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# An electrochemical method for measuring magnetic flux density

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A magneto-electrochemical method is designed and validated for measuring magnetic flux density. This method is based on the correlation of the change of open circuit potential to the flux density of an applied magnetic field. Electrochemical systems with iron in ferric solutions are selected for demonstrating the validity of the proposed methods. Magnetic flux density can be measured with this method by voltmeter without using a Tesla meter.

## 1. Introduction

Magnetism has been studied and explored for a long time.<sup>1–3</sup> In 1600, Gilbert's book "De Magnete" initiated magnetism as a scientific academic field. In the early 19th century, a series of milestone discoveries led to the formation of the modern magnetic theory. In the 1860s, Maxwell integrated the equations of classical electricity and magnetism to Maxwell's equations, and developed Maxwell's electromagnetic field theory that unified electrical, magnetic, and optical theories. From the concepts of physics, the field that transfers the magnetic force between objects is considered as the definition of the magnetic field. Magnetic fields are reflected in all aspects of the world and life, and have been found in various applications such as large-scale entertainment and leisure equipment, traffic workpieces, aerospace workpieces, medical equipment and other undertakings.<sup>4</sup> Magnetic flux density (MFD, represented by symbol  $B$ ) is one of the important parameters for the quantitative characterization of magnetic field. The measurement of MFD is crucial for scientific research and engineering applications. There are many physical-based methods for measuring MFD, such as the rotating and vibrating coils and the fluxmetric method including flux meter coils, the flux-ball, the ballistic galvanometer, and electronic integrators.<sup>5,6</sup> The measurements of magnetic flux density (MFD) are based on some principles such as Faraday's law of electromagnetic induction, Hall effect, magnetoresistance effect, magnetic resonance, magneto-optic Kerr effect, magnetostrictive effect, magnetic quantum tunneling effect, and superconductivity effect.<sup>5</sup> Based on these theories and methods, many devices and equipment have been developed to measure MFD.

Representing all instruments for measuring MFD, magnetometers can be divided into two main types, one type for time-

independent magnetic field such as constant magnetic field and the other type for time-dependent magnetic field such as alternating magnetic field. According to the principles, magnetometers for constant magnetic field<sup>7–11</sup> include fluxgate magnetometer, Hall sensor, anisotropic magneto-resistive sensor (AMR), giant magneto impedance (GMI), nuclear magnetic resonance field meter, *etc.* Magnetometers for measuring alternating magnetic field<sup>12–16</sup> include the superconducting quantum interference device (SQUID), induction coil magnetometer, *etc.* These magnetometers mentioned above have their advantages and some limitations.

Fluxgate magnetometer is designed based on the Faraday's law of electromagnetic induction and has the characteristics of simple, small, low power consumption, high sensitivity with the target magnetic field ranging from 1 pT to 10 nT. Generally, the volume of fluxgate magnetometer is large and its response speed is slow. Fluxgate magnetometer is suitable for measuring constant magnetic field or slowly changing weak magnetic field. It has been widely used for industrial detection, geomagnetic measurement, navigation system, military engineering.<sup>17,18</sup> Hall sensor is small and has fast response speed but has low sensitivity.<sup>19–22</sup> AMR has the advantages of noncontact operation, easy maintenance, and robustness to contamination<sup>23,24</sup> and they are much more sensitive than any semiconductor sensor,<sup>25</sup> which is usually used to measure MFD of 0.2 mT to 2.5 mT. SQUID uses the principle of Josephson effect to measure the magnetic field. SQUID has been used for measuring alternating magnetic field with high sensitivity *via* its response to the change of MFD. SQUID has been widely used in scanning SQUID microscopy, medical diagnostics and quantum computing.<sup>26–28</sup>

These methods for measurement of magnetic flux density require Gauss meter, thus it is more complex for measuring the MFD than potential. If there is method to measure the MFD by potentiometer, it will make the measurement for MFD more convenient and can be applied to more fields.

The electrochemical parameters in the electrochemical system are influenced by the magnetic field and a lot of research

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has been studied widely before, likely the open circuit potential of iron or other metals in aqueous solutions would shift under magnetic field.<sup>29–35</sup> Due to the modulation of magnetic field on electrode kinetics, mass transport, and deposition morphologies, its effects on electrochemical reactions have been formulated by five external forces acting on active substances, namely magnetic gradient force, Lorentz force, paramagnetic force, magnetic damping force and electrokinetic shear stress.<sup>35</sup> Among them, magnetohydrodynamic (MHD) effect<sup>36–39</sup> and magnetic field gradient force effect (MFGF)<sup>36,40,41</sup> have been used to interpret the mechanism of the influence of magnetic field on electrochemical behaviors of corrodible metals in aqueous solutions. Some electrochemical parameters of a specific electrochemical system will be affected by the MFD and these effects are related to MFD. For instance, Lu *et al.* studied the relationship of the magnetic field with the open circuit potential as well as the cathodic diffusion current and gave relevant electrochemical kinetics explanations.<sup>32</sup> These works enlighten us on the possibility of obtaining a standard curve by designing a suitable system and measuring the changes of specific electrochemical parameters to MFD of the applied magnetic fields. Then, the unknown MFD can be obtained by the measured changes of the electrochemical parameter based on the standard curves.

Based on the magneto-electrochemical theory and the previous experimental investigation on the effect of magnetic field on corrosion behavior of iron in various corrosive solutions,<sup>29–33</sup> an electrochemical method is designed and

validated here for measuring MFD by correlating the change of open circuit potential to the magnitude of MFD, which is defines as  $\Delta E_{\text{MFD}}$ , as shown in eqn (1). The motivation of this design is to establish a novel and convenient method to measure magnetic flux density using a voltmeter instead of a Tesla meter. This method is inspired by the previous research results on the magnetic field effect on electrochemical corrosion: the open circuit potential of iron in the solutions containing ionic cathodic depolarizers shifts significantly in the noble direction after the application of magnetic field, and the value of the potential shift increases with the increase of magnetic flux density. According to the reverse thinking, if the correlation standard curve between the potential shift of iron and the magnetic flux density of the applied magnetic field is established, then the numerical value of the magnetic flux density can be determined by measuring the change of the open circuit potential of iron caused by any magnetic flux density. This test does not require magnetic measurements, and only potential measurements are necessary.

$$\Delta E_{\text{MFD}} = E_{\text{corr,MFD}} - E_{\text{corr,0T}} \quad (1)$$

where  $E_{\text{corr,0T}}$  represents the open circuit potential under 0 T and  $E_{\text{corr,MFD}}$  under a specific MFD.

The schematic diagram is shown in Fig. 1. During the electrochemical test, the electrochemical sample and the magnetic field are placed vertically and horizontally respectively. The direction of MFD is parallel to the working surface of sample. The values of  $\Delta E_{\text{MFD}}$  after applying magnetic field at various flux

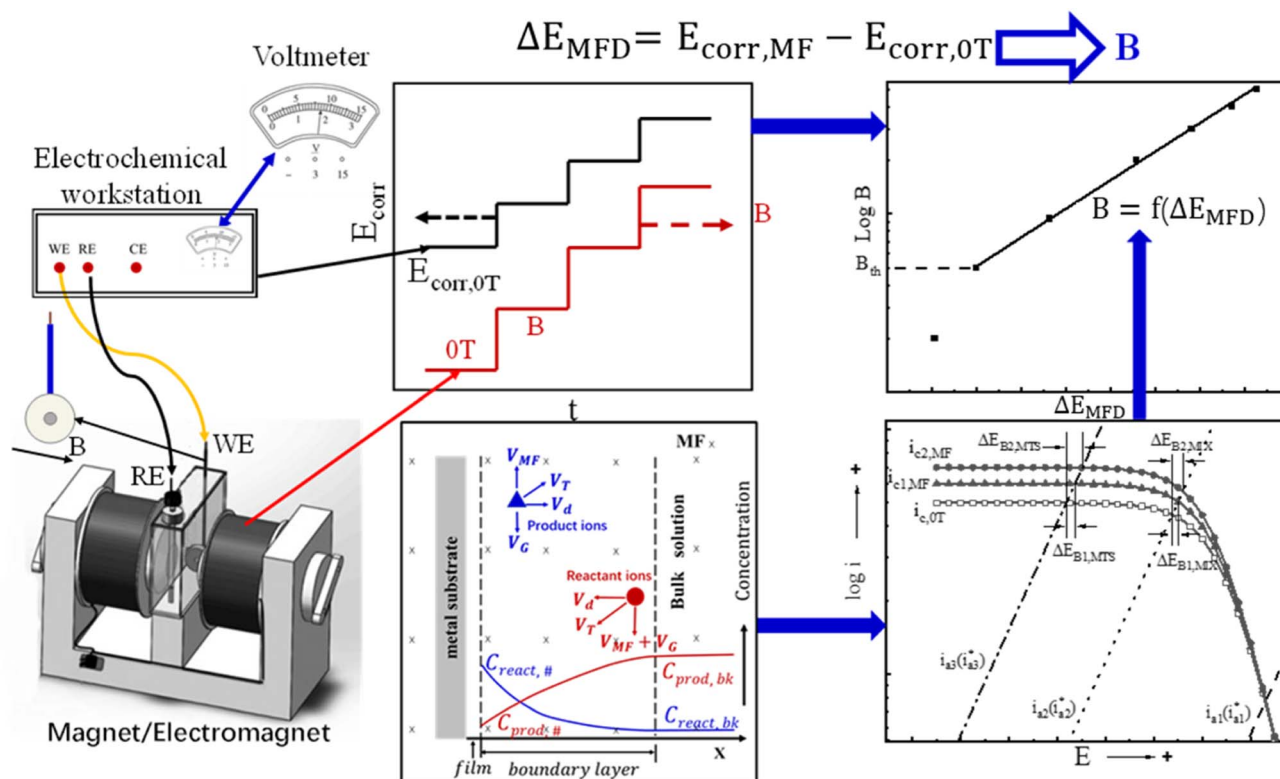


Fig. 1 The roadmap for measuring the MFD.

densities are recorded, and the  $\Delta E_{\text{MFD}}$  vs.  $B$  standard curves can be established. According to these standard curves, a specific MFD can be measured by its corresponding  $\Delta E_{\text{MFD}}$ . The objective of this work is to establish the standard relationship curve between the magnetic flux density and the change of open circuit potential induced by magnetic field for the working electrode in specific solutions, represented by  $B = f(\Delta E_{\text{MFD}})$  function. The value of an unknown magnetic flux density  $B$  can be determined by putting the measured  $\Delta E_{\text{MFD}}$  into the standard  $B = f(\Delta E_{\text{MFD}})$  curve. Various standard  $B = f(\Delta E_{\text{MFD}})$  curves are obtained for validating the proposed method in this work. In Fig. 1, the electrochemical workstation used in this work is simply used here as a voltmeter with high input resistance and data-log system for measuring and recording the open circuit potential and its response to the magnetic field of various flux densities. According to the developed method, MFD can be quantitatively measured simply by a voltmeter.

## 2. Experimental methods

The electrochemical tests were carried out in a two-electrode electrochemical system consisting of working electrode and reference electrode. The reference electrode was saturated calomel electrode (SCE) and the working electrode was industrial pure iron with a purity of 99.5%. The working surface was circular with 5 mm in diameter and exposed to the test solutions. Other non-working surfaces are sealed with epoxy resin insulators. The working electrode surface was at first ground with abrasive paper up to 1500 # grit and fine-polished with metallographic sandpaper of W5, then rinsed in ethanol and acetone in turn before the electrochemical measurements. The iron-working electrode surface was placed vertically. The magnetic field generated by an electromagnet was placed horizontally. The direction of magnetic flux density was parallel to the working electrode surface. The magnetic flux intensities were adjusted to 0.02 T, 0.05 T, 0.1 T, 0.2 T, 0.3 T, 0.4 T and 0.5 T. The test solutions were  $X \text{ mol L}^{-1}$   $\text{Fe}_2(\text{SO}_4)_3$  solutions ( $X = 0.04, 0.08, 0.12, 0.16$ ) and  $Y \text{ mol L}^{-1}$   $\text{FeCl}_3$  solutions ( $Y = 0.08, 0.16, 0.24, 0.32$ ) prepared with analytical grade  $\text{Fe}_2(\text{SO}_4)_3$  or  $\text{FeCl}_3$  as the sources of ferric ions as well as deionized water. The approach proposed in this work for measuring magnetic flux density is based on the shift of the open circuit potential of the working electrode as the response to the applied magnetic field, according to the mixed potential theory in the fundamental electrode kinetics.<sup>42</sup> The principle of designing the working electrode/solution system is: the rate-determining step for the anodic reaction on the working electrode should be electron-transfer step, and the rate of the cathodic reaction on the working electrode should be purely or partly controlled by mass-transport step. Under these conditions, applying a magnetic field would modify the mass transport of the cathodic depolarizers from the bulk solution to the electrode interface therefore change the cathodic reaction rate. The open circuit potential would shift after applying magnetic field, and the magnitude of this shift is dependent on the magnetic flux density. By establishing the calibration equation correlating the shift of open circuit potential to the magnetic flux density, the

unknown magnetic flux density can be determined by the measurement of the shift of open circuit potential. Any corrosion system with the anodic reaction rate determined by electron transfer step as well as the cathodic reaction rate partly or fully determined by mass transport step of ionic depolarizers can be used for achieving the objective of this manuscript. Electrochemical systems with iron in solutions with ferric ions such as  $\text{FeCl}_3$  and  $\text{Fe}_2(\text{SO}_4)_3$  in the solutions or in the solutions with dichromate ions<sup>14,15</sup> have been found to meet the above requirements.

The working electrode was initially immersed in a  $\text{Fe}_2(\text{SO}_4)_3$  or  $\text{FeCl}_3$  solution containing ferric ions as depolarizers. The magnetic field was imposed quickly after the open circuit potential reached a steady or quasi-steady value under 0 T, and then observing and recording the change of open circuit potential due to the magnetic field. The magnetic field was applied to the electrochemical system at various magnetic flux densities *via* a stepwise ascending mode. The open circuit potential was recorded and the steady state or quasi-steady state under each MFD was used in constructing the  $B$ - $\Delta E_{\text{MFD}}$  diagram.

According to the measured open circuit potential under various MFD,  $B$  (logarithmic scale) vs.  $\Delta E_{\text{MFD}}$  ( $X$ -axis) curve was generated and linearly fitted.  $\Delta E_{\text{MFD}}$  is expressed by eqn (1). According to the standard curves by linear fitting, the value of MFD can be determined according to the change of open circuit potential by magnetic field, as represented by  $\Delta E_{\text{MFD}}$ .

## 3. Results

### 3.1 The open circuit potential under various MFDs

The values of  $E_{\text{corr}}$  for iron in  $\text{Fe}_2(\text{SO}_4)_3$  and  $\text{FeCl}_3$  solutions with or without magnetic fields were obtained and summarized in Fig. 2 and 3. Under 0 T,  $E_{\text{corr}}$  became stable after a period of immersion in  $\text{Fe}_2(\text{SO}_4)_3$  and  $\text{FeCl}_3$  solutions. The time required for the working electrode to reach a steady state or quasi-steady state was shorter with increasing  $\text{Fe}^{3+}$  concentration under 0 T. The transient change of  $E_{\text{corr}}$  after imposing the magnetic field could be seen from the recorded  $E_{\text{corr}}$  vs. time curves.  $E_{\text{corr}}$  shifted to the noble direction quickly after applying the magnetic field, decreased subsequently, and finally reached a steady or quasi-steady value. The response of  $E_{\text{corr}}$  to magnetic field was very rapid. The change of  $E_{\text{corr}}$  induced by magnetic field increased with increasing MFD.

### 3.2 $\Delta E_{\text{MFD}}$ induced by various MFDs

$B$  vs.  $\Delta E_{\text{MFD}}$  curves are summarized in Fig. 4 and 5. In the range of MFD from 0.02 T to 0.5 T, the change of  $E_{\text{corr}}$  increases with the increase of MFD in  $\text{Fe}_2(\text{SO}_4)_3$  or  $\text{FeCl}_3$  solutions. The increasing amplitude of the change of  $E_{\text{corr}}$  induced by magnetic field shows a trend of first increasing and then decreasing. For each solution in this paper, the increasing amplitude of  $E_{\text{corr}}$  induced by magnetic field of 0.2 T was the biggest. The response of  $E_{\text{corr}}$  to magnetic field was more obvious with the increase of magnetic field. Whether in  $\text{Fe}_2(\text{SO}_4)_3$  or  $\text{FeCl}_3$  solutions, the change of  $E_{\text{corr}}$  was more sensitive to the MFD in low concentration solution.



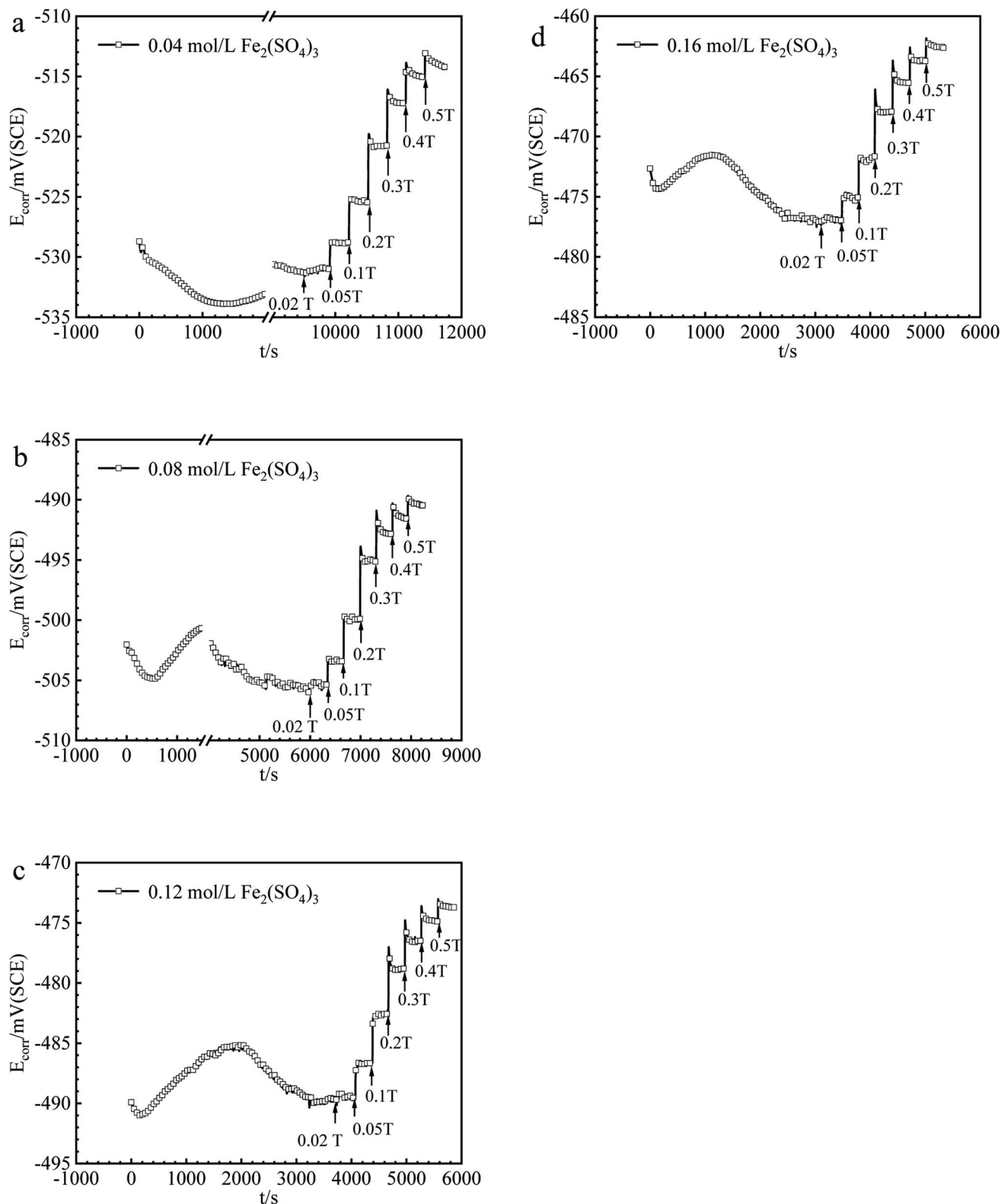


Fig. 2 The values of  $E_{\text{corr}}$  for iron in (a) 0.04, (b) 0.08, (c) 0.12, (d) 0.16 mol per L  $\text{Fe}_2(\text{SO}_4)_3$  solutions under various MFDs.

### 3.3 Cathodic polarization curves under 0 T and 0.4 T

The cathodic polarization curves for iron in  $\text{Fe}_2(\text{SO}_4)_3$  and  $\text{FeCl}_3$  solutions are summarized in Fig. 6. The cathode current density

platform with diffusion control characteristics appears in the solution with lower ferric ions of  $0.08 \text{ mol L}^{-1}$ . And the diffusion control characteristics also appear in the solution with

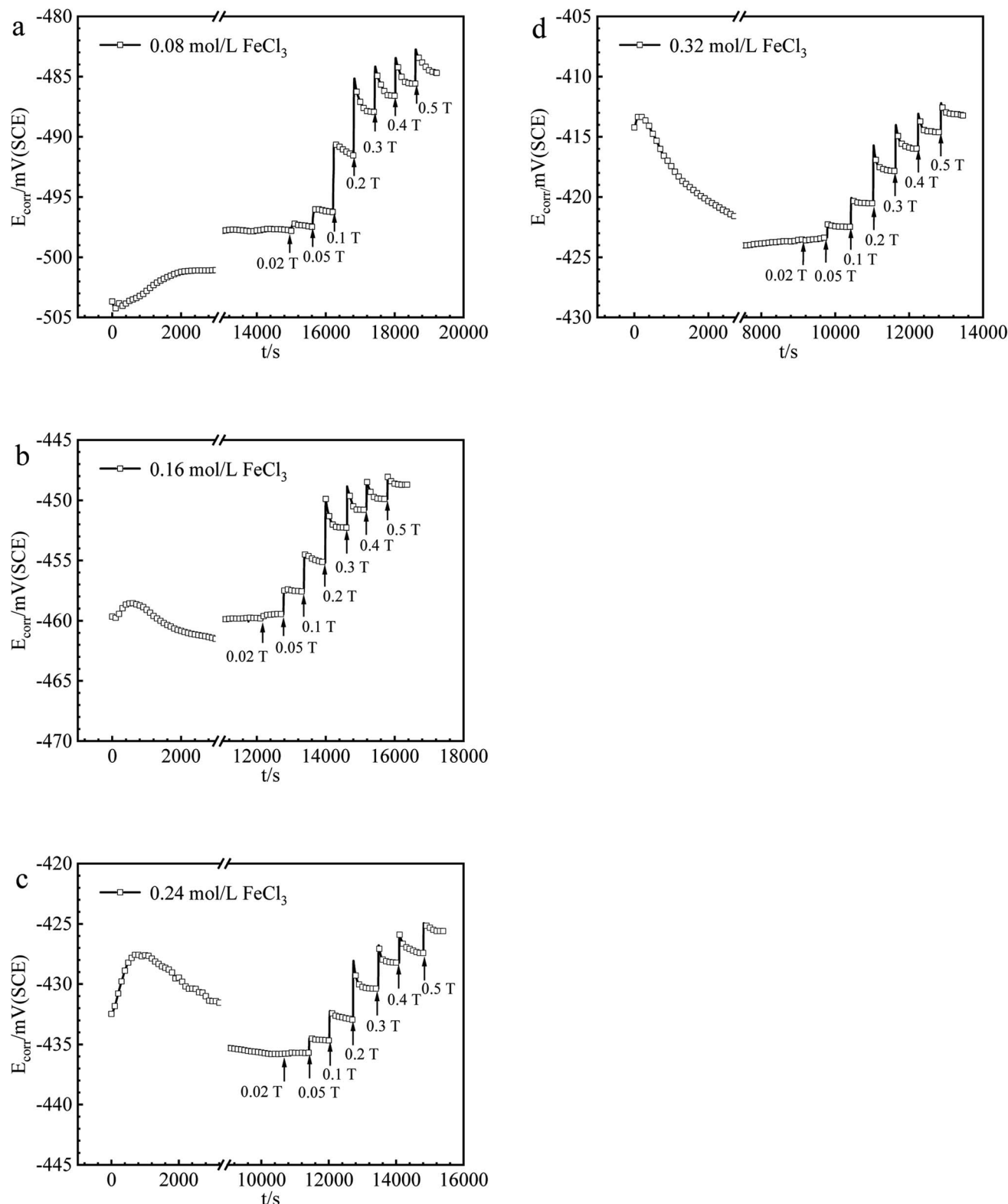


Fig. 3 The values of  $E_{\text{corr}}$  for iron in (a) 0.08, (b) 0.16, (c) 0.24, (d) 0.32 mol per L  $\text{FeCl}_3$  solutions under various MFDs.

other ferric ions concentration, but the current density platform is not obvious. Under 0 T or 0.4 T, the limiting current density for iron in a  $\text{Fe}_2(\text{SO}_4)_3$  solution was lower than that in the  $\text{FeCl}_3$  solution for the same nominal ferric ion concentration of

0.08 mol  $\text{L}^{-1}$ , as shown in Fig. 6a. Similar trends were found in other solutions of other nominal ferric concentrations under 0 T. The enhancement factor of cathodic limiting current density by magnetic field is expressed by eqn (2). For the





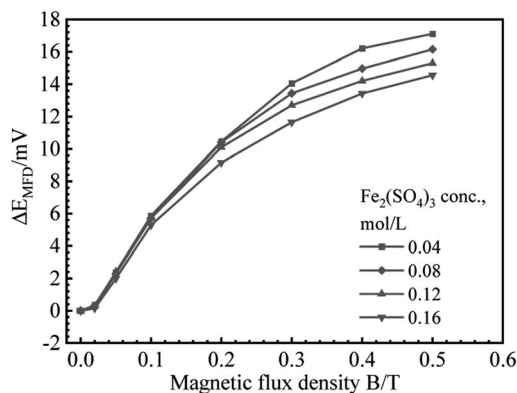


Fig. 4  $\Delta E_{\text{MFD}}$  vs.  $B$  curves for iron in  $\text{Fe}_2(\text{SO}_4)_3$  solutions with various concentrations.

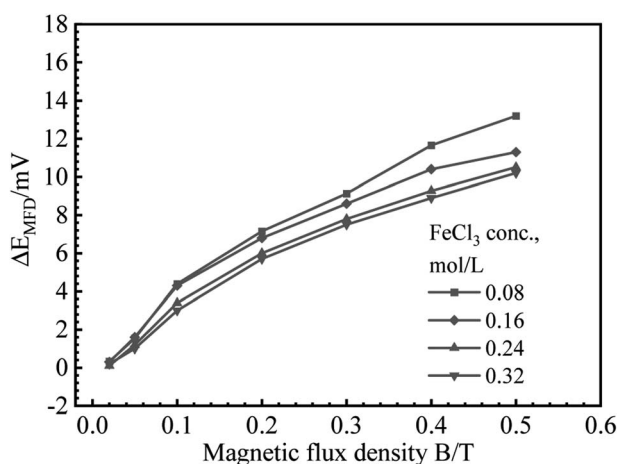


Fig. 5  $\Delta E_{\text{MFD}}$  vs.  $B$  curves for iron in  $\text{FeCl}_3$  solutions with various concentrations.

nominal ferric concentration of  $0.08 \text{ mol L}^{-1}$ , there are  $\delta_{\text{MFD}} = 1.67$  in  $0.08 \text{ mol per L FeCl}_3$  solution and  $\delta_{\text{MFD}} = 1.83$  in  $0.04 \text{ mol per L Fe}_2(\text{SO}_4)_3$  solution, and similar trends were observed in solutions with other nominal concentrations of ferric ions.

$$\delta_{\text{MFD}} = i_L^* / i_L \quad (2)$$

where  $i_L$  represents the limiting cathodic current density under 0 T and  $i_L^*$  under magnetic field.

## 4. Discussion

As schematically shown in Fig. 1, for iron in ferric sulfate or ferric chloride solutions, it is assumed that the rate of anodic reaction rate is completely controlled by the charge-transfer step (ETS), the variation of anodic reaction induced by magnetic field can be ignored. Then the effect of magnetic field on  $E_{\text{corr}}$  would be dependent only on the type of rate controlling step for the cathodic reaction under the open circuit state.

If the cathodic reaction rate under the open circuit state is absolutely controlled by ETS,  $\Delta E_{\text{MFD}}$  can be expressed by eqn

(3).  $i_c @ i_{a1}$  is used to represent the coupling of the cathodic reaction line  $i_c$  and anodic reaction  $i_{a1}$ . Other combinations of cathodic and anodic reactions follow this definition.

$$(\Delta E_{\text{MFD}})_{i_c @ i_{a1}} = 0 \quad (3)$$

If the cathodic reaction rate is absolutely controlled by mass transport step (MTS),  $\Delta E_{\text{MFD}}$  can be expressed by eqn (4).

$$(\Delta E_{\text{MFD}})_{i_c @ i_{a3}} = \beta_a \ln \left( \frac{i_L^*}{i_L} \right) \quad (4)$$

where  $\beta_a$  is the Tafel slope (in natural logarithm scale) for the anodic reaction.

If charge-transfer step ETS and mass transport step MTS both participate in controlling the cathodic reaction rate, which is defined as mixed type control, which is defined as mixed type control, then analytical form of  $\Delta E_{\text{MFD}}$  would not be simple. By considering eqn (3) and (4), there is,

$$0 < (\Delta E_{\text{MFD}})_{i_c @ i_{a2}} < \beta_a \ln \left( \frac{i_L^*}{i_L} \right) \quad (5)$$

The form of  $i_L^*$  would be complex. If taking the proposed formulation by Aaboubi *et al.*<sup>39</sup> for the limiting current density, there are  $i_L^* \propto C^{\text{mb}}$  and  $i_L^* \propto C^{\text{mc}}$ , where mb and mc are constants. Linear  $(\Delta E_{\text{MFD}})_{i_c @ i_{a3}}$  vs.  $\log B$  relationship is expected, as schematically shown in Fig. 1. It is not intended to solve  $(\Delta E_{\text{MFD}})_{i_c @ i_{a2}}$  analytically here, while the approximate form of  $(\Delta E_{\text{MFD}})_{i_c @ i_{a2}}$  can be deduced to be close to  $(\Delta E_{\text{MFD}})_{i_c @ i_{a3}}$ . Based on these theories, the measured  $E_{\text{corr}}$  or  $\Delta E_{\text{MFD}}$  data as function of  $B$  are analyzed by linear fit of the experimental data in Fig. 4 and 5. The fitting results of for  $B$  vs.  $\Delta E_{\text{MFD}}$  curves (exclude the first point) are summarized in Fig. 7 and 8, exhibiting quasi-linear relationship between  $\log B$  and  $\Delta E_{\text{MFD}}$  for all the experimental data by excluding the first point at  $B = 0.02 \text{ T}$ . The relationship can be expressed by:

$$\log B = m \times E_{\text{MFD}} + n \quad (6)$$

where  $m$  and  $n$  are constant for a certain solution system, which would change with the type of the solution as well as the concentration of the reactive species.  $\Delta E_{\text{MFD}}$  is in mV.

The first point clearly deviates from the  $\log B$  vs.  $\Delta E_{\text{MFD}}$  linear line obtained by the fitting formula. In other words, this method of measuring the MFD by electrochemical method is feasible when the magnetic field strength is greater than  $0.05 \text{ T}$  in this paper. The goodness of fit in terms of  $R$  for various data sets are also summarized in Fig. 7 and 8. The values of  $R$  from the fitted data without the first point are higher than 0.98, showing the validity of the fitting relationship. The deviation between the experimental data at low  $B$  and the fitted linear line  $\log B - \Delta E_{\text{MFD}}$  would come from the fundamental electrode kinetics at a “micro-magnetic polarisation”, somehow similar to the micro-weak-strong polarization theory in the fundamentals of electrochemistry. For the same concentration of  $\text{Fe}^{3+}$ ,  $R$  is higher for  $\text{Fe}_2(\text{SO}_4)_3$  solution than that in  $\text{FeCl}_3$  solution. Whether in  $\text{Fe}_2(\text{SO}_4)_3$  or  $\text{FeCl}_3$  solutions,  $m$  increases with the



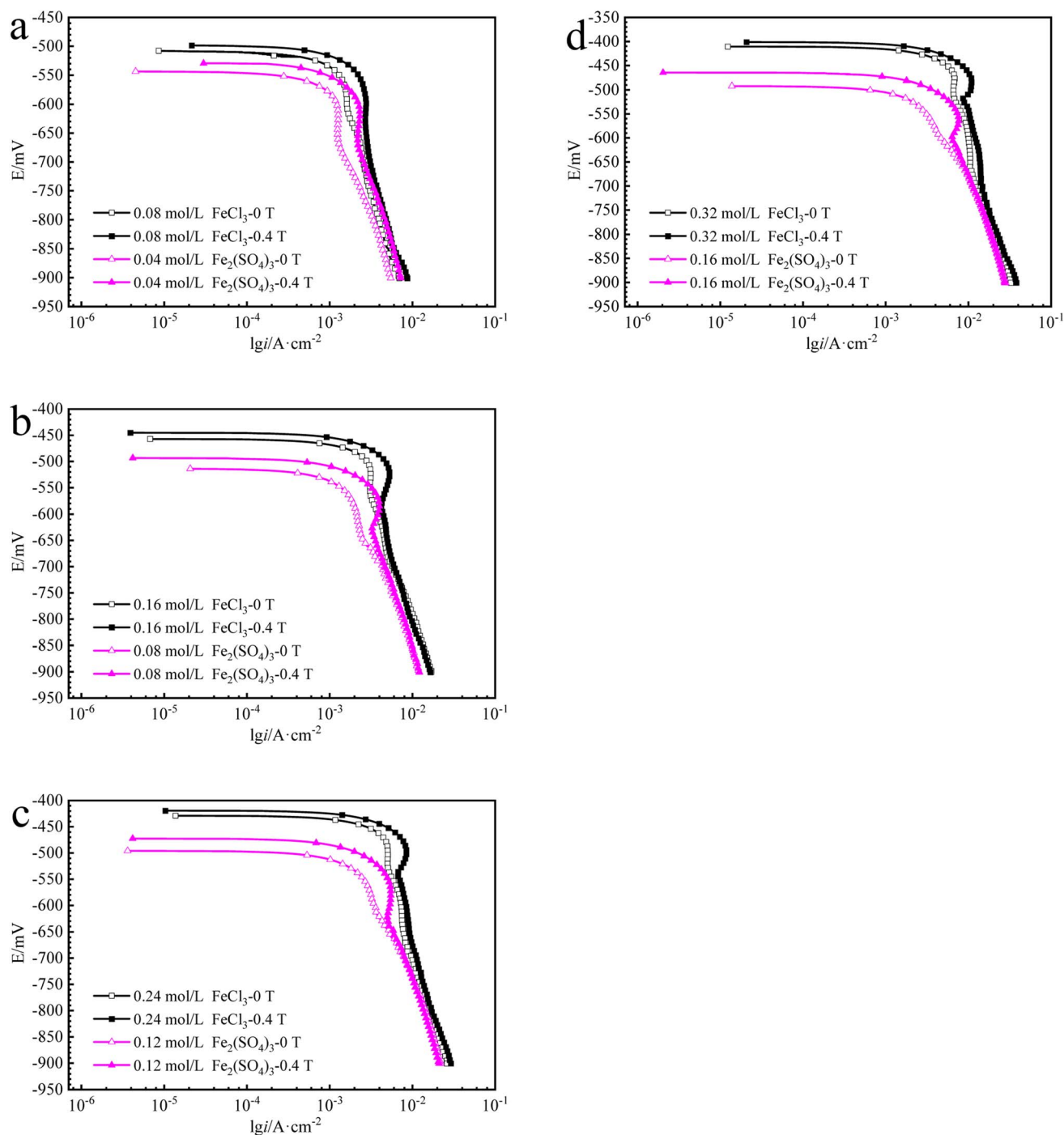


Fig. 6 Cathodic polarization curve for iron in  $\text{FeCl}_3$  and  $\text{Fe}_2(\text{SO}_4)_3$  solutions with various ferric ion concentrations. (a) 0.08 mol per L  $\text{Fe}^{3+}$ ; (b) 0.16 mol per L  $\text{Fe}^{3+}$ ; (c) 0.24 mol per L  $\text{Fe}^{3+}$ ; (d) 0.32 mol per L  $\text{Fe}^{3+}$ .

increases of  $\text{Fe}^{3+}$  concentration, indicating that  $\Delta E_{\text{MFD}}$  is more sensitive to  $B$  if the concentration of  $\text{Fe}^{3+}$  is low in the solution. For the same concentration of  $\text{Fe}^{3+}$ ,  $m$  is lower in  $\text{Fe}_2(\text{SO}_4)_3$  solution than in  $\text{FeCl}_3$  solution. If the cathodic reaction rate is fully controlled by mass transport step at open circuit potential, for the solution with the same nominal concentration of ferric ions, the limiting cathodic current is not the same and the  $i_L^*/i_L$  ratio is different. Assuming that the open circuit state is mainly

determined by the cathodic reaction rate in various solutions, according to eqn (4),  $\Delta E_{\text{MFD}}$  increases with increasing  $i_L^*/i_L$  ratio. For the electrochemical systems with the cathodic reaction rate controlled by both the mass transport step and the electron transfer step, the value of  $\Delta E_{\text{MFD}}$  is lower than the calculated value by eqn (4), while the dependence of  $\Delta E_{\text{MFD}}$  on the type of solution or the ferric concentration is consistent with eqn (4).  $\Delta E_{\text{MFD}}$  in  $\text{FeCl}_3$  solution is less than that in the



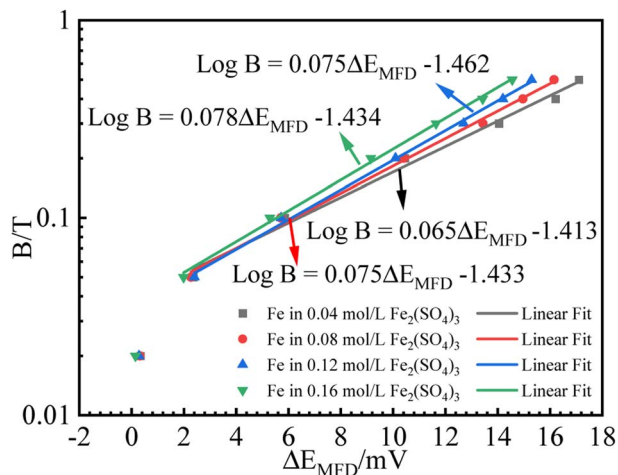


Fig. 7 Fitting results for  $B$  (logarithmic scale) vs.  $\Delta E_{\text{MFD}}$  curve for iron in  $\text{Fe}_2(\text{SO}_4)_3$  solutions with various ferric ion concentrations.

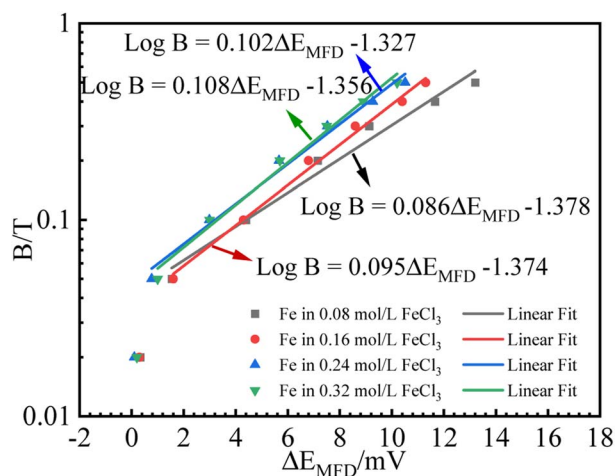


Fig. 8 Fitting results for  $B$  (logarithmic scale) vs.  $\Delta E_{\text{MFD}}$  curve for iron in  $\text{FeCl}_3$  solutions with various ferric ion concentrations.

$\text{Fe}_2(\text{SO}_4)_3$  solution, and the slope  $m$  is higher in  $\text{FeCl}_3$  solution than in  $\text{Fe}_2(\text{SO}_4)_3$  solution if the ferric ion concentration is the same.

Based on the experimental data in Fig. 2–5, the parameters in the fitting equation, eqn (5), can be obtained. Then, the unknown magnetic flux density in the range of 0.05 T to 0.5 T can be obtained by the suggested method through the measurement of  $\Delta E_{\text{MFD}}$ . It is noted that the parameters for fitting are related to the type of solution and the concentration of the reactive species. For the measurement systems with iron in  $\text{Fe}_2(\text{SO}_4)_3$  solutions in the present work, 1 mV increase of  $\Delta E_{\text{MFD}}$  corresponds to 16–20% increase of  $B$ , namely, 1.6–2.0% increase of  $B$  would be able to be indicated by 0.1 mV increase of  $\Delta E_{\text{MFD}}$ . For iron in  $\text{FeCl}_3$  solutions in the present work, 1 mV increase of  $\Delta E_{\text{MFD}}$  corresponds to 22–28% increase of  $B$ , namely, 2.2–2.8% increase of  $B$  would be able to be detected by 0.1 mV increase of  $\Delta E_{\text{MFD}}$ .

## Conclusions

A novel electrochemical method has been developed for measuring magnetic flux density, as an alternative way of magnetic measurements without using tesla meter.

(1) The change of open circuit potential for iron in  $\text{Fe}_2(\text{SO}_4)_3$  or  $\text{FeCl}_3$  solutions induced by magnetic field can be used to determine the magnetic flux density.

(2) The linear relationship for  $\log B$  vs.  $\Delta E_{\text{MFD}}$  has been used in the fitting equation for the standard curves. The electrochemical method has been validated for measuring the magnetic flux density in the range from 0.05 T to 0.5 T in this work.

(3) The fitting parameters for the standard curve are related to the type of solution as well as the concentration.

(4) About 2% change of magnetic flux density in the range of 0.05 T to 0.5 T can be detected by the proposed electrochemical methods, supposing that the configuration of the system remains to be the same for the measurement conditions.

## Conflicts of interest

No conflict of interest exists in the submission of this manuscript.

## Acknowledgements

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## References

- 1 R. S. Elliott, *Electromagnetics: history, theory, and applications*. IEEE Press, 1993.
- 2 K. H. J. Buschow and F. R. De Boer, *Physics of Magnetism and Magnetic Materials*, Springer-Verlag New York Inc, 2013.
- 3 R. S. Elliott, *Antennas & Propagation Society International Symposium IEEE*, 1988, vol. 6, pp. 6–18.
- 4 J. D. Kraus and D. A. Fleisch, *Electromagnetics with Applications*, McGraw-Hill, 1999.
- 5 H. Zijlstra, *Experimental Methods in Magnetism*. John Wiley & Sons, Inc: New York, 1967.
- 6 S. Tumanski, *Handbook of Magnetic Measurements*, CRC Press Inc, 2011.
- 7 Z. X. Chen and J. J. Lu, *Mine Warfare & Ship Self-Defence*, 2011, **19**, 1–4.
- 8 S. M. Lim and J. S. Park, *J. Electr. Eng. Technol.*, 2019, **14**, 377–383.
- 9 J. Lee, Y. Oh and S. Oh, *Sens.*, 2020, **20**, 5285.
- 10 D. Jurman, M. Jankovec and R. Kamnik, *Sens. Actuators, A*, 2007, **138**, 411–420.
- 11 M. Vopálenký, A. Platil and P. Kašpar, *Sens. Actuators, A*, 2005, **123**, 303–307.
- 12 M. Kocan, *Fusion Eng. Des.*, 2017, **123**, 936.
- 13 V. Zhukova, A. Zhukov, K. L. Garcia, V. Kraposhin and A. Prokoshin, *Sens. Actuators, A*, 2003, **106**, 225–229.





- 14 S. L. Zhang, G. F. Zhang, Y. L. Wang, M. Liu, H. Li, Y. Qiu, J. Zeng, X. Y. Kong and X. M. Xie, *Chin. Phys. B*, 2013, **22**, 128501.
- 15 H. Dong, Y. L. Wang, S. L. Zhang, Y. Sun and X. M. Xie, *Supercond. Sci. Technol.*, 2008, **21**, 115009.
- 16 M. Schmelz, R. Stolz, V. Zakosarenko, T. Schoenau, A. Anders, L. Fritzsche, M. Mueck and H. G. Meyer, *Supercond. Sci. Technol.*, 2011, **24**, 065009.
- 17 J. Zeng, Y. Zhang, M. Mueck, H. J. Krause, A. I. Braginski, X. Y. Kong, X. M. Xie, A. Offenhaeusser and M. Jiang, *Appl. Phys. Lett.*, 2013, **103**, 042601.
- 18 F. Kaluza, A. Gruger and H. Gruger, *Sens. Actuators, A*, 2003, **106**, 48–51.
- 19 B. Andò, S. Baglio, A. R. Bulsara and C. Trigona, *Sens. Actuators, A*, 2009, **151**, 145–153.
- 20 R. S. Popovic, Z. Randjelovic and D. Manic, *Sens. Actuators, A*, 2001, **91**, 46–50.
- 21 A. Girgin, M. Bilmez, H. Y. Amin and T. C. Karalar, *Microelectron. J.*, 2019, **90**, 12–18.
- 22 S. Q. Mo, R. S. Wei, Z. Q. Zeng and M. H. He, *Microelectron. J.*, 2021, **113**, 105067.
- 23 J. Jezný and M. Čurilla, *Am. J. Mech. Eng.*, 2013, **1**, 231–235.
- 24 M. H. Kang, B. W. Choi, K. C. Koh, J. H. Lee and G. T. Park, *Sens. Actuators, A*, 2005, **118**, 278–284.
- 25 H. Hauser, P. L. Fulmek, P. Haumer, M. Vopalensky and P. Ripka, *Sens. Actuators, A*, 2003, **106**, 121–125.
- 26 S. Wissberg, M. Ronen, Z. Oren, D. Gerber and B. Kalisky, *Sci. Rep.*, 2020, **10**, 1573.
- 27 S. J. Lee, K. Jeong, J. H. Shim, H. J. Lee, S. Min, H. Chae, S. K. Namgoong and K. Kim, *Sci. Rep.*, 2019, **9**, 12422.
- 28 F. Arute, K. Arya, R. Babbush, D. Bacon and J. C. Bardin, *Nature*, 2019, **574**, 505–510.
- 29 Z. P. Lu, D. L. Huang, W. Yang and G. Z. Zhao, *J. Chin. Soc. Corros. Prot.*, 2000, **20**, 230–236.
- 30 Z. P. Lu, D. L. Huang and W. Yang, *Corros. Prot.*, 2002, **23**, 185–189.
- 31 F. M. F. Rhen, G. Hinds and J. M. D. Coey, *Electrochem. Commun.*, 2004, **6**, 413–416.
- 32 Z. P. Lu, D. L. Huang and W. Yang, *Corros. Sci.*, 2005, **47**, 1471–1492.
- 33 Z. P. Lu and W. Yang, *Corros. Sci.*, 2008, **50**, 510–522.
- 34 R. Sueptitz, K. Tschulik, M. Uhlemann, A. Gebert and L. Schultz, *Electrochim. Acta*, 2010, **55**, 5200–5203.
- 35 M. Waskaas and Y. I. Kharkats, *J. Electroanal. Chem.*, 2001, **502**, 51–57.
- 36 G. Hinds, J. M. D. Coey and M. E. G. Lyons, *Electrochem. Commun.*, 2001, **3**, 215–218.
- 37 L. M. A. Monzon and J. M. D. Coey, *Electrochem. Commun.*, 2014, **42**, 38–41.
- 38 T. Z. Fahidy, *J. Appl. Electrochem.*, 1983, **13**, 553–563.
- 39 O. Aaboubi, J. P. Chopart, J. Douglade, A. Olivier, C. Gabrielli and B. Tribollet, *J. Electrochem. Soc.*, 1990, **137**, 1796–1804.
- 40 L. M. A. Monzon and J. M. D. Coey, *Electrochem. Commun.*, 2014, **42**, 42–45.
- 41 S. R. Ragsdale, K. M. Grant and H. S. White, *J. Am. Chem. Soc.*, 1998, **120**, 13461–13468.
- 42 C. Wagner and W. Traud, *Corrosion*, 2006, **62**, 277–314.

