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Separating a multicomponent and multiphase liquid mixture with a 3D-printed membrane device

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The separation of multicomponent and multiphase liquid mixtures is critical in many important applications, e.g., wastewater treatment. While conventional technologies have been utilized in the separation, it usually takes many steps, resulting in high cost and energy consumption. Here we have demonstrated that, using a 3D-printed membrane device with multiple selectivity, a multicomponent and multiphase liquid mixture can be separated in a much more efficient way. The water–benzene–heptane mixture has been successfully separated with a 3D-printed “box”, which has a supported ionic liquid membrane (SILM) on the side wall and a hydrogel-coated hydrophilic/oleophobic membrane on the bottom. The water and oil (*i.e.*, benzene/heptane) are separated by the hydrogel-coated hydrophilic/oleophobic membrane. Then the benzene is separated from heptane with the SILM. To further increase the separation throughput, the structure of the 3D-printed “box” has been optimized to increase the total surface area of SILM. Our results suggest that 3D-printed membrane device with multiple selectivity is promising in the separation of multicomponent and multiphase liquid mixtures.

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1. Introduction

Separating multicomponent and multiphase liquid mixtures is critical in many applications. For example, the purification of oily wastewater, a worldwide challenge brought by the direct discharge of sewage from many industries, requires effective separation of multicomponent and multiphase liquid mixtures.^{1–4} The state-of-the-art technology involves multistep processes, which are often costly and energy intensive. Moreover, there are challenges in separating both immiscible and miscible liquid mixtures. For immiscible liquid mixtures, conventional processes, such as air flotation, coagulation, and flocculation, are limited by the low efficiency.^{1–4} For miscible liquid mixtures, distillation has been widely utilized though it has very high energy consumption. Nevertheless, some liquid mixtures contain azeotropes where simple distillation without supporting facilities will not work.^{5,6} Currently available distillation processes for azeotrope separations are azeotropic, extractive, and pressure swing distillations. However, these technologies involve more steps and are all very energy intensive. Another alternative process is liquid–liquid extraction. But it takes large amounts of solvents and is not favored.^{6–9}

Membrane technologies, which did not come to light until the mid-1970s, are promising in separating liquid mixtures due to their environmental and economic advantages.^{10,11} To date, membrane separation has been explored in separating both

immiscible and miscible liquid–liquid mixtures. For the separation of immiscible liquid mixtures, *i.e.*, oil–water separation, membrane technology has attracted more and more interest in past decades because of its low cost and high efficiency.² The surface wettability of membranes has been optimized to improve the separation efficiency. Both hydrophobic/oleophilic and hydrophilic/oleophobic membranes have been studied, and the latter are preferred because they improve not only the separation efficiency but also the fouling resistance.^{12–16} Regarding the separation of miscible liquid mixtures, Supported Ionic Liquid Membranes (SILMs) have been shown to be promising due to lower energy consumption, easier operation, less waste, and more flexibility in system design.^{17–19} Ionic liquids serve as the extraction solvent in SILMs and are impregnated in the supporting membrane.^{7,20} Due to their low vapor pressure and high stability compared to conventional liquids, ILs are expected to improve the reliability of SILMs.

Though membrane technology shows great promise in separating both immiscible and miscible liquid mixtures, to date there has been no report on the separation of multicomponent and multiphase liquid mixtures using a single membrane device. The key challenge here is that each membrane only has single selectivity and it takes multiple selectivity to separate multicomponent and multiphase liquid mixtures. In the current paper, we take advantage of 3D printing to integrate two types of membranes into one membrane device, *i.e.* a 3D-printed “box” that has SILMs on the side wall and a hydrogel-coated hydrophilic/oleophobic membrane²¹ on the bottom. A three-component and two-phase model liquid

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mixture, *i.e.*, water–benzene–heptane, has been successfully separated with the 3D-printed “box”. The oil phase, *i.e.*, benzene–heptane, is separated from the water phase by the hydrogel-coated hydrophilic/oleophobic membrane. Then benzene is separated from heptane using a [Bmim][PF₆] based SILM. To increase the separation throughput, we have optimized the structure of the “box” to increase the total surface area. Our results suggest that the 3D-printed membrane device has great promise in separating multicomponent and multi-phase liquid mixtures.

2. Method

2.1 Chemicals

Benzene (99.8%; anhydrous) was purchased from Sigma-Aldrich. *n*-Hexadecane (99.5%) and *n*-heptane (HPLC grade) were purchased from Alfa Aesar. 1-Butyl-3-methylimidazolium hexafluorophosphate ([Bmim][PF₆]; 98+%) was obtained from Fisher Scientific. DI water was produced with a Millipore Academic A10 system. These chemicals were utilized as received. Viton fluoroelastomer rubber sheet (chemical-resistant, 12" × 12", 1/32") were purchased from McMaster-Carr. PVDF (Polyvinylidene fluoride) membrane filters (MilliporeSigma™ Durapore™; hydrophilic: 0.65 μm pore size) was purchased from Fisher Scientific.

2.2 3D printing of membrane device (“box”)

A desktop stereolithography (SLA) 3D printer (Form 2, Formlabs) was utilized to fabricate the integrated membrane “box”, with a clear liquid photopolymer resin (Clear Resin 1L, Formlabs).²² Printing was performed on a platform with a maximum 145 × 145 × 145 mm³ building volume. Pre-programmed Clear V4 settings in open mode at room temperature with 100 μm layer thickness were selected to print the membrane “box”, which was pre-designed with a solid modeling computer-aided design (CAD) software (*i.e.*, Solidworks). The 3D printing software (Preform, Formlabs) imports STL files to the 3D printer with preferred printing layout settings. After each printing task was completed, the printed membrane “box” was further processed with a washer (Form Wash, Formlabs) containing pure IPA for 20 minutes followed by UV irradiation in a post-curing machine (Form Cure, Formlabs) for 60 minutes at 60 °C to produce the final integrated membrane “box”.

2.3 Preparation of SILM

The 90 mm-diameter PVDF membrane was soaked in approximately 1.5 mL of [Bmim][PF₆] in a Petri dish, which was kept inside a pressurized oven at 60 °C and 27 in. Hg for at least 24 hours to impregnate [Bmim][PF₆] into the PVDF membrane.^{19,23,24}

2.4 Fabrication of hydrogel coated membrane

A hydrogel coating was developed in our lab previously²¹ for oil–water separation and is applied to 3D-printed membranes here to separate water from organic mixtures. The hydrogel-coated membrane for oil–water separation was fabricated following

the same procedure in our previous work.²¹ Briefly, a plastic membrane was firstly fabricated by the desktop SLA 3D printer (Form 2, Formlabs) and then immersed into a zwitterionic hydrogel solution for 1 minute. After taking it out, the coated membrane was placed on a Spectroline Bi-O-Vision trans-illuminator (wavelength: 312 nm) for 5 minutes. After the hydrogel has been *in situ* photopolymerized, the coated membrane was immersed in deionized (DI) water for 1 day, followed by being stored in an enclosed culture dish.²¹

2.5 Characterizations

To visualize the impregnation of ionic liquid on the supporting membrane before and after separation, a scanning electron microscope (SEM) characterization was performed with a Zeiss SIGMA VP system at 3 kV accelerating voltage. The loss of ionic liquid was also calculated by weighting the SILM before and after the separation. To determine the composition of the liquid mixture of both the feed and the receiving sides, thermogravimetric analysis (TGA) (SEIKO-220 TG/DTA) and nuclear magnetic resonance (NMR) (Bruker AVANCE III 300 MHz) analyses were performed to identify each component from both sides of the membrane. Due to a higher boiling point, TGA can differentiate hexadecane from benzene and heptane (BP: 98 °C) so TGA was used to determine the amount of hexadecane diffused across SILM to the feed side. For each test, approximately 40 mg of liquid sample was added into an aluminum pan and heated to 120 °C at a rate of 10 °C min^{−1} under air purging. The receiving side liquid was further analyzed using ¹H NMR spectroscopy with an inverse observe probe. Acetone-d₆ as NMR solvent was referenced at 2.05 ppm chemical shift to trace impurity. Receiving side component purities were calculated using peak integrals from NMR spectra plots for each sample. Because the NMR peaks representing heptane and hexadecane hydrogen chemical shifts overlapped, the following system of equations were used to calculate the molar fractions of heptane, hexadecane, and benzene from the receiving side of the boxes.

$$\begin{cases} x + y + z = 1 \\ \frac{\text{peak integral of CH}_3}{\text{peak integral of CH}_2} = \frac{3(2x + 2y)}{2(5x + 14y)} \\ \frac{\text{peak integral of CH}_3}{\text{peak integral of benzene}} = \frac{3(2x + 2y)}{(6z)} \end{cases} \quad (1)$$

where *x*, *y*, and *z* are molar fractions of heptane, hexadecane, and benzene respectively. Peak integrals were generated in the NMR analysis software (Mnova, Mestrelab). Receiving side component purities were calculated by solving the set of equations listed above. Only zero heptane and hexadecane exchange trials were considered successful runs. All experiments were repeated for at least three times.

3. Results & discussions

3.1 Characterizations of SILM and hydrogel coated membrane

Characterization of the surface morphology of SILM using SEM images shown in Fig. 1 illustrated the distribution of [Bmim]



[PF₆] throughout the entire membrane after 24 hours of impregnation. Fig. 1 shows an example of plain PVDF membranes with 0.65 μm pores and SILMs that are filled with ionic liquids by using the pressure and vacuum method inside a vacuum oven. For the ionic liquid choice used when preparing SILM, [Bmim][PF₆] was selected because it showed high selectivity towards benzene/heptane separation.^{19,23,25}

With our integrated membrane boxes, SILMs were used to separate benzene from the initial three-component two-phase mixture and the hydrogel-coated plastic membrane, Fig. 2, was used to separate water from the feed mixture. A layer of hydrogel was coated on 3D-printed plastic membranes through *in situ* polymerization to realize the separation of immiscible liquid mixtures such as oil and water. The microscope image in Fig. 3(a) shows that the plastic membrane has a pore size of ~2 mm, which is consistent with the computer-aided sketch. After being coated by hydrogel, the membrane pores were plugged by hydrogel, while they can be “opened” again after the membrane was immersed in water for a week, as shown in Fig. 3(b) and (c). This is because the hydrogel trapped in membrane pores will swell by absorbing water, through which the internal stress of hydrogel builds up and eventually cracks the hydrogel to create the small pore. Fig. 3(d) indicates those cracks were not lost or enlarged even after running 31 cycles of oil–water separation.

3.2 3D-printed membrane “box”

The structure of 3D-printed membrane “box” is shown in Fig. 4. There is a center box where the feed, *i.e.*, benzene (80 mL)/heptane (80 mL)/water (80 mL) mixture, is added. Around the center box there are four receiving box containing the receiving solvent, *i.e.*, hexadecane (120 mL). As shown in Fig. 4, four identical SILMs were sandwiched between the center and the four receiving boxes with Viton rings to clamp them together, respectively, and the hydrogel-coated membrane was mounted on the bottom of the center box.

Oil (*i.e.*, benzene and heptane) and water was separated by the hydrogel-coated hydrophilic/oleophobic membrane at the bottom of the “box”. Water goes through the membrane due to the gravity and the hydrophilicity of the membrane. Oil cannot go through the membrane because the capillary force, which is induced by the oleophobicity of the membrane, is larger than the gravitational force.²¹ The oil–water separation is complete within 10 minutes and the separation results are summarized in

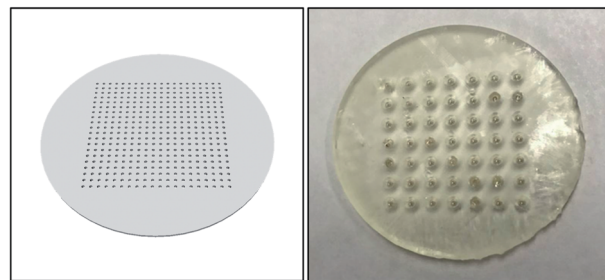


Fig. 2 A digital model of 3D-printed membrane (left) and 3D-printed plastic membrane coated by zwitterionic hydrogel (right).

Table 1. The solution going through the hydrogel-coated membrane has a water purity of 99.5% (v), indicating a successful oil–water separation. The reusability of the 3D-printed hydrogel-coated membrane was excellent and additional details on hydrogel-coated membranes are provided in our previous study.²¹

As shown in Fig. 4, benzene was separated from heptane *via* the SILMs. Since benzene is solvable in [Bmim][PF₆] while heptane is not, benzene will go through the SILM and heptane will not. During separation, the benzene in the center box goes through four SILMs to the four receiving boxes. The separation results are shown in Fig. 5. After 24 hours of separation, 2.7% of the initial benzene went through each SILM. Thus, a total of 11 vol% of benzene was withdrawn from the initial benzene in the center box.

3.3 Effect of surface area/volume ratio

While oil–water separation is reasonably fast, *i.e.*, within 10 minutes, the benzene–heptane separation with SILMs is much slower, *i.e.*, only ~2.7% of the initial benzene is separated after 24 hours. The benzene throughput $\left(\frac{dC}{dt}\right)$, from the feed to the receiving solution through SILMs can be described by eqn (2) shown below:²⁵

$$Ak(C_f - C_r) = V \frac{dC}{dt} \quad (2)$$

Here A is the surface area of the membrane that is in contact with the solution, k is mass transfer coefficient of the solute, C_f and C_r are concentrations of benzene in the feed solution and in the receiving solution, respectively, V is the volume of the receiving solution, t is time. To increase the separation throughput of SILMs, surface area to volume (A/V) ratio needs to be maximized. To further verify this idea, three types of 3D-printed cubes with different sizes (*i.e.*, A/V ratios), as shown in Fig. 6, were studied. Since A/V is disproportional to the size of the cube, smaller cube is expected to increase the benzene throughput (in percentage of initial benzene volume).

The SILM was sandwiched between two cubes with the same size (see Fig. 6), *i.e.*, one feeding and the other receiving. The separation results are shown in Fig. 7. The benzene throughput after 6 hours increases with the A/V ratio, which conforms our hypothesis. Interestingly, after 24 hours, the

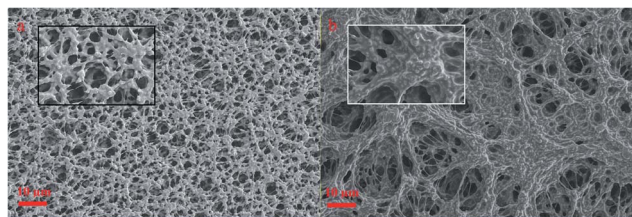


Fig. 1 The SEM images of supported ionic liquid membranes made from PVDF membranes (0.65 μm pore size) (a) without [Bmim][PF₆] (b) impregnated with [Bmim][PF₆]. Magnification setting: 1000× (original image) & 5000× (enlarged image).



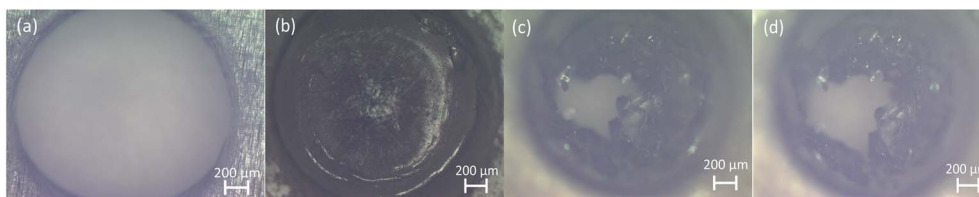


Fig. 3 Optical microscope images of a pore of (a) bare plastic membrane, (b) hydrogel-coated membrane before water immersion, (c) hydrogel-coated membrane after water immersion and (d) hydrogel-coated membrane after 31 times oil–water separation. Reproduced with permission of the American Chemical Society.²¹

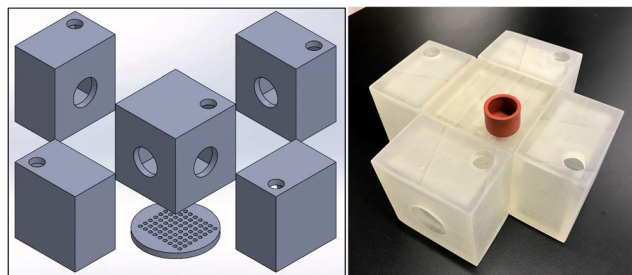


Fig. 4 The CAD model (left) and the 3D-printed prototype (right) of 1st-design integrated membrane box.²¹

Table 1 NMR results for oil–water separation with a hydrogel coated membrane in the 3D-printed integrated “box”

Water separation	Initial feed volume	Remaining feed mixture	Receiving side mixture
Benzene	80 mL	54.8%	0.2%
Heptane	80 mL	44.6%	0.3%
DI water	80 mL	0.6%	99.5%

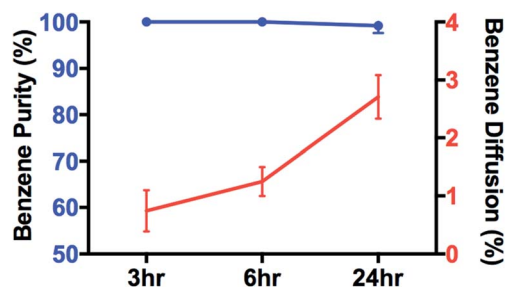


Fig. 5 Benzene–heptane separation results with each SILM for 3D-printed integrated membrane “box”.

benzene throughput was similar for the $3 \times 3 \times 3$ cm cube and $2 \times 2 \times 2$ cm cube, which is ~ 1.5 times of that of the $6 \times 6 \times 6$ cm cube. Compare with the clear A/V trend for 6 hour data, a possible reason for losing A/V effects in long-term runs might be due to the drop of concentration gradient which is the driving force of SILM. For a higher A/V ratio, the batch separation completes faster which could be a sign of reaching equilibrium.

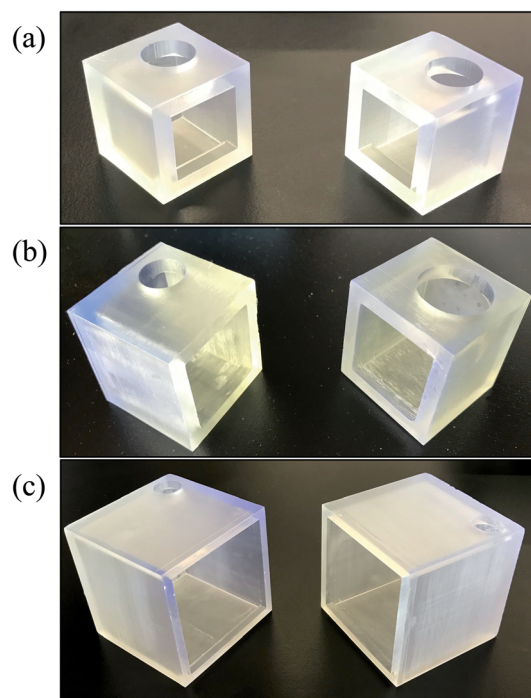


Fig. 6 3D-printed cubes for surface area/volume ratio experiments (a) $2 \times 2 \times 2$ cm cube (b) $3 \times 3 \times 3$ cm cube (c) $6 \times 6 \times 6$ cm cube.

3.4 Modified 3D-printed membrane “box”

Taking advantage of the idea that smaller cube with higher A/V ratio results in higher benzene throughput, the structure of the membrane “box” was modified. As shown in Fig. 8, the

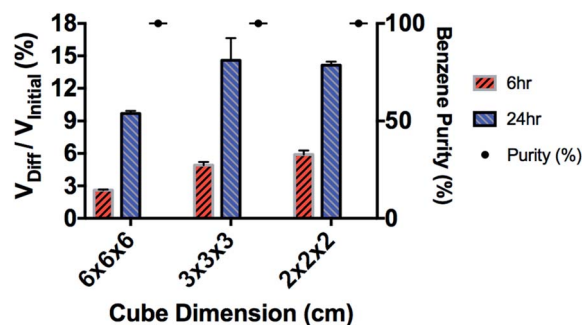


Fig. 7 Total benzene diffusion across SILM for $6 \times 6 \times 6$ cm cube, $3 \times 3 \times 3$ cm cube, and $2 \times 2 \times 2$ cm cube comparison for 6 hour and 24 hour results. V_{Diff} and V_{Initial} are the benzene volume diffused through SILM and the initial benzene volume in the feed mixture.



modified “box” consists of three identical separation sectors which hold a maximum capacity of 90 mL initial feed mixture. The SILM is mounted between the neighboring separation sectors. Each separation sector is composed of nine $1.5 \times 1.5 \times 1.5$ cm cubes. The volume of the entire “box” is comparable to that of the center box in the original design. For the modified membrane “box”, each feed side within a separation sector contains equal volume of benzene (10 mL), heptane (10 mL), and DI water (10 mL). The attached receiving side located on the back of the neighboring separation sector contains 15 mL of hexadecane. Two separate sectors which only includes a single feed or a single receive was used to sandwich all other separation sectors. When clamping all sectors together as shown in Fig. 8, feed solutions were added into three feed sides from the top of each column. The receiving side solvent, hexadecane, was added to the built-in receiving side from the smaller top holes. A total of three individual systems was tested for benzene diffusion experiments with a left-side feed box, a right-side receiving box, and two center boxes designed to function as both feed and receiving side for separation across SILM. Viton sheets were used to sandwich each SILM to provide supporting functions. The hydrogel-coated membrane was “built-in” on the bottom of each

separation sector. The hydrogel coating procedure is the same as described in Section 2.4. In this design, all centerpieces (*i.e.*, separation sectors) were identical and includes both feeding and receiving functions. As a result, it can expand easily by adding more separation sectors.

The separation results are shown in Fig. 9. More than 11 vol% of benzene is separated through each separation sector after 24 hours of separation, which is significantly higher than $\sim 2.7\%$ (Fig. 9) in the original “box”. These results demonstrate that the higher A/V ratio increases the benzene throughput, which is consistent with previous reports.^{26–29} The purity of benzene (benzene/(benzene + heptane)) in the receiving solution was $\sim 100\%$ up to 6 hours of separation. After 24 hours of separation, it maintained at ~ 95 vol%, which indicates a small amount of heptane also diffused through SILM. This could result from the loss of ionic liquids. After 24 hours of separation, for both original and modified “box”, the benzene throughput is $\sim 11\%$ of the initial feed benzene. However, the modified “box” has much lower volume, needs less SILM and is easier to scale up. These advantages result from the smaller cube with higher A/V ratio. Oil–water separation results for the modified 3D-printed membrane box is summarized in Table 2. Hydrogel coated membrane built in at the bottom of the membrane box remain efficient for oil–water separation.

Our results highlight the potential of 3D-printed integrated membrane system with multiple selectivity in separating multicomponent and multiphase liquid mixture. Although we only tested the device on a three-component and two-phase mixture (benzene/heptane/water), this approach can be extended to other on-demand multicomponent and multiphase liquid mixtures with modified and complex 3D-printing designs. Compared to conventional multi-step separation process, the novel prototype of a 3D-printed integrated device is more compact, energy-efficient, cost-efficient, and produces less wastes. Moving forward, the major challenge for industry application is still the relatively slow SILM separation. The solution could be a high A/V ratio *via* geometry optimization plus a continuous flow process to enhance the reliability and feasibility of the device. The 3D-printing approach could also apply to the bio-separation field to address the advanced purification challenges.

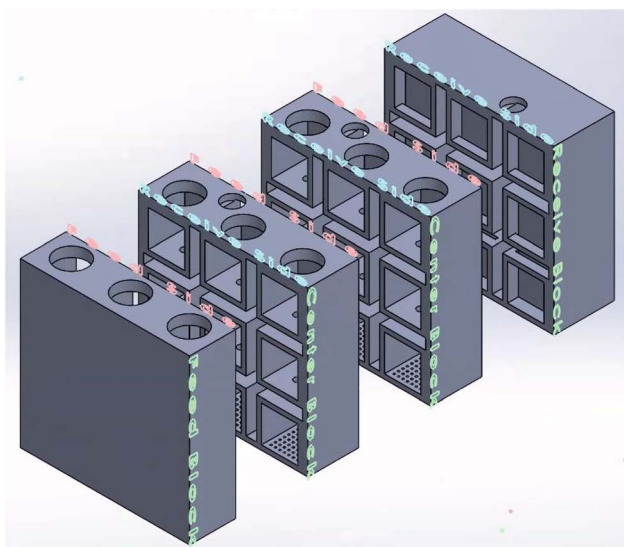


Fig. 8 Cross section view of the CAD model (top) and the 3D-printed prototype (bottom) of 2nd-design integrated membrane box.

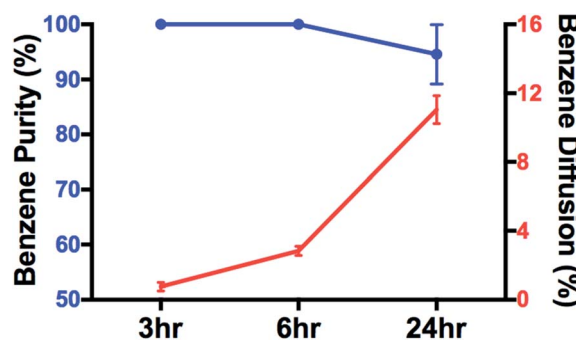


Fig. 9 Benzene and heptane diffusion across SILM for modified 3D-printed integrated membrane “box”.

Table 2 NMR results for oil–water separation with a hydrogel coated membrane in the modified 3D-printed integrated “box”

Water separation	Initial feed volume	Remaining feed mixture	Receiving side mixture
Benzene	10 mL	51.9%	0.0%
Heptane	10 mL	46.3%	0.0%
DI water	10 mL	1.8%	100%

4. Conclusion

To conclude, a benzene/heptane/water mixture has been successfully separated using a 3D-printed integrated membrane, which contains supported ionic liquid membranes and a hydrogel-coated hydrophilic/oleophobic membrane. The separation results highlighted the ability of the 3D-printed integrated membrane in separating a multi-component and multi-phase liquid mixture. Our results also showed that the separation throughput can be increased significantly by increasing the total surface area of the SILM.

Abbreviations

CAD	Computer-aided design
NMR	Nuclear magnetic resonance
PVDF	Polyvinylidene fluoride
SEM	Scanning electron microscope
SILM	Supported ionic liquid membrane
SLA	Stereolithography
TGA	Thermogravimetric analysis
[Bmim]	1-Butyl-3-methylimidazolium
[PF ₆]	Hexafluorophosphate

Conflicts of interest

There are no conflicts to declare.

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References

- M. Cheryan and N. Rajagopalan, Membrane processing of oily streams. Wastewater treatment and waste reduction, *J. Membr. Sci.*, 1998, **151**(1), 13–28.
- M. Padaki, *et al.*, Membrane technology enhancement in oil–water separation. A review, *Desalination*, 2015, **357**, 197–207.
- S. Munirasu, M. A. Haija and F. Banat, Use of membrane technology for oil field and refinery produced water treatment—A review, *Process Saf. Environ. Prot.*, 2016, **100**, 183–202.
- J. Dickhout, *et al.*, Produced water treatment by membranes: A review from a colloidal perspective, *J. Colloid Interface Sci.*, 2017, **487**, 523–534.
- I. Rodríguez-Donis, V. Gerbaud and X. Joulia, Entrainer Selection Rules for the Separation of Azeotropic and Close-Boiling-Temperature Mixtures by Homogeneous Batch Distillation Process, *Ind. Eng. Chem. Res.*, 2001, **40**(12), 2729–2741.
- V. Gerbaud, *et al.*, Review of extractive distillation. Process design, operation, optimization and control, *Chem. Eng. Res. Des.*, 2019, **141**, 229–271.
- A. B. Pereiro, *et al.*, Ionic liquids in separations of azeotropic systems – A review, *J. Chem. Thermodyn.*, 2012, **46**, 2–28.
- L. C. Branco, J. G. Crespo and C. A. M. Afonso, Highly Selective Transport of Organic Compounds by Using Supported Liquid Membranes Based on Ionic Liquids, *Angew. Chem., Int. Ed.*, 2002, **41**(15), 2771–2773.
- J. D. Thornton, *Science and practice of liquid-liquid extraction*, Oxford science publications, Oxford, 1992, Clarendon Press.
- I. Pinnau and B. D. Freeman, Formation and Modification of Polymeric Membranes: Overview, in *Membrane Formation and Modification*, 1999, American Chemical Society, pp. 1–22.
- D. S. Sholl and R. P. Lively, Seven chemical separations to change the world, *Nature*, 2016, **532**(7600), 435–437.
- J. Yang, *et al.*, Superhydrophilic–superoleophobic coatings, *J. Mater. Chem.*, 2012, **22**(7), 2834–2837.
- A. K. Kota, *et al.*, Hygro-responsive membranes for effective oil–water separation, *Nat. Commun.*, 2012, **3**, 1025.
- J. A. Howarter and J. P. Youngblood, Amphiphile grafted membranes for the separation of oil-in-water dispersions, *J. Colloid Interface Sci.*, 2009, **329**(1), 127–132.
- P. Brown, O. Atkinson and J. Badyal, Ultrafast oleophobic-hydrophilic switching surfaces for antifogging, self-cleaning, and oil–water separation, *ACS Appl. Mater. Interfaces*, 2014, **6**(10), 7504–7511.
- P. S. Brown and B. Bhushan, Mechanically durable, superoleophobic coatings prepared by layer-by-layer technique for anti-smudge and oil–water separation, *Sci. Rep.*, 2015, **5**, 8701.
- R. Egashira, *et al.*, A Simple Way for the Improvement of Separation Selectivity of Hydrocarbons by O/W/O Emulsion Liquid Membrane, *J. Chem. Eng. Jpn.*, 1995, **28**(1), 38–45.
- N. Yamanouchi, A. Ito and K. Yamagiwa, Separation of Benzene/Cyclohexane by Vapor Permeation through Triethylene Glycol Liquid Membrane, *J. Chem. Eng. Jpn.*, 2003, **36**(9), 1070–1075.
- M. Matsumoto, Y. Inomoto and K. Kondo, Selective separation of aromatic hydrocarbons through supported liquid membranes based on ionic liquids, *J. Membr. Sci.*, 2005, **246**(1), 77–81.
- I. Domínguez, *et al.*, Separation of Benzene from Heptane Using Tree Ionic Liquids: BMimMSO₄, BMimNTf₂, and PMimNTf₂, *Procedia Eng.*, 2012, **42**, 1597–1605.
- Y. Song, *et al.*, 3D-Printed Membranes with a Zwitterionic Hydrogel Coating for More Robust Oil–Water Separation, *Ind. Eng. Chem. Res.*, 2020, **59**(48), 21058–21065.



- 22 R. Salas, *3D printing for the rapid prototyping of structural electronics*, ProQuest Dissertations Publishing, 2013.
- 23 A. P. de los Ríos, *et al.*, On the importance of the nature of the ionic liquids in the selective simultaneous separation of the substrates and products of a transesterification reaction through supported ionic liquid membranes, *J. Membr. Sci.*, 2008, **307**(2), 233–238.
- 24 F. J. Hernández-Fernández, *et al.*, Preparation of supported ionic liquid membranes: Influence of the ionic liquid immobilization method on their operational stability, *J. Membr. Sci.*, 2009, **341**(1), 172–177.
- 25 M. Kamaz, *et al.*, π Electron induced separation of organic compounds using supported ionic liquid membranes, *Sep. Purif. Technol.*, 2020, **236**, 116237.
- 26 F. Eisenhaber, *et al.*, The double cubic lattice method: Efficient approaches to numerical integration of surface area and volume and to dot surface contouring of molecular assemblies, *J. Comput. Chem.*, 1995, **16**(3), 273–284.
- 27 V. Thavasi, G. Singh and S. Ramakrishna, Electrospun nanofibers in energy and environmental applications, *Energy Environ. Sci.*, 2008, **1**(2), 205.
- 28 L. J. Lozano, *et al.*, Recent advances in supported ionic liquid membrane technology, *J. Membr. Sci.*, 2011, **376**(1), 1–14.
- 29 A. K. Pabby, B. Swain and A. M. Sastre, Recent advances in smart integrated membrane assisted liquid extraction technology, *Chem. Eng. Process.*, 2017, **120**, 27–56.

