P})$ with an obvious red-shift, indicating an inversion of the spinel of $\text{CoMn}_2\text{O}_4(\text{C})$, which should be due to the effect of Mn on the Co–O bond at the tetrahedral site (Fig. 2c). Furthermore, the red-shift also indicates more oxygen vacancies, which is beneficial to the activation of oxygen species and promotes catalytic performance.⁴¹ On the other hand, these phenomena can also be clarified as the simultaneous coexistence of Co and Mn cations with different valence states at the tetrahedral and octahedral sites, which facilitates the synergistic redox reaction between the redox-coupled ion pairs, thus promoting charge transfer and oxygen vacancy generation.⁴² Finally, the catalysts were subjected to another Raman test after four uses and it was found that the Raman spectra of all three catalysts were significantly red-shifted, which was consistent with the EPR results (Fig. 2d).

Surface valences and PDS activation

The full XPS survey scan spectrum of the as-prepared materials in Fig. 3 showed the existence of all elemental components (O, Co, and Mn) consistent with their chemical structures. As shown in Fig. 3c and d, O 1s peaks included two distinct oxygen components. The peak at $\sim 529\text{ eV}$ and 530 eV (marked as O_L and O_A),⁴³ ascribed to lattice oxygen in a coordinately saturated environment, surface-adsorbed oxygen species, and oxygen vacancies in the unsaturated coordination modes, respectively,⁴⁴ demonstrating the coexistence of O_A adsorbed on oxygen vacancies and O_L in the three catalysts. As shown in Tables S2 and S3,[†] the $\text{CoMn}_2\text{O}_4(\text{C})$ exhibits more adsorbed oxygen (O_A) which means it has more oxygen vacancies before and after use. The O_A/O_L ratio is consistent with the performance ranking of the catalyst, which indicates that oxygen vacancies play an important part in TCs and PDS activation. In addition, the increase in adsorbed oxygen concentration might be ascribed to the formation of Co–OH or Mn–OH groups or O_2 adsorbed on the catalyst surface and these oxygen species play a key role in PDS activation.⁴⁵

The XPS spectrum of Co 2p shows (Fig. 3e and f) that there are two different valence peaks in $\text{CoMn}_2\text{O}_4(\text{P})$, $\text{CoMn}_2\text{O}_4(\text{S})$, and $\text{CoMn}_2\text{O}_4(\text{C})$, and the corresponding valence states are Co^{2+} and Co^{3+} . As shown in Fig. 3f, Co^{2+} in all catalysts increased to some extent after use, indicating that valence conversion between metals occurred during the catalytic process, which promoted the catalytic reaction. In the XPS spectrum of Mn 2p

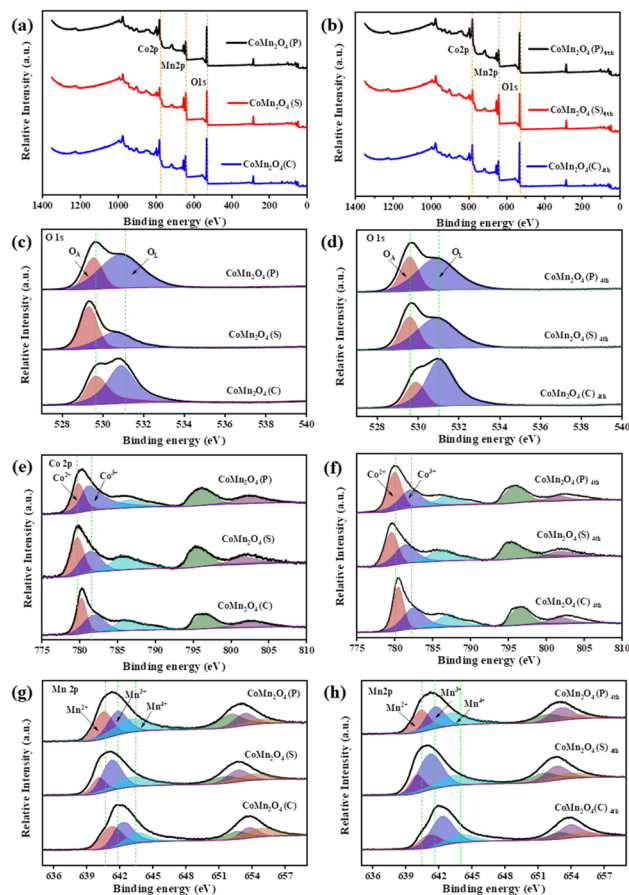
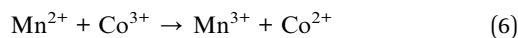
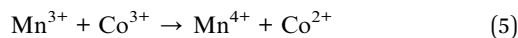
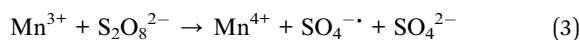
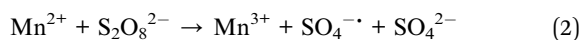
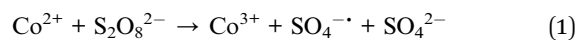


Fig. 3 XPS spectra of the synthesized catalysts before and after use: (a and b) survey spectra of the samples; (c and d) O 1s (e and f) Co 2p and (g and h) Mn 2p for $\text{CoMn}_2\text{O}_4(\text{P})$, $\text{CoMn}_2\text{O}_4(\text{S})$, $\text{CoMn}_2\text{O}_4(\text{C})$.

(Fig. 3g and h), a corresponding increase of Mn^{3+} and Mn^{4+} also occurred. However, compared with Co^{2+} , the rise of Mn^{3+} and Mn^{4+} was in a smaller range, indicating that the main metal-active neutral in the catalytic process was Co. The defects in the spinel structure are considered to be Schottky defects and occur in pairs with oxygen vacancies and cation vacancies. In addition, it has been shown that Co cations can occupy tetrahedral and octahedral positions in CoMn_2O_4 , while Mn cations are located only in octahedral positions. Therefore, it is further demonstrated that Co is the key metal for the activation of PDS.

Based on these results, a possible mechanism is proposed to effectively activate PDS through CoMn_2O_4 . It is assumed that metal ions act as Lewis sites and combine with H_2O resulting in lots of hydroxyls forming activated oxygen species on the surface of CoMn_2O_4 . Meanwhile, $\text{S}_2\text{O}_8^{2-}$ is bonded in the form of $\text{CoMn}_2\text{O}_4\text{--O--H--S}_2\text{O}_8^{2-}$ through a hydrogen bond in the solution.⁴⁶ In this case, Co^{2+} , Mn^{2+} and Mn^{3+} undergo redox reactions with $\text{S}_2\text{O}_8^{2-}$ to produce $\text{SO}_4^{\cdot-}$ (eqn (1)–(3)). $\text{SO}_4^{\cdot-}$ can be partially converted by the equation conversion to $\cdot\text{OH}$ (4). In addition, the reduction potential required for the reduction of Co^{3+} and Mn^{3+} by PDS to generate Co^{2+} and Mn^{2+} is low, so the process is thermodynamically easy to carry out as in eqn (5) and (6).





Catalytic performance

Fig. 4 shows a comparative test of the catalytic degradation of tetracycline by PDS activated by different catalysts. As shown in Fig. 4a, $\text{CoMn}_2\text{O}_4(\text{P})$, $\text{CoMn}_2\text{O}_4(\text{C})$, and $\text{CoMn}_2\text{O}_4(\text{S})$ removed no more than 20% of TC in 120 min, indicating that the degradation of TC depends mainly on catalysis rather than adsorption. $\text{CoMn}_2\text{O}_4(\text{C})/\text{PDS}$ exhibited the highest TC degradation efficiency of 99.8% within 120 min, because of strong molecular-level interactions between Co/Mn and PDS that accelerated charge transfer on the surface of $\text{CoMn}_2\text{O}_4(\text{C})$.^{47,48} Guo *et al.*⁴⁹ reported that the interplay between Co and Mn in CoMn_2O_4 resulted in increasing Mn–O covalence, accelerating electron mobility between Mn and O species, and facilitating the activation of PMS by the CoMn_2O_4 activator.

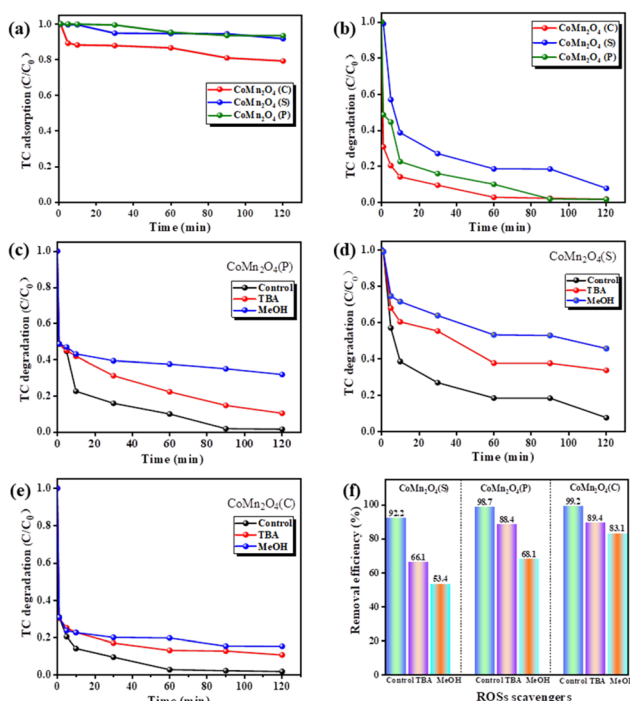


Fig. 4 The catalytic performance of various catalysts (a) adsorption, (b) degradation. (c–f) Effect of different quenchers on TC degradation in $\text{CoMn}_2\text{O}_{4-\delta}/\text{PDS}$ system. Reaction conditions: [catalyst] = 0.25 g, [PMS] = 10 mL, 0.1 mol L⁻¹, [TC] = 250 mL, 50 mg L⁻¹, [temperature] = 30 °C.

For the purpose of this experiment, TC was selected as the representative organic pollutant, and the removal rate of TC by NaBH_4 under different conditions is shown in Fig. S3a.† As shown in Fig. S3a,† the reduction preparation of spinel at 70 °C has the best degradation effect on tetracycline under four temperature conditions, which can reach 99.8%. Fig. S3b† shows that the concentration of the reducing agent during the preparation of spinel has no significant effect on the degradation effect of tetracycline, probably because the reducing agent is added in excess during the formation of spinel, so the change of concentration is not the main factor affecting the process of spinel preparation. Fig. S3c† shows the catalytic degradation test of cobalt–manganese spinel on tetracycline at different reaction times, from which it can be seen that the degradation effect decreases as the reaction time increases, especially the catalytic degradation effect of 1 mol L⁻¹ 70 °C 15 min (P) in the first ten minutes is significantly higher than that of 1 mol L⁻¹ 70 °C 12 h (P), while it can be inferred with reference to the XRD results that better is the crystal shape, worse is the catalytic degradation effect of tetracycline.

Since activation of PDS can generate both free radicals and non-free radicals, we performed quenching experiments on the above three catalysts using methanol (MeOH) and *tert*-butanol (TBA) to determine the main types of free radicals generated during PDS activation. As it is well-known, MeOH is usually used to scavenge both $\cdot\text{OH}$ and $\text{SO}_4^{\cdot-}$ due to its high reactivity for both oxidation species. Additionally, TBA mainly is used as a quenching agent for $\cdot\text{OH}$ because of its high reactivity, but not for $\text{SO}_4^{\cdot-}$ radicals.⁵⁰ The results of the quenching experiments (Fig. 4c–f) showed that the removal of tetracycline by $\text{CoMn}_2\text{O}_4(\text{S})$, $\text{CoMn}_2\text{O}_4(\text{P})$, and $\text{CoMn}_2\text{O}_4(\text{C})$ decreased to 66.1%, 88.4%, 89.4%, and 53.4%, 68.1%, 83.1% after the addition of the quenching agents *tert*-butanol (TBA) and methanol (MeOH) for the quenching of $\cdot\text{OH}$ and $\text{SO}_4^{\cdot-}$, respectively. Methanol exhibits a clear quenching effect, unlike TBA, implying that the addition of MeOH can reduce the reaction rate more than TBA, so the main reaction species for TC degradation is $\text{SO}_4^{\cdot-}$.

Stability and reusability of $\text{CoMn}_2\text{O}_{4-\delta}$

The reusability and stability of a catalyst are essential factors in determining its practical applications. Therefore, the catalytic performance of the three catalysts was investigated by four consecutive TC removal tests under identical reaction conditions. More specifically, after the first adsorption/degradation process, the used catalyst was collected by centrifugation, washed with water, and dried. After re-dispersing the sample into a fresh TC solution, a subsequent cycle was conducted. Fig. 5a–c shows four cycles of $\text{CoMn}_2\text{O}_4(\text{S})$, $\text{CoMn}_2\text{O}_4(\text{P})$, and $\text{CoMn}_2\text{O}_4(\text{C})$, and the experimental results show that the catalytic degradation of tetracycline by $\text{CoMn}_2\text{O}_4(\text{P})$ and $\text{CoMn}_2\text{O}_4(\text{C})$ showed a 5–10% decrease in the process of cycling. In contrast, $\text{CoMn}_2\text{O}_4(\text{S})$ did not show a decrease in the degradation of tetracycline after four cycles. Fig. 5d shows a summary plot of $\text{CoMn}_2\text{O}_{4-\delta}$ in four cycles with the time taken at 120 min after each cycle for the plot. In summary, it can be concluded that the stronger the crystalline shape of the cobalt–manganese



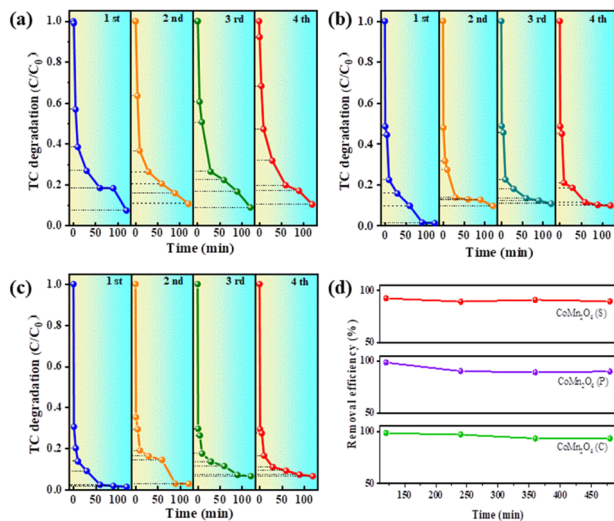


Fig. 5 Cycling experiments of tetracycline degradation by (a) $\text{CoMn}_2\text{O}_4(\text{S})$, (b) $\text{CoMn}_2\text{O}_4(\text{P})$, (c) $\text{CoMn}_2\text{O}_4(\text{C})$, and (d) $\text{CoMn}_2\text{O}_{4-\delta}$. Reaction conditions: [catalyst] = 0.25 g, [PMS] = 10 mL, 0.1 mol L^{-1} , [TC] = 250 mL, 50 mg L^{-1} , [temperature] = $30 \text{ }^\circ\text{C}$.

spinel in the activation of PDS for the degradation of tetracycline, the more stable the lattice formed between the crystalline shape of the spinel will be and it will not be easily destroyed, so it can maintain a stable catalytic activity.

Proposed degradation pathway of TC

The LC-MS technique was used to study the degradation process of TC in $\text{CoMn}_2\text{O}_4(\text{S})$, $\text{CoMn}_2\text{O}_4(\text{P})$, and $\text{CoMn}_2\text{O}_4(\text{C})$ -PDS systems. The molecular structure of TC has three functional groups, namely a double bond, an amino group, and a phenolic hydroxyl group. The LC-MS analysis of the degradation products of $\text{CoMn}_2\text{O}_4(\text{S})$, $\text{CoMn}_2\text{O}_4(\text{P})$, and $\text{CoMn}_2\text{O}_4(\text{C})$ in the catalytic degradation of tetracycline at 30 min and 120 min showed that there were some differences in the m/z of the three products at 30 min sampling and testing, but the m/z values of the reaction products corresponding to the three catalysts were identical when the reaction products at 120 min were taken for testing, and it was tentatively judged that the degradation mechanism of tetracycline by the three catalysts was the same. Fig. S4–S9† shows the mass spectra of TC degradation products there at different times, and the details of the intermediates are shown in Table S4.† A total of 9 intermediates were detected, indicating that the tetracycline molecule was degraded mainly through functional group deletion and ring-opening reactions, such as hydroxylation, dehydroxylation, demethylation, and amide bond breakage.

The oxidative degradation of TC consisted of four possible degradation pathways, as shown in Fig. 6. In pathway I, TC ($m/z = 445$) takes off an amino group to form P1 ($m/z = 397$), which in turn loses CO_2 to obtain P2 ($m/z = 354$). In pathway II, P3 ($m/z = 340(1)$) is the action of electrophilic addition, dehydroxylation, and dimethylamine on the corresponding groups on C_2 , C_3 , C_4 , and C_6 . The P4 ($m/z = 340(2)$) is formed by the removal of dimethylamine, hydroxyl, carbonyl, amino, and hydroxylation

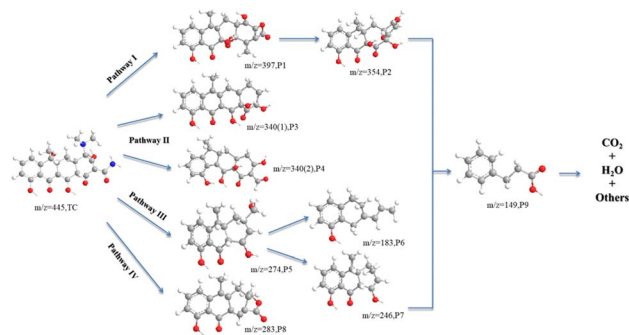


Fig. 6 Possible degradation pathways of TC in $\text{CoMn}_2\text{O}_{4-\delta}$ /PDS systems.

from tetracycline. In pathway III, the methyl group is shed due to the lower N–C bond energy of the dimethylamine at C_4 , the product 1 in C_1 is dehydrated and the methanol group in C_2 substitutes the acylamine, which in turn breaks the methanol group in C_2 and the carbon atom undergoes cleavage to produce the product with P5 ($m/z = 274$), which is further dehydroxymethylated to form the product with P7 ($m/z = 246$),⁵¹ and also undergo ring opening to form a product with P6 ($m/z = 183$). In pathway IV, P8 ($m/z = 283$) was obtained by dehydration of TC, dehydration of amide group, demethylation, and cleavage followed by cleavage of carbon atom ring and then successive dehydroxylation reactions. The intermediate product with P9 ($m/z = 149$) was seen in the analysis of all samples by LC-MS, which was the compound with the smallest m/z value detected during the degradation of tetracycline. By increasing the reaction time, oxidative decomposition and ring-opening reactions occur further, and the aromatic compounds are finally decomposed into H_2O , CO_2 , and inorganic ions.

Toxicity evaluation of intermediate products

The acute toxicity, bioaccumulation factors, developmental toxicity, and mutagenicity of TC and its degradation intermediates were evaluated using the Toxicity Evaluation Software Tool (TEST). The LD_{50} of TC in rats was 807 mg kg^{-1} , which is considered very toxic.⁴¹ As shown in Fig. 7a, the LD_{50} of most of the degradation intermediates of TC was above 1000 mg kg^{-1} , indicating that the acute toxicity was effectively controlled. However, the products P1, P2, P3, P6, and P9 were still considered “toxic”. Fig. 7b shows that the bioaccumulation factors of all intermediates increased, with the highest bioaccumulation factor for product P6. Fig. 7c shows that the developmental toxicity of TC is also significantly reduced during the oxidation process. Specifically, TC was developmentally toxic, and almost all intermediates except P8, P1, P5, and P7 had lower developmental toxicity than TC. In addition, TC was positively mutated (Fig. 7d) and all intermediate products except P4 and P1 were negatively mutated. From the calculations, the $\text{CoMn}_2\text{O}_{4-\delta}$ /PDS system can mitigate the toxicity of TC and effectively suppress environmental hazards even if some intermediates are still toxic.



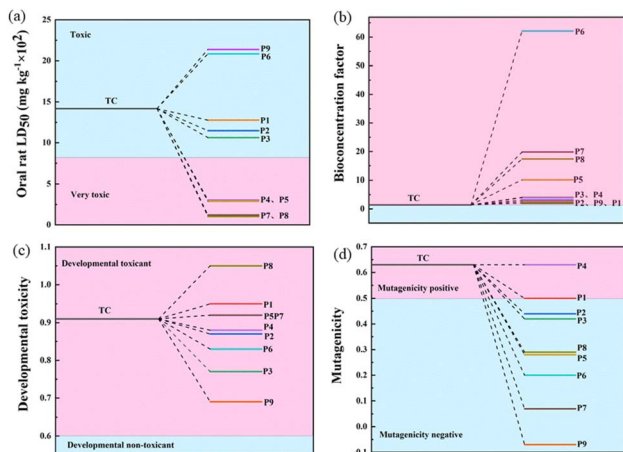


Fig. 7 Acute toxicity LD₅₀ (a), bioaccumulation factor (b), developmental toxicity (c), and mutagenicity (d) of TC and degradation intermediates.

Conclusions

In this study, we have successfully prepared CoMn₂O_{4-δ} by low-temperature reduction crystallization method, which has a high specific surface area and abundant oxygen vacancies, compared with other spinel synthesis methods; this method is energy-saving, simple, and efficient, and is an excellent activator for TC degradation by activated persulfate (PDS). The bimetallic oxide catalysts were thoroughly characterized for pertinent surface properties, and tested for the catalytic performance in PDS activation for the removal of TC in water. In TC degradation experiments, CoMn₂O₄(C) was found to exhibit good degradation and cycling stability, which was attributed to the irregular structure of CoMn₂O₄(C), thus exposing more active sites. In addition, the redox interaction between oxygen vacancies and Co-Mn promoted the generation of reactive radicals (SO₄^{-•}, •OH) by PDS, which accelerated the degradation of tetracycline. Finally, the pathway of TC degradation by CoMn₂O_{4-δ} was proposed in combination with LC-MS and toxicity assessment, and the biological toxicity was significantly reduced after the reaction. The results of this study may expand the further development of transition metal oxide catalysts for the activation of persulfates.

Author contributions

Jingdan Gao and Ruijia Xiong conducted the experiments. Lei Wang and Song Qiao edited the program and performed the data analysis. Yonggang Sun and Yulong Ma analyzed the experimental results. Juan Zhang, Wenxin Ji, and Yuanyuan Li revised the manuscript. Yonggang Sun and Yulong Ma directed the research, acquired funding, and reviewed the manuscript. All authors contributed to the revision and final discussion of the manuscript.

Conflicts of interest

The authors have no relevant financial or non-financial interests to disclose.

Acknowledgements

This work was supported by the National Natural Science Foundation of China (22006079), The West Light Talent Program of the Chinese Academy of Sciences, the Youth Talent Training Program of the Ningxia, and the Scientific and Technological Innovation Team of Industrial Water Treatment and Recycling, Ningxia.

Notes and references

- M. M. Mullis, I. M. Rambo, B. J. Baker and B. K. Reese, *Front. Microbiol.*, 2019, **10**, 2518.
- M. Kumar, S. Jaiswal, K. K. Sodhi, P. Shree, D. K. Singh, P. K. Agrawal and P. Shukla, *Environ. Int.*, 2019, **124**, 448–461.
- X. Wang, R. Yin, L. Zeng and M. Zhu, *Environ. Pollut.*, 2019, **253**, 100–110.
- M. J. F. Calvete, G. Piccirillo, C. S. Vinagreiro and M. M. Pereira, *Coord. Chem. Rev.*, 2019, **395**, 63–85.
- Y. Ben, C. Fu, M. Hu, L. Liu, M. H. Wong and C. Zheng, *Environ. Res.*, 2019, **169**, 483–493.
- F. Saadati, N. Keramati and M. M. Ghazi, *Crit. Rev. Environ. Sci. Technol.*, 2016, **46**, 757–782.
- F. Chen, Q. Yang, X. Li, G. Zeng, D. Wang, C. Niu, J. Zhao, H. An, T. Xie and Y. Deng, *Appl. Catal., B*, 2017, **200**, 330–342.
- D. Huang, X. Wang, C. Zhang, G. Zeng, Z. Peng, J. Zhou, M. Cheng, R. Wang, Z. Hu and X. Qin, *Chemosphere*, 2017, **186**, 414–421.
- X. Peng, Z. Yang, F. Hu, C. Tan, Q. Pan and H. Dai, *Sep. Purif. Technol.*, 2022, **287**, 120525.
- J. Deng, C. Ya, Y. Ge, Y. Cheng, Y. Chen, M. Xu and H. Wang, *RSC Adv.*, 2018, **8**, 2338–2349.
- V. Nguyen, T. Nguyen, C. Chen, C. Hung, T. Vo, J. Chang and C. Dong, *Bioresour. Technol.*, 2019, **284**, 197–203.
- J. Tang, M. Yang, M. Yang, J. Wang, W. Dong and G. Wang, *New J. Chem.*, 2015, **39**, 4919–4923.
- N. Prado, J. Ochoa and A. Amrane, *Bioresour. Technol.*, 2009, **100**, 3769–3774.
- W. H. M. Abdelraheem, M. N. Nadagouda and D. D. Dionysiou, *Appl. Catal., B*, 2020, **269**, 118807.
- L. Lai, J. Yan, J. Li and B. Lai, *Chem. Eng. J.*, 2018, **343**, 676–688.
- J. Rodríguez-Chueca, S. Giannakis, M. Marjanovic, M. Kohantorabi, M. R. Gholami, D. Grandjean, L. F. de Alencastro and C. Pulgarin, *Appl. Catal., B*, 2019, **248**, 62–72.
- F. Ghanbari and M. Moradi, *Chem. Eng. J.*, 2017, **310**, 41–62.
- J. Sharma, I. M. Mishra, D. D. Dionysiou and V. Kumar, *Chem. Eng. J.*, 2015, **276**, 193–204.
- C. Nie, Z. Dai, H. Meng, X. Duan, Y. Qin, Y. Zhou, Z. Ao, S. Wang and T. An, *Water Res.*, 2019, **166**, 115043.
- X. Chen, W. Wang, H. Xiao, C. Hong, F. Zhu, Y. Yao and Z. Xue, *Chem. Eng. J.*, 2012, **193–194**, 290–295.
- Q. Zhao, Q. Mao, Y. Zhou, J. Wei, X. Liu, J. Yang, L. Luo, J. Zhang, H. Chen, H. Chen and L. Tang, *Chemosphere*, 2017, **189**, 224–238.



- 22 J. Rodríguez-Chueca, C. García-Cañibano, R. J. Lepistö, Á. Encinas, J. Pellinen and J. Marugán, *J. Hazard. Mater.*, 2019, **372**, 94–102.
- 23 J. C. Espinosa, P. Manickam-Periyaraman, F. Bernat-Quesada, S. Sivanesan, M. Álvaro, H. García and S. Navalón, *Appl. Catal., B*, 2019, **249**, 42–53.
- 24 W. Li, S. Li, Y. Tang, X. Yang, W. Zhang, X. Zhang, H. Chai and Y. Huang, *J. Hazard. Mater.*, 2020, **389**, 121856.
- 25 J. Zhang, C. Zhai, W. Zhao, Y. Chen, R. Yin, L. Zeng and M. Zhu, *Chem. Eng. J.*, 2020, **397**, 125310.
- 26 Y. Qian, X. Liu, K. Li, P. Gao, J. Chen, Z. Liu, X. Zhou, Y. Zhang, H. Chen, X. Li and G. Xue, *Chem. Eng. J.*, 2020, **384**, 123332.
- 27 Y. Zhu, M. Wei, Z. Pan, L. Li, J. Liang, K. Yu and Y. Zhang, *Sci. Total Environ.*, 2020, **705**, 135960.
- 28 L. Yang, J. Xue, L. He, L. Wu, Y. Ma, H. Chen, H. Li, P. Peng and Z. Zhang, *Chem. Eng. J.*, 2019, **378**, 122146.
- 29 W. Oh, Z. Dong and T. Lim, *Appl. Catal., B*, 2016, **194**, 169–201.
- 30 I. Köktaş, Ö. Gökkuş, I. Kariper and A. Othmani, *Chemosphere*, 2023, **315**, 137758.
- 31 A. Ledjeri, I. Yahiaoui and F. Aissani-Benissad, *J. Environ. Manage.*, 2016, **184**, 249–254.
- 32 D. Wang, M. Suo, S. Lai, L. Deng, J. Liu, J. Yang, S. Chen, M. Wu and J. Zou, *Appl. Catal., B*, 2023, **321**, 122054.
- 33 L. Guo, L. Zhao, Y. Tang, J. Zhou and B. Shi, *Chem. Eng. J.*, 2023, **452**, 139381.
- 34 C. Cai, S. Kang, X. Xie, C. Liao, X. Duan and D. D. Dionysiou, *J. Hazard. Mater.*, 2020, **399**, 122979.
- 35 Y. Aoki, K. Takase, H. Kiuchi, D. Kowalski, Y. Sato, H. Toriumi, S. Kitano and H. Habazaki, *J. Am. Chem. Soc.*, 2021, **143**, 6505–6515.
- 36 A. Khan, K. Zhang, A. Taraqqi-A-Kamal, X. Wang, Y. Chen and Y. Zhang, *J. Colloid Interface Sci.*, 2021, **599**, 805–818.
- 37 N. S. Shah, J. Ali Khan, M. Sayed, Z. Ul Haq Khan, H. Sajid Ali, B. Murtaza, H. M. Khan, M. Imran and N. Muhammad, *Chem. Eng. J.*, 2019, **356**, 199–209.
- 38 Y. Wang, W. Guo and X. Li, *RSC Adv.*, 2018, **8**, 36477–36483.
- 39 C. Ma and Y. Zhang, *Sep. Purif. Technol.*, 2021, **258**, 118024.
- 40 Y. Liu, C. Wang, J. Veder, M. Saunders, M. Tade, S. Wang and Z. Shao, *J. Colloid Interface Sci.*, 2018, **530**, 556–566.
- 41 G. Li, N. Li, Y. Sun, Y. Qu, Z. Jiang, Z. Zhao, Z. Zhang, J. Cheng and Z. Hao, *Appl. Catal., B*, 2021, **282**, 119512.
- 42 W. Gu, C. Li, J. Qiu and J. Yao, *J. Alloys Compd.*, 2022, **892**, 162185.
- 43 K. Li, R. Zhang, R. Gao, G. Shen, L. Pan, Y. Yao, K. Yu, X. Zhang and J. Zou, *Appl. Catal., B*, 2019, **244**, 536–545.
- 44 H. Zhao, Z. Qu and H. Sun, *Appl. Surf. Sci.*, 2020, **529**, 147044.
- 45 Y. Sun, X. Zhang, N. Li, X. Xing, H. Yang, F. Zhang, J. Cheng, Z. Zhang and Z. Hao, *Appl. Catal., B*, 2019, **251**, 295–304.
- 46 P. Wang, J. Wang, X. An, J. Shi, W. Shangguan, X. Hao, G. Xu, B. Tang, A. Abudula and G. Guan, *Appl. Catal., B*, 2021, **282**, 119560.
- 47 Y. Wang, H. Sun, H. M. Ang, M. O. Tadé and S. Wang, *Appl. Catal., B*, 2015, **164**, 159–167.
- 48 C. Li, C. Chen, J. Lu, S. Cui, J. Li, H. Liu, W. Li and F. Zhang, *Chem. Eng. J.*, 2018, **337**, 101–109.
- 49 Z. Y. Guo, C. X. Li, M. Gao, X. Han, Y. J. Zhang, W. J. Zhang and W. W. Li, *Angew. Chem., Int. Ed.*, 2021, **60**, 2.
- 50 T. Zhang, H. Zhu and J. Croué, *Environ. Sci. Technol.*, 2013, **47**, 2784–2791.
- 51 Q. Wang, H. Zhu and B. Li, *Chem. Eng. J.*, 2019, **378**, 122072.

