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## Correlation between the structural features and intrinsic activity trend of Fe surfaces for ammonia synthesis†

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The Haber–Bosch process, which was developed more than a century ago, remains the primary method for nitrogen fixation on a large scale and Fe is typically the main catalyst used in the process. Despite having been extensively studied, some anomalies regarding the activity trend across various Fe surfaces still exist. To understand the intrinsic activity trend of Fe catalysts, we utilize density functional theory (DFT) to calculate the reaction energetics on various Fe surfaces in conjunction with microkinetic analyses to examine the activity of the Fe surfaces. The catalytic activity order obtained is  $\text{Fe}(111) > \text{Fe}(211) > \text{Fe}(210) > \text{Fe}(100) > \text{Fe}(110)$ . We find that the activity trend is correlated to the barrier of the rate-determining step,  $\text{N}_2$  dissociative adsorption barrier, and perhaps more importantly to the surface energies. It is also noted that the association barriers of flat surfaces are generally larger than those of stepped surfaces, for which a clear explanation is provided.

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## 1. Introduction

Ammonia ( $\text{NH}_3$ ) is indispensable to the global economy in both industrial and agricultural production,<sup>1</sup> as well as being considered as an energy carrier<sup>2–5</sup> to play a potential role in the storage/conversion of renewable energy. The significance of ammonia motivates extensive studies in innovating and optimizing ammonia synthesis, involving thermocatalysis, electrocatalysis, photocatalysis, biocatalysis and plasma-catalytic synthesis.<sup>6–11</sup> Nevertheless, the primary industrial approach to fix nitrogen to produce  $\text{NH}_3$  is still the Haber–Bosch process (HBP), even though it is energy and capital-intensive (350–550 °C, 150–350 atm)<sup>12,13</sup> due to the stability of  $\text{N}\equiv\text{N}$ ,<sup>14</sup> consuming 2% of the total energy supply in the world and releasing more than 400 Mt of  $\text{CO}_2$ , which accounts for 3% of total global  $\text{CO}_2$  emissions.<sup>15</sup>

Although ammonia synthesis has been industrialized for more than 100 years, designing good catalysts to moderate the reaction conditions is the eternal pursuit of researchers.<sup>16–21</sup> There are mainly three types of catalysts that activate nitrogen

molecules: (i) homogeneous catalysts,<sup>22,23</sup> (ii) natural biocatalysts,<sup>24,25</sup> and (iii) heterogeneous catalysts.<sup>26–30</sup> All the existing research findings suggest that the most energy-intensive step in ammonia synthesis is either the activation of  $\text{N}_2$  or the hydrogenation of the surface intermediate species  $\text{NH}_x$  to ammonia.<sup>27</sup> It can be inferred that an ideal catalyst for ammonia synthesis should possess both a low  $\text{N}_2$  activation energy and a low  $\text{NH}_x$  hydrogenation barrier, which are difficult to realize simultaneously due to the scaling relationship on the transition metal (TM) surface. In any case, the active sites for these steps play significant and crucial roles in catalysis. Gaining an understanding of these active sites is probably one of the most essential problems in ammonia synthesis.

Somorjai and co-workers<sup>31</sup> showed clearly that ammonia synthesis was a structure-sensitive reaction by using various single crystal surfaces of Fe and reckoned that  $\text{C}_7$  sites were the active sites that exist only on  $\text{Fe}(111)$  and  $\text{Fe}(211)$ , exhibiting reaction activity:  $\text{Fe}(111) > \text{Fe}(211) > \text{Fe}(100) > \text{Fe}(210) > \text{Fe}(110)$ . Meanwhile, it is difficult to measure microscopic reaction pathways experimentally. Theoretically, the ammonia synthesis mechanism and kinetics on the  $\text{Fe}(111)$  and reconstructed  $\text{Fe}(211)$  surfaces were studied by Qian *et al.* and Fuller *et al.*, respectively.<sup>32,33</sup> At variance with common thinking, Fuller *et al.* suggested that the reconstructed  $\text{Fe}(211)$  surface is the active phase under the HBP conditions.<sup>33</sup> To further explore the active site of the Fe catalyst, Zhang *et al.*<sup>34</sup> investigated the intrinsic rate of the nitrogen reduction reaction (NNR) on each surface site exposed over bcc Fe particles, addressing the effects of intrinsic activity, the density of active sites and the particle size. Theoretical

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results showed that the activity of Fe surfaces varied, being consistent with the experiment<sup>31</sup> except Fe(100).<sup>34</sup> It is clear that these Fe surfaces deserve further investigations.

Fundamentally, the active site is generally an important concept in heterogeneous catalysis, which should lay a foundation for understanding any catalytic system. Liu and Hu<sup>35</sup> studied some typical reactions occurring on flat, stepped, and kinked metal surfaces, obtaining several rules to predict where the reaction should occur. It would be interesting to apply similar approaches to systematically study the active sites of Fe catalysts for ammonia synthesis (Fig. 1).

Thus far, there has been a lack of a correlation between the surface structure of Fe catalysts and activity of ammonia synthesis, and some puzzles regarding the different activity on various Fe surfaces have not been rationalized. In particular, the following questions remain unanswered: (i) Fe(210) and Fe(211) are structurally similar. However, why does the large difference exist in activity? (ii) Experimentally, Fe(100) was found to be more active than Fe(210) even though Fe(100) is the most inactive surface from theoretical calculations.<sup>31,34</sup> How can one rationalise these results? (iii) What are the controlling factors that influence the activity trend of Fe catalysts for ammonia synthesis?

To answer these questions, in this work we carried out a detailed density functional theory (DFT) study of ammonia synthesis on various Fe surfaces and developed a kinetic model to determine the activity trend across them. We found that the order of activity is Fe(111) > Fe(211) > Fe(210) > Fe(100) > Fe(110), which is linearly correlated with the surface energy and N<sub>2</sub> dissociative adsorption barrier. Furthermore, we examined the electronic and geometric effects and discussed our findings.

## 2. Computational methods

### 2.1 Surface model

A  $p(3 \times 3)$  supercell was constructed to calculate the elementary reactions of ammonia synthesis on various Fe

surfaces. The layer number varies; there are 6 layers for Fe(100), 5 layers for Fe(110), and 4 layers for Fe(111), Fe(210) and Fe(211), respectively. When optimizing the structure for each elementary reaction, the top 2–3 layers with the surface species were fully relaxed while the rest of the bottom layers of the surface model were fixed (see Fig. S1 in the ESI†). The thickness of the vacuum layer in the Z direction was set as 15 Å. The parameter  $k$ -point grid involved in the calculation could be determined according to the lattice parameters through the Monkhorst–Pack scheme,<sup>36</sup> typically  $2 \times 2 \times 1$   $k$ -point meshes in this case, and has been confirmed by  $k$ -point sampling tests (see Fig. S2 in the ESI†).

### 2.2 Computational details

In this work, all the calculations were performed with spin-polarized density functional theory with the Vienna *ab initio* simulation package (VASP),<sup>37</sup> using the Perdew–Burke–Ernzerhof (PBE) functional within the generalized gradient approximation (GGA).<sup>38</sup> The core–valence electron interaction was described by the project-augmented wave (PAW) method,<sup>39</sup> and the valence electronic states were expanded in the plane wave basis sets with an energy cutoff of 450 eV. The constraint optimization method<sup>40,41</sup> is adopted to search the transition state (TS) and the force convergence standard during structural optimization which is set at 0.05 eV Å<sup>−1</sup>. All the transition states were checked by vibrational frequency analysis.

### 2.3 Microkinetic modelling with/without coverage effects

According to the current consensus,<sup>18</sup> the reaction mechanism of N<sub>2</sub> and H<sub>2</sub> converting to ammonia on the surface of the Fe-based catalyst consists of the following elementary steps listed in Table 1 (\* represents the free site).  $r_i$  is the rate of reaction for reaction step  $i$  ( $i = 1, 2, \dots, 7$ ).  $k_i$  and  $k_{-i}$  are the forward rate constant and reverse rate constant, respectively. The microkinetic modelling and analyses were performed using CATKINAS.<sup>42–44</sup> While there

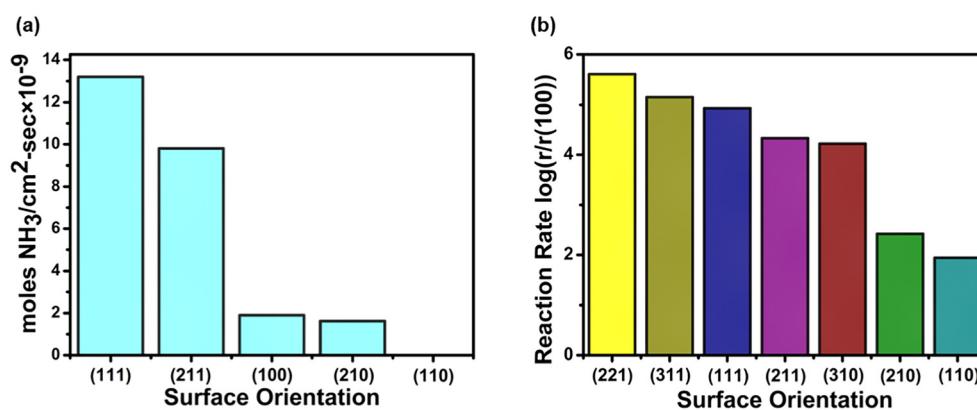


Fig. 1 Nitrogen reduction reaction activity. (a) Activity of single Fe crystal surfaces from the experimental work of Somorjai and co-workers.<sup>31</sup> Adapted with permission from ref. 31 copyright (1994) Topics in Catalysis. (b) Calculated reaction rates from the theoretical work of Li and co-workers.<sup>34</sup> Adapted with permission from ref. 34 copyright (2019) ChemCatChem. Both figures are redrawn here according to the original figures. To a large extent, both trends are similar with some differences.



**Table 1** Elementary steps and the rate equations of ammonia synthesis used in the microkinetic modelling (\* represents the free site on the surface). Details of the microkinetic software can be found in ref. 41–43

	Surface reactions	Rate equations
1	$H_2(g) + 2^* \leftrightarrow 2H^*$	$r_1 = k_1 P_{H_2} \theta^2 - k_{-1} \theta_H^2$
2	$N_2(g) + 2^* \leftrightarrow N_2^*$	$r_2 = k_2 P_{N_2} \theta_{N_2}^2 - k_{-2} \theta_{N_2}$
3	$N_2^* + * \leftrightarrow N^* + N^*$	$r_3 = k_3 \theta_{N_2} \theta^* - k_{-3} \theta_N^2$
4	$N^* + H^* \leftrightarrow NH^* + *$	$r_4 = k_4 \theta_N \theta_H - k_{-4} \theta_{NH} \theta^*$
5	$NH^* + H^* \leftrightarrow N_2^* + *$	$r_5 = k_5 \theta_{NH} \theta_H - k_{-5} \theta_{N_2} \theta^*$
6	$NH_2^* + H^* \leftrightarrow NH_3^* + *$	$r_6 = k_6 \theta_{NH_2} \theta_H - k_{-6} \theta_{NH_3} \theta^*$
7	$NH_3^* \leftrightarrow NH_3 + *$	$r_7 = k_7 \theta_{NH_3} - k_{-7} P_{NH_3} \theta^*$

are still some challenges associated with microkinetics, such as the incompatibility of non-random distribution models,<sup>45</sup> our group has developed a novel method that integrates surface coverage effects with microkinetics, which offers a valuable means to achieve the consistency between theory and experimental results.<sup>46</sup>

**With coverage effects.** The two-line model was used to quantify the dominance of the coverage effects over chemisorption energies and reaction barriers.<sup>46–49</sup> The entire coverage is determined by the sum of all the adsorbate coverages. The two-line model describes mainly how the energy of chemisorption varies at low and high coverages:

$$E_i(\theta) = \begin{cases} \sum_j (a_{i/j} \times \theta + b_{i/j}) \times \frac{\theta_j}{\theta} & \theta \leq \theta_c \\ \sum_j (a'_{i/j} \times \theta + b'_{i/j}) \times \frac{\theta_j}{\theta} & \theta > \theta_c \end{cases} \quad (1)$$

where  $\theta$ ,  $\theta_j$ ,  $i$  and  $j$  represent the total coverage, the coverage of species  $j$ , the target adsorbate  $i$ , and environmental species  $j$ , respectively.  $a$  and  $b$  are the slope and intercept of the two-line model.  $\theta_c$  is the critical point separating the low coverage from the high coverage.

The definition of the differential chemisorption energy of all species under various coverage conditions is:

$$E_{\text{ads}}^{\text{diff}} \left( \frac{\theta_N + \theta_{N-1}}{2} \right) = E_{\text{ads},N} - E_{\text{env},N-1} - E_{\text{gas}} \quad (2)$$

where  $E_{\text{ads},N}$  and  $E_{\text{env},N-1}$  are the total energy after adsorption of  $N$  adsorbates and the  $N - 1$  environmental species, respectively, and  $E_{\text{gas}}$  is the energy of the adsorbate in the gas phase.

The definition of the  $N_2$  dissociative adsorption barrier under various coverage conditions is:

$$E_a^{\text{dis}}(\theta_N) = E_{\text{TS},N} - E_{\text{env},N-2} - E_{N_2} \quad (3)$$

The turnover frequency (TOF) was calculated using a self-consistent microkinetic model shown in the scheme in Fig. S17 in the ESI† which was performed under experimental conditions with a temperature of 673 K and pressure of 20 bar.<sup>31</sup> The converged TOF and coverages for different species

at the steady-state were achieved when the convergence of coverages reaches a sufficiently low level.

**Without coverage effects.** On Fe(111) and Fe(110), the adsorption energies with a coverage of 0.04 ML were used in the coverage-independent model, whereas a coverage of 0.17 ML was employed for the dissociative adsorption barrier. They are 0.03 ML and 0.13 ML for Fe(100) and Fe(211), and 0.06 ML and 0.25 ML for Fe(210), respectively.

## 3. Results and discussion

### 3.1 Structures and energies of reaction intermediates

In order to obtain a comprehensive understanding of activity on various Fe surfaces, in this section we focus on the structures and energies of the reaction intermediates. Firstly, the surface energy<sup>50</sup> as an important property of the catalyst surface, which is difficult to quantify experimentally, was calculated in this work. The surface energy is defined as follows:

$$\gamma = \frac{dE}{S} = \frac{E - E_{\text{bulk}} \times n}{2S} \quad (4)$$

where  $E$  is the total energy;  $E_{\text{bulk}}$  is the bulk energy;  $n$  is the multiple of the number of surface atoms to the number of atoms in the bulk phase;  $S$  is the surface area. The  $\alpha$ -Fe bulk phase energy was calculated to be -8.31 eV.

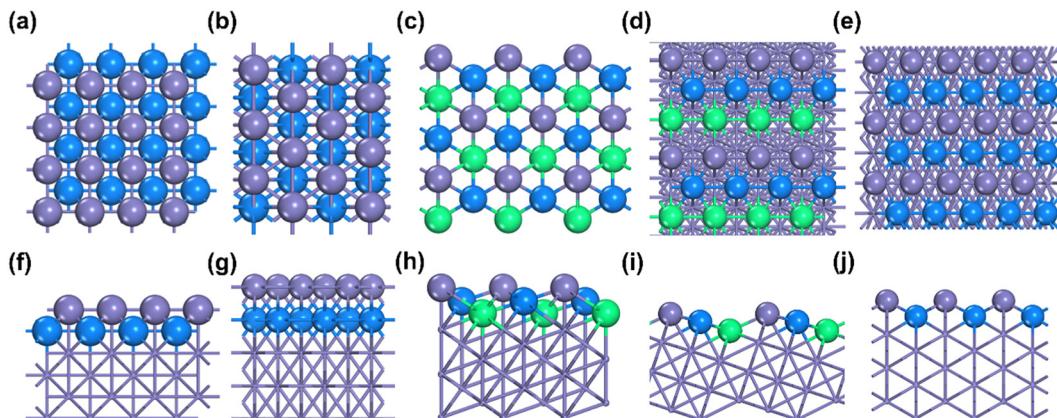
Our calculation results display that the surface energy order is Fe(111) > Fe(211) > Fe(210) > Fe(100) > Fe(110) (see Table 2), which is consistent with the trend of the literature value.<sup>16</sup> The most active surface of Fe, *i.e.*, Fe(111), has the highest surface energy, 0.166 eV, which is similar to the literature value (only 0.004 eV lower).<sup>18</sup> Not surprisingly, Fe(110) as the most inactive surface has the lowest surface energy. The structure of each Fe surface is shown in Fig. 2. As can be seen, both Fe(100) and Fe(110) are flat surfaces, while Fe(111), Fe(210) and Fe(211) possess stepped surface features.

Then the  $N_2$  adsorption was calculated. In this work, three adsorption sites of  $N_2$  were considered: top, bridge and hollow sites. After optimizations, the  $N_2$  bond length is found to be elongated from 1.115 Å to 1.277 Å, when adsorbing on the hollow site of Fe(110). It is observed that the longer the N–N bond length on the surface, the stronger the adsorption of  $N_2$ . For N, the adsorption energies on the top, bridge and hollow sites are -0.74 eV, -0.54 eV and -0.85 eV, respectively.

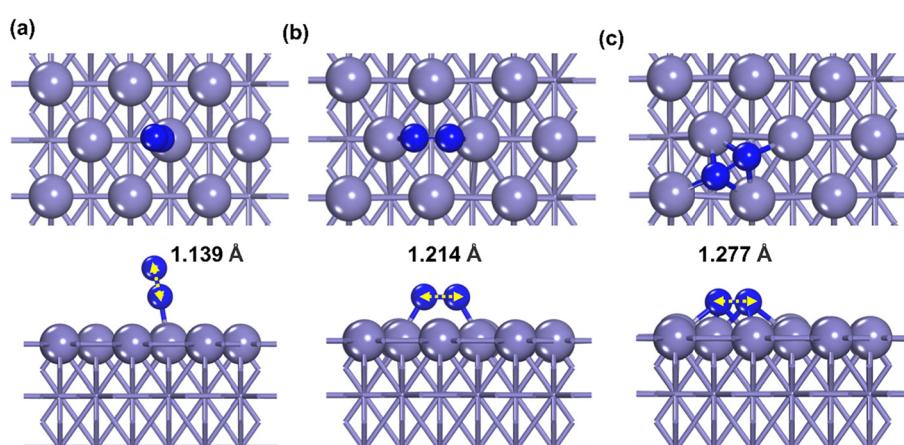
**Table 2** Surface energies of various Fe surfaces calculated versus the values in the literature. It can be seen that the agreement is good

Fe surface	$\gamma$ (eV Å <sup>-2</sup> )	The literature value <sup>16</sup>
Fe(100)	0.155	0.156
Fe(110)	0.151	0.153
Fe(111)	0.166	0.170
Fe(210)	0.156	—
Fe(211)	0.160	0.163





**Fig. 2** Top (a-e) and side (f-j) views of the optimized surface structures of Fe(100), Fe(110), Fe(111), Fe(210) and Fe(211). The Fe atoms on the top layer are grey; the second Fe atoms are blue, and the next layer is green. Grey, blue and green balls indicate the top layer, the second layer and the third layer of Fe, respectively.



**Fig. 3** Optimized structures of  $\text{N}_2$  adsorption on Fe(110). Dark blue represents the N atom. (a) Top site, (b) bridge site, and (c) hollow site. The distances between N atoms are illustrated in the figure.

**Table 3** Reaction barrier ( $E_a$ ) and enthalpy change ( $\Delta H$ ) of each elementary step in ammonia synthesis on the Fe surfaces

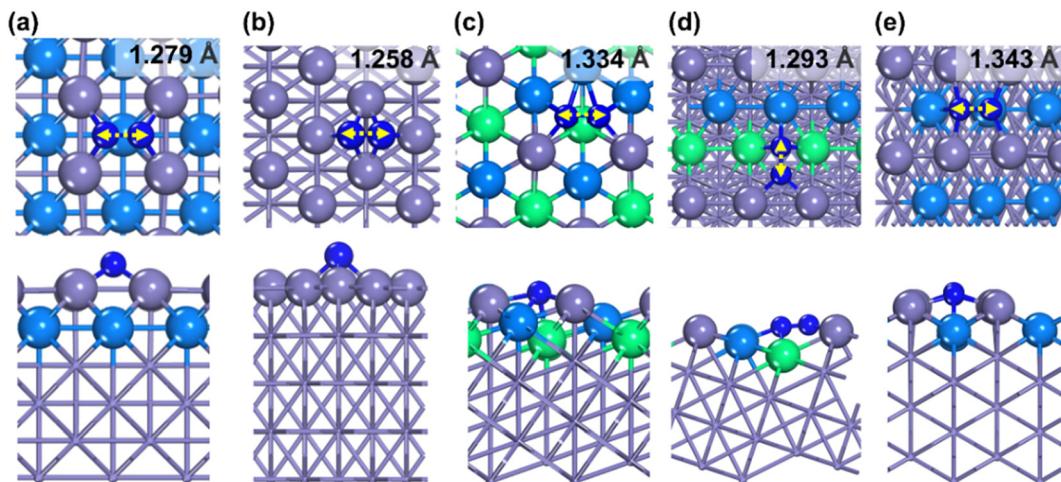
Fe surface	$\text{H}_2 + 2^* \rightleftharpoons 2\text{H}^*$		$\text{N}_2 + * \rightleftharpoons \text{N}_2^*$		$\text{N}_2^* + * \rightleftharpoons 2\text{N}^*$		$\text{N}^* + \text{H}^* \rightleftharpoons \text{NH}^* + *$		$\text{NH}^* + \text{H}^* \rightleftharpoons \text{N}_2^* + *$		$\text{NH}_2^* + \text{H}^* \rightleftharpoons \text{NH}_3^* + *$		$\text{NH}_3^* \rightleftharpoons \text{NH}_3 + *$	
	$E_a$	$\Delta H$	$E_a$	$\Delta H$	$E_a$	$\Delta H$	$E_a$	$\Delta H$	$E_a$	$\Delta H$	$E_a$	$\Delta H$	$E_a$	$\Delta H$
Fe(100)	-0.80		-0.95		1.15	-2.15	1.25	0.36	1.25	0.28	1.31	0.34		0.88
Fe(110)	-1.37		-1.02		1.34	-1.72	1.51	0.23	1.32	0.96	1.50	0.47		0.89
Fe(111)	-0.86		-0.77		0.35	-1.43	0.96	0.40	0.90	-0.03	1.04	0.09		1.05
Fe(210)	-1.35		-0.91		0.81	-1.90	1.23	0.72	1.19	0.15	1.61	0.63		1.04
Fe(211)	-1.15		-1.08		0.69	-1.22	1.20	0.47	0.88	-0.21	1.37	0.71		1.02

Because the adsorption energy on the hollow site (Fig. 3(c)) is the strongest, the hollow adsorption state was selected to be calculated for the  $\text{N}_2$  dissociation (Table 3).

Hydrogenation reactions from N to NH,  $\text{NH}_2$  and  $\text{NH}_3$  were also calculated. By a comparison of each elementary reaction among various Fe surfaces, it is found that almost all the reaction barriers follow the order: Fe(111) < Fe(211) < Fe(210) < Fe(100) < Fe(110), except the step of  $\text{NH}_2^* + \text{H}^* \rightleftharpoons \text{NH}_3^* + *$ . Surprisingly, in the last step of the

hydrogenation process the activity order changes markedly, following this order: Fe(111) < Fe(100) < Fe(211) < Fe(110) < Fe(210). As shown in Fig. 4, the bond length of nitrogen initially starts at 1.115 Å, which is lengthened after adsorption, leading to easier  $\text{N}_2$  dissociation. For the more reactive Fe(111) and Fe(211) surfaces, the N-N bond length is longer than 1.3 Å while for the less reactive Fe(100), Fe(110) and Fe(210) surfaces, the N-N bond length is less than 1.3 Å.





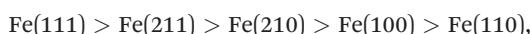
**Fig. 4** Optimized structures of  $\text{N}_2$  adsorption on (a)  $\text{Fe}(100)$ , (b)  $\text{Fe}(110)$ , (c)  $\text{Fe}(111)$ , (d)  $\text{Fe}(210)$ , and (e)  $\text{Fe}(211)$ . The distances between N atoms are illustrated in the figure.

It can be seen from Fig. 5 that  $\text{Fe}(111)$  with the highest catalytic activity has a relatively uniform arrangement of  $\text{C}_7$ . The transition state structures of the last hydrogenation step are similar except that on  $\text{Fe}(111)$ , on which nitrogen atom is only coordinated with one Fe atom, lowering the hydrogenation reaction barrier. It is worth noting that the longer the bond between the Fe atom and N atom, the easier it is for the Fe–N bond to break. Based on this observation, we can explain why the  $\text{NH}_2^* + \text{H}$  reaction barrier order is  $\text{Fe}(111) < \text{Fe}(100) < \text{Fe}(211) < \text{Fe}(110) < \text{Fe}(210)$  using the Fe–N bond length.

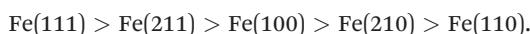
### 3.2 Kinetic analyses without coverage effects

Based on the DFT calculated energy barriers above, we carried out microkinetic simulations for ammonia synthesis in a wide range of conditions (273–873 K,  $10^{-2}$ – $10^3$  bar,  $\text{N}_2 : \text{H}_2 : \text{NH}_3 = 1 : 3 : 0.01$ ), which is similar to the work of Nørskov and co-workers.<sup>18</sup> Using the DFT energetics at low coverages (0.04 ML) from  $\text{Fe}(111)$ , we created a 2D activity heatmap depicting the TOF as a function of temperature and pressure from the microkinetic modelling, considering that the two variables can be varied independently of each other. This trend is similar on each surface; as the temperature and pressure increase, the activity is increased (Fig. 6).

To compare the relative activity of various Fe surfaces, the typical ammonia synthesis conditions (673 K, 100 bar) were chosen as an example. Under these conditions, the activity order of ammonia synthesis reaction from our simulations is



while the order from the experiment work<sup>31</sup> is



It can be seen that they are the same except the relative positions of  $\text{Fe}(210)$  vs.  $\text{Fe}(100)$ : the experimental work

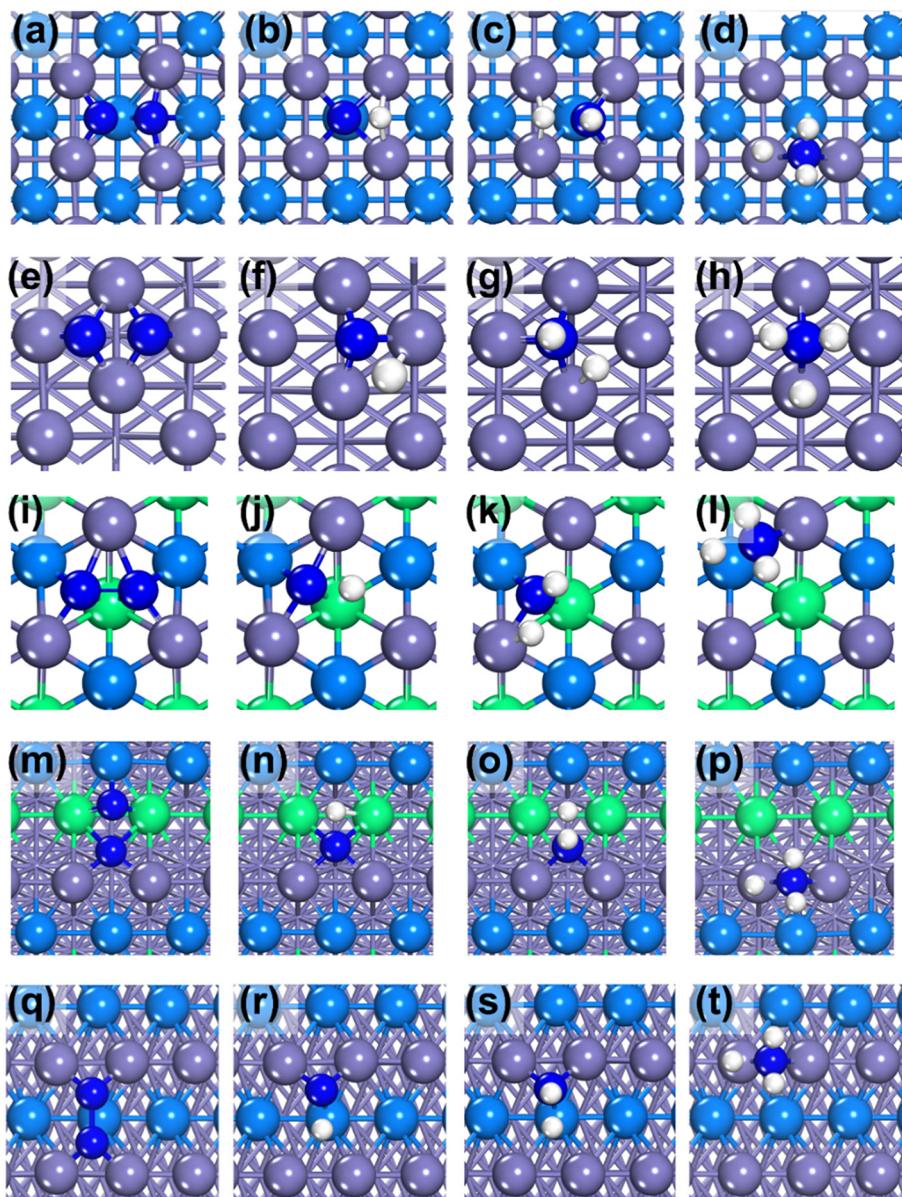
showed that  $\text{Fe}(100)$  is more active than  $\text{Fe}(210)$  while our simulations demonstrate that this is not the case. How can we understand the discrepancy between the experimental work<sup>31</sup> and our calculations for  $\text{Fe}(210)$  and  $\text{Fe}(100)$ ? At first glance, our result appears to be more reasonable:  $\text{Fe}(210)$  is a stepped-like surface while  $\text{Fe}(100)$  is a flat surface; it is expected that the stepped surface is more active than the flat surface. More analyses can confirm this (see below).

In order to understand the activity trend, we studied the rate-determining step of each Fe surface, finding that regardless of the Fe surface, R3 (dissociation of  $\text{N}_2^*$ ) is always the rate-determining step under the typical conditions (673 K, 100 bar). However, for the most active  $\text{Fe}(111)$  surface, the situation changes in the range of 600–700 K at 100 bar, which is shown in Fig. 7: R2 (adsorption of  $\text{N}_2$ ) begins to dominate the overall reaction, while R5 (hydrogenation of  $\text{NH}_2^*$ ) and R6 (hydrogenation of  $\text{NH}_2^*$ ) also play some considerable roles. This is reasonable; on active catalysts the rate-determining step is typically accelerated to prevent any single step from becoming too dominant.

As shown in Fig. 8(a) and (b), for the less reactive surfaces  $\text{Fe}(100)$ ,  $\text{Fe}(110)$  and  $\text{Fe}(210)$ ,  $\text{N}_2^*$  dissociation (R3) maintains the role of being the rate-determining step. However, for  $\text{Fe}(111)$  and  $\text{Fe}(211)$ , only in a narrower temperature range, the rate-determining step is the  $\text{N}_2^*$  dissociation. Fig. 8(c) shows that the adsorption of  $\text{N}_2$  and the  $\text{N}_2$  dissociation cancel each other largely on the reaction control degree. The result that the rate-determining step is the  $\text{N}_2$  dissociation is consistent with the fact that the overall activity order is similar to that of the  $\text{N}_2$  dissociation (Fig. 8(d)).

The relationship between the  $\text{N}_2$  dissociation barrier and TOF value of each surface is shown in Fig. 9(a). Comparing the calculated results and the experimental ones or other relevant theoretical calculations, interestingly, several differences can be found. Firstly, the activity on  $\text{Fe}(210)$  surpasses that on  $\text{Fe}(100)$ , which disagrees with experiment work, as mentioned before,<sup>31</sup> but it is consistent with the





**Fig. 5** Structures of the nitrogen dissociation transition states and step-wise hydrogenation on each Fe surface. (a–d) The structures on Fe(100), (e–h) on Fe(110), (i–l) on Fe(111), (m–p) on Fe(210), and (q–t) on Fe(211). White balls represent the H atoms.

work of Li and co-workers.<sup>34</sup> Secondly, the result that Fe(100) substitutes Fe(110) as the least activity surface<sup>34</sup> is contrary to our results and also experimental one.

To further understand the impact of the rate-determining step, we plot the relationship between  $\lg(\text{TOF})$  and the  $\text{N}_2$  dissociative adsorption barrier, as illustrated in Fig. 9(a). This shows that the  $\lg(\text{TOF})$  value declines when the  $\text{N}_2$  dissociative adsorption barrier increases, as expected. Moreover, Fig. 9(a) displays that these surfaces can be divided into two types, stepped surfaces and flat surfaces, showing clearly that the stepped surfaces are more active than the flat surfaces. It is worth mentioning that the actual activity value of Fe(211), considering the Fe(211) reconstruction, may be different.<sup>33</sup> More interestingly, the surface energy can also be linked with the  $\lg(\text{TOF})$ , as shown

in Fig. 9(b): as the surface energy rises, the  $\lg(\text{TOF})$  value increases, which is linearly correlated. Notably, the relationship between the surface energy and reaction barrier has been implicitly discussed,<sup>51</sup> supporting our results. It is worth emphasizing that the surface energy is a simple property of any surface and the observed correlation between activity and surface energy is a valuable finding for future catalyst design, particularly for catalysts having strong interactions with reactants.

### 3.3 The microkinetic modelling with coverage effects

To carry out a more quantitative comparison with the experimental values, we performed microkinetic simulations on the most active Fe(111) surface at 673 K



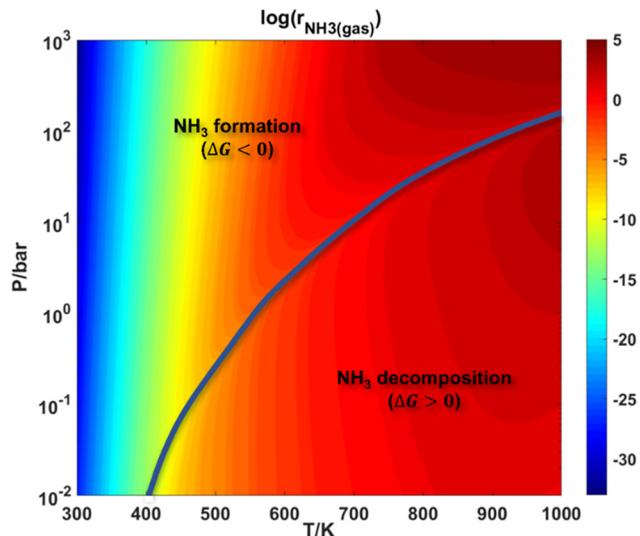


Fig. 6 2D activity ( $\lg(\text{TOF})$ ) heatmap of Fe(111) calculated at 273–873 K,  $10^{-2}$ – $10^3$  bar,  $\text{N}_2:\text{H}_2:\text{NH}_3 = 1:3:0.01$ . The line illustrates the boundary between the  $\text{NH}_3$  formation and  $\text{NH}_3$  decomposition.

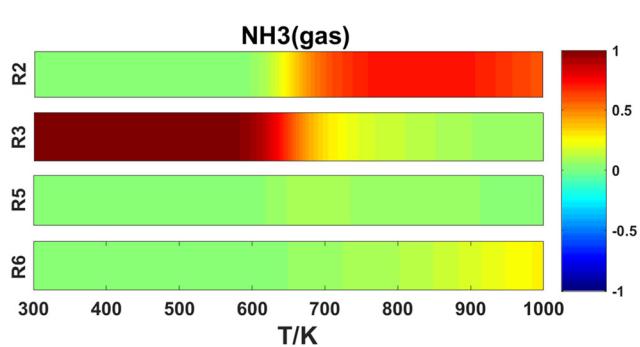


Fig. 7 Degree of rate control from microkinetic simulations on Fe(111) under the condition of 100 bar. Reactions R2, R3, R5 and R6 are listed in Table 1.

and 20 bar ( $\text{N}_2:\text{H}_2:\text{NH}_3 = 1:3:0.01$ , an experimental condition<sup>31</sup>), by taking the coverage effects into account. All the interactions of reaction intermediates ( $\text{H}^*$ ,  $\text{N}^*$ ,  $\text{NH}^*$ ,  $\text{NH}_2^*$  and  $\text{NH}_3^*$ ), including self-interactions and cross-interactions of these surface species, were considered in the coverage-dependent kinetic simulations. In order to achieve good accuracy, we carefully calculated many structures of surface species co-adsorption at each coverage, and the most stable energy at the specific coverage was used in the kinetic modelling (see Fig. S5–S9 in the ESI†). To ensure feasibility in our calculations, we only considered the coverage effects of all the species on the  $\text{N}_2$  dissociative adsorption barrier, which is the rate-determining step.

For the coverage effects on adsorption states, both self and cross adsorbate–adsorbate interactions of all reaction intermediates are studied (see sections S3 and S5 in the ESI†). Furthermore, the transition state energies, another critical factor, were explicitly calculated considering the coverage effects, which were found to be divided into two

distinct categories (see Fig. S16 in the ESI†). Specifically, the  $\text{N}_2$  dissociative adsorption barriers are hardly influenced by the coverage and remain nearly constant at low coverages. However, at high coverages, these barriers show an increasing trend as the total coverage is increased. Therefore, the  $\text{N}_2$  dissociative adsorption barriers can be described by a two-line model as a function of the total coverage. All the slopes and intercepts of the interaction between the transition state and environmental species are listed in Table S3 in the ESI†.

By using the self- and cross-interactions to correct the adsorption energies and  $\text{N}_2$  dissociative adsorption barrier, the coverage distribution on Fe(111) at the steady-state is obtained: 0.99 ML, containing 0.51 ML of N, 0.39 ML of  $\text{NH}_2$ , 0.05 ML of H and 0.04 ML of others ( $\text{NH}$  and  $\text{NH}_3$ ) (Fig. 10). The TOF calculated by the coverage-dependent model is  $3.6 \text{ s}^{-1}$  per site, in excellent agreement with the experimental result of  $\text{TOF} = 11.1 \text{ s}^{-1}$  per site.

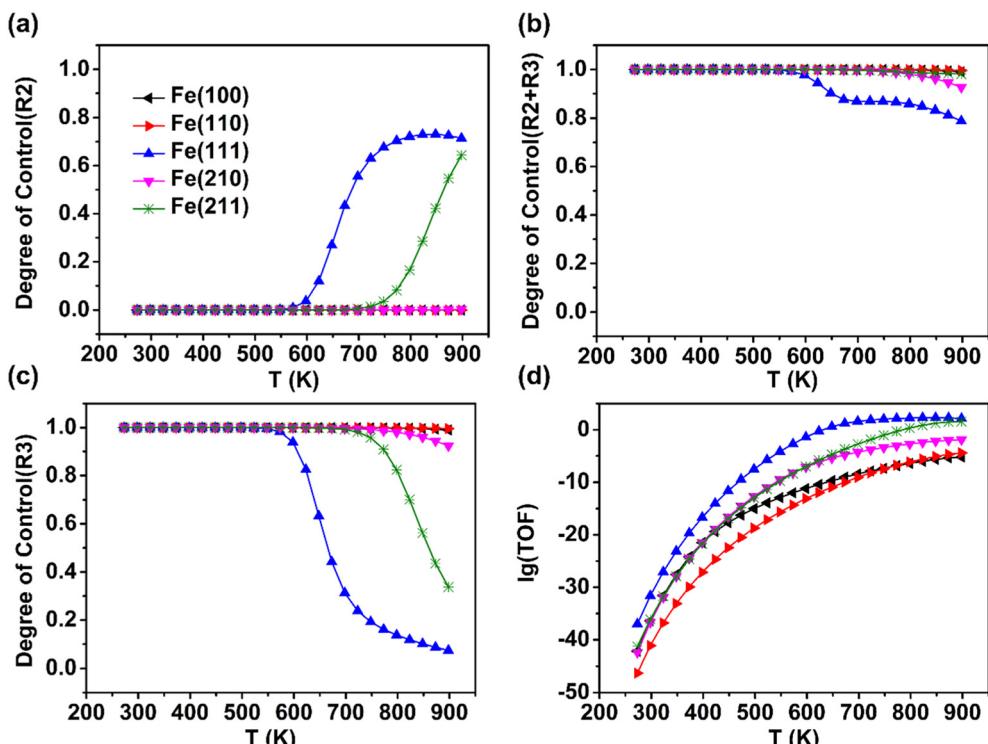
To simplify the calculations, we applied the coverage effects of Fe(111) to other Fe surfaces. The new activity, considering the coverage effects, was compared with the original activity at low coverages, as shown in Fig. 11, which indicates that the new activity trend with the coverage effects is consistent with the original coverage-independent results. We also replotted the relationships between  $\lg(\text{TOF})$  from the microkinetic modelling with the coverage effects and  $\text{N}_2$  dissociative adsorption barrier/surface energy. As can be seen in Fig. S18 in the ESI† linear correlations are apparent, which is similar to the results from the coverage-independent modelling (Fig. 9).

### 3.4 Energy decomposition

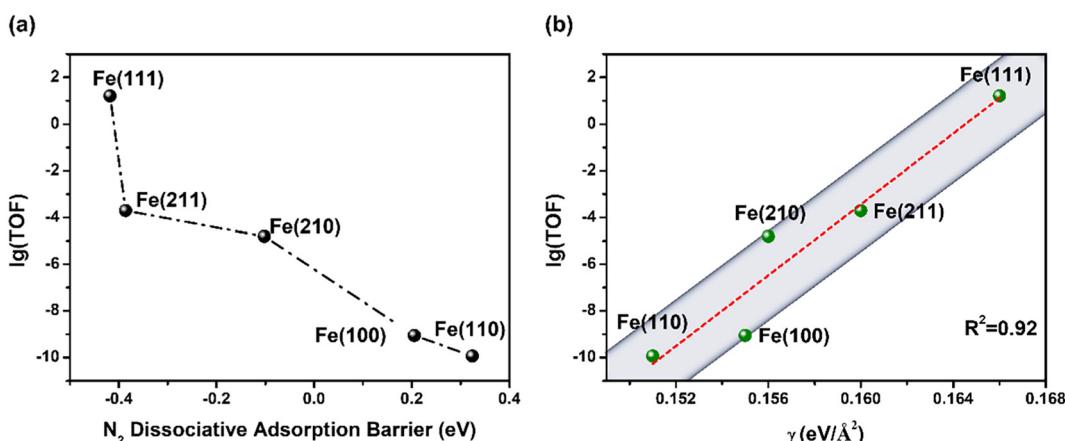
Fe(111), Fe(211) and Fe(210) are all stepped surfaces that exhibit good activity. However, there are differences in their activity levels. To further understand the activity differences of these surfaces, we performed detailed analyses on the reaction energies: the energy barrier decompositions on Fe(111), Fe(211) and Fe(210) were carried out. For the  $\text{N}_2$  dissociation reaction, starting from an  $\text{N}_2$  molecule in the gas phase to the adsorbed  $\text{N}_A$  and  $\text{N}_B$  atoms on the surface  $\text{N}_2(\text{g}) \rightarrow \text{N}_A^* + \text{N}_B^*$ , we decomposed the energies of adsorbed atoms at the transition state ( $E^{\text{TS}}$ ) and the final state ( $E^{\text{FS}}$ ) as eqn (5)–(7), where  $E_A^{\text{TS}}$  and  $E_B^{\text{TS}}$  are the adsorption energies of individual species  $\text{N}_A$  and  $\text{N}_B$  at the transition state. The adsorption energies of adsorbed species  $\text{N}/\text{N}_2$  are defined by referring to the clean surface and gaseous  $\text{N}_2$ , and  $E_{\text{int}}^{\text{TS}}$  is the repulsion energy between  $\text{N}_A$  and  $\text{N}_B$  at the transition state, which is a quantitative measure of the geometrical effect on the surfaces. Similarly,  $E_A^{\text{FS}}$ ,  $E_B^{\text{FS}}$  and  $E_{\text{int}}^{\text{FS}}$  represent the corresponding energies at the final state. Hence, the barrier of  $\text{N}_2$  dissociation ( $E_a^{\text{dis}}$ ) and association process ( $E_a^{\text{as}}$ ) can be expressed as:<sup>35</sup>

$$E_a^{\text{dis}} = E^{\text{TS}} = E_A^{\text{TS}} + E_B^{\text{TS}} + E_{\text{int}}^{\text{TS}} \quad (5)$$

$$E_a^{\text{as}} = E_A^{\text{FS}} + E_B^{\text{FS}} + E_{\text{int}}^{\text{FS}} \quad (6)$$



**Fig. 8** Degree of rate control as a function of temperature under industrial reaction conditions ( $P = 100$  bar); (a)  $N_2$  adsorption (R2); (b)  $N_2^*$  dissociation (R3); (c)  $N_2$  dissociative adsorption (R2 + R3). (d) TOF against temperature.



**Fig. 9** Coverage-independent kinetic modelling. (a) Relationship between  $\lg(\text{TOF})$  and the  $N_2$  dissociative adsorption barrier. (b) Relationship between  $\lg(\text{TOF})$  and the surface energy.

$$E_a^{\text{as}} = E^{\text{TS}} - E^{\text{FS}} = (E_A^{\text{TS}} + E_B^{\text{TS}}) - (E_A^{\text{FS}} + E_B^{\text{FS}}) + E_{\text{int}}^{\text{TS}} - E_{\text{int}}^{\text{FS}} \quad (7)$$

where  $E_{\text{int}}^{\text{FS}}$ , under the reaction conditions we studied (low coverages), is normally very small.

The individual energy components of  $N_2$  dissociation on the Fe stepped surfaces are listed in Table 4, and the FS chemisorption energies are also listed for comparison. Since the  $E_A^{\text{TS}}$  and  $E_B^{\text{TS}}$  mostly depend on their bonding ability to the Fe surface, which is determined by the electronic properties of the local metal, it can be suggested that  $E_A^{\text{TS}}$  and  $E_B^{\text{TS}}$  are correlated to their FS counterparts.

By comparing these terms, the following features can be identified:

i. For  $N_2$  dissociation on Fe(111), it not only exhibits a high electron effect ( $-1.52$  eV), but also a low geometrical effect ( $1.10$  eV), resulting in the highest activity.

ii. Fe(210) has the highest electron effect ( $-1.68$  eV) but shows the lowest activity among the stepped surfaces due to its relatively large geometrical effect ( $1.58$  eV), as shown in Fig. 5(m-p). Its surface structure is a combination of Fe(100) and Fe(110), which leads to a strong geometrical effect.



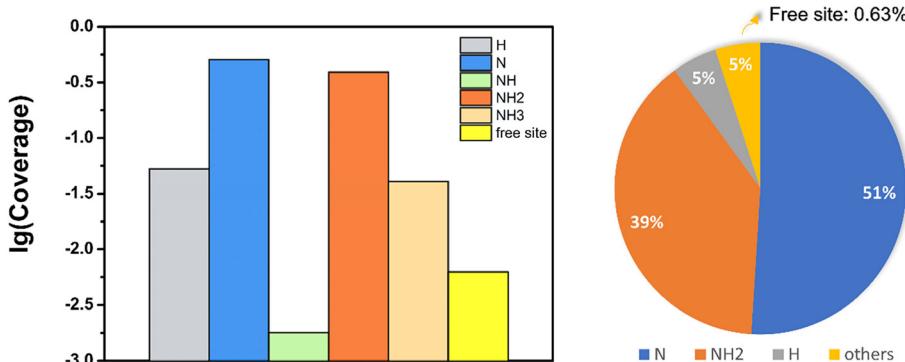


Fig. 10 Surface coverages at the steady state for the NNR on Fe(111) using the coverage-dependent methods at 673 K and 20 bar ( $N_2 : H_2 : NH_3 = 1 : 3 : 0.01$ , an experimental condition); others including NH, NH<sub>3</sub> and the free site.

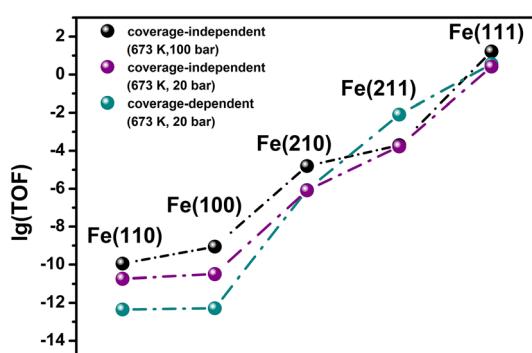


Fig. 11 Activity trend of various Fe surfaces with the coverage effects and the one from the low coverages.

iii. While the electron effect of  $N_2$  dissociation on Fe(211) may not be as strong as the former two, the weak geometrical effect of Fe(211) (0.82 eV) results in a lower dissociative barrier compared to Fe(210).

We also did the following analyses on the observation that the association barriers of flat surfaces are larger than those of stepped surfaces (the average values of  $E_a^{as}$  are 1.73 eV and 3.02 eV for stepped surfaces and flat surfaces, respectively): according to the definitions of the dissociative ( $E_a^{dis}$ ) and associative energy barriers ( $E_a^{as}$ ), the relationship is:

$$E_a^{as} = E_a^{dis} - \Delta H \quad (8)$$

while the BEP relationship for the dissociation barrier is

Table 4 Energy decompositions for the rate-determining step ( $N_2 + * \rightleftharpoons 2N^*$ ) on stepped surfaces (SE stands for the sum of  $E_A$  and  $E_B$ )

$N_2 + *$ $\rightleftharpoons 2N^*$		$E_A$ (eV)	$E_B$ (eV)	SE (eV)	$E_{int}$ (eV)	$E_a^{dis}$ (eV)	$E_a^{as}$ (eV)
Fe(111)	TS	-0.76	-0.76	-1.52	1.10	-0.42	1.20
	FS	-0.82	-0.83	-1.65	0.03	-0.39	
Fe(211)	TS	-0.61	-0.60	-1.21	0.82	-0.39	1.65
	FS	-0.91	-0.88	-1.79	-0.25	-0.10	
Fe(210)	TS	-0.66	-1.03	-1.68	1.58	-0.10	2.34
	FS	-0.94	-1.36	-2.31	-0.13	-0.13	

$$E_a^{dis} = \alpha \Delta H + \beta \quad (9)$$

where  $\alpha$  is closed to 1.<sup>52-54</sup> Combining these two equations, we can deduce:

$$E_a^{as} = E_a^{dis} - \Delta H = (\alpha - 1) \Delta H + \beta \approx \beta \quad (10)$$

In general, the values of  $\beta$  for flat surfaces are larger than those of stepped surfaces, which explains the observation mentioned above. Nørskov and co-workers<sup>55</sup> studied the BEP relationship between the transition state energy and the dissociative chemisorption energy of nitrogen on the (211) surface of pure transition metals all having the fcc crystal structure, concluding that the best fit for  $\beta$  is 1.61 eV, which is close to our result, 1.65 eV.

## 4. Conclusion

In summary, nitrogen reduction reactions on various Fe surfaces have been systematically studied by DFT calculations together with microkinetic simulations, aiming at figuring out the correct activity trend of these surfaces and solving the existing puzzle in the literature. The main findings are as follows:

i. The activity order of various Fe surfaces was determined to be Fe(111) > Fe(211) > Fe(210) > Fe(100) > Fe(110). It is worth mentioning that this study primarily focuses on the intrinsic activity trends of Fe catalysts. Surface reconstruction, although it may occur in real experiments, has not been considered in this work.

ii. The above activity order was found to be related to the rate-determining step barrier, which is the  $N_2$  dissociative adsorption barrier, as expected. However, the finding that there is a good linear correlation between the activity order and the surface energy is slightly surprising but understandable. Hence, the surface energy of a catalyst may serve as a good indicator of activity of the catalysts especially when the rate-determining step is the dissociation of the reactants and might be of general importance in heterogeneous catalysis.

iii. For a more quantitative comparison with the experimental values, a coverage-dependent microkinetic



modeling for the NNR on Fe(111) using DFT energetics was carried out under the experimental conditions (673 K, 20 bar,  $\text{N}_2 : \text{H}_2 : \text{NH}_3 = 1:3:0.01$ ), from which the calculated TOF is  $3.6 \text{ s}^{-1}$  per site, in good agreement with the experimental results ( $11.1 \text{ s}^{-1}$  per site). Furthermore, we applied the surface coverage effects on Fe(111) to other Fe surfaces as an approximation. The activity trend of various Fe surfaces considering the coverage effects we obtained remains the same as the coverage-independent model.

iv. The  $\text{N}_2$  dissociative adsorption barriers were decomposed into electronic and geometrical effects to illustrate the differences in activity. Fe(111) exhibits the highest activity due to its strong electron effect and weak geometrical effect. In contrast, Fe(210) has the strongest electron effect but shows the lowest activity among the stepped surfaces due to its relatively large geometrical effect.

v. The association barriers of flat surfaces are larger than those of stepped surfaces. We deduced that  $E_a^{\text{as}}$  is approximately equal to  $\beta$  by combining the definition of the association barriers and the BEP relationship for the dissociation barrier, which can provide an understanding of the result: the  $\beta$  values from the flat surfaces are larger than those of stepped surfaces.

## Conflicts of interest

The authors declare no competing financial interest.

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## References

- 1 J. W. Erisman, M. A. Sutton, J. Galloway, Z. Klimont and W. Winiarwarter, *Nat. Geosci.*, 2008, **1**, 636–639.
- 2 A. Valera-Medina, H. Xiao, M. Owen-Jones, W. I. F. David and P. J. Bowen, *Prog. Energy Combust. Sci.*, 2018, **69**, 63–102.
- 3 A. Klerke, C. H. Christensen, J. K. Nørskov and T. Vegge, *J. Mater. Chem.*, 2008, **18**(20), 2285–2392.
- 4 C. Zamfirescu and I. Dincer, *Fuel Process. Technol.*, 2009, **90**, 729–737.
- 5 C. H. Christensen, T. Johannessen, R. Z. Sørensen and J. K. Nørskov, *Catal. Today*, 2006, **111**, 140–144.
- 6 N. J. Weise, F. Parmeggiani, S. T. Ahmed and N. J. Turner, *J. Am. Chem. Soc.*, 2015, **137**, 12977–12983.
- 7 Q. Wang, J. Guo and P. Chen, *J. Energy Chem.*, 2019, **36**, 25–36.
- 8 J. Shah, J. Harrison and M. Carreon, *Catalysts*, 2018, **8**, 437.
- 9 J. H. Montoya, C. Tsai, A. Vojvodic and J. K. Norskov, *ChemSusChem*, 2015, **8**, 2180–2186.
- 10 R. Hawtow, S. Ghosh, E. Guarr, C. Xu, R. M. Sankaran and J. N. Renner, *Sci. Adv.*, 2019, **5**, eaat5778.
- 11 X. Chen, N. Li, Z. Kong, W.-J. Ong and X. Zhao, *Mater. Horiz.*, 2018, **5**, 9–27.
- 12 S. Klinsrisuk, S. Tao and J. T. S. Irvine, in *Membrane Reactors for Energy Applications and Basic Chemical Production*, 2015, pp. 543–563, DOI: [10.1016/b978-1-78242-223-5.00018-2](https://doi.org/10.1016/b978-1-78242-223-5.00018-2).
- 13 S. L. Foster, S. I. P. Bakovic, R. D. Duda, S. Maheshwari, R. D. Milton, S. D. Minteer, M. J. Janik, J. N. Renner and L. F. Greenlee, *Nat. Catal.*, 2018, **1**, 490–500.
- 14 H. P. Jia and E. A. Quadrelli, *Chem. Soc. Rev.*, 2014, **43**, 547–564.
- 15 S. Chen, S. Perathoner, C. Ampelli and G. Centi, in *Horizons in Sustainable Industrial Chemistry and Catalysis*, 2019, pp. 31–46, DOI: [10.1016/b978-0-444-64127-4.00002-1](https://doi.org/10.1016/b978-0-444-64127-4.00002-1).
- 16 A. Vojvodic, A. J. Medford, F. Studt, F. Abild-Pedersen, T. S. Khan, T. Bligaard and J. K. Nørskov, *Chem. Phys. Lett.*, 2014, **598**, 108–112.
- 17 B. H. R. Suryanto, H.-L. Du, D. Wang, J. Chen, A. N. Simonov and D. R. MacFarlane, *Nat. Catal.*, 2019, **2**, 290–296.
- 18 A. R. Singh, J. H. Montoya, B. A. Rohr, C. Tsai, A. Vojvodic and J. K. Nørskov, *ACS Catal.*, 2018, **8**, 4017–4024.
- 19 R. Michalsky, P. H. Pfromm and A. Steinfeld, *Interface Focus*, 2015, **5**, 20140084.
- 20 H. Liu, *Chin. J. Catal.*, 2014, **35**, 1619–1640.
- 21 J. Fuller, Q. An, A. Fortunelli and W. A. Goddard, *Acc. Chem. Res.*, 2022, **55**, 1124–1134.
- 22 R. R. Schrock, *Acc. Chem. Res.*, 2005, **38**, 955–962.
- 23 E.-Y. Jeong, C.-Y. Yoo, C. H. Jung, J. H. Park, Y. C. Park, J.-N. Kim, S.-G. Oh, Y. Woo and H. C. Yoon, *ACS Sustainable Chem. Eng.*, 2017, **5**, 9662–9666.
- 24 H.-B. Wang, J.-Q. Wang, R. Zhang, C.-Q. Cheng, K.-W. Qiu, Y.-J. Yang, J. Mao, H. Liu, M. Du, C.-K. Dong and X.-W. Du, *ACS Catal.*, 2020, **10**, 4914–4921.
- 25 T. Spatzal, K. A. Perez, O. Einstle, J. B. Howard and D. C. Rees, *Science*, 2014, **345**, 1620–1623.
- 26 P. Wang, F. Chang, W. Gao, J. Guo, G. Wu, T. He and P. Chen, *Nat. Chem.*, 2017, **9**, 64–70.
- 27 Y. Tsuji, M. Kitano, K. Kishida, M. Sasase, T. Yokoyama, M. Hara and H. Hosono, *Chem. Commun.*, 2016, **52**, 14369–14372.
- 28 B. Lin, Y. Qi, K. Wei and J. Lin, *RSC Adv.*, 2014, **4**, 38093–38102.
- 29 M. Kitano, Y. Inoue, Y. Yamazaki, F. Hayashi, S. Kanbara, S. Matsuishi, T. Yokoyama, S. W. Kim, M. Hara and H. Hosono, *Nat. Chem.*, 2012, **4**, 934–940.
- 30 L. M. Azofra, N. Morlanes, A. Poater, M. K. Samantaray, B. Vidjayacoumar, K. Albahily, L. Cavallo and J. M. Basset, *Angew. Chem. Int. Ed.*, 2018, **57**, 15812–15816.
- 31 G. A. Somorjai and N. Materer, *Top. Catal.*, 1994, **1**, 215–231.
- 32 J. Qian, Q. An, A. Fortunelli, R. J. Nielsen and W. A. Goddard, *J. Am. Chem. Soc.*, 2018, **140**, 6288–6297.
- 33 J. Fuller, A. Fortunelli, W. A. Goddard III and Q. An, *Phys. Chem. Chem. Phys.*, 2019, **21**, 11444–11454.
- 34 B. Y. Zhang, H. Y. Su, J. X. Liu and W. X. Li, *ChemCatChem*, 2019, **11**, 1928–1934.
- 35 Z. P. Liu and P. Hu, *J. Am. Chem. Soc.*, 2003, **125**, 1958–1967.
- 36 H. J. Monkhorst and J. D. Pack, *Phys. Rev. B: Solid State*, 1976, **13**, 5188–5192.
- 37 G. Kresse and J. Furthmüller, *Phys. Rev. B: Condens. Matter*, 1996, **54**, 11169–11186.



- 38 J. P. Perdew, A. Ruzsinszky, G. I. Csonka, O. A. Vydrov, G. E. Scuseria, L. A. Constantin, X. Zhou and K. Burke, *Phys. Rev. Lett.*, 2008, **100**, 136406.
- 39 G. Kresse and D. Joubert, *Phys. Rev. B: Condens. Matter Mater. Phys.*, 1999, **59**, 1758–1775.
- 40 A. Michaelides and P. Hu, *J. Am. Chem. Soc.*, 2000, **122**, 9866–9867.
- 41 A. Alavi, P. Hu, T. Deutsch, P. L. Silvestrelli and J. Hutter, *Phys. Rev. Lett.*, 1998, **80**, 3650–3653.
- 42 W. Xie, J. Xu, J. Chen, H. Wang and P. Hu, *Acc. Chem. Res.*, 2022, **55**, 1237–1248.
- 43 J.-F. Chen, Y. Mao, H.-F. Wang and P. Hu, *ACS Catal.*, 2016, **6**, 7078–7087.
- 44 J. Chen, M. Jia, P. Hu and H. Wang, *J. Comput. Chem.*, 2021, **42**, 379–391.
- 45 N. K. Razdan and A. Bhan, *Proc. Natl. Acad. Sci. U. S. A.*, 2021, **118**(8), e2019055118.
- 46 W. Xie and P. Hu, *Catal. Sci. Technol.*, 2021, **11**, 5212–5222.
- 47 C. Guo, Y. Mao, Z. Yao, J. Chen and P. Hu, *J. Catal.*, 2019, **379**, 52–59.
- 48 Y. Ding, Y. Xu, Y. Song, C. Guo and P. Hu, *J. Phys. Chem. C*, 2019, **123**, 27594–27602.
- 49 A. C. Lausche, A. J. Medford, T. S. Khan, Y. Xu, T. Bligaard, F. Abild-Pedersen, J. K. Nørskov and F. Studt, *J. Catal.*, 2013, **307**, 275–282.
- 50 N. E. Singh-Miller and N. Marzari, *Phys. Rev. B: Condens. Matter Mater. Phys.*, 2009, **80**, 235407.
- 51 Q. An, M. McDonald, A. Fortunelli and W. A. Goddard, *ACS Nano*, 2021, **15**, 1675–1684.
- 52 S. Wang, B. Temel, J. Shen, G. Jones, L. C. Grabow, F. Studt, T. Bligaard, F. Abild-Pedersen, C. H. Christensen and J. K. Nørskov, *Catal. Lett.*, 2010, **141**, 370–373.
- 53 A. Vojvodic, F. Calle-Vallejo, W. Guo, S. Wang, A. Toftlund, F. Studt, J. I. Martinez, J. Shen, I. C. Man, J. Rossmeisl, T. Bligaard, J. K. Nørskov and F. Abild-Pedersen, *J. Chem. Phys.*, 2011, **134**, 244509.
- 54 A. Logadottir, T. H. Rod, J. K. Nørskov, B. Hammer, S. Dahl and C. J. H. Jacobsen, *J. Catal.*, 2001, **197**, 229–231.
- 55 T. R. Munter, T. Bligaard, C. H. Christensen and J. K. Nørskov, *Phys. Chem. Chem. Phys.*, 2008, **10**, 5202–5206.

