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Efficacy analysis of compartmentalization for ambient CH_4 activation mediated by a Rh^{II} metalloradical in a nanowire array electrode†

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Compartmentalization is a viable approach for ensuring the turnover of a solution cascade reaction with ephemeral intermediates, which may otherwise deactivate in the bulk solution. In biochemistry or enzyme-relevant cascade reactions, extensive models have been constructed to quantitatively analyze the efficacy of compartmentalization. Nonetheless, the application of compartmentalization and its quantitative analysis in non-biochemical reactions is seldom performed, leaving much uncertainty about whether compartmentalization remains effective for non-biochemical reactions, such as organometallic, cascade reactions. Here, we report our exemplary efficacy analysis of compartmentalization in our previously reported cascade reaction for ambient CH_4-to-CH_3OH conversion, mediated by an O_2-deactivated Rh^{II} metalloradical with O_2 as the terminal oxidant in a Si nanowire array electrode. We experimentally identified and quantified the key reaction intermediates, including the Rh^{II} metalloradical and reactive oxygen species (ROS) from O_2. Based on such findings, we experimentally determined that the nanowire array enables about 81% of the generated ephemeral intermediate Rh^{II} metalloradical in air, to be utilized towards CH_3OH formation, which is 0% in a homogeneous solution. Such an experimentally determined value was satisfactorily consistent with the results from our semi-quantitative kinetic model. The consistency suggests that the reported CH_4-to-CH_3OH conversion surprisingly possesses minimal unforeseen side reactions, and is favorably efficient as a compartmentalized cascade reaction. Our quantitative evaluation of the reaction efficacy offers design insights and caveats into application of nanomaterials to achieve spatially controlled organometallic cascade reactions.

Introduction

Compartmentalization, ubiquitous in biology, allows efficient transfer of reaction intermediates or ephemeral species within a multienzyme cascade reaction in an intracellular medium.[1–3] By segregating subsequent catalytic sites from the bulk environment at the microscopic or even nanoscopic level, spatial control of catalytic reactions ensures the functionality of biological metabolism in a factory-like manner with high efficiency.[4–6] Here the key to a successful compartmentalized cascade reaction is the capability of confining a transient intermediate within the compartment and preventing its outflux that leads to either intermediate loss or deactivation

(Fig. 1A). A number of theoretical models have been established to evaluate the capability of compartmentalized cascade reactions in fulfilling this task,[7,8] predominantly in the context of enzymatic catalytic reactions.[9–13] Reaction efficiency (γ), defined as the ratio between the product outflux and the substrate influx to the compartment for a one-to-one stoichiometric reaction (Fig. 1A), quantitatively measures the efficacy of a cascade system in retaining and utilizing the intermediate species generated within the compartment.[6,9,14,15] With the value of γ commonly approaching unity for cascade reactions in biology,[4–6,14] nature masters the design strategy of compartmentalization for enzymatic reactions.
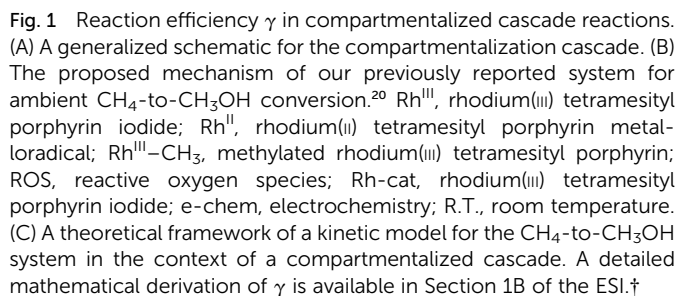
The benefits of confining catalytic reactions spatially at microscopic and nanoscopic levels in nature inspire the development of other non-enzymatic cascades, mostly with surface-attached molecular, nanoparticle, or enzyme catalysts in porous media such as metal–organic frameworks[16–18] or superposed on scaffolds.[10–12] Nonetheless, analyzing and determining the value of γ, a quantitative figure-of-merit for the efficacy of compartmentalization, remains infrequent, to say the least, for non-enzymatic scenarios. As reported in recent publications,[9,16,19] the scarcity of experimentally determined γ values

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Fig. 1 Reaction efficiency γ in compartmentalized cascade reactions. (A) A generalized schematic for the compartmentalization cascade. (B) The proposed mechanism of our previously reported system for ambient CH_4-to-CH_3OH conversion.[20] Rh^{III}, rhodium(III) tetramesityl porphyrin iodide; Rh^{II}, rhodium(II) tetramesityl porphyrin metalloradical; Rh^{III}–CH_3, methylated rhodium(III) tetramesityl porphyrin; ROS, reactive oxygen species; Rh-cat, rhodium(III) tetramesityl porphyrin iodide; e-chem, electrochemistry; R.T., room temperature. (C) A theoretical framework of a kinetic model for the CH_4-to-CH_3OH system in the context of a compartmentalized cascade. A detailed mathematical derivation of γ is available in Section 1B of the ESI.†

casts uncertainty about the effectiveness of a certain design strategy of compartmentalization. A synergistic study comparing experimentally determined γ values with the one from a theoretical model will offer valuable insights whether the designed cascade reaction is effective without undesirable side effects, ascertain the merits of designed compartmentalization, and further justify the design strategy of non-enzymatic compartmentalized systems. This research report aims to offer an exemplary case of such a study for organometallic catalysis with compartmentalized systems.

We are interested in employing microscopic concentration gradients within nanomaterials to design organometallic catalytic cycles of seemingly incompatible steps, in which key reaction intermediates will be quickly deactivated once they diffuse out of the nanomaterials. In our previous report,[20] a cascade catalysis with O_2-sensitive reaction intermediates was established to achieve ambient CH_4-to-CH_3OH conversion with O_2 as the terminal oxidant assisted by electricity. As shown in Fig. 1B, the nanowire array electrode electrochemically reduces rhodium(III) tetramesityl porphyrin iodide (Rh^{III}) into rhodium(II) tetramesityl porphyrin metalloradical (Rh^{II}) in aprotic solvent 1,2-difluorobenzene (1,2-DFB). At the same time, the nanowire array reduces O_2 into reactive oxygen species (ROS) and creates a sharp O_2 concentration gradient in a local O_2-free environment near the bottom of the nanowire array under aerobic conditions. In the O_2-free microenvironment, two equivalents of the generated Rh^{II} species, while highly reactive with O_2[21], activate one equivalent of CH_4 ambiently to yield methylated rhodium(III) tetramesityl porphyrin (Rh^{III}–CH_3) and rhodium(III) tetramesityl porphyrin hydride (Rh^{III}–H). Both

species are proposed to react with the generated ROS that remain to be further identified (vide infra), leading to the formation of CH_3OH. While no barrier is present to physically separate the liquid phase within the nanowire array from the bulk solution, the whole system can be considered to be a compartmentalized cascade with the nanowire array as the compartment with its unique microenvironment (Fig. 1C), analogous to the previous argument in the case of two-enzyme cascades in which enzymes are placed in close proximity at the nano-scale.[12,22] The overall process was reported to be catalytic, achieving a turnover number up to 52 000 within 24 hours.[20] The synergy between nanomaterials and organometallic chemistry warrants a new catalytic route of CH_4 functionalization, while additional studies are needed to understand the underlying mechanism and quantitatively evaluate the efficacy of the strategy that interfaces nanowires with organometallics.[23]

Here we report our analysis of the above-mentioned CH_4-to-CH_3OH catalysis in the context of a compartmentalized cascade. We translated the reported catalytic system into a theoretical model that estimates the numerical value of γ. Electron paramagnetic resonance (EPR) spectroscopy with a spin-trap agent, along with other characterization experiments, unraveled that the predominant ROS present in the system is a superoxide and illustrated its role in CH_3OH formation. This piece of mechanistic insight allowed us to subsequently determine the value of γ in the catalysis, which surprisingly amounts to more than 80%. The high value of measured γ is consistent with our theoretical framework and illustrates the efficacy of the created nanoscopic concentration gradient with minimal side reactions. Our results demonstrate that carefully designed compartmentalization, spatially controlling the occurrence of organometallic reactions in solution at the microscopic length scale, can circumvent undesirable reactions efficiently and create organometallic catalytic cycles impossible in homogeneous solutions.

Results and discussion

A theoretical framework of cascade reactions in a nanowire array electrode

Generally applicable for non-enzymatic cascade design as noted above, one question that we ask is whether our previously reported design employing the nanowire array and a concentration gradient is effective in utilizing the ephemeral O_2-sensitive intermediate, Rh^{II}, whose activation of CH_4 was considered turnover-limiting.[20,24] Our approach to this question is to construct a numerical model in the context of compartmentalization and analyze the reaction efficiency γ that will be valuable for future design consideration. Fig. 1C shows the reported reaction in the context of compartmentalized cascade reactions. Here the compartment, schematically shown as a yellow-colored dashed box, is defined as the O_2-free liquid phase within the nanowire array where Rh^{II}-initiated CH_4 activation is proposed to take place. Following its definition,[9,15] γ is expressed as the ratio between the outward flux of Rh^{III}–CH_3 for CH_3OH formation (R_p) and the rate of Rh^{II} generation (R_s)

during the electrolysis. Based on the proposed reaction mechanism (Fig. 1B and C), R_p and R_s are dictated by the kinetic rate constant of electrochemical reduction of Rh^{III} into Rh^{II} (k_1) as well as the Rh^{II}-initiated CH_4 activation (k_2), respectively. We note that γ could also be interpreted as the competition between the rate of CH_4 activation (R_p) in the compartment and the deactivation of Rh^{II} with O_2 in the bulk, whose rate constant is denoted as k_e. Because such a competition depends on the diffusive mass transport at a steady state, another important factor is the diffusive conductance F, as used in the design of enzymatic cascades,[6,9,13] which describes the rate of mass transport for chemical species crossing into and out of the compartment boundary. However, in order to obtain the flux of a particular species in and out of the compartment, F must be normalized to the volume of the compartment V and Avogadro's number N_A.[9] We anticipate that F and V will be co-dependent, therefore we derive an expression for $F/(VN_A)$, denoted F_V, in terms of the nanowire geometry (Section 1A of the ESI†). Since the Rh^{II}, Rh^{III}, and Rh^{III}–CH_3 species share the bulky metalloporphyrin structure, as a first-order approximation F_V is assumed to be the same among Rh^{II}, Rh^{III}, and Rh^{III}–CH_3, and only dependent on the morphology of the nanowire array. Assuming $k_e \to \infty$ due to the reported rapid deactivation,[21] we incorporated the above-mentioned components and derived a numerical model (Sections 1B of the ESI†), which describes γ in a compartmentalized cascade as shown below:

$$\gamma = \frac{R_p}{R_s} = \frac{k_1 F_V C_{Rh,total}}{k_2 (F_V + k_1)[Rh^{II}]^2 C_{CH_4}} \tag{1}$$

$$F_V \approx \frac{8D}{L^2} \tag{2}$$

Here $C_{Rh,total}$ is the total concentration of Rh species in the bulk solution, almost exclusively in the form of Rh^{III}; $[Rh^{II}]$ is the steady-state concentration of Rh^{II} in the compartment during electrolysis that remains to be numerically calculated; C_{CH_4} is the concentration of CH_4 in the bulk solution; D is the diffusion coefficient of the Rh species; and L is the length of the nanowire array. Similarly, we derived the expression of γ in the non-compartmentalized homogeneous solution (Section 1C of the ESI†). After solving the steady-state kinetic equations that include the mass transport across the compartment, we further derived the expressions of γ from eqn (1) for the nanowire array electrode:

$$\gamma = \frac{(F_V + k_1)\left(-F_V + \sqrt{F_V^2 + \frac{4F_V k_1 k_2 C_{CH_4} C_{Rh,total}}{F_V + k_1}}\right)^2}{4F_V k_1 k_2 C_{CH_4} C_{Rh,total}} \tag{3}$$

And the expressions of γ in a homogeneous solution:

$$\gamma' = \frac{\left(-k_e + \sqrt{k_e^2 + 4k_1 k_2 C_{CH_4} C_{Rh,total}}\right)^2}{4k_1 k_2 C_{CH_4} C_{Rh,total}} \tag{4}$$

we note that k_e is explicitly incorporated in eqn (4) while we assumed $k_e \to \infty$ in eqn (3). The above equations establish the theoretical framework for us to analyze the efficacy of the organometallic reactions in the nanowire array electrode.

The established theoretical model demands input from experimental results. Because of the high reactivity between Rh^{II} and O_2 outside of the O_2-free microenvironment in the nanowire array,[21] i.e. $k_e \to \infty$, γ can be approximated as the ratio between the amount of generated CH_3OH (N_{CH_3OH}) and Rh^{II} from electrochemical reduction of Rh^{III} ($N_{Rh(II)}$) (Fig. 1C), if we presume that the conversion from Rh^{III}–CH_3 to CH_3OH is stoichiometric as corroborated by using our prior experimental evidence.[20] While N_{CH_3OH} is experimentally readily measurable as we have done before,[20] the value of $N_{Rh(II)}$ is less accessible and requires the quantification of ROS because the electrochemical reduction of Rh^{III} into Rh^{II} is concurrent with the electrochemical reduction of O_2 into the ROS (Fig. 1B). Therefore, identification and quantification of the ROS in this catalytic system is needed, not only for deeper insights about the chemical steps involved in the catalysis but also for a quantitative determination of γ.

Identification and quantification of reactive oxygen species in the catalysis

The identity of the predominant ROS was probed by EPR spectroscopy with the addition of spin trap agent 5,5-dimethyl-1-pyrroline N-oxide (DMPO) during electrolysis.[25,26] Superoxide ($O_2^{\cdot-}$), hydrogen peroxide (H_2O_2), and hydroxyl radical ($^{\cdot}OH$) were presumed to be the possible ROS from O_2 reduction in aprotic solvent systems.[27,28] Among these possible ROS, H_2O_2, along with other hydroperoxide species, react with DMPO to yield the adduct DMPO–$OH^{\cdot}$, which can be detected by EPR spectroscopy.[29] While $O_2^{\cdot-}$ and $^{\cdot}OH$ are short-lived,[27,30] their reactions with DMPO yield more stable adducts DMPO–$O_2^{\cdot-}$ and DMPO–$OH^{\cdot}$, whose prolonged lifetimes are roughly 1 and 20 minutes, respectively, at room temperature and much longer under liquid N_2 conditions.[26] By trapping the generated ROS with DMPO during the electrolysis and discerning the trapped radicals in EPR spectroscopy[26,31,32] the possible presence of $O_2^{\cdot-}$ and $H_2O_2/^{\cdot}OH$ could be unveiled.

EPR spectra indicate that $O_2^{\cdot-}$ is the predominant ROS during the CH_4-to-CH_3OH conversion. As reported in our previous work (Section 3A in the ESI†),[20] CH_4-to-CH_3OH catalysis was conducted in a customized single-chamber electrochemical reactor (Fig. S1†), which was fed with a mixture of CH_4 and air (P_{CH_4}/P_{air} = 35) at a constant flow rate at ambient pressure and room temperature. Chronoamperometry of −1.4 V vs. the Saturated Calomel Electrode (SCE) was performed in 1,2-DFB with 1 mM of Rh^{III} as the pre-catalyst and 0.1 M tetrabutylammonium perchlorate (TBAClO$_4$) as the supporting electrolyte. A Si nanowire array with an average wire length of 15 μm and diameter of 50 nm (Fig. S2†), prepared based on the literature,[20,33] was used as the working electrode with a Pt wire counter electrode and a Ag$^+$/Ag pseudo-reference electrode equipped with a glass frit. 50 mM DMPO was added during the electrolysis to trap the generated ROS, and aliquots were taken for EPR experiments 5, 15, and 60 minutes after the addition of DMPO. Unless stated specifically, the aliquots were stored in liquid N_2 before the EPR measurements, although the DMPO adduct has been observed to be stable at room temperature for at least 90 minutes (Fig. S3†). We

note that the addition of DMPO *per se* does not significantly alter the electrochemistry in the system, if any, because previous studies have shown that DMPO is cathodically stable up to −2.35 V *vs.* SCE.[34] The EPR spectrum from the aliquot 15 minutes after DMPO addition is shown in Fig. 2A, which is similar to the ones from the aliquot taken at 5 and 60 minutes after DMPO addition (Fig. S4†). This similarity suggests that the radical species observed in EPR spectroscopy is the predominant species in the steady state during the electrolysis and not all of the transient ROS involved in the catalytic cycle may be captured in our experiments. Control experiments include the DMPO-added electrolysis without the Rh^{III} pre-catalyst (Fig. 2B), the reaction between DMPO and 0.5 mM KO_2 as a surrogate of $O_2^{\bullet-}$ (Fig. 2C and S5†), as well as the reaction between DMPO and 0.5 mM 2-hydroperoxypropan-2-ylbenzene ($PhC(CH_3)_2OOH$, cumene hydroperoxide) as a surrogate of $H_2O_2/{}^{\bullet}OH$ (Fig. 2D and S5†). The captured ROS during electrolysis is predominantly $O_2^{\bullet-}$, based on the similar spectra shown in Fig. 2A and C. Nonetheless, we note that the spectral pattern observed for the DMPO–$O_2^{\bullet-}$ in 0.1 M $TBAClO_4$ in 1,2-DFB solution is noticeably distinct from the DMPO–OOH observed in the aqueous solvent.[25,26] This difference can be rationalized by the employment of 1,2-DFB in place of H_2O and the resulting solvation sphere surrounding the adduct, the reduced proton concentration, and the possibility of TBA^+ cations to coordinate the anionic complex, which could explain the increased stability of the observed adduct upwards of 90 min. The similarity between Fig. 2A and B suggests that it is likely that the electrochemistry of Si nanowires rather than the Rh species is responsible for the generation of $O_2^{\bullet-}$.

We propose to quantify the generated ROS, predominantly $O_2^{\bullet-}$ at the steady state, by colorimetric assay with the use of nitroblue tetrazolium (NBT) chloride as a $O_2^{\bullet-}$-selective chromogen. NBT is reported to selectively react with the $O_2^{\bullet-}$ over H_2O_2 and other ROS,[35] leading to the emergence of a purple color in monoformazan, with a maximum absorption peak at ~530 nm,[35,36] from a pale yellow background. The stoichiometric reactivity between NBT and $O_2^{\bullet-}$ (1 : 2), ensured by utilizing a concentration of NBT/$O_2^{\bullet-}$ < 2, enables the use of UV-Vis absorption spectroscopy for the quantification of $O_2^{\bullet-}$ generation.[35,37–39] Additionally, NBT exhibits minimal reductive activity in organic solvent within its electrochemical window, which was not only reported in the previous literature[36] but also shown in our cyclic voltammograms (Fig. S6†) and chronoamperometry (Fig. 3A) on a glassy carbon working electrode in 0.1 M $TBAClO_4$ in 1,2-DFB solution. Thus, when added during the electrolysis under CH_4-to-CH_3OH conditions, NBT will have minimal interference with the O_2-reducing electrode and act as an $O_2^{\bullet-}$ scavenger for a colorimetric quantification of the accumulated $O_2^{\bullet-}$. While multiple methods including fluorescence measurements are viable for the $O_2^{\bullet-}$ quantification,[38] the absorbance at 600 nm from monoformazan after the reaction between NBT and $O_2^{\bullet-}$ (ref. 36) was chosen in order to mitigate interference from the optical absorbance and
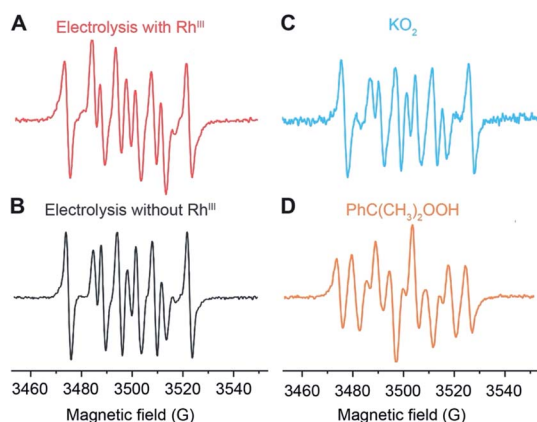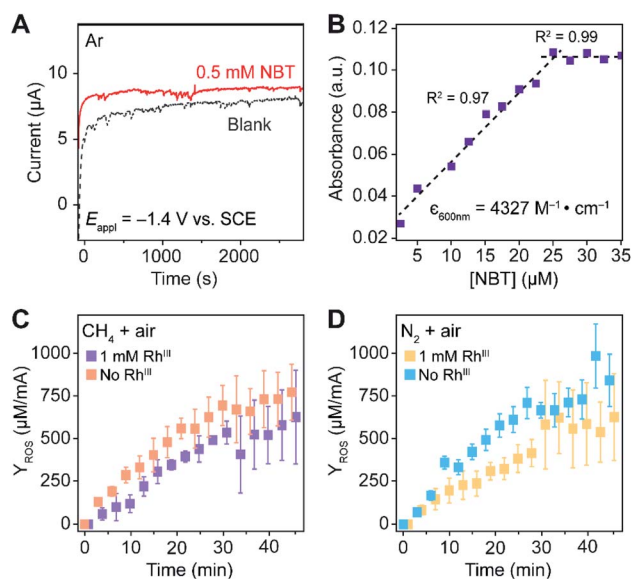

Fig. 2 Electron paramagnetic resonance (EPR) spectra depicting the adducts formed in the reaction of 50 mM DMPO (5,5-dimethyl-1-pyrroline N-oxide): (A) the electrolysis with the Rh catalyst during CH_4-to-CH_3OH conversion; (B) control electrolysis in the absence of the Rh catalyst; (C) 0.5 mM potassium superoxide (KO_2); (D) 0.5 mM 2-hydroperoxypropan-2-ylbenzene ($PhC(CH_3)_2OOH$, cumene hydroperoxide). Unless otherwise noted, the electrolyte solution is 0.1 M tetrabutylammonium perchlorate ($TBAClO_4$) in 1,2-difluorobenzene (1,2-DFB). Following previously reported conditions,[20] chronoamperometry was conducted at −1.4 V *vs.* SCE with the Si nanowire working electrode under a constant flow of a CH_4/air mixture P_{CH_4}/P_{air} = 35 in a customized electrochemical reactor (Fig. S1†) under ambient pressure.

Fig. 3 Quantification of superoxide ($O_2^{\bullet-}$) with $O_2^{\bullet-}$-selective chromogen nitroblue tetrazolium (NBT). (A) Chronoamperometry with a glassy carbon working electrode in Ar. (B) The absorbance at 600 nm in 1,2-DFB of a fixed concentration of KO_2, a surrogate of ephemeral $O_2^{\bullet-}$, for varying concentrations of NBT. ε_{600nm}, the established absorption coefficient at 600 nm of the yielded monoformazan from a stoichiometric reaction between NBT and $O_2^{\bullet-}$.[35] (C and D) The yield of ROS (Y_{ROS}), determined as the detected $O_2^{\bullet-}$ normalized by the average electric current, is displayed against electrolysis duration with a Si nanowire array of 15 μm length as the working electrode. (C) A CH_4/air atmosphere (P_{CH_4}/P_{air} = 35) with (purple, n = 4) and without (orange, n = 3) 1 mM Rh^{III}. (D) N_2/air atmosphere (P_{N_2}/P_{air} = 35) with (yellow, n = 5) and without (blue, n = 5) 1 mM Rh^{III}. −1.4 V *vs.* SCE 0.1 M $TBAClO_4$ in 1,2-DFB. Error bars denote standard deviations.

phosphorescence of Rh species (630–750 nm).[40] Furthermore, due to the ephemeral nature of $O_2^{\bullet-}$ that hinders the preparation of a standard solution of known $O_2^{\bullet-}$ concentration,[35,41] we specifically designed experiments that establish a calibration curve of the absorbance at 600 nm which accounts for the stoichiometric reaction between NBT and KO_2, the $O_2^{\bullet-}$ surrogate.[35] When an increasing concentration of NBT was mixed with a fixed concentration of KO_2 in 1,2-DFB, the absorbance at 600 nm follows a linear correlation before plateauing (Fig. 3B), illustrating a stoichiometric reaction between NBT and $O_2^{\bullet-}$ without other chromogenic side reactions. This led us to determine the absorption coefficient at 600 nm of the yielded monoformazan, $\varepsilon_{600\ nm} = 4327\ M^{-1}\ cm^{-1}$ ($R^2 = 0.97$) (Section 3B of the ESI†). A similar linear response between NBT and $O_2^{\bullet-}$ was also observed in the presence of Rh catalysts in 1,2-DFB (Fig. S7†), which suggests that the presence of Rh^{III} in the bulk solution does not interfere with the colorimetric assay.

The rate of $O_2^{\bullet-}$ generation was quantified with the use of NBT in the nanowire-based cascade system for CH_4-to-CH_3OH conversion. Under the same electrochemical conditions with the use of the Si nanowire array electrode of 15 μm length at −1.4 V *vs.* SCE, aliquots of the electrolyte solution were sequentially sampled, measured for optical absorbance at 600 nm, and applied to calculate the amount of accumulated $O_2^{\bullet-}$ (Section 3C of the ESI†). The yields of the net accumulated $O_2^{\bullet-}$ (Y_{ROS}), normalized by the average electric current during electrolysis, were shown as a function of electrolysis duration in CH_4/air and N_2/air atmospheres (P_{CH_4}/P_{air} and $P_{N_2}/P_{air} = 35$; Fig. 3C and D, respectively). The initial slopes of the Y_{ROS} before plateauing ($\partial Y_{ROS}/\partial t$) were determined as the rate of electrochemical ROS generation in the compartmentalized cascade reaction. $\partial Y_{ROS}/\partial t$ = 18 ± 4 and 22 ± 4 μM mA^{-1}·min^{-1} in the CH_4/O_2 atmosphere with the presence and absence of 1 mM Rh^{III} ($n = 4$ and $n = 3$; purple and orange traces in Fig. 3C, respectively); $\partial Y_{ROS}/\partial t = 16 \pm$ 4 and 23 ± 3 μM mA^{-1}·min^{-1} in the N_2/air with the presence and absence of 1 mM Rh^{III} ($n = 5$; yellow and blue traces in Fig. 3D, respectively). The similar values of $\partial Y_{ROS}/\partial t$ between the CH_4 and N_2 atmosphere suggests that the ROS formation is independent of the gaseous environment. The similar values of $\partial Y_{ROS}/\partial t$ with and without Rh^{III} suggests that the electrode surface of Si nanowires is primarily responsible for ROS generation, albeit the presence of Rh^{III} does seem to lower the ROS yield. Here we note that $\partial Y_{ROS}/\partial t$ could be underestimated, because NBT is less reactive towards other ROS that may be concurrently generated during the electrochemical process.

Experimental determination and analysis of reaction efficiency γ

Our successful quantification of the electrochemical ROS generation rate ($\partial Y_{ROS}/\partial t$) led to an experimentally determined value of reaction efficiency γ. As the reductive current is responsible for the generation of both ROS and CH_4-activating Rh^{II}, the equation for γ in Fig. 1C can be written as:

$$\gamma = \frac{R_p}{R_s} \sim \frac{N_{CH_3OH}}{N_{Rh(II)}} = \frac{N_{CH_3OH}}{\int I dt - \int I F_{Faradaic} V \frac{\partial Y_{ROS}}{\partial t} dt} \quad (5)$$

Here I denotes the electric current, $F_{faradaic}$ the faradaic constant, and V the volume of electrochemical reactor. Eqn (5) leads to $\gamma = 81\%$ for a 3 h electrolysis of CH_4 activation (Section 1D of the ESI†), based on the results of our previous report[20] and the value of Y_{ROS} determined in Fig. 3. The experimentally determined value of γ is relatively close to unity, suggesting that a large portion of the generated Rh^{II} activates CH_4 before diffusing out the nanowire array despite the high reactivity between Rh^{II} and O_2 (Fig. 1C).

In an effort to compare our experimentally determined γ values with the theoretical maximum, we numerically calculated the values of γ based on the established theoretical framework for a nanowire-based compartmentalization. Following the model displayed in Fig. 1C, the calculated values of R_s (Fig. 4A and D), R_p (Fig. 4B and E), and the Rh^{II} flux diffusing out of the compartment R_i (Fig. 4C and F) were displayed as a function of k_1 and F_V (Section 1B of the ESI†). These calculations use $k_e \to \infty$, $C_{CH_4} = 9.5$ mM,[20] $C_{Rh,total} = 1.0$ mM, and $k_2 = 2.9 \times 10^4\ M^{-2}\ s^{-1}$ for Rh^{II}-initiated CH_4 activation within the nanowire array as determined in our previous report.[20] Because the rate of electrochemical reduction of Rh^{III} (k_1) was not readily determinable in our system, k_1 was assigned as a range of values spanning four orders of magnitude (10^6 to $10^{10}\ s^{-1}$) based on a typical range reported for electron transfer of metalloporphyrin complexes in the literature.[42] Nonetheless, Fig. 4 shows that the effect of compartmentalization is not sensitive to the value of k_1, evident as the k_1 term cancels out in eqn (S14), (S18), and (S19)† during the derivation as long as k_1 is sufficiently larger ($\geq 10^6\ s^{-1}$) than the value of F_V, with an increased F_V value leading to increased fluxes both outward and inward of the compartment. Because the value of F_V is dependent on the nanowire array's morphology, such a trend suggests that we can control and possibly optimize the mass transport across the compartment by controlling the length L of the nanowire array based on eqn (2).

A comparison between the experimental value of γ with simulation results suggests that the Rh-based organometallic catalysis enabled by the nanowire array is indeed functioning near its theoretical limit. Given the strong dependence on the value of F_V for R_s, R_p, and R_i, we envisioned that γ is mostly a function of F_V, whose relationship is displayed as the red trace in Fig. 5. While R_s, R_p, and R_i all increase with larger values of F_V (*vide supra*), overall a larger F_V value tends to decrease the value of γ (Fig. 5). Such a trend is corroborated with our previous observation that a nanowire array of longer length L, hence smaller F_V value based on eqn (2), corresponds to a larger yield of CH_3OH before mass transport becomes rate-limiting.[20] One thing to note is that our developed theoretical framework does not account for those Rh^{III} molecules that enter and leave the nanowire compartment without undergoing the initial electrochemical reduction reaction. However, the alignment of the experimental and theoretical values indicates that this phenomenon, while it cannot be excluded completely, remains minimal in our system. In comparison, the value of γ for a non-compartmentalized scenario, *i.e.* homogeneous solution without a nanostructured electrode, is also shown as the black trace in Fig. 5 (Section 1C in the ESI†). A clear difference is
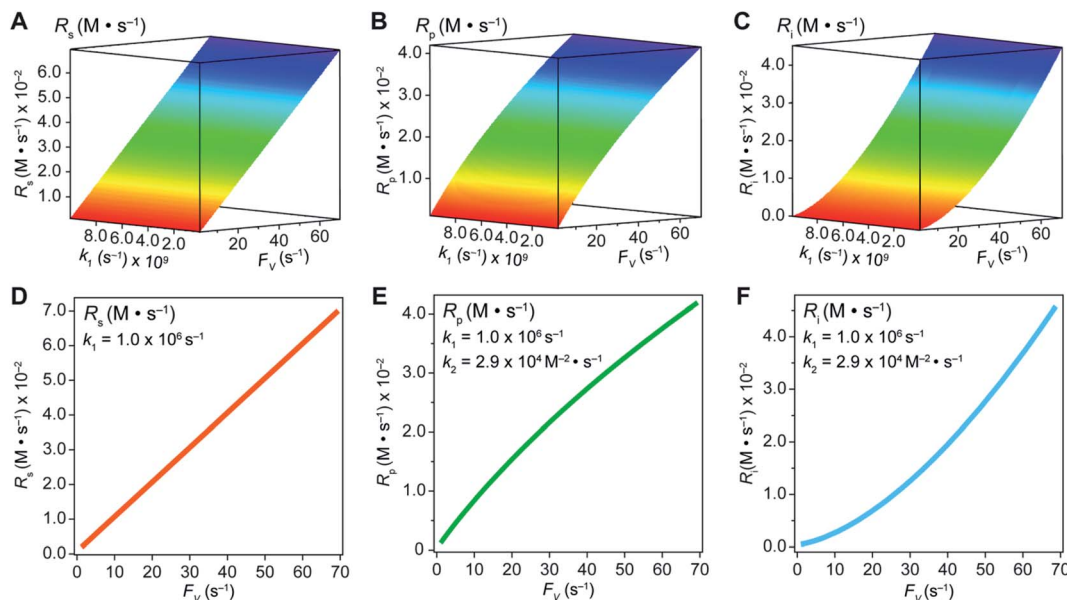
Fig. 4 Graphical representations of substrate conversion (R_s), product formation (R_p), and intermediate outflux (R_i) in the compartmentalized system. Panels (A), (B), and (C) represent R_s, R_p, and R_i, respectively, as a function of both F_V and k_1. Panels (D), (E), and (F) represent R_s, R_p, and R_i, respectively, as a function of F_V for a constant value of k_1 (1.0×10^6 s^{-1}). k_2 was experimentally determined to be 2.9×10^4 M^{-2} s^{-1} within the nanowire array in our previous report.[20]

Fig. 5 Reaction efficiency γ plotted as a function of diffusive conductance F_V for the scenarios with nanowire-enabled compartmentalization (red trace) and γ plotted as a function of k_1 without nanowire-enabled compartmentalization (black trace). The experimentally determined data point of γ for nanowire array of 15 μm length is represented by the star. The error bar presents the approximation when deriving the experimental value of F_V (Section 1A in the ESI†).

observable as the value of γ for the non-compartmentalized scenario is virtually near zero (at most 0.001% indeed), in line with our previous experimental work that utilized a planar electrode surface and resulted in no CH$_3$OH generation.[20] We also positioned our experimentally determined γ value in Fig. 5, after we determined $F_V = 20$. s^{-1} given $L = 15$ μm and $D = 5.6 \times 10^{-10}$ m^2 s^{-1} in 1,2-DFB as measured before.[20] The error bar in Fig. 5 represents the approximation incurred when deriving the expression for F_V (eqn (2)) (Section 1A in the ESI†). A good agreement between the experimental and theoretical values of γ for the nanocompartment was observed (Fig. 5), yet the slightly

higher value of experimentally derived γ might originate from the underestimation of $\partial Y_{ROS}/\partial t$ (*vide supra*). The agreement indicates that minimal unforeseen side reactions, if any, are present in the catalyst system and the proposed benefit of a nanowire-generated O$_2$-free microenvironment for Rh^{II}-initiated CH$_4$ activation is well demonstrated.

Despite the findings that O$_2^{\bullet-}$ is the dominant ROS at steady state, we propose that O$_2^{\bullet-}$ is not the immediate oxidant that reacts with Rh^{III}–CH$_3$ for CH$_3$OH formation. We found that under strictly dry conditions, no CH$_3$OH was observed in a mixture of KO$_2$ and the as-synthesized Rh^{III}–CH$_3$. Yet a stoichiometric amount of CH$_3$OH, calculated using ^{1}H NMR, was observed in experiments with Rh^{III}–CH$_3$ and KO$_2$ "wet" in 1,2-DFB (5.1 ± 0.3 mM H$_2$O based on Karl Fischer titration). Along the same lines, 1 : 1 reactivity was observed upon mixing Rh^{III}–CH$_3$ with hydroperoxide species such as cumene hydroperoxide or *t*-butyl hydroperoxide in dry 1,2-DFB (Section 4 of the ESI†).[20] Such observations prompted us to propose that trace hydroperoxide, namely H$_2$O$_2$, is constantly generated during the electrolysis and is the immediate reactant towards Rh^{III}–CH$_3$ to afford CH$_3$OH as the product. We speculate that the electrochemical reduction of O$_2$ to O$_2^{\bullet-}$ is followed by a chemical protonation step to generate other ROS such as a hydroperoxyl radical (HO$_2^{\bullet}$),[43] which is susceptible to heterolytic and homolytic cleavages and eventually converges on H$_2$O$_2$.[44–46] Whether the conversion of HO$_2^{\bullet}$ to H$_2$O$_2$ proceeds electrochemically or chemically should be dependent on the proton donor concentration in solution and the reduction potential applied.[46] Once the hydroperoxide species is formed, CH$_3$OH formation proceeds from its reaction with Rh^{III}–CH$_3$. Such mechanistic consideration would be useful in designing other ROS-initiated CH$_4$-activation reactions.

Additional design insights are available from our results. We examined the dependence of γ on different hypothetical values of the CH_4-activation rate constant k_2. Smaller values of k_2 significantly lower γ, *i.e.* the efficiency of compartmentalization created by the nanowire array (Fig. S8†). Such a trend is reasonable since a lower value of k_2 will lead to more prominent outward flux R_i of the unreacted Rh^{II} species which will introduce a larger percentage of undesirable Rh^{II} deactivation. Therefore, while our Rh-based catalysis demonstrates the benefits of compartmentalization by constructing a catalytic cycle of seemingly incompatible steps for organometallics, we caution that the efficacy of this strategy depends on the specific chemical system under consideration. As the value of γ depends on F_V and thus the nanostructure's morphology, such as nanowire length L in our case, there exists an optimal morphology of nanostructures for specific organometallic compounds' reactivities in order to create an effective microenvironment and efficient cascade reactions with minimal detrimental deactivation. A quantitative evaluation of reaction efficiency γ, however estimated, is recommended in order to justify the introduction of nanostructures and a micro-environment. A general numerical design framework of nanostructures for a typical organometallic catalytic cycle that includes oxidative addition and reductive elimination is currently being developed in the authors' laboratory.

Conclusion

In this work, we applied the concept of reaction efficiency γ in biochemical cascades to quantitatively evaluate the efficacy of compartmentalization for organometallic reactions with the use of nanowire array electrodes. A high γ value approaching unity, the theoretical limit, was experimentally observed, suggesting minimal detrimental side reactions. This observation indicates that with suitable design it is possible to employ nanomaterials to spatially control organometallic reactions and achieve efficient cascade with ephemeral intermediates, analogous to the biological counterparts with near-unity γ values. This work quantitatively highlights the transformative power of spatial control at the nanoscale for new chemical reactivity.

Author's contribution

C. L. supervised the project. C. L. and B. S. N. designed experiments and wrote the paper. B. S. N. synthesized the compounds and conducted electrochemical characterization experiments with assistance from D. M. D. B. J. J. performed the mathematical derivations on the compartmentalized system. All the authors discussed the results and assisted during the manuscript preparation.

Conflicts of interest

The authors declare no competing financial interest.

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