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Selective and controlled H₂ generation upon additive-free HCOOH dehydrogenation over a Pd/NCS nanocatalyst†

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Although sodium formate is widely used as a conventional additive to enhance selective H₂ evolution from HCOOH dehydrogenation, this leads to a waste of resources and an increase in the cost of H₂ production. For this reason, N-doped carbon nanospheres with abundant graphitic C/N have been designed to enrich the electron cloud density of the Pd atom for improving its catalytic activity in H₂ generation upon additive-free HCOOH dehydrogenation. Herein, we have synthesized N-doped carbon nanosphere-stabilized Pd nanoparticles (Pd/NCSs) as high-efficiency nano-catalysts, *via* fixation of Pd nanoparticles onto N-doped carbon nanospheres (NCSs), for selective and controlled H₂ generation upon additive-free HCOOH dehydrogenation. Pd/NCS-800 (1640 h⁻¹) provided a 12 times larger TOF than commercial Pd/C (134 h⁻¹) in H₂ generation upon additive-free HCOOH dehydrogenation. It seemed that graphitic N/C of NCS-800 enriched the electron cloud density of the Pd atom, which was favorable for the cleavage of C–H bonds in HCOOH dehydrogenation. In addition, the selective H₂ evolution from additive-free HCOOH dehydrogenation over Pd/NCS-800 is successfully controlled by adjusting the pH.

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Introduction

Humanity's high dependence on traditional fossil fuels has caused the growth of greenhouse gas emission (e.g. CO₂ and CH₄),^{1–3} which leads to ocean acidification, climatic anomaly, global warming and other environmental deterioration.^{4–7} To overcome this issue, it is of high significance to develop renewable energy sources, switching from fossil fuels, for a green future.^{8–10} Hydrogen (H₂) is identified as the most promising renewable energy carrier because of its superior energy density and environmentally-friendly economy.^{11–15} However, physical storage of H₂ gas suffers from low capacity, high costs and explosibility.^{16–20} In this regard, a good deal of hydrogen storage materials, for instance methanol,^{21–24} borohydrides,^{25,26} silicohydrides,²⁷ ammonia borane,²⁸ hydrazine hydrate²⁹ and formic acid,^{30–32} are being intensively developed for H₂ generation.

Since 1978,³³ formic acid (HCOOH), which could be readily obtained from biomass, has been deemed as the most promising liquid hydrogen carrier due to its excellent hydrogen storage capacity (4.4 wt% and 53 g L⁻¹), low toxicity, outstanding stability and safe transportation/storage.^{34–40} As a consequence, plenty of heterogeneous and homogeneous catalysts have been explored for selective H₂ evolution from formic acid dehydrogenation (HCOOH → H₂↑ + CO₂↑) and preventing CO release from formic acid dehydration (HCOOH → H₂O + CO↑).^{41–47} Among them, PdAg bimetal nanomaterials exhibited

superior catalytic activities in H_2 generation from formic acid dehydrogenation because the alloying of Ag could enrich the electron cloud density of the Pd atom in PdAg, which was in favor of C-H bond cleavage in HCOOH dehydrogenation.⁴⁸ Although sodium formate is widely used as an additive to improve selective H_2 evolution upon HCOOH dehydrogenation,⁴⁹ this leads to a waste of resources and an increase in the cost of H_2 production.

For this reason, we have designed and synthesized N-doped carbon nanospheres with abundant graphitic C/N for enriching the electron cloud density of the Pd atom in additive-free HCOOH dehydrogenation. Herein, we have synthesized N-doped carbon nanosphere-stabilized Pd nanoparticles (Pd/NCSs) as high-efficiency nano-catalysts, *via* fixation of Pd nanoparticles onto N-doped carbon nanospheres (NCSs), for selective and controlled H_2 generation upon additive-free HCOOH dehydrogenation. Then the kinetic behavior and catalytic activity of Pd/NCSs, mechanistic insight using a tandem reaction, CO_2 capture ability, and “on-off” control for selective and controlled H_2 generation upon additive-free HCOOH dehydrogenation were investigated.

Results and discussion

As described in Scheme 1, NCS-700, NCS-800 and NCS-900 were synthesized by the calcination of melamine, α -D-glucose hydrochar and $NaHCO_3$, with a mass ratio of 1.0 : 1.0 : 1.0, at 700 °C, 800 °C and 900 °C under a N_2 atmosphere for 1 h, respectively.⁵⁰ Then Pd/NCS-700, Pd/NCS-800 and Pd/NCS-900 were synthesized by using K_2PdCl_4 and NCSs, followed by $NaBH_4$ reduction, respectively. For studying the structure and morphology of NCS and Pd/NCSs, their SEM images were obtained and are shown in Fig. 1. As illustrated in Fig. S1,[†] the SEM image shows that the NCS precursor has a uniform spherical structure with a mean size of 0.27 μm (Fig. S2[†]). After high temperature carbonization, the uniform spherical structure was retained in Pd/NCS-700 (0.23 μm , Fig. 1a, b & S3[†]), Pd/NCS-800 (0.22 μm , Fig. 1c, d & S4[†]) and Pd/NCS-900 (0.22 μm , Fig. 1e, f & S5[†]), and the size of the NCSs reduced as the calcination temperature increased. Then, XRD, FTIR, Raman spectrum and BET analyses were employed to measure the microstructure of Pd/NCS-700, Pd/NCS-800 and Pd/NCS-900. As shown in Fig. 2a, a broad diffraction peak of graphitic C (002) at $\theta = 24^\circ$ appeared in all of the Pd/NCSs (JCPDS 75-1621).⁵¹ Pd (111) and Pd (200) were also found in Pd/NCSs (JCPDS 87-0638),⁵² showing that the PdNPs were immobilized on the surface of NCSs. In the FTIR spectra of

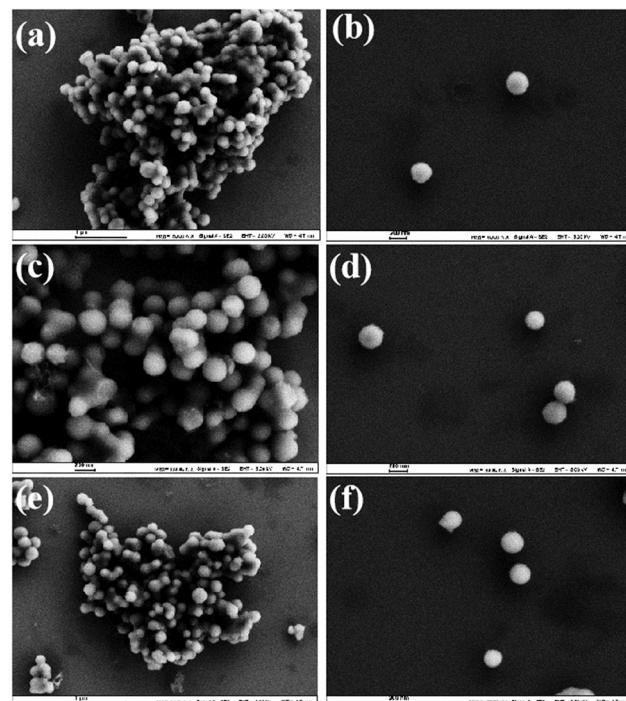


Fig. 1 SEM images of (a and b) Pd/NCS-700, (c and d) Pd/NCS-800 and (e and f) Pd/NCS-900.

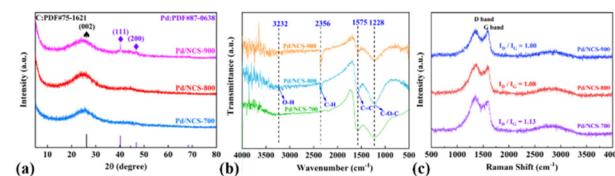


Fig. 2 (a) XRD, (b) FT-IR, and (c) Raman spectra of Pd/NCS-700, Pd/NCS-800 and Pd/NCS-900.

Pd/NCSs (Fig. 2b), the absorption peaks at 3232, 2356, 1575 and 1228 cm^{-1} corresponded to the -OH, C-H, C=C and C-O-C groups, respectively,⁵³ which were favorable for PdNP stabilization. As presented in Raman spectra (Fig. 2c), the three peaks at 1338, 1613 and 2756 cm^{-1} were assigned to the D-band, G-band and 2D-band, respectively.⁵⁴ The values of I_D/I_G in Pd/NCS-700, Pd/NCS-800 and Pd/NCS-900 were 1.00, 1.08 and 1.13, respectively, suggesting that the content of disordered carbon increased as the calcination temperature increased. Moreover, the texture properties of Pd/NCSs were studied by BET analysis. As shown in Fig. S6[†] and Table 1,



Scheme 1 The synthesis of Pd/NCS-800 nanocomposites.

Table 1 BET analysis of Pd/NCS-700, Pd/NCS-800 and Pd/NCS-900

Catalysts	Surface area ($m^2 g^{-1}$)	Pore volume ($m^3 g^{-1}$)	Pore size (nm)
Pd/NCS-700	458.43	0.27	2.34
Pd/NCS-800	572.74	0.33	2.33
Pd/NCS-900	635.09	0.37	2.33

Pd/NCS-900 exhibited a larger surface area and pore volume ($635.09\text{ m}^2\text{ g}^{-1}$ & $0.37\text{ m}^3\text{ g}^{-1}$) than Pd/NCS-700 and Pd/NCS-800.

First, the catalytic performances of Pd/NCSs in H_2 generation upon additive-free HCOOH dehydrogenation were compared as shown in Fig. S7.† H_2 production was carried out with HCOOH (1 mmol) and 2 mol% of Pd/NCSs in 5 mL of H_2O at 60°C . It is clear that Pd/NCS-800 exhibited a superior catalytic performance, with a TOF of 1640 h^{-1} , compared to Pd/NCS-700 (1456 h^{-1}) and Pd/NCS-900 (921 h^{-1}) in additive-free HCOOH dehydrogenation. Hence, Pd/NCS-800 was chosen as the optimal catalyst because of its kinetic behavior, recyclability, CO_2 capture ability, tandem reaction, and “on-off” switch of H_2 generation upon additive-free HCOOH dehydrogenation.

For probing why Pd/NCS-800 was so super-efficient in H_2 generation upon additive-free HCOOH dehydrogenation, TEM and HRTEM were employed to confirm the morphology of Pd/NCS-800. From Fig. 3a–e, it is clear that Pd/NCS-800 possessed a homogeneous nanospherical structure, and PdNPs (3.19 nm, Fig. S8†) were successfully stabilized onto the surface of N-doped carbon nanospheres. As shown in Fig. 3f, Pd (111), whose corresponding lattice space is 0.22 nm, was recorded in Pd/NCS-800, verifying the presence of PdNPs on NCSs. Then, the precise localization of Pd, N, O and C elements in Pd/NCS-800 was further investigated by EDX elemental mapping. As described in Fig. 4, the Pd/NCS-800 nanocomposite was made up of palladium, nitrogen, oxygen and carbon elements, verifying that N atoms were successfully doped into carbon nanospheres.

In addition, XPS was employed to investigate the elemental composition and chemical valence of Pd/NCS-800. As displayed in Fig. 5a, the Pd 3d_{5/2} spectrum is deconvoluted into two peaks of Pd⁰ (336.26 eV) and Pd^{II} (337.94 eV), demonstrating that Pd nanoparticles were partly oxidized by air into Pd^{II}.⁵⁵ In Fig. 5b, the N 1s spectrum is fitted into four peaks of nitric oxide (405.1 eV, 19.9%), graphitic-N (401.4 eV, 18.5%), pyrrolic-N (399.9 eV, 26.2%) and pyridinic-N (398.2 eV, 35.4%). As displayed in Fig. 5c, the C 1s spectrum is fitted into five

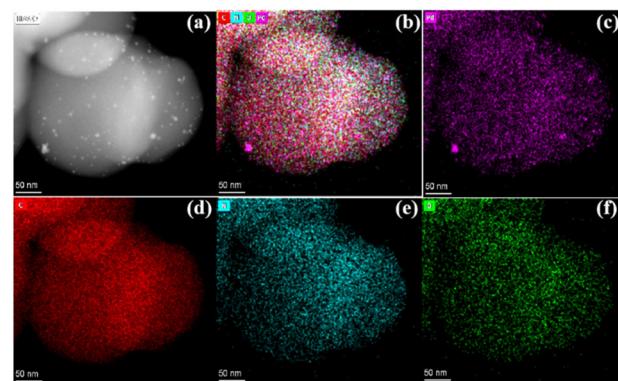


Fig. 4 (a) STEM and (b) combined C, N, O and Pd, (c) Pd, (d) C, (e) N and (f) O EDX mapping of Pd/NCS-800.

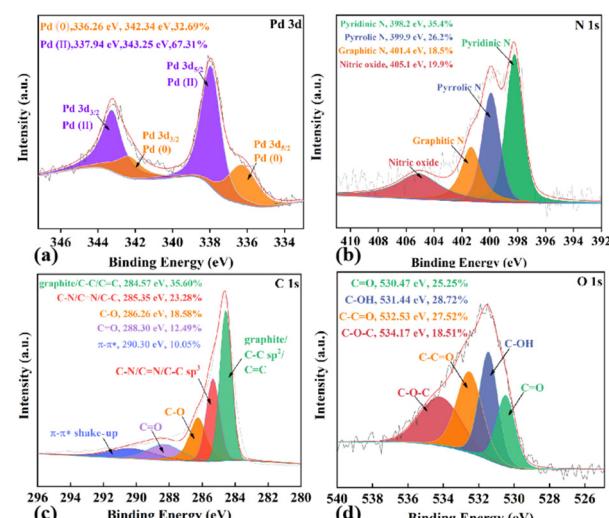


Fig. 5 (a) Pd 3d, (b) N 1s, (c) C 1s and (d) O 1s XPS of Pd/NCS-800.

typical peaks at 290.3, 288.3, 286.3, 285.4 and 284.6 eV, which are assigned to $\pi-\pi^*$ (10.05%), C=O (12.49%), C–O (18.58%), C–N (23.28%) and C–C/C=C (35.60%), respectively. As illustrated in Fig. 5d, the O 1s spectrum is fitted into four typical peaks of C–O–C (534.17 eV), C–C=O (532.53 eV), C–OH (531.44 eV) and C=O (530.47 eV), respectively. These results exhibited the presence of N and O-containing functional groups at the Pd/NCS-800 surface. ICP-AES verified that Pd nanoparticles were stabilized onto the surface of NCSs (5.38 wt% Pd, which was slightly smaller than the theoretical value of 6.62 wt%).

The kinetics of H_2 generation upon additive-free HCOOH dehydrogenation (including different Pd/NCS-800 catalyst dosages, various initial HCOOH concentrations and reaction temperatures) was further studied for the potential industrial application. As described in Fig. 6a, the H_2 generation upon additive-free HCOOH dehydrogenation was conducted with various dosages of the Pd/NCS-800 catalyst from 1.5 to 3.0 mol%. The H_2 generation rate elevated as the Pd/NCS-800

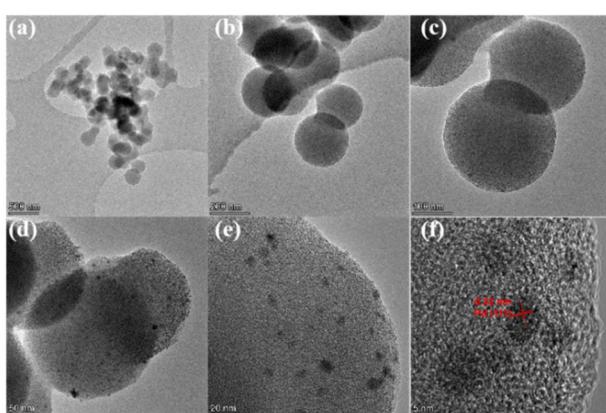


Fig. 3 (a)–(e) TEM and (f) HRTEM images of Pd/NCS-800.

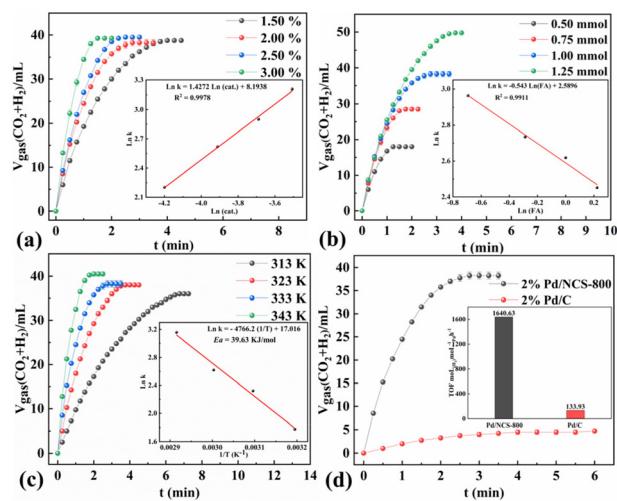


Fig. 6 The volumes of generated CO_2 and H_2 gases vs. time for H_2 generation upon additive-free HCOOH dehydrogenation (a) with various amounts of the catalyst, (b) with different amounts of HCOOH and (c) at different reaction temperatures; (d) comparison of additive-free HCOOH dehydrogenation catalyzed by Pd/NCS-800 and Pd/C.

catalyst dosage increased, with a slope of 1.4, illustrating that there was a linear positive relationship between them. As presented in Fig. 6b, the H_2 production rate was independent of the initial HCOOH concentration, indicating that additive-free HCOOH dehydrogenation was a zero-order reaction with the initial HCOOH concentration. Then H_2 generation upon additive-free HCOOH dehydrogenation over Pd/NCS-800 was measured at various reaction temperatures from 313 to 343 K (Fig. 6c). The E_a of H_2 generation upon additive-free HCOOH dehydrogenation over Pd/NCS-800 was obtained to be 39.63 kJ mol⁻¹. The comparison of Pd/NCS-800 and commercial Pd/C in H_2 generation upon additive-free HCOOH dehydrogenation was recorded and is shown in Fig. 6d. The result shows that Pd/NCS-800 (1640 h⁻¹) provided a 12 times larger TOF than commercial Pd/C (134 h⁻¹) in H_2 generation upon additive-free HCOOH dehydrogenation. In addition, the Pd/NCS-800 catalyst also showed excellent catalytic performance in H_2 generation from NH_3BH_3 ($\text{NH}_3\text{BH}_3 + 4\text{H}_2\text{O} \rightarrow \text{NH}_4\text{B}(\text{OH})_4 + 3\text{H}_2\uparrow$, TOF = 11 116.1 h⁻¹, Fig. 7a), tetrahydroxydiboron ($\text{B}_2(\text{OH})_4 + 2\text{H}_2\text{O} \rightarrow 2\text{B}(\text{OH})_3 + \text{H}_2\uparrow$, TOF = 10 111.6 h⁻¹, Fig. 7b), dimethylaminoborane ($\text{Me}_2\text{NHBH}_3 + 4\text{H}_2\text{O} \rightarrow \text{Me}_2\text{NH}_2\text{B}(\text{OH})_4 + 3\text{H}_2\uparrow$, TOF = 2902 h⁻¹, Fig. 7c) and tetramethyldisiloxane ($[\text{Me}_2\text{SiH}]_2\text{O} + 2\text{H}_2\text{O} \rightarrow [\text{Me}_2\text{Si}(\text{OH})]_2\text{O} + 2\text{H}_2\uparrow$, TOF = 1955 h⁻¹, Fig. 7d), confirming that the Pd/NCS-800 catalyst is a versatile and applicable catalyst.

The stability of the Pd/NCS-800 catalyst in H_2 generation upon additive-free HCOOH dehydrogenation was investigated for further industrial application.⁵⁶ When H_2 generation was completed, the Pd/NCS-800 nanocatalyst was isolated and recycled by filtration. Next, another fresh HCOOH solution was injected into the medium for next recycling. As described in Fig. S9,[†] it is clear that the Pd/NCS-800 catalyst still maintained excellent catalytic activity at least for 5 cycles in H_2

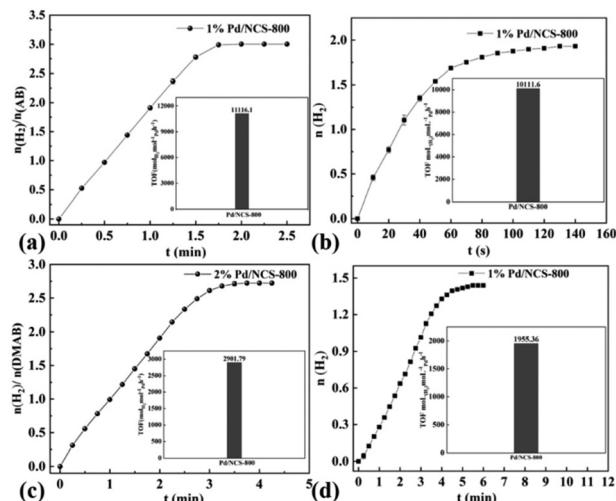
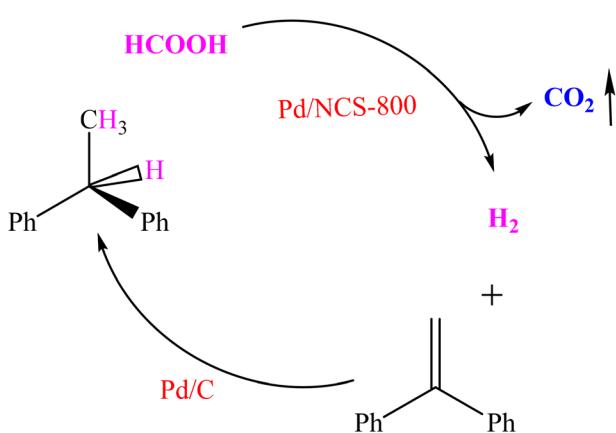


Fig. 7 Pd/NCS-800 catalyzed H_2 generation from (a) ammonia borane, (b) $\text{B}_2(\text{OH})_4$, (c) dimethylaminoborane and (d) tetramethyldisiloxane at 30 °C.

generation upon additive-free HCOOH dehydrogenation without any activity loss. Then, the 5 times reused Pd/NCS-800 catalyst was further analyzed by XRD, and Fig. S10[†] shows that its crystal structure remained almost the same as that of the fresh one, demonstrating that Pd/NCS-800 is a heterogeneous and recyclable nanocatalyst for H_2 generation upon additive-free HCOOH dehydrogenation.

H_2 generation upon additive-free HCOOH dehydrogenation is applied not only for safe and economical production, storage and transportation of hydrogen, but also for a tandem reaction.⁵⁷ 1,1-Diphenylethylene hydrogenation with the *in situ* released H_2 from additive-free HCOOH dehydrogenation was carried out in a two-chamber reactor (Scheme 2). The left tube was applied for H_2 generation upon additive-free HCOOH dehydrogenation, and the right one was applied for 1,1-diphenylethylene hydrogenation with the H_2 from the left tube *via* a glass tube (Fig. S11[†]). The yield of the target product (1,1-



Scheme 2 The tandem reaction.

diphenylethane) was 99% (Fig. S12†), illustrating selective H_2 generation upon additive-free HCOOH dehydrogenation.

For verifying the selective H_2 generation upon additive-free HCOOH dehydrogenation, a gas mixture was passed through a NaOH solution for CO_2 absorption. As shown in Fig. 8a, the volume of the gas mixture was reduced by half with the sodium hydroxide trap, suggesting that the released gases were H_2 and CO_2 , with a volumetric ratio of 1.0 : 1.0. Then the released gases were also confirmed by GC to be H_2 and CO_2 , with a molar ratio of 1.0 : 1.0 (Fig. 8b). The CO_2 capture test and GC analysis verified that the selective H_2 generation upon additive-free formic acid dehydrogenation over the Pd/NCS-800 catalyst was successfully designed for fuel cells. Based on the CO_2 capture test, GC analysis and relevant literature,^{58,59} a possible mechanism involved in HCOOH dehydrogenation is discussed in Fig. S13.† First, a HCOOH molecule was decomposed into Pd–H and HCOO–Pd on the surface of Pd/NCS-800. Then, CO_2^* and Pd–H were formed from HCOO–Pd *via* β -hydride elimination. Finally, H_2 was obtained by the reductive elimination of two Pd–H molecules.

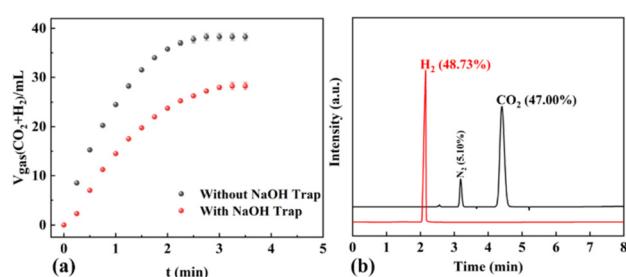


Fig. 8 (a) HCOOH dehydrogenation over Pd/NCS-800 with and without a sodium hydroxide trap; (b) GC spectra of the gases released from additive-free HCOOH dehydrogenation at 60 °C.

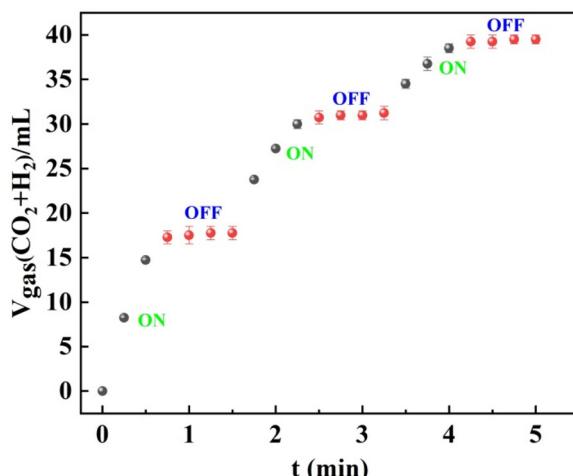


Fig. 9 "On-off" switch of H_2 generation upon additive-free formic acid dehydrogenation. Reaction conditions: 1 mmol of formic acid and 2 mol% of Pd/NCS-800 in water (5 mL) at 60 °C.

The exploitation of the "on-off" switch for demand-based H_2 production is highly desirable.^{60–62} As demonstrated in Fig. 9, selective H_2 generation upon additive-free HCOOH dehydrogenation over Pd/NCS-800 was successfully controlled by adjusting the pH. Specifically, H_2 generation upon additive-free HCOOH dehydrogenation stopped after the addition of NaOH solution because formic acid converted into formate. Then, H_2 generation upon additive-free formic acid dehydrogenation restarted after the addition of H_2SO_4 solution due to the regeneration of formic acid. However, a slight decrease in the H_2 generation rate was recorded after each "on-off" switch, which may be caused by the dilution effect.

The catalytic performances of Pd/NCS-800 and other reported catalysts for H_2 generation upon additive-free HCOOH dehydrogenation were compared and are shown in Table S1.†^{63–72} The result shows that Pd/NCS-800 exhibited an excellent TOF of 1641 h^{-1} , illustrating that Pd/NCS-800 is an excellent catalyst for selective and controlled H_2 generation upon additive-free HCOOH dehydrogenation.

Conclusions

In summary, a battery of N-doped carbon nanosphere-stabilized Pd nanoparticles (Pd/NCSs) have been synthesized as high-efficiency nano-catalysts, *via* fixation of Pd nanoparticles onto N-doped carbon nanospheres (NCSs), for selective and controlled H_2 generation upon additive-free HCOOH dehydrogenation. The characterization studies confirmed that Pd/NCS-800 has a homogeneous nanospherical structure, and PdNPs are stabilized onto the surface of N-doped carbon nanospheres. Pd/NCS-800 showed superior catalytic performance, with a TOF of 1640 h^{-1} , compared to Pd/NCS-700 (1456 h^{-1}) and Pd/NCS-900 (921 h^{-1}) in H_2 generation upon additive-free HCOOH dehydrogenation. The CO_2 capture test, GC analysis and tandem reaction verified that selective H_2 generation upon additive-free formic acid dehydrogenation over the Pd/NCS-800 catalyst was developed for fuel cells. Pd/NCS-800 (1640 h^{-1}) provided a 12 times larger TOF than commercial Pd/C (134 h^{-1}) in H_2 generation upon additive-free HCOOH dehydrogenation. It seemed that graphitic N/C of NCS-800 enriched the electron cloud density of the Pd atom, which was favorable for the cleavage of C–H bonds in HCOOH dehydrogenation. In addition, the selective H_2 production from additive-free HCOOH dehydrogenation over Pd/NCS-800 is successfully controlled by adjusting the pH. The strategy derived from glucose in this work might generate new ideas for the development of N-doped carbon nanospheres for selective and controlled H_2 generation.

Author contributions

Q. Zhang: investigation and formal analysis. Y. Wang and X. Jin: formal analysis. X. Liu: project administration, supervi-

sion, resources, conceptualization, and writing – original draft, review & editing.

Conflicts of interest

The authors declare no competing financial interest.

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