

Cite this: *Chem. Sci.*, 2021, 12, 4139

All publication charges for this article have been paid for by the Royal Society of Chemistry

## Tandem catalyzing the hydrodeoxygenation of 5-hydroxymethylfurfural over a Ni<sub>3</sub>Fe intermetallic supported Pt single-atom site catalyst†

Ge Meng,<sup>‡a</sup> Kaiyue Ji,<sup>‡a</sup> Wei Zhang,<sup>‡b</sup> Yiran Kang,<sup>b</sup> Yu Wang,<sup>\*c</sup> Ping Zhang,<sup>‡d</sup> Yang-Gang Wang,<sup>‡b</sup> Jun Li,<sup>‡a</sup> Tingting Cui,<sup>a</sup> Xiaohui Sun,<sup>a</sup> Tianwei Tan,<sup>e</sup> Dingsheng Wang,<sup>‡\*a</sup> and Yadong Li<sup>‡a</sup>

Single-atom site catalysts (SACs) have been used in multitudinous reactions delivering ultrahigh atom utilization and enhanced performance, but it is challenging for one single atom site to catalyze an intricate tandem reaction needing different reactive sites. Herein, we report a robust SAC with dual reactive sites of isolated Pt single atoms and the Ni<sub>3</sub>Fe intermetallic support (Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC) for tandem catalyzing the hydrodeoxygenation of 5-hydroxymethylfurfural (5-HMF). It delivers a high catalytic performance with 99.0% 5-HMF conversion in 30 min and a 2, 5-dimethylfuran (DMF) yield of 98.1% in 90 min at a low reaction temperature of 160 °C, as well as good recyclability. These results place Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC among the most active catalysts for the 5-HMF hydrodeoxygenation reaction reported to date. Rational control experiments and first-principles calculations confirm that Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC can readily facilitate the hydrodeoxygenation reaction by a tandem mechanism, where the single Pt site accounts for C=O group hydrogenation and the Ni<sub>3</sub>Fe interface promotes the C–OH bond cleavage. This interfacial tandem catalysis over the Pt single-atom site and Ni<sub>3</sub>Fe IMC support may develop new opportunities for the rational structural design of SACs applied in other heterogeneous tandem reactions.

Received 31st October 2020  
Accepted 29th January 2021

DOI: 10.1039/d0sc05983h

rsc.li/chemical-science

## Introduction

Upgrading of renewable biomass and its derivatives to fuels and fine chemicals through green catalytic processes is an effective strategy to reduce our dependence on fossil fuels.<sup>1–7</sup> Among them, 2,5-dimethylfuran (DMF) has been regarded as an important biomass-derived “platform” chemical, which is widely applied in the perfume and pharmaceutical industries and as a promising alternative biofuel.<sup>8</sup> For DMF production, one of the most favorable approaches is the hydrodeoxygenation of biomass-derived 5-hydroxymethylfurfural (5-HMF), which is a typical tandem reaction involving the hydrogenation of the –CHO group and hydrogenolysis of –CH<sub>2</sub>OH

groups.<sup>8–12</sup> Numerous noble (Pt, Ru, Pd, *etc.*) and non-noble (Ni, Fe, Cu, Co, *etc.*) metal based catalysts have been designed to boost the reaction, and much progress has been made.<sup>8,13–17</sup> Nevertheless, it is still challenging for one catalyst to simultaneously have high reaction kinetics for both the hydrogenation and dehydroxylation processes, and thus achieve high reaction efficiency and DMF selectivity without side-reactions (furan ring hydrogenation, ring opening, condensation reactions, *etc.*).<sup>18–20</sup> Recently, single-atom site catalysts (SACs) have been of major interest in heterogeneous catalysis with high atom utilization and enhanced catalytic performance,<sup>21–38</sup> which provide a great opportunity for efficient catalyst exploration towards the 5-HMF hydrodeoxygenation reaction. However, when applying SACs to catalyze the intricate tandem reactions needing multiple steps and catalytic sites, theoretically it is difficult for one single-atom site to cover all the catalytic steps with high efficiencies simultaneously.

Tandem or synergistic catalysis, in which the reactants are simultaneously activated by judiciously designed two or more distinct active sites, has been developed as a powerful strategy to improve the efficiency and selectivity of numerous homogeneous and heterogeneous reactions that cannot be easily catalyzed by a single active species.<sup>39–45</sup> Thus, construction of multiple catalytic sites is a significant strategy to overcome the drawback of single reactive sites in SACs for multitudinous tandem reactions, such as dual single-atom site design.<sup>46–48</sup>

<sup>a</sup>Department of Chemistry, Tsinghua University, Beijing 100084, China. E-mail: wangdingsheng@mail.tsinghua.edu.cn

<sup>b</sup>Department of Chemistry, Southern University of Science and Technology, Shenzhen, Guangdong 518055, China. E-mail: wangyg@sustech.edu.cn

<sup>c</sup>Shanghai Synchrotron Radiation Facility, Shanghai Advanced Research Institute, Chinese Academy of Sciences, Shanghai 201204, China. E-mail: wangyu@sinap.ac.cn

<sup>d</sup>College of Civil Engineering & Mechanics, Xiangtan University, Xiangtan 411105, China

<sup>e</sup>Beijing Key Laboratory of Bioprocess, College of Life Science and Technology, Beijing University of Chemical Technology, Beijing 100029, China

† Electronic supplementary information (ESI) available: Experimental details and supplementary characterization. See DOI: 10.1039/d0sc05983h

‡ G. M., K. J., and W. Z. contributed equally.



Besides, one of the crucial endeavors should be developing functional support systems to introduce single atom/support tandem catalysis. Taking this concept to the reaction of 5-HMF hydrodeoxygenation to DMF, the rational choice of the single-atom species and the unique support is crucial to realize the tandem catalysis of sequential  $-\text{CHO}$  hydrogenation and  $-\text{CH}_2\text{OH}$  hydrogenolysis reactions. Currently, Ni-Fe bimetallic alloy catalysts have been demonstrated to have high selectivity in this reaction because of the oxyphilic Fe sites favoring the selective C-OH bond cleavage.<sup>8,49-51</sup> However, their hydrogenation abilities are still unsatisfactory compared to that of many noble metal catalysts. In contrast, noble Pt-based nanocatalysts have exhibited superior activity in the hydrogenation of C=O bonds, but are prone to break the C=C bonds or furan ring, resulting in a loss of DMF selectivity.<sup>52-54</sup> Recently, the single-atom design of Pt catalysts has been proved to be an effective strategy to tune their selectivity in hydrogenation reactions.<sup>55-58</sup> Inspired by the above facts, a unique Ni-Fe nanocrystalline supported Pt SAC can be an ideal model to tandem catalyze the 5-HMF hydrodeoxygenation to DMF, where the hydrogenation of the C=O group can mainly be catalyzed by the single-atom Pt site, and the C-OH bond rupture processes can occur on the Ni-Fe interface, and thus both the activity and selectivity would be guaranteed simultaneously.

Herein, to construct the Pt/Ni-Fe dual interface tandem catalyst, we develop a novel approach to accomplish synthesis of  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMC SACs derived from the  $\text{PtCl}_6^{2-}$  adsorbed ultrathin NiFe layered double hydroxide (NiFe-LDH) precursor. The  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMC sample exhibited remarkable 5-HMF hydrodeoxygenation activity (99.0% conversion within 30 min) and optimal selectivity (98.1% yield of DMF in 90 min) at a low reaction temperature of 160 °C, which is among the best results for DMF production from 5-HMF as reported in the literature. Moreover, in the sixth cycle, the  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMC catalyst still maintained robust reactivity, further indicating its great potential as a candidate for industrial applications. Subsequently, a series of catalytic control experiments and density functional theory (DFT) calculations indicated that the excellent reactivity of the  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMC SAC arises from the tandem catalysis over Pt and  $\text{Ni}_3\text{Fe}$  interfacial sites, where the single-atom Pt site lowers the hydrogenation energy barrier of the aldehyde group, and the  $\text{Ni}_3\text{Fe}$  interface accelerates the C-OH bond rupture process. Therefore, this work illustrates a successful paradigm for the rational design of SACs with multiple catalytic sites towards boosting the tandem hydrodeoxygenation reactions, which also shows potential application in other heterogeneous reactions.

## Results and discussion

$\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMC was synthesized by a LDH transformation method. Firstly,  $\text{PtCl}_6^{2-}$  adsorbed NiFe-LDHs (named  $\text{PtCl}_6^{2-}/\text{NiFe-LDHs}$ ) were prepared by a co-precipitation process. Then, a thermal reduction treatment was applied to transform  $\text{PtCl}_6^{2-}/\text{NiFe-LDHs}$  into  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMC. As revealed by the transmission electron microscopy (TEM) image and corresponding particle size histogram in Fig. S1a and b,<sup>†</sup> the

obtained  $\text{PtCl}_6^{2-}/\text{NiFe-LDHs}$  show an irregular nanosheet morphology with an average diameter of 27.4 nm and thickness of 2.3 nm. The X-ray diffraction (XRD) pattern (Fig. S1c<sup>†</sup>) of  $\text{PtCl}_6^{2-}/\text{NiFe-LDHs}$  presents the characteristic diffraction peaks of LDHs around 11.5°, 22.5°, 34.5° and 60°, which originate from the in-plane (003), (006), (100) and (110) reflections and confirm the formation of two-dimensional LDH nanosheets. After being reduced in a 5%  $\text{H}_2/\text{N}_2$  atmosphere at 300 °C,  $\text{PtCl}_6^{2-}/\text{NiFe-LDHs}$  were transformed into  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMC nanoparticles, as shown in Fig. S2.<sup>†</sup> For comparison,  $\text{Ni}_3\text{Fe}$  IMC was also prepared (Fig. S3<sup>†</sup>), which shows morphological similarity to the  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMC sample. As shown in Fig. 1a, the typical XRD patterns of  $\text{Ni}_3\text{Fe}$  and  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMC conform to the standard peaks of  $Pm\bar{3}m$  (221)  $\text{Ni}_3\text{Fe}$  (JCPDS file no. 38-0419), with a face-centered cubic (fcc) structure, where the eight vertices of an individual unit cell are occupied by Fe atoms, and the centers of the six faces bear Ni atoms. To further confirm the atomic-scale geometrical structure of the as-prepared  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMC, the atomic resolution aberration-corrected high-angle annular dark-field scanning TEM (AC-HAADF-STEM) image (Fig. 1b), high-resolution TEM (HRTEM) image (Fig. S4<sup>†</sup>) and the fast Fourier transform (FFT) pattern (Fig. 1c) of  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMC oriented along the [220] zone axis are presented. The AC-HAADF-STEM image exhibits an ordered crystalline atomic arrangement. The lattice spacings of 2.04 Å and 1.77 Å correspond to the (111) and (200) planes of  $Pm\bar{3}m$   $\text{Ni}_3\text{Fe}$ , respectively, as also characterized by HRTEM analysis. The FFT pattern reveals a simple cubic (sc) structure of  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMC, which agrees with the XRD result. Moreover, as shown in Fig. 1d, the ideal crystal structure model of  $\text{Ni}_3\text{Fe}$  along the [220] zone axis coincides exactly with the experimental STEM image (Fig. 1b), confirming the formation of  $\text{Ni}_3\text{Fe}$  IMC. As shown in the low-magnified HAADF-STEM image in Fig. 1e, no obvious brighter Pt nanoparticles can be observed. Energy-dispersive X-ray spectroscopy analysis (EDXA) (Fig. 1e and S5<sup>†</sup>) reveals that Pt, Fe and Ni elements are uniformly distributed. The Pt content in  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMC is 2.1 wt% as shown by inductively coupled plasma optical emission spectrometry (ICP-OES). This value is similar with the EDXA result (2.2 wt%, Table S1<sup>†</sup>), further indicating that Pt is homogeneously dispersed in the  $\text{Ni}_3\text{Fe}$  matrix. In another AC-HAADF-STEM image of  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMC (Fig. 1f) with a different observation direction, many isolated bright dots can be observed, demonstrating that the isolated Pt atoms are uniformly embedded in the surface of the  $\text{Ni}_3\text{Fe}$  IMC nanocrystals.

To further verify the electronic and geometrical structure of  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMCs, X-ray absorption spectrometric (XAS) studies at the Pt  $L_{3-}$  edge, Fe K-edge and Ni K-edge were conducted (Fig. 2). As shown in Fig. 2a, for Pt in  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMCs, the white line intensity, which reflect the Pt oxidation state, is lower than that of Pt foil, revealing the electron-richness of Pt atoms in  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMC compared to metallic  $\text{Pt}^0$ . This phenomenon demonstrates the electron transfer from Ni or Fe to Pt atoms due to the higher electronegativity of Pt (2.20) than Ni (1.91) and Fe (1.83). The electron transfer characteristics were further demonstrated by X-ray photoelectron spectroscopy (XPS) measurements. For comparison, Pt nanoparticles supported on



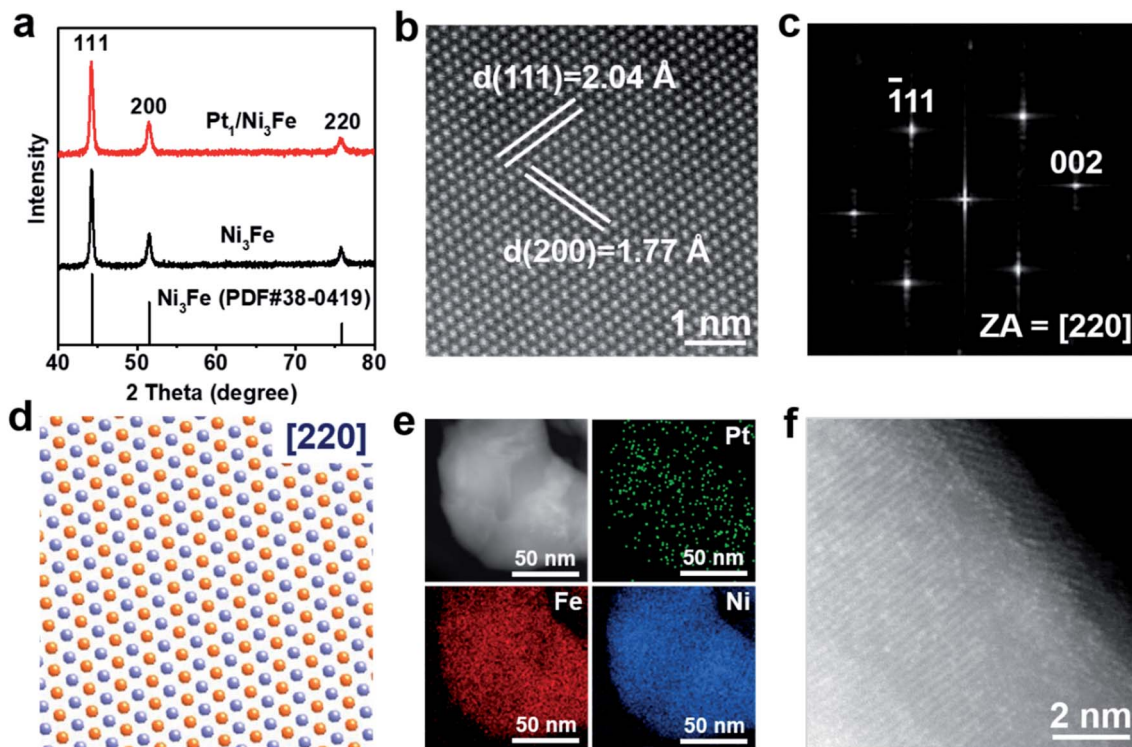


Fig. 1 Structural characterization of the Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC catalyst. (a) XRD patterns of Ni<sub>3</sub>Fe and Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC. Atomic resolution AC-HAADF-STEM image (b) and FFT pattern (c) of Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC nanocrystals oriented along the [220] zone axis. (d) Ideal crystal structure models along the [220] zone axis. Blue and orange spheres show Ni and Fe atoms, respectively. (e) HAADF-STEM image and the corresponding elemental maps, Pt (green), Fe (red), Ni and (blue), respectively. (f) AC-HAADF-STEM image of Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC.

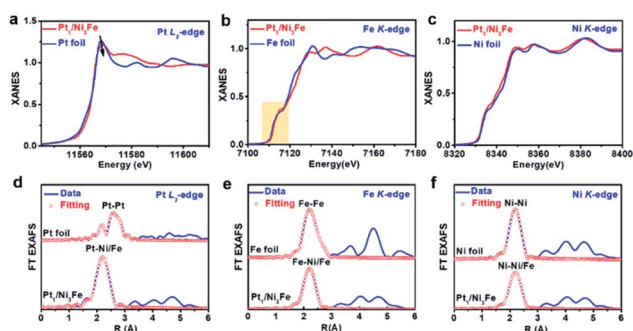


Fig. 2 X-ray absorption spectroscopy characterization of the Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC catalyst. Pt L<sub>3</sub>-edge (a), Fe K-edge (b) and Ni K-edge (c) XANES profiles of Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC as well as the reference samples. The Fourier transform (FT) of Pt L<sub>3</sub>-edge (d), Fe K-edge (e) and Ni K-edge (f) EXAFS spectra and fitting curves of the samples. The plots are not corrected for phase shift.

Ni<sub>3</sub>Fe IMC (noted as Pt NPs/Ni<sub>3</sub>Fe IMC; Pt content of 2.23 wt%) were also prepared and characterised (Fig. S6–S8<sup>†</sup>). As shown in Fig. S9<sup>†</sup>, the Pt 4f peaks of Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC show slightly lower binding energies than Pt NPs/Ni<sub>3</sub>Fe IMC with characteristic peaks of metallic Pt (Pt<sup>0</sup>), indicating the electronegative feature of Pt atoms in Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC. Pt isolated single atoms in Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC were identified from the EXAFS spectra and the theoretical fitting results (Fig. 2d, Table S2<sup>†</sup>), and only the Pt–Ni/Fe shell at  $\sim 2.2$  Å was observed without any contribution

from Pt–Pt scattering paths ( $\sim 2.6$  Å) compared with Pt foil. This reveals that the Pt atoms are isolated and no aggregations exist in Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC. Specially, the fitting results show that the coordination number (CN) of Pt–Ni/Fe in Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC is  $\sim 10.6$ . The unsaturated coordination of the Pt site testifies the enriched Pt element on the surface, agreeing well with the XPS result (Table S1<sup>†</sup>) that the Pt content on the surface of Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC (5.12 wt%) is much higher than the total content observed from ICP-OES (2.1 wt%) and EDXA (2.2 wt%). The single-atom Pt structure was further demonstrated by wavelet transform (WT) analysis of Pt L<sub>3</sub>-edge EXAFS as shown in Fig. S10<sup>†</sup>. Compared to the WT contour plots of Pt foil (Fig. S10a<sup>†</sup>), the intensity maximum of Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC (Fig. S10b<sup>†</sup>) arises at  $\sim 8.0$  Å<sup>-1</sup> from the contribution of the Pt–Ni/Fe path and no intensity maximum of the Pt–Pt path ( $\sim 10.8$  Å<sup>-1</sup>) is detected. Evidenced by AC-HAADF-STEM, XANES, EXAFS and WT analysis, we can draw a conclusion that Pt atoms are isolated, dispersed in Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMCs and stabilized by Pt–Ni/Fe bonds with a feature of electron-richness (Pt<sup>δ-</sup>).

Fig. 2b shows the normalized Fe K-edge XANES spectra of Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC and Fe foil, in which Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC exhibits a similar near-edge absorption energy compared to Fe foil, revealing the metallic state of Fe atoms in Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC. Specifically, from the Fe K-edge EXAFS spectra and the curve fitting results (Fig. 2e and Table S3<sup>†</sup>), it can be found that the Fe atoms in Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC are present in an fcc packing form with a CN of  $10.7 \pm 2.1$ , rather than the body-centered cubic (bcc)



structure as Fe foil. Besides, the intensity enhancement and location shift (from  $\sim 7.9$  to  $\sim 8.2 \text{ \AA}^{-1}$ ) in the K-edge WT contour plots of Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMCs (Fig. S11<sup>†</sup>) compared to that of Fe foil also demonstrate the coordination environment difference of Fe atoms in these two samples. These results conform to the XRD and AC-HAADF-STEM analysis that the intermetallic structure of fcc Ni<sub>3</sub>Fe was formed without the existence of Fe clusters or nanoparticles. For the Ni K-edge, XANES (Fig. 2c), EXAFS oscillations (Fig. 2f and Table S4<sup>†</sup>) and WT analysis (Fig. S12<sup>†</sup>) of Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMCs are very similar to those of Ni foil, indicating the metallic and fcc structure of Ni in Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC. The smaller CN of 10.1 for Ni in Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC than Ni foil can be attributed to the finite size effect. All these results agree well with the XRD, AC-HAADF-STEM and HRTEM analysis as discussed above.

Typically, as depicted in Fig. 3a, the tandem hydrodeoxygenation of 5-HMF to DMF can occur through two reaction pathways.<sup>10,15</sup> For one pathway (Path 1), 2,5-di(hydroxymethyl)furan (DHMF) appears as the primary product through the hydrogenation of the formyl group (–CHO) in 5-HMF. For Path 2, 5-HMF is firstly converted to methyl furfural (MFF) by the hydrogenolysis of the hydroxyl group. Both of them are then followed by further hydrogenation or hydrogenolysis processes and DMF can be obtained. The

hydrodeoxygenation reaction catalyzed by the Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC sample was firstly investigated at a temperature of 160 °C and H<sub>2</sub> pressure of 1.0 MPa. As shown in Fig. 3b and Table S5,<sup>†</sup> Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC exhibited an extraordinary catalytic performance, in which 99.0% conversion of 5-HMF was achieved within 30 min and the DMF yield reached 98.1% after 90 min. As shown in Table S6,<sup>†</sup> the lower reaction temperature, higher reaction rate and DMF selectivity, and low noble metal consumption of Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC make it one of the best catalysts compared to the results reported in the literature. In addition, during the whole reaction process, except for DMF, the intermediates of DHMF, 2-methyl-5-hydroxymethylfuran (MFA) and trace amounts of MFF, no signs of other compounds were observed. These results reveal the superior effectiveness of Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC for the fast and highly selective hydrodeoxygenation of the oxygenic group (–CHO, –OH) in 5-HMF, without C=C group hydrogenation or furan-ring-opening reactions. Moreover, it is also suggested that the hydrodeoxygenation reaction mainly follows Path 1 on the Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC catalyst. To further evaluate its cycling stability, the reaction was recycled six times (160 °C/2 h), and both the 5-HMF conversion and DMF yield remained at >99% (Fig. 3c). After the sixth cycle, the spent Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC catalyst was fully characterized (Fig. S13–S17<sup>†</sup>) and the results reveal that the morphology and intermetallic structure were well preserved and the Pt atoms were maintained atomically dispersed, indicating the outstanding structural stability of the Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC catalyst.

Subsequently, to understand the roles of the Pt single-atom site and Ni<sub>3</sub>Fe interface in the Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC catalyst for the hydrodeoxygenation reaction, a series of control experiments were performed. Accordingly, the reaction was firstly carried out over Pt NPs/Ni<sub>3</sub>Fe IMC. It is worth noting that, Fig. 3d, after 120 min of reaction, the conversion of 5-HMF attained 90.9%, wherein the corresponding DMF yield was 51.1% and remaining products distributed over MFA (19.9%), DHMF (7.1%) and some by-products ( $\sim 12.0\%$ ). Such inferior performance on Pt NPs/Ni<sub>3</sub>Fe IMC demonstrates that the Pt nanoparticle surface suffers from poor reactivity and selectivity sparking an assortment of side reactions (furan ring hydrogenation, ring-opening reactions, *etc.*), which conforms to previous reports.<sup>8,52,59</sup> To further confirm the catalytic behavior of Pt single-atom sites, the Pt<sub>1</sub>/NiFe-LDHs SAC with the catalytically inactive NiFe-LDHs as the support was also synthesized and tested. The structure of Pt<sub>1</sub>/NiFe-LDHs was well characterized as shown in Fig. S18–S21<sup>†</sup> and the Pt content in Pt<sub>1</sub>/NiFe-LDHs is 1.3 wt% as determined by ICP-OES. As shown in Fig. S22,<sup>†</sup> Pt<sub>1</sub>/NiFe-LDHs exhibit obvious activity for 5-HMF hydrogenation to DHMF, with a 5-HMF conversion of 50.8% and DHMF yield of 42.4% after 2 h of reaction. However, this catalyst exhibits extremely weak activity for the hydrogenolysis of –OH groups with only trace DMF and other intermediate products presented. These results demonstrate that, compared to Pt nanoparticles, the single-atom design of Pt catalysts can suppress their catalytic activity for furan ring hydrogenation and ring-opening side reactions to a large extent, with specificity in high –C=O hydrogenation ability but low –OH hydrogenolysis capacity. Thus, it can be inferred that the Pt single-atom site in the Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC

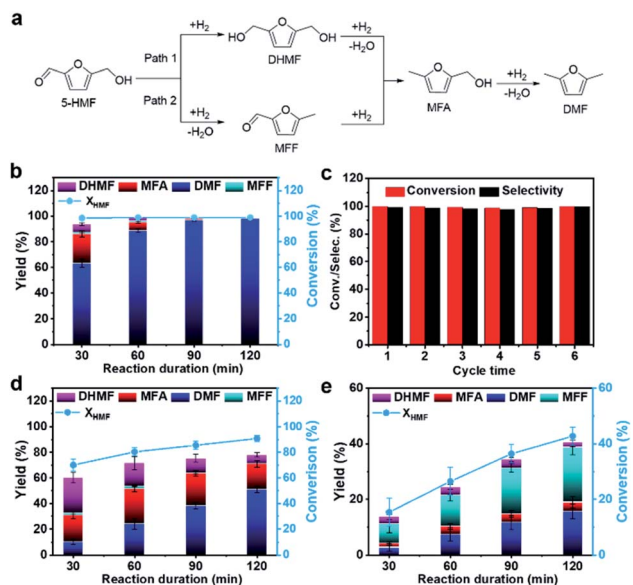


Fig. 3 Performance evaluation for the hydrodeoxygenation reaction over different catalysts. (a) Schematic paths for the conversion of 5-HMF to DMF. (b) 5-HMF conversion and product yields as a function of reaction time over Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC with the 5-HMF/Pt molar ratio of 100/1. (c) 5-HMF conversion and DMF selectivity as a function of catalytic cycles (run time: 2 h). 5-HMF conversion and product yields as a function of reaction time over Pt NPs/Ni<sub>3</sub>Fe IMC (d) and Ni<sub>3</sub>Fe IMC (e). Reaction conditions: All reactions were run at 160 °C and 1.0 MPa H<sub>2</sub>. The loading of 5-HMF was 0.5 wt% in 60 ml THF solvent. The catalyst dosage was introduced according to the 5-HMF/Pt molar ratio of 100/1 for Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC (196.0 mg) and Pt NPs/Ni<sub>3</sub>Fe IMC (184.6 mg). The mass dosage of Ni<sub>3</sub>Fe IMC (196.0 mg) was the same as that of Pt<sub>1</sub>/Ni<sub>3</sub>Fe IMC for comparison. All the error bars were evaluated from >3 times of independent measurements.



catalyst can take responsibility for the  $-C=O$  group hydrogenation in the 5-HMF hydrodeoxygenation reaction. To study the role of the  $Ni_3Fe$  interface in the hydrodeoxygenation catalysis, the catalytic behavior of the  $Ni_3Fe$  IMC sample was also studied. As presented in Fig. 3e, after 120 min of reaction, the conversion of 5-HMF reaches only 42.8% and gives a poor DMF yield of 15.7%, indicating the slow kinetics of the hydrodeoxygenation reaction over the pure  $Ni_3Fe$  IMC surface. More importantly, the MFF intermediate with a high yield of 19.8% was detected, which reveals that C–OH dehydroxylation is preferred over hydrogenation of the  $-C=O$  group in 5-HMF on the  $Ni_3Fe$  IMC catalyst (Path 2). Therefore, we can infer that the  $Ni_3Fe$  interface in the  $Pt_1/Ni_3Fe$  IMC catalyst mainly accounts for the dehydroxylation of  $-OH$  groups in the reaction of 5-HMF hydrodeoxygenation. The raw data of GC-MS analysis of Pt NPs/ $Ni_3Fe$  IMC,  $Pt_1/NiFe$ -LDHs and  $Ni_3Fe$  IMC in 120 min reaction duration are provided in Fig. S23–S25.† Summarizing the catalytic results (Table S5†) elucidates that the excellent performance of  $Pt_1/Ni_3Fe$  IMC for the 5-HMF hydrodeoxygenation reaction can arise from tandem catalysis over Pt and  $Ni_3Fe$  interfacial sites, where the  $-C=O$  group in 5-HMF was firstly hydrogenated to DHMF on single Pt sites, and then, the C–OH bonds of DHMF ruptured on the  $Ni_3Fe$  interface to form DMF.

To further understand the tandem catalysis process and the excellent activity of the  $Pt_1/Ni_3Fe$  IMC catalyst, we performed DFT calculations to explore the hydrodeoxygenation mechanisms on different substrates including Pt,  $Ni_3Fe$  IMC and  $Pt_1/Ni_3Fe$  IMC surfaces. The calculated reaction pathways as well as reaction energetics are shown in Fig. 4, and the corresponding reaction equations are shown in Scheme S1.† For the hydrogenation process, the hydrogen atom is considered to be located at the adjacent site to the carbonyl group. Recent studies have

also suggested that on Nickel and Platinum catalysts the furyl ring of the furanic derivatives can strongly interact with the metal d orbitals and the carbonyl group mostly interacts with the pre-adsorbed hydrogen.<sup>60–62</sup> Generally, the conversion of 5-HMF to DMF can be divided into two tandem parts: the first is the hydrogenation of 5-HMF to DHMF; and the second is the hydrogenolysis of DHMF to DMF. On a pure Pt catalyst, the rate-limiting steps are found to be the dehydroxylation of DHMF (vi  $\rightarrow$  vii) and MFA (xii  $\rightarrow$  xiii). The calculated barriers (TS-a and TS-b, as marked in green areas) are 1.79 eV and 2.20 eV, respectively, which indicates that the dehydroxylation of DHMF and MFA is kinetically unfavorable over the pure Pt surface. However, the low hydrogenation barriers (TS-1 = 0.52 eV and TS-2 = 0.54 eV) have suggested that the Pt catalyst should exhibit high hydrogenation performance, which agrees well with previous observations.<sup>59,63</sup> In contrast, we find that on the  $Ni_3Fe$  catalyst the rate-limiting step is the first hydrogenation step of 5-HMF (iii  $\rightarrow$  iv) with a high barrier of 1.25 eV (TS-1, as marked in blue area), suggesting the difficult conversion of 5-HMF to DHMF. However, for the selective cleavage of the C–OH bond, the  $Ni_3Fe$  catalyst shows very low barriers of 0.73 eV and 0.93 eV for TS-a and TS-b, respectively.

Comparing Pt and  $Ni_3Fe$  catalysts, we can find that the former is effective for the hydrogenation step and the latter is significant for the dehydroxylation step. Without surprise,  $Pt_1/Ni_3Fe$ , which combines Pt and  $Ni_3Fe$  catalysts, shows significantly improved catalytic performance for the hydrodeoxygenation of 5-HMF. The barrier for the first hydrogenation step on  $Pt_1/Ni_3Fe$  decreases from 1.25 eV to 0.55 eV compared to that of  $Ni_3Fe$ , and the barrier for the dehydroxylation of MFA decreases from 2.20 eV to 0.64 eV compared to that of Pt. The configurations for the first hydrogenation of 5-HMF and the

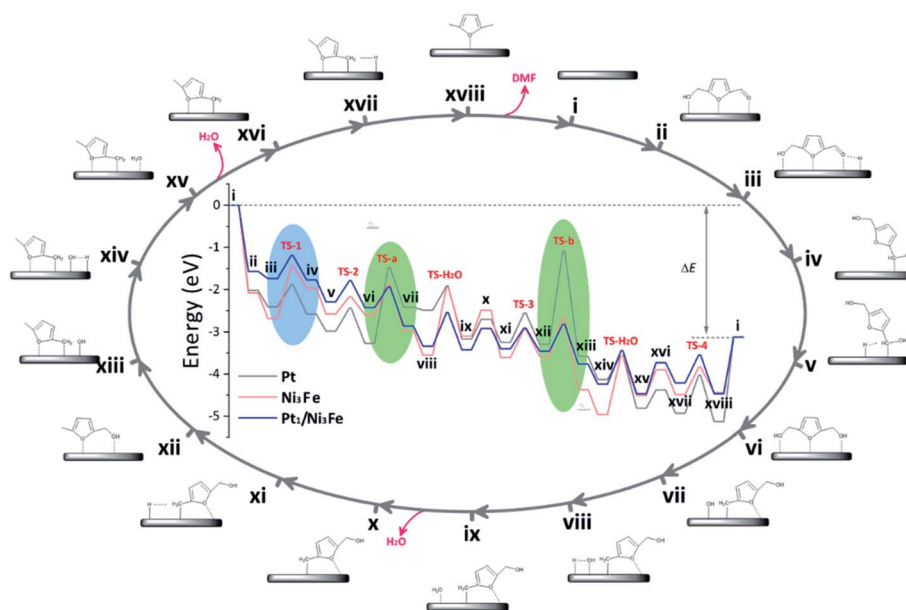


Fig. 4 Calculated reaction pathways for the hydrodeoxygenation of 5-HMF to DMF over Pt,  $Ni_3Fe$  and  $Pt_1/Ni_3Fe$  catalysts. The elementary steps were numbered with i–xviii; “TS-1”, “TS-2”, “TS-3” and “TS-4” represent the transition states of the hydrogenation steps, “TS-a” and “TS-b” represent the transition states of dehydroxylation steps, and “TS- $H_2O$ ” denotes the transition state of water formation.



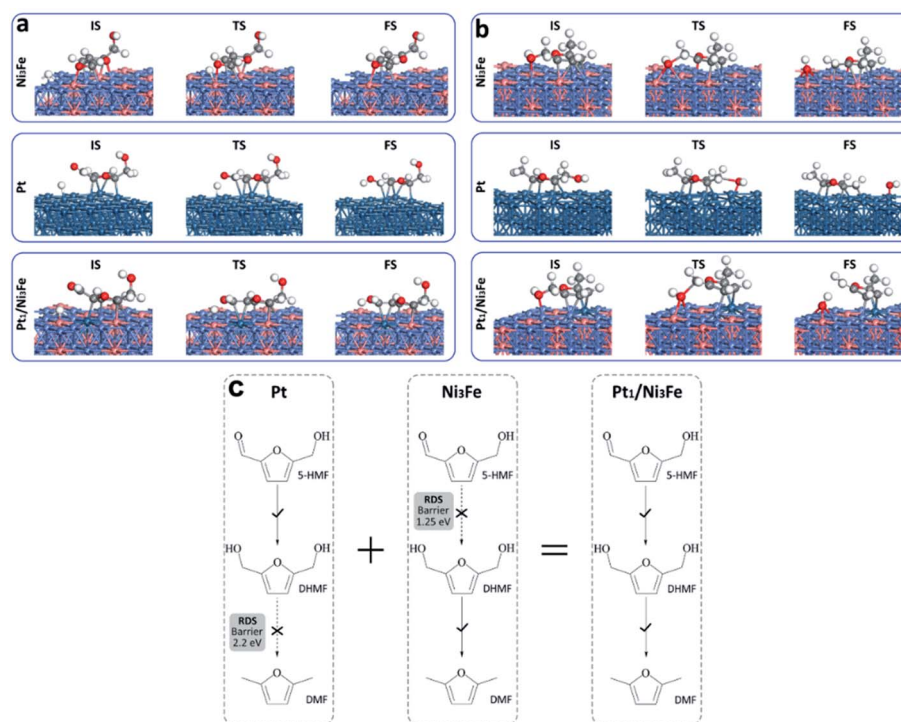


Fig. 5 The tandem mechanism of Pt and the  $\text{Ni}_3\text{Fe}$  interface. Optimized structures of reaction intermediates for the first hydrogenation step (a) and the dehydroxylation of MFA (b) over Pt,  $\text{Ni}_3\text{Fe}$  and the  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  surface. (c) Tandem mechanism on  $\text{Pt}_1/\text{Ni}_3\text{Fe}$ , combining the catalytic performance of both Pt and  $\text{Ni}_3\text{Fe}$  catalysts. The light blue, orange, blue, grey, red and white spheres represent Ni, Fe, Pt, C, O and H atoms, respectively.

dehydroxylation of DHMF on each catalyst are also shown in Fig. 5a and b. It is demonstrated that the aldehyde group on  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  directly correlates with the single Pt sites, which accounts for the high activity for the hydrogenation step. For the dehydroxylation of DHMF, the cleavage of C–OH occurs at the  $\text{Ni}_3\text{Fe}$  interface and the produced hydroxyl exhibits a strong interaction with the Fe site. This is confirmed by the cleavage energies of the C–OH bond ( $-0.36$  eV on  $\text{Ni}_3\text{Fe}$  vs.  $0.85$  eV on Pt). Our results suggest that the prepared  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMC has combined the advantages of Pt and  $\text{Ni}_3\text{Fe}$  catalysts and the tandem mechanism results in the high catalytic reactivity for the hydrodeoxygenation of 5-HMF, as schematically shown in Fig. 5c.

## Conclusions

In summary, a  $\text{Ni}_3\text{Fe}$  intermetallic compound supported Pt single-atom site catalyst ( $\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMC) was designed through an efficient LDH transformation strategy for tandem catalyzing the hydrodeoxygenation of 5-HMF to DMF, where the aldehyde hydrogenation and C–OH bond cleavage processes can be respectively promoted by the single-atom Pt site and  $\text{Ni}_3\text{Fe}$  interface. Therefore, it delivered a robust catalytic performance with a 99.0% conversion of 5-HMF in 30 min and a DMF yield of 98.1% within 90 min at  $160^\circ\text{C}$ , as well as an excellent cycling stability. Experimental and DFT calculation studies support our hypothesis that the tandem catalysis over Pt and  $\text{Ni}_3\text{Fe}$  interfacial sites accounts for the excellent reactivity of  $\text{Pt}_1/\text{Ni}_3\text{Fe}$  IMC

SACs in the hydrodeoxygenation reaction, in which the single-atom Pt site accelerates the hydrogenation of the aldehyde group, and the  $\text{Ni}_3\text{Fe}$  interface facilitates the C–OH bond cleavage. These results provide not only an efficient synthetic strategy for a new type of IMC supported SAC, but also guidelines for the tandem catalysis design of SACs by constructing functional support systems for numerous intricate tandem reactions.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

This work was supported by the National Key R&D Program of China (2018YFA0702003), National Natural Science Foundation of China (21890383, and 21871159), Science and Technology Key Project of Guangdong Province of China (2020B010188002) and Beijing Municipal Science & Technology Commission No. Z191100007219003. We thank the BL14W1 station in the Shanghai Synchrotron Radiation Facility (SSRF) for use of the instruments. W. Z. and Y. G. W. were financially supported by NSFC (22022504, and 22003022) of China, the Guangdong “Pearl River” Talent Plan (2019QN01L353), and the Guangdong Provincial Key Laboratory of Catalysis (2020B121201002). The computational resource was provided by the Center for Computational Science and Engineering at SUSTech.



## Notes and references

- G. W. Huber, S. Iborra and A. Corma, *Chem. Rev.*, 2006, **106**, 4044–4098.
- C. Li, X. Zhao, A. Wang, G. W. Huber and T. Zhang, *Chem. Rev.*, 2015, **115**, 11559–11624.
- C. Mondelli, G. Gözaydın, N. Yan and J. Pérez-Ramírez, *Chem. Soc. Rev.*, 2020, **49**, 3764–3782.
- P. Sudarsanam, R. Zhong, S. V. D. Bosch, S. M. Coman, V. I. Parvulescu and B. F. Sels, *Chem. Soc. Rev.*, 2018, **47**, 8349–8402.
- Y. Deng, R. Gao, L. Lin, T. Liu, X.-D. Wen, S. Wang and D. Ma, *J. Am. Chem. Soc.*, 2018, **140**, 14481–14489.
- A. J. Ragauskas, C. K. Williams, B. H. Davison, G. J. P. Britovsek, J. Cairney, C. A. Eckert, W. J. Frederick, J. P. Hallett, D. J. Leak, C. L. Liotta, J. R. Mielenz, R. J. Murphy, R. H. Templer and T. J. Tschaplinski, *Science*, 2006, **311**, 484–489.
- N. Brun, P. Hesemann and D. Esposito, *Chem. Sci.*, 2017, **8**, 4724–4738.
- S. Chen, R. Wojcieszak, F. Dumeignil, E. Marceau and S. Royer, *Chem. Rev.*, 2018, **118**, 11023–11117.
- C. Xu, E. Paone, D. Rodríguez-Padrón, R. Luque and F. Mauriello, *Chem. Soc. Rev.*, 2020, **49**, 4273–4306.
- J. Luo, H. Yun, A. V. Mironenko, K. A. Goulas, J. D. Lee, M. Monai, C. Wang, V. Vorotnikov, C. B. Murray, D. G. Vlachos, P. Fornasiero and R. J. Gorte, *ACS Catal.*, 2016, **6**, 4095–4104.
- S. Kim, E. E. Kwon, Y. T. Kim, S. Jung, H. J. Kim, G. W. Huber and J. Lee, *Green Chem.*, 2019, **21**, 3715–3743.
- Y. Roman-Leshkov, C. J. Barrett, Z. Y. Liu and J. A. Dumesic, *Nature*, 2007, **447**, 982–985.
- J. B. Binder and R. T. Raines, *J. Am. Chem. Soc.*, 2009, **131**, 1979–1985.
- Q. Wang, J. Feng, L. Zheng, B. Wang, R. Bi, Y. He, H. Liu and D. Li, *ACS Catal.*, 2020, **10**, 1353–1365.
- J. M. R. Gallo, D. M. Alonso, M. A. Mellmer and J. A. Dumesic, *Green Chem.*, 2013, **15**, 85–90.
- G. Wang, J. Hilgert, F. Richter, F. Wang, H. Bongard, B. Spliethoff, C. Weidenthaler and F. Schuth, *Nat. Mater.*, 2014, **13**, 293–300.
- T. Thananathanachon and T. B. Rauchfuss, *Angew. Chem., Int. Ed.*, 2010, **49**, 6616–6618.
- J. Chen, R. Liu, Y. Guo, L. Chen and H. Gao, *ACS Catal.*, 2014, **5**, 722–733.
- M. E. Zakrzewska, E. Bogel-Lukasik and R. Bogel-Lukasik, *Chem. Rev.*, 2011, **111**, 397–417.
- X. Kong, Y. Zhu, Z. Fang, J. A. Kozinski, I. S. Butler, L. Xu, H. Song and X. Wei, *Green Chem.*, 2018, **20**, 3657–3682.
- A. Wang, J. Li and T. Zhang, *Nat. Rev. Chem.*, 2018, **2**, 65–81.
- H. Fei, J. Dong, D. Chen, T. Hu, X. Duan, I. Shakir, Y. Huang and X. Duan, *Chem. Soc. Rev.*, 2019, **48**, 5207–5241.
- R. T. Hannagan, G. Giannakakis, M. Flytzani-Stephanopoulos and E. C. H. Sykes, *Chem. Rev.*, 2020, **120**, 12044–12088.
- N. Zhang, C. Ye, H. Yan, L. Li, H. He, D. Wang and Y. Li, *Nano Res.*, 2020, **13**, 3165–3182.
- L. Liu and A. Corma, *Chem. Rev.*, 2018, **118**, 4981–5079.
- Z. Zhuang, Q. Kang, D. Wang and Y. Li, *Nano Res.*, 2020, **13**, 1856–1866.
- Z. Wang, S. M. Xu, Y. Xu, L. Tan, X. Wang, Y. Zhao, H. Duan and Y. F. Song, *Chem. Sci.*, 2019, **10**, 378–384.
- T. Sun, L. Xu, D. Wang and Y. Li, *Nano Res.*, 2019, **12**, 2067–2080.
- J. Jones, H. Xiong, A. Delariva, E. J. Peterson, H. N. Pham, S. R. Challa, G. Qi, S. Oh, M. H. Wiebenga, X. I. P. Hernandez, Y. Wang and A. K. Datye, *Science*, 2016, **353**, 150–154.
- X. Li, H. Rong, J. Zhang, D. Wang and Y. Li, *Nano Res.*, 2020, **13**, 1842–1855.
- B. Lee, S. Park, M. Kim, A. K. Sinha, S. C. Lee, E. Jung, W. J. Chang, K. Lee, J. H. Kim, S. Cho, H. Kim, K. Nam and T. Hyeon, *Nat. Mater.*, 2019, **18**, 620–626.
- J. Yang, W. Li, D. Wang and Y. Li, *Small Struct.*, 2020, 2000051.
- S. Yang, J. Zhang, L. Peng, M. Asgari, D. Stoian, I. Kochetygov, W. Luo, E. Oveisi, O. Trukhina, A. H. Clark, D. T. Sun and W. L. Queen, *Chem. Sci.*, 2020, **11**, 10991–10997.
- J. Zhang, C. Zheng, M. Zhang, Y. Qiu, Q. Xu, W.-C. Cheong, W. Chen, L. Zheng, L. Gu, Z. Hu, D. Wang and Y. Li, *Nano Res.*, 2020, **13**, 3082–3087.
- L. Chen, K. Hou, Y. Liu, Z. Qi, Q. Zheng, Y. Lu, J. Chen, J. Chen, C. Pao, S. Wang, Y. Li, S. Xie, F. Liu, D. Prendergast, L. E. Klebanoff, V. Stavila, M. D. Allendorf, J. Guo, L. Zheng, J. Su and G. A. Somorjai, *J. Am. Chem. Soc.*, 2019, **141**, 17995–17999.
- S. Tian, M. Hu, Q. Xu, W. Gong, W. Chen, J. Yang, Y. Zhu, C. Chen, J. He, Q. Liu, H. Zhao, D. Wang and Y. Li, *Sci. China Mater.*, 2021, **64**, 642–650.
- H. Wei, Y. Ren, A. Wang, X. Liu, X. Liu, L. Zhang, S. Miao, L. Li, J. Liu, J. Wang, G. Wang, D. Su and T. Zhang, *Chem. Sci.*, 2017, **8**, 5126–5131.
- J. Yang, W. Li, D. Wang and Y. Li, *Adv. Mater.*, 2020, **32**, 2003300.
- Y. B. Huang, J. Liang, X. S. Wang and R. Cao, *Chem. Soc. Rev.*, 2017, **46**, 126–157.
- J. Su, C. Xie, C. Chen, Y. Yu, G. Kennedy, G. A. Somorjai and P. Yang, *J. Am. Chem. Soc.*, 2016, **138**, 11568–11574.
- X. Wang and R. Rinaldi, *Angew. Chem., Int. Ed.*, 2013, **52**, 11499–11503.
- M. Shiramizu and F. D. Toste, *Angew. Chem., Int. Ed.*, 2013, **52**, 12905–12909.
- Y. Yamada, C. Tsung, W. Huang, Z. Huo, S. E. Habas, T. Soejima, C. Aliaga, G. A. Somorjai and P. Yang, *Nat. Chem.*, 2011, **3**, 372–376.
- M. H. Beyzavi, N. A. Vermeulen, A. J. Howarth, S. Tussupbayev, A. B. League, N. M. Schweitzer, J. R. Gallagher, A. E. Plateroprats, N. Hafezi, A. A. Sarjeant, J. T. Miller, K. W. Chapman, J. F. Stoddart, C. J. Cramer, J. T. Hupp and O. K. Farha, *J. Am. Chem. Soc.*, 2015, **137**, 13624–13631.



- 45 X. Wu, F. A. Cruz, A. Lu and V. M. Dong, *J. Am. Chem. Soc.*, 2018, **140**, 10126–10130.
- 46 B. B. Sarma, J. Kim, J. Amsler, G. Agostini, C. Weidenthaler, N. Pfander, R. Arenal, P. Concepcion, P. Plessow, F. Studt and G. Prieto, *Angew. Chem., Int. Ed.*, 2020, **59**, 2–12.
- 47 Q. He, D. Liu, J. H. Lee, Y. Liu, Z. Xie, S. Hwang, S. Kattel, L. Song and J. G. Chen, *Angew. Chem., Int. Ed.*, 2020, **59**, 3033–3037.
- 48 J. Chen, H. Li, C. Fan, Q. Meng, Y. Tang, X. Qiu, G. Fu and T. Ma, *Adv. Mater.*, 2020, **32**, 2003134.
- 49 L. Yu, L. He, J. Chen, J. Zheng, L. Ye, H. Lin and Y. Yuan, *ChemCatChem*, 2015, **7**, 1701–1707.
- 50 C. Wang, J. Luo, V. Liao, J. D. Lee, T. M. Onn, C. B. Murray and R. J. Gorte, *Catal. Today*, 2018, **302**, 73–79.
- 51 S. Sitthisa, W. An and D. E. Resasco, *J. Catal.*, 2011, **284**, 90–101.
- 52 J. Luo, L. Arroyo-Ramírez, R. J. Gorte, D. Tzoulaki and D. G. Vlachos, *AIChE J.*, 2015, **61**, 590–597.
- 53 J. Shi, Y. Wang, X. Yu, W. Du and Z. Hou, *Fuel*, 2016, **163**, 74–79.
- 54 R. Goyal, B. Sarkar, A. Bag, N. Siddiqui, D. Dumbre, N. Lucas, S. K. Bhargava and A. Bordoloi, *J. Catal.*, 2016, **340**, 248–260.
- 55 Z. Zhang, Y. Zhu, H. Asakura, B. Zhang, J. Zhang, M. Zhou, Y. Han, T. Tanaka, A. Wang, T. Zhang and N. Yan, *Nat. Commun.*, 2017, **8**, 16100.
- 56 H. Wei, X. Liu, A. Wang, L. Zhang, B. Qiao, X. Yang, Y. Huang, S. Miao, J. Liu and T. Zhang, *Nat. Commun.*, 2014, **5**, 5634.
- 57 F. R. Lucci, J. Liu, M. D. Marcinkowski, M. Yang, L. F. Allard, M. Flytzanistephanopoulos and E. C. H. Sykes, *Nat. Commun.*, 2015, **6**, 8550.
- 58 B. Zhang, H. Asakura, J. Zhang, J. Zhang, S. De and N. Yan, *Angew. Chem., Int. Ed.*, 2016, **55**, 8319–8323.
- 59 M. Chatterjee, T. Ishizaka and H. Kawanami, *Green Chem.*, 2014, **16**, 4734–4739.
- 60 V. Vorotnikov, G. Mpourmpakis and D. G. Vlachos, *ACS Catal.*, 2012, **2**, 2496–2504.
- 61 Z. Jiang, W. Wan, Z. Lin, J. Xie and J. G. Chen, *ACS Catal.*, 2017, **7**, 5758–5765.
- 62 S. Tsatsos, S. Ladas and G. Kyriakou, *J. Phys. Chem. C*, 2020, **124**, 26268–26278.
- 63 H. Cai, C. Li, A. Wang and T. Zhang, *Catal. Today*, 2014, **234**, 59–65.

