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# CO<sub>2</sub> capture by pumping surface acidity to the deep ocean†

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To remain below 2 °C of warming, most IPCC pathways call for active CO<sub>2</sub> removal (CDR). On geological timescales, ocean uptake regulates atmospheric CO<sub>2</sub> concentration, with two homeostats driving CO<sub>2</sub> uptake: dissolution of deep ocean carbonate deposits (1 ka timescales) and terrestrial weathering of silicate rocks (100 ka timescales). Many current ocean-based CDR proposals effectively act to accelerate the latter. Here we present a method which relies purely on the redistribution and dilution of acidity from a thin layer of the surface ocean to a thicker layer of deep ocean, in order to reduce surface acidification and accelerate carbonate homeostasis. This downward transport could be seen analogous to the action of the natural biological carbon pump. The method offers advantages over other ocean alkalinity and CO<sub>2</sub>-stripping methods: the conveyance of mass is minimized (acidity is pumped *in situ* to depth), and expensive mining, grinding and distribution of alkaline material is eliminated. No dilute substance needs to be concentrated, reducing the quantity of seawater to be processed. Finally, no terrestrial material is added to the ocean, avoiding significant alteration of seawater ion concentrations or issues with heavy metal toxicity (encountered in mineral-based alkalinity schemes). The artificial transport of acidity accelerates the natural deep ocean compensation by calcium carbonate. It has been estimated that the total compensation capacity of the ocean is on the order of 1500 GtC. We show through simulation that pumping of ocean acidity could remove up to 150 GtC from the atmosphere by 2100 without excessive increase of local pH. The permanence of the CO<sub>2</sub> storage depends on the depth of acid pumping. At >3000 m, ~85% is retained for at least 300 years, and >50% for at least 2000 years. Shallow pumping (<2000 m) offers more of a stop-gap deferral of emissions for a few hundred years. Uptake efficiency and residence time also vary with the location of acidity pumping. Requiring only local resources (ocean water and energy), this method could be uniquely suited to utilize otherwise-unusable open ocean energy sources at scale. We present a brief techno-economic estimate of 130–250\$ per tCO<sub>2</sub> at current prices and as low as 93\$ per tCO<sub>2</sub> under modest learning-curve assumptions.

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## Broader context

In addition to near-total decarbonization of the world economy it is increasingly clear that already emitted CO<sub>2</sub> will also need to be actively removed from the atmosphere in order to stabilize the Earth's temperature. Due to their natural role in regulating CO<sub>2</sub> over geological periods of time, the weathering of alkaline minerals and the subsequent flow of alkalinity into the oceans are an attractive candidate for CO<sub>2</sub> sequestration with the potential to store many hundreds of gigatonnes of CO<sub>2</sub>. With the aim of accelerating such dissolution most prior work has focused on terrestrial minerals, while less attention has been paid to the alkaline carbonate sediments in the deep ocean. Our electrochemical approach of pumping surface acidity into deeper ocean layers could provide a means to induce the dissolution of alkaline mineral deposits (calcite) in the deep ocean while accelerating CO<sub>2</sub> uptake at the surface. The approach is uniquely suited for open ocean energy sources since no terrestrial material is needed and could thus provide an interesting new technology in the overall portfolio of negative emissions that will be needed in the latter half of this century.

## 1 Introduction

Stabilizing the earth's climate into the next centuries will require a near total decarbonization of the world energy supply, *i.e.* reducing emissions from their current peak levels. However,

some industrial processes, such as industrial heat and concrete manufacturing as well as emissions from land use changes, air travel, or livestock are very difficult to decarbonize.<sup>1</sup> Further, even if future emissions were curbed, enough historical CO<sub>2</sub> has already accumulated in the atmosphere to cause problematic warming and could trigger tipping points. Thus, the vast majority of IPCC RCP2.6 scenarios which remain under 2 °C of warming require negative emissions on the order of 150 GtC before 2100<sup>2,3</sup> in addition to rapid decarbonization. On geological timescales

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mixed layer long before dissolution,<sup>22</sup> limiting applicability to shallow coastal areas.<sup>23</sup> Grinding down to 1  $\mu\text{m}$  would enable open ocean distribution, but significantly increase grinding energy costs.<sup>24</sup> Iron, abundant in most olivine minerals, would inadvertently fertilize the ocean leading to significant ecological disruption<sup>2,14</sup> and changes in silicate concentration would shift the phytoplankton species composition towards diatoms.<sup>22</sup> Nickel, also found in olivines,<sup>25,26</sup> is biologically both an essential co-factor and toxic at high concentration with different concentrations optimal for different marine species.<sup>27</sup> Chromium is present in flood-basalts and ultra-basic rocks in similar quantities to nickel.<sup>25</sup>

This proposal shares many properties with the above ocean alkalinity enhancement proposals, with some advantages. Firstly there is no need for large mass transport of alkaline rocks to the ocean<sup>13</sup> or transport of products away from electrolyzers.<sup>28</sup> The only matter transport needed is the pumping of a small amount of water a few kilometers downwards. This locality makes the method uniquely suitable for open ocean deployment and provides a way to use otherwise unusable renewable energy resources. Open waters offer greater scalability at reduced ecological impact as dilution over large areas is trivial. The proposed method also avoids the severe impacts of creating a gigatonne-scale mining operation on terrestrial ecosystems. The net cation composition of the ocean is not changed, avoiding introduction of iron, silicate or toxic trace metals into ocean ecosystems, a major concern with most mineral-based alkanization approaches.<sup>2</sup> The redistribution of alkalinity dilutes the already occurring anthropogenic acidification of the surface ocean into the deeper ocean. Due to these advantageous ecological properties, the proposed method may find it easier to gain social license, as it aims to mitigate human impact by spatial and temporal dilution. In general, all ocean alkalinity methods are currently regulated by international maritime laws such as the London Convention<sup>29</sup> which would have to be reviewed and possibly amended before deployment could begin at scale.<sup>30</sup>

We note also that widely discussed biological ocean CDRs<sup>31</sup> which propose increasing primary biological productivity and sinking of biological matter, such as ocean fertilization, could be seen as equivalent to the acidity pumping proposed here. This is because the vast majority of sunk soft tissue is remineralized in the water column or on the ocean floor, thus acidifying deep waters.<sup>32</sup> Only 0.4% of the originally fixed carbon is buried in sediments and permanently removed from circulation.<sup>10</sup> Thus efforts increasing primary biological production likewise rely on the dissolution of deep  $\text{CaCO}_3$  deposits to prevent the transported carbon from being re-emitted to the atmosphere on the timescales of ocean circulation. Thus, these methods also ultimately aim to accelerate deep carbonate dissolution, albeit indirectly. The same can be said for efforts to directly inject  $\text{CO}_2$  into the deep sea, as the resulting  $\text{CO}_2$  lakes or hydrates gradually dissolve.<sup>33</sup>

In this paper we present ocean circulation simulations to examine the effects and limitations of large-scale acidity pumping as well as techno-economic arguments which suggest that the cost per tonne of  $\text{CO}_2$  could potentially be competitive

with terrestrial direct air capture (DAC) and other negative emissions technologies while avoiding the ecological impacts of accelerated mineral weathering.<sup>2</sup>

## 2 Methods

### 2.1 Global circulation model of acid-base pumping

To simulate the effect of acid-base pumping on surface and deep water pH, as well as net ocean  $\text{CO}_2$  uptake, and evaluate the return time of acidity, we used a full ocean circulation model in a  $128 \times 64$  worldwide spherical polar grid using MITgcm.<sup>34</sup> The simulation had cell sizes of  $2.8^\circ \times 2.8^\circ$  divided into 20 exponentially spaced depth levels, from 10 m thick at the surface to 690 m thick at depth. The simulation was initialized and forced as detailed in Dutkiewicz *et al.* (2005).<sup>35</sup> The MITgcm GEOM and DIC modules were used to simulate the soft tissue and carbonate pumps, as well as ocean-atmosphere gas exchange. A number of studies<sup>36,37</sup> have simulated addition of alkalinity to the ocean in the context of realistic emission scenarios with increasing atmospheric  $p\text{CO}_2$ . Here we chose to focus instead on the efficiency of  $\text{CO}_2$  uptake and the circulation aspects of acidity return, and thus the atmospheric concentration of  $\text{CO}_2$  was simply held constant at 415 ppm similar to work by Köhler *et al.*<sup>22</sup>

**2.1.1 Perturbation.** Custom code was added to simulate the transport of alkalinity from a parameterizable slab of deep water to the top 10 m of surface water corresponding to the pumping of acidity in the opposite direction, keeping the total ocean alkalinity constant. To investigate the fate of alkalinity and acidity separately, some simulations were modified to only alkalize, in which case the total alkalinity change was not conservative. These simulations represent an idealized addition of pure alkalinity to the surface ocean. In all experiments the pumped alkalinity was released into the top 10 m slab (the top most gridcell). The acid-injection slab was approximately 1100 m thick to within the precision allowed by the vertical grid spacing. However, its depth, as well as the lat-lng distribution of pumping, were varied from experiment to experiment, as detailed in the Results section. The movement of volume was not explicitly modelled, as the involved quantities are tiny ( $\sim 5 \times 10^{-3}$  Sv  $\text{GtC}^{-1}$ ) compared to the natural ocean overturning circulation.

**2.1.2 Carbonate compensation.** The return of the acidity with the overturning circulation is the timeframe in which the transported acidity can be neutralized by dissolving carbonate sediments. Both the dissolution of existing  $\text{CaCO}_3$  deposit inventories (estimated<sup>6</sup> at a total of 1600  $\text{GtC}$ ), and reduction of new carbonate deposition (estimated at 0.27  $\text{GtC}$  per year to 0.1  $\text{GtC}$  per year<sup>38,39</sup>) increase net alkalinity in the ocean and would act to neutralize any pumped acidity. Due to the relatively short amount of time that sinking particles spend in the water column, most of the dissolution below the carbonate saturation horizon (CSD) occurs on the ocean floors. Despite the relatively uncertain current carbonate dissolution rates (0.3  $\text{GtC}$  per year  $\pm 60\%$ )<sup>11</sup> a basic model of increased carbonate



compensation due to pumped acidity can be constructed. The rate  $r$  of seafloor dissolution has been expressed<sup>40,41</sup> as

$$r = k^*([\text{CO}_3^{2-}]_{\text{sat}} - [\text{CO}_3^{2-}]) \quad (1)$$

The effective rate constant,  $k^*$ , is limited by sediment-side mass transport ( $K_s$ ) or water-side diffusion ( $\beta$ ) through a boundary layer, whichever is slower:<sup>40,41</sup>

$$k^* = K_s\beta/(K_s + \beta) \quad (2)$$

Most locations of significant (>20%) carbonate content are limited by water-side diffusion,<sup>11</sup> as bottom water speeds are relatively slow. Thus the resulting kinetics are linear with respect to the carbonate ion concentration and relatively independent of sediment  $\text{CaCO}_3$  content. To simulate the dissolution of  $\text{CaCO}_3$  deposits during our simulations, a gridded map of dissolution rate constant,  $k^*$  and sedimentary  $\text{CaCO}_3$  content was obtained from work by Sulpis *et al.*<sup>11</sup> The bottom dissolution rate was then calculated by eqn (1) for all grid tiles where the  $\text{CaCO}_3$  fraction >10%. For grid tiles containing less than 10% the dissolution rate was set to 0. At the same time, any biological carbonate flux reaching the ocean floor was modelled to have settled onto the seafloor. At steady state the rate of sedimentation and dissolution was found to be relatively balanced, *i.e.* the total ocean alkalinity was not changing rapidly. Riverine alkalinity input was not modelled. An initial simulation allowed the ocean system to equilibrate for 2500 years and was used as the starting point for

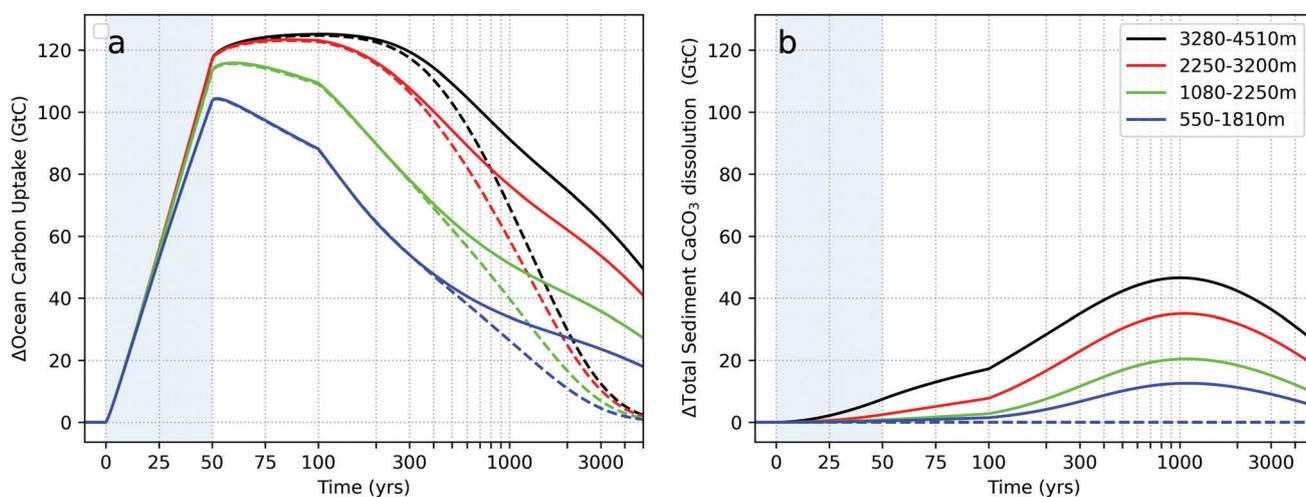
all subsequent pumping simulations. All the simulation setups, code modifications and parameters are available.<sup>42</sup>

## 3 Results

### 3.1 Uniform pumping

In our initial simulations alkalinity was pumped uniformly over the entire ocean, wherever the respective depth was available to pump acidity to. The amount of alkalinity pumped was 0.25 Pmol per year, the equivalent to a maximum uptake of 3 GtCeq per year, roughly the same amount as was used by Köhler *et al.*<sup>22</sup> Note that throughout this paper we will use units of 1 GtCeq = 0.833 Tmol to provide a better intuitive sense for the quantities involved (relative to human emissions of ~10 GtC per year). Pumping proceeded for 50 years which would yield roughly the required amount of negative emissions called for by most RCP2.6 pathways.

We also investigated lower and higher pumping rates up to 10 GtCeq per year to examine the effect on pH and carbonate saturation and to provide context for assessing a reasonable level of alkalization without excessively affecting marine ecology. Previous work<sup>37</sup> examined alkalinity addition as high as ~22 GtCeq per year although such a high rate may not be practical or ecologically safe. After the 50 year pumping period was over the simulation was allowed to continue up to the 5000 year mark to investigate carbonate compensation and the longevity of the stored carbon. To identify the role of carbonate compensation a control run was performed with sediment



**Fig. 2** Shown is the total excess  $\text{CO}_2$  uptake and total excess calcite dissolution at the seafloor with respect to time (logarithmic scale past the 100 year mark). Alkalinity and acidity are separated and acidity is pumped to depth, wherever possible, with a total rate of 3 GtC equivalent per year. Different colors represent different depths at which acidity is injected. The solid lines represent simulations including carbonate compensation, whereas the dashed lines are simulations ignoring carbonate compensation. The grey shading indicates the period for which pumping was active (the first 50 years). (a) Shows the total excess carbon (in GtC) absorbed by the ocean due to alkalinity pumping, relative to a reference simulation without any perturbation. Note that the maximal  $\text{CO}_2$  uptake reaches ~85% of the total amount of alkalinity moved (150 GtCeq over 50 years), in agreement with the compensation behavior of the carbonate system shown in Fig. S0 (ESI<sup>†</sup>) (see also Renforth *et al.*<sup>13</sup>). As long as acidity is moved below 2000 m, even in the absence of carbonate compensation, the absorbed carbon is retained well beyond 300 years. (b) Shows the relative increase in global sedimentary carbonate dissolution. When acidity is transported below 3280 m about 40% of the absorbed  $\text{CO}_2$  is compensated by calcite. Note that the total excess dissolved calcite begins to drop again at ~1000 years. This is due to the fact that our simulation kept the atmospheric  $\text{CO}_2$  concentration constant at 418 ppm, and thus the system begins to return to an equilibrium point where sedimentation rate and dissolution rate balance. The true long-term equilibrium point of the carbonate homeostat will depend strongly on future anthropogenic  $\text{CO}_2$  emissions, which are highly uncertain.



compensation turned off. A positive control run was also performed to compare to the case where alkalinity is added at the surface but no compensating acid is deposited at depth, effectively simulating the addition of a fast dissolving alkaline material.

Fig. 2a shows that alkalinity pumping results in rapid uptake of CO<sub>2</sub>, virtually indistinguishable from simple net alkalinity addition to the surface for the first 50 years. In the subsequent period, the depth of acid release strongly determines the return time and the eventual re-emission of any previously captured CO<sub>2</sub>. Injection of acidity in too shallow waters causes reemission within a few hundred years, an insufficient amount of time for any significant amount of carbonate compensation to occur. However, for acid depths greater than 3200 m the CO<sub>2</sub> absorbed does not begin to be re-emitted for at least 300 years, retaining 85–95% of the absorbed CO<sub>2</sub>. For an acidity release below 2250 m, the relaxation half-life of CO<sub>2</sub> return to the atmosphere is found to be ~2000 years. This time provides sufficient contact time for deep carbonate dissolution to occur as shown in Fig. 2b, with the global calcite dissolution rate increasing by as much as 0.25 GtCeq per year. We note that the system relaxation time is significantly increased due to this dissolution, as the half life for CO<sub>2</sub> return in the reference simulations without carbonate dissolution was much shorter (~1000 years), depending solely on ocean circulation. We note that because carbonate compensation is a bidirectional homeostat, simply balancing net dissolution with net deposition, the proportion of CO<sub>2</sub> which will be permanently removed depends on the future emissions scenarios and the eventual equilibrium point of the ocean. The method proposed here simply allows the homeostat to respond much more quickly than it would have otherwise done.

Fig. 3 tracks median and 95%ile changes in surface and ocean floor pH. See Fig. S1 (ESI<sup>†</sup>) for the corresponding change in calcite saturation. The median surface ΔpH rises rapidly for the first 1–2 years (0.03 per year) but slows within 10 years to a steady rate of  $2 \times 10^{-4}$  per year, reaching a maximum median ΔpH of 0.022 after 50 years. The increased rate of CO<sub>2</sub> dissolution is mostly able to buffer the increase in surface alkalinity. The seafloor pH however continues to decrease throughout the pumping period due to the considerably slower calcite dissolution rate. Despite this, the perturbation is at most –0.15 pH units at its most extreme point. Varying the global pumping rate between 0.3 and 10 GtCeq per year we found a roughly linear dependence of pH and Omega perturbation and pumping rate (Fig. 4). The sensitivity of benthic ecosystems to pH perturbation is poorly understood and requires further research. However, seasonal changes in open-ocean pH can be up to 0.2 pH units<sup>43</sup> while diurnal changes in coastal areas can reach as much as a full pH unit.<sup>44</sup> Using this as a guide we suggest that alkalinity pumping at global rates of 1–3 GtCeq per year may be feasible without excessive stress on marine systems, though this is a critical area in need of further research.<sup>45</sup>

### 3.2 Location dependence

Uniform pumping is neither practical nor efficient. From a practical perspective, the location of pumping will depend strongly on the mode of deployment (see Discussion). From an oceanographic perspective, both the efficiency of alkalinity

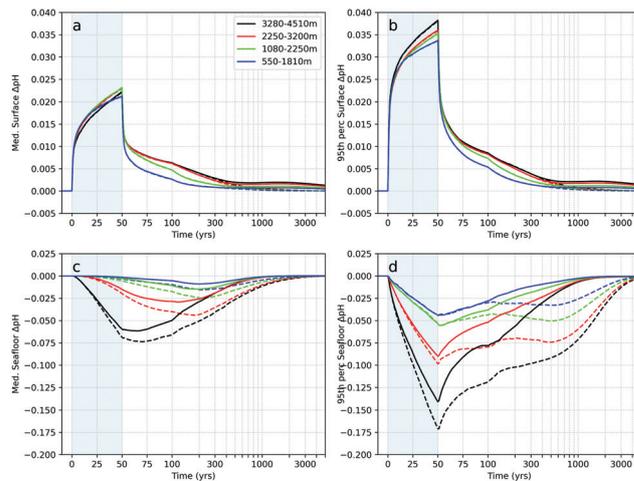


Fig. 3 Median and 95%ile changes in pH at the surface (a and b) (increase in pH) and at the seafloor (c and d) (decrease in pH) for the same runs. It can be seen that even in locations of most extreme pH change, the localized pH changes are not excessive. The changes at the surface are smaller than at depth (despite originating in a much thinner slice of water) because the lowered partial pressure of CO<sub>2</sub> immediately pulls in more carbon due to the relatively fast equilibration time. At depth the compensation with carbonate deposits proceeds much more slowly and therefore the pH response to acidity pumping is larger over time. Fig. S1 (ESI<sup>†</sup>) shows the equivalent plots of median and 95%ile changes in calcite saturation ( $\Omega$ ).

compensation at the surface and the timescales of return of acidity from deep waters vary substantially depending on the location in the ocean. The former varies due to differences in the uptake efficiency factor and surface currents, while the

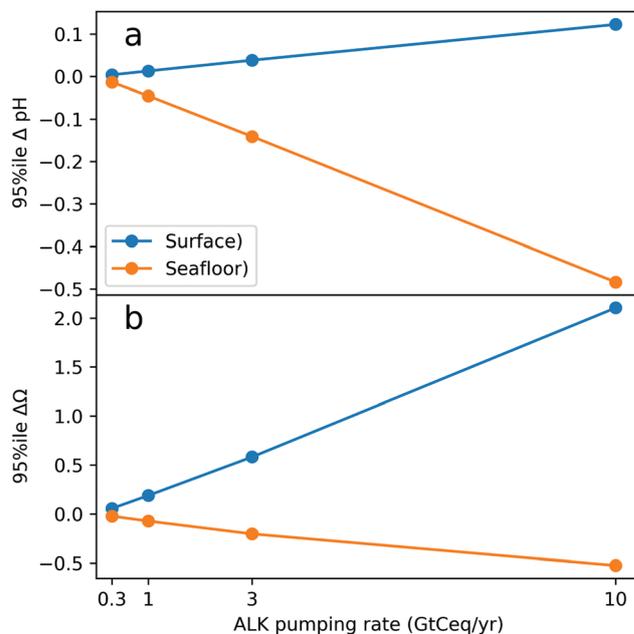


Fig. 4 (a) 95%ile pH changes at the end of 50 year alkalinity pumping across surface and across ocean seafloor for uniform alkalinity pumping at different global rates. (b) Likewise, median changes in calcite saturation ( $\Omega$ ), relative to reference simulation. A roughly linear dependence with respect to alkalinity pumping rate is observed.



latter depends on how soon deep waters are returned to the surface with the global overturning circulation.

The carbonate equilibrium in seawater responds to an increase in alkalinity by shifting towards the carbonate ion. The concomitant reduction in the partial pressure  $p\text{CO}_2$  causes an uptake of  $\text{CO}_2$  from the atmosphere until equilibrium is restored. The number of moles of  $\text{CO}_2$  absorbed for every mole of alkalinity added, the uptake efficiency  $\eta_{\text{CO}_2}$ , can be expressed as the ratio of the partial pressure sensitivities of  $p\text{CO}_2$  with respect to total alkalinity (Alk) and total inorganic carbon (DIC).<sup>13,38</sup> This compensation ratio presents a fundamental inefficiency that needs to be taken into account when calculating potential  $\text{CO}_2$  uptake of any ocean alkalization method in addition to any process inefficiencies. The commonly used approximations  $\text{DIC} \approx [\text{HCO}_3^-] + [\text{CO}_3^{2-}]$  and  $\text{Alk} \approx [\text{HCO}_3^-] + 2[\text{CO}_3^{2-}]$  at typical ocean pH yield a good approximation for the uptake factor: (derivation in ESI†).

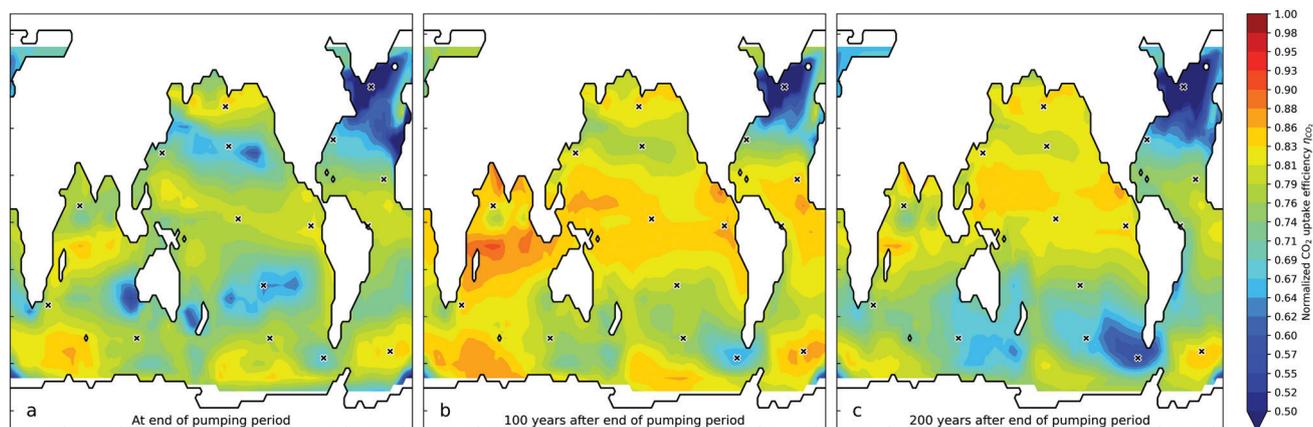
$$\eta_{\text{CO}_2} = -\frac{\partial p\text{CO}_2}{\partial \text{Alk}} / \frac{\partial p\text{CO}_2}{\partial \text{DIC}} \approx \frac{1}{3 - 2\text{DIC}/\text{Alk}} = \frac{1}{1 + 2[\text{CO}_3^{2-}]/\text{Alk}} \quad (3)$$

which evaluates to  $\sim 0.8$  at average surface ocean concentrations of  $\text{DIC} = 2000 \mu\text{M}$  and  $\text{Alk} = 2300 \mu\text{M}$ . The intuition why  $\eta_{\text{CO}_2}$  is smaller than 1 is that while each mole of additionally absorbed  $\text{CO}_2$  will be neutralized by one mole of  $\text{OH}^-$  to bicarbonate, some fraction of it will consume additional  $\text{OH}^-$  to become a carbonate ion. A full carbonate model<sup>46,47</sup> was used to calculate the plot in Fig. S1 (ESI†), showing that this uptake factor varies substantially depending on the latitude and is one aspect to determine optimal alkalinity release locations. Alkalinity addition to areas with high efficiency factor will cause a greater uptake of

$\text{CO}_2$  in the near term, however ocean surface currents will tend to move the uptake towards an average efficiency over time, so longer term efficiency can only be predicted with explicit circulation simulation.<sup>36,37</sup> Furthermore, in our case, the return time of the acidity is dependent on the direction and speed of bottom currents and the proximity to upwelling areas.

We thus performed a grid scan of the ocean, where in each simulation an amount of 100 Tmol per year of alkalinity (0.12 GtCeq per year) was pumped at any one grid point only. Altogether  $\sim 1000$  independent simulations were conducted, one for every gridpoint with sufficient depth to inject acidity. In each case the entire ocean biogeochemistry was monitored compared to a reference simulation with no pumping.

Fig. 5 and Fig. S3 (ESI†) show the normalized total uptake of  $\text{CO}_2$ , such that a value of 1.0 represents an ocean uptake equimolar to the amount of alkalinity pumped. Previous work that examined alkalinity addition in different coarse latitude bands<sup>22</sup> found not all areas are equally efficient at  $\text{CO}_2$  uptake or retention. We extend this work with a finegrained map and find that on short timescales the efficiency is dominated by the local surface efficiency and atmospheric  $p\text{CO}_2$ . However, after some time surface currents spread the excess surface alkalinity and the effect becomes less pronounced. For the case of alkalinity addition (rather than pumping) most of the locations eventually reach close to the full average efficiency of 0.85 except areas of significant downwelling in the polar regions (see Fig. S3, ESI†). The alkalinity is pulled downwards and removed from the surface as is evident in depth plots of calcite saturation (Fig. S5, ESI†). In the case of acidity pumping the behaviour is very similar, but on longer timescales, uptake efficiency becomes dominated by the rate of acid return. Since deep return currents



**Fig. 5** Efficiency of alkalinity pumping ( $\eta_{\text{CO}_2}$ ) as a function of latitude and longitude. Here ( $\eta_{\text{CO}_2}$ ) is the number of moles of excess  $\text{CO}_2$  absorbed by the ocean normalized by the number of moles of alkalinity pumped. Each point on the grid represents an entire ocean simulation in which 1 Tmol per year were pumped at that point only (a total of  $\sim 1000$  simulations). Mapped is the relative increase in total oceanic dissolved inorganic carbon (relative to the reference), normalized by the amount of acidity pumped. Three different timepoints are shown: (a) uptake of  $\text{CO}_2$  at the end of the 50 year pumping period. Significant differences in the effective  $\eta_{\text{CO}_2}$  are observed, depending on where the alkalinity was pumped, varying from 0.5 to 0.85. The differences during this period are driven primarily by the efficiency of  $\text{CO}_2$  uptake, as the distribution closely matches that of simple alkalinity addition (cf. Fig. S6, ESI†). In particular the northern Atlantic exhibits poor  $\text{CO}_2$  uptake. (b)  $\text{CO}_2$  uptake 100 years after the end of pumping. Alkalinity pumping in most northern hemisphere areas has caught up to an uptake efficiency of 0.85 with equatorial regions exhibiting the best retention. (c) 200 years after the end of pumping. The apparent  $\text{CO}_2$  uptake is fully dominated by the acid return kinetics (cf. Fig. S6 (ESI†), where alkalinity was added instead of pumped). It is apparent that acidity pumping in the southern hemisphere is less efficient, likely due to the fact that ventilation of deep water occurs in the Southern Ocean and thus acidity returns to the surface more rapidly. Conversely the North Pacific retains pumped acidity the best.



generally move southwards, injection of acidity in the northern hemisphere appears to be significantly more efficient in the long run, with some small areas as notable exceptions. Two large areas in the southern ocean appear to return acidity faster than others and are inefficient locations for alkalinity pumping (Fig. 5). Fig. S3 (ESI<sup>†</sup>) gives detailed plots of the total excess absorbed CO<sub>2</sub> due to pumping at a selected number of locations. We compared our computed CO<sub>2</sub> retention times with results from a multi-model comparison<sup>48</sup> which used models of comparable resolution to simulate direct CO<sub>2</sub> injection (see Fig. S7, ESI<sup>†</sup>). We find, in general, good agreement for almost all locations and depths with the model ensemble.

### 3.3 Impact on surface and deep water pH

Understanding the pH sensitivity of different locations allows optimization of the alkalization strategy to minimize ecological effects and costs while maximizing CO<sub>2</sub> uptake.

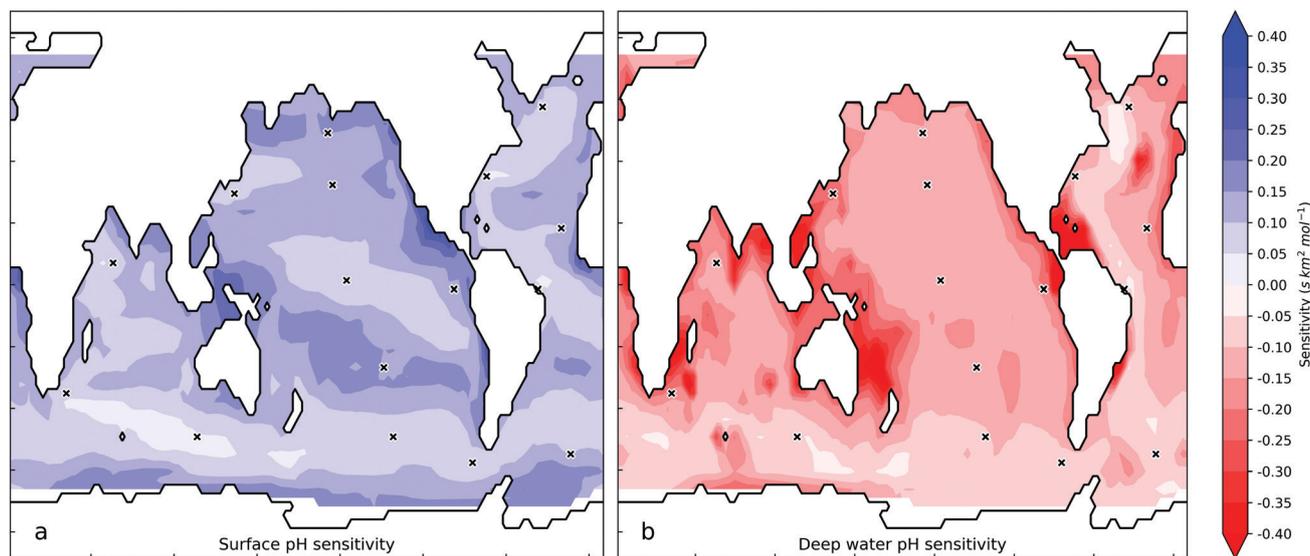
At the surface, the pH increase will be highest right at the injection site, decreasing exponentially with distance. The alkalinity will be compensated by CO<sub>2</sub> uptake, but depending on the local currents and eddies which transport and distribute the alkalinity, as well as wind speeds, surface agitation and local atmospheric CO<sub>2</sub> concentration, we can expect different sensitivities at different injection sites. It is important to avoid too large a pH change both for ecological reasons as well as needing to avoid triggering inorganic precipitation<sup>49</sup> of CaCO<sub>3</sub>. At depth, the injection of acidity must also be considered against an ecological safety margin. We propose that the acidity is injected no closer than 500 m to the seafloor and at least 2000 m from the surface. This area of the ocean is the least

populated by marine species and thus gives ample time for the acidity to dilute horizontally away from the diffuser pipes. Fig. 6 shows the sensitivity of surface and deep water pH on the pumping location from ~1000 individual simulations of single-point alkalinity pumping. The sensitivity ( $\text{m}^2 \text{s mol}^{-1}$ ) was calculated by dividing the maximal  $\Delta\text{pH}$  observed for any given simulation by the pumping rate density ( $\text{mol m}^{-2} \text{s}^{-1}$ ). As expected, areas with stronger surface currents spread surface alkalinity most efficiently, reducing the pH impact at the release location. This effect would be less pronounced if the release stations were free floating with these bulk water movements; however, the horizontal eddy diffusivity is considerably larger in these currents, which would make them preferential release sites nevertheless. Another factor reducing surface pH impact are wind speeds, which reduce the ocean-atmosphere CO<sub>2</sub> equilibration time. The circumpolar wind band likely accounts for the low surface sensitivities observed in the southern ocean (Fig. 6 and Fig. S4, ESI<sup>†</sup>).

## 4 Discussion

### 4.1 Deployment possibilities

The proposed method is only reliant on local resources (seawater) and power and could be implemented in a variety of locations with varying power sources, as shown in Fig. 1. Specifically, it would be uniquely matched for untethered power generators, obviating the otherwise arising problem of energy storage or transmission and material transport encountered in other offshore methods,<sup>50</sup> thus providing a productive use of open-ocean power sources *in situ*.



**Fig. 6** Local surface pH sensitivity in  $\text{s km}^2 \text{mol}^{-1}$  obtained by injection at each grid point only (each grid point represents an entire independent simulation). The sensitivity was calculated by dividing the globally maximal  $\Delta\text{pH}$  in either direction observed for any given simulation by the pumping rate density ( $\text{mol km}^{-2} \text{s}^{-1}$ ). Panel (a) reflects pH changes in the alkaline direction (typically found at the surface release site). The surface sensitivity represents the efficiency with which a stationary addition of alkalinity at any given location with some constant rate is distributed and neutralized by CO<sub>2</sub> invasion. Larger values indicate slower spreading from the release site and/or slower neutralization by CO<sub>2</sub> invasion. Areas with stronger surface currents can spread surface alkalinity most efficiently and are least sensitive to surface pH changes. Panel (b) reflects pH changes in the acidic direction (found in deep water where the acidity is pumped to). The crosses mark the location of the individual plots in Fig. S4 (ESI<sup>†</sup>).



Open-ocean stations could operate on wave, wind or ocean thermal (OTEC<sup>51–54</sup>) power and could be scaled with a large number of untethered, identical units. Open-ocean photovoltaics have been investigated<sup>55</sup> and trial projects are underway.<sup>56</sup> All of these technologies are still in early development and have not yet benefited from commercial efficiencies of scale and are thus currently relatively expensive. Part of the reason for the lack of wide scale adoption is the need for energy transmission in one form or another. Ocean acidity pumping could thus be a perfect match for these technologies. The lack of need for power transmission or transport can further reduce costs compared to current estimates. Alkalinity release in open waters, rather than coastal waters, might be less impactful to marine biology permitting deployment at larger scale.

An alternative approach could involve near-coast operation; larger sized plants could tap into cheap terrestrial energy, especially daytime excess solar. Acid/base generators could potentially be located just-off-coast with a grid connection to land – transportation of electricity being considerably cheaper than transport of matter, *i.e.* the pumping of seawater onto land and back should be avoided.<sup>57</sup> Decommissioned oil rigs may offer an ideal platform for such deployment.

Coastal locations where the continental slope is close to the coast and strong surface currents occur would be preferred, because they shorten the distance acid and base need to be transported, and currents would be able to distribute the excess surface alkalinity effectively. A potential intermediate deployment would consist of near-shore wind farms. Where possible, especially in areas where deep waters are not accessible, the acid stream could also be injected underground, into basalt formations<sup>58–60</sup> or depleted oil wells where it would react with silicate rocks and be neutralized.<sup>16</sup> Injection of hydrochloric acid into rock formations is conceptually similar to the CarbFix process<sup>58</sup> and more generally to carbon capture and storage approaches (CCS).<sup>61</sup> However experimental studies of injectivity, the ensuing *in situ* chemistry and the storage capacities for such acid injections are needed to assess the viability of this approach. Injection into depleted oil reservoirs might be appropriate for example for the North Sea although such areas may be limited to smaller amounts of alkalinity that can be safely released while keeping pH changes below ecological thresholds. However, this could present a feasible method to stabilize ocean pH in localized areas to counteract ecological damage from acidification.<sup>18–20</sup>

## 4.2 Techno-economic estimation

Although a full techno-economic analysis is beyond the scope of this paper, we conduct a rough estimation of potential costs of electrolysing seawater using published data from other methods which create pH gradients. Acid/base production could be implemented using either electrolysis or bipolar membrane electro dialysis. Electrolysis was among the first methods suggested for negative emissions technology,<sup>16</sup> though the generation of gases is energetically inefficient and has to be either recouped using a fuel cell, adding complexity and cost, or recouped by selling the products,<sup>28</sup> which

necessitates mass transport of the products.<sup>50</sup> The use of electrolysis on seawater at gigatonne scale may also produce significant quantities of volatile halogenated organics which are ozone depleting, such as bromo- and chloromethane.<sup>17</sup> Here we choose to focus on electro dialysis methods, which have been proposed and tested for seawater CO<sub>2</sub> extraction.<sup>62–67</sup> However, even if colocated with desalination plants, costs are high (373–604\$ per tCO<sub>2</sub>,<sup>63</sup> 540\$ per tCO<sub>2</sub><sup>66</sup>) in part due to very large quantities of seawater needing to be processed (about 11 000 m<sup>3</sup> tCO<sub>2</sub><sup>-1</sup>). In contrast, releasing the alkalinity to the ocean for passive CO<sub>2</sub> absorption and storage is conceptually and technologically simpler, consisting only of the acid/base generator. The quantity of seawater needing to be processed is greatly reduced (100–500 m<sup>3</sup> tCO<sub>2</sub><sup>-1</sup> depending on the exact concentration of effluent acid and base). There is no CO<sub>2</sub> extraction, thus saving capital and operational costs of membrane contactors<sup>63</sup>. Indeed Digdaya *et al.* found membrane contactors and vacuum pumps accounted for 90% of the equipment cost.<sup>66</sup> Instead, leveraging the ocean as a sorbent surface obviates the need for air contactors as well as additional storage, as the CO<sub>2</sub> is stored as relatively benign bicarbonate ions. From a capital and operational cost perspective, alkalinity pumping is a strict subset of electro dialysis-driven CO<sub>2</sub> extraction and should thus always be cheaper, whether the acidity is moved to deep ocean or underground. The three largest contributors to overall levelized cost would be the cost of electricity to drive the electro dialysis stack, the cost of pre-treating seawater to prevent fouling of the membrane stack and the cost and lifetime of the membranes themselves. Minor contribution costs are the pumping of acidified water to depth. In the open ocean scenario we assume that the cost of the structure are implicit in the assumed levelized costs for open-ocean electricity, and that the electro dialysis apparatus is generally much smaller than the structure. In the following we discuss the likely current ranges of these costs and likely learning curve improvements into the future. However it should be noted that in order to further narrow these estimates, construction of medium-size prototypes<sup>63</sup> is essential.

**4.2.1 Energy costs.** In bipolar membrane electro dialysis (BPMED), the thermodynamic minimum energy to create effluent streams at a given pH can be calculated from the Nernst equation as

$$\Delta G = 2.303RT\Delta\text{pH} \quad (4)$$

where  $\Delta\text{pH}$  is the pH difference between the acid and base effluents. For a base effluent concentration of 1 M NaOH, the minimum energy is  $\sim 80 \text{ kJ mol}^{-1}$  ( $E^0 \approx 0.83 \text{ V}$ ) at ambient conditions. A real BPMED stack of course will require considerably more energy due to ohmic losses in the membranes and the thin solution layers, electrolytic losses at the electrodes, and back-leakage of protons or hydroxide ions. Electro dialysis is, in principle, more efficient than electrolysis for creating a pH gradient, since no additional energy is expended to generate gaseous O<sub>2</sub> or H<sub>2</sub> ( $E^0 = 1.23 \text{ V}$ ) which has to be recouped economically<sup>50</sup> or *via* fuelcell.<sup>16</sup> The specific energy consumption ( $E_{\text{sp}}$ ,  $\text{kJ mol}^{-1}$ ) varies substantially in the literature ranging from 160 to over 350  $\text{kJ mol}^{-1}$



(162 kJ mol<sup>-1</sup>,<sup>68</sup> 155 kJ mol<sup>-1</sup>,<sup>66</sup> 242 kJ mol<sup>-1</sup>,<sup>63</sup> 236 kJ mol<sup>-1</sup>,<sup>67</sup> 255 kJ mol<sup>-1</sup>,<sup>69</sup> 259 kJ mol<sup>-1</sup>,<sup>70</sup> 328 kJ mol<sup>-1</sup>,<sup>71</sup> 341 kJ mol<sup>-1</sup>,<sup>72</sup>). This represents process efficiencies of only 20–45%, suggesting that there is potential for learning curves and technological improvements. Many of the above studies aim to valorize reject brines and are optimized to produce both concentrated (>1 M) and pure acids and bases for industrial use and thus require deionized water to feed acid and base tanks in feed-and-bleed flow schemes. For purposes of acidity pumping the effluent can be more impure and dilute than in the above studies, affording potentially lower costs. The levelized cost of electricity for free floating power generation is highly variable, and likely suboptimal due to the lack of current economies. Wind power has been estimated at \$30–80 per MWh.<sup>54</sup> OTEC is estimated to provide energy at a cost of \$150–200 per MWh.<sup>50,53</sup> Wave power generators levelized costs are highly uncertain and maybe in the range of \$120–470 per MWh.<sup>73</sup> Even though transmission costs can be saved in our case, the present-day costs are likely too high for economical carbon capture, but have considerable potential for reduction with economies of scale. As an alternative, land-based power could be used in near-coast applications where strong currents allow for nearby alkalinity distribution. Examples include the Agulhas, the Kuroshio, the Gulfstream and the North Brazilian current. However deep-water acid disposal becomes more limited as bottom currents are much slower and it may be better to instead pump the acidified stream underground if suitable underground formations are available. Utility scale solar is likely the cheapest land-based energy source with unsubsidized levelized costs as cheap as \$32–44 per MWh and wind at \$28–54 per MWh.<sup>74</sup> It is thought that there will be a considerable excess of this power during daytime hours, for which finding a carbon negative use would be desirable to help with load leveling.

Assuming an efficiency range of 160–250 kJ mol<sup>-1</sup>, energy prices of \$30–80 per MWh and an ocean uptake efficiency  $\eta_{\text{CO}_2}$  of 0.8 we obtain a range for the energy costs of \$38–158 per tCO<sub>2</sub>. It is interesting to compare these energy requirements to other CDR approaches. Electrolytic approaches require about ~300 kJ mol<sup>-1</sup>.<sup>28</sup> Direct air capture (DAC) had been estimated at 312–524 kJ mol<sup>-1</sup>.<sup>75</sup> A comprehensive analysis of recent DAC methods reported 371–546 kJ mol<sup>-1</sup> for liquid solvent approaches and 174–260 kJ mol<sup>-1</sup> for solid sorbents,<sup>76</sup> however much of the energy required is heat rather than electrical.

Energy requirements for methods involving mafic or ultramafic rocks to the ocean, likely needing to be ground to 1  $\mu\text{m}$  for open ocean application,<sup>22</sup> vary substantially from<sup>15,49</sup> 175–315 kWh t<sup>-1</sup> to<sup>24</sup> 500–1000 kWh t<sup>-1</sup>. Depending on the rock type, with a net uptake efficiency of 0.3–0.8 tCO<sub>2</sub> per tonne of rock, one obtains an energy requirement of 35–528 kJ per mol of CO<sub>2</sub> absorbed.

**4.2.2 Water pretreatment costs.** As ion-exchange membranes are prone to scaling and fouling,<sup>77</sup> methods that electrolysise seawater typically use nano-filtration (nF) and reverse osmosis (RO) pretreatment to remove divalent ions,<sup>62,70</sup> concentrate the input brine and provide deionized water, especially for the base compartment where scaling would be most pronounced. The associated costs are not negligible and

tradeoffs need to be considered. Higher flow rates increase pretreatment costs but reduce concentration gradients in the BPMED stack leading to higher faradaic efficiency. There is a tradeoff point, typically around 0.5–1.0 M effluent acid/base, corresponding to a pretreated water need of 56–114 m<sup>3</sup> tCO<sub>2</sub><sup>-1</sup> (accounting for an uptake factor of 0.8). We estimate the cost of water pretreatment<sup>78</sup> at \$0.5 per m<sup>3</sup>, leading to a cost range of \$28–57 per tCO<sub>2</sub>. Development of BPMED processes which are more resistant to fouling, may mitigate this pretreatment cost.

**4.2.3 Bipolar membrane capital costs.** Current densities in BPM stacks vary typically between 450–700 A m<sup>-2</sup> and cell resistivities of ~0.003  $\Omega\text{ m}^3$ , giving a power density of  $P_D = 1.5\text{--}0.6\text{ kW m}^{-2}$ . We can thus calculate the levelized cost contribution of the membranes as  $C_M \eta E_{\text{sp}} / P_D$ , where  $C_M$  ( $\text{\$s}^{-1}\text{ m}^{-2}$ ) is the levelized discounted cost of the membranes and  $\eta = 0.8$  is the CO<sub>2</sub> uptake efficiency. Lower current densities improve the energy efficiency due to lower resistive losses but increase membrane capital costs,<sup>71</sup> leading to cost tradeoffs. Reduction of membrane costs by 5–10 $\times$  through economies of scale and technological advances<sup>79</sup> thus has the opportunity to drastically reduce energy costs. Commercial bipolar membrane stacks (consisting of one bipolar membrane and two monopolar membranes) are currently produced at relatively small quantities, but at moderate scale, with an assumed active lifetime of about 3 years, we could reasonably expect a levelized cost<sup>63,66</sup> of  $C_M = \$200\text{ year}^{-1}\text{ m}^{-2}$ . Thus we estimate the membrane capital cost contribution between \$20–75 per tCO<sub>2</sub>.

**4.2.4 Dispersion.** Depending on the deployment mode, the alkalinity and acidity need to be separated and transported. In the case of open ocean deployment, the alkalinity is simply released on site, while the acidity is pumped to depth. We can assume that the capital costs of the floating structure are implicitly included in the levelized cost of the chosen offshore energy system, as the electrolysis unit would be quite small compared to the energy structure. We can estimate the additional requirements for pumping as follows. Assuming an acid concentration of 0.5–1.0 M, the quantity of water to be pumped is 28–56 m<sup>3</sup> tCO<sub>2</sub><sup>-1</sup>. As no net work is done against gravity, the energy for pumping is that of overcoming the friction in the pipe. We can estimate the head loss (in meters of water) using the empirical Hazen–Williams equation (in SI units):

$$h_f = 10.67 \left( \frac{Q}{C} \right)^{1.852} d^{-4.8704} L \quad (5)$$

where  $Q$  is the flow rate (m<sup>3</sup> s<sup>-1</sup>),  $d$  and  $L$  are the diameter and length of the pipe (m), respectively, and  $C$  is an empirical pipe roughness coefficient, about 140 for a typical smooth pipe. For example a 3000 m long pipe, 5 cm wide, and a flow rate of 5 L s<sup>-1</sup> would require a head pressure of ~40 bar. This is quite similar to injection of CO<sub>2</sub> into basalt formations requiring ~27 m<sup>3</sup> tCO<sub>2</sub><sup>-1</sup> of water and pressures of 25 bar.<sup>58</sup> The power needed to pump water at a rate of  $Q$  through the pipe is given by:

$$P_{\text{pump}} = h_f \rho_w Q \quad (6)$$



where  $\gamma_w$  is the specific weight of water,  $9.8 \text{ kN m}^{-3}$ . The power required to generate the acid and base is given by

$$P_{\text{ED}} = c_{\text{H}} E_{\text{sp}} Q \quad (7)$$

where  $E_{\text{sp}}$  is the specific energy requirement of the BPMED stack ( $\text{kJ mol}^{-1}$ ) and  $c_{\text{H}}$  is the concentration of acid produced ( $c_{\text{H}} = 10^{-\text{pH}}$ ). Assuming for example  $c_{\text{H}} \approx 0.75 \text{ M}$  and  $E_{\text{sp}} \approx 180 \text{ kJ mol}^{-1}$  we obtain  $P_{\text{ED}} \approx 675 \text{ kW}$  and  $P_{\text{pump}} \approx 20 \text{ kW}$ , just 3% of the dialysis energy requirements. However, the engineering requirements for a deep-ocean pipe system are non-negligible, resembling in many ways that of deep ocean lift cables for deep ocean ROV systems in terms of size, design and required resistance to ocean stress. The amortized costs, for a production at scale, are highly dependent on the particular ocean location and mode of deployment and thus difficult to estimate. As an orientation, if we assume conservatively a 5 year lifespan and a cost of \$60 per m for a 2500 m pipe we obtain a levelized cost of about \$7.2 per  $\text{tCO}_2$ . However the challenges of open-sea engineering are formidable and pilot studies would be necessary to narrow the cost estimates.

If alkalinity is generated near shore at scale it will need to be dispersed away far from the shore to avoid local pH spikes. However, because the alkalinity is relatively dilute ( $0.1\text{--}1 \text{ mol kg}^{-1}$ ) compared to dry solid alkaline materials ( $\sim 25 \text{ mol kg}^{-1}$ ) bulk transportation is considerably less efficient. For example, at  $\eta = 0.8$ , 28.4 tonnes of  $1 \text{ mol kg}^{-1}$  hydroxide solution are required for every tonne of  $\text{CO}_2$  absorbed. Large-scale maritime shipping costs are around \$0.0016–0.004 per t per km and produce about  $7 \text{ gCO}_2$  per t per km.<sup>49</sup> Assuming alkalinity to be dispersed in a 150 km strip around the coast, *i.e.* well within the exclusive economic zone of any bordering country, and typical tanker speeds of 14 knots ( $7.2 \text{ m s}^{-1}$ ), the 300 km roundtrip (150 km zone) could be completed in 12 hours, with a daily turnaround. Assuming a factor of 2 inefficiency compared to ordinary shipping, due to the very frequent loading, we obtain a cost of \$13–33 per  $\text{tCO}_2$ . Furthermore, as tankers are hard to decarbonize,  $\sim 57 \text{ kgCO}_2$  are emitted for every tonne of  $\text{CO}_2$  absorbed, about a 5% reduction in efficiency. The additional costs and the additional  $\text{CO}_2$  impact of transport limit alkalinity release to coastal areas and thus limit the total scaling of land-based alkalinity production.

Overall for open-ocean deployment we obtain a minimum cost per tonne of  $\text{CO}_2$  captured of  $\sim \$93\text{--}297$  per  $\text{tCO}_2$ . This estimate is quite close to estimations obtained by a recent study<sup>57,63</sup> ( $110\text{--}325$  per  $\text{tCO}_2$ ) for the BPMED portion of their process, which conducted a much more detailed technoeconomic analysis for  $\text{CO}_2$  extraction. As expected the costs are much lower than estimates for  $\text{CO}_2$  extraction ( $373\text{--}604$  per  $\text{tCO}_2$ <sup>63</sup>,  $540$  per  $\text{tCO}_2$ <sup>66</sup>)

At the lower end, the total cost estimate has similar-sized cost contributions from energy cost, membrane cost and water treatment cost. Thus to drive down overall costs development and cost reduction is needed in all three areas. We note that the dialysis membrane industry is currently very small and very significant cost savings could be expected at scale.<sup>79</sup> Furthermore, as with all ocean CDRs, working with ocean water and in marine environments in general poses significant challenges in terms of

corrosion and longevity of the equipment which will need to be addressed for a practical, scalable application.

For comparison, costs for direct air capture have been reported at \$89–407 per  $\text{tCO}_2$  for solid sorbent systems and \$156–506 per  $\text{tCO}_2$  for liquid solvent systems.<sup>76</sup> The operational costs of enhanced weathering has been estimated at \$70–578 per  $\text{tCO}_2$  and \$24–123 per  $\text{tCO}_2$  for basic and ultrabasic rocks respectively<sup>49</sup> and ocean liming falls in the \$72–159 per  $\text{tCO}_2$  range.<sup>13</sup>

## 5 Conclusions

We have explored the feasibility of accelerating the natural compensation of ocean acidification by  $\text{CaCO}_3$  deposits by artificially pumping excess acidity towards the abyssal  $\text{CaCO}_3$  sediments. The subsequent alkalization of the surface would counteract anthropogenic acidification and increase the uptake of significant quantities of atmospheric  $\text{CO}_2$ . Thus alkalinity pumping could meaningfully contribute to a portfolio of negative emissions technologies. Based on our simulation we estimate 1–3 GtC per year could be removed over a 50 year period, without lowering deep water pH by more than 0.2. For acid injection depth  $>3000 \text{ m}$  we show that carbonate compensation is significantly engaged, permanently removing up to 40% of the absorbed  $\text{CO}_2$ . Reemission of the remainder occurs only after 300 years and slowly over several millenia of gradual outgassing, effectively flattening the curve of the anthropogenic  $\text{CO}_2$  shock to the atmosphere. In theory up to 150 GtC could be removed this way before the end of the century, satisfying requirements for negative emissions laid out by RCP2.6 pathways. What might a scaled up deployment look like? Modern offshore 10 MW wind turbines can generate on the order of 50 GWh of energy per year, which could be used to sequester on the order of 10 ktC per year. Thus for a total scale of 1 GtC per year about 100 000 of such units would be necessary (*i.e.* about 1000 GW of total capacity). For comparison current global offshore wind capacity is already expected to reach about 500 GW by 2050, thus a goal of 1 GtC per year negative emissions could be feasible before the end of the century.

The pumping of ocean acidity presented in this paper avoids many of the environmental issues with mineral-adding alkalinity methods both in terms of impurity dissolution in the ocean and mining impacts on land. It is conceptually simple and requires only locally available resources (seawater and energy), and is thus uniquely suited to openwater deployment. While in the short term, on-shore electrochemical alkalization is likely more economical due to the inherent engineering challenges of marine engineering, it is also inherently limited in scale. We have shown that transport of dilute acid or base is not economical beyond 150 km away from the production site. Disposal of dilute acid into deep basalt aquifers provides a partial solution but its scaling limits are not well understood. Therefore open-water production of acid and base could supplement terrestrially powered CDR and is an interesting



avenue of research despite the usual challenges of marine engineering. Open-water CDR also provides a route to make use of otherwise unusable renewable energy, an area of CDR research that has been underexplored. In general, manipulation of acidity/alkalinity as a proxy for CO<sub>2</sub> may be technologically simpler and/or more efficient than manipulation of CO<sub>2</sub> directly, whether the acidity is moved into deep ocean or underground. We also presented a fine-grained analysis of location dependence of surface alkalization and show that in the short term there is substantial variation in CO<sub>2</sub> uptake efficiency which will need to be considered in any ocean alkalization plan, mineral-based or not. As with all ocean-based CDR methods, simulations have inherent limits and the ecological parameters and limitations require substantial further research of natural analogues<sup>45</sup> and experimentation in meso-scale pilot programs.

## Conflicts of interest

There are no conflicts to declare.

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