The low overpotential regime of acidic water oxidation part II: trends in metal and oxygen stability numbers‡

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The operating conditions of low pH and high potential at the anodes of polymer electrolyte membrane electrolyzers restrict the choice of catalysts for the oxygen evolution reaction (OER) to oxides based on the rare metals iridium or ruthenium. In this work, we investigate the stability of both the metal atoms and, by quantitative and highly sensitive $^{18}$O isotope labelling experiments, the oxygen atoms in a series of RuO$_x$ and IrO$_x$ electrocatalysts during the OER in the mechanistically interesting low overpotential regime. We show that materials based on RuO$_x$ have a higher dissolution rate than the rate of incorporation of labelled oxygen from the catalyst into the O$_2$ evolved (“labelled OER”), while for IrO$_x$-based catalysts the two rates are comparable. On amorphous RuO$_x$, metal dissolution and labelled OER are found to have distinct Tafel slopes. These observations together lead us to a full mechanistic picture in which dissolution and labelled OER are side processes to the main electrocatalytic cycle. We emphasize the importance of quantitative analysis and point out that since less than 0.2% of evolved oxygen contains an oxygen atom originating from the catalyst itself, lattice oxygen evolution is at most a negligible contribution to overall OER activity for RuO$_x$ and IrO$_x$ in acidic electrolyte.

Broader context

Water electrolysis, which produces hydrogen (H$_2$) and oxygen (O$_2$) from water and electricity, is a central technology for decarbonization of industry and transport. Polymer electrolyte membrane electrolysis cells have several advantages over other electrolysis technologies but require the rare element iridium to catalyze water oxidation in the high-potential, low-pH environment of the anode. Iridium is produced as a byproduct of platinum mining in only 3 times the annual global production of Ir (ref. 9), and so is also a significant bottleneck in technologies essential to enabling society’s transition away from fossil fuels. In the requirement of the extremely rare noble metal iridium (Ir) in the anode of polymer electrolyte membrane electrolysis cells (PEMFC) for production of H$_2$ by water electrolysis with renewable electricity, the most-studied alternatives to Ir-based PEMFC anode electrocatalysts are oxides based on ruthenium (Ru), which show lower stability, but slightly higher OER activity, than Ir-based oxides. However, Ru is, like Ir, a platinum mining byproduct with only ~3 times the annual global production of Ir (ref. 9), and so is also

Introduction

A major bottleneck in technologies essential to enabling society’s transition away from fossil fuels looms in the requirement of the extremely rare noble metal iridium (Ir) in the anode of polymer electrolyte membrane electrolysis cells (PEMFC) for production of H$_2$ by water electrolysis with renewable electricity. The most-studied alternatives to Ir-based PEMFC anode electrocatalysts are oxides based on ruthenium (Ru), which show lower stability, but slightly higher OER activity, than Ir-based oxides. However, Ru is, like Ir, a platinum mining byproduct with only ~3 times the annual global production of Ir (ref. 9), and so is also
insufficiently scalable. Continued research in Ru- and Ir-based oxides is nonetheless valuable because: (i) modest improvements in stability and activity improve the scalability of Ir or Ru-based PEMEC technology by enabling electrolyser devices to run at the same efficiency with lower catalytic loading; and (ii) a better understanding of why these two materials are relatively active and stable helps guide the discovery of new acid-stable OER catalysts based on more abundant elements.

Stability and catalytic activity of metal oxides for the OER are linked through the reactivity of oxygen atoms: metal–oxygen bonds are formed and broken during the electrocatalytic cycle oxidizing water, and metal–oxygen bonds are also what holds the material together. A way to probe this interplay is by isotope labelling of the oxygen in the electrocatalyst with $^{18}$O and determining whether this labelled oxygen is incorporated in the O$_2$ released and/or unlabelled oxygen from the electrolyte is incorporated in the electrocatalyst during operation. In acidic electrolyte (the focus of our study) incorporation of labelled oxygen in O$_2$ has previously been detected from amorphous oxides of iridium formed by thermal decomposition of HIrCl$_6$ (ref. 10) potential cycling$^{11,12}$ or leaching of SrIrO$_3$ (ref. 11) as well as RuO$_x$ sputter-deposited on a porous membrane$^{13}$ and doped nanocrystalline RuO$_2$ (ref. 14), but not on smooth crystalline IrO$_2$ (ref. 11 and 12) or RuO$_2$ (ref. 15). In alkaline electrolyte, incorporation of labelled oxygen in O$_2$ was detected from perovskite electrocatalysts with oxygen vacancies (La$_{0.5}$Sr$_{0.5}$CoO$_3$ and Pr$_{0.5}$Sr$_{0.5}$CoO$_3$) (ref. 16) and spinel Co$_3$O$_4$ (ref. 17), but not LaCoO$_3$ (ref. 16) or NiFeO$_x$ (ref. 18). Fig. 1 compiles these results from prior isotope-labelling studies:

Studies that showed labelled oxygen evolution are above the x-axis. Of these, studies where the amount of labelled oxygen evolution was shown to be more than one monolayer are further located in one of the top two sectors (I or II). studies where the amount of labelled oxygen evolution was shown to be more than the amount of metal dissolution during the same measurement are further located in one of the two left sectors (I or III).

Comparison of results in isotope-labeling OER studies is complicated by the use of varying experimental procedures, which are compiled in Table S1 (ESI†). To summarize the variety of experimental procedures: isotopic signals (or lack thereof) in the evolved O$_2$ have been detected by several in situ electrochemistry – mass spectrometry (EC-MS) techniques including differential EC-MS (DEMS)$^{10,13,14,17,19}$ on-line EC-MS (OLEMS)$^{15,16,20}$ and chip EC-MS.$^{18,21}$ The isotopic composition of the oxygen in the electrocatalyst has been measured by ex situ isotope-sensitive techniques including Raman spectroscopy,$^{22}$ atomic probe tomography (APT)$^{23}$ and low-energy ion scattering spectrometry (LEIS).$^{18}$ While most studies use various methods to isotopically label the electrocatalyst,$^{11,12,21–24}$ some instead label the electrolyte.$^{10,18}$

When the isotopic label of the electrocatalyst has been detected in the evolved O$_2$, it has often been attributed to a “lattice oxygen evolution mechanism” (LOM), of which several have been proposed.$^{7,11,16,25,26}$ In both acidic and alkaline electrolytes, observation of a LOM has been proposed to be associated with increased activity compared to catalysts which only produce oxygen through the conventional mechanism involving sequential adsorption and deprotonation of water,$^{11,23}$ while in acidic electrolytes it has also been correlated with electrocatalyst dissolution.$^{11,12}$ None of these works, however, provides an explicit definition of “lattice oxygen”, implicitly equating it with the “labelled oxygen” that the experiment is able to measure. The distinction is however important: labelled

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Fig. 1: Summary of results of $^{18}$O isotope-labelling studies. The y-axis indicates the amount of labelled oxygen detected in the O$_2$ evolved. If no labelled oxygen is detected from the electrocatalyst, it is placed below the x-axis. If the labelled oxygen evolution exceeded metal dissolution, the study is placed above the horizontal line labelled $n_O = 1$ ML in either sector I or II. The x-axis indicates the amount of metal dissolved from the catalyst. If the labelled oxygen evolution exceeded metal dissolution, the study is placed above the 45° line labelled $n_O = n_{diss}$ in either sector I or III. The two dashed lines thus divide the space into four sectors with the following implied meanings: (I) true lattice oxygen evolution, (II) degradative lattice oxygen evolution, (III) surface bound oxygen evolution, and (IV) labelled oxygen evolution of unknown origin. A is ref. 10; B is ref. 12; C is ref. 14; D is ref. 24; E is ref. 16; F is ref. 15; and G is ref. 18.
oxygen can include water intercalated in an electrocatalyst, and at the surface of the electrocatalyst it is not trivial to categorize oxygen atoms as “adsorbed oxygen” vs. “lattice oxygen”, nor is it trivial to know for sure if they can be labelled or will exchange spontaneously with oxygen atoms in the electrolyte.

We propose, in line with previous work,\textsuperscript{16,27,28} that lattice oxygen should be defined as oxygen atoms with the same coordination environment as is experienced by oxygen in the bulk of a crystalline material. Loosely adsorbed water molecules or oxygen adsorbed on secondary oxide phases are not considered lattice oxygen by this definition, and can also not easily be isotopically labelled since they are in equilibrium with the bulk electrolyte. Tightly coordinated oxygen atoms on the surface can be borderline cases. For instance, on the (110) surface of rutile RuO\textsubscript{2} or IrO\textsubscript{2}, our definition of “lattice oxygen” includes three-fold coordinated surface oxygen but excludes any oxygen adsorbed on metal coordinatively unsaturated (CUS) sites as well as bridging oxygen atoms, even though bridging oxygen atoms do not exchange spontaneously with the electrolyte at the open-circuit potential\textsuperscript{29} and can thereby retain an isotopic label from synthesis to the start of OER. See Fig. S1 of the (ESI?) for further discussion of this definition.

To test a lattice oxygen evolution mechanism according to this definition of lattice oxygen, two conditions need to be met: (i) an experiment should show that the amount of labelled oxygen from the electrocatalyst which is incorporated in the O\textsubscript{2} evolved (\(n_0\)) exceeds one monolayer equivalent (1 ML), as otherwise the labelled oxygen could come from tightly bound surface adsorbed oxygen such as bridging oxygen. Furthermore, to examine that lattice oxygen evolution is a catalytic mechanism and not part of a degradation process, (ii) an experiment should also show that the amount of lattice oxygen evolved exceeds the amount of metal dissolved (\(n_{\text{diss}}\)), which can be measured by inductively coupled plasma – mass spectrometry (ICP-MS). We indicate the studies that satisfy either of these two criteria by the divisions in Fig. 1: if criterion (i) is met, a study lies above the \(n_0 = 1\) ML line; and if criterion (ii) is met, it lies above the \(n_0 = n_{\text{diss}}\) line. Unfortunately, most prior studies were qualitative in nature and did not measure the electrochemically active surface area, and/or did not measure metal dissolution. To the best of our knowledge, sector I of Fig. 1 is empty, i.e., no isotope-labelling study of oxygen evolution electrocatalysis has conclusively shown a lattice oxygen evolution mechanism according to these criteria.

Quantitative results are also needed to gauge the potential importance of a lattice oxygen evolution mechanism if it does occur. To this end, with inspiration from the “stability number” introduced by Geiger and Kaskan et al.,\textsuperscript{11} we introduce the oxygen stability number as the total number of O\textsubscript{2} molecules evolved divided by the number of labelled oxygen atoms from the electrocatalyst incorporated in the O\textsubscript{2}. Like the original stability number\textsuperscript{11} (here referred to as the metal stability number to avoid confusion), which is the number of O\textsubscript{2} evolved divided by the number of metal atoms dissolved, the oxygen stability number of an electrocatalyst material is in general a function of the electrolysis conditions such as the applied current density.

In this article, we present an extensive dataset of labelled oxygen evolution and metal dissolution for a range of ruthenium and iridium based oxides prepared with \(^{16}\text{O}\) during electrolysis in acidic electrolyte in the mechanistically interesting low-overpotential regime. We use chip EC-MS to detect oxygen evolved during OER, LEIS to characterize the isotopic label on the electrocatalytic surface before and after OER, and ICP-MS to measure metal dissolution; and the results are organized in a homemade relational database accompanying this article. In addition to being fully quantitative, these are by far the most sensitive isotope labelling experiments in OER to date: while, for example, SFC-OLEMS has a detection limit of \(~4\) nmol s\(^{-1}\) cm\(^{-2}\) (ref. 30) chip EC-MS has a detection limit of \(<1\) pmol s\(^{-1}\) cm\(^{-2}\) (ref. 31). It is this sensitivity which enables us to quantify labelled oxygen evolution in a low current regime where depletion of the isotopic label can be ruled out, allowing us to determine conclusively the oxygen stability numbers, and thus the relative importance of the adsorbate oxidation and lattice oxygen oxidation mechanisms to the OER activity. By comparing trends in metal stability number and oxygen stability number across materials and applied current densities, we are able to sketch a general mechanistic picture relating water oxidation, lattice oxygen evolution, and metal dissolution in Ru- and Ir-based catalysts for water oxidation in acid.

Results

Fig. 2a is a sketch of the experimental procedure, described in detail in the Experimental section. Briefly, isotopically labelled Ru\textsuperscript{18}O\textsubscript{2} and Ir\textsuperscript{18}O\textsubscript{2} catalysts were synthesized, usually by reactive sputter deposition in a plasma including \(^{16}\text{O}_{2}\), and the initial surface isotopic composition was characterized by LEIS. Samples were tested at constant current in the chip EC-MS setup modified to collect electrolyte samples for ICP-MS measurements of metal dissolution before post-reaction LEIS characterization. The dissolution of OER catalysts is known to be dependent on the flow characteristics of the setup\textsuperscript{32} – in this regard, the stagnant thin layer of electrolyte in the EC-MS setup resembles more the environment experienced by an OER catalyst in a PEMEC than do most aqueous model systems.

Fig. 2b shows raw EC-MS data from a typical experiment, here for a catalyst of amorphous ruthenium oxide created by reactive sputter deposition at room temperature (s-25 °C Ru\textsuperscript{18}O\textsubscript{2}). Signals associated with O\textsubscript{2} at \(m/z = 32\) (\(^{16}\text{O}_{2}\)) and \(m/z = 34\) (\(^{16}\text{O}^{18}\text{O}\)) and with CO\textsubscript{2} at \(m/z = 44\) (\(^{12}\text{C}^{16}\text{O}_{2}\)) and \(m/z = 46\) (\(^{13}\text{C}^{16}\text{O}_{2}\)) increased at the start of the electrolysis period. There was a detectable amount of C\textsubscript{18}O\textsubscript{2} at \(m/z = 48\) but \(^{18}\text{O}_{2}\) at \(m/z = 36\) was not detectable; the small \(m/z = 36\) signal observed moves together with N\textsubscript{2} (\(m/z = 28\)) and \(^{40}\text{Ar}\) (\(m/z = 40\)) and is therefore attributed to \(^{36}\text{Ar}\) in air. The detected CO\textsubscript{2} decreased with time and can be attributed to the oxidation of adventitious carbon species adsorbed on the catalyst surface. The isotopic analysis of CO\textsubscript{2} formed electrochemically was the subject of two recent works,\textsuperscript{31,33} and will not be evaluated in detail in the present work, where we focus on isotopic signals of O\textsubscript{2}. The four
Electrolyte sampling events during electrolysis were visible in the $m/z = 28$ signal, as the fresh electrolyte drawn into the cell is air-saturated. Each sample of the electrolyte involves collecting $\sim 200 \mu L$ to ensure that the entire working electrolyte of $2 \mu L$ is collected and replenished with fresh electrolyte. However, electrolyte sampling did not cause a change in the electrochemical potential or steady state $O_2$ signals at $m/z = 32 \ (^{16}O_2)$ and $m/z = 34 \ (^{16}O^{18}O)$, which indicates that the electrolyte flow did not influence the electrochemical kinetics.

Careful analysis of the data in Fig. 2b reveals that some labelled oxygen from the amorphous RuO$_x$ catalyst was incorporated into the $O_2$ evolved. In order to understand whether the $m/z = 34$ signal can be fully accounted for by the natural 0.20% abundance of $H_2^{18}O$ in the electrolyte, corresponding to a natural $^{16}O^{18}O/^{16}O_2$ ratio of 0.40%, we re-plot the $O_2$ signals of Fig. 2b in Fig. 3a as an “isotope-tracking plot”. In the middle panel of Fig. 3a, calibrated and background-subtracted $O_2$ signals are plotted vs. time on two separate linearly scaled y-axes, with the $^{16}O^{18}O$ flux plotted in red on a left y-axis and the $^{18}O_2$ flux plotted in black on a right y-axis. The two axes are scaled according to the natural $^{16}O^{18}O/^{16}O_2$ ratio of 0.40%. The natural $^{16}O^{18}O/^{16}O_2$ ratio was confirmed regularly by OER with un-labelled samples, consistently resulting in 0.400% ± 0.005%. Plotted this way, whenever $^{18}O$ from the labelled oxide electrocatalysts is incorporated in the $O_2$ evolved, the red trace will deviate from the black trace. In this experiment (Fig. 3a), the red trace exceeds the black trace by about 0.5 pmol s$^{-1}$ cm$^{-2}$ only of $^{16}O^{18}O$ flux, easily discernible due to the sensitivity of the method. This is the rate at which labelled oxygen from the electrocatalyst was incorporated into the $O_2$ evolved. In comparison, the total OER rate was 1300 pmol s$^{-1}$ cm$^{-2}$ only $\sim 50$ ppm of the total oxygen evolved contained a labelled oxygen atom. The integrated excess $^{18}O$ in the $O_2$ was about 750 pmol cm$^{-2}$.

The ruthenium dissolution rate was about 20 pmol s$^{-1}$ cm$^{-2}$ this is about a factor 60 smaller than the rate of oxygen evolution (1300 pmol s$^{-1}$ cm$^{-2}$), consistent with Roy et al., but at the same time about a factor 40 larger than the rate of labelled oxygen incorporated in the $O_2$ evolved (0.5 pmol s$^{-1}$ cm$^{-2}$). This result is shown in the top panel of Fig. 3a as the normalized rate of ruthenium dissolution indicated in pmol s$^{-1}$ cm$^{-2}$ for each electrolyte sample taken during electrolysis. The average ruthenium dissolution rate was the highest at the start of the electrolysis period and slowly decreased with time. Note the dissolution rate plotted in the top panel is averaged over the time interval between the taking of electrolyte samples, but that this value underestimates the dissolution rate at the start of the electrolysis period. To further facilitate the quantitative comparison between the amounts of dissolution and labelled oxygen evolution, their integral values in pmol cm$^{-2}$ are displayed as annotations with blue font in Fig. 3a. Two timespans are used for the integral values: one for the ramp-up and first 2 minutes of electrolysis, during which capacitive charging makes up a significant portion of the current and the other for the remainder of the electrolysis in steady-state. Taking into account that the Ru dissolution.
commences with the onset of applied current, the ramp-up to 0.5 mA cm$^{-2}$geo (\(\sim 1.4 \text{ V}_{\text{RHE}}\)) was found to have more than 100 Ru atoms dissolved per labelled oxygen in the evolved O$_2$ (6500 pmol cm$^{-2}$geo dissolved Ru compared to 60 pmol cm$^{-2}$geo labelled OER), in contrast to the reduced dissolution rate of \(\sim 40\) Ru atoms dissolved per labelled oxygen atom evolved during steady state electrolysis (27 000 pmol cm$^{-2}$geo dissolved Ru compared to 680 pmol cm$^{-2}$geo labelled OER).

The labelled oxygen evolved during 30 minutes of electrolysis was \(\sim 2\%\) of a monolayer, using the capacitive charging current to determine the surface area, whereas the ruthenium dissolution approximately corresponded to one monolayer. In the first article of this series,\textsuperscript{25} we showed that ruthenium oxides sputter-deposited at a series of temperatures ranging from 25 °C to 400 °C had widely varying activity on a geometric basis, but that activity converges when normalizing by capacitive charging current, motivating capacitive charging current as a measure of the electrochemically active surface area (ECSA) on these catalysts. To determine the number of moles in a monolayer equivalent, we further use a specific capacitance of 115 \(\mu\text{F cm}^{-2}\text{geo}\) from ref. 35 and an active site density of 5 nm$^{-2}$, which is the density of coordinatively unsaturated sites on RuO$_2$(110). The fact that the amount of labelled oxygen evolution is much lower than a monolayer equivalent implies that it is likely limited to oxygen atoms at the surface of the catalyst, such as bridging oxygen atoms.

The experiment described in Fig. 2 and 3 was performed on a range of Ir$^{18}$O labelled electrocatalysts (see Experimental section and ESI†), most with multiple repetitions on separate samples of the same electrocatalyst type, and all details are included in the ESI† and in the online repository. As an illustrative comparison, a measurement for hydrous iridium oxide (Ir$^{18}$O$_2$H$_2$O) is shown in Fig. 3b. This catalyst was prepared by the method described in ref. 11: an Ir$^{18}$O$_2$ film was prepared by reactive sputter deposition with $^{18}$O in the plasma and then electrochemically cycled (200 times at 50 mV s$^{-1}$ from 0 $\text{V}_{\text{RHE}}$ to 1.5 $\text{V}_{\text{RHE}}$) in 0.1 M HClO$_4$ electrolyte made with $^{18}$O$_2$; a procedure known to form an amorphous hydrous surface layer.\textsuperscript{36,37} Ir$^{18}$O$^{2+}$H$_2$O evolved a significant amount of labelled oxygen at the beginning of the measurement, peaking at about \(3 \text{ pmol s}^{-1} \text{ cm}^{-2}\text{geo}\), but the labelled OER rate decreased to about \(1 \text{ pmol s}^{-1} \text{ cm}^{-2}\text{geo}\) within the first five minutes at 0.5 mA cm$^{-2}$geo. Compared to a crystalline sputter-deposited Ir$^{18}$O$_2$ film (Fig. S2, ESI†), Ir$^{18}$O$^{2+}$H$_2$O showed higher activity (1.46 $\text{V}_{\text{RHE}}$ instead of 1.51 $\text{V}_{\text{RHE}}$ to reach 0.5 mA cm$^{-2}$geo), higher dissolution (\(\sim 1 \text{ pmol s}^{-1} \text{ cm}^{-2}\text{geo}\) instead of 0.1), and higher labelled oxygen evolution (\(\sim 1 \text{ pmol s}^{-1} \text{ cm}^{-2}\text{geo}\) instead of 0.2). This is in agreement with previous results reported at higher overpotentials,\textsuperscript{11,12,23} except that previous measurements were not sensitive enough to measure the labelled oxygen evolved from Ir$^{18}$O$_2$. All iridium samples were much more stable against dissolution than RuO$_2$. Dissolution of Ir from Ir$^{18}$O$_2$H$_2$O exceeded evolution of labelled oxygen by a factor 2.5 in the ramp-up (870 pmol cm$^{-2}$geo Ir compared to 350 pmol cm$^{-2}$geo $^{18}$O) and only by a factor 1.3 at steady state (1400 pmol cm$^{-2}$geo Ir compared to 1050 pmol cm$^{-2}$geo $^{18}$O). On several other iridium-based samples, labelled oxygen incorporation into O$_2$ modestly exceeded metal dissolution (Fig. 4 and Fig. S2, ESI†).

By correlating the labelled oxygen evolution rate with the metal dissolution rate in Fig. 4, distinct groupings emerge for Ir-based and Ru-based catalysts. The y-axis shows the metal stability number, which is the number of O$_2$ molecules evolved per metal atom dissolution.\textsuperscript{11} The x-axis shows the oxygen stability number, defined in the introduction and which we in practice equate with the total number of O$_2$ molecules evolved per included $^{16}$O atom in excess of that expected from the natural isotope ratio. The labelled oxygen evolution rate increases to the left in the plot and the metal dissolution rate...
increases downwards. Both stability numbers were calculated for the first ~2 minutes of electrolysis at 0.5 mA cm$^{-2}$ geo and for steady state, as indicated by the integral values in Fig. 3. This enables us to plot each catalyst type as if it were two distinct surfaces – a transient surface during the ramp-up period (open symbols) and the stable surface of steady state (filled symbols, $t > \sim 2$ min). Sputter-deposited oxides are indicated as circles, electrochemically oxidized metallic films as squares, and electrochemically cycled films as stars. Error bars are standard deviation for at least two samples.

For RuO$_x$, a higher sputter deposition temperature results in a more crystalline film and lower geometric activity, but the same activity when normalized to capacitance, indicating a difference only in the geometric density of accessible surface sites. However, this cannot by itself explain the higher oxygen stability number observed in s-400 °C RuO$_2$ compared to s-25 °C RuO$_2$, which we would expect to be the same if the surfaces had the same intrinsic activity and stability numbers did not change as a function of potential. Nor would lower geometric density of accessible surface sites by itself be able to explain the higher metal and oxygen stability numbers seen in s-400 °C IrO$_2$ compared to s-25 °C IrO$_2$. In both cases it must be related either to the intrinsic stability of surface sites (though not necessarily the same surface sites) for oxygen evolution or to the difference potential required to reach the 0.5 mA cm$^{-2}$ applied current density used in these measurements.

Some iridium-based samples exhibit more labelled oxygen evolution than metal dissolution, i.e. $n_O > n_{\text{diss}}$. This list includes s-400 °C Ir$^{18}$O$_2$ (crystalline Ir$^{18}$O$_2$, sputter-deposited at 400 °C). The steady-state metal and oxygen evolution reaction (surface LOER), i.e., some of the labelled oxygen on the surface enters the OER catalytic cycle as if it were an adsorbate. In contrast to OER, electrochemical CO oxidation on s-25 °C Ir$^{18}$O$_2$, first described in ref. 21, exhibited unambiguous lattice oxygen incorporation in the CO$_2$ evolved with $n_O > n_{\text{diss}}$ and $n_O > 1$ ML as shown in Fig. S3 (ESI†).

It is informative to compare films that differ only in their sputter deposition temperature. As described in the first article of this series, for RuO$_x$, the higher sputter deposition temperature results in a more crystalline film and lower geometric activity, but the same activity when normalized to capacitance, indicating a difference only in the geometric density of accessible surface sites. However, this cannot by itself explain the higher oxygen stability number observed in s-400 °C RuO$_2$ compared to s-25 °C RuO$_2$, which we would expect to be the same if the surfaces had the same intrinsic activity and stability numbers did not change as a function of potential. Nor would lower geometric density of accessible surface sites by itself be able to explain the higher metal and oxygen stability numbers seen in s-400 °C IrO$_2$ compared to s-25 °C IrO$_2$. In both cases it must be related either to the intrinsic stability of surface sites (though not necessarily the same surface sites) for oxygen evolution or to the difference potential required to reach the 0.5 mA cm$^{-2}$ applied current density used in these measurements.

For RuO$_x$, dissolution always exceeded labelled oxygen evolution, but the two processes did not follow the same trend with applied current density (Fig. 5a) or potential (Fig. 5b). Since $n_O < n_{\text{diss}}$ for all ruthenium-based samples (Fig. 4), the additional experiments in Fig. 5 were needed to determine whether labelled oxygen evolution from ruthenium-based oxides is “surface LOER”, “degradative LOER”, or both. If the labelled oxygen evolving mechanism shared a rate-determining step with water oxidation, we should expect labelled O$_2$ evolution to be proportional to total O$_2$ production and thus for the lattice oxygen stability number to be constant with respect to total current density. On the other hand, if the labelled oxygen evolving mechanism is a bi-product of degradation, we should expect it to be proportional to the metal dissolution, and thus for the lattice oxygen stability number to show the same dependence on overall current density as the metal stability number. Fig. 5a shows the result for s-25 °C Ru$^{18}$O$_2$. The steady-state metal stability number for s-25 °C Ru$^{18}$O$_2$ increases with...
current density, indicating that dissolution increases more slowly with potential (has a higher Tafel slope) than oxygen evolution. On the other hand, the lattice oxygen stability number remains steady at about 3000 O₂ molecules evolved for each inclusion of a labelled oxygen atom. The different trends indicate that lattice oxygen evolution on RuO₂ is mechanistically distinct from dissolution, i.e. that it is more likely to be “surface LOER” than “degradative LOER”. The same analysis was not repeated on IrO₂ since labelled oxygen evolution and metal dissolution do not significantly exceed the respective detection limits at lower current densities than 0.5 mA cm⁻² geo.

It is illustrative to think of (electrolyte) oxygen evolution, metal dissolution, and labelled (lattice) oxygen evolution as three processes occurring simultaneously at different rates as a function of potential. Fig. 5b shows the capacitance-normalized molar rates for the exchange and dissolution data in Fig. 5a against potential together with the activity dataset for sputter-deposited RuO₂ films and Ru foam introduced in the first article of this series (DOI: 10.1039/D1EE03914H). The intrinsic activity of all three processes can also be expressed as approximate turn-over-frequencies by normalizing to the number of active sites, as indicated by the right y-axis of Fig. 5b. While labelled oxygen evolution follows the same trend vs. potential as water oxidation on RuO₂, metal dissolution follows a different trend. Specifically, in the range studied, lattice oxygen evolution has a Tafel slope of 60 mV per decade which decreases (higher potential dependence) with decreasing overpotential, following the overall OER activity, while metal dissolution has a Tafel slope of ~120 mV per decade.

Low-energy ion scattering spectrometry (LEIS) characterization after electrolysis experiments revealed that more oxygen from the electrolyte was incorporated into the surface of both ruthenium-based and iridium-based catalysts than could be explained by exchange through lattice oxygen evolution. Fig. 6a and b show the

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**Fig. 5** Trends in lattice oxygen and metal steady-state stability for labelled ruthenium oxide sputter-deposited at room temperature (s-25 °C Ru¹⁸Oₓ). (a) The metal stability number (black) and oxygen stability number (green) are plotted against the applied geometric current density. Each point at a given current density is from an independently prepared sample. (b) The same results shown as molar rate normalized by electrode capacitance and plotted against potential. The activity measurements (small symbols) and model (dashed line) from the accompanying manuscript are included for context. The right y-axis indicates the corresponding turn-over frequency estimated using a specific capacitance of 115 μF cm⁻² ESCA (from single crystal measurements [ref. 39 and DOI: 10.1039/D1EE03914H]) and a site density of 5 nm⁻² ESCA (that of CUS sites on RuO₂(110)) for the conversion.

**Fig. 6** Low-energy ion scattering (LEIS) measurements of (a) s-25 °C Ru¹⁸Oₓ and (b) electrochemically cycled Ir¹⁸Oₓ (Ir¹⁸Oₓ-yH₂¹⁸O). The spectra shown were taken before (“As-prepared”, green trace) and after (“After OER”, blue trace) the respective EC-MS experiments shown in Fig. 2. An additional spectrum was taken after sputtering approximately one monolayer of material away to determine if any change in isotopic composition was confined to the surface. The centers of the ¹⁸O and ¹⁶O peaks and the isotopic distribution of O on the surface, determined by fitting of the peaks, are indicated. The Ru and Ir peaks are > 800 eV and not in the window shown. The peak at ~ 650 eV in (b) is chlorine from the 0.1 M HClO₄ electrolyte used in the catalyst preparation.
spectra for the s-25 °C RuO2 and IrO2-yH2O catalysts following the EC-MS experiments shown in Fig. 3a and b, respectively. The 16O in the as-prepared samples (lower spectra) may come from impurities in the sputter chamber during sample synthesis or strong adsorption of water (surface hydration) during air exposure between synthesis and characterization. After OER (middle spectrum in Fig. 6a), the portion of 16O on the as-prepared s-25 °C Ru18O2 catalyst had increased from ~13% to ~30%, implying a small degree of either oxygen exchange or hydration during the electrolysis experiment. The difference, ~20% of a monolayer, is much greater than the ~2% of 18O from the sample that was evolved as O2, but less than the amount of Ru dissolution (~1 ML) during the OER measurement. After sputtering (upper spectrum), the isotopic ratio of oxygen at the surface is close to the pre-electrolysis ratio, implying that any exchange of oxygen atoms was confined to the outer surface. Similarly, electrochemical labelling by oxidizing or electrochemically cycling a Ru18O2 electrocatalyst in 16O-containing electrolyte only incorporated the 18O in the outer monolayer (Fig. S4, ESI†), highlighting why reactive sputter deposition with 18O2 was necessary to produce labelled samples.

Ir18O2-yH2O formed by electrochemical cycling treatment shows significant 18O incorporation (Fig. 6b). Ir18O2-yH2O contains ~25% 18O before electrolys, possibly due to easy exchange of intercalated water with water vapor in the air; ~58% 18O on the surface after electrolys, implying a large degree of oxygen exchange during electrolys; and ~34% 16O even after the surface atomic layer is sputtered off. This result again implies more oxygen exchange than can be explained by lattice oxygen evolution. Ir18O2 which has not been electrochemically cycled before OER shows less incorporation (Fig. S4, ESI†), but still more than labelled oxygen evolution. Note that LEIS is only sensitive to the outermost atomic layer, so even in this catalyst, the surface layer retained about ~42% of its original oxygen atoms during 30 minutes of OER at 0.5 mA cm−2. These results are in good agreement with the atomic probe tomography results by Schweinar et al.35 LEIS spectra were taken before and after OER for most classes of sample included in Fig. 4. The fitting results for all spectra are summarized in Fig. S4 (ESI†). For all sample classes, 18O remained the dominant oxygen isotope on the surface after OER, but with the modest increase in 16O nonetheless consistently exceeding that expected based on the amount of 18O in the O2 evolved. This indicates that the main mechanism of oxygen exchange is not a lattice oxygen evolution mechanism, but something else. Possibilities include hydration and exchange of water or exchange of tightly bound surface adsorbates. Note that both of these explanations involve oxygen atoms which we exclude from our definition of lattice oxygen. After argon sputtering, the spectra consistently returned to a 16O/18O ratio close to, but slightly higher than, the pre-OER ratio. We hypothesize that, rather than implying bulk activity, this slight increase is due to the rough and in some cases porous surface of the catalyst casting shadows where the post-OER surface is not uniformly sputtered away.

Discussion

The portion of O2 produced by Ru- and Ir-based catalysts during OER in acid at 0.5 mA cm−2 geo that contained an oxygen atom originating from the electrocatalyst ranged from about one in 500 (s-25 °C Ru18O2 and Ir18O2-yH2O at the start of electrolysis) to less than one in 10 000 (s-400 °C Ru18O2 and s-400 °C Ir18O2 at steady-state). These “oxygen stability numbers” are the x-axis of Fig. 4. In other words, for all materials studied here, the vast majority of O2 molecules consisted of two oxygen atoms originating from the water of the electrolyte. This means that a water oxidation mechanism dominates over any lattice oxidation mechanism by multiple orders of magnitude. That the majority of O2 evolved does not contain an oxygen molecule from the catalyst is consistent with prior isotope labelling studies: For instance, Kasian et al. (ref. 12), measuring at 10–25 mA cm−2 geo (much higher than the 0.5 mA cm−2 geo used in our present study), also observe an oxygen stability number of ~500 for IrO2-yH2O.

In principle, for an OER electrocatalyst with activity dominated by a lattice oxygen evolution mechanism, the isotopic signal would return to the natural baseline once the isotopic label of the oxygen in the active portion of the electrocatalyst was depleted, and so a transient isotopic signal has often been interpreted as evidence of a dominant lattice oxygen evolution mechanism. However, unlike most previous studies, our experiments can rule out 18O depletion for two reasons: (i) the 18O isotopic label remains at the surface of all catalysts tested as measured by LEIS. With the exception of the hydrous catalyst IrO2-yH2O, the majority of the oxygen at the surface, and the vast majority below the surface atomic layer, remains 18O (Fig. 6 and Fig. S4, ESI†). Furthermore, (ii) the total amount of labelled oxygen from the catalysts incorporated into the O2 evolved was less than one atomic layer equivalent in all experiments. This is an advantage of chip EC-MS: the high sensitivity of the system enables us to quantitatively label oxygen evolution even at low applied current densities where it amounts to well under a picomole of O2 per second.

We can therefore decisively conclude that the dominant oxygen evolution mechanism on Ru- and Ir-based oxides in acidic electrolyte does not incorporate lattice oxygen into O2. Labelled oxygen evolution instead results from a minor side process, but one that could nonetheless provide insight into the oxygen evolution and degradation pathways. Even though lattice oxygen is not directly involved in the dominant OER mechanism, lattice oxygen is of course still important for holding the electrocatalyst together and for defining the coordination environment of the active sites.

Referring to Fig. 1 and our definition of lattice oxygen as oxygen atoms with the same coordination environment as oxygen in the bulk of a crystalline material, we briefly comment on whether the observed labelled oxygen evolution represents lattice oxygen evolution. The metal dissolution rate far exceeds the labelled oxygen evolution rate for ruthenium-based catalysts (collectively, Ru18O2) while the two rates are similar on iridium-based catalysts (collectively, Ir18O2), resulting in two groupings...
when Ru$^{18}$O and Ir$^{18}$O surfaces are mapped out according to metal stability number and oxygen stability number (Fig. 4). This seemingly implies that labelled oxygen evolution on Ru$^{18}$O could result from the generation of undercoordinated surface oxygen atoms, which enter the electrocatalytic cycle as metal atoms dissolve; but that this is not a likely explanation for Ir$^{18}$O. However, no catalyst tested in our work does the amount of labelled oxygen evolved during the experiment exceed one monolayer equivalent based on capacitance measurements. This implies that the evolved $^{18}$O, including on Ru$^{18}$O, could all be strongly bound surface oxygen such as bridging oxygen. Thus, our studies place Ru$^{18}$O in sector IV of Fig. 1 (“labelled oxygen evolution of unknown origin”) and Ir$^{18}$O in sector III of Fig. 1 (“surface bound oxygen evolution”). It is likely that lattice oxygen does occur to some extent for IrO based on previous studies done at higher current density, which show amounts of labelled oxygen evolution likely exceeding a monolayer equivalent.

Fig. 4 also reveals that metal dissolution and labelled oxygen evolution are correlated across different catalytic surfaces for both metals, implying that the underlying mechanisms are linked for RuO and IrO in acidic electrolyte. This correlation can be explained by the two processes occurring through a common intermediate. As both dissolution and lattice oxygen evolution involve the breaking of metal oxygen bonds, this shared intermediate could be a destabilized surface state, *i.e.* a surface metal atom that partially leaves its coordination environment. This hypothesis is illustrated in the proposed combined reaction scheme in Fig. 7. The electrocatalyst is indicated as a surface layer and subsurface layer of metal atoms interspersed with labelled oxygen atoms, and the surface site that reacts in the pathways is emphasized with a highlighted outline. Note that the states are drawn for conceptual clarity rather than structural accuracy.

The main oxygen evolution pathway, indicated in the top row, is in essence the conventional “metal peroxide” pathway involving four concerted proton-electron transfers, labelled steps 1–4 in Fig. 7. The only difference is that we have drawn the peroxide intermediate, $^{*}$OOH, with the hydrogen atom abstracted to a neighboring surface-bound oxygen atom, as has been proposed to take place on Ru(110), stabilizing this intermediate and lowering the OER overpotential. We have labelled the peroxide intermediate as the “active state” or $S_{RDS}$, *OH as $S_{RDS-1}$, and *OH as $S_{RDS-2}$ based on the analysis in the first article of this series. The destabilized state that we propose as the link between labelled oxygen evolution and metal dissolution is indicated at the start of the middle row.

![Fig. 7](image_url)
It is reached from a state in the OER catalytic cycle by step 5. From the destabilized state we propose one of three things can happen: the metal atom can fall back into its original coordination environment, reversing the destabilization (step –5); the metal atom can leave its coordination environment further, leading to dissolution (6); or it can return to its original coordination environment but with two oxygen atoms switched such that a lattice oxygen atom ends on the surface (–5'). The last possibility results in lattice oxygen evolution, i.e. the evolution of a lattice oxygen molecule and the incorporation of an unlabelled oxygen atom into the catalyst, as indicated on the bottom row of Fig. 7 (steps 2', 3', and 4'), which are equivalent to the corresponding steps for surface bound oxygen evolution. Significantly, this arrangement of the steps implies that lattice oxygen evolution starts by taking a step down the degradation pathway.

The fact that rates of labelled oxygen evolution are similar on RuO$_x$ and IrO$_x$ catalysts but that dissolution occurs at a much higher rate on RuO$_x$ catalysts indicates that the important difference between the two metal elements is the branching between steps 6 (dissolution) and –5' (labelled oxygen evolution): the ratio $k_{-5'}/(k_{-5} + k_d)$ is much higher for IrO$_x$ than for RuO$_x$. In other words, a destabilized iridium atom is much more likely to restabilize than a destabilized ruthenium atom. This may be related to the ability of Ru to oxidize beyond the 4+ state that it has in RuO$_2$: the thermodynamically stable state of Ru appearing in the Pourbaix diagram at typical OER conditions of pH = 1 and $U = 1.6$ V$_{BHE}$ is volatile RuO$_4$, whereas for Ir at the same conditions it is rutile IrO$_2$ (ref. 43 and 44).

Fig. 5b shows that on s-25 °C Ru$^{18}$O$_x$ (amorphous labelled ruthenium oxide sputter-deposited at room temperature), the labelled oxygen rate was proportional to the total oxygen evolution rate as a function of potential whereas the dissolution rate decreased in proportion to oxygen evolution rate with increasing potential. One possible explanation is that oxygen evolution with and without lattice exchange have equivalent rate-determining steps (RDS; steps 4 and 4' in Fig. 7) whereas dissolution has a rate-determining step (step 6) with a weaker potential-dependence (higher Tafel slope). Note that 4' can be the effective RDS for lattice oxygen evolution even without 5 and –5' being in equilibrium if lattice oxygen evolution is one of two competing pathways down which *$^{18}$OH can go once formed. The fact that $^{16}$O is incorporated in the catalysts at a higher rate than $^{18}$O is incorporated into the O$_2$ evolved, as shown by LEIS (Fig. 6) and in agreement with Schweinar et al.’s results for IrO$_2$ (ref. 23), implies that this is the case: *$^{18}$OH can likely exchange with water to form *$^{18}$OH (step –1’ followed by 1) if it does not react down 2’, 3’, and 4’ fast enough, so the potential dependence of labelled oxygen evolution comes from the RDS of the OER.

The choice of *OH as the intermediate from which the dissolution and lattice oxygen evolution mechanisms branch out is motivated by two factors: first, we provide evidence in our previous work$^{33}$ and in Fig. S3 (ESI?) that CO reacts with lattice oxygen via *OH, indicating that the surface is prone to expose lattice oxygen when covered by *OH. Second, the fact that the metal stability number increases with increasing potential hints at the branching point being a state with higher coverage at lower overpotential, namely S$_{RDS2}$, which we tentatively assigned to *OH in the first article of this series.$^{39}$ This implies that the Tafel slopes for oxygen evolution, metal dissolution, and labelled oxygen evolution should converge (i.e., both oxygen and metal stability numbers should become constant with potential) at higher overpotentials, when *OH coverage is negligible at equilibrium but *OH is formed transiently as an intermediate of the OER electrocatalytic cycle, consistent with the previously reported results for IrO$_x$ (ref. 12). We should point out that the explanations provided by Fig. 7 are not exclusive – another possible explanation for the differing Tafel behavior of labelled oxygen evolution and metal dissolution is that the dissolution mechanism changes as a function of potential, as suggested by Kasian et al. in ref. 25, whereas the lattice oxygen mechanism remains constant.

This result in Fig. 5 also rules out electrochemical potential as an explanation for the difference in oxygen stability number between s-400 °C RuO$_x$ and s-25 °C RuO$_x$ observed in Fig. 4, since oxygen stability number apparently does not change as a function of potential alone on s-25 °C RuO$_x$. Thus, we can conclude that there is an intrinsic difference in the surfaces of s-400 °C RuO$_2$ and s-25 °C RuO$_x$. Though we cannot determine the precise difference from the present data, we hypothesize that the rougher surface of RuO$_x$ has more highly undercoordinated Ru sites that are able to bring a labeled oxygen atom into the OER catalytic cycle. In contrast, the overall OER activity converges when normalized to capacitance, indicating the same intrinsic activity of the dominant sites. An implication is that labelled oxygen evolution might come primarily from sites that differ from the sites which dominate the overall OER activity. This interpretation, that there are different sites associated with activity and catalyst degradation, is promising as it implies that an electrocatalyst can be optimized for activity without necessarily compromising stability.

As a last discussion point, we wish to comment on the implications of our methods and results on future $^{18}$O isotope-labelling studies in oxygen evolution catalysis. Quantitative results are essential. Firstly, quantification of (i) the labelled oxygen evolution rate, (ii) the metal dissolution rate, and (iii) the number of active sites is necessary to determine whether labelled oxygen evolution is a surface phenomenon, a degradative processes, or a true catalytic mechanism involving lattice oxygen (see Fig. 1). Secondly, the quantified labelled oxygen evolution rate has to be compared to the total oxygen evolution rate to gauge the importance of a possible lattice oxygen evolution mechanism to the overall activity. Finally, isotopic composition of the oxygen in the catalytic surface should also be quantified both before and after oxygen evolution to determine whether labelled oxygen evolution matches oxygen exchange in the catalyst. Because data analysis interpretation can be quite difficult, we encourage the use of public repositories to enable groups to see exactly how the analysis was done and repplot each other’s data. This will benefit from open-source analysis tools. In this article, we presented quantitative data for a range of RuO$_x$ and IrO$_x$ catalysts at low overpotential, but the study was far from exhaustive. It would
be especially interesting to see labelled oxygen studied as described above for alkaline electrocatalysts, where the mechanism and relation to degradation might be quite different. On the other hand, since our results indicate that labelled oxygen evolution seems to be largely a proxy for instability, at least for RuO₂ and IrO₂ in acidic electrolyte (Fig. 4), researchers may wish to prioritize careful measurements of activity and stability in the search for better acid-stable OER electrocatalysts. The challenge, based on this and the accompanying article, is to optimize the metal-oxygen binding energy for catalytic intermediates at sites on the surface while making the bulk metal-oxygen binding as strong as possible to stabilize the catalyst. Promising strategies towards scalable acid-stable OER electrocatalysis include bulk alloying with more stable elements and stabilization of optimally coordinated surface sites to complement engineering techniques that lower the required loading.

Conclusion

In this study, we introduced the oxygen stability number in the oxygen evolution reaction (OER) as the ratio of the total number of O₂ molecules generated to the number of oxygen atoms from the catalyst incorporated into the O₂. Using a highly sensitive chip EC-MS setup, we showed that the oxygen stability number in acidic electrolyte at 0.5 mA cm⁻² geo ranges from ~500 (0.2% labelled oxygen evolution on amorphous Ru₁₈Oₓ and hydrous Ir₁₈Oₓ•yH₂O at the start of electrolysis) to ~10000 (0.01% labelled oxygen evolution on crystalline Ru₁₈O₂ and Ir₁₈O₂ at steady-state). On this basis, and by ruling out depletion of the isotopic label at the surface using LEIS, we conclude that lattice oxygen evolution is at most a negligible contribution to overall OER activity for Ru- and Ir-based catalysts in acidic electrolyte. For RuO₂, metal dissolved at a higher rate than labelled oxygen was evolved, i.e. the oxygen stability number was always significantly higher than the metal stability number, while the two rates were similar for IrO₂. Between different catalytic surfaces within these two classes of catalysts, labelled oxygen evolution rate increased with metal dissolution rate. These results are consistent with a picture in which lattice oxygen evolution on RuO₂ and IrO₂ in acidic electrolyte is mechanistically related to dissolution – that, put simply, to get to the lattice oxygen evolution pathway, you have to cross through the dissolution pathway. We highlight the need to report quantitative results and to quantitatively compare the isotopic signal to both degradation rate and overall catalytic rate when performing isotopic labelling mechanistic studies in electrocatalysis. Our results indicate that future studies in acid-stable OER electrocatalysis should focus on understanding, controlling, and optimizing the reactivity of catalytic surface sites while maximizing the stability of the bulk electrocatalyst.

Experimental

Sample synthesis

Most samples were synthesized by reactive sputter deposition of ruthenium or iridium in a plasma of 20%¹⁸O₂ (99% isotopic purity). Some included a subsequent electrochemical step in their preparation. We studied the following samples based on previous work:

- s-25 °C Ru₁₈O₂ sputter deposited at room temperature (XRD-amorphous)
- s-400 °C Ru₁₈O₂ sputter deposited at 400 °C (rutile)
- Ru₁₈O₂/Ru formed by oxidation of sputter deposited metallic Ru in 97% H₂¹₈O electrolyte
- Ru₁₈O₂/Ru-foam formed by oxidation of ruthenium foam (see the first article of this series) in 97% H₂¹₈O electrolyte
- s-25 °C Ir₁₈O₂ sputter deposited at room temperature
- s-400 °C Ir₁₈O₂ sputter deposited at 400 °C
- Ir₁₈O₂/Ir formed by oxidation of sputter deposited metallic Ir in 97% H₂¹₈O electrolyte
- Ir₁₈O₂•yH₂O, an amorphous hydrous iridium layer formed by potential cycling of sputter deposited Ir₁₈O₂ samples in 97% H₂¹₈O electrolyte

The isotopic composition of the surface of each sample was characterized by LEIS before testing in chip EC-MS in 1.0 M HClO₄ of the natural isotopic composition.

EC-MS and ICP-MS

The chip EC-MS technique and setup have been described in detail elsewhere. The only addition to the setup in this work was the capability for extracting samples of electrolyte. The cell, which held the sample, had four electrolyte channels – two were used for the reference and counter electrodes, while the other two were used as an inlet and an outlet, see Fig. 2a. The outlet was connected to a syringe for controlled collection of electrolyte samples, which diluted the initial ~2 μL working volume between the sample and the membrane chip (the mass spectrometer inlet) by a factor of about ~100. The extracted electrolyte sample was later further diluted to exactly 10 ML in 2% nitric acid for ICP-MS measurement, where the sub-ppb sensitivity of ICP-MS corresponded to ~3 pmol of Ru or ~1 pmol of Ir per sample (see the ICP-MS calibration curves in Fig. S5, ESIF). While the electrolyte sample was collected, a valve on the inlet was opened to an electrolyte reservoir, so that the working volume was not subjected to a significant pressure fluctuation as the syringe for the electrolyte was withdrawn.

Each EC-MS experiment included a potential ramp and a 30 minute electrolysis period at constant current (0.5, 0.15, or 0.05 mA cm⁻² geo) with helium (He) gas making up the pressure in the chip. Electrolyte samples were taken without interrupting the electrochemical program after approximately 2, 10, 20, and 30 minutes of electrolysis, after which the experiment was ended. The sample was then rinsed in pure isotopically natural H₂O before being transferred to the vacuum chamber for LEIS. Priority was taken to do post-OER LEIS as quickly as possible after EC-MS (usually a few hours) to reduce the possible effect of slow exchange of oxygen with air.

Low-energy ion scattering (LEIS)

LEIS spectra were acquired on two different ultra high vacuum instruments: a ThetaProbe surface analysis system from Thermo Scientific with an EX05 ion gun producing He⁺ ions at 980 eV;
and, a Multiscan Lab XP surface analysis system from Scienta Omicron equipped with a NanoSAM detector and ISEE100 Fine Focus ion gun for producing He⁺ ions at 1000 eV. The analysis is described more in the ESI† and all the scripts converting the raw data into figures are included in the accompanying repository. Briefly, the ¹⁶O and ¹⁸O isotope peaks were fitted to reference spectra, and the area for each peak was compared to the total oxygen signal to quantify the ratio of each oxygen isotope on the surface. For the spectra acquired on the ThetaProbe system, there was a tendency for the spectra to be arbitrarily shifted – presumably due to charging of the sample. This was handled by shifting the entire spectrum such that the oxygen isotope with the highest signal was aligned with the expected peak position.

Data analysis

All data was analyzed and organized with the open-source “In situ Experimental Data Tool” (isdat, https://isdat.readthedocs.org) and a homemade database, all available at https://github.com/isdat/LowOverpotentialRegime.

Conflicts of interest

The authors do not have any conflicts of interest to declare.

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