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New insight into the kinetic study on the different loadings of the CuO/CNT catalyst and its optimization for *p*-chloroaniline photodegradation†

Nur Farahain binti Khusnum,^a Aishah Abdul Jalil,^{ab} Arshad Ahmad,^{*ab} Muhammad Ikram,^{ab} Nurul Sahida Hassan,^a Walid Nabgan,^d Mahadi Bahari,^e Rafiziana Kasmani^{ab} and Norafneezah Norazahar^{ab}

The effect of the copper (Cu) content on Cu oxide loaded onto a carbon nanotube (CuO/CNT) catalyst on the mechanistic, kinetic, and photonic efficiency of the photodegradation of *p*-chloroaniline (PCA) under visible (Vis) and ultraviolet (UV) light irradiation has been explored. For low-loading (1–5 wt%) CuO/CNTs, photodegradation performed better under UV (>84%) rather than the Vis system; this may be due to the presence of abundant defect sites on both CuO and CNTs, which allowed the multielectron reduction of oxygen at their impurity levels to generate more hydrogen peroxide and subsequent ·OH radicals. The active species under UV were in the following order: $\text{h}^+ \gg \text{e}^- > \cdot\text{OH}$, while it was vice versa for the Vis system with a well-balanced 50 wt% CuO/CNT catalyst that exhibited a similar performance. The kinetic study showed the transition of the kinetic order from the zeroth to the first order on increasing the PCA concentration under the Vis system and vice versa for the UV system. The Thiele modulus (ϕ) further confirmed that the effect of internal mass transfer was negligible under UV light. In contrast, the transition from mass transfer to kinetic control limitation was observed under the Vis system. The optimum PCA degradation predicted from the response surface analysis was 97.36% at the reaction pH of 7.3, catalyst dosage of 0.45 g L⁻¹, and initial PCA concentration of 11.02 mg L⁻¹. The condition obtained was fairly close to the forecasted value with an error of 0.26%.

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Introduction

Over the last decades, advanced oxidation processes (AOPs) have been broadly industrialized to remediate water containing persistent organic pollutants.^{1,2} Among AOPs, semiconductor photocatalysis is applicable to a wide variety of applications. It can resolve environmental issues economically and safely, and has attracted increasing interest.^{3–6} However, conventional photocatalysis still faces unsolved problems such as the narrow spectral response range ($\lambda < 365$ nm) and low photon utilization

efficiency. Many strategies, such as the modification of the crystal structure of metal oxides, exposed facet-engineering, morphology tuning, constructing heterojunction structures, and improving carbon materials, have been investigated on the studied semiconductors to enhance charge separation.⁷ Recently, the use of smaller band gap semiconductors such as copper oxide (CuO) has become a matter of great significance because its light absorption is expected to be extended to the visible light (Vis) region. CuO is a p-type semiconductor with exciting properties such as high stability, direct bandgap (1.2–1.7 eV), plentiful sources, easy preparation, less harmful, inexpensive, and ecofriendly. CuO has been used as an active photocatalyst by many researchers previously.^{8–10} However, using CuO has some limitations; its narrow band gap causes the recombination of the photogenerated electrons and holes.¹¹

Innovative carbon materials, especially carbon nanotubes (CNTs) that have a metal oxide surface built into them to improve the photocatalytic activity, have become a hot topic.¹² CNTs have been shown to exhibit superior conductivity and electron mobility, high specific surface area, and stability that have become a component of semiconductors in various environmental applications.^{13,14} They also modify the light

^aSchool of Chemical and Energy Engineering, Faculty of Engineering, Universiti Teknologi Malaysia, 81310 UTM Johor Bahru, Johor, Malaysia. E-mail: arshad@utm.my

^bCentre of Hydrogen Energy, Institute of Future Energy, Universiti Teknologi Malaysia, 81310 UTM Johor Bahru, Johor, Malaysia

^cSolar Cell Applications Research Lab, Department of Physics, Government College University Lahore, 54000, Punjab, Pakistan. E-mail: dr.muhammadikram@gcu.edu.pk

^dDepartament d'Enginyeria Química, Universitat Rovira I Virgili, Av Països Catalans 26, 43007, Tarragona, Spain

^eFaculty of Science, Universiti Teknologi Malaysia, 81310 UTM Johor Bahru, Johor, Malaysia

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absorption properties due to changes in the dynamics of charge carriers and increase in the surface electrical charge of metal oxides in the composite.¹⁵ Niyaz *et al.* found out that the dyes Reactive Red 120 and Direct Red 31 from colored wastewater were successfully degraded by the CuO/CNT nanocomposite photocatalyst.¹⁶ Moreover, previous studies have also proved that combining CuO and CNTs can achieve the highest photodegradation efficiency of PCA under both Vis and UV light irradiation systems.^{17,18}

However, not many attempts have been made to quantify the activity in terms of photon efficiency for synthesized CNT semiconductor photocatalysts in recent years. In addition, most researchers have aimed at studying the effect of operating parameters on the degradation rate and design aspects of the reactor.^{19,20} To the best of our knowledge, the detailed work has been rarely reported in the literature. Hence, this study investigated those aspects thoroughly on the CuO/CNT catalyst towards the photodecomposition of PCA under both Vis and UV light irradiation systems. Optimization using the response surface methodology (RSM) was also examined to determine the optimal conditions for the degradation of PCA by the best catalyst.

Materials and methods

Materials, synthesis of the catalyst, and characterization

Multiwalled carbon nanotubes (MWCNTs) (CAS Num. 308068-56-6) with a diameter of 10–20 nm and a length of 10–50 nm were purchased from Chengdu Organic Chemicals Co., Ltd (China). *N,N*-Dimethylformamide (DMF) (CAS Num. 4472-41-7) was obtained from J. T. Baker and naphthalene (CAS Num. 91-20-3) was obtained from Fluka. Copper (Cu) (CAS Num. 7440-50-8) and platinum (Pt) (CAS Num. 7440-06-4) plates were purchased from Nilaco, Japan. Sodium hydroxide (NaOH) (CAS Num. 1310-73-2) and hydrochloric acid (HCl) (CAS Num. 7647-01-0) were obtained from Merck. *p*-Chloroaniline (PCA) (CAS Num. 7647-01-0) was obtained from Acros. Deionized water was used for the preparation of the pH solution. All chemicals and solvents used were guaranteed or analytical grade reagents

commercially available and used without further purification. In this work, a 36 W UV lamp (254 nm) and 39 W metal halide lamp (400 nm) were used for UV and visible light sources, respectively. The schematic of the reactor used is illustrated in Fig. 1. The details of the synthesis of the CuO/CNT photocatalysts, characterization, and the degradation of *p*-chloroaniline (PCA) were discussed in the previous paper.^{17,18}

Photonic efficiency

The photonic efficiency is introduced to quantify the efficiency of the reaction process in this study. The description of photonic efficiency proposed by Serpone as the number of molecules converted in relation to the total number of incident photons is shown in eqn (1).²¹

$$\Phi = \frac{r_0}{I} \quad (1)$$

where Φ is the photonic efficiency, r_0 is the initial reaction rate ($\text{mmol L}^{-1} \text{s}^{-1}$), and I is the photon flux ($\text{Einstein L}^{-1} \text{s}^{-1}$). The rates of the incident photon flux reaching the reactor were obtained by an actinometer. In this study, the measured photon flux (I) was 3.35×10^{-4} and 1.57×10^{-4} Einstein $\text{L}^{-1} \text{s}^{-1}$ for Vis and UV light irradiation systems, respectively.

Experimental design and optimization

In this study, a combination of mathematical and statistical methods by response surface methodology (RSM) was applied on the photodegradation of PCA to find the optimum value of the process variable. The main purpose of RSM was to find out a suitable model to predict and optimize the reactions. The optimum value of the independent variable is determined by finding a point known as the stationary point. A standard RSM analysis is used in conjunction with a central composite design (CCD) to generate reasonable experimental runs and to analyze the interaction between the variables. An analysis of variance (ANOVA) was also performed for the generated regression model to ensure its statistical significance.^{22,23}

Results and discussion

Photocatalytic performance and proposed mechanism of PCA under UV and Vis light irradiation

Fig. 2A exhibits the performance of all catalysts on the photodegradation of PCA after 300 min irradiation of light. The 40% photodegradation (not shown in the figure) from the photolysis result evidently showed that the presence of the catalyst was important in this study. It was observed that under Vis light, pristine CNTs exhibited almost similar activity as the lower CuO loading (<3 wt%) under UV light. However, increasing the CuO loading up to 50 wt% enhanced the degradation to 97%, verifying that the CuO/CNT composite with a band gap of 1.7 eV is indeed a Vis light-driven photocatalyst. At the same time, the activity of pristine CNTs was slightly lower under UV irradiation but increased with the increase in the CuO loading up to 3 wt% CuO/CNTs to give the highest degradation of PCA (96%). A further addition to 5 wt% CuO seems to inhibit degradation due

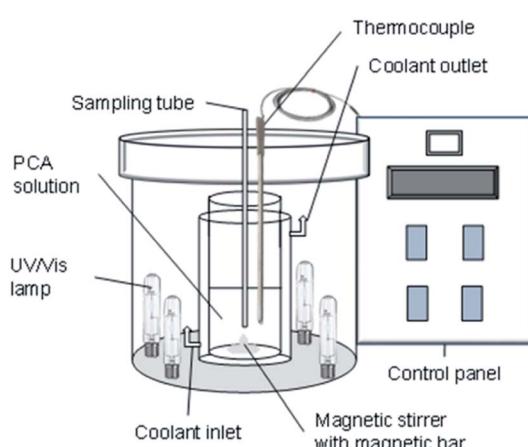


Fig. 1 Schematic of the photoreactor.



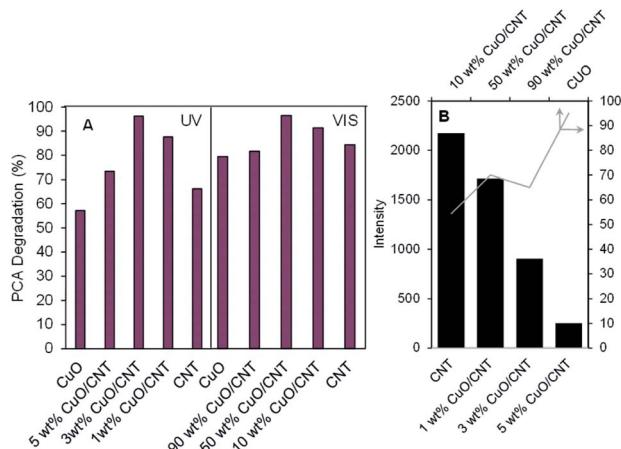


Fig. 2 (A) Performance of the CuO/CNT catalyst toward the photodegradation of PCA under both light irradiation systems. (B) Summary of ESR peaks for all catalysts.

to the excess dispersion of less active CuO on the surface of CNTs.¹⁷ From these results, it can be concluded that there is an optimum amount of CuO, which should be loaded on CNTs for the best Cu-CNT interaction for the enhanced degradation of PCA in both Vis and UV irradiation systems. For evaluation, an additional experiment on the photodegradation of PCA was conducted using commercial TiO₂ under the same conditions to compare the performance with the synthesized catalyst. As shown in Fig. S3,† the percentages of PCA degradation obtained by commercial TiO₂ under UV and Vis systems are only 38.4% and 56%, respectively. It is proved that the synthesized CuO/CNT catalyst has higher activity towards PCA photodegradation.

The unpaired electrons inside the catalyst were investigated previously by electron spin resonance (ESR) spectroscopy,^{17,18} and their peak intensities are summarized in Fig. 2B. It can be clearly observed that low CuO loading (1–5 wt%) onto CNTs, particularly 1 wt% CuO/CNTs, possessed more than twenty three times higher number of unpaired electrons than the higher CuO loading (10–90 wt%) catalysts. This is certainly due to the interaction between the Cu species with $\cdot\text{OH}$ and -COOH -enriched CNTs, which led to the formation of excess oxygen vacancies (OVs) or oxygen atom defects.^{1,24} Comparing 1 wt% CuO/CNTs with 3 wt% CuO/CNTs and 5 wt% CuO/CNTs, the number of unpaired electrons dropped about six folds, indicating that the charge compensation by the higher loading of Cu species fixed the defect sites of CNT backbones²⁵ In contrast, further introduction of Cu species from 10 to 90 wt% demonstrated an increasing amount of unpaired electrons, and this most probably came from the excess defect sites of Cu species (Cu^{2+} , Cu^+), which were unfulfilled by the low amount of CNTs. These variations in the defect sites undoubtedly offer an interesting impact that may lead to different PCA degradation pathways under both Vis and UV light irradiation.

Based on the abovementioned and previous data,¹⁷ the mechanism of PCA degradation over both ranges of CuO loaded onto CNTs under both UV and Vis light irradiation is proposed, as shown in Fig. 3. In fact, the energy potentials to reduce O_2 to

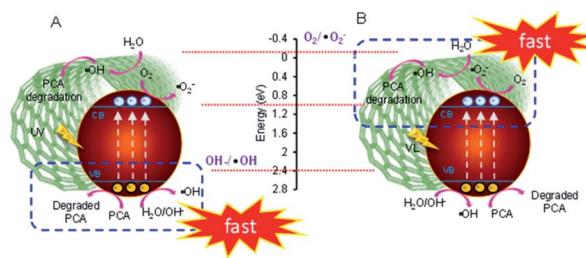


Fig. 3 Proposed mechanism of the reaction under (A) UV and (B) Vis light irradiation systems.

generate $\text{O}_2^{\cdot-}$ and $\cdot\text{OH}$ radicals are -0.046 eV (as shown in the figure) and 2.4 eV, respectively.²⁶ Thus, the excited electrons in the conduction band (CB) position of CuO (1.0 eV vs. NHE) can merely possibly generate $\cdot\text{OH}$ under both systems. For low CuO loading, it is obviously observed from Fig. 2A that generally, photodegradation performed better under Vis than UV irradiation. In addition, the performance under Vis light over low-loading CuO/CNTs is also similar when using CNTs under the UV light. This may be due to the higher number of defects where CNTs with a smaller bandgap (1.5 eV) than CuO was the main component, and this enabled the excitation of electrons not only from the valence band (VB) to the CB of CNTs and CuO but also between both the positions of its impurity levels. However, at a certain level of hybridization of Cu with CNTs, specifically, 3 wt% CuO/CNTs, the high energy of UV may exploit maximum electron excitation, while the optimum interaction between Cu-CNT may give adequate defect sites as well as oxygen vacancies (OV), which act as electron acceptors to suppress the e^-/h^+ recombination thus preserving the degradation. The holes (h^+) generated in both VBs of CNTs and CuO then react with water or hydroxyl anions (-OH) to generate $\cdot\text{OH}$ or directly react with PCA to degrade it.²⁷ This is in line with the scavenger results, which confirm that the active species that play an important role in UV degradation are in the following order: $\text{h}^+ \gg \text{e}^- > \cdot\text{OH}$.¹⁷

In the case of high-loading CuO/CNTs under Vis light, the electrons on the CB position of CuO and CNTs also faced the same circumstances for being unable to generate $\text{O}_2^{\cdot-}$ radicals. Still, they could be involved in the multielectron reduction of oxygen to generate hydrogen peroxide that finally gave $\cdot\text{OH}$ radicals.²⁸ The effect of the scavenger study proved that the important active species order was: $\text{e}^- \geq \cdot\text{OH} > \text{h}^+$, which signified that the impurity levels of both CNTs and CuO were significant in PCA degradation by exciting and accepting electrons, particularly in the well-balanced CuO-CNT ratio of 50 wt%.¹⁸ Further addition of copper may block the surface contact of CNTs, thus reducing the synergistic effect of both CuO-CNT and PCA degradation.

Kinetic study

Based on the abovementioned results, the two best catalysts, 3 wt% CuO/CNTs and 50 wt% CuO/CNTs were used to investigate the kinetics of PCA degradation under UV and Vis light irradiation, respectively. In fact, the effect of the initial



concentration ($10\text{--}100\text{ mg L}^{-1}$) on the degradation of PCA under UV and Vis systems is shown in Fig. S1.† Herein, three kinetic models were used: zeroth-, first-, and second-order, and are expressed from eqn (2) to eqn (4),²⁹

$$\frac{dC}{dt} = -k_{app_0} \quad (2)$$

$$\frac{dC}{dt} = -k_{app_1} C \quad (3)$$

$$\frac{dC}{dt} = -k_{app_2} C^2 \quad (4)$$

where C is the PCA concentration, t is the reaction time, and k_{app_0} , k_{app_1} , and k_{app_2} are the apparent rate constants of pseudo zeroth-, first-, and second-order kinetic models, respectively. An integration of these equations gave their linear form as expressed from eqn (5) to eqn (7),

$$(C_t) = (C_0) - k_{app_0} t \quad (5)$$

$$\ln\left(\frac{C_0}{C_t}\right) = k_{app_1} t \quad (6)$$

$$\frac{1}{(C_t)} = \frac{1}{(C_0)} + k_{app_2} t \quad (7)$$

where C_t is the PCA concentration after irradiation for time t .

The linear plots of these kinetic models under both UV and Vis systems are shown in Fig. S2.† The k_{app} and coefficient linear regression (R^2) values were obtained from the slopes of the resulting straight line and are tabulated in Table S1.† From the values, it is clearly observed that at a lower concentration range of $10\text{--}50\text{ mg L}^{-1}$, degradation under the UV system followed the first-order kinetic model, and this seems to deviate to the zeroth-order kinetic model when the concentration increased up to 100 mg L^{-1} (although the fitting to eqn (4) is still remarkable) and *vice versa* for degradation under the Vis system (Fig. 4). These kinetic transitions could be explained based on the schematic shown in Fig. 4. For the UV-irradiated system, the low concentration of PCA is supposed to be easily oxidized directly or indirectly *via* $\cdot\text{OH}$ radicals generated by holes, particularly in the VB of a major component of CNTs.¹⁷

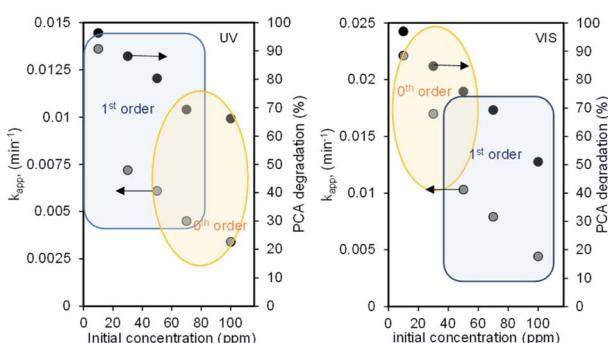


Fig. 4 Effect of the initial concentration on the reaction order under (A) UV and (B) Vis light irradiation systems.

A similar phenomenon occurred in the VB of CuO but increasing the concentration of PCA proportionally increased the generation of $\cdot\text{OH}$ radicals, including $\cdot\text{OH}$ generated from oxygen, which then acted as limiting reactants in the system and caused the reaction to be controlled by lower-order kinetics.³⁰ In contrast, the defect site-rich high CuO content-loaded CNTs allowed the excess excitation of electrons when irradiated by VL not only from the VB to CB of both CNTs and CuO but also from their impurity levels, and this led to the electrons with high energy to generate more $\cdot\text{OH}$ radicals, which became the limiting reactant at a lower PCA concentration and the degradation is not controlled by any concentration in the system. However, a higher concentration of PCA decreased the degradation rate and caused the transition from kinetic-controlled reaction to mass transfer limitation.³¹

Next, mass transfer studies were also done to determine the rate-limiting step for the adsorption of PCA from the aqueous solution on the catalyst. The influence of internal mass transfer was estimated by the Thiele modulus (ϕ) using eqn (8),³²

$$\phi = R_p \sqrt{\frac{k_v}{D_{eff}}} \quad (8)$$

where R_p is the catalyst size (m), k_v is an apparent rate constant, and D_{eff} is the effective diffusion coefficient. As shown in Fig. 5, the value of ϕ under Vis light is greater than 1 and higher than that under the UV system, signifying that the internal mass transfer resistance is significant for the former than the latter system, which is negligible.³² Hence, it supports the fact that the reaction was controlled by mass transfer rather than kinetics under the Vis system, and *vice versa* for the UV system.

Effect of CuO loading on initial rates and photonic efficiency

The photon efficiency (Φ) of PCA photodegradation was further investigated by relating the initial reaction rates of PCA (r_0) to the rates of the incident photons, reaching the reactor (I) by an actinometer (eqn (1)). As shown in Table 1, in the case of the UV system, r_0 increased proportionately with Φ up to 3 wt% CuO/CNTs, and then decreased when 5 wt% CuO was added. A similar trend was observed from 10 wt% CuO/CNTs to 50 wt% CuO/CNTs under the Vis system, but Φ considerably increased for 90 wt% CuO/CNTs. In both cases, the higher degree of defect sites or/and Cu–O–C interaction probably triggered more adsorption sites for PCA, which facilitated the

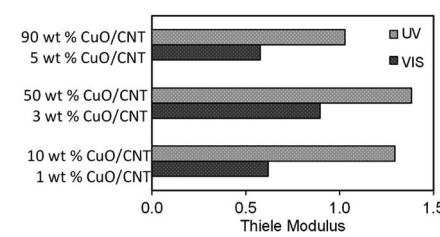


Fig. 5 Thiele Modulus of each catalyst for both light irradiation systems.

Table 1 Rates and photonic efficiency for each catalyst

Catalyst	Initial rate, r_0 ($\times 10^{-5}$ mmol L $^{-1}$ s $^{-1}$)	Photonic efficiency, Φ (%)
UV		
1 wt% CuO/CNTs	1.50	0.96
3 wt% CuO/CNTs	2.10	1.34
5 wt% CuO/CNTs	1.26	0.83
CuO	0.81	5.27
Vis		
10 wt% CuO/CNTs	1.83	2.01
50 wt% CuO/CNTs	2.14	6.39
90 wt% CuO/CNTs	1.39	45.7
CuO	2.17	21.0

photogenerated $e^- - h^+$ transfer and enhanced the photodegradation efficiency.^{17,18}

Photonic efficiency for hydroxyl radical generation

To quantify the rate of $\cdot OH$ radicals generated by the photo-generated holes on the catalyst surface, a known hydroxyl radical scavenger, methanol, was used and the reaction was performed with 3 wt% CuO/CNTs and 50 wt% CuO/CNTs under the UV and Vis systems, respectively.³³ As shown in Fig. 6A, the reduction trend of the methanol concentration as a function of time is similar under both UV and Vis systems. The degree of reduction is slightly higher for the latter, demonstrating that the rate of $\cdot OH$ generation under Vis is higher than that under UV irradiation. Considering the reaction following the pseudo-first-order Langmuir–Hinshelwood model, the initial rate of methanol reduction (r_0) could be calculated using eqn (7) by multiplying the value of k_{app} with the corresponding initial methanol concentration (Fig. 6B).³⁴

As tabulated in Table S2,† r_0 values are 4.40 and 8.93×10^{-7} mmol L $^{-1}$ s $^{-1}$, while the photonic efficiencies (Φ) obtained during the photocatalytic oxidation of 2 M methanol in aqueous suspension of the catalysts are 2.81 and 2.67×10^{-3} mmol Einstein $^{-1}$ for UV and VL system, respectively. These values

were calculated by assuming the relation $\Phi_{methanol} = 2\Phi_{\cdot OH}$, which agrees with the oxidation mechanism reported in the literature.³⁵ Due to the initial methanol concentration of 2 M, which can trap all photogenerated $\cdot OH$, these values can be taken as the maximum Φ obtainable in an $\cdot OH$ -mediated photocatalytic oxidation.

Both values in both systems are relatively smaller than the corresponding values listed in Table 2, confirming a part of the role of $\cdot OH$ in photodegradation. Although Φ for UV and Vis systems are almost similar, r_0 under Vis is two times higher than that under UV, further verifying the vital role of $\cdot OH$ under the former than that under the latter.

Optimization by response surface methodology (RSM)

In order to study the effect of reaction parameters on the catalytic performance of 50 wt% CuO/CNTs, a statistical approach was employed to design the experiments using CCD interface of RSM. All 16 experimental runs of CCD were performed. CCD was adopted to develop a model that predicts the interaction between the process parameters and response (PCA degradation percentage) (Sadhukhan *et al.*, 2016; Saeed *et al.*, 2015). As shown in Table S3,† three important parameters, pH (A), catalyst dosage (B), and PCA initial concentration (C) were considered as independent variables. At the same time, the photodegradation percentage (Y) was selected as the study's response (dependent variable). Based on the RSM result, the obtained data were matched into the general quadratic polynomial (eqn (9)) and the final model is stated in eqn (10):

$$y = \beta_0 + \sum_{i=1}^k \beta_i x_i + \sum_{i=1}^k \beta_{ii} x_i^2 + \sum_{i=1}^k \sum_{j=1}^k \beta_{ij} x_i x_j + \varepsilon \quad (9)$$

where y is the calculated response, β_0 is the intercept term, β_i , β_{ij} and β_{ii} are the measure of the effect of variable x_i , $x_i x_j$, and x_i^2 , respectively, and ε is the residual associated with the experiments.

$$Y = 96.5983 + 8.68A + 5.36B + 3.84C - 30.2448A^2 - 12.6448B^2 - 18.6448C^2 - 4.85AB - 15.45AC + 14.9BC \quad (10)$$

Fig. S4† shows the parity plot comparing the observed values of percentage degradation (%) with the predicted values. The coefficient of determination (R^2) is 0.9301, indicating that the model accounts for 93.01% of data variability. Haaland (1989) stated that the empirical model should be more than 0.75 in order to adequately explain most of the variability in reading the essay.³⁶ Table S4† shows the variance (ANOVA) analysis of the regression parameters for the predicted response surface quadratic model. According to the ANOVA results, the model was significant, as evidenced by a larger calculated F -value ($F_{model} = 5.38$) than a tabulated F -value ($F_{table} = 4.099$) for the respective degrees of freedom and probability ($p = 0.05$).³⁷

Simple approaches for studying and optimizing the efficiency of the reaction process include response surfaces and contour graphs. To better understand the relationship between the degradation of PCA and studied variables A, B, and C, three-dimensional surface graphs based on polynomial functions

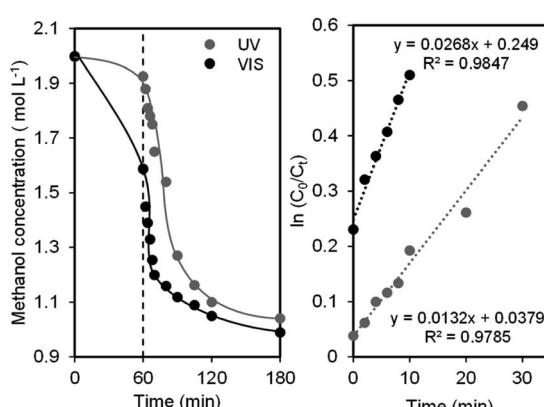


Fig. 6 (A) The evolution of methanol oxidation as a function of time and (B) pseudo-first order Langmuir–Hinshelwood model fitting.



Table 2 Rates and photonic efficiency for each parameter under both UV and Vis light irradiation

Condition	UV 3 wt% CuO/CNTs		Vis 50 wt% CuO/CNTs	
	Initial rate, ($\times 10^{-5}$ mmol L $^{-1}$ s $^{-1}$)	Photonic efficiency, Φ (%)	Initial rate, r_0 ($\times 10^{-5}$ mmol L $^{-1}$ s $^{-1}$)	Photonic efficiency, Φ (%)
pH				
3	1.08	0.69	1.63	4.86
5	1.18	0.75	1.68	5.02
7	2.10	1.34	2.14	6.39
9	1.89	1.21	1.79	5.37
11	2.06	1.31	1.22	3.64
Catalyst dosage (g L$^{-1}$)				
0.125	1.78	1.15	1.40	4.19
0.25	2.15	1.37	2.14	6.39
0.375	2.10	1.34	2.14	6.39
0.5	1.65	1.05	1.55	4.63
0.625	1.93	1.23	1.14	3.41
Initial concentration (mg L$^{-1}$)				
10	2.10	1.34	2.14	6.39
30	2.83	1.81	6.69	2.00
50	4.00	2.55	6.76	2.02
70	4.13	2.64	7.17	2.14
100	4.46	2.85	7.22	2.16

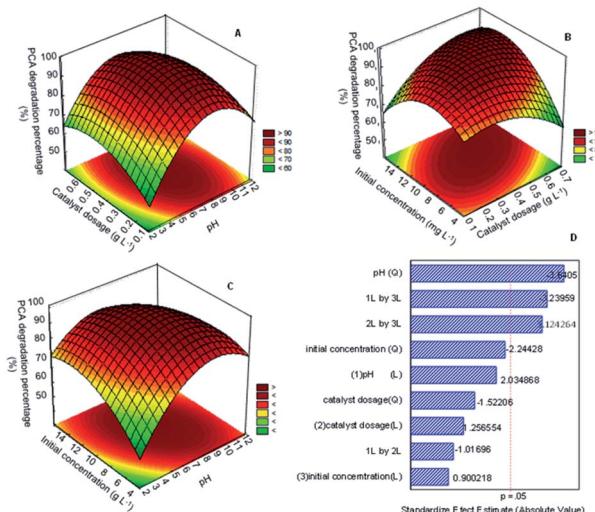


Fig. 7 Response surface plots for the photodegradation of PCA showing interaction between (A) catalyst dosage and pH, (B) initial concentration and catalyst dosage, (C) initial concentration and pH, and (D) Pareto chart of the standardized effect estimate.

were plotted. Fig. 7A displays the relationship between the catalyst dosage and pH, while Fig. 7B and C correspond to the initial concentration and catalyst dosage and initial concentration and pH. All the response surface plots have an elliptical shape, indicating a good interaction between the variables studied.³⁷

Fig. 7A shows the relationship between catalyst dosage and pH on PCA degradation onto the best catalyst. The result shows that the catalyst dosage did not give a much significant effect on

the PCA degradation at low pH (<5), but the degradation increased on increasing pH up to pH 9. This finding matched with the analysis of variance (ANOVA) in Table S4[†] and pareto chart in Fig. 7D, for which the mean square value (47.045) and *t*-value (-1.02) for 1 L by 2 L was lower compared to other variables, supporting that the relationship of these variables had less significant factor for PCA degradation. It might be due to excess catalyst covering the active surface and impeding light penetration. On the other hand, the rise in the number of hydroxyl groups competes with the PCA ions in the system. These phenomena would decrease the efficiency of the photodegradation of PCA.

The relationship between the initial concentration and the catalyst dosage is displayed in Fig. 7B. The result shows that the increase in the catalyst dosage up to 0.5 g L $^{-1}$ and initial concentration up to 10 mg L $^{-1}$ increased the PCA degradation. The relationship between these parameters gave quite a significant impact on the PCA degradation as the mean square value reached 444.04 and the *t*-value was 1.12. Nevertheless, a further increase in the catalyst dosage to more than 0.5 g L $^{-1}$ and 10 mg L $^{-1}$ of the PCA initial concentration decreased the PCA degradation. As mentioned before, the surplus amount of the catalyst used and high initial concentration of PCA could inhibit light penetration to the surface of the catalyst and thus reduce the formation of radicals that plays such an important role in degradation.

Fig. 7C shows the relationship between the initial concentration and pH. As shown, PCA degradation occurred when both the pH and initial concentration increased more than 10 mg L $^{-1}$ and pH 5, respectively. However, the degradation decreased with the decrease in both parameters. From this result, it could



be seen that both these parameters have a significant impact on the degradation of PCA. This finding matched with the analysis of variance (ANOVA) in Table S4† and Pareto chart in Fig. 6D, for which the mean square value (477.405) and *t*-value (−3.24) for 1 L by 3 L was higher compared to the other variables, supporting that the relationship of these variables had a highly significant factor in PCA degradation.

The *t*-distribution values in a Pareto chart, as well as the related *p*-values of the variables for the PCA degradation using CuO/CNTs are shown in Fig. 7D. The relevance of the related parameter was determined using the *p*-value and *t*-value, with the smaller *p*-value and larger figure of the *t*-value representing the more vital parameter. According to Fig. 7D, pH (*Q*) ($A^2 = 3.6405$), interaction pH (*A*) with initial concentration (*C*) ($AC = 3.23959$) and interaction catalyst dosage (*B*) with initial concentration (*C*) ($BC = 3.124264$) are the most significant variables for PCA degradation, followed by initial concentration (*Q*) ($C^2 = 2.24428$), owing to the *p*-value < 0.05.

The optimum PCA degradation predicted from the response surface analysis was 97.36% at pH 7.3, catalyst dosage of 0.45 g L^{−1}, and initial concentration of 11.01 mg L^{−1}. A confirmation experiment was performed to validate the optimization results obtained from the response surface analysis. The PCA degradation of the experiment under optimal conditions was 97.1% and the difference between the predicted and observed values was 0.26%.

Conclusions

In this study, a low- (1–5 wt%) and high-loading (10–90 wt%) of CuO in a CuO/CNT catalyst were studied in detail for their mechanistic, kinetics, and photonic efficiency. From the results, the low-loading of CuO achieved higher degradation under UV compared to Vis. The excess defect sites from CuO and CNTs were found to be the cause for the multielectron reduction of oxygen at their impurity levels to generate more hydrogen peroxide and subsequent ·OH radicals. However, 3 wt% CuO/CNTs reached the highest degradation (96%) under UV irradiation due to the creation of more Cu-CNT interaction, oxygen vacancies, and defect sites, which act as electron acceptors to hinder the recombination of electrons and holes. In contrast, the same achievement was obtained by the high-loading of CuO (50 wt% CuO/CNTs) under Vis irradiation. It can be alleged that an optimum amount of CuO should be loaded on CNTs to enhance the performance under both UV and Vis systems. The kinetic study showed the transition of the kinetic order from the first to zeroth order under the UV system on increasing the PCA concentration, and *vice versa* for the Vis system. The effect of internal mass transfer was found to be negligible under the UV light as the value of the Thiele modulus (ϕ) obtained was less than 1 ($\phi_{\text{Vis}} > 1$). Hence, it supports the fact that under the UV system, the reaction is controlled by kinetics rather than mass transfer and *vice versa* for the VIS system. Optimization by response surface methodology over the best catalyst of 50 wt% CuO/CNTs indicated that pH was the main parameter affecting the reaction with a 97.36% degradation at pH 7.3, catalyst dosage of 0.45 g L^{−1}, and PCA initial

concentration of 11.02 mg L^{−1}. The condition obtained was fairly close to the predicted value with an error of 0.26%.

Author contributions

Nur Farahain Khusnun: formal analysis; investigation; methodology; validation; writing – original draft, Aishah Abdul Jalil: conceptualization; funding acquisition; supervision; writing – original draft, Ahmad Arshad: conceptualization; supervision Muhammad Ikram: conceptualization; resources, Nurul Sahida Hassan: validation; writing – review & editing, Mahadi Bahari: writing – original draft, Walid Nabgan: writing – original draft, Rafiziana Kasmani: supervision Norafneezza Norazahar: validation.

Conflicts of interest

There are no conflicts to declare.

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Notes and references

- 1 C. N. C. Hitam, A. A. Jalil and Y. O. Raji, *Top. Catal.*, 2020, **63**, 1169–1181.
- 2 C. N. C. Hitam, A. A. Jalil, S. M. Izan, M. S. Azami, M. H. Hassim and N. Chanlek, *Powder Technol.*, 2020, **375**, 397–408.
- 3 A. Fauzi, A. Jalil, C. Hitam, F. Aziz and N. Chanlek, *J. Environ. Chem. Eng.*, 2020, **8**, 104484.
- 4 L. Gnanasekaran, R. Pachaiappan, P. S. Kumar, T. K. A. Hoang, S. Rajendran, D. Durgalakshmi, M. Soto-Moscoso, L. Cornejo-Ponce and F. Gracia, *Environ. Pollut.*, 2021, **287**, 117304.
- 5 S. Rajendran, R. Pachaiappan, T. K. A. Hoang, S. Karthikeyan, L. Gnanasekaran, S. Vadivel, M. Soto-Moscoso and M. A. Gracia-Pinilla, *J. Hazard. Mater.*, 2021, **416**, 125989.
- 6 G. Ramalingam, R. Pachaiappan, P. S. Kumar, S. Dharani, S. Rajendran, D.-V. N. Vo and T. K. A. Hoang, *Chemosphere*, 2022, **288**, 132448.
- 7 M. Azami, A. Jalil, N. Hassan, I. Hussain, A. Fauzi and M. Aziz, *J. Hazard. Mater.*, 2021, **414**, 125524.
- 8 R. Katal, S. Masudyanah, E. Y. J. Kong, N. Dasineh Khiavi, M. H. D. Abadi Farahani and X. Gong, *Catal. Today*, 2020, **340**, 236–244.
- 9 D. C. T. Nguyen, K. Y. Cho and W.-C. Oh, *Sep. Purif. Technol.*, 2019, **211**, 646–657.
- 10 A. Jalil, M. Satar, S. Triwahyono, H. Setiabudi, N. Kamarudin, N. Jaafar, N. Sapawe and R. Ahamad, *J. Electroanal. Chem.*, 2013, **701**, 50–58.



11 S. S. Hossain, M. Tarek, T. D. Munusamy, K. M. Rezaul Karim, S. M. Roopan, S. M. Sarkar, C. K. Cheng and M. M. Rahman Khan, *Environ. Res.*, 2020, **188**, 109803.

12 Z. Liu, X. Cui, C. Piao, J. Tang, S. Li, D. Fang and J. Wang, *Powder Technol.*, 2020, **368**, 213–226.

13 S. Bargozideh, M. Tasviri and M. Ghabraei, *Environ. Sci. Pollut. Res. Int.*, 2020, **27**, 36754–36764.

14 Y. Chen, J. Qian, N. Wang, J. Xing and L. Liu, *Inorg. Chem. Commun.*, 2020, 119.

15 I. Ahmad, S. Shukrullah, M. Y. Naz, M. A. Rasheed, M. Ahmad, E. Ahmed, M. S. Akhtar, N. R. Khalid, A. Hussain and S. Khalid, *Int. J. Hydrogen Energy*, 2021, **46**, 26711–26724.

16 N. M. Mahmoodi, P. Rezaei, C. Ghotbei and M. Kazemeini, *Fibers Polym.*, 2016, **17**, 1842–1848.

17 N. Khusnun, A. Jalil, S. Triwahyono, N. Jusoh, A. Johari and K. Kidam, *Phys. Chem. Chem. Phys.*, 2016, **18**, 12323–12331.

18 N. Khusnun, A. Jalil, S. Triwahyono, C. Hitam, N. Hassan, F. Jamian, W. Nabgan, T. Abdullah, M. Kamaruddin and D. Hartanto, *Powder Technol.*, 2018, **327**, 170–178.

19 T. A. Kandiel, R. Dillert, L. Robben and D. W. Bahnemann, *Catal. Today*, 2011, **161**, 196–201.

20 L. A. Al-Hajji, A. A. Ismail, M. Faycal Atitar, I. Abdelfattah and A. M. El-Toni, *Ceram. Int.*, 2019, **45**, 1265–1272.

21 N. Serpone, *J. Photochem. Photobiol. A*, 1997, **104**, 1–12.

22 M. A. Bezerra, R. E. Santelli, E. P. Oliveira, L. S. Villar and L. A. Escaleira, *Talanta*, 2008, **76**, 965–977.

23 H. Chaker, A. E. Attar, M. Djennas and S. Fourmentin, *Chem. Eng. Res. Des.*, 2021, **171**, 198–212.

24 N. S. Hassan, A. A. Jalil, F. F. A. Aziz, A. A. Fauzi, M. S. Azami and N. W. C. Jusoh, *Top. Catal.*, 2020, **63**, 1145–1156.

25 A. V. Sidorenko, P. A. Rodnyi, O. Guillot-Noel, D. Gourier and C. W. E. Van Eijk, *Phys. Solid State*, 2003, **45**(9), 1676–1678.

26 Z. Cai, Y. Song, X. Jin, C. C. Wang, H. Ji, W. Liu and X. Sun, *Sci. Total Environ.*, 2021, **781**, 146754.

27 F. Aziz, A. Jalil, N. Hassan, C. Hitam, A. Rahman and A. Fauzi, *J. Hazard. Mater.*, 2021, **401**, 123277.

28 A. Zada, M. Khan, M. A. Khan, Q. Khan, A. Habibi-Yangjeh, A. Dang and M. Maqbool, *Environ. Res.*, 2021, **195**, 110742.

29 M. Shaban, M. R. Abukhadra, A. Hamd, R. R. Amin and A. Abdel Khalek, *J. Environ. Manage.*, 2017, **204**, 189–199.

30 D. Dimitrakopoulou, I. Rethemiotaki, Z. Frontistis, N. P. Xekoukoulotakis, D. Venieri and D. Mantzavinos, *J. Environ. Manage.*, 2012, **98**, 168–174.

31 D. Klauson, J. Babkina, K. Stepanova, M. Krichevskaya and S. Preis, *Catal. Today*, 2010, **151**, 39–45.

32 M. V. Martin, O. M. Alfano and M. L. Satuf, *J. Environ. Chem. Eng.*, 2019, **7**, 103478.

33 R. Gao, J. Stark, D. W. Bahnemann and J. Rabani, *J. Photochem. Photobiol. A*, 2002, **148**, 387–391.

34 D. Jiang, H. Zhao, Z. Jia, J. Cao and R. John, *J. Photochem. Photobiol. A*, 2001, **144**, 197–204.

35 J. Marugán, D. Hufschmidt, M.-J. López-Muñoz, V. Selzer and D. Bahnemann, *Appl. Catal. B*, 2006, **62**, 201–207.

36 P. D. Haaland, *Experimental Design in Biotechnology*, CRC press, 2020.

37 N. F. Khusnun, A. A. Jalil, T. A. T. Abdullah, S. S. M. Latip, C. N. C. Hitam, A. A. Fauzi, N. S. Hassan, M. A. H. Aziz, A. F. A. Rahman, F. F. A. Aziz, M. Bahari, R. H. Adnan and R. Saravanan, *J. CO₂ Util.*, 2022, **58**, 101901.

