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# Reactivity of presolvated and solvated electrons with CO<sub>2</sub> in water up to 118 bar at 298 and 308 K†

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The reactivity of electrons in the CO<sub>2</sub>-water system was evaluated through picosecond electron pulse radiolysis at different gas pressures (ranging from 1 to 118 bar) and temperatures (25 and 35 °C) coupled with UV-vis transient spectroscopy. A custom-made spectroscopic cell was utilized for these experiments, which allowed for regulation of temperature and pressure. The scavenging of electrons was measured directly at gas pressures even in the supercritical state, and the results showed a non-monotonic dependence of electron reactivity with CO<sub>2</sub> concentration, in agreement with the changing molar concentration of CO<sub>2</sub> in water under varying pressure.

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## 1 Introduction

The capture and subsequent chemical transformation of CO<sub>2</sub> is a global issue. There are several ways to reduce it: electrochemical, photochemical, *e.g.*, the use of a hydrated electron ( $e_{\text{hyd}}^-$ ), which is the most reducing species in solution (standard reduction potential of  $-2.9$  V NHE), is one of the effective approaches for CO<sub>2</sub>/CO<sub>2</sub><sup>•-</sup> ( $-2.14$  V NHE) reduction without using any catalyst at room temperature. Although electrochemical<sup>1</sup> and photoelectrochemical<sup>2</sup> approaches have been developed to reduce CO<sub>2</sub> using  $e_{\text{hyd}}^-$  chemistry, their faradaic efficiency remains low. A promising alternative method involves the use of high-energy ionizing radiation to generate reducing radicals directly in water at room temperature. This method eliminates the need for a catalyst but requires appropriate chemical conditions to maximize CO<sub>2</sub> conversion yield.<sup>3</sup> A better understanding of CO<sub>2</sub> reduction processes may lead to the development of methods for reducing carbon dioxide emissions by converting it into useful compounds or energy.

This study extends previous research<sup>4</sup> by investigating the reactivity of electrons dissolved in a CO<sub>2</sub>-water solution at increased pressure (1 to 118 bar) and temperature (25, 35 °C) using picosecond electron pulse radiolysis. Unlike the previous work, which only covered pressures up to 52 bar, this study expands the analysis to include measurements of reaction rate in the supercritical state of CO<sub>2</sub> ( $P = 72.9$  bar,  $T = 30.85$  °C) in

water. It is important to clarify that the measurements were conducted in water with dissolved CO<sub>2</sub> gas. Throughout all experimental conditions, the water was not in a supercritical state; rather, the CO<sub>2</sub> existed as a separate phase on top of the water as a gas, liquid, and supercritical liquid, respectively, of the pressure.

## 2 Experimental

### 2.1 Pulse radiolysis setup

The ELYSE picosecond pulse radiolysis facility at the Institute de Chimie Physique, Université Paris-Saclay was used to track the formation yields and decay kinetics of solvated electrons,  $e_s^-$ . We employed a pulse-probe setup with a broad supercontinuum probe and charge-coupled device (CCD) detection for transient absorption measurements. The absorption measurements in the near-UV to visible region were conducted using a configuration previously detailed in ref. 4 The setup included a supercontinuum generated by focusing a laser source (@790 nm, 1 μJ into a CaF<sub>2</sub> disk. The electron pulses were delivered at a repetition frequency of 5 Hz, with an electron energy of 6–8 MeV, a charge of 6 nC, and an average dose per pulse of 100 Gy<sup>4–6</sup> This setup enabled the recording of the entire transient spectra between 350–780 nm, independent of shot-to-shot fluctuations and long-term drifts of the electron source.<sup>4–6</sup>

The experimental setup is illustrated in Fig. 1S (ESI†), using a schematic illustration. The setup comprises a high-pressure cell filled with distilled water (1.5 ml) to approximately 3/4 of its capacity. CO<sub>2</sub> gas is introduced into the cell at high pressure through a single channel, regulated by a NEM-B207-01D syringe pump, CETONI GmbH. The system has a pressure capacity of

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up to 200 bar. However, the highest reached value in our was 120 bar for safety reason. The measurements taken in a static cell were compared to those taken in a circulating solution under the same thermodynamic conditions and the results were found to be similar. As a result, all subsequent studies were conducted in a static solution. The high-pressure cell was maintained at a regulated temperature using a MINISTAT CC Cryothermostat, which was monitored by an RTD-100 sensor and an Agilent 34411A Digital Multimeter. Temperature was regulated using a closed water loop. The system was thermodynamically equilibrated for 30 minutes after the gas pressure was applied before the measurement.

The production of a hydrated electron,  $e_{\text{hyd}}^-$ , following a 7 ps electron pulse is associated with the scavenging of the pre-solvated electron,  $e_{\text{pre}}^-$ , by the solute. The degree of scavenging of  $e_{\text{pre}}^-$  during the pulse duration increases with decreasing  $e_{\text{hyd}}^-$  production. The reactivity of  $e_{\text{pre}}^-$  with the solute can be determined by adjusting the solute concentration, and is commonly expressed as the  $C_{37}$  value, which represents the solute concentration at which 37% of the initial  $e_{\text{hyd}}^-$  remains.<sup>7,8</sup> The  $C_{37}$  value is an useful comparative parameter for describing the ultrafast long-range reactions such as  $e_{\text{pre}}^-$  with solutes. The radiolytic yield of  $e_{\text{hyd}}^-$  in the studied water-CO<sub>2</sub> solution was calculated using eqn (1)–(2) provided in a previous study.<sup>4</sup> The equations are explained in the supplementary information, ESI†

The dose deposited per pulse was determined from the measurements of the absorbance of  $e_{\text{hyd}}^-$  ( $A_{e_{\text{aq}}^-}(\lambda, t)$ ) in neat water and verified before each series of experiments, considering the initial yield of the solvated electrons, measured at 10 ps, to be  $G_{10\text{ps}} = 4.4 \times 10^{-7} \text{ mol J}^{-1}$ .<sup>5,7</sup>

Table S1 and S2 (ESI†) present the calculated dose factor  $F$  for 25 °C and 35 °C respectively. The energy absorption of ionizing radiation is influenced by the quantity of electrons in the substance. At low concentrations of dissolved material, the solvent absorbs most of the energy. However, in highly concentrated solutions, the dissolved substance start to absorb significant amount of the energy, resulting in an increase in excess electron production with increasing CO<sub>2</sub> concentrations. In this way, the yield of the excess electron is altered in the presence of high CO<sub>2</sub> concentration by less than 2%.

### 3 Results and discussion

The absorption of the  $e_{\text{hyd}}^-$  in solutions of CO<sub>2</sub> was measured by pump-probe spectroscopy in subnano- and nanosecond timescale, in order to determine the reactivity of  $e_{\text{pre}}^-$  and  $e_{\text{hyd}}^-$  with CO<sub>2</sub> at two different temperatures, 25 °C and 35 °C (Fig. 1).

The dependence of the pulse radiolysis data of the water-CO<sub>2</sub> system demonstrates similar behavior for normal and supercritical state (for  $P > 63$  bar and  $T = 35$  °C). With pressure increase the lifetime of  $e_{\text{hyd}}^-$  drops down (the observed rate of its disappearance increases, Fig. 1, 2) and the initial formation yield of  $e_{\text{hyd}}^-$  decreases (Fig. 3).

As the pressure of CO<sub>2</sub> increases, its concentration in water also increases. The solubility of CO<sub>2</sub> is known to exhibit a non-

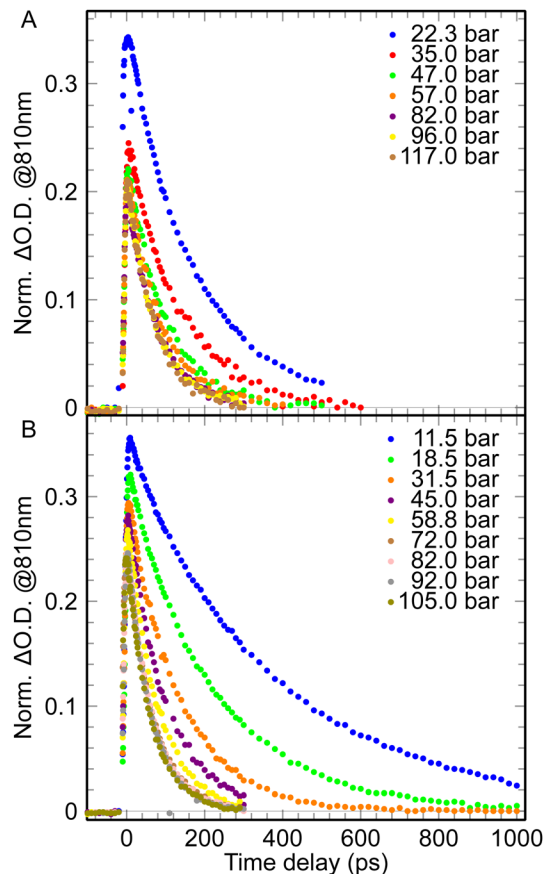


Fig. 1 The pulse radiolysis data of a water-CO<sub>2</sub> system at different pressures for nanosecond timescale: A – for 25 °C; B – for 35 °C.

linear dependence,<sup>9–11</sup> and the actual Henry's law is no longer applicable above *ca.* 20 bar.‡ Moreover, beyond the liquidus pressure, the concentration of CO<sub>2</sub> increases even more slowly with an increase in pressure (Fig. S2, ESI†).

As it can be seen from the Fig. 2 and 3 the dependencies of  $e_{\text{hyd}}^-$  lifetime and  $e_{\text{hyd}}^-$  initial yields at 10 ps after the pulse demonstrate the same behavior, reaching the plateau after the liquidus pressure, both for normal and supercritical liquid state, namely 25 °C and 35 °C, 53 and 63 bars, respectively.

The rate of decay of  $e_{\text{hyd}}^-$  below 60 bar increases from 0.1 to  $13 \times 10^{-9} \text{ s}^{-1}$  as pressure increases, remaining almost constant afterwards. For the supercritical state, it slightly increases from 15 to  $17 \times 10^{-9} \text{ s}^{-1}$ . However, there is a tendency for the value to plateau as in the normal liquid state. The decay rate constants of  $e_{\text{hyd}}^-$  were determined up to the point of liquidus for experimental temperatures as:  $K^{25^\circ\text{C}} = 8.1 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  and  $K^{35^\circ\text{C}} = 10.2 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ , respectively. These values are consistent with literature data.<sup>4,12</sup>

The leveling off of decay rates can be attributed to the saturation of CO<sub>2aq</sub> concentration, as depicted in Fig. S2 (ESI†). The concentration of CO<sub>2aq</sub> reach values up to 1.4 M above 60 bars (Fig. S2, ESI†). It should be noted that under the

‡ The CO<sub>2</sub> concentration were determined according to the literature data.<sup>9, 10, 11</sup>



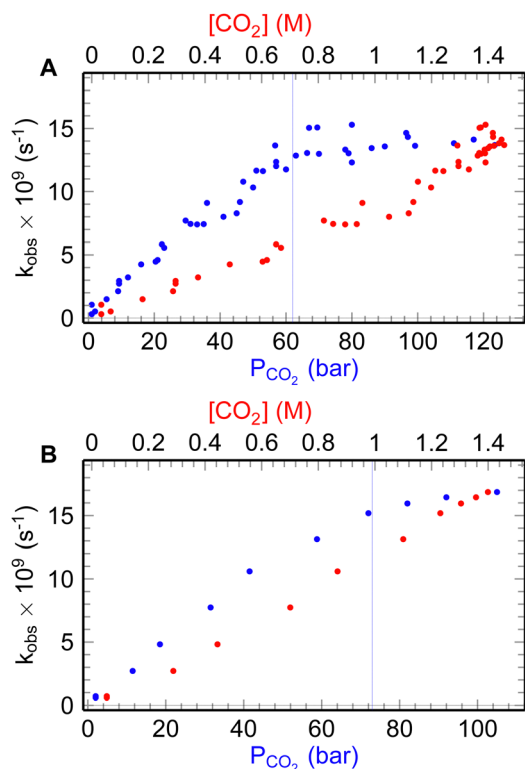


Fig. 2 The  $e_{\text{hyd}}^-$  decay rate (blue dots) at different pressures and concentrations of  $\text{CO}_2$  (red dots): A – for 25 °C; B – for 35 °C.

experimental conditions,  $\text{CO}_{2\text{aq}}$  is present almost at its non-protonated form, as evidenced by the solutions pH going low as 3. For additional information refer to the ESI† of our previous study.<sup>4</sup>

As shown in Fig. 3, the formation yield of  $e_{\text{hyd}}^-$  10 ps after the pulse initially drops from 4.4 to  $3 \times 10^{-7} \text{ mol J}^{-1}$  upon reaching 60 bars, and subsequently slow further decrease continues with pressure rise. It is noteworthy that the dependence of electron yield remains unchanged in the supercritical state. The formation yield of  $e_{\text{hyd}}^-$  is decreasing with the pressure increase due to the interaction between  $e_{\text{pre}}^-$  and  $\text{CO}_{2\text{aq}}$ , forming  $\text{CO}_2^{\bullet-}$ .

The scavenging efficiency of  $\text{CO}_2$  towards  $e_{\text{pre}}^-$  is inversely proportional to its  $C_{37}$  value. The initial yield of  $e_{\text{hyd}}^-$  decreases in the presence of a high concentration of scavengers and the fraction  $e_{\text{hyd}}^-$  could be described by the expression  $f = \exp(-[S]/C_{37})$ . The  $C_{37}$  value is determined for each temperature and are  $C_{37}^{25} = 3.3 \text{ mol kg}^{-1}$ ;  $C_{37}^{35} = 3.6 \text{ mol kg}^{-1}$ , for 25 °C, 35 °C, respectively. In the previous<sup>4</sup> measurement the value of 4.2 was determined for room temperature, that is erroneous (Fig. 3), that could be explained by the smaller range of used pressures. However, the  $C_{37}$  concentrations are not achievable since even at ultra-high pressures (> 500 bar) the  $\text{CO}_{2\text{aq}}$  can only reach *ca.* 1.8 M.

The experimental data indicates that after reaching pressures higher than 60 bar, the solvated electrons' rate of disappearance is reduced; the same is observed for the initial yield change with pressure for all temperatures, that correlates with the molar concentration of carbon dioxide (Fig. S2, ESI†).<sup>11,13</sup>

Our new experimental data is in a good agreement with previously published one<sup>4</sup> describing reactivity of  $\text{CO}_2$  with

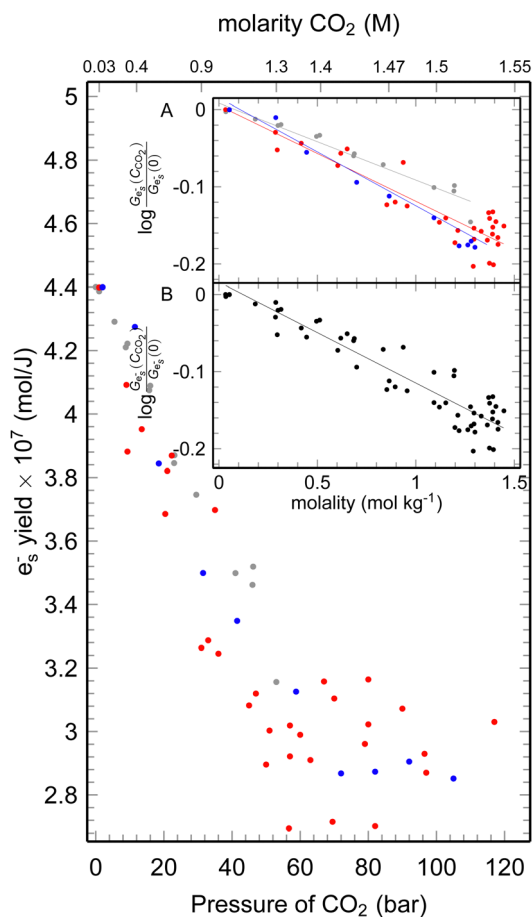


Fig. 3 The yield of  $e_{\text{hyd}}^-$  at 10 ps after the 7 ps electron pulse at different  $\text{CO}_2$  pressures, the gray dots data up to 51 bars;<sup>4</sup> red dots – data at 25 °C, blue dots – data at 35 °C. Inset: Plot of the  $e_{\text{hyd}}^-$  yield fraction remaining vs. the concentration of the  $\text{CO}_2$  A – 25 °C, B – 35 °C.

$e_{\text{hyd}}^-$  and  $e_{\text{pre}}^-$  in water under atmosphere and elevated pressures (below 53 bar) at room temperatures.

Under supercritical conditions,  $\text{CO}_2$  molecules have been observed to form neutral clusters, which exhibit a diverse size distribution that is influenced by changes in pressure and temperature. As a result, a broad range of cluster anions could be present in supercritical  $\text{CO}_2$ . Considering the fast reaction kinetics observed in electron transfer and the slow diffusivity of larger clusters, it is probable that in low-pressure scenarios, the primary electron donor is a small cluster, such as a  $(\text{CO}_2)_2^-$  dimer.<sup>14</sup> It could be inferred that the behavior of  $\text{CO}_2$  reactivity with excess electrons might be influenced in the water phase, when  $\text{CO}_2$  is in its supercritical state above the water phase. Specifically, clusters of  $\text{CO}_2$  molecules could potentially emerge in water, leading to an impact on the reactivity involving  $e_s^-$  and  $e_{\text{pre}}^-$  with  $\text{CO}_2$ . However, our experimental results do not indicate that.

In addition, we would like to state that there is no detectable spectral shift observed for either the normal or supercritical state with an increase in pressure (Fig. S3, ESI†).

The direct implication of this work could be related to corrosion in steel caused by water dissolved in supercritical



CO<sub>2</sub> that is a widely acknowledged issue.<sup>15–17</sup> The corrosion rate is largely determined by the ability of CO<sub>2</sub> to form anions. As international programs for CO<sub>2</sub> storage and transportation move towards liquid forms, the problem of pipe and storage facility corrosion will need to be addressed. The radiolysis technique provides a powerful research tool to investigate the fundamental properties of radicals in solutions and mixtures, and may bring the engineers to an effective solution of mentioned issue. Given that the dimerization of the CO<sub>2</sub> anion radical results in the creation of oxalate,<sup>3</sup> it is reasonable to anticipate not only corrosion of steel pipes transporting liquid CO<sub>2</sub>, but also the deposition of oxalate on walls of the tubes in the presence of natural ionizing radiation.

## 4 Conclusions

The reactivity of  $e_{\text{pre}}^-$  in CO<sub>2</sub>-water system was studied in the pressure range of 1–118 bar at two temperatures 25, 35 °C. Additionally, studies were carried out for the supercritical state (for  $P > 63$  bar, 35 °C). The  $C_{37}$  values were determined to be 3.3 and 3.6 mol kg<sup>-1</sup>, respectively, for 25 °C and 35 °C. Such concentrations for these systems are not achievable for practical study, so they could be used as reference concentrations demonstrating the scavenge rate of  $e_{\text{pre}}^-$  in water solution for CO<sub>2</sub>. In addition, the rates of the reaction between  $e_{\text{hyd}}^-$  and CO<sub>2</sub> were determined to be  $8.1 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  and  $10.2 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ , respectively, for 25 °C and 35 °C. These results are agreement with previously published data.<sup>4</sup>

## Author contributions

D. Dobrovolskii contributed to the project by data curation, formal analysis, visualization, resources, investigations and writing the original draft. S. Denisov's contributions included conceptualization, data curation, methodology, project administration, investigations, funding acquisition, formal analysis, resources, software, supervision, validation, visualization, conceptualization and writing for review and editing. M. Mostafavi's contributions comprised conceptualization, funding acquisition, methodology and writing for review and editing.

## Conflicts of interest

There are no conflicts to declare.

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## References

- 1 M.-Y. Lee, K. T. Park, W. Lee, H. Lim, Y. Kwon and S. Kang, *Crit. Rev. Environ. Sci. Technol.*, 2020, **50**, 769–815.
- 2 A. U. Pawar, C. W. Kim, M.-T. Nguyen-Le and Y. S. Kang, *ACS Sustainable Chem. Eng.*, 2019, **7**, 7431–7455.
- 3 C. Hu, S. A. Gharib, Y. Wang, P. Gan, Q. Li, S. A. Denisov, S. L. Caer, J. Belloni, J. Ma and M. Mostafavi, *Chem. Phys. Chem.*, 2021, **22**, 1900–1906.
- 4 S. A. Denisov and M. Mostafavi, *Phys. Chem. Chem. Phys.*, 2021, **23**, 5804–5808.
- 5 J. L. Marignier, V. Waele, H. Monard and F. Gobert, *Radiat. Phys. Chem.*, 2006, **75**, 1024–1033.
- 6 J. Belloni, *et al.*, *Nucl. Instrum. Methods Phys. Res., Sect. A*, 2005, **539**, 527–539.
- 7 F. Wang, U. Schmidhammer, J. P. Larbre, Z. Zong, J. L. Marignier and M. Mostafavi, *Phys. Chem. Chem. Phys.*, 2018, **20**, 15671–15679.
- 8 Y. Muroya, *et al.*, *Radiat. Phys. Chem.*, 2005, **72**, 169–172.
- 9 R. F. Weiss, *Mar. Chem.*, 1974, **2**, 203–215.
- 10 N. Spycher, K. Pruess and J. Ennis-King, *Geochim. Cosmochim. Acta*, 2003, **67**, 3015–3031.
- 11 Z. Duan, R. Sun, C. Zhu and I. M. Chou, *Mar. Chem.*, 2006, **98**, 131–139.
- 12 A. Lisovskaya and D. M. Bartels, *Radiat. Phys. Chem.*, 2016, **158**, 61–63.
- 13 A. Hebach, A. Oberhof and N. Dahmen, *J. Chem. Eng. Data*, 2004, **49**, 950–953.
- 14 N. M. Dimitrijevic, D. M. Bartels, C. D. Jonah and K. Takahashi, *Chem. Phys. Lett.*, 1999, **309**, 61–68.
- 15 Z. Cui, S. Wu, S. Zhu and X. Yang, *Appl. Surf. Sci.*, 2006, **252**, 2368–2374.
- 16 B. McGrail, H. Schaefer, V. Glezakou, L. Dang and A. Owen, *Energy Procedia*, 2009, **1**, 3415–3419.
- 17 Y.-S. Choi and S. Nešić, *Int. J. Greenhouse Gas Control*, 2011, **5**, 788–797.

