RSC Advances

PAPER

Cite this: RSC Adv., 2023, 13, 7569

Received 19th December 2022 Accepted 1st March 2023

DOI: 10.1039/d2ra08089c

rsc.li/rsc-advances

1. Introduction

Zhundong coalfield, located in Xinjiang province, is the largest integrated coal field in China. Zhundong coal has the advantages of low ash content, easy ignition, and strong combustion stability.¹–⁵ Based on these high-quality characteristics of Zhundong coal, scholars have extensively studied the fields of pyrolysis, liquefaction, gasification, and combustion from different perspectives, aiming to explore the thermal reactivity of coal and its reaction mechanism.⁶⁻⁸ Meanwhile, maceral composition in the utilization of coal can play a vital role in these thermal reactivities, even affecting formulating coal–

Construction and verification of vitrinite-rich and inertinite-rich Zhundong coal models at the aggregate level: new insights from the spatial arrangement and thermal behavior perspective

Xiaoling Wang, **D** Shaoging Wang,* Yungang Zhao and Yu Liu

To explore the thermal behavior of Zhundong coal from the perspective of maceral, it is essential to conduct molecular simulations based on constructing a realistic aggregate model of coal. Here, two Zhundong coal samples ZD-V (vitrinite-rich) and ZD-I (inertinite-rich) were collected, and coal models were constructed using elemental analysis, solid-state 13 C-nuclear magnetic resonance (13 C-NMR), X-ray photoelectron spectroscopy (XPS), and Fourier transform infrared spectrometry (FTIR). The chemical formulas of 2D vitrinite-rich coal and inertinite-rich coal constructed are $C_{152}H_{167}NO_{36}$ and $C_{155}H_{119}NO_{28}$, respectively. The chemical structure information matches well with that determined by those analysis results, including elemental analysis, structural composition, and ¹³C-NMR spectra. The final aggregate models show that the dimension of the unit cell is 2.785 \times 2.785 \times 2.785 nm for ZD-V and 2.743 \times 2.743 \times 2.743 nm for ZD-I, including six macromolecules respectively. The final aggregate structure models were verified by comparing experiments and simulation results. In addition to the verification with He density, the spatial arrangement of the aggregate model was verified by simulated XRD spectrum. And moreover, the thermal behavior was verified by ReaxFF MD, and the simulated trend of thermal weight loss and cumulative total molecules released were consistent with TG-MS. The final models show the visual difference between ZD-V and ZD-I, whether the 2D molecular structure or aggregation state. ZD-V is dominated by chain hydrocarbons, while ZD-I is dominated by cyclic hydrocarbons with linked aromatic rings. The aromatic substitution of oxygen atoms is different, ZD-V is mainly composed of ortho-disubstituted arenes, and ZD-I is mainly composed of meta-disubstituted arenes. In addition, ZD-V has a lower ultra-micropore size distribution and porosity than ZD-I. This study presents a comprehensive approach to construct and verify aggregate models from the spatial arrangement and thermal behavior perspective, and the constructed Zhundong coal models can provide a foundation for further exploration of the thermal reactivity (e.g. combustion, liquefaction, etc.) of coal from maceral aspects. PAPER

Construction and verification of vitrinite-rich and
 α Cheek for undates

Construction and verification of vitrinite-rich and

inertimite-rich Zhundong coal models at the

aggregate level: new insights from the

> water slurry.^{9,10} With the continuous development of molecular simulation technology, it is urgent to construct a reasonable Zhundong coal structure model for further research.

> It is generally believed that coal model building is fundamental and critical for further molecular simulation.¹¹ In the past several decades, hundreds of coal structure models have been proposed, including the well-known models such as Given,¹² Wender,¹³ Solomon,¹⁴ and Shinn.¹⁵ Besides, Takanohashi et al.¹⁶ constructed the Upper Freeport coal model by the extract from carbon disulfide/N-methyl-2-pyrrolidinone mixed solvent, and the energy minimum stable configuration was calculated using molecular simulation technology. By comparing the simulated and experimental 13 C-NMR spectrum of different fractions, the Upper Freeport coal model was modified by Kawashima et al.¹⁷ for improving accuracy. Zhang et $al.^{18}$ used elemental analysis, high-resolution transmission

College of Geoscience and Surveying Engineering, China University of Mining and Technology (Beijing), D11, Xueyuan Road, Beijing 100083, China. E-mail: wangzq@ cumtb.edu.cn

electron microscope (HRTEM), laser desorption time-of-flight mass spectrometry (LD-TOF MS), solid state ¹³C-nuclear magnetic resonance $(^{13}C\text{-NMR})$, and X-ray photoelectron spectroscopy (XPS) techniques to obtain the molecular structural information of Chinese Xishan bituminous coal, and the first large scale Chinese bituminous coal model of diverse molecular weight and structure was constructed. Gao et al.¹⁹ proposed a strategy for constructing large and reasonable coal models manually with varied chemical structures, and constructed a multicomponent molecular model of Fugu subbituminous coal. Castro-marcano et al.²⁰ generated a large-scale molecular model of Illinois No. 6 Argonne Premium coal based on an automated construction method (including the Fringe3D protocols and the Perl scripts developed in Materials Studio), aiming to capture the continuum structure. Recently, as a combined 3-parameters about lattice fringe curvature of coal based on HRTEM, it has been applied in constructing the 3D cubic model of Qingdao petroleum coke and Fenghuangshan anthracite coal.21,22 With the widespread application of computer-aided molecular design (CAMD) techniques in coal macromolecular structure studies, more and more coal structure models will be constructed in the future to adapt to the abundance of coal types. However, the accuracy and validation of coal structure model are still emerging. RSC Advances (IRTEM), have describen uncered light Theoretics, it is necessary to construct structure nodels of
mosc is percentron (IP/TPM). Say, solid state "Crimeter" 2needed to more interpretate of moscovering the
mosc

The validation pathway of coal structure models has currently been extended from determining the chemical structure of coal to its spatial arrangement, such as bulk density, pore size distribution, pair distribution function (PDF),²³ and radial distribution function (RDF).^{24,25} The spatial arrangement of coal molecules generally depends on the microcrystalline structure.²⁶⁻²⁸ However, in most cases, the verification of microcrystalline structure in coal is often ignored because the structural parameters obtained by HRTEM or XRD are hard to match well with the model. If the XRD spectrum can be calculated from the model and then linked well with the experimental spectrum, it will be more practical. On the other hand, with availability of powerful computers and parallel computing methods, the molecular dynamics combined with ReaxFF (ReaxFF MD) provides an opportunity to explore thermal reaction process, product distribution, reaction mechanism during coal pyrolysis, which can supplement experimental studies.²⁹ ReaxFF is an empirical force field based on bond order and has the capability to simulate larger and more complex condensed systems without any pre-defined reaction pathways.³⁰⁻³² At the same time, the thermal behavior of coal is closely related to the composition and spatial arrangement of the molecular structure, and it is a promising approach to validate the models by comparing the pyrolysis simulation via ReaxFF MD with real pyrolysis experiments.

For Zhundong coal, Hong and co-works³³⁻³⁷ have done a lot of work in thermal simulation research. Although many structure models of Zhundong coal have been constructed, the verification modeling rationality is still need for further study. Meanwhile, from the petrological point of view, coal is composed of three macerals: vitrinite, inertinite and liptinite. Vitrinite and inertinite are major components of coal, which are closely related to the thermal reaction behavior of coal.

Therefore, it is necessary to construct structure models of Zhundong coal from the perspective of macerals, especially considering the high inertinite content of Zhundong coal with good liquefaction properties.^{2,38} However, most scholars ignored the maceral differences when constructing the macromolecular structure model of coal. So, in this study, two Zhundong coal structures with maceral enrichment (vitrinite and inertinite) were characterized using various testing methods. Secondly, according to the molecular structure information, the 2D and aggregate models of the two maceralenriched coals were constructed respectively. Finally, the spatial arrangement and the thermal behavior of the final models were verified to ensure the accuracy of the models.

2. Materials and methods

2.1 Sampling

The two Zhundong coal samples, ZD-V and ZD-I (obtained from vitrain and durain, respectively), were collected in Wucaiwan, Xinjiang Province. The samples were ground in a mill, and 20, 80, 200 mesh of sample were obtained to prepare coal fine polished section after drying for petrographic analysis, as used for determination of maximum vitrinite reflectance, proximate analysis and ultimate analysis, as well as various chemical structure tests, respectively. The mean maximum vitrinite reflectance (R_o) , proximate analyses, and ultimate analyses were conducted following Chinese national testing standards (GB/T 6948-2008, GB/T 212-2008 and GB/T 476-2001).

2.2 Characterizing chemical structures of coal samples

2.2.1 XRD experiment. The XRD experiment was performed with a Brucker D8 Advance X-ray diffractometer made in Germany using CuK α radiation. The start position (2 θ) was 5°, and the end position (2 θ) was 80°, with a scanning speed (ω) 4° per minute. The operating conditions of the X-ray tube are given as follows: $U = 40$ kV, $I = 40$ mA. Following the Bragg law and Scherrer formula, XRD structural parameters including interlayer spacing (d_{002}) , the average lateral size (L_a) , stacking height (L_c) , and the number of aromatic layers (N) were calculated by the eqn (1) – (4) .^{39–41}

$$
d_{002} = \lambda (2 \sin \theta_{002}) \tag{1}
$$

$$
L_{\rm c} = 0.94\lambda/(\beta_{002}\cos\theta_{002})\tag{2}
$$

$$
L_{\rm a} = 1.84\lambda/(\beta_{100}\cos\theta_{100})\tag{3}
$$

$$
N = Lc / d002
$$
 (4)

where θ (002) and θ (100) are the value of 002 and 100 peaks, respectively, λ is the wavelength for Cu radiation (1.5406 Å), and $\beta(002)$ and $\beta(100)$ are the angular widths at a half-height of 002 peak and 100 peak, respectively.

2.2.2 FTIR experiment. In this study, the Fourier Transform Infrared Spectroscopy instrument was performed by Nicolet IS10 made in America. During the sample preparation, we mixed potassium bromide (KBr) and coal samples together,

and then put the mixed coal and KBr in the mold for pressurization. After that, the sample mixed was scanned 64 times in the wavenumber range of 4000–400 cm^{-1} with a spectral resolution of 4 cm−¹ . To obtain the position and number of peaks, Origin 2018 software was used to fit the peaks of the spectrum map, and all peak shapes, peak heights, and peak areas were obtained by fitting Gaussian peaks. The parameters H_{al}/H and f_a are calculated by the following eqn $(5)-(7):^{42}$

$$
H_{\rm al}/H = H_{\rm al}/(H_{\rm al} + H_{\rm ar}) = A_{3000-2800}/(A_{3000-2800} + A_{900-700})
$$
 (5)

$$
C_{\rm al}/C = (H_{\rm al}/H \times H/C)/(H_{\rm al}/C_{\rm al})\tag{6}
$$

$$
f_{\rm a} = 1 - C_{\rm al}/C \tag{7}
$$

where $C_{\rm al}/C$ is the aliphatic carbon fraction, $H_{\rm al}/H$ is the fraction of total hydrogen present as aliphatic hydrogen, H/C is the ratio of hydrogen to carbon atoms calculated from elemental analysis, and H_{al}/C_{al} is valued as approximate 1.8 for coal.^{43,44}

The index I indicates the aromaticity and coal rank, and is calculated by eqn (8) .⁴⁵ It is usually used to reflect the relative abundance of aromatic and aliphatic functional groups.

$$
I = A_{700-900}/A_{2800-3000} \tag{8}
$$

where $A_{700-900}$ and $A_{2800-3000}$ are the integrated area of 700–900 $\,$ and 2800–3000 cm^{-1} respectively.

The degree of condensation (DOC)^{45,46} of aromatic rings can be determined as eqn (9).

$$
DOC = A_{700-900}/A_{1600}
$$
 (9)

The structural parameter of oxygen-containing functional groups, 'C', represents the changes in the ratio of $C=O$ to $C=C$ groups, is used to indicate the maturation of coal, $47,48$ which can be determined as eqn (10).

$$
{}^{c}C = A_{1650-1800} / (A_{1650-1800} + A_{1600})
$$
 (10)

The length and the degree of branching of aliphatic sidechains are calculated using the ratio of $A(CH_2)$ to $A(CH_3)$.⁴⁸ The higher value of $A(CH_2)/A(CH_3)$ indicates longer aliphatic chains of aromatic rings, while the lower value corresponds to a relatively compact structures with less space between aromatic clusters.^{43,49} The $A(CH_2)/A(CH_3)$ is estimated as:

$$
A(\text{CH}_2/\text{CH}_3) = A_{2915-2940}/A_{2950-2975} \tag{11}
$$

2.2.3 XPS experiment. The surface carbon functional bonds of the coal samples were determined by an X-ray photoelectron spectroscope (Thermo escalab 250XI, America), and the target source of the instrument was a monochromator Al (K α) (hv = 1486.6 eV). The operating power, spot diameter, voltage, and current were 150 W, 650 μ m, 14.8 kV, and 1.6 A, respectively. The wide scanning transmission was 100 eV, and the narrow scanning transmission was 20 eV. The charge calibration was conducted by using contaminated carbon C $1s = 284.8$ eV.

Then, the C 1s, O 1s, N 1s, and S 2p spectrum curves were fitted using XPSPEAK 4.1 software.

2.2.4 13° C-NMR experiment. The solid-state 13° C-nuclear magnetic resonance spectrum analysis was measured by JNM-ECZ600R (Electronics JEOL production, Japan), and the 13 C core resonance frequency was 150.913 MHz. The tube diameter is 3.2 mm, and the magic-angle spinning (MAS) frequency is 12 kHz. The relaxation delay is 2 s, and the scanning times were 2000 times.

2.2.5 TG-MS experiment. The thermogravimetric experiments were performed using a combination of a thermo plus EV2/thermo mass photo from Japan. The coal pyrolysis gas was introduced into the mass spectrometer through a capillary tube; the ionization voltage of the mass spectrometer was 40 V. The sample was raised from room temperature to 1000 °C at a heating rate of 15 °C min⁻¹. The experimental atmosphere was helium, with a flow rate of 300 mL min^{-1} . Mass spectrometry was performed under high vacuum conditions, and gas products with a mass range (relative molecular mass) of 1–200 were detected. Paper
 On 08 Advances and the multiple on the multiple of the similar paper in the similar paper in the similar paper in the similar paper in the similar state of the similar state of the similar state of the similar st

2.2.6 Helium density test. The helium density test was conducted by the volumetric method. Based on employing the electronic balance, the mass of the coal samples were obtained. By testing the volume changes of void space before and after sample put in sample cell using helium gas, the volume of the coal samples were obtained. Then, the helium density of the coal samples were calculated.

2.3 Coal molecular structure model construction methods and verification

2.3.1 2D structure model construction. Firstly, the C skeleton information in coal can be obtained based on 13 C-NMR, and the ratio of bridge carbon to peripheral carbon (X_{BP}) , a key parameter in 13 C-NMR, is used to calculate the relative content of each type of aromatic carbon. It can be assumed that the number of bridge carbons (note that it can only be an even number, and is limited by the maximum number of carbon atoms), the number of peripheral carbons and the number of aromatic rings can be obtained by using the ratio of the number of bridge carbons to X_{BP} . Therefore, the corresponding number of different carbon forms can be obtained by using 13 C-NMR parameters. Meanwhile, combined with the atomic ratio of each heteroatom to C obtained by elemental analysis, the number of other heteroatoms such as O, N, and S can be roughly obtained. The occurrence forms and quantity of heteroatom were obtained from the fitting results of XPS analysis, and FTIR results could be used to further verify some functional groups semi-quantitatively. With the aid of ACD/ GNMR software, the model was continuously adjusted until it matched the 13 C-NMR spectrum. Then, the 2D structure was determined based on the information about the structural units obtained above. Finally, the 3D configuration was obtained through geometry optimization and molecular dynamics simulation using a Dreiding force field in the Forcite module of Materials Studio software.

2.3.2 Aggregate structure model construction. To avoid overlapping of aromatic rings, the initial low bulk density of

RSC Advances **Paper** Paper **Paper Paper Paper**

0.3 g cm−³ was set during the cell construction, and six optimized molecules were put into a periodic box by the Amorphous Cell module in Materials Studio software. Then, the optimization was carried out on the compressed box by the Forcite module, and the optimized box was then annealed in the same module. The simulation detail is that the smart algorithm method, Q_{eq} charge equilibration method, Dreiding force filed, Ewald for the electrostatic and atom based for van der Waals with 12.5 Å cutoff distance were used in the geometric optimization, box-construction and annealing procedure, respectively.50,51 The optimized box with six optimized molecules were first annealed in NPT ensemble from 300 to 500 K with NHL thermostat. And then, the NVT annealing was performed on the annealed NPT structure with the lowest total potential energy, using NHL thermostat from 300 to 500 K in 300 ps.

2.3.3 Verification for 2D and aggregate structure model. The rationality of the model can be verified from two levels. The 2D model can be verified by element composition and molecular structure parameters. The aggregate model was verified from three aspects, including He density, the spatial arrangement and thermal behavior. The simulation details were as follows:

As gases with different molecular sizes can probe different void spaces in the aggregate coal model, the simulation density is calculated using helium as the probe (radius $= 0.13$ nm). Atom Volume & Surface tools in Materials Studio software were used to calculate ultra-micropores in the aggregate structure model by using the probing method.⁵² The simulated density was calculated by eqn $(12).^{25}$

$$
D_{\text{he}} = M \times 10^{21} / [(L^3 - V_{\text{he}}) \times N_A]
$$
 (12)

where $D_{\rm he}$ is the helium density, ${\rm g\,cm^3;}$ M is the molecular weight of the aggregate molecule; L is the side length of the lattice, nm; V_{he} can be calculated in the software by using helium as the probe; and N_A is the Avogadro constant, 6.02 \times 10²³.

The XRD spectrum comparison between simulation and experiment was used to verify the spatial arrangement of coal molecular. The simulated XRD spectrum was calculated in the Reflex module in Materials Studio software, and the calculation of a simulated powder pattern was performed using the current powder diffraction parameters. The detail parameters were set as follows: the analogue function was selected as Pseudo-Voigt, and the temperature factor was atomic. X-ray diffraction with Cu K α and $\lambda = 1.54056 \text{ Å}$, $2\theta = 10-80^{\circ}$ were taken into account, and the polarizability value was 0.5, $U = 30$, $V = 30$, and $W = 30$ for FWHW.

The thermal simulation was performed using ReaxFF in ADF software, which is a reactive force field based on the bond order principle, and relates the bond energy to bond lengths, valence angles and torsion angle. $53,54$ The H/C/O/N/S/B force field parameters were taken into account in this study. A Berendsen thermostat with a damping constant of 0.1 ps was used to keep the temperature in equilibrium in this thermal simulation. This initial model system was further optimized through the energy minimization method. The model system was equilibrated at 300 K for 10 ps using the NVE ensemble with a time step of 0.25 fs. The system was relaxed at 300 K using the Velocity Verlet + algorithm to avoid any reaction. To study the mass loss and product distributions of the two Zhundong coal upon heating, a heat up simulation was performed on the model system from 300 to 3000 K at rates of 20 K ps−¹ . The simulation temperature of ReaxFF-MD is much higher than the temperature range of the pyrolysis experiment, which does not mean that the ReaxFF-MD pyrolysis simulation cannot react at the experimental temperature, but the simulation time is longer at low temperatures. Due to the limitation of computing power, the simulation process often needs to be completed in nanoseconds or even picoseconds, which is much lower than the reaction time scale of the experiment. Thus, it is worth mentioning that the higher temperature (300–3000 K) used in the ReaxFF simulation is higher than that employed in the laboratory experiment to allow the reactions to occur within picoseconds. According to the Arrhenius formula, increasing the reaction temperature can significantly increase the reaction rate. Therefore, ReaxFF-MD simulation often shortens the reaction time by increasing the reaction temperature.55,56 Despite time and temperature between the simulations and experiments are different, good qualitative agreement on product distribution and chemical reaction mechanism were obtained in the literature.⁵⁷⁻⁵⁹ RSC Advances Courses Articles. The interaction and skopik something in the three on problems are computed to the interaction of the interaction o

3. Results and discussion

The petrographic analysis, mean maximum vitrinite reflectance (R_o) , proximate analyses, and ultimate analyses of samples are shown in Table 1. ZD-V has a higher vitrinite content up to 95.8%, and the vitrinite/inertinite ratio is larger than that of ZD-I obviously. Proximate analysis shows that ZD-V has a higher volatile component content and ultimate analysis shows that the carbon content for ZD-V is lower than ZD-I, while the oxygen content is higher than ZD-I.

3.1 Crystalline structure parameters

The XRD spectrum of the two coal samples used in the experiment are shown in Fig. 1. Each coal sample exist high

Table 1 The petrographic analysis, mean maximum vitrinite reflectance (R_o) , proximate analysis, and ultimate analysis of samples⁴

	Petrographic analysis, vol/%				Proximate analysis, w/%				Ultimate analysis, w_{daf} /%					
Sample	Vitrinite	Inertinite	Liptinite	V/I	$M_{\rm ad}$	$A_{\rm ad}$	V_{daf}	FC_{d}	$R_{\rm o}/\%$	C_{daf}	$H_{\rm{daf}}$	O_{daf}	$N_{\rm{daf}}$	$S_{\rm t.d.}$
ZD-V ZD-I	95.8 18.3	4.2 81.7	$\hspace{0.1mm}-\hspace{0.1mm}$	22.67 0.22	15.14 14.33	2.93 3.95	48.57 31.73	51.30 66.78	0.37 0.56	72.92 78.66	4.27 3.10	21.57 17.01	0.61 0.63	0.63 0.60

 a Note: " $-$ " is not detected.

The XRD spectrum of two coal samples (a); Gaussian fitting curve of γ and 002 peak in 2 θ range of 5–35° for ZD-V (b) and ZD-I (c).

background intensity, which indicates that the coal sample contains a certain proportion of highly disordered material in the form of amorphous carbon. Two clear peaks, 002 and 100, are located at about 26° and 47°. Compared with ZD-V, ZD-I has a sharper 002 peak and a relatively obvious 100 peak. Origin 2018 was used to perform split-peak fitting of peaks from 5 to 35° and 35 to 50°. The corresponding structural parameters such as peak position, area, half-height and width can be obtained. Taking the peaks from 5 to 35° as an example, the fitting curve of ZD-V at $5-35^{\circ}$ is shown in Fig. 1b and c, respectively, resulting in two Gaussian peaks: γ and 002. All structural parameters calculated by XRD are shown in Table 2. The microcrystalline structures of different enriched maceral of Zhundong coal are different. ZD-V has relatively larger aromatic

layers, stacking degree, and smaller spacing between aromatic layers. According to the parameter L_a/L_c value, if the coal microcrystals are regarded as multiple completed BSU units, the lateral dimension of ZD-V develops more than the longitudinal height.

3.2 FTIR data

Fig. 2 shows the FTIR spectrum of Zhundong coal with baseline correction, and the obtained subtracted spectrum can be divided into 4 absorbance bands for analyzing the functional groups in coal, that is, aromatic structures (700–900 $\rm cm^{-1}$), oxygen-containing structures (1000–1800 cm−¹), aliphatic structures (2800–3000 cm−¹) and hydroxyl structures (3000– 3600 cm−¹).46,60 It can be clearly seen that despite the different coal maceral content, all the characteristic adsorption bands are similar, suggesting that vitrinite and inertinite have similar surface structures and functional groups.⁴⁶ From the overall functional group assignment of the samples, the absorption peak (3000-3600 cm^{-1}) is relatively obvious, indicating that Zhundong coal contains more –OH functional groups. There is a sharp main peak near 1600 cm^{-1} , which is attributed to the

Fig. 2 FTIR spectrum of Zhundong coal samples.

Fig. 3 700–900 cm−¹ spectra (a), 1000–1800 cm−¹ spectra (b), 2800–3000 cm−¹ spectra (c), 3000–3600 cm−¹ spectra (d) of ZD-V; 700– 900 cm−¹ spectra (e), 1000–1800 cm−¹ spectra (f), 2800–3000 cm−¹ spectra (g), 3000–3600 cm−¹ spectra (h) of ZD-I.

aromatic nucleus (C=C), and the intensity of the C=O vibration peak at 1700 cm^{-1} is weaker. Compared with ZD-V, ZD-I has a relatively obvious absorption peak at 1700 $\mathrm{cm}^{-1},$ indicating that inertinite has relatively more $C=O$ functional groups. According to the detail information for absorption peak assignments in FTIR spectrum from the reference,⁴⁰ the 4 absorbance bands were fitted with Gaussian curves respectively (Fig. 3) to quantify the functional groups of Zhundong coals with different maceral. The corresponding structural parameters $(f_a, I, DOC, A(CH_2)/A(CH_3)$ and 'C') are calculated from the fitted peaks with eqn $(5)-(11)$ and the results are shown in Table 3. Compared with ZD-V, the aromaticity, I, DOC and 'C' of ZD-I are higher, but the degree of branching of aliphatic side-chains is lower. For the linkage between aromatic carbons, the aliphatic carbon in vitrinite rich coal will be considered to add more aliphatic side chains, while the aliphatic ring is the main one in inertinite rich coal. These results are helpful for the preliminary construction of structural model of Zhundong coal.

3.3 XPS data

The information on different chemical functional groups of the coal particles can be obtained by XPS experiment.^{61,62} According to the XPS wide-scan spectra data (Fig. 4), the surface of the Zhundong coal particles is mainly composed of carbon and oxygen atoms, followed by little nitrogen and sulfur. These

Fig. 4 XPS wide-scan spectra of the two Zhundong coals.

results are consistent with the data from elemental analysis (Table 1). Fig. 5 show the XPS C 1s, O 1s, N 1s, and S 2p scans of the two Zhundong coals. To quantify the contents of different types of functional groups, peak-fitting was performed on these XPS narrow scans. Here, Table 3 shows the peak-fitting results of C 1s, O 1s, N 1s, and S 2p scan spectrum of the two coal samples. For the results of C 1s, it can be seen that the form of three types of bonding C–C, $C = C$, and C–H occupy most of the total carbon atoms, and its content close to 70% for the two Zhundong coals. Thus, carbon atoms mainly exist in the chemical groups of aromatic rings and aliphatic chains. Apart from this, nearly 30% of total carbon atoms are bonded to oxygen atoms, where the bonding form of carbon and oxygen atoms is different. For the two Zhundong coals, the content of C–O is slightly more than that of $C=O$, which can be suggested

that the functional groups of alcohol hydroxyl, phenolic hydroxyl, or ether/both more abundant than those of carbonyl and carboxyl functional group. Compared with the ZD-V coal, the content of the carbonyl functional group $(C=0)$ in ZD-I is richer, and the content of C–O in ZD-I coal is less correspondingly. From Fig. 5 and Table 4, it can be found that nitrogen atoms in the Zhundong coals are mainly in the formation of pyrrolic nitrogen, followed by pyridinic and quaternary nitrogen. The content of pyrrolic nitrogen for ZD-V and ZD-I coal occupied 46% and 73% of the total nitrogen respectively, suggesting that pyrrole is the most abundant nitrogen of all types, which is considered to be added to the subsequent models. Although the content of sulfur atoms in the Zhundong coal is very low, it can be still detected in the existence of the following four formations: thiophenes sulfur, sulphoxides

sulfur, sulphones sulfur, and sulphates sulfur, and thiophenes sulfur is the main form existed in the two coals. Considering the proportional assignment of the overall elements, sulfur atoms will not be added to the model.

3.4 ¹³C-NMR data

The solid-state ¹³C-NMR has been proved as the most effective technique for 2D coal molecular model construction, which can get detail information about the chemical structure of coal. Referring to previous studies for the detail information of chemical shift assignments in 13 C-NMR spectrums,⁶³⁻⁶⁶ the assignments of different carbon types can be obtained. Fig. 6 shows the solid-state 13 C-NMR spectrum and its fitting curves of ZD-V and ZD-I. It was observed that there are three main

Table 4 Peak-fitting results of C 1s, O 1s, N 1s, and S 2p scan spectrum of the two Zhundong coals

Table 5 Structural parameters of the two Zhundong coals⁴

a Note: $f_{\rm a}$ – total aromatic carbon; $f_{\rm a1}$ – total aliphatic carbon; $f_{\rm a}^{\rm c}$ – carbonyl δ (chemical shift) > 165 × 10^{−6}; $f_{\rm a}^{\rm c}$ – in an aromatic ring; $f_{\rm a}^{\rm H}$ – protonated and aromatic; f_a^N – nonprotonated and aromatic; f_a^P – phenolic or phenolic; f_a^S – alkvlated aromatic; f_a^B – aromatic bridgehead; f_{a}^* – CH₃ or nonprotonated; $f_{\rm al}^{\rm H}$ – CH or CH₂; $f_{\rm al}^{\rm O}$ – bonded to oxygen.

Table 6 Types and quantities of aromatic unit structures of the two Zhundong coals

chemical regions: aliphatic carbons (0–90 ppm), aromatic carbons (90–170 ppm), and carbonyl carbons (170–220 ppm). For the two coals, the aromatic carbons are the largest

proportion of the total organic carbons, followed by aliphatic carbons and carbonyl carbons. The content distribution of the carbon types of the two coals is signicantly different, and the aliphatic carbon of ZD-V is signicantly higher than that of ZD-I. For the aromatic carbons (90–170 ppm) region, it is worth noting that in addition to the large peak at 127 ppm (indicating protonated aromatic carbons), ZD-V also contains peaks around 143 ppm and 154 ppm, both of which represent the substitution of oxygen atoms for H in the aromatic carbon. However, the substitution forms are different. The former is *ortho*-disubstituted arenes and the latter is meta-disubstituted arenes. The oxygen atoms for ZD-I is mainly composed of meta-

Fig. 7 The 2D chemical structure model of ZD-V (C₁₅₂H₁₆₇NO₃₆) and ZD-I (C₁₅₅H₁₁₉NO₂₈)

disubstituted arenes. To further quantify the different carbon types of the two samples, Origin 2018 software was used for peak-fitting, and 12 structural parameters can be calculated based on the integral peak area (Table 5). Compared with ZD-V, ZD-I has a relatively large amount of aromatic rings (64.7%) and carbonyl content (10.56%), which is consistent with the result obtained by XPS. Accordingly, ZD-I has a low content of aliphatic carbons (24.75%), especially $CH₃$ content (10.1%). Additionally, a key parameter, X_{BP} , can be calculated. It presents the ratio of aromatic bridge carbon to aromatic pericarbon $(X_{BP}$ $=f_{a}^{B}/(f_{a}^{H}+f_{a}^{P}+f_{a}^{S}),$ which was usually used to calculate the size of the aromatic clusters. According to the calculation results of the parameter X_{BP} , the X_{BP} value of ZD-I (0.182) is larger than ZD-V

(0.142). It can be suggested that inertinite has more polycondensed aromatic rings than vitrinite, and the result is consistent with XRD analysis. These structural parameters in Table 5 can provide basic information for the construction of the coal macromolecular model.

3.5 Construction and correction of the two coal molecular structure model

The construction of the coal molecular structure model is based on XPS, FTIR and ¹³C-NMR data. Among these, the formation of aromatic clusters is mainly based on the 13C-NMR data. The value of X_{BP} for the two coal is very low, and its value is between the benzene ($X_{\text{BP}} = 0$) and naphthalene ($X_{\text{BP}} = 0.25$). Thus, it

Fig. 8 Comparison between the experimental NMR spectrum and the calculated NMR spectrum based on the constructed 2D coal structure; ZD-V (a) and ZD-I (b).

Fig. 9 The aggregate structure of the two Zhundong coals in the unit cell. (a) aggregate structure; (b) ultra-micropore in aggregate structure; (c) ultra-micropore (Probe: He).

Table 7 Structural parameters of chemical structure model

Sample	Molecular formula	Molecular weight	Element content	$X_{\rm BP}$	Aromaticity
ZD-V	$C_{152}H_{167}NO_{36}$	2583.9	$C(70.65\%), H(6.51\%), N(0.54\%),$ O(22.29%)	0.148	0.612
$ZD-I$	$C_{155}H_{119}NO_{28}$	2443.6	$C(76.19\%), H(4.19\%), N(0.57\%),$ $O(18.33\%)$	0.186	0.658

Table 8 Assignment of functional groups in structure model of the two Zhundong coals

was considered that the aromatic clusters of Zhundong coal are mainly composed of benzene and naphthalene. Meanwhile, given that ACD Predictor can only calculate up to 255 carbon atoms, the number of different types of aromatic unit structures will be continuously adjusted under full alignment to make the $X_{\rm BP}$ close to 0.182 and 0.142 for ZD-V and ZD-I, respectively. Combining results from XPS data and elemental analysis, the information of N atom type in the coal molecule is estimated, and the S atom did not put in the model because of the negligible amount. Finally, the determining types and quantities of aromatic unit structures are shown in Table 6.

The next step is to analyze the type and content of aliphatic carbon based on the 13 C-NMR and FTIR data for better matching the aromatic rings in the model. The type and number of oxygen-containing functional groups in coal can be obtained by XPS data and 13 C-NMR. After that, the crosslinking forms of these species is the key to establish the 2D coal model. In the initial model of ZD-V, more aliphatic long chains will be assigned considering a higher $A(CH_2)/A(CH_3)$ value of ZD-V,

whereas ZD-I is dominated by aliphatic rings. The experimental spectrum of 13 C-NMR can be utilized to verify the connection of different species whether it is reasonable. Therefore, we need to continuously adjust the initial model by calculating the chemical shifts of the model to match the 13 C-NMR data obtained from the experiment. Finally, the 2D chemical structure of the two Zhundong coal models enriched with different maceral was established as shown in Fig. 7. The green markers show visual differences in aromatic substitution, as reflected by 13 C-NMR, and the red dashed line shows that ZD-V is dominated by chain hydrocarbons, while ZD-I is dominated by cyclic hydrocarbons with linked aromatic rings. The molecular formula of the constructed coal structure is $C_{152}H_{167}NO_{36}$ for ZD-V and $C_{155}H_{119}NO_{28}$ for ZD-I. The corresponding total molecular weight is 2584 and 2444 respectively. From Fig. 8, it can be seen that the calculated spectrum and experimental spectrum were in good agreement whether the regions of aromatic clusters or aliphatic structures. **PSC Advances**
 Table 7 Succession Published on March 2023. Downloaded in the speed of 2023. Downloaded on 10/2024
 $\frac{2}{3}$
 $\frac{$

Then, the initial 2D molecular model for the two coals were introduced into Materials Studio to calculate the threedimensional (3D) minimum energy configuration respectively, and it was obtained by performing molecular mechanics (MM) and molecular dynamics (MD) calculations using the Dreiding force field in the Forcite module. Finally, two aggregate structure models of Zhundong coal were constructed as shown in Fig. 9. The aggregate structure model for the two Zhundong coals consist of six macromolecules respectively, and the dimension of the unit cell is $2.785 \times 2.785 \times 2.785$ nm for ZD-V, and $2.743 \times 2.743 \times 2.743$ nm for ZD-I. It can also be visualized

Fig. 10 Experimental and simulated XRD spectrum of the ZD-V (a) and ZD-I (b).

from the models that ZD-I has a larger ultra-micropore size distribution and porosity compared to ZD-V (Fig. 9b and c). The construction details of the aggregate structure model can be found in the Methods section.

3.6 Verification of the two Zhundong coal models

As we all known, verifying model validity is critical for efficient model application. Here, the Zhundong coal structure models constructed with different enrichment maceral were verified by combining experiments and simulations, including its physicochemical structures, density, spatial arrangement and pyrolysis behaviors.

Fig. 11 TG-DTG plots of ZD-V and ZD-I during pyrolysis.

3.6.1 Physicochemical structure verification. Table 7 shows some of the structural parameters obtained by the model, and the elemental content of the two Zhundong coals is basically consistent with the results of elemental analysis (Table 1). The X_{BP} parameters obtained by the model are 0.148 and 0.186, respectively, which are close to the results obtained by the 13 C-NMR experiment (Table 5). Meanwhile, the aromaticity of the two models was calculated, which was 0.612 and 0.658 respectively, and the aromaticity of inertinite-rich coal (ZD-I) was higher. Although the aromaticity parameters are different from the specific values obtained by FTIR and 13 C-NMR, the maceral differences are consistent. Table 8 shows the distribution of oxygen-containing functional groups in the models, which are almost consistent with the results obtained by XPS (Table 4). Published on 08.2 Hotel on 08.2 American article of the strength commonstrate the creation of provided and the strength commonstrate of the strength commonstrate of the strength common of the strength common of the strengt

3.6.2 Density verification. According to the results of the He density experiment, the true densities of ZD-V and ZD-I are 1.40 g cm $^{-3}$ and 1.48 g cm $^{-3}$, respectively, which are close to the density values of ZD-V (1.37 g cm^{-3}) and ZD-I (1.51 g cm^{-3}) obtained by simulation calculation, respectively. ZD-I contains a large true density associated with its larger ultra-micropore size distribution and porosity. The rationality of the aggregated structure model of Zhundong coal is verified preliminarily.

3.6.3 Spatial arrangement verification. From the perspective of spatial arrangement, it is found that the simulated XRD spectrum for the two aggregate models are in good agreement with the experimental spectrum respectively (Fig. 10). In

Fig. 12 TG plots of ZD-V and ZD-I during pyrolysis experiment and pyrolysis simulation.

Fig. 13 Thermal evolution of cumulative total molecules released obtained from (a) ReaxFF MD simulations and (b) TG-MS pyrolysis experiments.

addition, the difference of the simulated XRD spectrum for ZD-V and ZD-I is significant. ZD-V has a wider 002 peak and an insignificant 100 peak compared with ZD-I, which is consistent with XRD results. These observation results also reflect the rationality of the spatial arrangement of the Zhundong coal aggregate structure model.

3.6.4 Pyrolysis behavior verification. TG is usually employed to investigate the thermogravimetric characteristics and identities of volatile components in coal pyrolysis.⁶⁷⁻⁶⁹ TG-DTG plots of two coals with different maceral content during pyrolysis are given in Fig. 11. From Fig. 11, it can be seen that the weight loss of samples increase gradually with increasing

Fig. 14 Snapshots from ReaxFF heat up MD simulations show the formative path of the first CH₄ molecule during pyrolysis for ZD-V (a and b) and ZD-I (d and e). The arrows located the broken bonds. Time evolutions of the number of CH₄ molecular fragments in ReaxFF MD for ZD-V and ZD-I (c). The stellate signs show the simulated temperature of the first CH_4 molecule released. Release curve of CH_4 gas with temperature detected using TG-MS experiment (f).

temperature, but the increasing degree is different. The thermal weight loss and weight loss rate of ZD-V are significantly larger than those of ZD-I, indicating that ZD-V has strong thermal reactivity and less thermal stability. This is mainly because ZD-V has a rich aliphatic structure and oxygen-containing functional groups, whose chemical bonds are easy to break in the pyrolysis process.⁷⁰ Fig. 12 shows the TG plots of ZD-V and ZD-I during pyrolysis experiment and pyrolysis simulation. It can be seen that the thermal weight loss trend is almost the same, especially for ZD-V. However, the weight loss of ZD-I under pyrolysis simulation is significantly less than the experimental value, and the possible reason is that the simulated environment is rapidly heating up, resulting in an incomplete reaction. This incomplete reaction is due to the poor reactivity of the aromatic skeleton and aliphatic ring. Although the temperature and time scale of the ReaxFF MD simulation are different from that of the experiment, ReaxFF MD method can still get the results similar to the experiment. As a result, this is because increasing the temperature in the ReaxFF-MD simulation has a greater effect on the reaction rate but a smaller effect on the reaction mechanism.⁷¹ Further, by simulating the thermal decomposition

progress of coal samples using ReaxFF-MD, it can be seen that a large number of aliphatic side chains and oxygen-containing functional groups in ZD-V fall off and decompose, while condensation occurs in ZD-I, which is mainly caused by the aliphatic rings.

On the other hand, ReaxFF-MD can describe the dynamic evolution of pyrolyzates during the coal pyrolysis process.⁵⁸ To examine the constructed coal model further, the simulated molecular fragments of the two Zhundong coal models were compared with that obtained from pyrolysis experiments in which the volatile species was detected using online TG-MS. As indicated in Fig. 13, the simulated evolution tendency of cumulative total molecules released shows qualitative agreement with the experimental results, although the simulation temperatures do not consistent with the experimental temperature range. The experimental and simulated results consistently show that the thermal decomposition rate of ZD-V is faster than that of ZD-I. To compare the differences of gas release from the two enriched maceral samples to further verify the rationality of the model, here, taking $CH₄$ gas generation as an example, the released behavior and the formation path of

Fig. 15 A diagram of the final detailed approach for 2D and aggregate model construction based on various experiments and simulation verification.

 $CH₄$ in the two enriched maceral samples were investigated by combining simulation and experiment. Fig. 14 shows the formation path of the first $CH₄$ molecule during pyrolysis simulation for ZD-V (a and b) and ZD-I (d and e). It can be seen that $CH₄$ is produced by methyl group at the end of the macromolecule for the two Zhundong coals. However, the detailed formation path is different. The methyl free radical shedding from ZD-V reacts with a hydrogen atom obtained from the hydroxyl group at the end of the other chain (Fig. 14a shows the broken bonds located on the hydroxyl group) to generate $CH₄$. While CH₄ generated by pyrolysis of ZD-I is *via* the reaction of the free methyl radical with a hydrogen atom on another methyl side chain group (Fig. 14d shows the specific location). Fig. 14c shows the time evolutions of the number of $CH₄$ molecular fragments in ReaxFF MD for ZD-V and ZD-I (c), and the first generated CH₄ for ZD-V and ZD-I were at 2188 K and 2416 K, respectively. In addition, ZD-V generates more $CH₄$ molecules than ZD-I in the pyrolysis simulation process. These results were in consistent with those obtained by TG-MS (Fig. 14f). RSC Advances Contribution and experience in the interval of Packet American control in the set of the creation and experiment in the set of the creation of t

3.7 Some ideas for structure model of Zhundong coal with different rich macerals

In this work, the initial structure models of different maceralrich Zhundong coals were constructed by elemental analysis, FTIR, XPS, and ¹³C-NMR. Based on molecular mechanics and molecular dynamics simulation, the optimal 3D structure was obtained. Then, the aggregate structure models for different maceral-rich Zhundong coals were established according to the Amorphous Cell module. The 2D model was verified by elemental analysis, XPS, FTIR, and ¹³C-NMR, and the aggregate models was verified between He density, XRD, TG-MS experiment and their simulations results. Fig. 15 shows the final detailed modeling construction progress. The final models will be used to explore further thermal reactions (e.g. combustion, liquefaction, etc.) and may even be useful for studying the interactions between macerals.

Through the construction of different maceral-rich coal structure models, the differences in the chemical structure of macerals are significant and can be preliminarily assessed. It is also interesting to capture these differences more deeply through the model. For instance, the maceral differences in aromatic substitution of oxygen atoms obtained by 13 C-NMR show that ZD-V is rich in ortho-disubstituted arenes, while ZD-I is rich in meta-disubstituted arenes. The differences in reactivity and quantum chemical properties on the aromatic substitution of oxygen atoms deserves to be explored. Meanwhile, the differences in the chemical structure and spatial arrangement of enriched-maceral coals will further affect their thermal behavior. In addition, the ultra-micropore structure is the key parameter in the aggregate structure of different maceral-rich coal, and its differential effect on its thermal behavior (e.g. combustion, liquefaction, etc.) deserves further investigation. Therefore, a maceral-related coal model is of great significance to the simulation of high-efficiency coal conversion process.

4. Conclusions

In this work, the Zhundong coal models of two enriched macerals (vitrinite, inertinite) were constructed respectively using elemental analysis, ¹³C-NMR, XPS, and FTIR experiment, and the models were verified by combining experiments (helium density test, XRD, and TG-MS experiment) and simulations. This study presents a comprehensive approach to construct and verify aggregate models from the spatial arrangement and thermal behavior perspective. Detailed conclusions are as follows:

The aromatic substitution of oxygen atoms for Zhundong coal with different enriched macerals is signicantly different. ZD-V is mainly composed of ortho-disubstituted arenes, and ZD-I is mainly composed of meta-disubstituted arenes. ZD-V contains more aliphatic side chains and oxygen-containing functional groups, and has a lower ultra-micropore size distribution and porosity than ZD-I. Besides, ZD-V is dominated by chain hydrocarbons, while ZD-I is dominated by cyclic hydrocarbons with linked aromatic rings. The chemical formulas of 2D vitrinite-rich coal and inertinite-rich coal constructed is $C_{152}H_{167}NO_{36}$ and $C_{155}H_{119}NO_{28}$ respectively, and the corresponding total molecular weight is 2584 and 2444 respectively.

The final aggregate model for the two Zhundong coals consists of six macromolecules respectively, and the dimension of the unit cell is $2.785 \times 2.785 \times 2.785$ nm for ZD-V, and 2.743 \times 2.743 \times 2.743 nm for ZD-I. The chemical structure of the two Zhundong coal models constructed are in good agreement with the experimental results. The spatial arrangement of the aggregate model was verified by experiment and simulation of He density and XRD, and the thermal behavior was verified by ReaxFF MD. The simulated trend of thermal weight loss and cumulative total molecules released were consistent with TG-MS. The final aggregate models can provide a basis for exploring the thermal behavior (e.g. combustion, liquefaction, etc.) of Zhundong coal at the maceral level in the future.

Conflicts of interest

There are no conflicts to declare.

Acknowledgements

The authors gratefully thank the National Natural Science Foundation of China (Research Project No. 42030807) and Key R & D Program of Ningxia Hui Autonomous Region (2021BEG02015) for financial support.

References

- 1 D. Liang, Q. Xie, Z. Wei, C. Wan, G. Li and J. Cao, J. Anal. Appl. Pyrolysis, 2019, 142, 104661.
- 2 Y. Zhao, L. Liu, P. Qiu, X. Xie, X. Chen, D. Lin and S. Sun, Fuel Process. Technol., 2017, 155, 144–152.
- 3 H. Zhang, X. Guo and Z. Zhu, Fuel, 2017, 189, 301–311.
- 4 Z. Zhang, M. Zhu, Y. Zhang, H. Y. Setyawan, J. Li and D. Zhang, Proc. Combust. Inst., 2017, 36, 2139–2146.
- 5 Q. Zhang, M. B. Zhang, S. Liu, X. Guo and C. He, Energy Policy, 1994, 22, 1075–1077.
- 6 C. Wang, L. Zhao, T. Han, W. Chen, Y. Yan, X. Jin and C. He, Energy Fuels, 2017, 32, 1242–1254.
- 7 C. A. Wang, X. Jin, Y. Wang, Y. Yan, J. Cui, Y. Liu and D. Che, Energy Fuels, 2015, 29, 78–85.
- 8 X. Li, Z. Q. Bai and W. Li, Fuel, 2018, 213, 144–149.
- 9 D. Das, S. K. Das, P. K. Parhi, A. K. Dan, S. Mishra and P. K. Misra, Energy Nexus, 2021, 4, 100025.
- 10 J. Meher, D. Das, A. K. Samal and P. K. Misra, Mater. Today: Proc., 2019, 9, 542–550.
- 11 J. P. Mathews, A. Duin and A. L. Chaffee, Fuel Process. Technol., 2011, 92, 718–728.
- 12 P. H. Given, Fuel, 1960, 39, 147–153.
- 13 I. Wender, Rev.: Sci. Eng., 1976, 14, 97–129.
- 14 P. R. Solomon, New Approaches in coal chemistry, 1981, vol. 169, pp. 61–71.
- 15 J. H. Shinn, Fuel, 1984, 63, 1187–1196.
- 16 T. Takanohashi, M. Iino and K. Nakamura, Energy Fuels, 1998, 12, 1168–1173.
- 17 H. Kawashima and T. Takanohashi, Energy Fuels, 2001, 15, 591–598.
- 18 Z. Zhang, Q. Kang, S. Wei, T. Yun, G. Yan and K. Yan, Energy Fuels, 2017, 31, 1310–1317.
- 19 M. Gao, X. Li, C. Ren, Z. Wang, Y. Pan and L. Guo, Energy Fuels, 2019, 33, 2848–2858.
- 20 F. Castro-Marcano, V. V. Lobodin, R. P. Rodgers, A. M. Mckenna, A. G. Marshall and J. P. Mathews, Fuel, 2012, 95, 35–49. Published on 08 Articles. Article on 08 C. Published on 10, 1982. Advantation and Article. Published on 2023. Download Application-Noncommercial and Access Article is licensed under a Creative Commons Attach 2023. The meth
	- 21 Y. Zhang, S. Hu, Q. Zhong, J. Zhuo and J. P. Mathews, Fuel, 2021, 295, 120616.
	- 22 Q. Zhong, Q. Mao, L. Zhang, J. Xiang, J. Xiao and J. P. Mathews, Carbon, 2018, 129, 790–802.
	- 23 S. J. Billinge and C. L. Farrow, J. Phys.: Condens. Matter, 2013, 25, 454202.
	- 24 D. Hong, L. Liu, C. Wang, T. Si and X. Guo, Fuel, 2021, 300, 120972.
	- 25 Y. Liu, S. Liu, R. Zhang and Y. Zhang, Int. J. Coal Geol., 2021, 246, 103833.
	- 26 X. Wang, S. Wang, C. Hao, Y. Zhao and X. Song, Fuel, 2022, 309, 122180.
	- 27 L. Liu, M. Du, G. Li, H. H. Schobert, J. Fan, J. Liu and Q. Wang, Fuel, 2022, 326, 124998.
	- 28 W. Li, Y. Song, W. Yang and J. P. Mathews, Fuel, 2022, 311, 122581.
	- 29 M. F. Russo Jr, R. Li, M. Mench and A. C. Van Duin, Int. J. Hydrogen Energy, 2011, 36, 5828–5835.
	- 30 M. Zheng, X. Li, J. Liu and L. Guo, Energy Fuels, 2013, 27, 2942–2951.
	- 31 M. Zheng, X. Li, J. Liu, Z. Wang, X. Gong, L. Guo and W. Song, Energy Fuels, 2014, 28, 522–534.
	- 32 F. Castro-Marcano, A. M. Kamat, M. F. Russo, A. C. T. van Duin and J. P. Mathews, Combust. Flame, 2012, 159, 1272– 1285.
	- 33 D. Hong and X. Guo, Fuel, 2017, 210, 58–66.
	- 34 T. Si, D. Hong, P. Li and X. Guo, J. Anal. Appl. Pyrolysis, 2021, 156, 105098.
- 35 D. Hong, T. Si and X. Guo, Proc. Combust. Inst., 2021, 38, 4023–4032.
- 36 D. Hong, Z. Cao and X. Guo, J. Anal. Appl. Pyrolysis, 2018, 137, 246–252.
- 37 D. Hong, T. Si, X. Li and X. Guo, Fuel Process. Technol., 2020, 199, 106305.
- 38 J. Zhou, X. Zhuang, A. Alastuey, X. Querol and J. Li, Int. J. Coal Geol., 2010, 82, 51–67.
- 39 M. J. Roberts, R. C. Everson, H. W. J. P. Neomagus, D. Van Niekerk, J. P. Mathews and D. J. Branken, Fuel, 2015, 142, 9–20.
- 40 R. C. Everson, G. N. Okolo, H. W. J. P. Neomagus and J. Dos Santos, Fuel, 2013, 109, 148–156.
- 41 H. Takagi, K. Maruyama, N. Yoshizawa, Y. Yamada and Y. Sato, Fuel, 2004, 83, 2427–2433.
- 42 D. Wu, G. Liu, R. Sun and X. Fan, Energy Fuels, 2013, 27, 5823–5830.
- 43 J. Ibarra, R. Moliner and A. J. Bonet, Fuel, 1994, 73, 918–924.
- 44 J. A. Orrego-Ruiz, R. Cabanzo and E. Mejía-Ospino, Int. J. Coal Geol., 2011, 85, 307–310.
- 45 Y. Guo and R. M. Bustin, Int. J. Coal Geol., 1998, 36, 259–275.
- 46 S. Wang, Y. Tang, H. H. Schobert, Y. Guo and Y. Su, Energy Fuels, 2011, 25, 5672–5677.
- 47 Y. Chen, M. Mastalerz and A. Schimmelmann, Int. J. Coal Geol., 2012, 104, 22–33.
- 48 X. He, X. Liu, B. Nie and D. Song, Fuel, 2017, 206, 555–563.
- 49 D. W. Van Krevelen, Coal: Typology-Physics-Chemistry-Constitution, 1993.
- 50 Z. Zhang, L. Guo, H. Zhang and J. Zhan, Int. J. Hydrogen Energy, 2019, 44, 25335–25346.
- 51 Y. Zhao, S. Wang, Y. Liu, X. Song, H. Chen, X. Zhang, Y. Lin and X. Wang, Energy Fuels, 2021, 35, 15663–15674.
- 52 Y. Liu, Y. Zhu, W. Li, C. Zhang and Y. Wang, Fuel, 2017, 210, 298–306.
- 53 K. Chenoweth, A. Duin and W. A. Goddard, J. Phys. Chem. A, 2008, 112, 1040–1053.
- 54 B. Sanjukta, T. Banerjee and K. Mohanty, Fuel, 2014, 136, 326–333.
- 55 Z. Zhou, L. Guo, L. Chen, S. Shan and Z. Wang, Int. J. Energy Res., 2018, 42, 2465–2480.
- 56 L. Guo, Z. Zhou, L. Chen, S. Shan and Z. Wang, J. Mol. Model., 2019, 25, 174.
- 57 E. Salmon, A. Duin, F. Lorant, P. M. Marquaire and W. A. Goddard III, Org. Geochem., 2009, 40, 1195–1209.
- 58 M. Zheng, X. Li, F. Nie and L. Guo, Energy Fuels, 2017, 31, 3675–3683.
- 59 F. Castro-Marcano, M. F. Russo, A. C. T. van Duin and J. P. Mathews, J. Anal. Appl. Pyrolysis, 2014, 109, 79–89.
- 60 J. V. Ibarra, E. Munoz, R. Moliner, C. Largeau and J. I. Hedges, Org. Geochem., 1996, 24, 725–735.
- 61 B. Wu, H. Hu, Y. Zhao, L. Jin and Y. Fang, J. Fuel Chem. Technol., 2009, 37, 385–392.
- 62 T. Grzybek, R. Pietrzak and H. Wachowska, Fuel Process. Technol., 2002, 77–78, 1–7.
- 63 G. Almendros, H. Knicker and F. J. González-Vila, Org. Geochem., 2003, 34, 1559–1568.
- 64 B. Erdenetsogt, I. Lee, S. K. Lee, Y. Ko and D. Bat-Erdene, Int. J. Coal Geol., 2010, 82, 37–44.
- 65 G. Gong, X. Yuan, Y. Zhang, Y. Li, W. Liu, M. Wang, Y. Zhao and L. Xu, RSC Adv., 2020, 10, 5468–5477.
- 66 F. Xu, S. Pan, C. Liu, D. Zhao, H. Liu, Q. Wang and Y. Liu, RSC Adv., 2017, 7, 41512–41519.
- 67 C. Zou, C. Ma, J. Zhao, R. Shi and X. Li, J. Anal. Appl. Pyrolysis, 2017, 127, 309–320.
- 68 M. Wang, Z. Li, W. Huang, J. Yang and H. Xue, Fuel, 2015, 156, 243–253.
- 69 F. Han, A. Meng, Q. Li and Y. Zhang, J. Energy Inst., 2016, 89, 94–100.
- 70 J. Wang, J. Du, L. Chang and K. Xie, Fuel Process. Technol., 2010, 91, 430–433.
- 71 X. Cheng, Q. Wang, J. Li, J. Wang and X. Li, J. Phys. Chem. A, 2012, 116, 9811–9818.