


Cite this: *RSC Adv.*, 2022, 12, 30549

# Promoting the mechanism of OMS-2 for gas adsorption in different K<sup>+</sup> concentrations

Shuangli Du,<sup>a</sup> Huan Zhang,<sup>a</sup> Cunbao Deng,<sup>a</sup> Xuefeng Wang,<sup>a</sup> Ruicong Zhai<sup>a</sup> and Zhijie Wen<sup>\*b</sup>

Catalytic combustion technology is an efficient and green method to deal with low concentration methane. Gas adsorption over the catalyst surface is a key step in the catalytic combustion process, which has attracted much interest. In this work, the first-principles density functional theory calculation method has been applied to explore the adsorption processes of CH<sub>4</sub> and O<sub>2</sub> molecules on the surface of cryptomelane type manganese oxide octahedral molecular sieves (OMS-2). In addition, the effect of K<sup>+</sup> concentration in the OMS-2 tunnel on the adsorption of the two gaseous molecules has also been investigated. The results of adsorption energy and structural characteristics show that the adsorption energies of CH<sub>4</sub> and O<sub>2</sub> molecules over the catalyst surface are favorable. Adsorption sites of CH<sub>4</sub> are the K<sup>+</sup> and O sites, among which the K<sup>+</sup> site is the most stable adsorption site. In addition, Mn sites are favorable for adsorbing O<sub>2</sub> molecules. The interactions between the catalyst and the adsorbed CH<sub>4</sub> and O<sub>2</sub> are enhanced with the increasing tunnel potassium ions. It should be noted that with the increasing strength of the adsorption energies, equilibrium distances from the two gaseous molecules to the active sites become shorter and the bond lengths of C–H and O–O bonds become longer. Moreover, the adsorption sites of CH<sub>4</sub> on the catalyst surface increase with the increasing K<sup>+</sup> concentration. Bader charge and cohesive energy calculations reveal that the tunnel K<sup>+</sup> can balance charges and help strengthen the structural stability of OMS-2. Interestingly, the electronegativity of the catalyst has been altered after introducing K<sup>+</sup>, which leads to better adsorption of gaseous CH<sub>4</sub> and O<sub>2</sub>. The microscopic mechanism of the effect of K<sup>+</sup> concentration on the adsorption of CH<sub>4</sub> and O<sub>2</sub> over the catalyst surface paves the way for further deciphering the mechanism underlying the catalytic oxidation process and helps design more efficient catalysts for methane utilization.

Received 1st September 2022  
Accepted 8th October 2022

DOI: 10.1039/d2ra05493k

rsc.li/rsc-advances

## 1. Introduction

Ventilation air methane emissions from coal mines have drawn worldwide attention because of the high global warming potential and the loss of methane resources.<sup>1</sup> Therefore, exploration and the development of ventilation air methane capture and utilization is technically challenging and has important environmental and safety concerns. Among the alternatives, catalytic combustion technology has been considered as the most effective way to solve this problem because of its efficient and green purification means.<sup>2,3</sup> Catalysts used in methane catalytic combustion are mainly divided into non-noble metal catalysts<sup>4–6</sup> (such as perovskite and hexaaluminate-type catalysts) and noble metal catalysts<sup>7,8</sup> (such as supported Pd and Pt catalysts), wherein non-noble metal

catalysts have a wide application prospect due to their low price, easy availability and strong thermal stability.

Among these non-noble metal catalysts, the special properties of manganese oxide molecular, such as high catalytic activity and thermal stability, low cost and easy to obtain, make it a new star material.<sup>9–11</sup> OMS-2 is a type of manganese oxide sieve with edge- and corner-sharing MnO<sub>6</sub> octahedra forming a 2 × 2 tunnel structure.<sup>12</sup> The key features for the high catalytic activities are mainly on account of the mixed valency of Mn (2+, 3+ and 4+), porous structure, easy release of lattice oxygen and acidic sites.<sup>13</sup> In addition, for the 0.46 nm tunnel cavity, some cations (such as Li<sup>+</sup>, Na<sup>+</sup> and K<sup>+</sup>) can be introduced into the tunnel to alter its chemical and physical properties. Many efforts have been invested to explore the effect of introduced metal cations on its catalytic activity. Ni *et al.*<sup>14</sup> found that the introduction of alkali earth metal ions (Mg<sup>2+</sup>, Ca<sup>2+</sup> and Sr<sup>2+</sup>) into the tunnel of OMS-2 can obviously change the catalytic activity for benzene oxidation. Among them, the Sr<sup>2+</sup>-doped catalyst exhibited the best catalytic activity and was even superior to the commercial 0.5% Pt/Al<sub>2</sub>O<sub>3</sub> catalyst. In addition, Hao *et al.*<sup>15</sup> revealed that introducing Co ions into the OMS-2 tunnel can

<sup>a</sup>College of Safety and Emergency Management Engineering, Taiyuan University of Technology, Taiyuan, 030024, China

<sup>b</sup>Key Laboratory of Mining Disaster Prevention and Control, Qingdao 266590, China. E-mail: zhijie\_wen1@163.com


effectively improve the catalytic activity of OMS-2. Further evidence of this remarkable effect of introducing metal cations has been provided by Hong *et al.*,<sup>16</sup> who demonstrated that ozone decomposition was promoted after introducing Na<sup>+</sup> into OMS-2 tunnels by facilitating lattice defect formation. Recently, Ming *et al.*<sup>17</sup> found that doping metal cations (Li<sup>+</sup>, Na<sup>+</sup>, Mg<sup>2+</sup>, Ca<sup>2+</sup>, Fe<sup>3+</sup>, Zn<sup>2+</sup> and Ag<sup>+</sup>) in OMS-2 catalysts promoted the selective catalytic reduction. It is widely known that the K<sup>+</sup> ion is close to the dimensions of the 2 × 2 tunnels of OMS materials and has been used as an ideal cationic template in OMS-2 tunnels.<sup>18–20</sup> Luo *et al.*<sup>21</sup> found that K<sup>+</sup> concentration significantly affected the magnetism of OMS-2. Hou *et al.* enhanced the oxidation of benzene<sup>18</sup> and arsenite<sup>22</sup> by tuning the K<sup>+</sup> concentration in the OMS-2 tunnel. Moreover, Hamaguchi *et al.*<sup>23</sup> investigated the effect of K<sup>+</sup> content on the NO-adsorption properties and suggested that the adsorption sites of NO<sub>x</sub> were the K sites.

In light of the above developments, it can be seen that lots of efforts have been directed toward the development of the OMS-2. Nevertheless, insufficient work has been reported on

methane adsorption over the OMS-2 surface. Recently, our group has reported that the positions of oxygen vacancies have influence on the adsorption capacity of the OMS-2 (110) surface for methane.<sup>24</sup> Do any other factors exist? Further, how does K<sup>+</sup> concentration affect methane adsorption? In addition, most of the studies focus on the experimental aspect. The detailed information and the mechanism of the adsorption process still remain unanswered.

In recent years, with the rapid development of computing technology and hardware, first-principles computation becomes an important tool for material design, synthesis and property prediction. Many experimental phenomena and microscopic reaction mechanisms have been well explained by theoretical research. Adsorption of reactant molecules on the catalyst surface is the first and key step in the catalytic reaction process. To this end, the reactants CH<sub>4</sub> and O<sub>2</sub> molecules were selected to explore the adsorption mechanism over the OMS-2 catalyst surface by a theoretical calculation method. In addition, the effects of tunnel K<sup>+</sup> concentrations (OMS-2 without K<sup>+</sup>, with 1 atom and 2 atom% K<sup>+</sup>) on the adsorption process were also analyzed. From the investigation of the geometric and energetic features of the complexes formed by the catalyst and the gaseous molecules, we suggest that the tunnel K<sup>+</sup> concentrations are essential for gas adsorption.

## 2. Computational details

All calculations were carried out using the Vienna *Ab initio* Simulation Package (VASP).<sup>25,26</sup> The Perdew–Burke–Ernzerhof (PBE) functional and the projector augmented wave (PAW) method were used for density functional theory (DFT) calculations.<sup>27</sup> To accurately describe the highly localized Mn 3d-orbitals, DFT + *U* calculations were performed with a value of *U* = 4 eV applied to the Mn 3d states. A cut-off energy of 500 eV and 2 × 2 × 1 Monkhorst–Pack *k*-point mesh were used throughout the calculations. All calculations were converged until the maximum force on all atoms was smaller than 0.02 eV

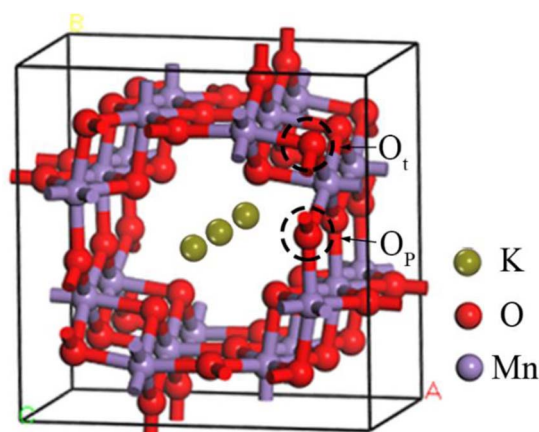


Fig. 1 Unit cell structure of OMS-2.

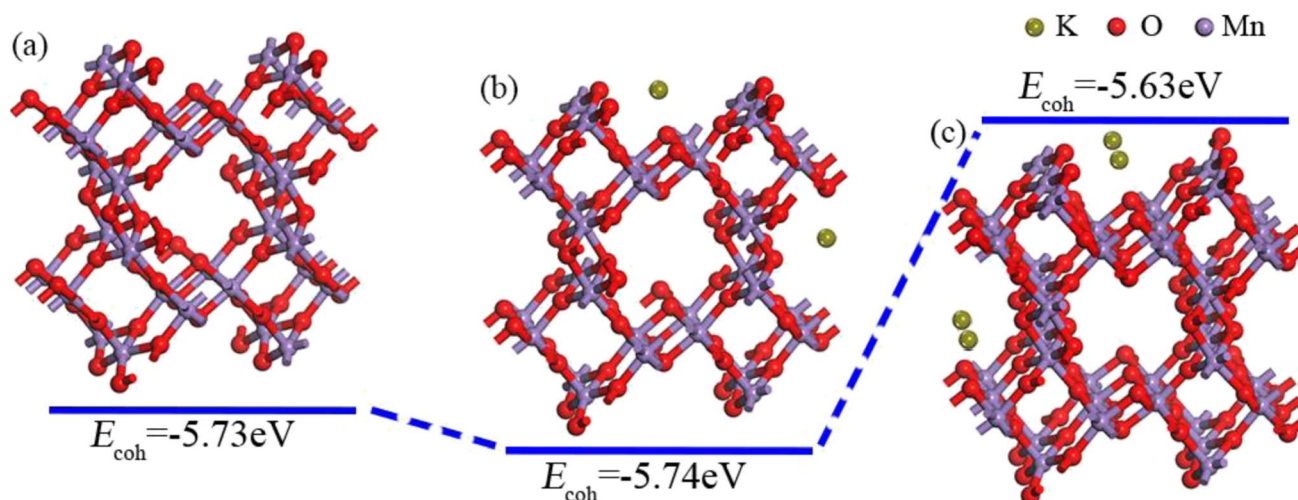


Fig. 2 OMS-2 (110) surface under different K<sup>+</sup> concentrations. (a) Without K<sup>+</sup>, (b) OMS-2 with 1 atom% K<sup>+</sup>, and (c) OMS-2 with 2 atom% K<sup>+</sup>.



$\text{\AA}^{-1}$ . Meanwhile, the electronic optimization steps were fewer than  $10^{-4}$  eV. Adsorption energy ( $E_{\text{ads}}$ ) of the gas molecules on the OMS-2 catalyst surface can be calculated by eqn (1):

$$E_{\text{ads}} = E_{\text{com}} - E_{\text{CH}_4} - E_{\text{OMS-2}} \quad (1)$$

where  $E_{\text{com}}$ ,  $E_{\text{CH}_4}$  and  $E_{\text{OMS-2}}$  represent the total energy of the adsorbed configuration, the isolated methane molecule and the optimized OMS-2 slab, respectively.

The unit cell model has been established based on the crystal structure information of OMS-2 in the Materials Project<sup>28</sup> database. As shown in Fig. 1, the crystal parameters after optimization are  $a = b = 9.74563 \text{ \AA}$ ,  $c = 5.81139 \text{ \AA}$ , and  $\alpha = \beta = \gamma = 90^\circ$ . In addition, it has been reported that the OMS-2 (110) surfaces have the lowest surface energy and dominate the largest surface area.<sup>29</sup> Therefore, the (110) surfaces were selected to explore the gas adsorption in different  $\text{K}^+$  concentrations. The slab (Fig. 2), with a  $(2 \times 2)$  supercell and a vacuum layer of  $15 \text{ \AA}$ , was constructed to model the OMS-2 (110) surface.<sup>30</sup> In addition, gas molecules ( $\text{CH}_4$  and  $\text{O}_2$ ) placed at all possible adsorption sites over the catalyst surface were optimized. Furthermore, it is worth noting that two types of oxygen atoms<sup>30</sup> are found in the structure of OMS-2, which are distinguished by  $\text{O}_\text{t}$  and  $\text{O}_\text{p}$  respectively.

### 3. Results and discussion

#### 3.1 Cohesion energy calculations

Cohesion energy ( $E_{\text{coh}}$ ) is representative of the energy needed to decompose a crystal into atoms, which is an important parameter to evaluate the stability of a crystal model.<sup>31</sup> A lower cohesion energy shows a higher crystal stability. Herein,  $E_{\text{coh}}$  has been calculated from the following equation:

$$E_{\text{coh}} = \frac{E_{\text{bulk}} - n_{\text{Mn}}E_{\text{Mn}} - n_{\text{O}}E_{\text{O}} - n_{\text{K}}E_{\text{K}}}{n_{\text{Mn}} + n_{\text{O}} + n_{\text{K}}} \quad (2)$$

wherein  $E_{\text{bulk}}$ ,  $E_{\text{Mn}}$ ,  $E_{\text{O}}$  and  $E_{\text{K}}$  are the energies of OMS-2, Mn atom, O atom and  $\text{K}^+$ , respectively.  $n_{\text{Mn}}$ ,  $n_{\text{O}}$  and  $n_{\text{K}}$  represent the number of Mn, O and  $\text{K}^+$  atoms, respectively.

Fig. 2 shows the OMS-2 (110) surface and the corresponding  $E_{\text{coh}}$  under different  $\text{K}^+$  concentrations. It is apparent that the cohesion energy of OMS-2 is  $-5.73 \text{ eV}$ . Upon introducing 1

**Table 1** Adsorption energy of  $\text{CH}_4$  molecules on the OMS-2 (110) surface ( $E_{\text{ads}}$ , eV), bond length of C–H ( $d$ ,  $\text{\AA}$ ) and the average bond length of C–H ( $\bar{d}$ ,  $\text{\AA}$ )

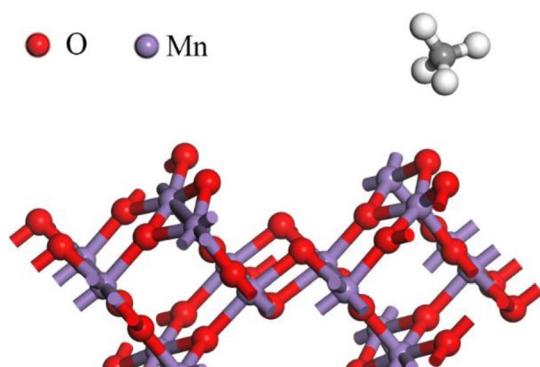
Adsorption site	$E_{\text{ads}}$	Chemical bond	$d$	$\bar{d}$
$\text{O}_\text{t}$	−1.13	C–H1	1.095	1.0955
		C–H2	1.096	

atom%  $\text{K}^+$  into the tunnel of OMS-2 (K1-OMS-2), the cohesion energy becomes  $-5.74 \text{ eV}$ , suggesting a significant enhancement of the catalyst stability. Interestingly enough, the cohesion energy decreases to  $-5.63 \text{ eV}$  after increasing  $\text{K}^+$  to a certain extent (2 atom%  $\text{K}^+$ , K2-OMS-2), which indicates that an appropriate  $\text{K}^+$  concentration can stabilize the Mn–O skeleton.

#### 3.2 Effects of $\text{K}^+$ concentration on $\text{CH}_4$ adsorption over the OMS-2 (110) surface

**3.2.1 Adsorption properties of  $\text{CH}_4$  on the OMS-2 (110) surface.** In order to explore the adsorption properties of  $\text{CH}_4$  on the OMS-2 (110) surface, all possible adsorption configurations were optimized. As shown in Fig. 3, the most stable adsorption site of  $\text{CH}_4$  is the  $\text{O}_\text{t}$ -top site with two H atoms of  $\text{CH}_4$  interacting with the  $\text{O}_\text{t}$  atom. In addition, the C–H bond lengths, interacting with the catalyst surface, are slightly elongated from its isolated state (shown in Table 1), implying that the electronic structure of  $\text{CH}_4$  has minimal perturbation after adsorption over the OMS-2 (110) surface. The adsorption energy is  $-1.13 \text{ eV}$ , exhibiting a weak chemical adsorption, which is in line with the change of structural parameters.

**3.2.2 Adsorption properties of  $\text{CH}_4$  on the K1-OMS-2 (110) surface.** To further test the influence of  $\text{K}^+$  on the adsorption of  $\text{CH}_4$  over the catalyst surface, we have tested all the possible adsorption configurations. The adsorption energies and the corresponding structural parameters are summarized in Fig. 4 and Table 2. Apparently, a significant difference exists after introducing  $\text{K}^+$  into the tunnel of OMS-2. Three different stable adsorption states ( $\text{O}_\text{p}$ ,  $\text{O}_\text{t}$  and  $\text{K}^+$  sites) are found. Upon  $\text{CH}_4$  adsorption at  $\text{O}_\text{p}$  and  $\text{O}_\text{t}$  sites, only one H atom of  $\text{CH}_4$  interacts with the adsorption site. The C–H bond lengths are also increased, suggesting a weakened C–H bond energy of  $\text{CH}_4$ . In addition, the adsorption energies of O sites are  $-1.15 \text{ eV}$  and  $-1.92 \text{ eV}$ , stronger than that over the OMS-2 surface ( $-1.13 \text{ eV}$ ). Interestingly, the distance from the C atom of  $\text{CH}_4$  to the adsorption site decreases with the increase of adsorption energy. For the adsorption of  $\text{CH}_4$  on the  $\text{K}^+$  site, three H atoms of  $\text{CH}_4$  interact with  $\text{K}^+$ . The C–H bond lengths are further increased compared with that on the O site. The adsorption energy is  $-2.07 \text{ eV}$ , with the closest distance from  $\text{CH}_4$  to the adsorption site. In light of the above discussion, we can conclude that the most stable adsorption site of  $\text{CH}_4$  on the K1-OMS-2 (110) surface is the  $\text{K}^+$  top site. All the adsorption energies of  $\text{CH}_4$  are enhanced compared with that over the OMS-2 (110) surface, indicating that the tunnel  $\text{K}^+$  of OMS-2 can affect methane adsorption. In addition, the C–H bond lengths of  $\text{CH}_4$  are also increased, which demonstrates that the changes of the



**Fig. 3** Stable structure of  $\text{CH}_4$  on the OMS-2 (110) surface.





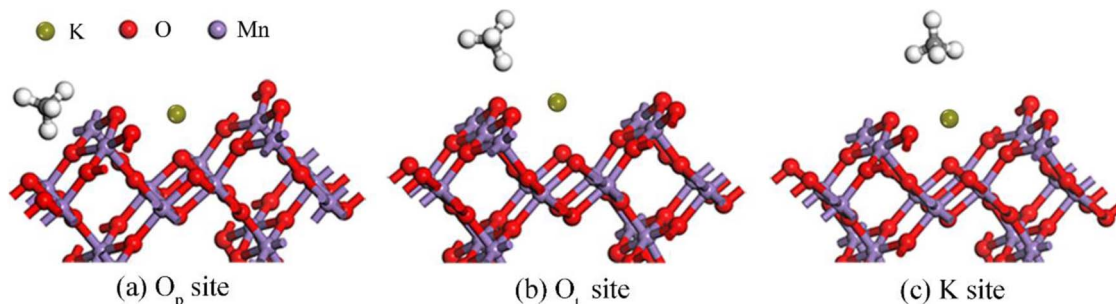


Fig. 4 Stable structures of CH<sub>4</sub> on the K1-OMS-2 (110) surface.

**Table 2** Adsorption energy of CH<sub>4</sub> molecules on the K1-OMS-2 (110) surface ( $E_{\text{ads}}$ , eV), bond length of C–H ( $d$ , Å), average bond length of C–H ( $\bar{d}$ , Å) and the distance from the C atom of CH<sub>4</sub> to the adsorption site ( $r$ , Å)

Adsorption site	$E_{\text{ads}}$	Chemical bond	$d$	$\bar{d}$	$r$
O <sub>p</sub>	−1.15	C–H1	1.097	1.097	3.507
O <sub>t</sub>	−1.92	C–H1	1.097	1.097	3.483
K <sup>+</sup>	−2.07	C–H1	1.099	1.0977	3.457
		C–H2	1.097		
		C–H3	1.097		

C–H bond lengths of CH<sub>4</sub> are in line with that of the adsorption energies.

**3.2.3 Adsorption properties of CH<sub>4</sub> on the K2-OMS-2 (110) surface.** To delve further into the distinct adsorption of CH<sub>4</sub>

over the OMS-2 (110) surface under different K<sup>+</sup> concentrations, the adsorption properties of CH<sub>4</sub> on the K2-OMS-2 (110) surface were investigated. All stable adsorption configurations are shown in Fig. 5. Apparently, four different stable adsorption states (Mn, O<sub>p</sub>, O<sub>t</sub> and K<sup>+</sup> sites) are obtained. Upon CH<sub>4</sub> adsorption at the Mn site, two H atoms of CH<sub>4</sub> interact with the Mn atom, with the 3.632 Å distance from the C atom to the Mn site, yielding an adsorption energy of −0.53 eV. In addition, the C–H bond lengths of methane are elongated to a certain degree. Upon CH<sub>4</sub> locating at O<sub>p</sub> and O<sub>t</sub> sites, only one H atom interacts with the adsorption site, which is similar to that over the K1-OMS-2 surface. In addition, with the increasing K<sup>+</sup> concentration, both the adsorption energies (−3.81 eV and −4.21 eV) at the two sites are enhanced. Meanwhile, methane becomes closer to the adsorption site accompanied by a longer C–H bond length. The most favorable configuration is the CH<sub>4</sub> adsorbing on the K<sup>+</sup>-top site with three H atoms interacting with K<sup>+</sup>, with

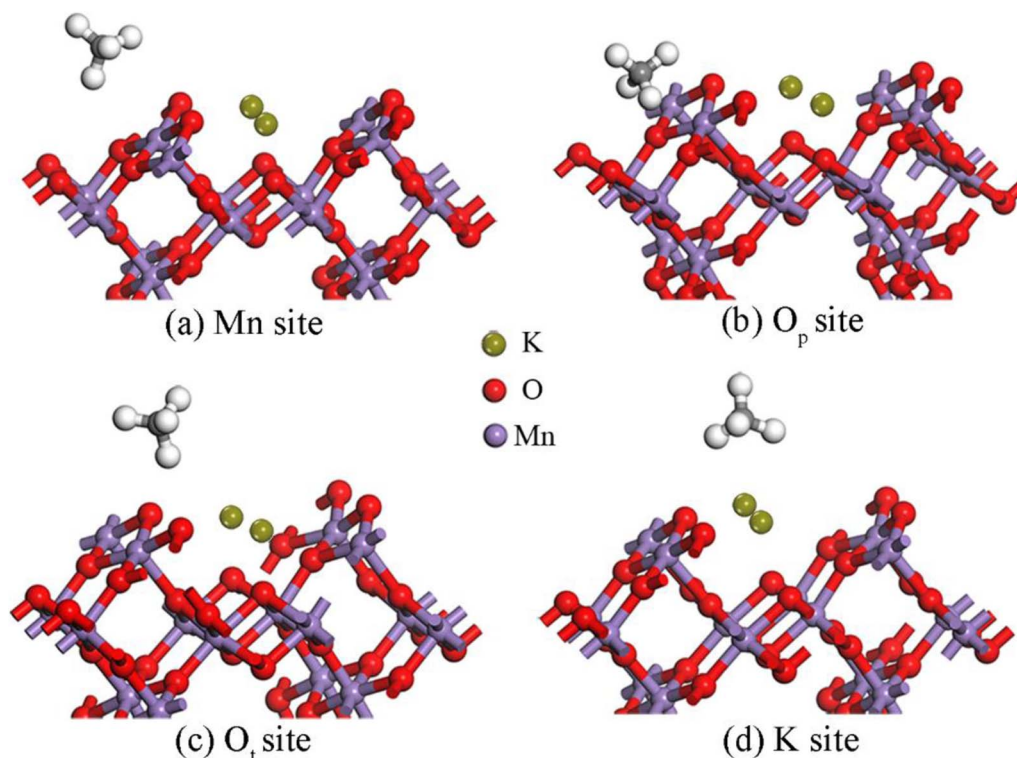


Fig. 5 Stable structures of CH<sub>4</sub> on the K2-OMS-2 (110) surface.



**Table 3** Adsorption energy of CH<sub>4</sub> molecules on the K2-OMS-2 (110) surface ( $E_{\text{ads}}$ , eV), bond length of C–H ( $d$ , Å), average bond length of C–H ( $\bar{d}$ , Å) and the distance from the C atom of CH<sub>4</sub> to the adsorption site ( $r$ , Å)

Adsorption site	$E_{\text{ads}}$	Chemical bond	$d$	$\bar{d}$	$r$
Mn	−0.53	C–H1	1.098	1.097	3.632
		C–H2	1.096		
O <sub>p</sub>	−3.81	C–H1	1.097	1.097	3.424
O <sub>t</sub>	−4.21	C–H1	1.098	1.098	3.472
K	−6.10	C–H1	1.100	1.098	3.424
		C–H2	1.096		
		C–H3	1.098		

the  $E_{\text{ads}}$  equal to −6.10 eV. As expected, the C atom is closest to the adsorption site (3.424 Å) accompanied by the longest C–H bond length. Moreover, it can be clearly found from analysis of the data in Table 3 that the longer the C–H bond length, the closer the C atom is to the adsorption site, and the stronger the interaction between methane and the surface. On the basis of these findings, we can conclude that the adsorption energy of CH<sub>4</sub> on the OMS-2 (110) surface is enhanced with the increase of K<sup>+</sup> concentration.

### 3.3 Adsorption properties of O<sub>2</sub> on the OMS-2 (110) surface under different K<sup>+</sup> concentrations

The adsorption properties of O<sub>2</sub> over the catalyst surface are very important to reveal the catalytic combustion mechanism. All possible adsorption configurations under different K<sup>+</sup> concentrations were investigated systematically. As depicted in Fig. 6, only one adsorption site (Mn site) can be found after O<sub>2</sub> adsorption over the OMS-2 catalyst surface, in which an O atom of the O<sub>2</sub> molecule tilts downward to interact with the Mn site. For the adsorption performances under low K<sup>+</sup> concentration (K1-OMS-2), the distance from the Mn-site to the closer O atom of O<sub>2</sub> is 3.239 Å, accompanied by an elongated O–O bond of the O<sub>2</sub> molecule. The adsorption energy is −0.90 eV. In addition, it can be seen from Table 4 that the O–O bond length is further elongated to 1.276 Å after increasing K<sup>+</sup> concentration. The corresponding adsorption energy is −5.67 eV, and the distance from the closer O atom of O<sub>2</sub> to the Mn site is shortened to 2.27

**Table 4** Adsorption energy of O<sub>2</sub> molecules on the catalyst surface ( $E_{\text{ads}}$ , eV), bond length of O<sub>2</sub> molecules ( $d$ , Å) and the distance from the closer O atom of O<sub>2</sub> to the adsorption site ( $r$ , Å)

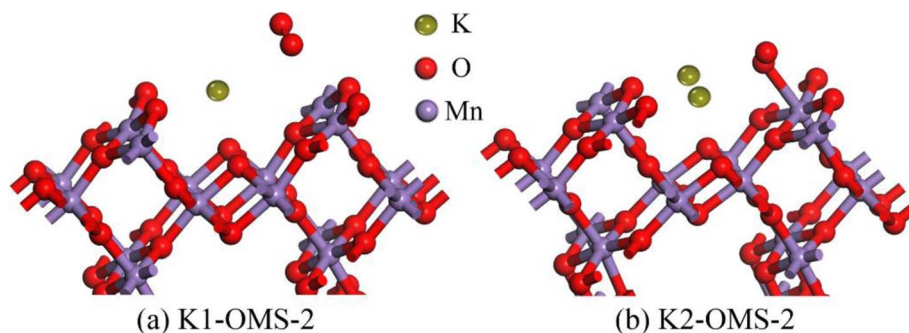
	$E_{\text{ads}}$	Chemical bond	$d$	$r$
K1-OMS-2	−0.90	O–O	1.236	3.239
K2-OMS-2	−5.67	O–O	1.276	2.27

Å. Similar to the result of CH<sub>4</sub> adsorption, the adsorption energy between O<sub>2</sub> and the catalyst surface is enhanced with the increase of K<sup>+</sup> concentrations, and the distance from the O<sub>2</sub> molecule to the active site becomes closer with an elongated O–O bond.

### 3.4 Bader charge analysis

Charge transfer provides very useful information on the adsorption and diffusion of molecules on the catalyst surface.<sup>32</sup> To get a deeper understanding of the effect of K<sup>+</sup> concentrations on the adsorption process, charge changes of gas molecules and catalyst surface have been calculated by Bader charge analysis.<sup>33</sup> Fig. 7 shows the charge distribution of the most stable adsorption configuration of CH<sub>4</sub> and O<sub>2</sub> molecules on the catalyst surface at different K<sup>+</sup> concentrations. As can be seen, CH<sub>4</sub> loses electrons and K<sup>+</sup> gains electrons, which indicates charge transfer from CH<sub>4</sub> to K<sup>+</sup> in all adsorption processes. In addition, the charges obtained by K<sup>+</sup> after CH<sub>4</sub> adsorption over K1-OMS-2 and K2-OMS-2 surfaces are 0.005e and 0.008e, indicating that the charge transfer increases with the increasing K<sup>+</sup> concentration. This trend of the charge transfer is consistent with that for the stability of CH<sub>4</sub> adsorbing over the catalyst surface. Furthermore, the two O atoms of the O<sub>2</sub> molecule obtain electrons after adsorption over the catalyst surface. The numbers of electrons obtained by the O<sub>2</sub> molecule increase with the increasing K<sup>+</sup> concentration, which is related to a stronger interaction between the O<sub>2</sub> molecule and the catalyst surface.

Bader charges of different active sites on the catalyst surface were also calculated (as shown in Fig. 8a). Clearly, the presence of K<sup>+</sup> changes the electronegativity of Mn and O atoms on the catalyst surface. There is a negative linear relationship between the concentration of K<sup>+</sup> and the electronegativity of Mn and O atoms. The higher the concentration of K<sup>+</sup>, the more obvious

**Fig. 6** Stable structures of O<sub>2</sub> on the catalyst surface.

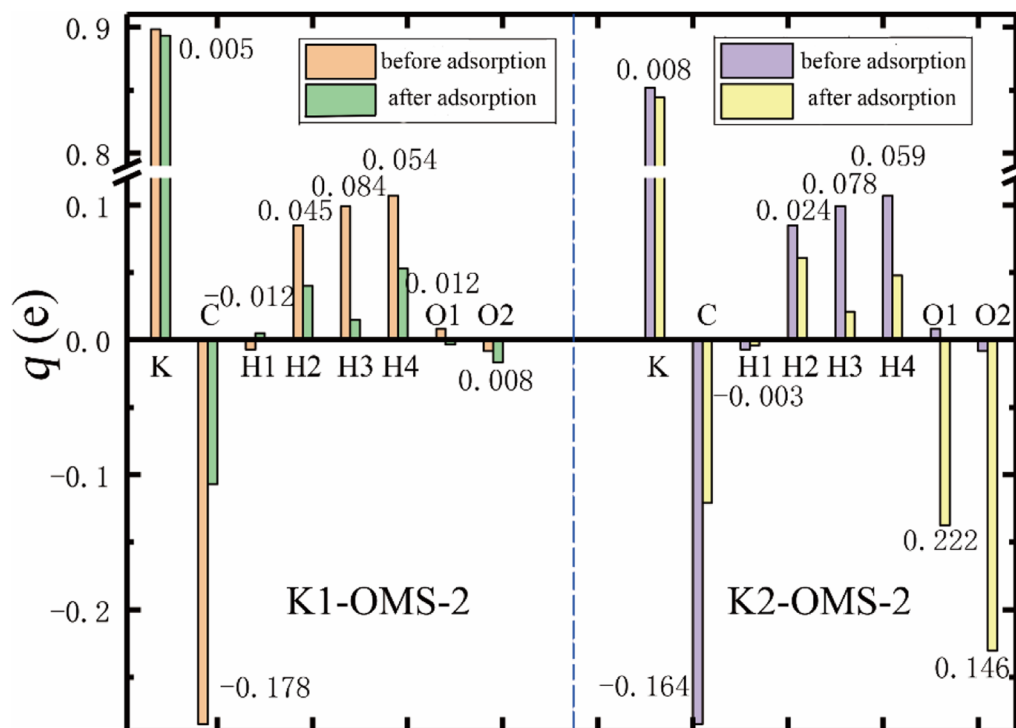


Fig. 7 Bader charge distribution ( $q$ , e) of  $\text{CH}_4$  and  $\text{O}_2$  molecules before and after adsorption on the catalyst surface. The numbers in the figure indicate the charge changes after adsorption ( $\Delta q$ , e).

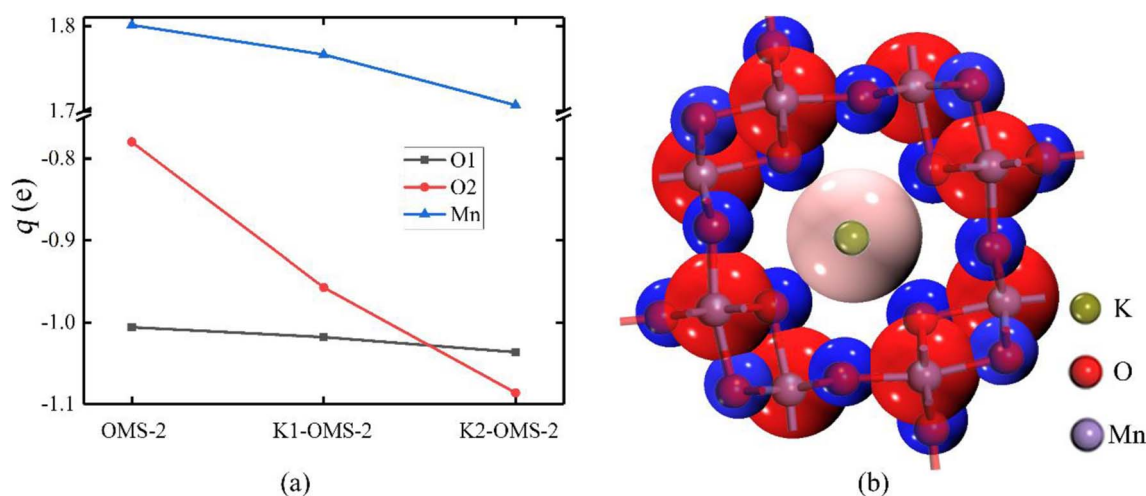


Fig. 8 (a) Charge changes ( $q$ , e) of adsorption sites on the catalyst surface with the change of  $\text{K}^+$  concentration. (b) The charge colorings on the K2-OMS-2. Red and blue represent positive and negative charges.

the changes of Mn and O electronegativity. It has been reported that the lower average oxidation state (AOS) of the Mn atom is related to the decreased charges on Mn atoms.<sup>34</sup> Hence, it can be inferred that the AOS of the Mn atom is decreased with the increasing  $\text{K}^+$  concentration. In addition, as depicted in Fig. 8a, the introduction of tunnel  $\text{K}^+$  changes the electronegativity of the OMS-2 skeleton, resulting in a strengthened interaction between the catalyst surface and the gas molecules.

Fig. 8b shows the charge colorings on the K2-OMS-2. It can be clearly seen that the positively charged  $\text{K}^+$  is surrounded by negatively charged O atoms in the tunnel. Moreover, the radius of  $\text{K}^+$  is well consistent with the radius of the OMS-2 tunnel. It can, therefore, be concluded that the introduction of  $\text{K}^+$  can balance the charge and stabilize the tunnel structure, in line with previous results of cohesion energy.



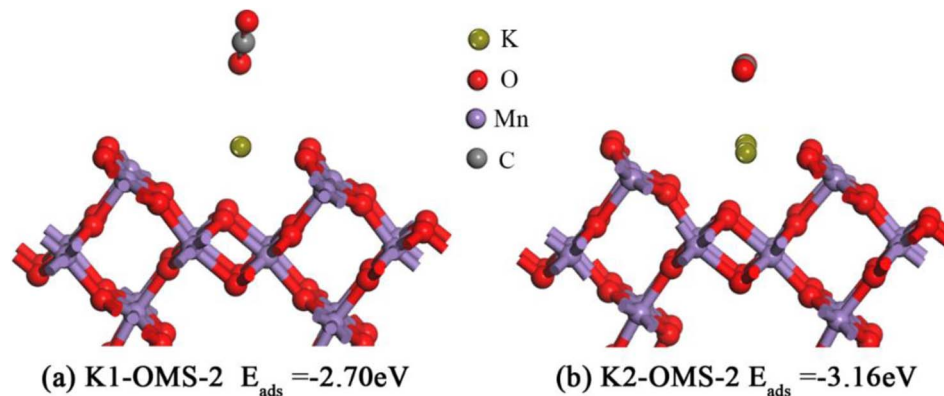


Fig. 9 Stable structures of  $\text{CO}_2$  on the catalyst surface.

### 3.5 Effects of $\text{K}^+$ concentration on $\text{CO}_2$ adsorption over the OMS-2 (110) surface

We also extend our investigation to  $\text{CO}_2$  adsorption over the OMS-2 (110) surface. It is widely known that  $\text{CO}_2$ , one of the products of methane catalytic combustion, can adsorb on the catalyst surface, hindering the reaction. Therefore, it is very important to study the adsorption properties of  $\text{CO}_2$  on the catalyst surface. As depicted in Fig. 9,  $\text{CO}_2$  molecules are found to have the most stable states when they are adsorbed on the  $\text{K}^+$  site, with O atoms of  $\text{CO}_2$  interacting with  $\text{K}^+$ . In addition, it should be noted that the  $\text{CO}_2$  molecule is almost parallel to the K2-OMS-2 catalyst plane with two O atoms of  $\text{CO}_2$  interacting with  $\text{K}^+$ . It is, therefore, reasonable to deduce that the adsorption energy of  $\text{CO}_2$  molecules on the catalyst surface becomes stronger with the increasing  $\text{K}^+$  concentration. The adsorption energies ( $E_{\text{ads}}$ , eV) are also calculated. As displayed in Fig. 9, the calculation results ( $-2.70\text{ eV}$  to  $-3.16\text{ eV}$ ) are consistent with the above deduction.

## 4. Conclusions

$\text{K}^+$  is the ideal cationic template in the OMS-2 tunnel and the  $\text{K}^+$  concentrations significantly affect gas adsorption. The first-principles density functional theory calculation method has been carried out to investigate the inner mechanism for the  $\text{CH}_4$  and  $\text{O}_2$  molecule adsorption under different  $\text{K}^+$  concentrations. Bader charge analysis indicates that the positive charge of the tunnel potassium ions can neutralize the negative charge of the O atom in the skeleton of OMS-2. Interestingly, the van der Waals radius of  $\text{K}^+$  is in good agreement with the radius of the OMS-2 tunnel. It can, therefore, be concluded that  $\text{K}^+$  can balance the charge and stabilize the tunnel structure. Adsorption energy and structural parameters show that  $\text{CH}_4$  and  $\text{O}_2$  molecules are favorably adsorbed over the catalyst surface.  $\text{CH}_4$  is preferentially adsorbed on the  $\text{K}^+$  and O sites, wherein the  $\text{K}^+$  site is the most stable adsorption site.  $\text{O}_2$  molecules preferentially reside at the Mn site to form the most favorable configurations. In addition, two different types of oxygen adsorption sites have been found.  $\text{CH}_4$  molecules tend to react with the O<sub>t</sub> species. Moreover, with the increasing strength of the

adsorption energies, equilibrium distances from the two gaseous molecules to the active sites become shorter and the bond lengths (C–H and O–O bond) become longer; especially, the adsorption performances between the catalyst and the gas molecules are enhanced with the increase of  $\text{K}^+$  concentration. Meanwhile, the adsorption sites of  $\text{CH}_4$  over the catalyst surface are also increased. Furthermore, we also extend our investigation to  $\text{CO}_2$  adsorption over the OMS-2 (110) surface. As expected, the adsorption energy becomes stronger with the increasing  $\text{K}^+$  concentration. In summary, the tunnel  $\text{K}^+$  can change the electronegativity of OMS-2, strengthening the interaction between the catalyst surface and gas molecules. The results presented here offer a broadened view of the subtle effects of the tunnel  $\text{K}^+$  on the gas adsorption of OMS-2, while providing the theoretical basis for the exploration and development of ventilation air methane capture and utilization.

## Author contributions

Shuangli Du: investigation and writing-original draft, Huan Zhang: formal analysis and review, Cunbao Deng and Xuefeng Wang: supervision and validation, Ruicong Zhai: data curation, and Zhijie Wen: supervision, review and editing. All authors analyzed data and contributed to writing the manuscript.

## Conflicts of interest

There are no conflicts of interest to declare.

## Acknowledgements

This study was supported by the National Natural Science Foundation of China (U1810206, 52004170), the Open Fund for Key Laboratory of Mining Disaster Prevention and Control (MDPC202009) and the Foundation of Taiyuan University of Technology (2022QN131).

## References

- 1 X. Wang, F. Zhou, Y. Ling, Y. Xiao, B. Ma, X. Ma, S. Yu, H. Liu, K. Wei and J. Kang, *Energy Fuels*, 2021, 35, 15398–15423.



- 2 D. Tian, K. Li, Y. Wei, X. Zhu, C. Zeng, X. Cheng, Y. Zheng and H. Wang, *Phys. Chem. Chem. Phys.*, 2018, **20**, 11912–11929.
- 3 S. Wang, C. Zhao, S. Li and Y. Sun, *Phys. Chem. Chem. Phys.*, 2017, **19**, 30874–30882.
- 4 F. Miao, D. Mao, X. Guo, J. Yu and H. Huang, *J. Technol.*, 2019, **19**, 242–248.
- 5 H. Zhang, S. Du and X. Wang, *Nat. Gas Chem. Ind.*, 2021, **46**, 10–14, 127.
- 6 W. Hu, J. Lan, Y. Guo, X. Cao and P. Hu, *ACS Catal.*, 2016, **6**, 5508–5519.
- 7 M. Hou, X. Zhang, C. Fu, W. Cen and J. Chen, *Phys. Chem. Chem. Phys.*, 2020, **22**, 4692–4698.
- 8 X. Wang, X. Zhang, M. Cao, X. Wang, Q. Gao, C. Deng and X. Huang, *Energy Fuels*, 2022, **36**, 6999–7005.
- 9 K. Wantala, T. Suwannaruang, J. Palalerd, P. Chirawatkul and R. Khunphonoi, *Surf. Interfaces*, 2021, **25**, 101286.
- 10 S. GUO, G. Zhang, Z. K. Han, S. Zhang and A. Baiker, *ACS Appl. Mater. Interfaces*, 2021, **13**, 622–630.
- 11 D. S. Pisal and G. D. Yadav, *Mol. Catal.*, 2021, **491**, 110991.
- 12 T. Gao, G. Marianne, K. Frank, N. Reinhard and F. Helmer, *J. Phys. Chem. C*, 2008, **112**, 13134–13140.
- 13 E. Cockayne and L. Li, *Chem. Phys. Lett.*, 2012, **544**, 53–58.
- 14 C. Ni, J. Hou, L. Li, Y. Li, M. Wang, H. Yin and W. Tan, *Chemosphere*, 2020, **250**, 126211.
- 15 Y. Hao, L. Li, Z. Lu, X. YU and X. Yang, *Appl. Catal., B*, 2020, **279**, 119373.
- 16 W. Hong, T. Zhu, Y. Sun, H. Wang and F. Shen, *Environ. Sci. Technol.*, 2019, **53**, 13332–13343.
- 17 S. Ming, P. Wang, P. Liu, J. Duan and T. Li, *Chem. Eng. J.*, 2020, **379**, 122287.
- 18 J. Hou, L. Liu, Y. Li, M. Mao, H. Lv and X. Zhao, *Environ. Sci. Technol.*, 2013, **47**, 13730–13736.
- 19 J. Liu, V. Makwana, J. Cai, L. S. Steven and M. Aindow, *J. Phys. Chem. B*, 2003, **107**, 9185–9194.
- 20 Q. Feng, H. Kanoh and K. Ooi, *J. Mater. Chem.*, 1999, **9**, 319–333.
- 21 J. Luo, H. T. Zhu, J. K. Liang, G. H. Rao, J. B. Li and Z. M. Du, *J. Phys. Chem. C*, 2010, **114**, 8782–8786.
- 22 J. Hou, Z. Sha, W. Hartely, W. Tan and M. Wang, *Environ. Pollut.*, 2018, **238**, 524–531.
- 23 T. Hamaguchi, T. Tanaka, N. Takahashi, Y. Tsukamoto, N. Takagi and H. Shinjoh, *Appl. Catal., B*, 2016, **19**, 234–239.
- 24 R. Zhai, C. Deng, S. Du and L. Li, *Chem. Phys.*, 2023, **564**, 111708.
- 25 G. Kresse and J. Furthmuller, *Appl. Catal., B*, 1996, **54**, 11169–11186.
- 26 J. Hafner, *J. Comput. Chem.*, 2008, **29**, 2044–2078.
- 27 J. P. Perdew, K. Burke and M. Ernzerhof, *Phys. Rev. Lett.*, 1998, **77**, 3865–3868.
- 28 A. Jain, S. P. Ong, G. Hautier, W. Chen and A. K. Persson, *APL Mater.*, 2013, **1**, 011002.
- 29 D. A. Tompsett, S. C. Parker and M. S. Islam, *J. Mater. Chem. A*, 2014, **2**, 15509–15518.
- 30 G. Zhu, J. Zhu, W. Jiang, Z. Zhang, J. Wang, Y. Zhu and Q. Zhang, *Appl. Catal., B*, 2017, **209**, 729–737.
- 31 Z. Chen, G. Li, H. Zheng, X. Shu, J. Zou and P. Peng, *Appl. Surf. Sci.*, 2017, **420**, 205–213.
- 32 D. Meng, W. Luo, G. Li and H. C. Chen, *Acta Phys. Sin.*, 2009, **58**, 8224–8229.
- 33 M. Yu and D. R. Trinkle, *J. Chem. Phys.*, 2011, **134**, 064111.
- 34 Z. Song, Z. Yan, X. Yang, H. Bai, Y. Duan, B. Yang and L. Leng, *Chem. Phys. Lett.*, 2018, **695**, 216–221.

