

## PAPER

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View Journal | View IssueCite this: *Energy Environ. Sci.*, 2022, 15, 3978The mechanism for acetate formation in electrochemical CO<sub>(2)</sub> reduction on Cu: selectivity with potential, pH, and nanostructuring†Hendrik H. Heenen, <sup>‡\*ab</sup> Haeun Shin, <sup>‡</sup> Georg Kastlunger, <sup>a</sup> Sean Overa, <sup>c</sup> Joseph A. Gauthier, <sup>§de</sup> Feng Jiao <sup>\*c</sup> and Karen Chan <sup>a</sup>

Nanostructured Cu catalysts have increased the selectivities and geometric activities for high value C–C coupled (C<sub>2</sub>) products (ethylene, ethanol, and acetate) in the electrochemical CO<sub>(2)</sub> reduction reaction (CO<sub>(2)</sub>RR). The selectivity among the high-value C<sub>2</sub> products is also altered, where for instance the yield of acetate increases with alkalinity and is dependent on the catalyst morphology. The reaction mechanisms behind the selectivity towards acetate vs. other C<sub>2</sub> products remain controversial. In this work, we elucidate the reaction mechanism for acetate formation by using *ab initio* simulations, a coupled kinetic-transport model, and loading dependent experiments. We find that trends in acetate selectivity can be rationalized from variations in electrolyte pH and the local mass transport properties of the catalyst and not from changes in Cu's intrinsic activity. The selectivity mechanism originates from the transport of ketene, a stable (closed shell) intermediate, away from the catalyst surface into solution where it reacts to form acetate. While this type of mechanism has not yet been discussed in the CO<sub>(2)</sub>RR, variants of it may explain similar selectivity fluctuations observed for other stable intermediates like CO and acetaldehyde. Our proposed mechanism suggests that acetate selectivity increases with increasing pH, decreasing catalyst roughness and significantly varies with the applied potential.

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## Broader context

The electrochemical reduction of CO<sub>2</sub> enables the storage of renewable energy in carbon neutral fuels while simultaneously reducing greenhouse gas emissions. Recent developments have led to industrially relevant performances exploiting nanostructured Cu catalysts and gas-diffusion electrodes, which produce high value C<sub>2</sub> products at high current densities. The selectivity between these C<sub>2</sub> products, which mainly consist of ethylene, ethanol and acetate, still poses a challenge to maximize cost efficiency. In this joint experimental-theoretical work, we elucidate the selectivity mechanism towards acetate vs. ethylene and ethanol using a multi-scale modelling approach with excellent agreement to experiments. We determine that the transport properties at the catalyst surface are pivotal in steering the selectivity between acetate and other C<sub>2</sub> products. While our insights deduce design rules for an acetate rich or poor CO<sub>2</sub> reduction process important for a pure liquid product stream, they can be generalized to understand selectivity changes with catalyst roughness of other products and processes.

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## 1 Introduction

The electrochemical reduction of carbon dioxide (CO<sub>2</sub>RR) or carbon monoxide (CORR) has the potential to enable the storage of renewable energy *via* the production of carbon neutral commodity chemicals. Cu electrocatalysts have thereby been extensively explored for the CO<sub>(2)</sub>RR, since Cu is the only material able to produce high value C–C coupled (C<sub>2</sub>) products (ethylene, ethanol and acetate).<sup>1</sup> Improvements in activity and selectivity of these catalysts are urgently needed to enable the commercialization and cost-effective operation of CO<sub>(2)</sub>RR electrolyzers.<sup>2,3</sup> To this end, two key developments have been made over the last decade. First, gas diffusion electrodes (GDE) in combination with flow cell setups achieve significantly



higher current densities towards  $\text{CO}_2\text{RR}$  products over traditional H-cell setups, which suffer from mass transport limitations.<sup>4–6</sup> Second, various means of nanostructuring Cu have been explored in order to increase the active surface area and to tune the selectivity towards high value products.<sup>1,7–10</sup> For instance, nanostructured catalysts in a GDE/flow-cell setup have led to significantly increased selectivities towards acetate under alkaline conditions.<sup>11,12</sup> Originally considered a minor product, under these specific conditions, acetate has Faradaic efficiencies comparable to those of ethylene and ethanol, the two major  $\text{C}_2$  products produced by Cu under neutral and mildly alkaline conditions.<sup>4,11,13</sup> To date, there is no consensus on how nanostructuring or mass transport impacts the intrinsic activity and selectivity of Cu towards the possible  $\text{C}_2$  products.<sup>9,10</sup>

In this paper, we suggest that nanostructuring of Cu changes the selectivity for acetate *vs.* other  $\text{C}_2$  products through altering the mass transport of products away from the electrode, and not through changes in intrinsic activity *via* new active sites.<sup>12</sup> We suggest that acetate forms *via* a solution reaction of ketene with  $\text{OH}^-$ , which is heavily affected by the transport and electrolyte pH. Our insight results from a comprehensive examination of the reported experimental activities of Cu catalysts normalized to the active surface area, an *ab initio* derived microkinetic model coupled to mass transport, and through activity measurements on different Cu catalysts in a range of pH and loadings.

Previous computational studies have attempted to rationalize the acetate activity and selectivity through reaction thermodynamics and barriers.<sup>11,12,14</sup> However, the dependence of acetate selectivity on pH and potential remained an open question, and performance differences in various Cu samples were assumed to arise from different active sites. We suggest that such mechanisms are inconsistent with the electrochemically active surface area (ECSA)-normalized activity of all reported Cu catalysts and the potential dependence of the observed selectivity. In contrast, our computational model shows that the interplay of kinetics and mass transport determines the acetate selectivity *vs.* other  $\text{C}_2$  products. The model agrees with the experimentally observed trends in the dependence of acetate selectivity on potential, electrolyte pH, and catalyst roughness. Previously, transport limitations have already been suggested to alter the selectivity behavior between  $\text{CO}_2\text{RR}$  products and  $\text{H}_2$  by affecting the reactant concentrations and local pH at the catalyst surface.<sup>6,15–20</sup> This work showcases how mass transport also controls the competition between the desorption and the further reduction of stable intermediates with a corresponding impact on selectivity. This concept has been similarly proposed for stable intermediates in the oxygen reduction reaction (ORR) and methanol oxidation.<sup>21</sup> This principle is, therefore, generalizable to controlling the selectivity of other stable intermediates in the  $\text{CO}_2\text{RR}$  like CO and acetaldehyde. Overall, our combined analysis of experiments and simulations suggests that acetate selectivity against other  $\text{C}_2$  products is optimized by a high interfacial and bulk pH and a low, microscopic surface roughness of the Cu catalyst, which should be considered in the design of  $\text{CO}_2\text{RR}$  electrolyzers.

## 2 Results & discussion

### 2.1 ECSA normalized current densities suggest no change in intrinsic activity toward $\text{C}_2$ products with nanostructuring

We compare ECSA-normalized current densities,  $j_{\text{ECSA}}$ , to evaluate  $\text{CO}_2\text{RR}$  activities and selectivities, in Fig. 1.  $j_{\text{ECSA}}$  is the best available estimate for the intrinsic activity in the absence of mass transport limitations, as turnover frequencies (TOF), which reflect the true intrinsic activity per active site, are generally not accessible in electrochemical measurements.<sup>1,10,22</sup> Within the variations in active site densities amongst the catalysts considered,  $j_{\text{ECSA}}$  is proportional to the turnover frequency.<sup>23</sup>

Fig. 1 shows  $j_{\text{ECSA}}$  for various Cu catalysts in both GDE and H-cell setups towards the sum of all  $\text{C}_2$  products in  $\text{CO}_2\text{RR}$  and specifically toward ethylene, ethanol, and acetate. Even under a wide range of reaction conditions (CO and  $\text{CO}_2$  as the reactant, different electrolytes with pH ranging from 6.8 to 14.3, wide potential range) and catalyst morphologies (from Cu single crystals and foils to deliberately roughened oxide-derived (OD) Cu, nanowires and nanoparticles), we find the currents to overlap within an order of magnitude for data sets without obvious transport limitations (blue lines in Fig. 1, which all

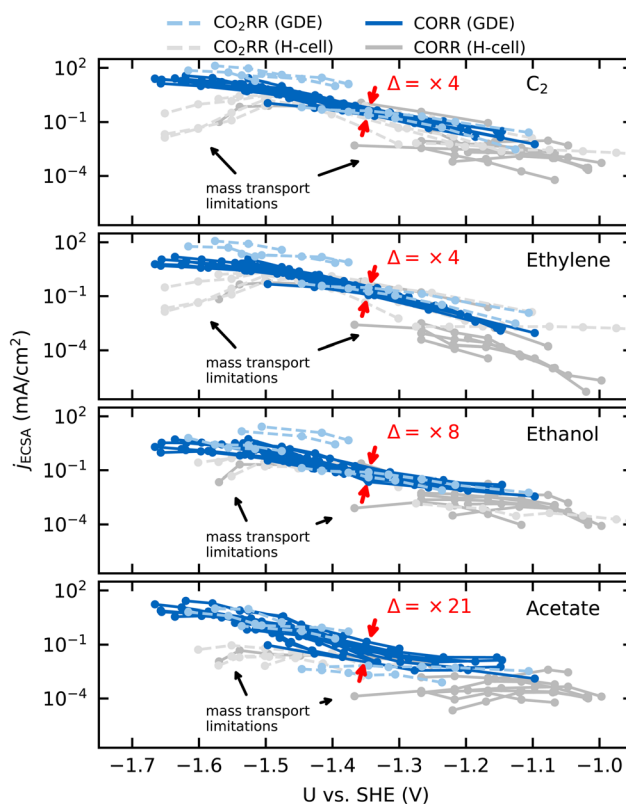
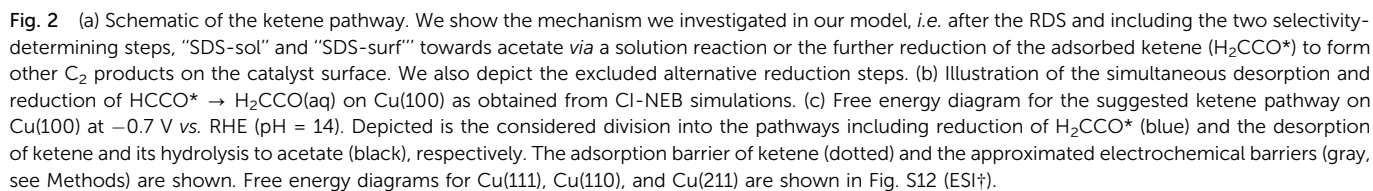


Fig. 1 ECSA normalized partial current densities against  $U_{\text{SHE}}$  for  $\text{C}_2$  (top), ethylene (upper center), ethanol (lower center), and acetate (bottom) adapted from different  $\text{CO}_2\text{RR}$  (dashed lines) and CORR (solid lines) studies conducted in a GDE/flow-cell setup (light-blue/blue) or a conventional H-cell setup (light-gray/gray). Each line represents an individual data set of the same reaction conditions. The GDE data is adapted from ref. 4, 11 and 25–29 and the H-cell data from ref. 7, 8, 30, 32 and 33. The red arrows indicate the (multiplicative) factor in variation of  $j_{\text{ECSA}}(\Delta)$  at  $-1.35V_{\text{SHE}}$ .



Fig. 1 also shows a subtly stronger variation of the acetate currents in comparison to ethylene and ethanol although all  $C_2$  products follow a similar potential behavior (or Tafel slope). While the former is a function of the electrolyte pH and catalyst morphology (see below), the latter indicates the same rate determining step for these  $C_2$  products. In what follows, we derive a comprehensive mechanism for acetate formation which rationalizes the dependence of its activity on pH and catalyst morphology.

Fig. 2(a) shows our proposed mechanism of the selectivity determining steps (SDS) towards acetate *vs.* other major  $C_2$  products, determined on the basis of DFT simulations. Central to this mechanism is the ketene intermediate as suggested previously.<sup>8,11,14</sup> However, we emphasize its importance in both its desorbed ( $H_2CCO(aq)$ ) and adsorbed ( $H_2CCO^*$ ) state. As shown in Fig. 2(a and b), a proton-coupled electron transfer (PCET) to  $HCCO^*$  leads to the formation of the stable ketene molecule, desorbed from the surface. This reaction step is pivotal because past its formation,  $H_2CCO(aq)$  can either react with  $OH^-$  to acetate in solution (a well-known reaction<sup>34</sup>) or readsorb and get further reduced to other  $C_2$  products. Either pathway is differently influenced by pH, (ketene) transport, and



potential. The elementary reactions making up this branching point evolve around two SDS as indicated in Fig. 2(a):

1. (SDS-surf, only low overpotentials) The PCET reaction of  $\text{H}_2\text{CCO}^*$  towards other  $\text{C}_2$  products vs. the desorption of re-adsorbed ketene.
2. (SDS-sol) The solution reaction vs. re-adsorption of desorbed ketene.

Firstly, we note that SDS-sol is dependent on the concentration of  $\text{H}_2\text{CCO}(\text{aq})$  and  $\text{OH}^-$  at the catalyst surface which depends strongly on mass transport. Secondly, we note that SDS-sol involves the competition between two chemical steps while SDS-surf between a chemical and an electrochemical step. Acetate selectivity of SDS-sol is therefore not (directly) potential dependent in contrast to SDS-surf. The concentration and potential (in)dependence have an important impact on the selectivity, as we detail below.

We derive and validate this mechanism using density functional theory (DFT) calculations. In our derivation, we assume the same rate determining step (RDS) for all  $\text{C}_2$  products based on previous experimental and theoretical studies, which has been suggested to either be a  $\text{CO}^*$  dimerization<sup>35–37</sup> or the protonation of the  $\text{OCCO}^*$  intermediate with water as the proton donor.<sup>38</sup> The same RDS is consistent with the range of similar Tafel slopes and the distinguishing lack of an inverse pH-activity relationship shared among the considered  $\text{C}_2$  products (ethylene, ethanol, acetate)<sup>11</sup> (see Fig. 1 above and elaboration of the pH effect in the ESI,† Section S6). Such a shared and early RDS means that the energetics of the following intermediates have no effect on the activity towards the sum of all  $\text{C}_2$  products, and only affect the selectivity amongst them (*i.e.*  $r_x = r_{\text{RDS}} \frac{r_x^{\text{SDS}}}{\sum_i r_i^{\text{SDS}}}$ , with  $x$

being a specific product of the SDS).<sup>39</sup> We evaluate our suggested reaction mechanism on representative facets: Cu(111) and Cu(100) as terraces and Cu(110) and Cu(211) as steps. We choose intermediates prior to  $\text{HCCO}^*$  (and thus ketene) based on their thermodynamic or kinetic stability which is in line with established trends.<sup>40</sup> On all facets considered, the free energies of all steps are mostly downhill and any uphill step is well below 0.75 eV as shown in Fig. 2(c) and Fig. S12 (ESI†) which makes the mechanism feasible at room temperature.<sup>23</sup> We also evaluated the chemical and PCET barriers at a constant potential<sup>41</sup> (see Methods and Section S3 in the ESI†) around SDS-sol and SDS-surf which are also low enough to lead to measurable rates at room temperature (see Fig. 2(c) and Fig. S12, Table S6 in the ESI†). An only exception is an insurmountable re-adsorption barrier for ketene on Cu(111) and Cu(110), which makes these facets inactive for the proposed mechanism to other  $\text{C}_2$  products (see Fig. S12 and Section S5.6 in the ESI†). We emphasize that the direct  $\text{HCCO}^* \rightarrow \text{H}_2\text{CCO}(\text{aq})$  step was an explicit result from the transition state search and occurs on all investigated facets.

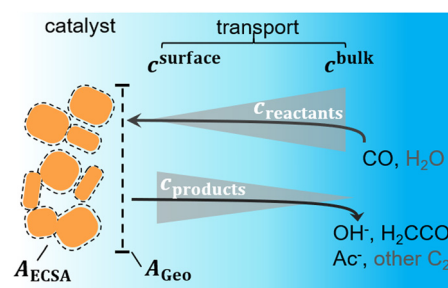
### 2.3 Acetate selectivity is determined by the interplay of kinetics, mass transport, and electrode roughness

To investigate the selectivity behavior we couple our DFT-based energetics with both a microkinetic and a mass transport model.

The microkinetic model describes the surface reactions of our proposed reaction mechanism to acetate and other  $\text{C}_2$  products (see Fig. 2 and the ESI,† Section S5.1). The mass transport model describes the transport according to the conditions of CORR operation in a GDE/flow cell setup (with corresponding pH, reactants, and diffusion lengths), where the highest selectivity for acetate is observed.<sup>4,8,11,25,30</sup> We only consider the dominant pathway for the acetate formation (*i.e.*  $\text{CO}_{(2)}\text{RR}$  at cathode) in this study, although acetate could also be formed through a partial oxidation of ethanol (the product of  $\text{CO}_{(2)}\text{RR}$ ) at the anode in certain cell configurations due to its cross-over through membranes.<sup>25,42</sup>

In our microkinetic model we fit the common RDS for the  $\text{C}_2$  products to the ECSA normalized activity found in experiments (see the ESI,† Section S5.1). Furthermore, we apply our DFT-derived energies for Cu(100) in the microkinetic model, whereby the quantitative behavior of the model is only sensitive to the re-adsorption, desorption, and reduction barrier of the ketene intermediate and insensitive to any other facet dependent energy (see the ESI,† Section S5.6). We note that we fitted the free energy of  $\text{H}_2\text{CCO}(\text{aq})$  at the interface to reproduce the experimental selectivity, as it is poorly represented by the static electrode-solvent interface applied in our calculations. This fit leads to an energy correction of 0.29 eV which is within DFT uncertainty on the one hand but also reproduces the adsorption barrier height on Cu(211) on the other hand, and is therefore a reasonable assumption (see the ESI,† Section S5.6.1 and Fig. S18).

For the description of the mass transport, we use a 1D-mass transport model where we account for the diffusion of  $\text{CO}$ ,  $\text{OH}^-$ , and  $\text{H}_2\text{CCO}$  as well as the solution reaction of  $\text{H}_2\text{CCO}$  and  $\text{OH}^-$  to acetate,<sup>19,43</sup> as illustrated by Fig. 3 and Fig. S14 (ESI†). We also include a Sherwood relation to account for the convective mass transport encountered in a flow cell. It describes the diffusion of species from the bulk of the flowing electrolyte to the electrode surface.<sup>44–46</sup> All constants and coefficients are taken from the literature, for details refer to Methods and the ESI,† Section S5. Within our 1D approximation, the effect of the nanostructuring of Cu is captured only by a single roughness factor  $\rho$ , and we assume a constant active site density.



**Fig. 3** Schematic of the mass transport considered in our model.  $\text{CO}$ ,  $\text{OH}^-$ ,  $\text{H}_2\text{CCO}$ , and Acetate ( $\text{Ac}^-$ ) (black color) are considered for transport while  $\text{H}_2\text{O}$  and other  $\text{C}_2$  are neglected (grey color). Typical concentration gradients are depicted and it is indicated how the transport scales with geometric area  $A_{\text{Geo}}$  while processes on the catalyst surface scale with  $A_{\text{ECSA}}$ .





The roughness  $\rho$  generally describes the ratio of active area and geometric area ( $A_{\text{ECSA}}/A_{\text{geo}}$ ). This ratio can change microscopically with local curvature and porosity of the nanostructured Cu surface or mesoscopically with the loading of Cu particles on the GDE. As discussed in detail later, the short diffusion length scales in the presence of the rapid solution reaction treated here, effectively define  $\rho$  to be a microscopic roughness.

The included mass transport limitations give rise to changes in the microscopic reaction environment at the catalyst surface through changes in the surface concentrations of individual species (in our case of CO, OH<sup>−</sup>, and H<sub>2</sub>CCO). Their local concentrations decisively affect the coupled reaction kinetics. For example, increasing flux and current densities at higher overpotentials give rise to increased concentration gradients, such that the surface concentrations of reactants (CO) decrease while those of the electrochemical products (OH<sup>−</sup> and H<sub>2</sub>CCO) increase (compare Fig. 3). The concentration profiles are further affected by pH and  $\rho$  as discussed in detail in the ESI,<sup>†</sup> Section S5.5 which importantly influence acetate selectivity trends. These relationships finally enable the simulation of the C<sub>2</sub> current and selectivity dependent on potential, bulk pH and catalyst roughness  $\rho$  as depicted in Fig. 4(a).

The simulated geometric current densities of C<sub>2</sub> products ( $j_{\text{geo}}^{\text{C}_2}$ ) are shown in the top panel of Fig. 4(a). The maximum  $j_{\text{geo}}^{\text{C}_2}$  reached at high overpotentials (more negative  $U$ ) reflects the CO diffusion limited current density (see Fig. S17a, showing the depletion of CO close to the surface, ESI<sup>†</sup>). At lower overpotentials, the linear dependence of  $j_{\text{geo}}^{\text{C}_2}$  on the catalyst  $\rho$  reflects the linear dependence of  $j_{\text{geo}}^{\text{C}_2}$  on  $A_{\text{ECSA}}$ .

The bottom panel in Fig. 4(a) shows the computed selectivity of acetate vs. the total C<sub>2</sub> products ( $S_{\text{Ac}^-}^{\text{C}_2}$ ). We emphasize that

the shown selectivities, being molar ratios relating between C<sub>2</sub> products, differ from Faradaic efficiencies (FE) which are weighted by transferred electrons and therefore ambiguous for mechanistic analysis. In general, we distinguish the critical variables affecting  $S_{\text{Ac}^-}^{\text{C}_2}$  as the roughness  $\rho$  and the (interfacial) pH. These variables depend on catalyst morphology and on electrolysis conditions. The resulting trends arise from the competition between the transport/solution reaction and re-adsorption of H<sub>2</sub>CCO(aq) in SDS-sol (see Fig. 2(a)):

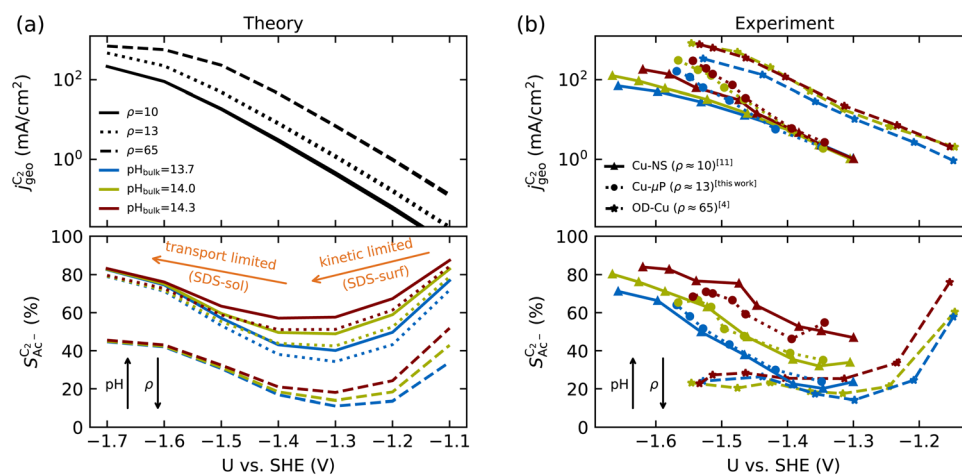
- An increasing roughness  $\rho$  lowers  $S_{\text{Ac}^-}^{\text{C}_2}$  since an increased catalyst surface area ( $A_{\text{ECSA}}$ ) favors H<sub>2</sub>CCO(aq) adsorption. Note that the area which affects the transport and solution reaction towards acetate ( $A_{\text{geo}}$ ) remains unchanged.
- An increasing concentration [OH<sup>−</sup>] increases  $S_{\text{Ac}^-}^{\text{C}_2}$  since OH<sup>−</sup> catalyzes the solution reaction of ketene to acetate. This selectivity behavior confirms a first order dependence of acetate formation with OH<sup>−</sup>. The interfacial pH (which scales with the bulk pH) is decisive because the conversion of ketene occurs close to the catalyst surface (as elaborated below).

$S_{\text{Ac}^-}^{\text{C}_2}$  scales stronger with the roughness and weaker with pH (compare Fig. 4) following the relationship

$$S_{\text{Ac}^-}^{\text{C}_2} \propto \frac{\sqrt{[\text{OH}^-]}}{\rho} \quad (1)$$

as we derive in the ESI,<sup>†</sup> Section S7. The U-shaped selectivity curve vs. potential can be explained by the interplay of SDS-sol and SDS-surf.

1. At low overpotentials: the selectivity towards other C<sub>2</sub> products is limited by the potential dependent protonation of H<sub>2</sub>CCO\* (in SDS-surf) while the step towards



**Fig. 4** Geometric current densities towards all C<sub>2</sub> products ( $j_{\text{geo}}^{\text{C}_2}$ , top) and acetate selectivity among them ( $S_{\text{Ac}^-}^{\text{C}_2}$ , bottom) against  $U_{\text{SHE}}$  as (a) simulated by our transport coupled microkinetic model and (b) experimentally measured. Each line represents an individual data set with the same reaction conditions. The different colors represent varying electrolyte pH and the solid, dotted, and dashed lines experiments and simulations with Cu-NS or  $\rho = 10$ , Cu- $\mu$ P or  $\rho = 13$ , and OD-Cu or  $\rho = 65$ , respectively. The experimental data has been measured in this work or is adapted from ref. 4 and 11. Note that the simulated  $j_{\text{geo}}^{\text{C}_2}$  is invariant to pH as it follows the pH independent RDS of the C<sub>2</sub> products and competition to C<sub>1</sub> products like methane and the hydrogen evolution reaction or cation effects<sup>47</sup> are not included in our model, the simulated  $j_{\text{geo}}^{\text{C}_2}$  is therefore depicted in black. The simulated  $j_{\text{geo}}^{\text{C}_2}$  for  $\rho = 10$  was scaled by  $\frac{1}{2}$  according to the lower loading used for the Cu-NS of 0.5 mg cm<sup>−2</sup> compared to 1.0 mg cm<sup>−2</sup>.<sup>4,11</sup> The dominating selectivity mechanisms including kinetic and transport competition are indicated (see the text).



acetate is potential independent. Therefore, as the overpotential increases, the selectivity towards acetate decreases.

- At high overpotentials: the protonation of  $\text{H}_2\text{CCO}^*$  is facile. The selectivity is then determined by  $\text{H}_2\text{CCO}(\text{aq})$  readsorption *vs.* the solution phase reaction of  $\text{H}_2\text{CCO}(\text{aq})$  with  $\text{OH}^-$  (in SDS-sol). The build-up of local  $\text{OH}^-$  concentration at increasing overpotentials (local pH, see the concentration profile in Fig. S17b, ESI†) favors the latter reaction and leads to an uptick in acetate selectivity.

The complex selectivity behavior of our simulations is consistent with experiments as shown in Fig. 4(b). We compare it to experimental data measured in this work and data adapted from ref. 4 and 11 which is based on conditions equivalent to our simulations (CORR in a GDE/flow-cell setup). Different Cu-catalyst morphologies are included in this data with nanosheets (Cu-NS), micron sized particles (Cu- $\mu\text{P}$ ), and oxide-derived Cu (OD-Cu). The roughness of these catalysts was determined to be 10, 13, and 65, respectively, *via* capacitance measurements and after normalization by loading (see the ESI,† Table S5).<sup>4,11</sup> At comparable catalyst loadings for these samples, the differences in the roughness should arise for the most part from microscopic variations amongst the catalysts' morphology. We therefore apply these roughness values to be the microscopic roughness  $\rho$  in our model. We find  $j_{\text{geo}}^{\text{C}_2}$  to align between theory and experiment regarding the limiting behavior of CO diffusion and the scaling with respect to  $\rho$ , which is expected as a direct result of the fitted RDS. Importantly, as a consequence of the proposed mechanism, the simulated acetate selectivity  $S_{\text{Ac}^-}^{\text{C}_2}$  shows very good agreement with the experiment. We observe the same trends in roughness and electrolyte pH for the acetate selectivity  $S_{\text{Ac}^-}^{\text{C}_2}$ , *i.e.* increasing  $S_{\text{Ac}^-}^{\text{C}_2}$  with decreasing roughness and increasing pH. Also, the complex potential dependent U-shape is found in both simulated and measured data. We note that this U-shape is not only observed in the acetate selectivity among  $\text{C}_2$  products ( $S_{\text{Ac}^-}^{\text{C}_2}$ ) shown here but can also be seen in acetate's Faradaic efficiency (see the ESI,† Fig. S1).

We note that at higher overpotentials, there is a pH dependence of activities (partial current densities  $j_{\text{geo}}^{\text{C}_2}$ ) in the experimental data in the upper panel of Fig. 4(b). We did not include the competing pH dependent  $\text{C}_1$  pathway or ion concentration effects<sup>1,47</sup> in our simulations which could reproduce such an apparent pH dependence. Other/smaller quantitative deviation may originate in uncertainty of the measured catalyst roughness, of assumed flow-rates and of the charge-neutral approximation or neglected size effects in our Nernst-Planck formulation in the transport model.

#### 2.4 Short diffusion lengths of ketene suggest that micro-, not macro-scopic roughness determines acetate selectivity

As we show in Fig. 5(a), the diffusion length  $L_d$  for  $\text{H}_2\text{CCO}(\text{aq})$  is within 200 nm of the catalyst surface due to the rapid solution reaction between  $\text{H}_2\text{CCO}$  and  $\text{OH}^-$ . This length scale is not only

well within a diameter of a single pore of a GDE electrode<sup>6,17,45</sup> but on the same order of magnitude as the diameter of the catalyst particles ( $d_p$ ) used for the experiments in Fig. 4(b) (see the ESI,† Fig. S2 and ref. 4, 11). Thus, in such an electrode arrangement the diffusion spheres around the nanoparticles do not overlap as we show in Fig. 5(c). Instead, the length scale of roughness features relevant for the competition between kinetics and mass transport in our selectivity mechanism are smaller than  $d_p$ . We therefore define  $\rho$  in our model as a microscopic roughness  $A_{\text{real}}/A_{\text{smooth}}$ , where  $A_{\text{smooth}}$  corresponds to the area of an ideal, smooth nanoparticle. This definition of the roughness fulfills its general definition  $A_{\text{ECSA}}/A_{\text{geo}}$ , but not *vice versa*. Thus, changes in catalyst loading (which alter  $A_{\text{ECSA}}/A_{\text{geo}}$ ) do not alter  $\rho$  and should therefore lead to no changes in the acetate selectivity. This is true unless the diffusion spheres of adjacent particles could overlap significantly which would be the case for very small nanoparticles ( $d_p \ll 100$  nm) (compare Fig. 5(c)).

We evaluate this hypothesis through our measurements of CO reduction in 1 M KOH on Cu catalysts of different morphology and at different loadings. Specifically, we compare micron-sized (Cu- $\mu\text{P}$ , same as above) and 25 nm-sized (Cu-25nmP) particles which we characterize with a mass normalized roughness  $\rho$  of 13 and 63, respectively (see the ESI,† Section S1.5). Note that by changing only the loading of Cu particles, the morphology of the catalyst and its microscopic surface roughness  $\rho$  remain the same. With higher loadings, the geometric current densities increase (which necessitates measurements at different potential ranges for matching current densities), but the current densities coincide after mass normalization (see Fig. S5, ESI†). This alignment with normalization suggests that the higher current densities at higher loadings are due to the increased active area with the same intrinsic activity. As shown in Fig. 5(b), the same selectivity of acetate among the  $\text{C}_2$  products ( $S_{\text{Ac}^-}^{\text{C}_2}$ ) is found within the range of 0.5–1.5  $\text{mg cm}^{-2}$  and 1.0–1.5  $\text{mg cm}^{-2}$  for Cu- $\mu\text{P}$  and Cu-25nmP, respectively. While  $S_{\text{Ac}^-}^{\text{C}_2}$  is independent of these loadings, it still differs according to the mass normalized roughness  $\rho$  and hence according to the catalyst morphology, in line with our computational model (compare Fig. 4(a) and Fig. S4, ESI†). These trends in  $S_{\text{Ac}^-}^{\text{C}_2}$  confirm that it is not the loading-dependent mesoscopic roughness but the morphology dependent microscopic roughness ( $\rho$ ) that affects the selectivity towards the solution reaction. In correspondence to our predicted length scales in Fig. 5(a), we do, however, see a loading dependence at very low loadings for the very small Cu-25nmP. Decreasing the loading progressively to 0.5 and 0.3  $\text{mg cm}^{-2}$  we find an increasing  $S_{\text{Ac}^-}^{\text{C}_2}$ . We hypothesize that, at such low loadings the overlap of diffusion lengths ( $L_d$ ) between particles decreases with loading since each particle has statistically fewer neighbors. This in turn noticeably lowers the effective surface area at the length scales relevant to the solution reaction, *i.e.* ketene has less (local) surface to re-adsorb, subsequently increasing  $S_{\text{Ac}^-}^{\text{C}_2}$ . At higher loadings the amount of neighbor particles saturates similar to a packing limit (leading to uniform selectivity with increasing loading). This particle size effect is very sensitive because we do not find any noticeable



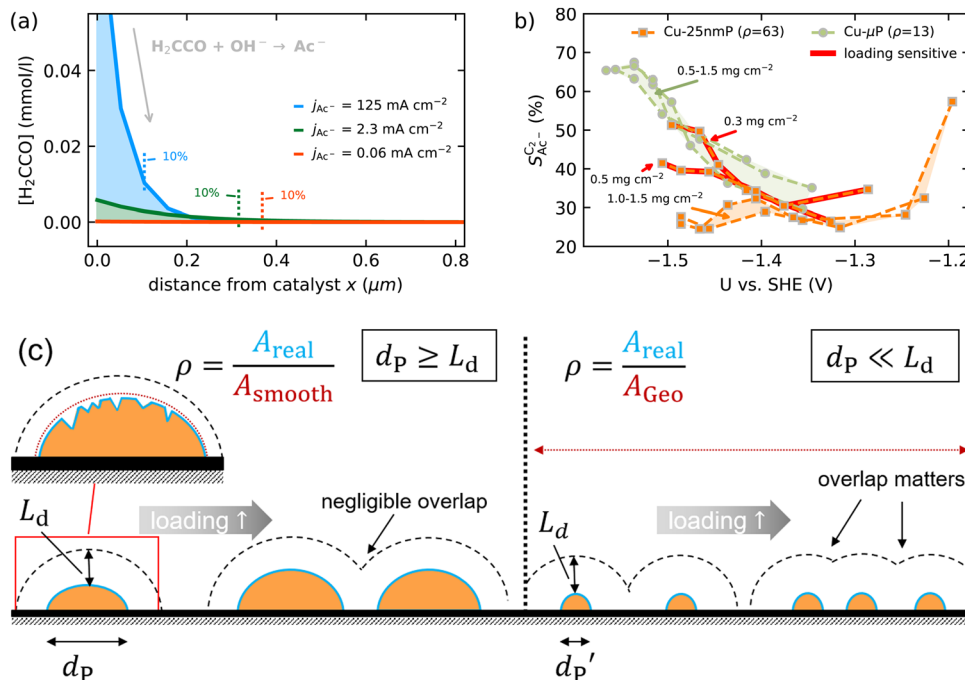


Fig. 5 (a) Concentration profile of ketene against distance from the catalyst indicating the length scales of its conversion to acetate as given by our mass transport model at different partial current densities for acetate. The vertical lines indicate the distance where 90% of ketene has reacted to acetate. (b) Acetate selectivity among all  $C_2$  products ( $S_{Ac}^{C_2}$ ) against  $U_{SHE}$  for experiments in a GDE with different loadings of Cu- $\mu$ P and Cu-25nmP. Each line represents an individual data set of the same reaction conditions. The shaded regions show the loading-independent selectivity ranges. The red highlighted lines are the loading dependent data found for the Cu-25nmP with small  $d_p$ . (c) Illustration of the effect of the diffusion length  $L_d$  in comparison to the particle diameter  $d_p$ , loading and the roughness  $\rho$  relevant to transport effects. At short  $L_d$  the overlap of diffusion spheres is negligible and only the local roughness matters (compared to a smooth particle surface). At long  $L_d$  diffusion spheres overlap and loading affects selectivity.

loading dependency for the slightly larger 40–60 nm sized Cu particles (Cu-50nmP) which are additionally shown in the ESI† (Section S1.4 and S1.5). From these particle sizes onward, the local surface area gained by particle overlap is negligible compared to the particles area at the solution reaction length scales (see Fig. 5(c)).

While our findings highlight the importance of the local, microscopic variations in the structure of the Cu catalysts, we emphasize that this relevance arises from the rapid solution reaction which leads to a very short diffusion length (compare Fig. 5). For intermediates that do not react in solution it has been shown in the ORR (for  $H_2O_2$ ) and methanol oxidation (for formaldehyde and formic acid) that the mesoscopic roughness (hence the loading) also influences their degree of re-adsorption and further reduction or oxidation, respectively.<sup>21</sup> This difference is due to the larger diffusion lengths expected for pure diffusion processes.

## 2.5 Considerations of alternative pathways

Since our mechanism in Fig. 2 is derived from DFT simulations, there may be inherent errors in the predicted energetics<sup>48</sup> and barriers and therefore uncertainties in the resultant pathways. Supporting our suggested mechanism, we discuss here why previously proposed<sup>11,12,14</sup> and other alternative pathways are unlikely from a theoretical analysis of the experimentally observed pH and potential dependence in the activity.

### 2.5.1 Acetate selectivity cannot be determined by a PCET.

The pH dependence of acetate in comparison to other  $C_2$  products is only possible with  $OH^-$  as a reactant in contrast to a recent study<sup>12</sup> which proposed an early PCET reaction as the SDS towards acetate. On a potential vs. SHE scale, PCET reactions in alkaline conditions, where water is a proton donor, are either pH independent<sup>49</sup> (where the RDS is the first PCET) or show a decrease in activity as pH increases (where the RDS is the 2nd or later PCET)<sup>38</sup> (also see the ESI,† Section S6). In contrast, as shown in Fig. 4, the activity for acetate increases with pH in relation to other  $C_2$  products. Since the  $C_2$  products do not depend on pH on an SHE scale<sup>1,38,50</sup> (or have even an apparent increasing activity with pH as visible in the upper panel of Fig. 4(b)) it follows that the SDS of acetate must in turn have an intrinsic pH dependence (which is greater than the apparent  $C_2$  one). This is only possible if  $OH^-$  is a reactant in the SDS, since the involvement of  $OH^-$  would lead to the necessary intrinsic pH dependence when involved in any reaction step prior to, coinciding with, or after the RDS.

**2.5.2 Acetate does not have an RDS separate from other major  $C_2$  products.** Our assumption of a shared RDS between acetate and other  $C_2$  products is the most likely scenario and has also been assumed in previous work.<sup>11,12,14</sup> As Fig. 1 shows, the total  $C_2$ 's, ethylene, ethanol, and acetate follow the same experimental trends: They share similar Tafel slopes (see ref. 11 and Fig. 1) and do not follow an otherwise distinguishing



inverse pH-activity relationship (see the ESI,† Section S6).<sup>38</sup> Furthermore, an alternative separate RDS of acetate would need to be a potential dependent reaction involving  $\text{OH}^-$  on the catalyst surface to yield the pH and potential dependence in acetate activity. This reaction step would, however, correspond to an oxidation reaction since  $\text{OH}^-$  would need to discharge.

**2.5.3 The SDS for acetate does not involve  $\text{OH}^-$  in a surface reaction.** Alternative to our suggested solution reaction, a hydrolysis on the catalyst surface has been suggested.<sup>11,14</sup> This reaction would imply a nucleophilic attack of  $\text{OH}^-$  occurring on the negatively charged surface onto  $\text{H}_2\text{CCO}^*$  (or another early intermediate). This step appears highly improbable due to electrostatic repulsion, the oxidative nature of the process and limited steric accessibility of the surface bound carbon atoms in those intermediates. Simulating this reaction for  $\text{H}_2\text{CCO}^*$ , we indeed find it associated with a high reaction barrier of  $\Delta G^\ddagger = 0.8$  eV and potential dependence which is inconsistent with the experimental behavior (see the ESI,† Section S3.2).

**2.5.4 The selectivity determining step(s) for acetate do not involve competing PCET vs. chemical reaction steps at high overpotentials.** Ref. 12 and 14 have, on the basis of reaction thermodynamics and barriers, suggested the selectivity towards acetate to be solely determined by the competition between a chemical surface reaction towards acetate vs. a PCET towards other  $\text{C}_2$  products. However, this mechanism is unlikely because the PCET step towards other  $\text{C}_2$  products would increase exponentially with increasing potential, which would result in negligible amounts of acetate, whose TOF would be potentially independent (compare potential dependence SDS-surf). In contrast, our proposed SDS-sol includes competition between  $\text{H}_2\text{CCO}$  re-adsorption and a solution reaction, where neither of these steps are PCET. This non-PCET dependence in SDS-sol compensates the potential dependence of the consecutive SDS-surf. The corresponding coupled transport-kinetic model (Fig. 4) shows significant selectivities for both acetate and  $\text{C}_2$ 's over a wide potential range consistent with experiments.

**2.5.5 A Cannizzaro-type reaction is less likely than ketene hydrolysis in solution phase.** The Cannizzaro reaction has been suggested as a possible source for acetate formation.<sup>51–53</sup> Since this solution-based disproportionation reaction of acetaldehyde to acetate and ethanol is also  $\text{OH}^-$  catalyzed, it would yield the same trends with pH and roughness as ketene hydrolysis. It would, however, also yield a 50:50 ratio of ethanol and acetate which is never found experimentally. Even if a substantial part of the additional ethanol would be oxidized to acetate at the anode,<sup>25,42</sup> a slightly increased ethanol yield with pH and roughness should still be expected. Experimentally, the opposite trend is found,<sup>11,12</sup> which renders this mechanism unlikely.

**2.5.6 Ketene hydrolysis in solution best explains the experimental observations.** The proposed solution reaction of ketene is in line with  $\text{C}^{18}\text{O}^4$  and  $\text{H}_2^{18}\text{O}^{52}$  isotope labeling experiments and a recent study where amines are co-fed to CORR.<sup>14</sup> For the latter, a competing solution reaction of ketene with  $\text{OH}^-$  or amines explains the studies selectivity trends with potential, pH, and amine identity.

**2.5.7 The proposed mechanism is not specific to the reaction conditions.** Our proposed mechanism and its implications are valid for both CORR and  $\text{CO}_2\text{RR}$ . However, the latter usually contains a reduced local pH due to the equilibrium of  $\text{CO}_2$  with bicarbonate<sup>4</sup> which gives rise to low acetate yields. A notable exception is highly alkaline electrolytes, e.g. 10 M KOH (pH  $\approx$  15) where high acetate yields are observed for the  $\text{CO}_2\text{RR}$ .<sup>13</sup> Similarly, high yields of acetate at high overpotentials are less often seen in H-cell experiments, since high current densities are not achievable which would lead to the necessarily high local pH values (pH  $\geq$  14–15, comparison in the ESI,† Fig. S16).

**2.5.8 The ketene pathway is most likely the main  $\text{C}_2$  pathway.** We assume in our computational model that all  $\text{C}_2$  products go through the ketene mechanism. This assumption is supported by acetate selectivities  $>80\%$  and direct FE competition between acetate and all other  $\text{C}_2$  products in the experiments of ref. 4 and 11 as shown in Fig. 4(b). Contrary to these observations, recent experiments at very negative potentials of  $<-1.9$  V<sub>SHE</sub> showed that acetate can be obtained as the sole liquid product, out-competing nearly all ethanol, while ethylene is less affected.<sup>12</sup> Our DFT simulations can also not provide a clear picture in that matter. An early bifurcation from the ketene pathway *via* the reduction of  $\text{HCCO}^*$  to  $\text{HCCOH}^*$  instead of  $\text{H}_2\text{CCO}(\text{aq})$  at very high overpotentials may be likely, but within the typical DFT error very uncertain (see the ESI,† Section S3.1). While most available data at low overpotentials or/and highly alkaline conditions<sup>4,8,11,14,31,42</sup> suggest that the ketene pathway is the main  $\text{C}_2$  pathway, we cannot exclude other pathways. However, the uncertainty about additional mechanisms does not affect the preceding arguments about selectivity since the contribution of any prior bifurcation must be small, given the overall high acetate yields.

### 3 Conclusion

In summary, we have presented a novel mechanism towards acetate in the  $\text{CO}_2\text{RR}$  based on the solution reaction of ketene which elucidates the dependence of its selectivity on potential, pH, and microscopic roughness. We gained this insight by analysis of the available GDE/flow cell and H-cell data, an experimental investigation of the effect of catalyst loading, and with the development of a multiscale model that predicts trends in selectivity vs. potential, pH, and roughness consistent with experiments. Our proposed mechanism dictates that acetate selectivity is determined by the transport and subsequent solution reaction of ketene vs. its (re-)adsorption and further reduction at the catalyst surface.

We emphasize that we have not invoked any special active site(s) towards acetate specific to the catalysts' morphology in our model; the effect of nanostructuring is captured by a single roughness parameter relevant at nm length scales consistent with experiments. The effect of roughness arises from its influence on the interplay between the transport and kinetics. Our examination of available ECSA-normalized data on





nanostructured Cu suggests that active site(s) remained to be the same across all types of Cu investigated thus far.

Based on our insight from the elaborated mechanism, we propose the following strategies to maximize or minimize acetate yields: Generally, a high pH, a low catalyst roughness, and very high ( $\geq -1.2 V_{\text{SHE}}$ ) or very low potentials ( $\leq -1.5 V_{\text{SHE}}$ ) maximize the acetate yield. For the highest acetate yield, the reaction should occur at low potentials and/or under very alkaline CORR conditions, similar to those exploited in recent work.<sup>11,12,42</sup> In contrast, a low acetate selectivity follows an operation of a very rough catalyst under neutral conditions using a buffer and intermediate potentials ( $-1.6$  to  $-1.3 V_{\text{SHE}}$ ).

The presented mechanism rationalizes the trends in acetate selectivity based on the transport of stable intermediates/products. We note that a similar transport related process may also be relevant for other stable intermediates in the  $\text{CO}_{(2)}\text{RR}$  like CO and acetaldehyde as also suggested by operando mass spectrometry experiments.<sup>53,54</sup> This work highlights the importance of a rigorous evaluation of intrinsic catalyst activities and the potential impact of the interplay of reaction energetics, solution phase reactions, and mass transport in mechanistic studies of the  $\text{CO}_{(2)}\text{RR}$  and beyond. From a simulation perspective, the combination of these effects on multiple length scales requires rigorous multiscale models beyond usual approaches focusing only on the reaction energetics on the catalyst surface.

## 4 Methods

### 4.1 Electrode preparation

The experiments were conducted using commercial micron-sized Cu particles (Cu- $\mu\text{P}$ , Alfa Aesar) and 40–60 nm Cu particles (Cu-50nmP, Sigma-Aldrich) and 25 nm Cu particles (Cu-25nmP, Sigma-Aldrich) as a cathode with  $\text{NiFeO}_x$  as an anode. To prepare the cathode catalyst ink, 35 mg of copper powder was dispersed in 3 ml of isopropanol and 50  $\mu\text{l}$  of Nafion ionomer (5 wt% in  $\text{H}_2\text{O}$ , Fuel Cell Store). The ink was drop-casted onto Sigracet 39 BB GDL (Fuel Cell Store) to a loading of  $1.0 \text{ mg cm}^{-2}$  for the electrolyte pH test. For the loading test, the loading was varied from 0.3 to  $1.5 \text{ mg cm}^{-2}$ . The anode was prepared *via* an electrodeposition method on the cleaned nickel foam following a previous report.<sup>55</sup> The nickel and iron ions were deposited onto the cleaned nickel foam at a potential of  $-1.0 \text{ V vs. Ag/AgCl}$  for 5 minutes in a mixture solution of 3 mM  $\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  (Sigma-Aldrich) and  $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$  (Sigma-Aldrich). A platinum wire was used as a counter electrode in this preparation.

### 4.2 CO electrolysis

All CO electrolysis was performed in a three-channel flow cell. The dimensions of the channel were  $2 \text{ cm} \times 0.5 \text{ cm} \times 0.15 \text{ cm}$  with  $1 \text{ cm}^2$  geometric area of the electrode exposed to the electrolyte flow. The cathode and anode were separated by an anion exchange membrane (FAA-3-50, Fumatech) activated in 1 M KOH (99.98% metal basis, Alfa Aesar) overnight prior to the experiment. The CO was fed into the electrolyzer at a 10 sccm flow rate controlled using a mass flow controller. Aqueous KOH

solution was fed into each anolyte and catholyte chamber. The catholyte flow rate was set to  $0.6 \text{ ml min}^{-1}$  without circulation while the anolyte flow rate was set to  $1 \text{ ml min}^{-1}$  to facilitate oxygen flow generated from the oxygen evolution reaction at the anode. Each electrode had direct contact with the electrolyte as the electrolyte flowed. The cathode potential was measured using an external Hg/HgO reference electrode (4.24 M KOH, Koslow Scientific) and converted to the standard hydrogen electrode (SHE) scale with 100% iR correction  $E(\text{vs. SHE}) = E(\text{vs. Hg/HgO}) + 0.098 \text{ V} - \eta_{\text{iR}}$ . During the electrolysis, the gas products (*i.e.* hydrogen, ethylene and methane) were transferred through HaySep D and Molsieve 5 Å columns and identified/quantified with a thermal conductivity detector and a flame ionization detector on a Multiple Gas Analyzer no. 5 gas chromatography (SRI Instruments). The liquid products (*i.e.* acetate, ethanol and *n*-propanol) were collected from the outlet of the catholyte for 5 minutes at each potential and quantified by  $^1\text{H}$  NMR spectroscopy (Bruker AVIII 600 MHz NMR spectrometer) using 25 ppm dimethyl sulfoxide (Alfa Aesar) in  $\text{D}_2\text{O}$  (Sigma-Aldrich) as an internal standard.

### 4.3 Material characterization

The surface structure of the cathode catalysts was characterized using a Zeiss Auriga-60 scanning electron microscope (see Fig. S2, ESI†).

The roughness factors ( $R_f$ ) of different Cu catalysts were calculated by normalizing the double-layer capacitance ( $C_{\text{dl}}$ ) of each catalyst deposited onto carbon paper to that of reference Cu (Cu foil). Cu foil was polished with sandpaper then cleaned in 1 M HCl solution prior to measurement for removing surface oxide layers. Toray carbon paper (Fuel Cell Store) was used to deposit the catalyst layer in order to minimize the contribution of the microporous layer capacitance of Sigracet 39 BB GDL during the measurement.  $0.1 \text{ mg cm}^{-2}$  of Cu particles were loaded on Toray carbon paper. The measurement was performed in a 0.1 M  $\text{HClO}_4$ -filled H-cell separated by a Nafion membrane with constant inert gas flowing. Multiple scans of cyclic voltammetry at various scan rates ( $50$  to  $200 \text{ mV s}^{-1}$ ) were performed by scanning a non-Faradaic potential window of Cu ( $-0.2$  to  $-0.1 \text{ V vs. Ag/AgCl}$ ) using a platinum wire as a counter electrode and Ag/AgCl (Pine Research) reference electrode. Then,  $C_{\text{dl}}$  was obtained from the slope of the geometric current density measured *vs.* the scan rate. The roughness factor  $R_f$  was normalized with its loading giving  $\tilde{R}_f$ .

$$\tilde{R}_{f, \text{catalyst}} = \frac{C_{\text{dl, catalyst}}}{C_{\text{dl, Cu foil}}} \times \frac{1}{\text{reference loading } (0.1 \text{ mg cm}^{-2})} \quad (2)$$

### 4.4 DFT calculations

DFT calculations were conducted using the BEEF-vdW<sup>56</sup> exchange-correlation functional. All thermodynamics were computed with GPAW<sup>57,58</sup> where an electrochemical environment was mimicked using a hybrid explicit/implicit solvation scheme including a static water layer.<sup>41</sup> Our GPAW results compared well with the results obtained in QuantumEspresso<sup>59</sup> in combination with the self-consistent continuum solvation (SCCS) model.<sup>60</sup>



Electrochemical reaction thermodynamics were referenced *via* the computational hydrogen electrode (CHE).<sup>61</sup> We applied the corrections by Christensen *et al.* to mitigate systematic DFT errors.<sup>48</sup> Free energies were obtained following the ideal gas law for gas phase species and the harmonic oscillator model for adsorbates, respectively. All possible surface adsorbates were thoroughly sampled for their most stable adsorption site on each Cu facet using the package CatKit package.<sup>62</sup> From this, sampling intermediates prior to HCCO\* were selected for each reduction stage according to their thermodynamic stability which is also in line with established kinetic trends<sup>40</sup> (see the final path in Fig. S12, ESI†). The grand canonical PCET barriers were computed in alkaline conditions (H<sub>2</sub>O as the proton donor) using the Solvated Jellium Model (SJM)<sup>41,63</sup> including an explicit water layer. We note that the calculations of electrochemical barriers still bear some uncertainties,<sup>64,65</sup> so we cautiously take these results as tentative. However, we note that the calculation of alkaline PCET barriers in this work was only possible *via* the use of this grand canonical framework, due to spontaneous coadsorption of OH<sup>−</sup> in conventional transition state searches. For handling of atomic structures, geometry optimizations, vibration calculations and climbing-image nudged-elastic-band (CI-NEB)<sup>66</sup> calculations, the Atomic Simulation Environment (ASE) package<sup>67</sup> was used. For further details of DFT calculations, slab models and convergence criteria see the ESI,† Section S2.

#### 4.5 Coupled microkinetic and transport model

The microkinetic model was solved for its steady-state using an ODE solver available in the SciPy distribution.<sup>68</sup> Lateral interactions were ignored as they appear insensitive to the investigated mechanism (see the ESI,† Section S5.6.3). The mass transport followed a hierarchical multiscale model where the transport within a short diffusion length from the catalyst surface is solved *via* a 1-D model employing the electro-neutral Nernst-Planck equation<sup>43,69</sup> and outside of this diffusion length described by effective mass transport relations.<sup>44–46</sup> The transport of CO was assumed solely from the gaseous side and solved analytically with a short diffusion layer of 150 nm, necessary to achieve the high current densities (see Fig. 4). On the gaseous side the partial pressure of CO was assumed with 1 atm and its aqueous solubility by the Henry constant.<sup>70</sup> The transport of OH<sup>−</sup> and H<sub>2</sub>CCO and their solution reaction was numerically solved for a diffusion length of 1 μm. Based on available experimentally determined constants employed in the model (see the ESI,† Section S5.2), the solution reaction is completed within this diffusion length (see Fig. 5(a)). Beyond the diffusion layer of 1 μm conditions equivalent to the electrode/electrolyte interface are assumed where the OH<sup>−</sup> concentration is determined through a Sherwood relation describing the flow perpendicular to the catalyst surface.<sup>45,46</sup> The microkinetic and transport models are iteratively solved for the catalyst surface concentrations. More details about the transport coupled microkinetic model can be found in the ESI,† Section 5.

## Code & data availability

The code for the coupled microkinetic and transport model with all input data used in this work as well as the digitized data from Fig. 1 is available under the MIT License (<https://opensource.org/licenses/MIT>) and CC BY 4.0 (<https://creativecommons.org/licenses/by/4.0/>), respectively, in Zenodo (<https://doi.org/10.5281/zenodo.5013854>).

## Conflicts of interest

There are no conflicts of interest to declare.

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