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# Understanding the active sites of Fe–N–C materials and their properties in the ORR catalysis system†

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Metal–N–C-based catalysts prepared by pyrolysis are frequently used in the oxygen reduction reaction (ORR). Zeolitic imidazolate frameworks (ZIFs), a type of metal organic framework (MOF), are selected as precursors due to their special structure and proper pore sizes. A series of Fe–N–C catalysts with different concentrations of 2-methylimidazole were prepared with a simple solvothermal-pyrolysis method, and the transformation productivity, morphology and ORR activity were investigated. It was found that the Fe–N–C catalyst with a 2-methylimidazole concentration of 0.53 mol L<sup>−1</sup> had the best performance. In 0.1 M KOH solution, the half-wave potential was 0.852 V (vs. RHE), with the highest electrochemically active surface area (ECSA) of 94.1 cm<sup>2</sup>, and the ORR reaction was dominated by a 4-electron process. The current only decreased by 10.5% after 50 000 s of chronoamperometry (CA), while the half-wave potential only decreased 20 mV in 3 M methanol. Additionally, this catalyst cannot be poisoned by Cl<sup>−</sup> and SO<sub>3</sub><sup>2−</sup> ions in the ORR process. Finally, some typical ions including SCN<sup>−</sup>, Fe(CN)<sub>6</sub><sup>3−</sup> and Fe(CN)<sub>6</sub><sup>4−</sup> were used to inhibit the active sites, and it was determined that Fe(II) is the real active species. The series of synthesis and testing experiments has significance in guiding optimization of the synthesis conditions and analysis of the mechanism of active sites in Fe–N–C materials.

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## 1 Introduction

With society's increasing demand for energy, the energy crisis has become a worldwide problem. Development of a highly efficient energy conversion device is a promising way to solve this problem. Fuel cells (FCs) have attracted extensive attention worldwide due to their advantages of clean products, high energy density, and highly efficient energy conversion. Alkaline fuel cells (AFCs) and proton exchange membrane fuel cells (PEMFCs)<sup>1,2</sup> are of particular interest due to their low operating temperature, which has more application prospects than other fuel cell designs. However, the sluggish ORR kinetics in the cathode have so far restricted their application and development. Therefore, the most effective catalysts of platinum group metals (PGMs) are typically selected to improve the cathode kinetic process. The main problem with PGM catalysts is the high price of Pt and its poor reserves in the Earth's crust,<sup>3</sup> which demand that researchers investigate new catalysts. Among the PGM-free catalysts, transition metals coordinate with nitrogen and form a metal–N<sub>x</sub> (M–N<sub>x</sub>) site in the carbon skeleton, which has been investigated as a highly active site in the alkaline

system of the ORR process<sup>4–7</sup> and has the potential to replace PGMs as a catalyst in AFCs. Fe–N–C is regarded as one of the most active sites,<sup>8–10</sup> while the abundant reserves and low price of Fe further indicate that Fe–N–C is worth investigating.

MOF derivatives with high conductivity and a high number of M–N–C sites are obtained by pyrolysis and carbonization of MOFs.<sup>11,12</sup> ZIFs, as typical MOF materials, are usually selected to synthesize M–N–C catalysts because of their high specific surface area, proper pore sizes and composition, structure and morphology, which are all easy to design.<sup>13–15</sup> ZIF-8 has been widely investigated in ORR electrocatalysis. The current research focuses on the control of synthesis,<sup>10,16,17</sup> design of pore patterns and morphology,<sup>18–21</sup> multicomponent doping<sup>21–24</sup> and composites with other materials<sup>25–28</sup> to achieve catalysts with high performance, in addition to discussing the catalytic mechanism. For the optimization of synthesis conditions, research is focused on the type and dosage of metal and the process of heat treatment. However, there are a few reports on tuning the concentration of the precursor to change the morphology of the ZIF. Zhang and coworkers changed the volume of methanol and synthesized a series of Fe–N–C catalysts with different particle sizes.<sup>29</sup> Their research showed that ORR activity is related to the particle sizes, which suggested that the influence of precursor concentrations on ORR activity can be used to optimize the synthesis conditions. The change in the volume of methanol can significantly affect the concentration of various precursors. Hence, variation of a single precursor is still worthy of investigation. On the other hand, some typical ions

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from the atmosphere and tap water, such as  $\text{Cl}^-$  and  $\text{SO}_3^{2-}$ , may have an attenuation effect on ORR activity in real FC conditions, but there are few studies on their effect on activity. Wang and coworkers selected poly-*m* phenylenediamine (PmPDA) to synthesize Fe-N-C catalysts.<sup>30</sup> Their research showed that the Fe-N-C catalyst had a decrease in ORR half-wave potential with the addition of  $\text{Cl}^-$  and  $\text{SO}_3^{2-}$ . Whether this phenomenon appears in other types of Fe-N-C catalysts remains unknown. In addition, in the study of the active site of Fe-N-C catalysts, further research is needed to understand whether the different valence states of the Fe site have the same catalytic properties. Potassium thiocyanide, KSCN, is used as an inhibiting reagent for Fe sites, but the effect of this reagent on other valence states of Fe sites and the effect of other inhibiting reagents on Fe sites is still unclear. Despite the progress made in this field, it remains unclear which valence state of Fe provides the best ORR activity.

In this work, a simple solvothermal-pyrolysis combination method is used to synthesize FeNC catalysts with different concentrations of 2-methylimidazole, and the relationships between 2-methylimidazole concentration and productivity, phase, morphology and ORR performance are analysed to optimize the synthesis conditions. The change in ORR activity can be explained by the trend in productivity and surface state. The optimized product has a high half-wave potential, high durability, strong ability to resist methanol poisoning and good ORR catalytic kinetic performance. The addition of  $\text{Cl}^-$  and  $\text{SO}_3^{2-}$  in solution do not decrease the half-wave potential, but instead increase it, although the mechanism for this effect still needs further investigation. Instead of the typical  $\text{SCN}^-$  ion used to inhibit Fe(III),  $\text{Fe}(\text{CN})_6^{4-}$  and  $\text{Fe}(\text{CN})_6^{3-}$  are used to block Fe(III) and Fe(II) sites, and the degree of half-wave potential attenuation confirms that Fe(II) is the real active site.

## 2 Experimental

### 2.1 Chemicals

$\text{Fe}(\text{acac})_3$  (98%, Shanghai Aladdin),  $\text{Zn}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  (99%, YiLi Fine Chemicals), 2-methylimidazole (98%, Shanghai Aladdin), methanol (>99.5%, Tianjin DaMao), *N,N*-dimethylformamide (>99.5%, Tianjin DaMao), KOH (95%, Macklin),  $\text{Na}_2\text{S} \cdot 9\text{H}_2\text{O}$  (>98%, Shanghai Aladdin), NaCl (>99.5%, Beijing Chemical Works),  $\text{Na}_2\text{SO}_3$  (>97%, Tianjin DaMao), KSCN (98%, Heowns),  $\text{K}_3\text{Fe}(\text{CN})_6$  (>99.5%, Sinopharm Chemical Regents),  $\text{K}_4\text{Fe}(\text{CN})_6$  (>99.5%, Tianjin FuChen), Nafion (5%, Sigma). All the chemicals were of AR grade and used as received without further purification. Commercial 20 wt% Pt/C electrocatalyst was supplied by Sigma Aldrich.

### 2.2 Synthesis of catalyst

**2.2.1 Synthesis of Fe-NC-X.** The synthesis of Fe-NC was conducted similarly to previously reported work.<sup>31</sup> Typically, 2-methylimidazole,  $\text{Zn}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  and  $\text{Fe}(\text{acac})_3$  were dissolved in methanol. The solution was transferred into a Teflon-lined stainless-steel autoclave for the solvothermal process. The product was washed and dried after separation by

centrifugation. The obtained powder was carbonized at 900 °C for 3 h in argon. The specific synthesis processes are shown in ESI† and the dosage of synthesis are shown in Table S1.†

The molar quantities of 2-methylimidazole were varied to produce different samples at 12 mmol, 16 mmol, 24 mmol, 32 mmol and 36 mmol. The as-prepared ZIFs are named FeZIF-*X* (where *X* is the number of mmols of 2-methylimidazole). The carbonized samples are named Fe-NC-*X* (where *X* is the number of mmols of 2-methylimidazole).

**2.2.2 Synthesis of NC-24.** The synthesis of NC-24 is the same as that of FeNC-24, with the absence of  $\text{Fe}(\text{acac})_3$ .

### 2.3 Characterization methods

The phase identification of the powder samples was performed with X-ray diffraction (XRD, Smartlab 3) at a scan rate of 10 degrees (°) per min from 5° to 80° and confocal laser microscopy Raman spectroscopy (Raman, Renishaw) from 900  $\text{cm}^{-1}$  to 2000  $\text{cm}^{-1}$ . The morphology was investigated by scanning electron microscopy (SEM, JSM-7900) and transmission electron microscopy (TEM, JEM-2100F). Valence states were analysed by X-ray photoelectron spectroscopy (XPS, ESCALAB 250Xi) with an Al K $\alpha$  radiation source (note: the XPS results after the CA test of FeNC-24 were obtained without the addition of binder. The elemental composition was analysed by an inductively coupled plasma optical emission spectrometer (ICP-OES, Optima8300)).

### 2.4 Electrochemical measurements

The electrochemical measurements were obtained in a three-electrode system, with the working electrode, a cylindrical glassy carbon electrode with a diameter of 5 mm, functioning as a rotating disk electrode (RDE, Pine AFMSRCE); the counter electrode, a carbon rod; the reference electrode, a Hg/HgO electrode in 0.1 M KOH and an electrolyte of 0.1 M KOH. The following experiments included cyclic voltammetry (CV), linear sweep voltammetry (LSV), chronoamperometry (CA) and Electrochemical Impedance Spectroscopy (EIS).

Generally, a 6 mg Fe-NC-*X* powder sample (2 mg for commercial Pt/C) was prepared in a centrifuge tube. Then, 1 mL ethanol and 0.5 mL 0.2% Nafion ethanol solution were added to the powder with ultrasonic dispersion for 10 min to disperse them into a slurry. Then, 20  $\mu\text{L}$  of slurry was added dropwise onto the glassy carbon electrode with a microsyringe and dried. The theoretical mass of FeNC catalysts on the electrode is  $8.00 \times 10^{-4}$  mg ( $2.67 \times 10^{-4}$  mg for commercial Pt/C).

In the chronoamperometry (CA) test, a glassy carbon piece of  $10 \times 10$  mm was used as the working electrode. The formulation of the electrode material slurry was dropwise added onto the electrode at 200  $\mu\text{L}$  for each side.

## 3 Results and discussion

### 3.1 Phase and morphology analysis

Fig. 1(a) exhibits the XRD patterns of different FeZIFs. All samples demonstrated the same patterns with ZIF-8, indicating the similar crystal structure. The XRD patterns of FeNCs are



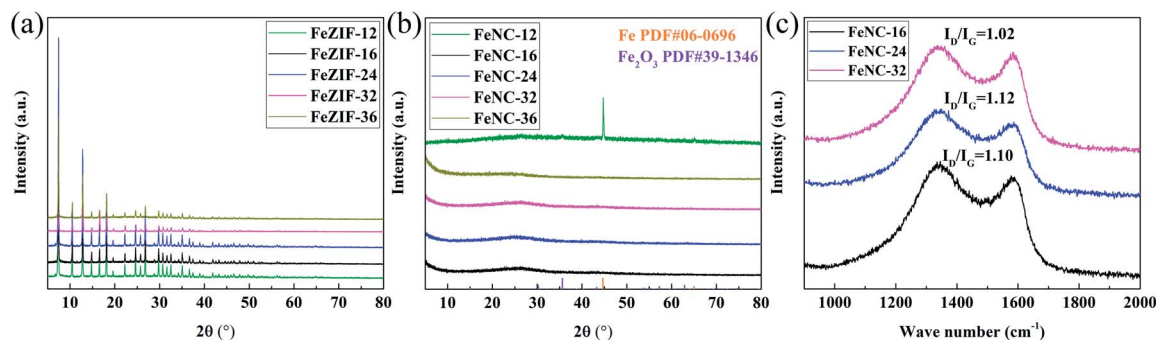


Fig. 1 XRD patterns of different (a) FeZIFs and (b) FeNCs samples. (c) Raman spectra of FeNC-16, FeNC-24 and FeNC-32. The dosage of 2-methylimidazole are respectively 12 mmol, 16 mmol, 24 mmol, 32 mmol and 36 mmol and the molar ratio of Zn : Fe in all the samples are 10 : 1.

shown in Fig. 1(b). Except mixed phase of Fe and Fe<sub>2</sub>O<sub>3</sub> for FeNC-12, the other samples show no crystal phase structure. It demonstrates that the crystallinity of these samples are limited during the heat treatment at 900 °C for 3 h. While for FeNC-12, the difference might be attribute to the extremely low productivity (Fig. S1†) of its FeZIF, resulting in the higher molar ratio of Fe(acac)<sub>3</sub> in the composite, which is favorable for the sintering of Fe species during the high-temperature process. Fig. 1(c) shows the Raman spectra of the typical three named as FeNC-16, 24, 32. The broad peaks around 1340 cm<sup>-1</sup> and 1580 cm<sup>-1</sup> attribute to the unordered carbon and ordered graphitic carbon. FeNC-24 has the highest peak ratio of I<sub>D</sub>/I<sub>G</sub> = 1.12, demonstrating the higher defects in carbon structure with the doping of N, Zn and Fe atoms, which is beneficial to its promotion in activity.<sup>32,33</sup>

The SEM images of FeNC-24 are shown in Fig. 2(a). It is observed that the achieved materials are in particles, uniformly distributed in this area. Fig. S2† shows SEM images and histogram of particle size distribution of typical FeNCs. The result of

particle size distribution statistics show that the average sizes of such samples are less than 1 μm. Fig. S3† are SEM images of typical FeZIFs. The diameter of FeZIF particles are also uniform, which demonstrates that FeNCs remain the dispersity of FeZIFs even after pyrolysis. As shown in Fig. S4(a),† the dispersity of FeZIF-12 is worse than typical FeZIFs. Pyrolyzed FeNC-12 shows a different morphology from other samples with the appearance of silk-like structures around the morphology of ZIF-like carbon (Fig. S4(b–d)†). The silk-like structure corresponding to the carbon nano tubes (CNTs) which was formed with the catalyzing of sintered iron particles during the heat treatment.<sup>34,35</sup> This result is consistent with XRD results.

The summary of average sizes of FeZIFs and FeNCs are shown in Fig. 2(b). The average size of obtained FeZIF distribution from 1.18 μm to 0.67 μm while that counterpart of FeNC is from 0.63 μm to 0.39 μm. It can be observed that the average sizes of FeZIFs and FeNCs decrease with the increase of 2-methylimidazole dosage. It also can be discovered that the sizes of FeZIFs are larger than that counterpart of FeNCs, which

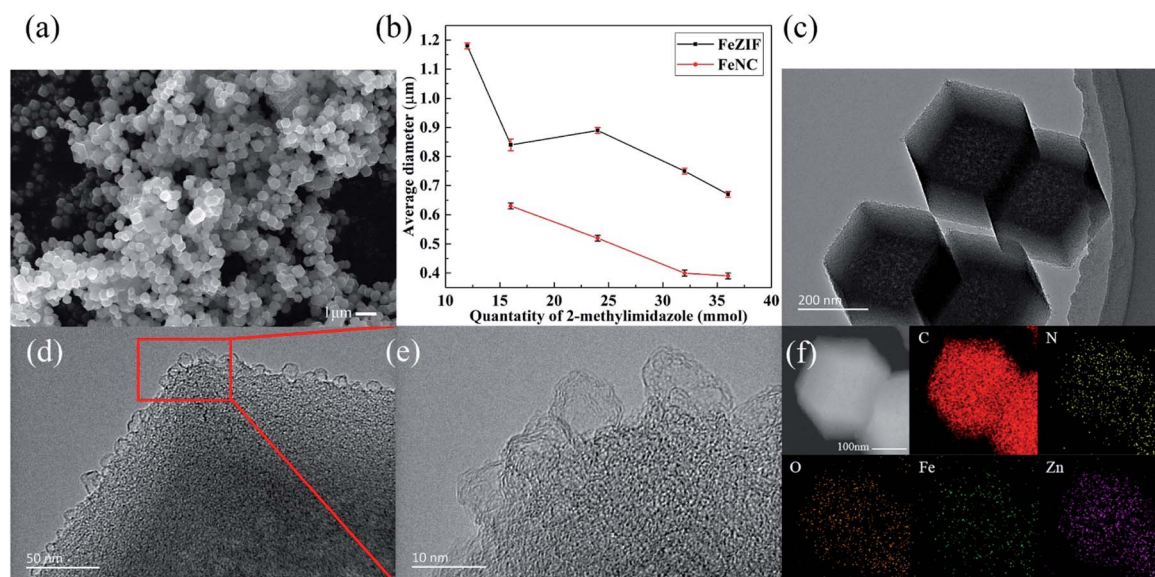


Fig. 2 (a) The SEM image of FeNC-24, (b) average particle size distribution curves of FeZIFs and FeNCs, (c–e) the TEM images of FeNC-24 (f) the EDS image of FeNC-24.



might be caused by the consumption in volume and mass during the pyrolysis of ZIFs.

Fig. 2(c) is the TEM image of FeNC-24. The shape of these particles clearly indicate that carbonized samples remain the dodecahedral structure of ZIF-8. The result in Fig. 2(d and e) show the amorphous structure of FeNC-24 from the bulk to the surface. And the rough structure on the surface might appear during the evaporation of zinc in the ZIFs. Fig. S5† shows the image of FeNC-24 in high-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM). No light-spots are observed, indicating metal particles does not existing in this sample, which manifests metal is not seriously sintered and formed in amorphous structure. Fig. 2(f) illustrates the energy dispersive spectrum (EDS) mapping of FeNC-24. The elements of C, N, O, Fe, Zn are equally dispersed in this material. The appearance of zinc in EDS demonstrate that part of zinc still remains in the material after heat treatment.

The XPS results are demonstrated in Fig. 3. For Fe species, the binding energy of  $\text{Fe}^{2+} 2\text{p}^{3/2}$ ,  $\text{Fe}^{3+} 2\text{p}^{3/2}$ ,  $\text{Fe}^{2+} 2\text{p}^{1/2}$ ,  $\text{Fe}^{3+} 2\text{p}^{1/2}$  respectively located at  $\sim 711.5$  eV, 714.5 eV, 724.5 eV, 727.5 eV, respectively (Fig. 3(a–c)). It can be observed that the valence state of Fe are in +2 and +3 in such samples, and the proportion of +2 is higher than +3, indicating Fe prefer +2 form after the process of heat treatment. For N species, the form of N in samples are in pyridine N, M (Fe or Zn)–N, pyrrole N, graphitic N, oxide N, the binding energy respectively assigned to  $\sim 398.5$  eV, 399.4 eV, 400.2 eV, 401.1 eV, 402.1 eV, respectively (Fig. 3(d–f)). The appearance of M–N indicates the coordination of metal and N. And in C 1 s pattern (Fig. S6†), C–N bond is observed, indicating the structure of M(Fe or Zn)–N–C is formed. The graphitic N have the ability in control the geometric and electronic structure of carbon framework<sup>36</sup> and improve the limiting current density of ORR catalysts.<sup>33</sup> Table S2† provide the atomic ratio of Fe measured by XPS and ICP-OES. FeNC-24 shows higher surface Fe atomic ratio than that

of bulk. On the contrary, the trend of FeNC-16 and 32 are distinct. Generally, XPS can measure the metal distribution on surface while ICP-OES measure that counterpart of bulk. The data in this table cannot give consistent result among the three samples, which might be caused by the inhomogeneity of MOF samples after pyrolysis at high temperature.

### 3.2 Electrochemical properties and analysis

The electrochemical properties of FeNC-X, NC-24, Pt/C samples are tested in  $0.1 \text{ mol L}^{-1}$  KOH solution. For CV and LSV tests, argon is saturated in electrolyte solution to ensure sample activated in the non-oxygen solution. Then, ORR activity is measured in oxygen saturated electrolyte. For stability tests, oxygen is saturated in electrolyte solution and kept plugging in electrolyte.

The LSV curves of FeNC-16, 24, 32, NC-24 and Pt/C are shown in Fig. 4(a). The half-wave potential of FeNC-24 is 0.852 V, which is 9 mV lower than that of commercial Pt/C(0.861 V) and is the best among the three typical FeNCs. NC-24 has much lower half-wave-potentials than FeNCs, demonstrating Fe might play the key roles in ORR electrocatalysis.

As shown in Fig. S7,† the FeNC-24 has the best ORR activity among all FeNCs. The half-wave potential of FeNCs first increased and then decreased with the increase of 2-methylimidazole dosage. Combined with production and morphology, it might be explained that: when the dosage of 2-methylimidazole is to a low level, the larger particle size of Fe will be obtained during the heat treatment, which is a negative factor for ORR. On the other hand, the much higher dosage of 2-methylimidazole will induce the extremely high production of ZIF, leading to the decrease of the density of Fe active sites, which is also unfavorable for ORR. The medium dosage of 2-methylimidazole will lead to the reasonable particle sizes and production, which is beneficial to the ORR catalyst.

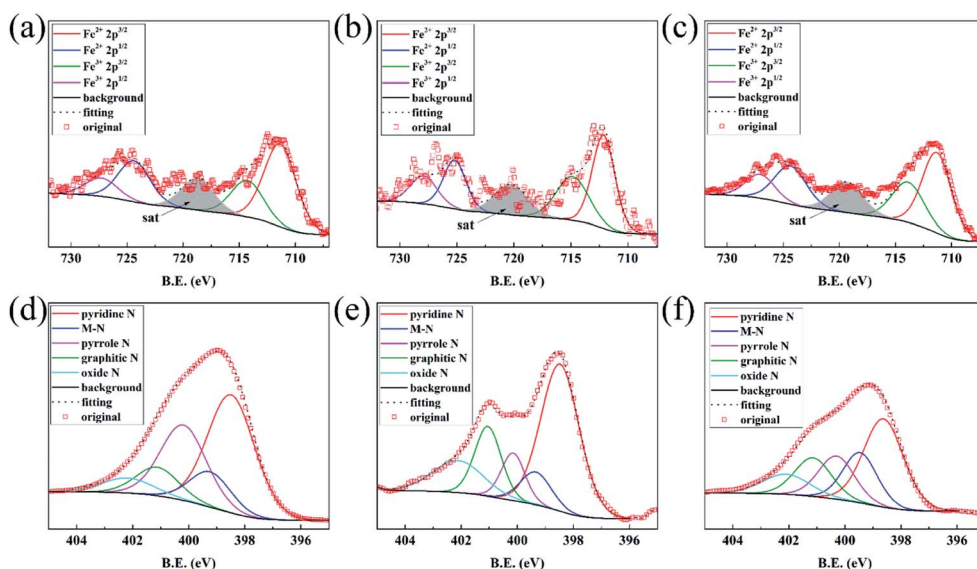


Fig. 3 The XPS patterns of Fe 2p for (a) FeNC-16, (b) FeNC-24, (c) FeNC-32. N 1s for (d) FeNC-16, (e) FeNC-24, (f) FeNC-32.



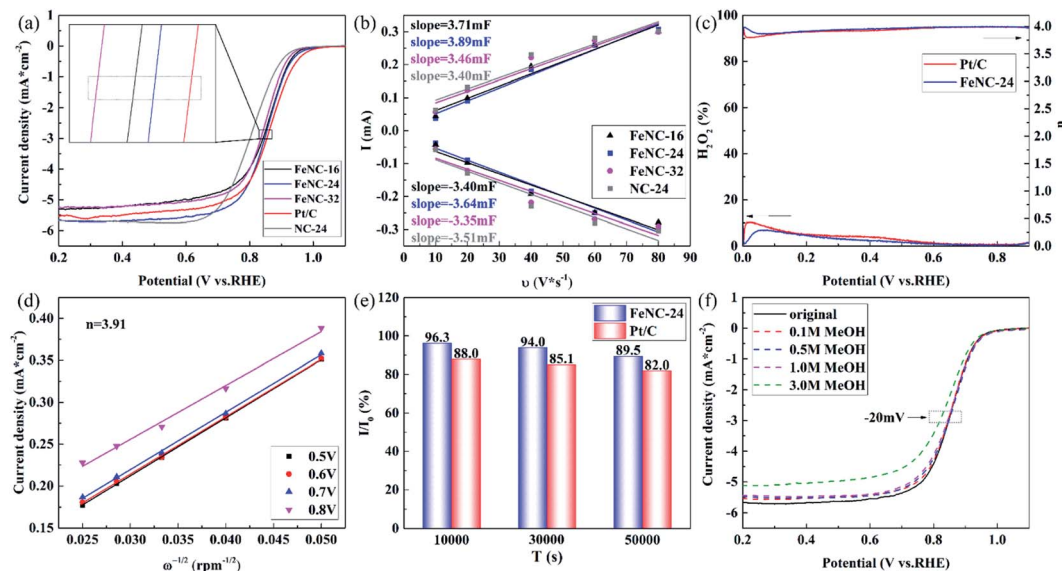


Fig. 4 (a) The LSV curves of FeNC-16, 24, 32, NC-24 and Pt/C in 0.1 M  $O_2$ -saturated KOH solution in 1600 rpm. (b) ECSA fitting results of FeNC-16, 24, 32, NC-24. (c) Productivity of  $H_2O_2$  and electron transfer number of FeNC-24 and Pt/C. (d) K–L equation fitting of FeNC-24. (e) The current attenuation rate of FeNC-24 and Pt/C in CA test. (f) The LSV curves of FeNC-24 in 0.1 M  $O_2$ -saturated KOH solution in 1600 rpm with methanol at different concentrations (0 M, 0.1 M, 0.5 M, 1.0 M and 3.0 M).

The ECSA fitting of such samples is shown in Fig. 4(b). The original curves are exhibited in Fig. S8.† The value of ECSA is calculated in Table S3.† It is demonstrated that FeNC-24 has the highest ECSA among these materials, which might provide more redox sites for ORR catalysis.

The electron transfer number and yield of  $H_2O_2$  are measured in RRDE test (Fig. 4(c)). The electron transfer number is close to 4, demonstrating ORR is basically a four-electron process. The productivity of  $H_2O_2$  is below 10% even in the apex of the curve for both FeNC-24 and Pt/C. The result of K–L equation fitting also supports the above conclusion (Fig. 4(d) and S9†). The calculated average electron transfer number is 3.91, which is in accordance with RRDE curve results.

The CA data is shown in Fig. 4(e). The current density decreases with increasing time. At 10000 s, 30000 s and 50000 s, the retention rates of current are respectively 96.3%, 94.0% and 89.5% for FeNC-24. And that counterpart of Pt/C are 88.0%, 85.1% and 82.0% (The original curves are shown in Fig. S10.†) For each time, FeNC-24 has a higher retention rate of current than that of Pt/C, demonstrating FeNC-24 is much better durable than that of commercial Pt/C. The TEM and EDS-mapping image of FeNC-24 after CA test is shown in Fig. S11.† It is clear that catalysts still remain the similar morphology and components as original after stability test. These results indicate the excellent durability of FeNC-24, and the change of carbon framework is negligible during the CA test.

Fig. 4(f) exhibits the LSV curve of FeNC-24 with the addition of different concentrations of methanol. The half-wave potential and limiting diffusion current density decrease with increasing methanol concentration. In the electrolyte with 3 M methanol, the half-wave potential left shifted ~20 mV. In contrast

with commercial Pt/C (Fig. S12†), the decrease of FeNC-24 is slight. Therefore it is suggested that FeNC-24 has satisfactory tolerance toward methanol. A previous research<sup>37</sup> demonstrates that FeNC sites have no activity in catalyzing the decomposition of small molecule alcohols, which is distinct with some noble metals. The poisoning of FeNC material is caused by the lower conductivity of solution with the addition of methanol and the blockage of pathway in ORR. The pores of FeNC-24 are not blocked by the methanol, presenting the less degree of activity.

The Tafel plot of such samples is presented in Fig. S13.† Except NC-24, FeNC samples in this graph have lower slope in the selected scope than commercial Pt/C, proving that FeNCs electrode possess better kinetics of ORR. And the EIS plots and equivalent circuit of FeNCs are shown in Fig. S14.† The solution resistances ( $R_s$ ) are the same while the polarization resistances ( $R_p$ ) of FeNC-16, 24, 32 are respectively 294  $\Omega$ , 201  $\Omega$ , 160  $\Omega$ . The  $R_p$  decreases with the increase of the dosage of 2-methylimidazole. It is attributed to the increase in productivity, improving the amount of carbon in FeNC, which promotes the conductivity of FeNC.

Some typical ions are added into the electrolyte to simulate the electrochemical environment in PEMFC. As shown in Fig. S15(a),† with the addition of 1 mM  $SO_3^{2-}$ , a very slight positive shift (4 mV) is observed in half-wave potential of FeNC-24, indicating that  $SO_3^{2-}$  has no obvious toxic effect on this material. This very slight improvement in half-wave potential is caused by the increase in the concentration of conductive ions. There is a larger increase in activity with the addition of  $Cl^-$  (Fig. S15(b)†). It is possible to relate to the pitting mechanism in a previous research in steel corrosion.<sup>38</sup> The effect on ORR activity of  $SO_3^{2-}$  and  $Cl^-$  is widely divergent with Wang and co-workers' experiments,<sup>30</sup> demonstrating that the real impact and



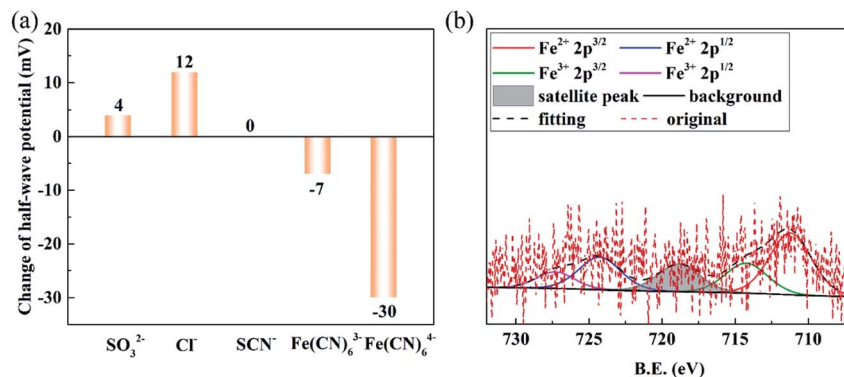


Fig. 5 The change in half-wave potential with the addition of some typical ions (a); the Fe 2p XPS result of FeNC-24 after CA test (b).

mechanism of poisoning toxic ions in different systems of FeNC material are highly important.

From the electrochemical measurements, Fe components are usually considered as important active sites for ORR activity. For XPS results, Fe could be divided into two valence of +2 and +3. Hence, the addition of complex ions are used to investigate which valence is the real active site for ORR. The LSV curves are shown in Fig. S16.†  $\text{SCN}^-$  is added to block  $\text{Fe}(\text{III})$ , which shows that it has no effect in half-wave potential. It is proposed that  $\text{Fe}(\text{II})$  might be the real source of activity rather than  $\text{Fe}(\text{III})$ .  $\text{Fe}(\text{CN})_6^{3-}$  is chosen to block  $\text{Fe}(\text{II})$ ; on the other hand,  $\text{Fe}(\text{CN})_6^{4-}$  is applied to block  $\text{Fe}(\text{III})$ . The obtained results reveal that the half-wave potential has a negative shift about 30 mV with the addition of  $\text{Fe}(\text{CN})_6^{3-}$  while that counterpart of  $\text{Fe}(\text{CN})_6^{4-}$  is only 7 mV. This significant gap in activity can reasonably prove that  $\text{Fe}(\text{II})$  is the centre of activity. In addition, it is observed in ion experiment is the difference of  $\text{SCN}^-$  and  $\text{Fe}(\text{CN})_6^{4-}$  in reducing the half-wave potential. It might be attributed to the oxidation of  $\text{Fe}(\text{CN})_6^{4-}$  in ORR process. As exhibit in Fig. S17,† the colour of the solution of 1 mM  $\text{Fe}(\text{CN})_6^{4-}$  changes from colourless into pale yellow after ORR test. While the electrolyte with 1 mM  $\text{Fe}(\text{CN})_6^{3-}$  is deep yellow, demonstrating some of  $\text{Fe}(\text{CN})_6^{4-}$  oxides into  $\text{Fe}(\text{CN})_6^{3-}$ , which blocks  $\text{Fe}(\text{II})$ , caused the small negative shift in half-wave potential. Some researches<sup>11,39–41</sup> demonstrate that KSCN has powerful ability in reducing the activity of Fe active sites. To sum up, for FeNC materials in different electron structure, skeleton structure and in even micro area environment, the real active site should to be analysed in specific circumstance.

The change in half-wave potential is summarized in Fig. 5(a). The XPS result of FeNC-24 after CA test is shown in Fig. 5(b). The valence states of Fe are still in +2 and +3 state, and +2 state is also the main valence state in the sample, which indicating the change in surface valence state of Fe is little after the CA test. Thus, the result of ion experiments is still applicable to sample after durability test.

## 4 Conclusions

A series of FeNC materials were synthesized by solvothermal-pyrolysis method with different dosage of 2-methylimidazole in this work.

No obvious crystalline structure was observed in these materials. And the N and metal atoms doped in carbon skeleton to form lots of defects and FeNC active sites. In addition, the particle sizes of FeNCs were uniformed and could be controlled by the dosage of 2-methylimidazole to some extent. Electrochemical measurements demonstrated that the ORR activity of samples increased first and then decreased with the increasing of 2-methylimidazole.

FeNC-24 had the highest half-wave potential of 0.852 V and ECSA among FeNCs. The half wave potential of FeNC-24 was only 9 mV lower than that of Pt/C. On the other hand, it also had favourable stability of ORR. The CA tests in the 50 000 s, retention rate of current density is 89.5%, and the morphology had no distinct difference after CA test. The tolerance of methanol test indicated the decrease in half-wave potential of FeNC-24 was only 20 mV in 3 M methanol, which was much lower than that of Pt/C. And the Tafel slope was  $122.6 \text{ mV dec}^{-1}$ , lower than Pt/C. Meanwhile, the ORR activity cannot be decreased by  $\text{Cl}^-$ ,  $\text{SO}_3^{2-}$  pollution ions.

The block test of activity sites indicated that  $\text{Fe}(\text{II})$  was an important active site, while the valence state had no change after the ORR test.

In this research, the synthesis conditions was optimized, and the real iron active species were revealed by the experiment of complex ions, which provided a new thinking and methods in the research of FeNC materials.

## Conflicts of interest

There are no conflicts to declare.

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