Dehydrogenation of methylcyclohexane over Pt-based catalysts supported on functional granular activated carbon†

Hong-Li Ye, a,b Shuang-Xi Liu, a,b, c Cui Zhang, a b, c You-Qiong Cai d and Yong-Fu Shi b,a

Herein, we developed the dehydrogenation of methylcyclohexane over Pt-based catalysts supported on functional granular activated carbon. Sulphuric acid, hydrogen peroxide, nitric acid and aminopropyl triethoxy silane were adopted to modify the granular activated carbon. The structural characterizations suggested that the carbon materials had a large surface area, abundant pore structure, and a high number of oxygen-containing functional groups, which influenced the Pt-based catalysts on the particle size, dispersion and dehydrogenation activity. The hydrogen temperature-programmed reduction technique was utilized to investigate the interaction between the active component Pt and the various functionalized granular activated carbon materials. The CO pulse technique revealed the particle sizes and dispersion of the as-prepared Pt-based catalysts. Finally, the Pt-based catalysts were successfully applied to study their catalytic activity in the dehydrogenation reaction of methylcyclohexane. The results showed that the Pt-based catalyst over granular activated carbon functionalized with sulphuric acid groups had a higher conversion of methylcyclohexane (63%) and a larger hydrogen evolution rate (741.1 mmol gPt⁻¹ min⁻¹) than the other resulting Pt-based catalysts at 300 °C.

A series of liquid organic hydrides have been developed by cyclohexane, methylcyclohexane (MCH), 1,4-dimethylcyclohexane, and decalin for their high hydrogen storage capacity (6–8%) and high boiling points (80–200 °C) to ensure they are in liquid state during transportation. Among them, MCH is a potential and satisfactory candidate due to its high reversibility and the low toxicity of the dehydrogenation products. The dehydrogenation reaction of MCH will be accelerated the reaction process and reduced the activation energy in the presence of catalysts. The active components of the dehydrogenation catalysts are Pt, Pd, Re, Ni, Cu, Co, La, especially the precious metals Pt and Pd. Shukla et al. reported that Pt-based catalysts showed a higher activity than the Pd-based catalysts for the dehydrogenation of MCH. Moreover, Pt-based catalysts can selectively activate the C–H bond without cleavage of the C–C bond and dramatically decrease the activation energy. What’s more, the rate of H spillover on Pt is more rapid than that on Pd, which effectively inhibits the background reaction. The catalyst supports play a significant role in the activity and stability of the Pt-based catalysts. Many efforts have been made on the supports for Pt-based catalysts, especially Al₂O₃, and activated carbon materials (ACM). Including activated carbons (AC), activated carbon filters (ACF), activated carbon nanotubes (ACN) and so on. Compared with Al₂O₃, ACM always possesses a high specific surface area, large pore volume and controllable surface, which are beneficial to the dispersion of catalysts. Wang et al. showed that the catalytic activity of

Introduction

Owing to the cleanliness, rich reserves, environment friendly and high combustion caloric value, hydrogen energy has attracted extensive attention as an alternative energy. The global demand for H2 has increased continuously by 3–4% annually. The flammability of hydrogen results in potential hazards during its storage and transportation. Hence, it is significant to develop a relatively mild and safe storage approach. Liquid organic hydrides have emerged as one of these promising hydrogen carriers owing to their advantages, such as their reversible hydrogenation–dehydrogenation cycles, easy storage and the release of hydrogen on demand via the catalytic process, high hydrogen storage capacity, high energy density, convenient transportation in the safe conditions, etc.

†Electronic supplementary information (ESI) available. See DOI: 10.1039/d1ra05480e
0.25% Pt/AC was equal to that of 1% Pt/Al2O3. Furthermore, ACM can be modified by HNO3 and O3 to increase the number of surface functional groups, which is another factor affecting the dispersion and activity of the catalysts. Viscardi et al. reported an MCM-41 sulfonated catalyst with great thermal stability, high surface area, abundant acid loading and the maximum methanol conversion. Hosseini et al. adopted sulfonic acid groups to modify the surface of reduced graphene oxide, which formed efficient solid acids with excellent catalytic efficiencies in acetalization and esterification reactions.

Herein, we investigated the dehydrogenation of MCH over Pt-based catalysts supported on functional granular activated carbon (GAC). Sulfuric acid, hydrogen peroxide, nitric acid and aminopropyl triethoxy silane were used to modify the GAC to yield GAC-S, GAC-HO, GAC-N and GAC-NH, respectively. The structural characterization results, including analysis performed using scanning electron microscopy (SEM), Fourier transform infrared spectroscopy (FTIR), N2-adsorption, X-ray photoelectron spectrometry (XPS) and thermogravimetric analysis (TGA), suggested that the carbon supports had large surface area, abundant pore structure, and a significant number of oxygen-containing functional groups, which influenced the particle size, dispersion and dehydrogenation activity of the Pt-based catalysts. The hydrogen temperature-programmed reduction (H2-TPR) technique was utilized to investigate the interaction between the active component Pt and the distinct functionalized granular activated carbon. The CO pulse technique revealed the particle sizes and the dispersion of the as-prepared Pt-based catalysts. Finally, the catalytic activities of the Pt-based catalysts for the dehydrogenation reaction of MCH were studied. The results showed that the Pt/GAC-S catalyst demonstrated a higher conversion of MCH (63%) and a larger hydrogen evolution rate (741.1 mmol gPt⁻¹ min⁻¹) than the other resulting Pt-based catalysts at 300 °C.

**Experimental section**

**Materials**

Chloroplatinic acid solution (H2PtCl6·6H2O) and ethylene glycol solution were purchased from Tianjin Jinhai Type Science and Technology Development Co. Ltd and Tianjin Jiangtian Chemical Technology Co. Ltd, respectively. GAC was provided by Fujian Xin Charcoal Industry Co., Ltd. MCH, toluene (TOL), aminopropyl triethoxy silane, nitric acid, and hydrogen peroxide were purchased from Tianjin Concord Technology Co., Ltd. Milli-Q deionized water, and dried at 110 °C for 12 h, and marked as GAC-S, GAC-NH, GAC-N, and GAC-HO, respectively.

**Preparation of the functional GAC supports**

Pt-based catalysts were prepared using a previously reported method. Briefly, 2.0 g GAC and 20 mL deionized water were dispersed into a 100 mL three-well flask. After stirring evenly, a certain amount of chloroplatinic acid was dropped into the suspension. Being stirred for 30 min later, 20 mL of ethylene glycol solution was added. The precursor was heated and refluxed for 4 h, then filtered and washed with deionized water. The as-prepared solid was finally dried in a vacuum oven for 12 h at 55 °C to yield Pt/GAC. The loaded amount of Pt in the catalysts was about 0.2% (measured by ICP-AES). The catalysts of Pt/GAC-S, Pt/GAC-HO, Pt/GAC-N and Pt/GAC-NH were synthesized using the same operation. Before the dehydrogenation reaction of MCH was performed, the Pt-based catalysts were reduced using H2 at 400 °C for 2 h.

**Preparation of the Pt-based catalysts**

**He-temperature-programmed decomposition (He-TPD) characterization**

He-TPD tests were carried out on a Micromeritics Chemisorb 2750 in a helium gas atmosphere. About 0.20 g of the sample was placed in a U-shaped quartz tube and pretreated in He gas for 1 h at 150 °C before the test, then cooled to 100 °C. Desorption of the sample was performed in the temperature range of 100–1000 °C with a heating rate of 10 °C min⁻¹, and the spectra were recorded.

**H2-TPR characterization**

The H2-TPR technique was also carried out on the Micromeritics Chemisorb 2750 equipped with a thermal conductivity detector. About 0.10 g of the sample was placed into a quartz U-shaped tube and purged for 0.5 h with 10% H2 in Ar, then heated to 900 °C with a heating rate of 10 °C min⁻¹ and the spectra were recorded on a computer.

**CO pulse characterization**

The CO pulse technique was conducted on a Micromeritics Chemisorb 2750 equipped with a thermal conductivity detector. About 0.10 g of the sample was acquired and reduced by H2 at 400 °C for 40 min, then cooled to 25 °C under helium protection. The adsorption of CO was begun when the temperature stabilized at 25 °C.
Catalytic reaction

Dehydrogenation of MCH to yield hydrogen and toluene was carried out under atmospheric pressure in a fixed-bed flow reactor (10 mm inner diameter (ID) × 250 mm) with 0.30 g of the Pt-based catalysts. The MCH was injected into the reactor with a pump under a nitrogen stream with a flow rate of 0.03 mL min⁻¹. The conversion of MCH was determined using a Rock GC 7800 gas chromatograph equipped with a flame ionization detector and an SE-30 column.

Recycling studies

Recycling assays were carried out to investigate the heterogeneity and stability of the catalysts. After the first catalytic reaction had finished, the Pt/GAC-S catalyst was recovered by filtration, washed with distilled water, dried at 55 °C for 12 h in a vacuum and reused for the second catalytic reaction. The same operations were implemented in another three runs. At the same time, after the first run, the amount of Pt in the recovered Pt/GAC-S and in the filtrate was detected by ICP-AES.

Results and discussion

Structural characterization of the supports

SEM images displayed the morphology of GAC, as shown in Fig. 1A. GAC appeared as a large number of amorphous spherical particles with a uniform size. The XRD pattern (Fig. 1B) revealed the crystal structure of GAC. The diffraction peaks at 24° and 44° were stemmed from the (002) crystal plane and the (100) crystal plane of graphite microcrystalline (PDF# 041-1487), respectively. The Raman spectrum further evidenced the degree of crystallization of GAC. As revealed in Fig. 1C, the peak at 1334 cm⁻¹ for the D band and the 1590 cm⁻¹ peak representing the G band were observed in the Raman spectrum of GAC, which were attributed to the disordered carbon and the Eg vibration of the sp² bonded carbon double bonds, respectively. Meanwhile, the ratio of I_D/I_G was employed to evaluate the disorder of the material structure. The ratio value of I_D versus I_G was calculated to be 1.05, which indicated that the amorphous carbon was a little higher than the crystal carbon in GAC. In addition, 2679 cm⁻¹ peak of 2D (an overtone of the D bond) was determined in the Raman spectrum of GAC, which was in agreement with the reported literature. The FTIR spectrum (Fig. 1D) confirmed the abundant oxygen-containing functional groups on the surface of GAC. The peak at 620 cm⁻¹ was assigned to the bending vibration of C–H. The absorption peak at 1630 cm⁻¹ was assigned to the C=O stretching vibration. 1274 cm⁻¹ and 1098 cm⁻¹ were attributed to the stretching vibration of C–O–C and the asymmetric stretching vibration of C=OH, respectively. The 3130–3740 cm⁻¹ region was resulted from the O–H stretching vibration.

The XPS spectra further evidenced the surface structure of GAC. As observed in Fig. 2A, the surface of GAC was composed of a great number of C and O elements. In the C 1s spectrum of GAC (Fig. 2B), the XPS peaks locating at 284.6, 285.5, 286.9 and
290.4 eV were registered in C–C/C–H, C–O, C–O and O–C–O bonds, respectively. The O 1s spectra (Fig. 2C) divided into two peaks of 532.4 and 536.5 eV, indicating the presence of C–O and C=O bonds. The results of XPS were identical with those of FTIR.

After modification, the structure of GAC was slightly changed. Table 1 lists the specific surface areas, pore volumes and pore sizes of GAC, GAC-S, GAC-HO, GAC-N and GAC-NH. The specific surface area of GAC was as high as 1782 m² g⁻¹, which decreased to 1444 m² g⁻¹ after treatment with 2 mol L⁻¹ sulfuric acid, 1540 m² g⁻¹ with 2 mol L⁻¹ hydrogen peroxide, 1415 m² g⁻¹ with 2 mol L⁻¹ nitric acid, and 905 m² g⁻¹ with 2 mol L⁻¹ aminopropyl triethoxy silane. The oxidative treatment might diminish the specific surface area, which coincided with the previously published literature. The same downward trends were observed in the microsurface area and pore volume. The drop in the specific surface area and pore volume may be caused by the blockage of some pores during the oxidative treatment.

Fig. 3 shows the adsorption isotherms and the pore diameter distributions of the supports. As observed in Fig. 3A, all the adsorption isotherms for the supports belonged to the type IV hysteresis loops, indicating the presence of mesoporous pores. The pore diameter distributions of the supports (Fig. 3B) suggested that the supports mainly consisted of the micropores. The most probable pore sizes of the supports were focused on the range of 0.5–0.6 nm.

After treatment, the surface of GAC was modified with the functional groups, which gradually decomposed and released CO or CO₂ gas with the increasing temperature under an inert gas atmosphere (e.g. He gas). Fig. 4A shows the He-TPD profiles of GAC, GAC-S, GAC-HO, GAC-N, and GAC-NH. As shown in

---

Table 1: Surface structural information of GAC supports treated with different reagents

<table>
<thead>
<tr>
<th>Supports</th>
<th>BET (m² g⁻¹)</th>
<th>Micropore area (m² g⁻¹)</th>
<th>Pore volume (cm³ g⁻¹)</th>
<th>Micropore volume (cm³ g⁻¹)</th>
<th>Mean pore size (nm)</th>
<th>Mean micropore size (nm)</th>
</tr>
</thead>
<tbody>
<tr>
<td>GAC</td>
<td>1782</td>
<td>832</td>
<td>1.03</td>
<td>0.37</td>
<td>2.32</td>
<td>0.54</td>
</tr>
<tr>
<td>GAC-S</td>
<td>1444</td>
<td>699</td>
<td>0.83</td>
<td>0.31</td>
<td>2.29</td>
<td>0.54</td>
</tr>
<tr>
<td>GAC-HO</td>
<td>1540</td>
<td>621</td>
<td>0.96</td>
<td>0.27</td>
<td>2.49</td>
<td>0.53</td>
</tr>
<tr>
<td>GAC-N</td>
<td>1415</td>
<td>757</td>
<td>0.78</td>
<td>0.34</td>
<td>2.19</td>
<td>0.53</td>
</tr>
<tr>
<td>GAC-NH</td>
<td>905</td>
<td>487</td>
<td>0.51</td>
<td>0.22</td>
<td>2.20</td>
<td>0.54</td>
</tr>
</tbody>
</table>
Fig. 4A(a), the peaks at 280 °C and 860 °C in the GAC He-TPD curve were attributed to the carboxylic acid group and the carbonyl substance, respectively. Meanwhile, the distinct peak at 290 °C in the GAC-S He-TPD curve (Fig. 4A(b)) was also assigned to the carboxylic acid group and at 850 °C to the carbonyl substance. However, the peak at 290 °C was obviously larger than that of GAC, we speculated that the difference was derived from the sulfonic acid group. The He-TPD curve of GAC-HO (Fig. 4A(c)) was essentially the same as that of GAC, which indicated that the types of functional group remained unchanged after being treated with hydrogen peroxide. After functionalization with nitric acid, many peaks were observed in Fig. 3 (A) N₂ adsorption isotherms and (B) pore diameter distributions of (a) GAC, (b) GAC-S, (c) GAC-HO, (d) GAC-N, and (e) GAC-NH.

Fig. 4 (A) He-TPD of (a) GAC, (b) GAC-S, (c) GAC-HO, (d) GAC-N, and (e) GAC-NH; TG and DTG of (B) GAC, (C) GAC-S, (D) GAC-HO, (E) GAC-N, and (F) GAC-NH.
the H$_2$-TPR curve of GAC-N (Fig. 4A(d)), which suggested the fabrication of more functional groups, such as carboxylic groups, lactone, carboxylic anhydride groups, etc. The H$_2$-TPR curve of GAC-NH (Fig. 4A(e)) was almost the same as that of GAC, which indicated that the functional groups kept unchanged after being treated with aminopropyl triethoxy silane. Fig. 4B-F show the TGA and DTG curves of GAC, GAC-S, GAC-HO, GAC-N, and GAC-NH, respectively, which further revealed the surface functional groups of several carbon materials. As shown in Fig. 4B of the GAC TG and DTG profile, the exothermic peak (30–100 °C) was assigned to the evaporation of moisture. Furthermore, the peak at 155 °C was ascribed to the decomposition of carboxyl acid, which was consistent with that of He-TPD and FTIR. Additionally, the weak peaks at 376 °C and 485 °C in the GAC DTG curve were attributed to the decomposition of the carboxyl anhydrides, and the one at 635 °C of the carbonyl group. In the first stage (30–100 °C) of the TG curve of GAC-S (black line in Fig. 4C), the mass loss was also ascribed to the evaporation of moisture, which was shown at 57 °C of the DTG curve of GAC-S (blue line in Fig. 4C). Similar to GAC, the peak at 160 °C of the GAC-S DTG curve was attributed to the decomposition of carboxyl acid. The obvious peak at 312 °C in the GAC-S DTG curve was derived from the decomposition of the sulfonic acid group. The peak at 490 °C in the GAC-S DTG curve was attributed to the decomposition of carboxyl anhydrides. As shown in Fig. 4D of the GAC-HO TG and DTG profile, the exothermic peak (30–100 °C) was assigned to the evaporation of moisture. The broad peaks in the regions of 90–280 °C and 284–500 °C were ascribed to the carboxylic acid and the carboxyl anhydrides, respectively. The peaks at 54 °C, 158 °C, 270 °C, 427 °C and 674 °C were attributed to the moisture, carboxylic acid, carboxyl anhydrides and carbonyl group, respectively (Fig. 4E), which was in agreement with the results of He-TPD. The peaks at 140 °C, 260 °C and 340 °C were assigned to the carboxylic acid, carboxyl anhydrides and amino group.

Structural characterizations of the Pt-based catalysts

Fig. 5 shows the H$_2$-TPR curves of the GAC and Pt-based catalysts, which depicted the reduction mechanism. As shown in Fig. 5a, the peak at 630 °C was observed in the H$_2$-TPR curve of GAC, which was attributed to the surface functional groups of GAC. Compared with GAC, the H$_2$-TPR curve of Pt/GAC (Fig. 5b) showed the peaks at 240 °C and 340 °C, which were generated by the reduction of Pt–O–Pt and Pt–O–C, respectively, further demonstrating the successful synthesis of Pt-based catalysts. The reduction peaks of Pt–O–Pt or Pt–O–C were also observed in the H$_2$-TPR curves of GAC-S (Fig. 5c), GAC-NH (Fig. 5d), GAC-HO (Fig. 5e), and GAC-N (Fig. 5f), which could improve the dispersion of the metal species. Moreover, the reduction peaks in the curves of the Pt-based catalysts were less than 400 °C, which indicated that the Pt was in the metallic state in the catalysts before the dehydrogenation of MCH.

The degree of dispersion of the Pt particles affects the catalytic activity. The CO pulse adsorption was adopted to measure the degrees of dispersion of the Pt-based catalysts, which were listed in Table 2. The degrees of dispersion of the active component Pt in Pt/GAC, Pt/GAC-S, Pt/GAC-HO, Pt/GAC-N and Pt/GAC-NH were 26.6, 34.7, 20.3, 19.4 and 11%, respectively. In addition, the particle sizes of Pt were 4.26, 3.57, 5.58, 5.83 and 10.3 nm, respectively. The degree of dispersion of Pt/GAC-S was larger than that of Pt/GAC, and the particle size of Pt/GAC-S was smaller than that of Pt/GAC, which indicated that the activated carbon modified by dilute sulfuric acid effectively improved the dispersion of the Pt precursor and reduced the particle size. However, the degrees of dispersion of the Pt/GAC-HO, Pt/GAC-N and Pt/GAC-NH catalysts were lower than that of Pt/GAC, and the particle sizes of the Pt/GAC-HO, Pt/GAC-N and Pt/GAC-NH catalysts were much larger than that of Pt/GAC, demonstrating that hydrogen peroxide, dilute nitric acid and aminopropyl triethoxy silane were not conducive to the homodispersion of the Pt-based catalyst or improving the immersion load of chloroplatinic acid. In summary, the results showed that dilute sulfuric acid was a good reagent for improving the degree of dispersion of the precious metal Pt and reducing the particle size, which was consistent with the previously reported results.

Dehydrogenation of MCH over the Pt-loaded catalysts

Fig. 6 shows the conversion curves of MCH to TOL and the hydrogen evolution histograms taking Pt/GAC, Pt/GAC-S, Pt/GAC-HO, Pt/GAC-N and Pt/GAC-NH as catalysts with a reaction temperature of 300 °C and a space velocity of 5 h$^{-1}$. As shown in Fig. 6A, the conversion of MCH using Pt/GAC as a catalyst was firstly about 21.2%, but dramatically decreased to 8.64% after 12 h, which might result from the agglomeration of the Pt/GAC catalyst. In contrast, the conversion of MCH adopting Pt/GAC-S as the catalyst was initially around 66.3% and slightly decreased to 61% after 12 h, which was higher and more stable than that of Pt/GAC. It might benefit from the high degree of dispersion and the small particle size of Pt/GAC-S. However, the conversion values of MCH utilizing Pt/GAC-HO, Pt/GAC-N, and Pt/GAC-NH as the catalysts were much lower than that of Pt/GAC, which indicated that dilute nitric acid,
hydrogen peroxide and aminopropyl triethoxy silane were not suitable for treating carbon materials to catalyze the dehydrogenation of MCH. The average conversion values of MCH utilizing Pt/GAC, Pt/GAC-S, Pt/GAC-HO, Pt/GAC-N, and Pt/GAC-NH as the catalysts were 13.6%, 63.0%, 7.78%, 1.41% and 1.09%, respectively, which were exploited to calculate the hydrogen evolution (Fig. 6B). The hydrogen evolution rate of Pt/GAC was 160.2 mmol gPt \(^{-1}\)/C0 \(^{-1}\) min \(^{-1}\)/C0 \(^{-1}\), which increased up to 741.1 mmol gPt \(^{-1}\)/C0 \(^{-1}\) min \(^{-1}\)/C0 \(^{-1}\) of Pt/GAC-S, further indicating the good catalytic activity of Pt/GAC-S in the dehydrogenation of MCH. However, the hydrogen evolution rates of Pt/GAC-HO, Pt/GAC-N, and Pt/GAC-NH were obviously less than that of Pt/GAC, which proved their poor catalytic abilities in the dehydrogenation of MCH. Table 3 lists a comparison of the dehydrogenation of MCH over previously reported Pt-based catalysts, which showed that the hydrogen evolution rate in this work was higher than previously reported results, further indicating the good performance of the resultant Pt/GAC-S for the catalytic dehydrogenation of MCH.

Fig. S1† displays the Pt 4f XPS spectra and S 2p XPS spectra of the fresh and the recovered Pt/GAC-S catalysts. As revealed in Fig. S1A†, two-doublet binding energies in the Pt 4f \(_{7/2}\) spectra of the fresh Pt/GAC-S catalyst were obtained. The peaks at 70.4 and 73.1 eV were attributed to metallic platinum and PtO, corresponding to Pt(0) and Pt(II), respectively. \(^{34}\) 76.1 and 79.9 eV in the Pt 4f \(_{5/2}\) spectra of the fresh Pt/GAC-S catalyst were assigned to Pt(0) and Pt(II), respectively. Compared to the fresh Pt/GAC-S, the doublets binding energies in the Pt 4f \(_{7/2}\) and 4f \(_{5/2}\) spectra of the recovered Pt/GAC-S catalyst were almost unchanged. The peaks at 70.0 eV in the Pt 4f \(_{7/2}\) spectra and 75.9 eV in the Pt 4f \(_{5/2}\) spectra resulted from metallic platinum, while that of 73.0 eV in the Pt 4f \(_{7/2}\) spectra and 80.2 eV in the Pt 4f \(_{5/2}\) spectra were caused by PtO. Fig. S1B† presents the decomposition curves of the S 2p spectra in fresh and the recovered Pt/GAC-S catalysts.
Conclusions

Herein, we developed the dehydrogenation of MCH over Pt-based catalysts supported on functional GAC. Sulphuric acid, hydrogen peroxide, nitric acid and aminopropyl triethoxy silane were utilized to modify GAC to yield GAC-S, GAC-HO, GAC-N, and GAC-NH supports. Characterizations including SEM, FTIR, N\textsubscript{2}-adsorption, XPS and TGA suggested that the as-prepared functional carbon supports had a large surface area, abundant pore structure, and a significant number of oxygen-containing functional groups. The results of H\textsubscript{2}-TPR analysis demonstrated the interaction between the active component Pt and the various functionalized carbon supports. CO pulse data revealed that Pt/GAC-S showed a smaller particle size and a higher dispersion than the other Pt-based catalysts. The catalytic activities of the Pt-based catalysts were finally studied in the dehydrogenation reaction of MCH. Recycling studies indicated the good stability of the Pt/GAC-S catalyst and the heterogeneous active sites of Pt component. The results of the catalytic reaction showed that the Pt/GAC-S catalyst demonstrated a higher conversion of MCH (63%) and a larger hydrogen evolution rate (741.1 mmol g\textsubscript{Pt} \textsuperscript{-1} min \textsuperscript{-1}) than the other resulting Pt-based catalysts at 300 °C.

Author contributions

Hong-Li Ye: conceptualization, investigation, methodology, data curation, writing – original draft; Shuang-Xi Liu: investigation, data curation; Cui Zhang: supervision, writing – review and editing, funding acquisition, project administration; You-Qiong Cai: supervision, writing – review and editing; Yong-Fu Shi: supervision, writing – review and editing.

Conflicts of interest

There are no conflicts of interest to declare.

Acknowledgements

This work was supported by the National Natural Science Foundation of China [no. 21003077] and the Key Project of Tianjin Application Foundation and Frontier Plan [no. 14JCZDJC32000].

References

8. N. Kariya, A. Fukuoka and M. Ichikawa, Efficient evolution of hydrogen from liquid cycloalkanes over Pt-containing catalysts supported on active carbons under “wet-dry


30 M. S. Hosseini, M. M. Farahani and S. Shahsavard, Chemical modification of reduced graphene oxide with sulfonic acid groups: Efficient solid acids for acetalization


