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## Immobilization techniques of a photocatalyst into and onto a polymer membrane for photocatalytic activity

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This article reviews the various techniques of immobilizing a photocatalyst into and onto the polymer membrane for pollutant removal and as a problem solver in handling suspended photocatalyst issues from the previous literature. A particular focus is given to the preparation of mixed matrix membranes and deposition techniques for photocatalytic degradation in applications for wastewater treatment. Advantages and disadvantages in this application are evaluated. Various operating conditions during the process are presented. About 90 recently published studies (2008–2020) are reviewed. From the literature, it was found that  $\text{TiO}_2$  is the most favoured photocatalyst that is frequently used in photocatalytic water treatment. Dry–wet co-spinning and sputtering techniques emerged as the promising technique for immobilizing a uniformly distributed photocatalyst within the polymeric membrane, and exhibited excellence pollutant removal. In general, the technical applicability is the key factor in selecting the best photocatalyst immobilizing technique for water treatment. Finally, the scope of various techniques that have been reviewed may provide potential for future photocatalytic study.

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## 1. Introduction

Recently, water pollution and wastewater problems have increasingly become a major concern, especially the leaching of organic pollutants that are not only found in industry and urban areas, but also in all surrounding environments, which can affect the health of mankind.<sup>1</sup> Wastewater consists of various pollutants. In particular, the production of chemicals, pharmaceuticals and personal care products (PPCPs) and endocrine disrupting compounds (EDCs) has increased dramatically due to increasing scientific developments.<sup>2</sup> Thus, all these chemicals can be considered as the contaminants of emerging concern (CEC). Despite this, the existence of metals and inorganic pollutants (such as nitrate, arsenic, chromium and mercury) in drinking water and wastewater has been given attention due to its environmental problems. Besides, the larger development of industries, especially in food processing, agriculture, and textiles and paper making, involves the excessive use of chemicals, which lead to the higher release of toxic compounds to

the environment.<sup>3</sup> These species enter water streams through rinsing, washing, processing, dilution, transportation and manufacturing cooling procedures, which lead to the discharge of these chemicals into water bodies, and can give adverse effects not only to human health, but also to the ecosystem.

Various techniques have been proposed for wastewater treatment, such as adsorption, photo-Fenton process,<sup>4</sup> biodegradation, ozonation, electrochemical filtration, photocatalytic degradation and membrane technologies. Adsorption offers excellent removal of contaminants in water due to their abundant pore sites and larger surface area to trap pollutants, as well as their low operating cost and ability to reduce the by-product discharge.<sup>5</sup> However, the synthesis of powdered adsorbents, such as activated carbon, or agricultural waste (such as date seeds, rice husk, coconut shells and nut shells) requires a higher amount of chemicals during operation,<sup>6</sup> have poor selectivity and demonstrate unstable performance.<sup>7</sup> Besides, the other technique in wastewater treatment is the Fenton process, which has been successfully implemented in the removal of water pollutants. It involves the use of sulfate radical from the decomposition of persulfate (PS) or peroxydisulfate (PDS) with UV, high temperature and metals.<sup>8</sup> Even though this technique offers a low cost method, it limits the oxidizing capability in the degradation of pollutants.

Due to the demands of renewable energy and green environment to save the Earth, photocatalytic treatment using membrane technologies has been widely discussed among various researchers, and has been chosen as an attractive topic

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in the purification of water and wastewater by using UV or visible light.<sup>7</sup> In this photocatalytic theory, the photocatalyst is needed due to the presence of a photogenerated active species that has the capability to activate the degradation process of various organic pollutants under the radiance of light.<sup>9</sup> During the degradation process, a hydroxyl radical will be formed from the photoexcitation between light energy with electrons and holes present in the photocatalyst to degrade the pollutant in water. Numerous photocatalysts have been successfully synthesized, such as titanium dioxide ( $\text{TiO}_2$ ),<sup>10</sup> silver oxide,<sup>7</sup> graphitic carbon nitride,<sup>11</sup> bismuth oxide,<sup>12</sup> and copper oxide.<sup>13</sup> Besides, other simple photocatalysts have also been successfully produced, such as phosphorus, boron, sulphur as well as their composites and polymers.<sup>14</sup>

In the meantime, photocatalytic membrane technology offers a cost-effective alternative as water treatment, which is composed of a flexible way for its usage and shows a powerful capacity of pollutant removal. Thus, it offers sustainable life with safe water. This process only uses a lower amount of energy and easy operation, which helps in saving the environment. In the past few research studies, membrane technologies have revealed its significance in various applications, such as in haemodialysis for blood purification,<sup>15</sup> biotechnology, food processing,<sup>16</sup> oil-water separation,<sup>17</sup> filtration system for drinking water and wastewater treatment. Membranes can be prepared in the form of a polymer structure based on their pore sizes and features.

However, when particles, proteins or colloids are deposited on the surface or in the pores of membrane, it tends to experience membrane fouling, which leads to lower permeation flux and reduces the life span of the membrane. The most unexpected phenomenon is when the fouling is permanent due to the chemisorbance of the foulant on the surface and in the pores of the membrane. According to the researchers, the main cause of the fouling is because the nature of the membrane is hydrophobic. According to Bellardita *et al.*,<sup>9</sup> coupling photocatalysis with a polymeric membrane shows better operation for the photodegradation process, and can minimize the fouling problems. Moreover, an immobilized photocatalyst with a polymeric membrane is better than a suspended photocatalyst to prevent any suspensions left behind in the water after filtration process. Most of the previous reviews only showed a general explanation about the polymeric membrane doped with certain nanoparticles for various wastewater treatments. As stated by Kim and Bruggen,<sup>18</sup> the review explains more on the types of nanoparticles used with a polymeric membrane, instead of the immobilization method.

Compared to other previous reviews, this article explains a critical overview on the step-by-step preparation of functionalized photocatalysts incorporated with a polymeric membrane with various techniques that only focuses on the photocatalytic activity. To highlight their technical applicability, various parameters have been discussed, including the specific procedure, structure, pore size and surface area of the immobilized photocatalytic membrane for every technique.

This paper focuses only on the polymeric membrane, instead of the ceramic membrane, because the photocatalyst can be immobilized both into and onto the polymeric membrane. Meanwhile, the photocatalyst can only be deposited onto the

surface of the ceramic membrane. This is because the photocatalyst is not recommended for immobilization into the ceramic membrane due to the higher temperature of the sintering process that may demolish the photocatalyst. This review also presents the best methods for immobilizing the photocatalyst into the polymeric membrane (mixed matrix membrane) and for deposition of the photocatalyst onto the polymeric membrane's surface (coating), which may provide a potential outlook for the future photocatalytic technology. The development of the photocatalytic membrane technology may lead to a sustainable environmental purification technology due to the purification without using fossil fuels or harmful chemicals. Not only for water treatment, this technology also can be implemented for wider applications, including air-purification, deodorization, antifouling, antifogging and freshness maintenance.<sup>19</sup>

## 2. Photocatalytic membrane

### 2.1 Photocatalysis

In the fundamentals of chemistry, the catalyst is referred to as a substance that is used to speed up the reaction in a chemical process. Photocatalysis has been known as one of the successful methods in water and wastewater treatment. The photocatalysis method is well known as 'photoactivated', and resembles the potentiality of the photocatalyst to perform under the radiance of light based on the active site available at the photocatalyst itself.<sup>20</sup> The photocatalyst can be divided into two types, which are the homogenous photocatalyst and heterogeneous photocatalyst, as can be seen in Table 1. According to Baruah *et al.*,<sup>21</sup> homogenous photocatalysis is when the photocatalyst and medium react in the same phase. In contrast, if the photocatalyst and reaction medium are not in the same phase, it can be called heterogeneous photocatalysis. Heterogeneous photocatalysis is better than homogenous photocatalysis due to the easier separation of the used catalyst after application. Moreover, the heterogeneous photocatalyst is more effective in the removal of pollutants because it employs a renewable solar energy that leads to green technology to solve environmental problems.<sup>22</sup> For example, a photocatalyst in the solid phase and a reactant pollutant in the liquid phase will be easily adsorbed and degraded in heterogeneous photocatalysis. The significance of the photocatalytic reaction is how it harvests the solar energy to produce more charge carriers, and escalates the exploitation of the charge carriers in the redox reaction.<sup>23</sup> In this technology, the ideal photocatalyst is needed to exhibit efficient photocatalytic behaviour, including good photogenerated charge carrier separation, broad light absorption and higher stability, as well as reusability.<sup>22</sup> However, the charge carrier recombination ratio, lower reduction potential and photo-corrosion can affect the efficiency of the degradation process.<sup>24</sup>

According to the photocatalytic reaction theory, there needs to be photoexcitation that occurs by visible light, UV light or infrared light, depending on the particular energy band gap through the redox reaction. An example of a fundamental theory of how the photocatalytic reaction occurs is revealed in eqn (1.1)–(1.8). When light energy penetrates the photocatalyst, the electrons ( $e^-$ ) in the valence band (VB) will be excited to the



Table 1 Difference between the homogenous and heterogeneous photocatalysts

Homogenous photocatalyst	Heterogeneous photocatalyst
Photocatalyst and medium reacted in same phase	Photocatalyst and medium reacted in different phase
Difficult to separate from solution after reaction	Easier separation after application
Absorb narrowly within solar spectrum	High activity and non-toxicity
Photocatalytic ability and stability are limited	Stability in aqueous phase
Examples: ruthenium and iridium polypyridyl complex	Examples: semiconductor $\text{TiO}_2$ , $\text{Cu}_2\text{O}$ , $\text{Ag}_2\text{O}$ , $\text{ZnO}$

conduction band (CB), producing holes ( $\text{h}^+$ ) in VB. Thus,  $\text{e}^-$  and  $\text{h}^+$  will be encountered in the redox reaction.<sup>10</sup> During the process, water will dissociate into oxygen ( $\text{O}_2$ ) and hydrogen ( $\text{H}^+$ ) by photoexcitation of the electron, which leaves the holes. Then, the absorption of energy that is either greater than or equal to its band gap occurs by a semiconductor. There are three stages of water splitting, of which the first stage is the absorbance of energy and  $\text{e}^-/\text{h}^+$  generated by photoexcitation. The second stage is the separation of charges at the opposite sides by minimal recombination, and the last stage consists of charge carriers triggering the oxidation and reduction at the VB and CB, respectively. The oxidation of holes towards the hydroxyl ion in water will produce a hydroxyl radical that will then degrade the pollutant, forming  $\text{CO}_2$  and  $\text{H}_2\text{O}$ . The schematic diagram of the basic photocatalysis can be seen in Fig. 1 for further understanding. It indicates how the process of the photocatalyst reacts with light in order to degrade the pollutant, which results in the purification of water.

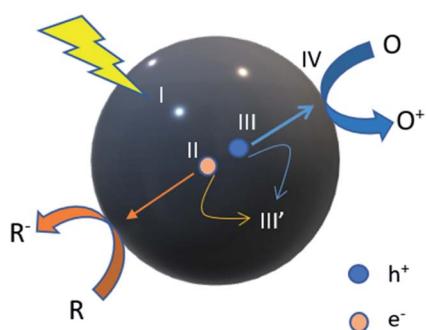
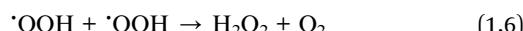
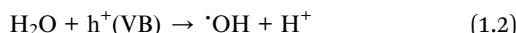


Fig. 1 Steps in the photocatalytic reaction process. R: chemicals in the reductive reaction, O: chemicals in the oxidative reactions. (I) Absorption of light to generate electron–hole pairs; (II) separation of excited charges; (III) holes ( $\text{h}^+$ ) and electron ( $\text{e}^-$ ) transfer to the photocatalyst surface; (III') recombination of electrons and holes; (IV) utilization of charges on the surface for redox reactions.

The significant characteristics in determining a good photocatalyst that can react under light irradiation are their physical and chemical stability, inexpensiveness, availability, oxidative capability and non-toxic nature.<sup>25</sup> The most outstanding photocatalyst that been used in the past literature is titanium dioxide ( $\text{TiO}_2$ ), whether in suspended form or immobilized into or onto the membrane.  $\text{TiO}_2$  has been chosen by most previous research groups as a photocatalyst due to the longer timespan of the electron–hole pairs, stability for a wide range of pH values, higher catalytic activity and known property as a cost-effective material.  $\text{TiO}_2$  can be confirmed as an effective photocatalyst under irradiation of UV light at wavelengths less than 400 nm due to its larger band gap of  $\text{TiO}_2$ .<sup>26</sup> However,  $\text{TiO}_2$  cannot be used under visible light irradiation due to its wide band gap. To overcome this problem,  $\text{TiO}_2$  must be doped with another narrow band gap photocatalyst, or the small band gap photocatalyst should be used alone in order to react effectively under visible light. There are photocatalysts with tunable band gaps that can be used, such as  $\text{ZnO}$ ,<sup>27</sup>  $\text{Cu}_2\text{O}$ ,<sup>28</sup>  $\text{Ag}$ ,<sup>29</sup>  $\text{Bi}_2\text{O}_3$ ,<sup>30</sup> carbon nanotubes,<sup>31</sup> and others.

Photocatalysis provides a good replacement for energy-saving treatment methods by using renewable and pollution-free solar energy. The process also offers the demolition of a variety of dangerous compounds, which lead to the formation of harmless products. In addition, the reaction condition requires less chemical input and minimal secondary waste generation. Not only for water treatment, photocatalysis can also be applied for the generation of hydrogen, gaseous phase and solid phase treatments.<sup>32</sup> Photocatalysis also has challenges in terms of the inhibition of the charge carrier recombination, charge separation and interfacial charge transfer.

## 2.2 Polymeric membrane

The various materials that have been successfully used in the fabrication of polymeric membranes are polyvinylidene fluoride (PVDF), polysulfone (PSF), polyether sulfone (PES), polyacrylonitrile (PAN), polyvinyl alcohol (PVA) and polyethylene (PE). Table 2 summarizes the various types of polymer membranes with their physical–chemical properties. The polymer membrane is widely used in industry due to its outstanding features, such as low cost, high mechanical strength, stability and flexibility.<sup>33</sup> In addition, the polymer membrane is also available in various configurations in order to achieve higher



Table 2 Various types of polymer membranes

Material	Physical-chemical properties	References
Polyvinylidene fluoride (PVDF)	High thermal stability Good chemical resistance Excellent mechanical property Withstands corrosive environment	38
Polyacrylonitrile (PAN)		39
Polyethersulfone (PES)	Better chemical & thermal stability Less hydrophobic	40
Polypropylene (PP)	Hydrophobicity Good thermal evaporation Better water flux	41
Polytetrafluoroethylene (PTFE)	Hydrophobic Narrow pore size Better porosity Excellent mechanical strength	22

performance of the membrane filtration. These configurations include the flat sheet, spiral, and hollow membrane, which play significant roles in producing the structure and characteristics of efficient membranes. Among these configurations, the flat sheet is the easiest to be fabricated. However, it experiences a lower surface area. Apart from that, the spiral configuration gained interest due to the higher surface area. Unfortunately, it also faces drawbacks, such as its ease of being clogged by particulates. Apart from that, the hollow fibre membrane configuration offers higher mechanical stability, higher surface area and ease in fabrication, as well as suitability for photocatalyst support.<sup>6</sup> The polymeric membrane can be formed for microfiltration (MF), ultrafiltration (UF), nanofiltration (NF), and reverse osmosis (RO).<sup>34</sup> The pore size of MF is between 0.1–10 µm, while UF is between 0.01–0.1 µm.<sup>35</sup> Besides, the pore size of NF is around 1 nm, which is capable of removing small particles, such as dyes.<sup>36</sup> Usually, MF is used for the removal of suspended solids, organic colloids, and bacteria, while UF is capable of removing pathogens, viruses and colloids.<sup>37</sup> The different characteristics between microfiltration, ultrafiltration and nanofiltration polymeric membranes that have been discussed is summarized in Table 3. There are various methods to fabricate polymer membranes, including electrospinning, sintering, template leaching, stretching, track-etching and phase inversion. Phase inversion is a simple technique, which can be used in fabricating various types of polymers with a variety of membrane configurations. Besides, various diameters and structures of membranes can be fabricated with easy operation by electrospinning. However, it possesses a slow speed yield of membrane. Other methods, namely sintering and

stretching, are capable of producing stable microfiltration polymeric membranes with certain types of polymers, namely PE and PTFE. Although this method does not involve a solvent, it needs a higher temperature during the procedure. Besides, the track-etching method shows an advantage because it can produce both microfiltration and ultrafiltration polymeric membranes. However, it also encounters a drawback due to its costly method, which is the same as the template leaching method. Table 4 summarizes the advantages and disadvantages of these methods.

### 2.3 Photocatalytic membrane

Recently, the photocatalytic membrane has become a promising technology to overcome the drawbacks of photocatalysis in terms of the suspended photocatalyst during the membrane separation process. According to Molinari *et al.*,<sup>43</sup> the suspended photocatalyst shows advantages, such as a higher surface area, which lead to higher photocatalytic efficiency. However, the photocatalyst used in the suspended nanosized photocatalyst encountered drawbacks in the recovery process, and was left behind in water during the filtration process. Therefore, it can cause membrane fouling that reduces the permeate flux, which lowers the photocatalytic activity. Moreover, the recovery of the photocatalyst after the separation process may require high-cost treatment and be more time-consuming.

The photocatalyst comes with different structures, including fine particles, powders, granules and a solid metal target. For a photocatalyst immobilized into the polymer membrane, a powdered photocatalyst is preferred. The powdered

Table 3 Different characteristics of polymer membranes<sup>42</sup>

	Microfiltration (MF)	Ultrafiltration (UF)	Nanofiltration (NF)
Thickness of separating layer	10–150 µm	0.1–1.0 µm	0.1–1.0 µm
Pore size	0.1–10 µm	0.01–0.1 µm	1–10 nm
Molecular separation size	Solids: >0.1 µm Particle separation	Solids: >0.5 µm Macromolecule separation	Solids: >0.001 µm Low-MW solute separation
Operating pressure	0.1–3 bar	0.5–10 bar	2–40 bar
Separating mechanism	Separation based on particle size		Separation based on difference in solubility and diffusivity
Module types	Spiral-wound, hollow fibre, tube, plate or cushion module		Spiral-wound, tube or cushion module



Table 4 The various methods used for fabricating the polymer membrane

Fabrication methods for membrane	Advantages	Disadvantages
Phase inversion	<ul style="list-style-type: none"> <li>• Increase speed yield</li> <li>• Better porosity</li> <li>• Simple</li> <li>• Flat-sheet and tubular membrane configuration</li> <li>• Broad polymer variety fabrication</li> </ul>	• Solvent needed
Electrospinning	<ul style="list-style-type: none"> <li>• Better versatility in controlling nanofiber diameter and structure</li> <li>• Easy operation with additive</li> <li>• Easy process</li> </ul>	• Slow speed yield
Sintering	<ul style="list-style-type: none"> <li>• Solvent not needed</li> </ul>	<ul style="list-style-type: none"> <li>• Difficult to achieve smaller pores below 100 nm</li> <li>• Lower porosity</li> <li>• High temperature needed</li> </ul>
Stretching	<ul style="list-style-type: none"> <li>• Produce 0.1–10 micrometre pore size</li> <li>• Chemically stable for polytetrafluoroethylene (PTFE) and polyethylene (PE)</li> <li>• Produces 0.1–3 micrometre pore size</li> <li>• Porosity (60–80%) with ladder-like slit shape</li> <li>• Chemically stable for PTFE and PE</li> </ul>	• High temperature needed
Track-etching	<ul style="list-style-type: none"> <li>• Produces 0.02–10 micrometre pore size</li> <li>• Narrow pore size distribution</li> <li>• Produces cylindrical pore shape</li> </ul>	<ul style="list-style-type: none"> <li>• Low porosity</li> <li>• Expensive</li> <li>• Limited polymer</li> </ul>
Template leaching	<ul style="list-style-type: none"> <li>• Produces 0.1–10 micrometre pore size</li> <li>• High flux</li> </ul>	<ul style="list-style-type: none"> <li>• Difficult to obtain nano pores</li> <li>• High cost</li> <li>• Complex process</li> </ul>

photocatalyst can be obtained by purchasing a commercial photocatalyst or by synthesis process, such as co-precipitation and sol-gel method. The commercial or synthesized photocatalyst was dispersed inside the polymer dope solution, and mixed homogenously to prevent agglomeration of the particles. Usually, for the mixed matrix membrane, a mixture of the polymer and photocatalyst was used as the main materials for fabrication. From the structure, it was observed that small particles were distributed inside the polymer matrix. Different from the deposition method, the fabricated polymeric membrane became a substrate or support for photocatalyst landing. For the deposition method, powdered or metal (target) photocatalyst may be used. For example, the polymeric membrane will be used as a substrate to be coated with photocatalyst dope solution by dip coating and electrospraying. For the sputtering method, the metal target will be used as a photocatalyst and deposited on the surface of the polymeric membrane by ejection of metal atoms. Hence, a layer of photocatalyst will be formed on the surface of the polymeric membrane. Furthermore, the photocatalyst only attaches on the surface without entering the polymeric membrane matrix.

For immobilization of the photocatalyst into the polymeric membrane, light will reach the polymeric membrane first before entering and being absorbed by the photocatalyst. In contrast, for immobilization of the photocatalyst onto the polymeric membrane, light will directly penetrate the photocatalyst layer attached on the surface of the membrane without reaching and entering the membrane. Fig. 2 indicates the illustration of light penetration towards the photocatalyst immobilized into and onto the polymeric membrane.

The chemical and physical nature of the photocatalyst and membrane surfaces act as significant factors in the interaction

between the photocatalyst and polymeric membrane.<sup>44</sup> It is critical to know how the photocatalyst interacts with the polymeric membrane for the membrane-binding photocatalyst. Based on a previous study in the literature explained by Rasch *et al.*,<sup>45</sup> the interaction between gold (Au) nanoparticles and the cell membrane has been studied. Au nanoparticles were observed to penetrate and embed the hydrophobic region ( $\text{L-}\alpha\text{-phosphatidylcholine}$ ). The accumulation and incorporation of nanoparticles at one side of the vesicle occurred due to the energy expended during this process, as can be seen in Fig. 3. Moreover, the larger number of embedded nanoparticles in the bilayer can be explained by considering the strong driving force that contributes to the nanoparticle insertion. The free energy change  $\Delta G_{\text{solv}}$  to fit the hydrophobic modified Au nanoparticles into the hydrophobic cell membrane from the water phase was found to be  $\pi D^2 \gamma$ , where  $D$  and  $\gamma$  are the diameter of the nanoparticle and liquid-vapor surface tension of water,

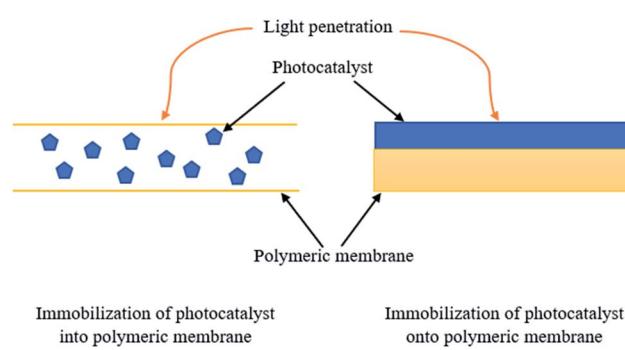


Fig. 2 Illustration of light penetration towards the photocatalyst immobilized into and onto the polymeric membrane.



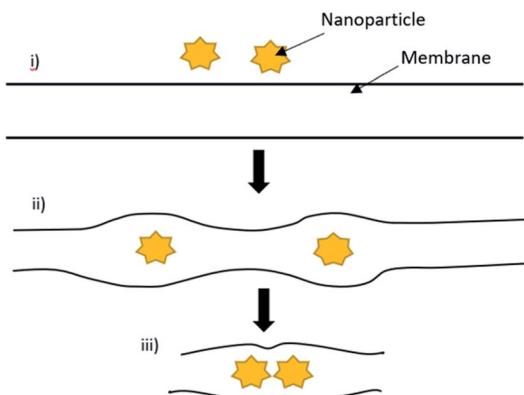


Fig. 3 (i) Insertion of the hydrophobic nanoparticle into the lipid bilayer leads to membrane deformation. (ii) Two nanoparticles present in the bilayer, and (iii) aggregation of the nanoparticles.

respectively. The accumulation of nanoparticles and the cell membrane may create voids around each individual nanoparticle. The voids form clusters by attracting other nanoparticles, and this clustering phenomenon may be known as the interparticle interaction.<sup>46</sup> Moreover, it is stated that strong van der Waals forces is the cause of the clustering of the nanoparticle during the heating process. The repulsive force at the gel phase and attractive force at the fluid phase specify that the embedded nanoparticles undergo clustering spontaneously during the heating process, while declustering during the cooling process.

Besides, adsorption or the particles' charge could also be one of the interaction modes between the photocatalyst and polymer membrane. For example, the photocatalyst and membrane must exhibit different charges, so that the electrostatic interaction can take place. Thus, the nanoparticles can embed inside the polymeric membrane or attach onto the membrane surface. According to Chen *et al.*,<sup>47</sup> a positively charged polymer with negatively charged nanoparticle uses electrostatic attraction as the driving force, and tends to increase the rigidity and alter the permeability.

If there is an interaction between the nanoparticles and polymeric membrane, the morphology is strongly decided by the charge and size of the interacting components.<sup>48–52</sup> Moreover, the higher loading of the nanoparticles by adsorption or incorporation into the polymeric membrane may be due to their higher stability.<sup>49</sup> When the nanoparticles with a size up to 100 nm interact with the polymeric membrane, dissimilar behaviour may be observed. It is stated that hydrophilic nanoparticles are immobilized onto or into the membrane, while hydrophobic nanoparticles can only be immobilized into the membrane with difficulty, as the membrane is destroyed when a higher loading of nanoparticles has been applied.<sup>53–55</sup> According to Krack *et al.*,<sup>56</sup> the mass ratio  $r = m_n/m_p$  of the nanoparticles, where  $m_n$  is the nanoparticle, while  $m_p$  is the polymer. It needs to be less than the critical ratio  $r^* \approx 0.2$  to 0.3; otherwise, agglomeration of the polymer/nanoparticles will occur. The nanoparticle decoration of the polymeric membrane interface can induce the bridge formation from one bilayer to an adjacent bilayer, resulting in bilayer pairing, as can be seen in Fig. 4 below.<sup>57</sup> Furthermore, when the hydrophobic

nanoparticles were introduced, it tended to increase the membrane thickness and enhance the mechanical strength.

Incorporating the photocatalyst into the polymeric membranes has been widely implemented in previous studies due to their hydrophilicity to minimize fouling, provide strength, as well as increase the permeability.<sup>6</sup> Previous research also concluded that by adding particles or a catalyst into the polymer matrix, the polymeric membrane became more stable due to the perm-selectivity and temperature changes. Moreover, by immobilising the photocatalyst onto the support (such as a polymeric membrane), it can prevent the post-separation obstacle correlated with the powdered photocatalyst.<sup>58</sup> Therefore, the performance of the photocatalytic technology can be increased as the polymeric membrane becomes the support for the photocatalyst, and also act as a membrane barrier for the removal of pollutants.<sup>59</sup> An illustration of the immobilized photocatalyst on the surface coated and embedded membrane with an illustration of the light illumination is shown in Fig. 5. The overview flow chart of the immobilized technique of the photocatalyst with a polymeric membrane in this study is revealed in Fig. 6. There are two techniques of deposition: either into or onto the substrate. Deposition into the membrane is called a mixed matrix membrane, while deposition onto the substrate membrane is referred to as coated membrane. This study will discuss the deposition of the photocatalyst into the polymeric membrane by dry-wet spinning, electrospinning, tape casting and spin coating. Meanwhile, deposition of the photocatalyst onto the surface of the membrane is composed of sputtering, dip coating, electrospraying and atomic layer deposition.

### 3. Photocatalyst immobilization method

#### 3.1 Deposition into the membrane structure

Basically, the polymer was mostly used as a support for the immobilized photocatalyst blended with the membrane or called as a mixed matrix membrane. By blending the photocatalyst into the membrane, it can be one of the efficient techniques in controlling the hydrophilicity of the membrane and prevent fouling.<sup>60</sup> This technique can reduce photocatalyst leaching, which contributes to the benefit of this membrane. Moreover, this technique offers advantages, including the low use of energy and better reusability.<sup>61</sup> However, some literature found that this technique also encountered a drawback, such as

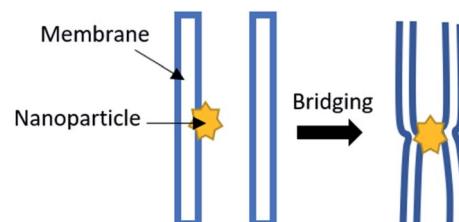


Fig. 4 Nanoparticle decorating the interface of the polymeric membrane, which induces the bridge formation.



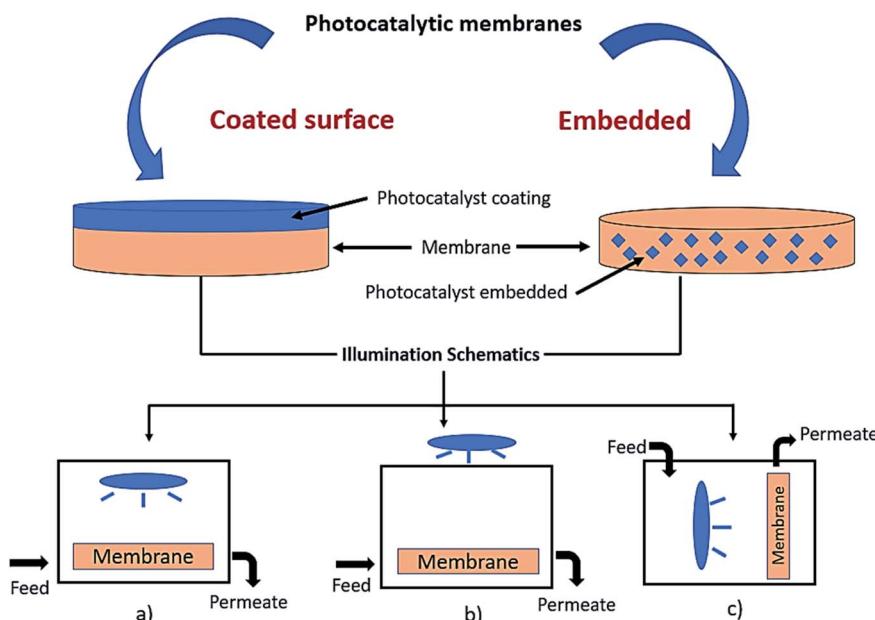


Fig. 5 Illustration of the immobilized photocatalyst on the surface and embedded membrane. Illustration of light illumination of the: (a) light source inside the reactor, (b) light source outside the reactor, and (c) vertical light source and membrane inside the reactor.

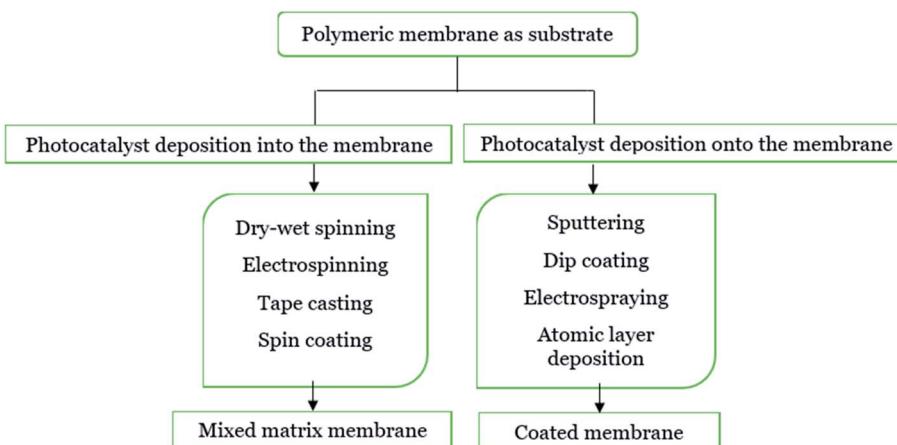


Fig. 6 Immobilization technique of the photocatalyst into/onto the polymeric membrane.

agglomeration of the photocatalyst inside the membrane. To obtain a mixed matrix membrane that blends with the photocatalyst, methods (including wet spinning, sintering and electrospinning) can be done.<sup>3</sup> Prepared polymer mixed matrix membranes (MMMs) have been reported in past research studies for dye removal using N-doped polyvinylidene fluoride (PVDF) hollow fibre membranes<sup>62</sup> and polysulfone (PSF)/N,Pd co-doped TiO<sub>2</sub> composite membranes,<sup>63</sup> ibuprofen degradation using a Cu<sub>2</sub>O/PSF membrane,<sup>28</sup> pollutant removal using a polyether sulfone (PES)-fGo mixed matrix membrane,<sup>64</sup> ammonium removal using the zeolite-doped PSF membrane,<sup>65</sup> 2,4-dichlorophenol degradation using the Co/TiO<sub>2</sub>-PES membrane<sup>66</sup> and nonylphenol removal using the TiO<sub>2</sub>/PVDF dual layer hollow fibre membrane.<sup>67</sup> A diagram of the mixed matrix membrane is illustrated in Fig. 7, while the SEM image of

the photocatalyst dispersed in the polymeric membrane is shown in Fig. 8.

**3.1.1 Dry-wet spinning and dry-wet co-spinning technique.** Titanium dioxide (TiO<sub>2</sub>) is a well-known metal oxide that

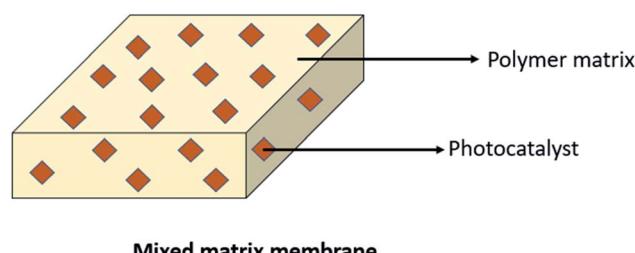


Fig. 7 Diagram of the ideal mixed matrix membrane.



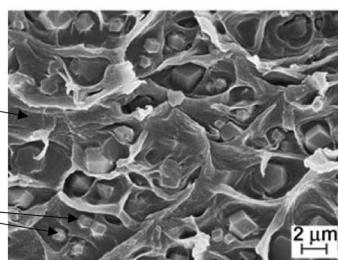


Fig. 8 SEM image of the photocatalyst dispersed in a polymeric membrane.<sup>68</sup>

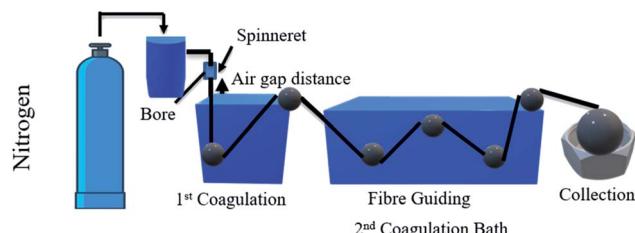


Fig. 9 Schematic diagram of the dry–wet spinning system for the single layer hollow fibre membrane.

has widely been used as a photocatalyst in photodegradation due to its outstanding characteristics, including good chemical stability,<sup>69</sup> safe to the environment, and low cost. It also has excellent oxidation capability to enhance the pollutant's degradation efficiency.<sup>70</sup> The polymeric membrane has gained much interest from the past literature as a landing support for  $\text{TiO}_2$  that acts as a photocatalytic membrane. The single layer photocatalytic polymeric hollow fibre membrane can be fabricated by dry–wet spinning technique using a single spinneret,<sup>71</sup> as shown in Fig. 9, while the dual layer of the membrane can be fabricated by dry–wet co-spinning technique using a triple orifice spinneret, as shown in Fig. 10. In addition, the single layer membrane only needs one dope solution. In contrast, the dual layer membrane needs inner and outer dope solutions.

The difference between the single layer and dual layer hollow fibre can be seen in Table 5.

Otitoju *et al.*<sup>72</sup> explained the fabrication of the single layer hollow fibre membrane. A mixture of the photocatalyst, namely  $\text{CaCu}_3\text{Ti}_4\text{O}_{12}$  (CT), with PVP, PES and DMAc was stirred for 24 hours as the dope solution, which was later used in the spinning system to produce the hollow fibre mixed matrix membrane. 18% of PES and a different percentage of CT were used as the dope composition. During the spinning process, the air gap used was 23.5 cm, distilled water as the bore fluid, 17 rpm for the gear pump, and the external diameter of spinneret was 0.6 mm. SEM images in Fig. 11 show the porous finger-like structure. A white cluster of CT nanoparticles can be seen on the surface of the membrane. The higher the amount of CT powder, the higher the white cluster of CT observed. Table 6 states the pore volume, pore diameter and surface area of the PES-CT membrane evaluated using  $\text{N}_2$  adsorption–desorption isotherms by BET analyzer. According to this study, the results show the increasing number of pore volume, pore diameter and surface area due to the increasing amount of CT powder. Thus, the photocatalytic activity was enhanced due to the larger surface area and high hydrophilicity. However, it might be different with other studies because the types of nanoparticles used are based on the nanoparticle size and other properties. A larger surface area of the membrane enhances the illumination of UV light, so that it improves the contaminant absorption. Besides, the porous membrane structure makes it easier for the contaminants to be entrapped in the pores. Therefore, there was a great chance for the photogenerated electron hole pairs to react with the contaminants. The photocatalytic mixed matrix membrane successfully degraded 74.83% of Rhodamine B under 360 W UV-C light irradiation.<sup>72</sup> However, when the CT powder was 4 wt% in C4, the pore volume, pore diameter and surface area started to decrease due to the higher amount of CT, leading to the aggregation of particles in the pores. According to Naushad *et al.*,<sup>73</sup> the undesirable light scattering or blocking of light may happen when the catalyst concentration used is too high. Moreover, the catalyst may be agglomerated at a higher concentration, which leads to the photocatalyst surfaces not

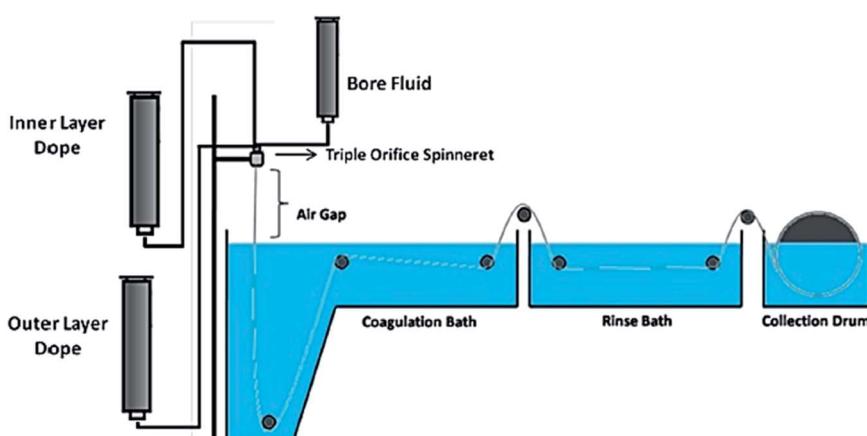


Fig. 10 Schematic diagram of the dry–wet–co spinning system for the dual layer hollow fibre membrane.<sup>62</sup>



**Table 5** Difference between the single layer and dual layer hollow fibre

Type	Single layer	Dual layer
System	Dry-wet co-spinning	Dry-wet spinning
Spinneret	Single	Triple orifice
No. of dope	One	Two
Application	Degradation Filtration	Outer-degradation Inner-filtration

being exposed completely during photocatalysis. Thus, there is a decrease in the degradation efficiency.

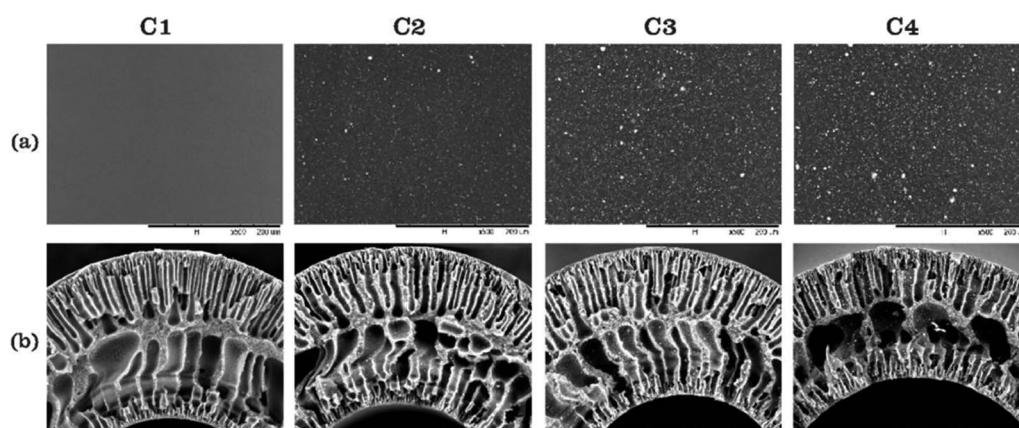
According to Dzinun *et al.*,<sup>67</sup>  $\text{TiO}_2$  has been chosen as an effective photocatalyst to be deposited onto the single layer and dual layer of the PVDF hollow fibre membrane in the photo-degradation of nonylphenol under UV light irradiation. The single layer polymeric membrane was fabricated when 7.5 wt% of  $\text{TiO}_2$  was mixed with PVDF and DMAc as the inner dope composition. From the SEM image in Fig. 12(b), the single layer hollow fibre membrane displays the agglomeration of  $\text{TiO}_2$  particles due to the higher loading of  $\text{TiO}_2$  that leads to less hydrophilic nature. For the dual layer photocatalytic polymeric membrane, a mixture of PVDF and DMAc acts as the inner dope composition, while the outer dope composition consists of  $\text{TiO}_2$ , PVDF and DMAc. The mixture of the inner and outer dope compositions was stirred well using an overhead stirrer until it became homogeneous. This technique can optimize the  $\text{TiO}_2$  dispersion and reduce the agglomeration problem. According to Dzinun *et al.*,<sup>67</sup> a lower amount of  $\text{TiO}_2$  particles was distributed well into the outer layer of the dual layer hollow fibre membrane than in the single layer, as shown in Fig. 12. Thus, no  $\text{TiO}_2$  diffusion into the inner layer was observed from the EDX analysis, as shown in this figure. As mentioned by Dzinun *et al.*,<sup>74</sup> the extensive spread of the  $\text{TiO}_2$  particles in the membrane matrix provides higher affinity of the metal oxide to water, which lead to more hydrophilicity. With the increase in the addition of  $\text{TiO}_2$  that was entrapped in the membrane, the performance of the photocatalytic degradation of nonylphenol

was around 85% using the dual layer, while 70% was achieved using the single layer under UV-A irradiation. Additionally, the uniform spread of  $\text{TiO}_2$  inside the polymer membrane led to the complete exposure of  $\text{TiO}_2$  towards light. This is due to the low amount of catalyst used that can prevent agglomeration, which can reduce the surface area.

Besides, Kamaludin *et al.*<sup>62</sup> stated in the paper that 75% of the Reactive Black 5 (RB5) dye was successfully degraded after 360 min using the N-doped  $\text{TiO}_2$ -PVDF dual layer hollow fibre membrane, which had a photocatalyst embedded inside the hollow fibre membrane. To produce the fabricated photocatalytic membrane, N-doped  $\text{TiO}_2$  was mixed with PVDF and PEG 6000 as the outer dope composition, while only PVDF and PEG 6000 were used as the inner dope composition. Both dope compositions were then transferred into the stainless-steel dope reservoir pump to produce the dual hollow fibre membrane. The triple orifice spinneret was used in the spinning system to extrude the dual hollow fibre membrane that acted as the mixed matrix membrane. The SEM images in Fig. 13 shows that the N-doped  $\text{TiO}_2$  nanoparticles with different weight percentages were evenly distributed on both membrane surfaces. However, when a higher amount of N-doped  $\text{TiO}_2$  nanoparticles was added to the dope solution, it resulted in a higher amount of nanoparticles distributed in the membranes. Thus, this resulted in agglomeration of N-doped  $\text{TiO}_2$  due to the higher surface tension between the solvent and N-doped  $\text{TiO}_2$  during the dope solution preparation. Moreover, when there was less hydrophilic DMAc contact with

**Table 6** The surface area, pore volume and pore diameter of the pristine and PES-CT composite membrane by BET isotherm<sup>72</sup>

Membrane type	Surface area ( $\text{m}^2 \text{ g}^{-1}$ )	Pore volume ( $\text{cm}^3 \text{ g}^{-1}$ )	Average pore diameter (nm)
C1	11.86	0.027	11.86
C2	14.45	0.032	23.10
C3	25.28	0.055	34.64
C4	23.22	0.053	32.47

**Fig. 11** SEM images of the (a) surface and (b) cross-section of the PES-CT composite membrane with a composition of CT powder at: (C1) 0 wt%, (C2) 1.25 wt%, (C3) 2.5 wt% and (C4) 4 wt%.<sup>72</sup>

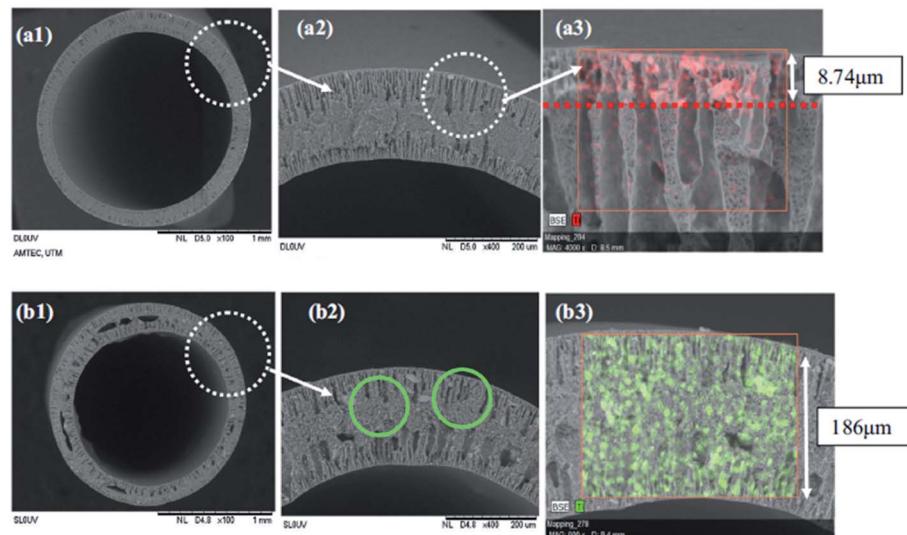


Fig. 12 The distribution of  $\text{TiO}_2$  particles in: (a) dual and (b) single layer of the PVDF hollow fibre membrane from SEM images.<sup>67</sup>

the hydrophilic N-doped  $\text{TiO}_2$ , it induced colloidal instability, which caused particle agglomeration. Agglomeration can cause the active site on the photocatalyst to be blocked from receiving light penetration, which leads to less photoabsorption of the catalyst. Thus, this change results in a reduction of the degradation rate of the pollutant.<sup>58</sup> Furthermore, the N-dopant remains attached to the  $\text{TiO}_2$  lattice, which is not affected by the high calcination. This results in no leaching during the fabrication process. Thus, it will strongly influence the photocatalytic activity. Between the single layer and dual layer hollow fibre membrane, the dual layer hollow fibre membrane provides

good dispersion of the nanoparticles compared to the single layer, which can minimize the problem of the nanoparticle agglomeration. Thus, it can increase the photocatalytic activity performance.

**3.1.2 Electrospinning.** Previously, the membrane fabrication technology known as electrospinning had successfully fabricated an electrospun mixed matrix membrane consisting of a mixture of photocatalyst and polymer. According to the previous literature, the electrospinning method provides the membrane with higher porosity and a larger surface area.<sup>75</sup> Therefore, it is stated that by electrospinning, the produced

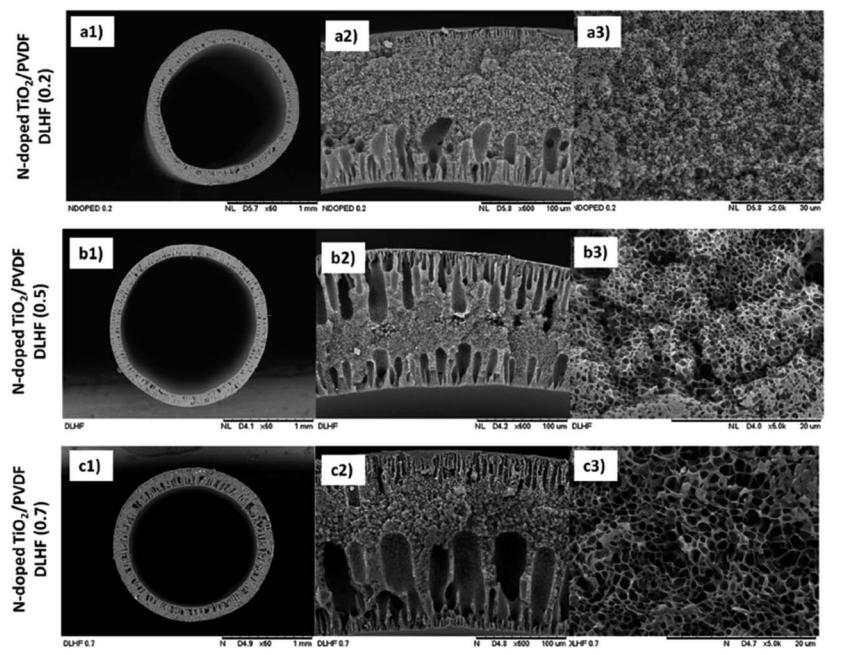


Fig. 13 SEM image of the: (a) 3.0, (b) 7.5, and (c) 10.5 wt% N-doped  $\text{TiO}_2$  in the PVDF dual layer hollow fibre membrane.<sup>62</sup>



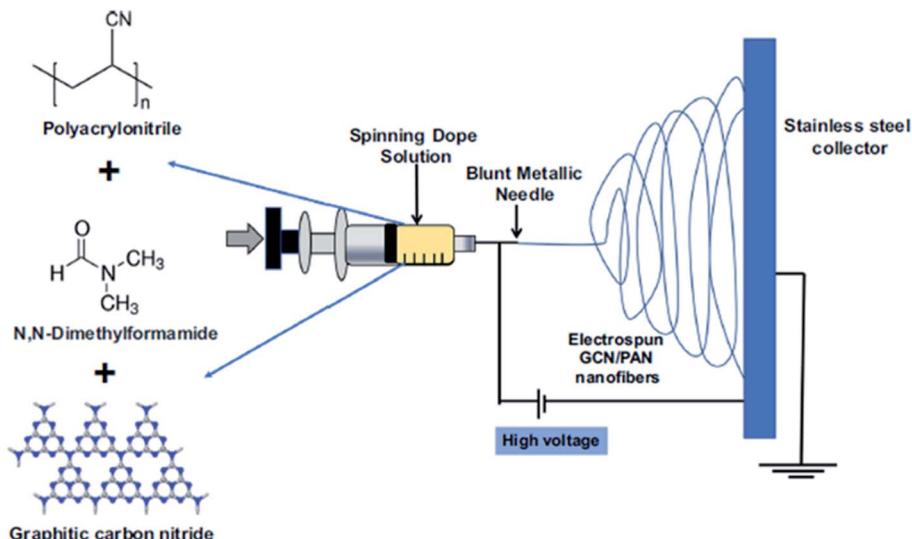


Fig. 14 Schematic diagram of the electrospinning method for the mixed matrix membrane.<sup>78</sup>

photocatalytic membrane will have better mechanical properties. The electrospinning system is illustrated in Fig. 14. A previous paper reported by Salazar *et al.*<sup>76</sup> showed that Ag-TiO<sub>2</sub>/polyvinylidene fluoride-hexafluoropropylene (PVDF-HFP) electrospun membranes were prepared by electrospinning for the photocatalytic degradation of norfloxacin under UV and visible light. The degradation rate of norfloxacin was about 64.2% under UV light in 90 min, while it was 80.7% under visible light for 300 min. Norfloxacin was degraded well under visible light, as well as UV light irradiation. This is due to the higher band gap energy of TiO<sub>2</sub> between 3.1–3.4 eV, which is suitable to be illuminated under UV light with a wavelength range of 100–400 nm.<sup>77</sup> Besides, when Ag was doped with TiO<sub>2</sub>, the band gap tends to slightly decrease to 2.9–3.0 eV, where it allows the photocatalyst to be irradiated by visible light at a wavelength range between 400 nm to 700 nm. TiO<sub>2</sub> nanocomposites were dispersed well in DMF, and PVDF-HFP was added afterwards. The prepared solution was poured into a syringe that was fitted with a 0.5 mm diameter steel needle. This procedure was operated by applying 14 kV voltage with a feed rate of 0.4 mL h<sup>-1</sup>. The electrospun product was collected in an aluminium plate with the distance between the needle and plate at 20 cm. By electrospinning, the membranes obtained were highly porous, non-woven fibres, and interconnected pores were formed. Fig. 15(a) indicates the smooth surface of PVDF-HFP without the presence of beads with an average diameter of

0.24  $\mu$ m. In contrast, Fig. 15(b and c) show the wrinkled surface with a high average diameter of 0.32  $\mu$ m due to the accumulation of nanoparticles at the fibre surface. Although the membranes with the photocatalyst show high porosity, the active photocatalytic sites for norfloxacin adsorption and light radiation exposure decreased due to the encapsulation and aggregation of the TiO<sub>2</sub>/Ag nanoparticles. This is due to the blocking of the active site, which did not receive enough light penetration for the formation of the radical to degrade the norfloxacin.

According to Alias *et al.*,<sup>78</sup> graphitic carbon nitride (g-C<sub>3</sub>N<sub>4</sub>) powder was mixed with DMF and polyacrylonitrile (PAN) as a dope suspension. The dope suspension was then used in the electrospinning process with the voltage of 15 kV and flow rate at 1 mL h<sup>-1</sup>. The distance between the electrospinning needle and collector was 18 cm. The electrospun collector used in this study was a stainless steel plate coated with aluminum foil. A thin sheet of g-C<sub>3</sub>N<sub>4</sub>/PAN nanofibers was collected by peeling off the electrospun product at the collector by hand. The electrospun product was an interconnected open pore structure. The uniform distribution of g-C<sub>3</sub>N<sub>4</sub> along PAN was observed due to the nodule-less structure formed with a mean diameter of synthesized bulk graphitic carbon nitride (bg-C<sub>3</sub>N<sub>4</sub>) equal to 207 nm, while the nanosheet graphitic carbon nitride (nsg-C<sub>3</sub>N<sub>4</sub>) was 262 nm. In addition, bg-C<sub>3</sub>N<sub>4</sub> has numerous lumps due to the bulky shape embedded in the nanofibers. Therefore,

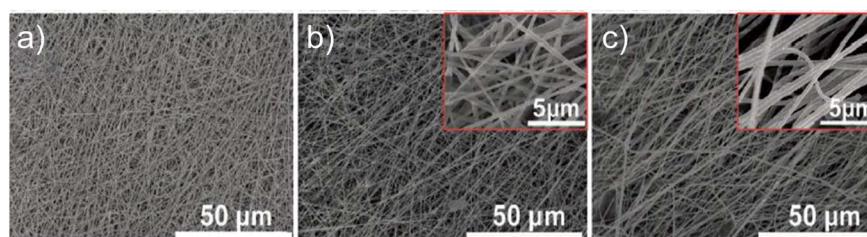


Fig. 15 SEM images of the electrospun (a) PVDF-HFP membrane, (b) TiO<sub>2</sub>-PVDF-HFP membrane, and (c) TiO<sub>2</sub>/Ag-PVDF-HFP membrane.<sup>76</sup>

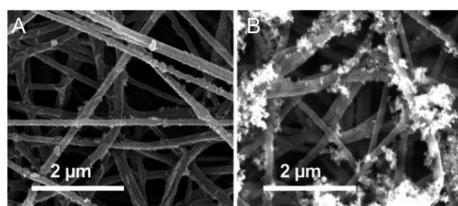


Fig. 16 SEM images of the: (A) 0.12 M colloidal  $\text{TiO}_2$ –PA-6 electrospun and (B) 0.50 M commercial  $\text{TiO}_2$ –PA-6 electrospun.<sup>80</sup>

nsg- $\text{C}_3\text{N}_4$  produced a uniform, smooth and straight length structure due to the lower number of lumps formed. The bulk properties are different from those of the nanosheet. The nano size of the photocatalyst shows better efficiency for water treatment and recycling ability due to their smaller size compared to the bulk photocatalyst. The smaller the catalyst size, the larger the numbers of atoms assembled, which lead to an increase in the surface to volume ratio. Moreover, it will enhance the number of active sites and interfacial charge carrier transfer rates. Thus, helps in increasing the catalytic efficiency.<sup>79</sup>

The other literature study that applied the electrospinning method in fabricating mixed matrix membranes can be seen through.<sup>80</sup> A mixed matrix membrane containing a polyamide-6 (PA-6) nanofiber, and the commercial and colloidal  $\text{TiO}_2$  photocatalyst has been successfully fabricated by electrospinning procedure, and successfully degraded up to 99% of methylene blue after 6 hours of UV illumination. Before the electrospinning process took place, the solutions of 16 wt% of PA-6 and 0.07 wt%, 0.30 wt%, 0.12 M and 0.50 M of  $\text{TiO}_2$  nanoparticles mixture were prepared first. The solution was poured into the multi-nozzle fed by syringe in order to produce the various thicknesses of the electrospun fiber membranes. The electrospinning procedure was operated at 20 kV voltage with the distance between the needle and collector at 10 cm. However, the higher concentration of the  $\text{TiO}_2$  nanoparticle can contribute to the agglomeration in the polymer membrane. This give a bad effect on the blending of the mixed matrix membrane during the spinning procedure, as can be seen in Fig. 16. When the amount of  $\text{TiO}_2$  was increased beyond the optimum concentration, the light penetration depth into the active site was reduced and consequently diminished the scattering of light. It is an insufficient amount of electrons to excite from the valence band to the conduction band to form holes,

which then reduces the redox reaction process. Thus, it reduces the photocatalytic activity.

**3.1.3 Tape casting.** Tape casting is one of the facile fabrications of the membrane, which produces the flat sheet membrane. The schematic diagram of this casting procedure is illustrated in Fig. 17. The immobilization of  $\text{TiO}_2$  in the PVDF membrane structures using the tape-casting method has attracted attention in recent studies as the photocatalytic membrane in the degradation of the methylene blue dye.<sup>58</sup> The literature written by Dzinun *et al.*<sup>58</sup> explains that the flat sheet configuration of the polymeric membrane was immobilized with  $\text{TiO}_2$  by using a knife-like tool in controlling the membrane thickness and dispersion of the polymer solution. SEM with 10k zoom images in Fig. 18 show the aggregation of 6 nm and 30 nm particle sizes of  $\text{TiO}_2$  at the outer membrane surface, causing the size of the membrane to become 385 nm and 568 nm. Thus, it reduces the surface area, resulting in the low performance of photodegradation due to the larger size of the  $\text{TiO}_2$  particle. When the size of the particles is larger, a small number of atoms accumulated, which then decreased the surface-to-volume ratio.<sup>79</sup> In the other literature study by Zangeneh *et al.*,<sup>81</sup> L-histidine (C,N-doped  $\text{TiO}_2$ –CdS) incorporated with a PES ultrafiltration membrane was fabricated by mixing the photocatalyst, PES and PVP as the casting solution. Then, the casting solution was cast onto a glass substrate with 150  $\mu\text{m}$  thickness. The glass substrate was then soaked into the distilled water bath to obtain the thin membrane film by peeling the fabricated membrane. The fabricated mixed matrix membrane was reported to successfully remove 65.26% COD at 3 bar and 150 L  $\text{h}^{-1}$  conditions under the irradiation of visible light.

Another literature study reported the fabrication of the flat sheet PSF/N, co-doped  $\text{TiO}_2$  membrane using the tape casting method in the degradation of 92% of eosin yellow dye under visible light irradiation.<sup>63</sup> Before casting the membrane, the photocatalyst was prepared using the sol-gel method.  $\text{Ti}(\text{OC}_3\text{H}_7)_4$  was mixed with 2-propanol to produce an isopropoxide/propanol solution, while  $\text{Pd}(\text{NH}_3)_2\text{Cl}_2$  was dissolved in ammonia to produce an ammoniacal solution. Then, the ammoniacal solution was mixed with the isopropoxide/propanol solution. After the sol was dried at 80 °C and calcined at 500 °C for 2 hours, the N,Pd co-doped  $\text{TiO}_2$  was obtained. The N,Pd co-doped  $\text{TiO}_2$  was then further used as the photocatalyst to be embedded with polysulfone, forming a photocatalytic polymeric membrane. The PSF pellet was dissolved in NMP, and N,Pd co-doped  $\text{TiO}_2$  was added and

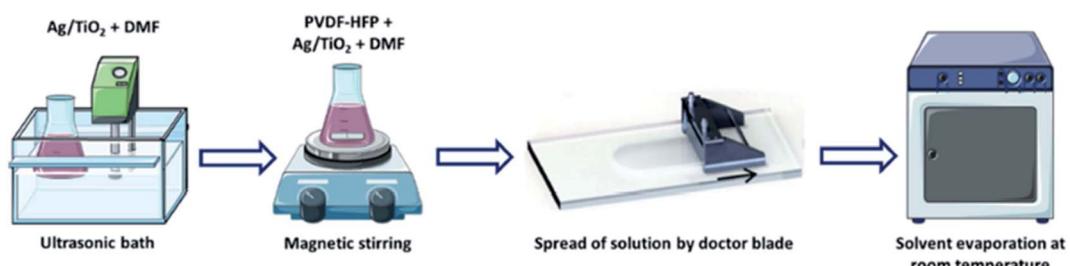


Fig. 17 Schematic diagram of the casting method of the mixed matrix membrane.<sup>76</sup>



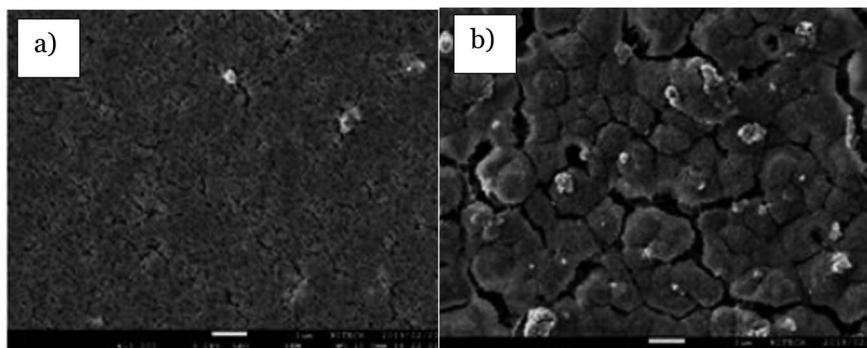


Fig. 18 SEM images of the tape casting membrane with: (a) 6 nm  $\text{TiO}_2$  and (b) 30 nm  $\text{TiO}_2$ .<sup>58</sup>

dispersed well in the dope solution. The dope solution was spread evenly on a clean glass plate by using a casting knife with a 250  $\mu\text{m}$  air gap. Then, the membrane was immersed in a deionised water bath. The membrane was obtained by peeling from the glass plate. The mixed matrix membrane was immersed in an ethanol/deionised water bath to remove the excess solvent, and then dried in air for 48 hours. According to the EDS characterization of the mixed matrix membrane, the N,Pd co-doped  $\text{TiO}_2/\text{PSF}$  mixed matrix membrane revealed that the photocatalyst embedded inside the membrane had a uniform dispersion without the formation of an agglomeration. However, nanomaterials have tendency to agglomerate in a medium of organic solvent or organic polymer body.<sup>82</sup> From the observation, a higher loading of 4% and 7% wt. of the photocatalyst inside the membrane in Fig. 19 caused the agglomeration of the nanoparticles at the near-outer surface

and within the membrane pores. This led to a higher surface roughness and increase in the contact angle of the membrane, as well as the low obtained surface area, which reduced the photodegradation performance. The concentration of the catalyst is one of the factors that influences the efficiency of the photocatalysis. If a very high concentration of photocatalyst was added, the photon blocking would occur and decrease the degradation rate.<sup>73</sup>

Besides, the  $\text{Cu}_2\text{O}/\text{PSF}$  ultrafiltration mixed matrix membrane was fabricated for photocatalytic ibuprofen removal.<sup>28</sup> This paper reported that 86% of ibuprofen was successfully removed under visible light irradiation. The mixed matrix membrane was prepared by dissolving the PSF, PEG and different amounts of  $\text{Cu}_2\text{O}$  in NMP solution as the membrane casting. The casting was evenly spread on a clean glass plate and peeled off after immersion in distilled water. According to the

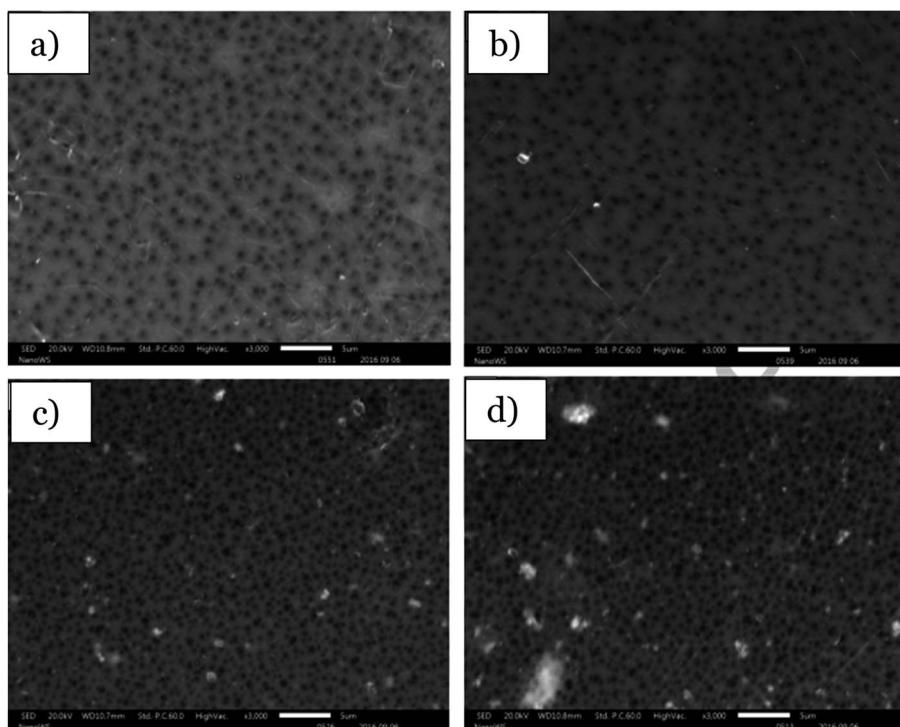


Fig. 19 SEM images of the tape casting of the PSF membrane with: (a) 1.0 wt%, (b) 2.0 wt%, (c) 3.0 wt% and (d) 4.0 wt% of N, co-doped  $\text{TiO}_2$ .<sup>63</sup>



FESEM micrograph, uniform pores were formed due to the significant role of the  $\text{Cu}_2\text{O}$  photocatalyst allowing the shrinkage of the polymer generated from mechanical stress during the casting process. Furthermore, the addition of  $\text{Cu}_2\text{O}$  inside the membrane enhanced the formation of a wider finger-like structure of mixed matrix membrane due to the hydrophilic nature of  $\text{Cu}_2\text{O}$  that improved the mass transfer solvent and non-solvent during the phase inversion procedure.<sup>83</sup> The intensity of the photons can have an impact on the degradation activity. When the intensity of the photons absorbed was higher, the reaction rate also increased. This is due to the greater photogenerated electron-hole pair concentration, which led to a greater radical formation and the occurrence of more photodegradation.<sup>73</sup>

The other literature study that explained this method was written by ref. 70, in which the paper indicates the fabrication of the  $\text{TiO}_2/\text{PVDF-HFP}$  and  $\text{Ag-TiO}_2/\text{PVDF-HFP}$  mixed matrix membrane using the casting procedure. The mixture between the photocatalyst and polymer was spread well on the glass substrate using a bar coater. Then, the solution was left at room temperature for 3 days to let the solvent evaporate and undergo the liquid-liquid phase separation process before the flat sheet membrane was crystallized. Smaller pores with a diameter between 1–8  $\mu\text{m}$  and larger pores formed by a double porous structure after the  $\text{TiO}_2$  nanoparticles were added can be observed from the SEM images in Fig. 20. When Ag was added with  $\text{TiO}_2$  into the membrane, the morphology showed that the pore diameter was reduced to between 1–4  $\mu\text{m}$ . Both morphologies did not show any agglomeration of nanoparticles formed in the membrane. From the photocatalytic study using UV light irradiation, norfloxacin was successfully degraded up to 45% and 64% for 3 wt%  $\text{TiO}_2/\text{PVDF-HFP}$  and  $\text{Ag-TiO}_2/\text{PVDF-HFP}$  flat sheet membranes, respectively. Comparing the  $\text{TiO}_2$  and  $\text{Ag-TiO}_2$  nanocomposites on the degradation performance, the  $\text{Ag-TiO}_2$  materials indicated higher degradation efficiency. This is due to the presence of Ag on the  $\text{TiO}_2$  surface reducing the electron/hole recombination rate.<sup>76</sup> Moreover, by tape casting the membrane, it helps to spread the photocatalyst well, which allowed the light to easily penetrate the active site of the photocatalyst to form an electron and holes for the redox reaction during photocatalysis.

**3.1.4 Spin coating (blended).** Spin coating is one of the methods in fabricating the thin sheet of membrane with high quality and uniform membrane film<sup>84</sup> by applying a viscous liquid on a horizontal rotating disc. This method can be divided into four processes, including deposition, spin-up, spin-off and evaporation process. First, a polymer solution was deposited

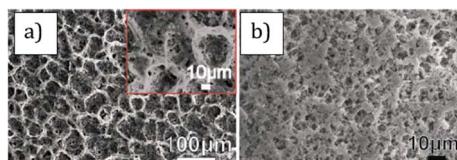


Fig. 20 SEM images of the flat sheet PVDF-HFP membrane with (a)  $\text{TiO}_2$  and (b)  $\text{Ag-TiO}_2$  nanoparticles.<sup>76</sup>

onto a centre of the spin coater, which is known as the substrate. This was then followed by rotating the substrate with high speed, leading to the liquid flow outwards due to the centrifugal force, or namely as spin-up stage. At the third stage or known as spin-off process, the excess polymer flowed outwards to the perimeter, and was ejected and formed accumulations. At the final stage, the polymer solution was evaporated, forming a thin solid membrane state. The spinning speed for the mass transfer kinetics during the spin coating procedure influences the membrane structure and photocatalytic performance. This method is visualized in Fig. 21.

Before this method was operated, the casting solution consisting of the photocatalyst and polymer was prepared first for further use in the spin coating procedure. The example of the preparation of the mixed matrix polymeric membrane using this method was explained by Dzinun *et al.*<sup>58</sup> About 3 wt% of  $\text{TiO}_2$  nanoparticles powder was mixed with 82 wt% of DMAc and 15 wt% of PVDF in a Scott bottle with a stirring speed of 400 rpm for 1 day, which was labeled as the casting solution. After that, the casting solution was further used in the spin coating method by dropping 2 mL of casting solution on a Petri dish with a spin coater (Aiden) at various spinning speeds for 30 s. The membrane produced was immediately immersed into a water bath, and went through post treatment by immersing the membrane into 50% of diluted ethanol for 1 hour, followed by 100% concentrated ethanol for another 1 hour in order to improve the wettability and pore collapse.<sup>58</sup> From this method, it is stated that the thickness of the membrane depends on different spinning speeds. The structure and outer surface of the produced membrane changes due to the process and solvent evaporation. The higher the spinning speed, the more the solvent evaporated, which led the film produced to become thinner. Moreover, by using this method,  $\text{TiO}_2$  was uniformly

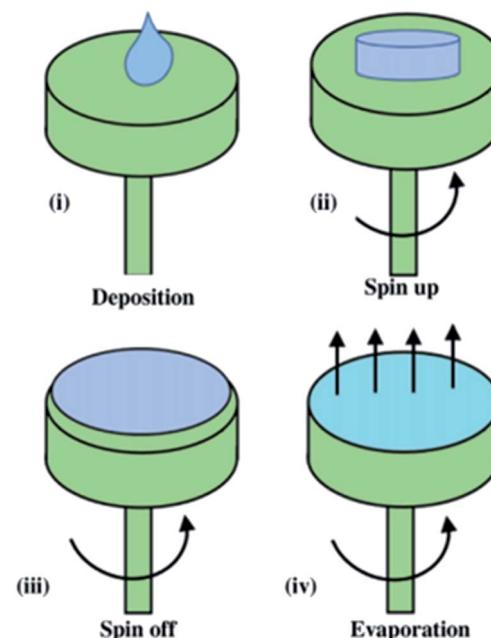


Fig. 21 Schematic diagram of the spin coating method.<sup>85</sup>



dispersed in the membrane through the centrifugal force produced by spinning effect. Therefore, the higher the spinning speed, the dispersion of the photocatalyst will be more uniform, as can be seen in Fig. 22. Furthermore, it is proved that by using the spin coating method, the membrane surface prepared was smoother than the tape casting method due to the liquid being spread evenly. In addition, the evaporation taking place is affected by the velocity of the rotating Petri dish. Besides, when the photocatalyst was evenly dispersed inside the polymer matrix, it would have a larger exposed area of photocatalyst to be irradiated with light. Hence, the light can penetrate the active site of the photocatalyst easily for the photodegradation process. The mixed matrix membrane prepared using this method has been successfully used to degrade 100% of methylene blue under UV light irradiation in 60 min.<sup>58</sup>

The other previous literature also reported that the spin coating method has been successfully implemented to form a thin layer of ZnO/polymer resin for the photodegradation of methylene blue. To form the thin layer, citric acid and  $Zn(NO_3)_2 \cdot 6H_2O$  were first dissolved in water at 70 °C. Then, ethylene glycol was added and the temperature was increased to 90 °C to obtain the homogenous resin. Samarium nitrate was later added to the mixture to obtain the Zn/samarium resin. To fabricate the photocatalytic polymer resin, a silicon substrate was used as a support to be deposited by the mixture of Zn/samarium polymer resin solution during the spin coating. The mixture solution was then poured onto the silicon substrate by spin coating at 7000 rpm for 30 s. The thin layer composed of mix Zn/polymer resin was formed and further annealed at 350 °C for 1 hour, and then dried at 700 °C to obtain the thin solid layer.<sup>86</sup> The photocatalytic membrane successfully

degraded 90.4% of methylene blue under UV-Vis light irradiation. The FESEM image in Fig. 23 shows the formation of small and larger grains formed due to the high energy applied during spin coating. The growth of larger grains was due to the coalescence of smaller grains. Overall, the distribution of the photocatalyst was uniform due to the smaller photocatalyst being used. Hence, it increased the surface area and enhanced the photodegradation of methylene blue.

The active sites of the photocatalyst played an important role in determining the photocatalytic activity. According to Hsiung *et al.*,<sup>87</sup> a few of the  $TiO_2$  active sites were detected, which influenced the photodegradation rate. The photoactive species of commercial  $TiO_2$  and synthesized  $TiO_2$  by sol gel method were studied using X-ray absorption near edge structural (XANES) spectroscopy. From the X-ray absorption near-edge structural (XANES) spectra, photocatalytic species such as A1 (4969.4 eV), A2 (4970.5 eV) and A3 (4972.3 eV) fit with the relative peaks at (101), (004) and (200) in the  $TiO_2$  photocatalyst, which are attributed to the three 1s–3d transition active sites, including for the four-( $TiO_4$ ), five-( $(Ti=O)O_4$ ) and six-( $TiO_6$ ) coordinated Ti structural species, respectively, as stated in Table 7. The synthesized  $TiO_2$  exhibited a higher surface area than the commercial  $TiO_2$ . Thus, methylene blue was degraded up to 90% using the synthesized  $TiO_2$  in 20 min rather than commercial  $TiO_2$ , which only shows 42%. Since the A2 species, ( $(Ti=O)O_4$ ), was enriched on the surface of the synthesized  $TiO_2$ , it contributes as the main active site during the photocatalytic degradation of methylene blue.

Other literature reported that the active species of ZnO depends on the exposed lattice plane. From the XRD spectra,  $2\theta$  at 34.4° (002) shows the highest peak, which was enriched in the

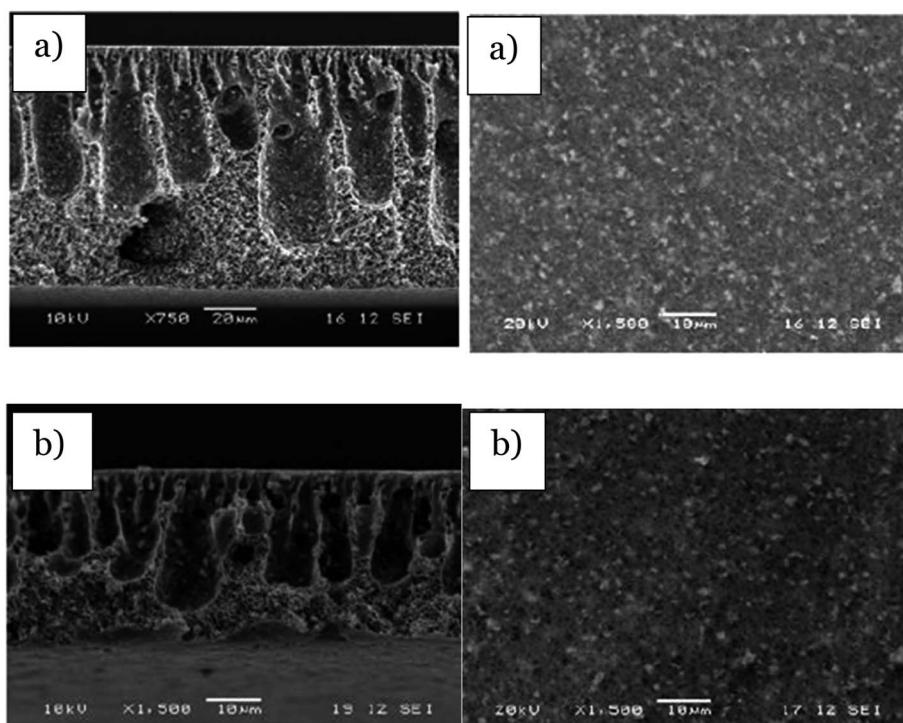


Fig. 22 SEM images of the cross-section and outer surface of the membrane via spin coating with a speed of (a) 500 rpm and (b) 1300 rpm.<sup>58</sup>



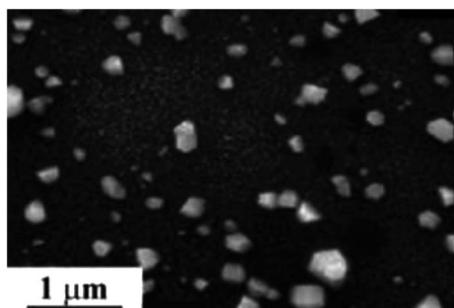


Fig. 23 FESEM micrograph of ZnO: 4% samarium distribution on the membrane.<sup>86</sup>

ZnO photocatalyst.<sup>88</sup> It was stated that the 002 facet absorbed UV radiation, which scatters light beyond the optical path length due to the honeycomb network structure. Moreover, the electric dipole was produced from the 002 polar surface, consisting of positive Zn-terminated (002) facets and negative O-terminated (00-2) facet. Furthermore, the exposed (002) facet was attributed to the increase of interstitial O<sub>2</sub> on this facet. From the XPS spectra, the highest peak with a binding energy of 1021.1 eV and 1044.2 eV confirmed that Zn<sup>2+</sup> existed abundantly as Zn ions. The Zn<sup>2+</sup> ionic sites on the (002) facets adsorbed the oxygen, resulting in a thin O<sub>2</sub><sup>-</sup> layer that helped in the redox reaction. Thus, it acted as the active sites that enhance the photocatalytic reaction. This can be seen when methylene blue has been successfully degraded up to 77% in 120 min using UV light irradiation. The differences of the active sites are summarized in Table 7.

In summary for this section, a mixed matrix membrane containing a photocatalyst that has been fabricated by various methods influences the morphology and performance in the photocatalytic activity. Mostly, the mixed matrix membrane provides benefits for water treatment, as the membrane produced is robust and can reduce the leaching of the photocatalyst since it is embedded inside the polymer matrix. However, it also shows drawbacks when a higher amount of photocatalyst is used. The photocatalyst may not be spread well inside the polymer matrix, which leads the photocatalyst to lump together and reduce the surface area. Thus, it blocks the active site of the photocatalyst from receiving enough light penetration. Besides, other factors that affect the photodegradation activity are the size and structure of the photocatalyst being used. The smaller the size of the photocatalyst, the larger the surface area.<sup>73</sup> Hence, it enhances the light penetration towards the active site of the photocatalyst, which increases the photocatalytic performance. The single and dual

layer of the hollow fibre mixed matrix membrane can be fabricated using dry-wet spinning and dry-wet co-spinning, respectively. Between these two procedures, the dual layer shows a more promising membrane than the single layer due to the photocatalyst being well distributed in the membrane, which enhances the light passing through the active sites of the membrane, resulting in the high photocatalytic degradation of the pollutant. Moreover, the hollow fibre configuration provides a higher surface area and easy flow for water flux. Besides, the electrospinning shows advantages, in which the photocatalysts can spread well inside the membranes. However, when a higher amount of photocatalyst was added, there was a formation of lumps inside the membrane that restricted the penetration of light, resulting in the low removal of the pollutant. Other methods that can be used to fabricate the mixed matrix membrane are tape casting and spin coating. Both methods provide a uniform distribution of the photocatalyst inside the membrane. However, by using the tape casting method, agglomeration of the photocatalyst was obtained when a higher amount of photocatalyst was used. Besides, the spin coating needs the high energy of speed to ensure the uniform and good photocatalyst distribution. For the mixed matrix membrane, it can be concluded that the photocatalyst, CaCu<sub>3</sub>Ti<sub>4</sub>O<sub>12</sub>, blended with the PES hollow fibre membrane using the dry-wet co-spinning technique was the most promising method in the photodegradation of the dye.<sup>72</sup> This is due to the faster degradation of rhodamine B under UV light irradiation up to 74.83% removal only within 40 min. Besides, the hollow fibre configuration provides a higher surface area for light penetration towards the active sites of the photocatalyst during photodegradation. The summary of the photocatalyst immobilized into the polymeric membrane is shown in Table 8.

### 3.2 Deposition onto the membrane surface

Nowadays, the coating method is widely used in order to immobilize the photocatalyst onto the membrane structure, such as sputtering,<sup>89</sup> dip coating,<sup>90</sup> electrospraying,<sup>80</sup> atomic layer deposition,<sup>91</sup> and others. The attachment of the thin layer photocatalyst on the polymer membrane as a support plays a crucial role in minimizing the agglomeration of nanoparticles, and provides better performance in the photocatalytic degradation activity. Besides, the coating polymer with photocatalyst seems to provide a more promising technique, rather than immobilized into the membrane due to the easier accessibility of the photocatalyst particle incorporated with the polymer membranes, as well as one-step technique. In addition, the mixed matrix membranes can experience an agglomeration of

Table 7 Different active sites that enhance the photocatalytic degradation

Photocatalyst	Active sites	XRD peaks	Pollutant	Time (min)	Photocatalytic degradation using UV lamp (%)	References
TiO <sub>2</sub>	TiO <sub>4</sub> (Ti=O)O <sub>4</sub> (main)	101 004 200	Methylene blue	20	90	87
ZnO	Zn <sup>2+</sup>	002	Methylene blue	120	77	88



Table 8 Summary of the mixed matrix polymer membrane methods for photocatalytic activity

Photocatalyst	Polymer type	Method	Configuration	Light irradiation	Time (min)	Pollutant	Photocatalytic factor	Removal (%)	References
N-doped TiO <sub>2</sub>	PVDF	Dry-wet Co-spinning	Hollow fibre membrane	UV (30 W, 312 nm) Visible	360	Reactive Black 5	High concentration of photocatalyst	100 75	62
CaCu <sub>3</sub> Ti <sub>4</sub> O <sub>12</sub>	PES	Dry-wet spinning	Hollow fibre membrane	UV-C (360 W)	40	Rhodamine B	High concentration of photocatalyst	74.83	72
Ag-TiO <sub>2</sub>	PVDF-HFP	Electrospinning	Electrospun mat	UV Visible (xenon, 600 W m <sup>-2</sup> )	90 300	Norfloxacin	Suitable band gap for irradiation	64.2 57.6	76
Graphitic carbon nitride (g-C <sub>3</sub> N <sub>4</sub> )	PAN	Electrospinning	Electrospun mat	Visible (white, 30 W, 420 nm)	300	Methylene blue	Small size of photocatalyst	97.3	78
TiO <sub>2</sub>	PA-6	Electrospinning	Electrospun mat	UV (300 W, 5 mW cm <sup>-2</sup> )	360	Methylene blue	High concentration of photocatalyst	99	80
C,N-doped TiO <sub>2</sub> – CdS	PES	Tape casting	Flat sheet	Visible (halogen, 500 W, 400 nm)	120	COD	Well dispersion of photocatalyst	65.2	81
N, co-doped TiO <sub>2</sub>	PSF	Tape casting	Flat sheet	Visible (450 W, 1000 W m <sup>-2</sup> )	180	Eosin yellow	High amount of photocatalyst	92	82
TiO <sub>2</sub>	PVDF	Tape casting	Flat sheet	UV	60	Methylene blue	Larger photocatalyst size	95	58
Cu <sub>2</sub> O	PSF	Tape casting	Flat sheet	Visible (250 W, 390–800 nm)	60	Ibuprofen	High intensity of photon	86	28
Ag-TiO <sub>2</sub>	PVDF-HFP	Tape casting	Flat sheet	Visible (xenon, 600 W m <sup>-2</sup> )	300	Norfloxacin	Lower band gap	80.7	76
TiO <sub>2</sub>	PVDF	Spin coating	Flat sheet	UV	60	Methylene blue	Well dispersion of photocatalyst	100	58
ZnO	Polymer samarium resin	Spin coating	Flat sheet	Visible	420	Methylene blue	Uniform dispersion of smaller photocatalyst due to high energy spin coating	90.4	86

the photocatalyst nanoparticle, which allows the obstacles to produce a uniform surface membrane. Besides, the agglomeration can clog the membrane pores, which can cause a surface defect that leads to the reduction of the surface area and photocatalytic activity.<sup>92</sup> This section will list several coating techniques that have been reported in the previous literature.

**3.2.1 Sputtering technique.** One of the coating techniques of the photocatalyst on the polymer support is sputtering technique. Sputtering is the process of the ionized ion from the target material (metal or metal oxide) bombarding the substrate (*e.g.*, polymer, glass, silicon), which then forms a thin layer deposited on the surface of the polymer.<sup>25</sup> This deposition process was carried out in a vacuum chamber by flow in the argon and oxygen gas, as well as working pressure to allow the ion bombardment to occur. Moreover, this technique is known as a cost-effective method because of the uniform sputtered layer formed, and less impurities are generated due to no chemicals being used.<sup>93</sup> In addition, this is one of the promising techniques for photocatalyst coating in a larger area production due to its single-step coating. Fig. 24 shows the schematic illustration of the sputtering process.

As mentioned by Tavakolmoghadam *et al.*,<sup>94</sup> TiO<sub>2</sub> was successfully sputtered on a commercial PVDF flat sheet membrane through the DC reactive sputtering technique. An electric field generated from a power source will ionize the argon gas to produce Ar<sup>+</sup> ion, which then bombards the Ti target to eject the Ti atoms. The Ti atoms will then react with O<sub>2</sub> to

produce TiO<sub>2</sub> and next bombard the PVDF surface, which results in a thin layer of TiO<sub>2</sub>. From this technique, it is proven in Fig. 25 that the uniform layer and small nanoparticles of TiO<sub>2</sub> were successfully deposited, which can avoid the blockage of pores. Thus, it is easy for the light penetration to reach the active sites of the photocatalyst. However, by using this method, it is stated that the bond between the sputtered TiO<sub>2</sub> and PVDF surface was not tightly attached together, which may cause TiO<sub>2</sub> leaching during the cleaning process. Thus, it can reduce the capability and applicability for the long-term filtration process. The modification of the polymer membrane was needed to ensure the strong attachment of the sputtered photocatalyst on the surface of the membrane. Thus, this reduces the drawback of the photocatalyst leaching during the treatment.

Recently, Marcelino *et al.*<sup>95</sup> reported on the good photocatalytic activity of TiO<sub>2</sub> sputtered on polyethylene terephthalate (PET) in the removal of contaminants of emerging concern, specifically for the fungicide carbendazim (CBZ) and anthropogenic pollution tracer caffeine (CAF) up to 39% under a combination of UV and visible light irradiation. It is stated that TiO<sub>2</sub> was successfully deposited onto the PET flat sheet surface by using the high power impulse magnetron sputtering (HiPIMS) technique. The argon and oxygen flow rate used in this sputtering procedure was fixed at 3.0 sccm and 50 sccm, respectively. The power supply was set at 700 Hz with a deposition time of 60 min, as well as the target substrate distance being equal to 100 cm. By using this method, the thin film



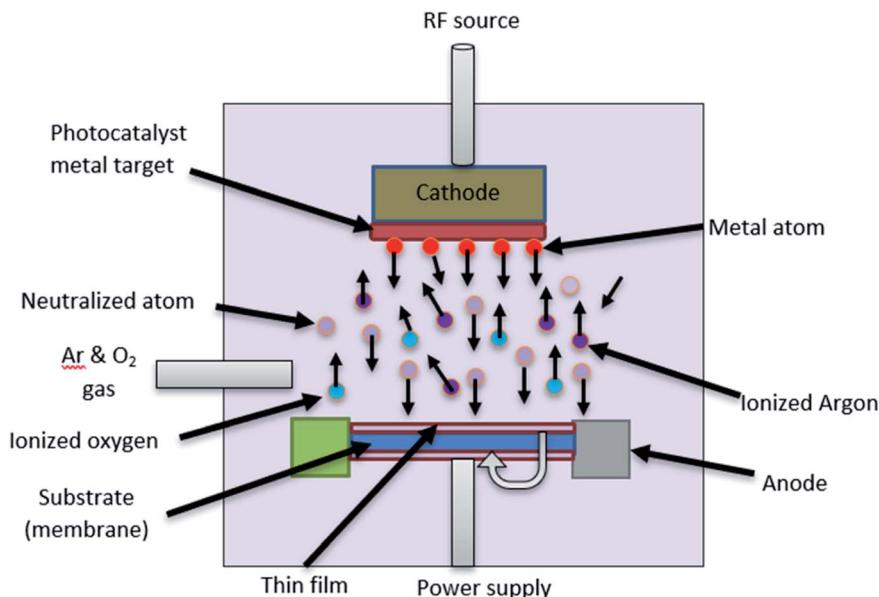


Fig. 24 Schematic diagram of the sputtering technique.

deposited was smooth and exhibited denser surfaces, rather than the coating using a DC magnetron sputtering. This is because the power applied was high energetic pulses with frequency (<1.5 kHz), current density ( $0.2 \text{ A cm}^{-2}$ ) and power density ( $>\text{kW cm}^{-2}$ ) on the target. Besides, the temperature sent to the substrate was also lower compared to the DC magnetron. Furthermore, the HiPIMS coatings can provide strong adhesion and higher crystallinity compared to the other magnetron sputtering.<sup>96</sup>

The sputtering technique of the material on the polymer surface is still lacking in the literature. Mostly, this technique was used to deposit the material or photocatalyst on the glass, silicon and quartz substrate. The sputtering technique has been proven to be successfully implemented in the sputtering of  $\text{TiO}_2$  and  $\text{Cu}_2\text{O}$  thin film onto the substrate, namely n-type Si (100) wafers and glass plate composed of indium tin oxide (ITO). The  $\text{TiO}_2/\text{Cu}_2\text{O}$  thin film was deposited by DC magnetron sputtering using pure Cu and Ti target. The sputtering process took place by applying 120 W of DC power in 30 min with an argon flow

rate of  $4 \text{ cm}^3 \text{ s}^{-1}$ , while the oxygen flow rate was  $1.5 \text{ cm}^3 \text{ s}^{-1}$  for  $\text{TiO}_2$  sputtering.

In contrast,  $\text{Cu}_2\text{O}$  was deposited later above the  $\text{TiO}_2$  layer with 80 W power in 40 min by applying  $3.0 \text{ cm}^3 \text{ s}^{-1}$  for the oxygen flow rate, while the argon flow rate was  $2.0 \text{ cm}^3 \text{ s}^{-1}$ . As mentioned in the paper, the closer the substrate was to the target, the higher the thickness of film deposited, as well as increasing the value of the grain sizes. Besides, by increasing the thickness of the thin film, the produced layer showed more uniformity, more roughness on the substrate surface and less deformation.<sup>97</sup> The micrograph of  $\text{TiO}_2$  and the  $\text{Cu}_2\text{O}$  coating on the membrane is shown in Fig. 26. The  $\text{Cu}_2\text{O}$  layer was thicker than  $\text{TiO}_2$  due to the close distance between the substrate and target. The properties of the sputtered material depend on several factors, including power, argon–oxygen flow rate, time and target–substrate distance. In general, the higher the sputtering power, the higher the film formation rate. Besides, the longer the deposition time, the thicker the sputtered film on the substrate surface. Hence, this increases the size of the grains of the coating material. The argon and oxygen flow rates also play important roles in the sputtering procedure. The higher flow rate of argon helps to ionize the target to eject the target atoms more easily, while the oxygen flow rate acts as a helper to produce metal oxide. For example, titanium atoms from the target will react with oxygen, forming  $\text{TiO}_2$ . The pressure of the sputtering system also affects the quality of the coating film on the substrate. From the previous literature, the high pressure during the sputtering procedure can lower the speed of the sputtered atoms that reach the substrates. Thus, it can cause the particles to collide with the gas, and unfortunately return back to the sputtered surface.<sup>98</sup>

Other studies have also discovered the sputtering process of nickel oxide ( $\text{NiO}$ ) on graphene oxide thin films using the direct current radio frequency sputtering technique, which is labeled as GNT. As mentioned by Jilani *et al.*,<sup>89</sup> the  $\text{NiO}$  metal oxide pure

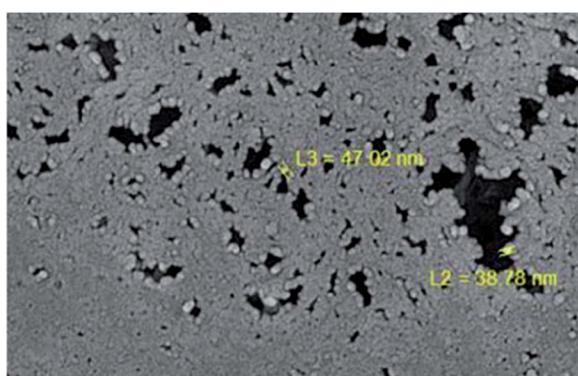


Fig. 25 SEM image of the modified PVDF membrane with the deposition of  $\text{TiO}_2$  (ref. 78).



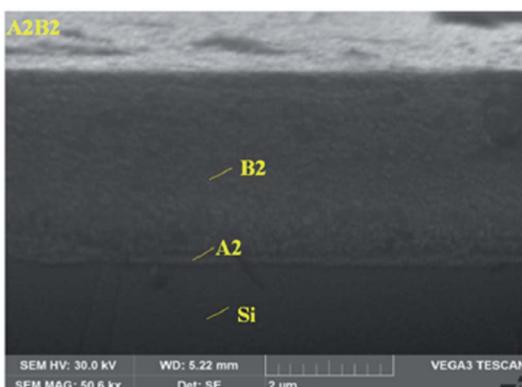


Fig. 26 SEM image of (A2)  $\text{TiO}_2$  and (B2) the  $\text{Cu}_2\text{O}$  layer on the Si membrane.<sup>97</sup>

target was used to sputter the  $\text{NiO}$  thin film with the distance between the target and substrate at 15 cm. The DC power of 200 W with an  $\text{O}_2$  flow rate was 40 sccm, and a base pressure equal to  $9 \times 10^{-7}$  torr were applied during the sputtering procedure. According to this paper, GNT exhibited good photocatalytic activity of 2-chlorophenol. The FESEM micrograph in Fig. 27 shows that the size of  $\text{NiO}$  in GNT-3 increased with increasing time deposition. In addition, the agglomeration of  $\text{NiO}$  occurred, which blocked the pores. When the deposition time was increased, the film became thicker and the grain size also increased. When the size of  $\text{NiO}$  increases, it may lump together and reduce the surface area of  $\text{NiO}$ . When the surface area of  $\text{NiO}$  is reduced, it causes less light penetration. Moreover, the charge carrier from the upper  $\text{NiO}$  layer to the inner GO layer became poorer when the deposited film was thicker. Moreover, a photoluminescence (PL) study stated that the thicker deposited film produced high PL intensity, which indicates the high rate of the recombination of the electron-hole.<sup>98</sup> Hence, this reduces the photocatalytic activity.

Another paper that mentions the sputtering process can be seen in the literature by Singh *et al.*<sup>99</sup> The sputtering process was achieved by depositing the  $\text{TiO}_2$  onto silica glass substrates from the titanium metal target using the radio frequency (RF) magnetron sputtering technique. The deposition of  $\text{TiO}_2$  thin films was carried out at  $2.5 \times 10^{-3}$  torr, and the temperature of the substrate was maintained at 200 °C. The gas pressure, RF power and temperature of the substrate were optimized. The thickness of the  $\text{TiO}_2$  thin film deposited was varied at 20 nm,

40 nm, 80 nm and 100 nm, which referred to T2, T4, T8 and T10, respectively. From the Tauc plot, the band gap of T2, T4, T8 and T10 were 3.4 eV, 2.8 eV, 3.0 eV and 2.9 eV, respectively. This shows that the optical properties changed with increasing film thickness. Among these samples, T4 possesses the highest degradation percentage of methylene blue up to 83% under sun light irradiation only in 45 min due to the lower band gap, which indicates the excellent efficiency of the sputtered  $\text{TiO}_2$  in the photodegradation of the dye. The band gap of the catalyst is necessary for photocatalytic study. When a lower band gap was used, the wavelength between 380–750 nm was more desirable for photocatalytic applications (effective sunlight region). Basically, the lower band gap can absorb light at higher wavelengths due to the lower energy requirement for the electron transition from the valence band to the conduction band.<sup>73</sup> Overall, to optimize the coating layer, the operational condition such as power supply, argon-oxygen flow rate, time and target-substrate distance need to be adjusted and considered.

**3.2.2 Dip coating.** This technique is employed by immersing the support, such as a polymer, into a solution for coating it. This is then followed by the removal of the support from the solution at a slow speed. This technique will produce different thicknesses of the coating layer from thinner to thicker film of the photocatalyst. Before the deposition occurs, the supports must first be cleaned and dried to avoid any contamination. The photocatalyst solution needs to be sonicated first to avoid any agglomeration of the photocatalyst particle on the surface after the dip out.<sup>100</sup> The schematic diagram of the dip coating is shown in Fig. 28.

According to Luo *et al.*,<sup>90</sup> the PVDF flat sheet membrane was modified by coating layer-by-layer with a 3D  $\text{TiO}_2$ /poly (sodium styrenesulfonate) (PSS) photocatalyst that had been successfully fabricated using the dip coating method. It was expected that by using this photocatalytic membrane, 91.42% Lanasol Blue 3R was successfully degraded under UV light irradiation. As mentioned in this paper, the PVDF membrane was dipped in 2 g  $\text{L}^{-1}$   $\text{TiO}_2$  solution for 15 min, followed by dipping in PSS solution for another 15 min. Then, the membrane surface was dipped again in  $\text{TiO}_2$  solution to form the layer-by-layer film coated on the surface. For every deposition step between  $\text{TiO}_2$  and PSS, the membrane was first dipped in distilled water to obtain the solid film in order to avoid the two photocatalysts being mixed together. During the dip coating procedure, the photocatalyst solution needs to be stirred to avoid any sedimentation of particles at the bottom of the solution. For the last step, the layer-by-layer coating membrane experiences the post treatment with ethanol and distilled water, and is then further dried in the oven for 90 min at 60 °C. Moreover, before characterization and analysis, the membrane was stirred vigorously in distilled water to remove any unstable attached photocatalyst. SEM images in Fig. 29 indicate that the deposited granules increase with increasing layers, resulting in a porous structure of membranes that make it into the hydrophilic membrane. The porous nanostructures gained much attention due to the larger accessible surface morphology, which is easier for light absorption. Besides, the structure of the catalyst also plays a significant role in the photocatalytic performance.

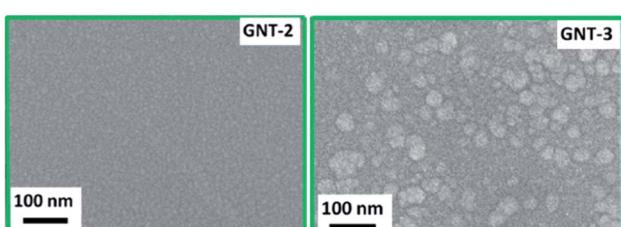


Fig. 27 FESEM micrograph of GNT-2 and GNT-3 with a deposition time of 800 s and 1200 s, respectively.<sup>98</sup>



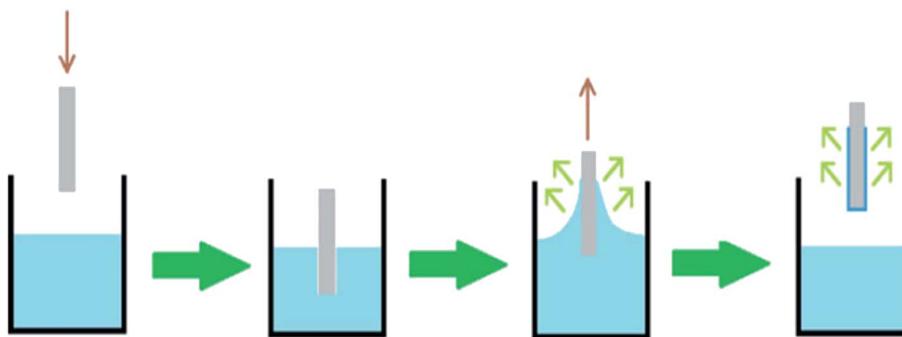


Fig. 28 Diagram of the dip coating method.<sup>100</sup>

Basically,  $\text{TiO}_2$  has three phase structures, namely rutile, anatase and brookite. Among these three phases, anatase has high photocatalytic activity due to its structural stability. Moreover, the available vacancies in  $\text{TiO}_2$  make the photoexcited electron easy to be trapped. Hence, the hole and electron are separated.<sup>101</sup> As a result, it is possible to reduce the charge recombination and enhance the photocatalytic efficiency.

The other paper that described the dip coating method can be seen through.<sup>102</sup> The polypropylene (PP) hollow fibre membrane was modified by forming a thin layer on the membrane surface by dip coating into the mixture of PSF/PEG400/ZnO solution to improve the anti-organic fouling properties. In addition, these two-layer membranes were stated to be a promising membrane in removing 70% of humic substances from peat water. Besides, the dip-coating method can help in increasing the hydrophilicity of the hydrophobic membrane that is suitable for water treatment. Before the dip-coating procedure was applied, the coating solution needed to be prepared by dissolving the PSF, PEG400 and ZnO into the DMAc solution. Then, the polypropylene hollow fibre membrane was dipped into the coating solution for 2 s and 10 s. After that, the PP hollow fibre membrane was taken out and further dried at room temperature to remove the solvent and form a thin solid layer coating. Thus, this dip coating technique was declared as a simple technique to deposit a coating layer onto the polymer membrane surface. When 40% of ZnO was deposited on the membrane, the SEM image in this literature proves that the aggregation of the ZnO particles with larger pores decrease the interconnection of the polymer during the

formation of the membrane, and creates voids in the polymeric layer. The time taken for the sample dip into the solution, type of solution and surface of the sample were the significant conditions that needed to be examined to obtain the optimized coating layer.

**3.2.3 Electrospraying.** Electrospraying is one of the methods that is closely related to electrospinning. It comes out with benefits, such as low energy consumed, and provides the good potential in the fabrication of nanoparticle coatings. It seems that by electrospraying the photocatalyst nanoparticles onto the polymer substrates, it will produce the efficient performance of the photocatalytic activity. In addition, this technique possesses several advantages, such as a simple coating technique for large area deposition.<sup>100,103</sup> The nanoparticles dispersed through the syringe needle will produce narrow nanoparticle size distributions. A substrate or collector will be placed horizontally to the needle. In contrast, a small motor with flexible speed is needed to rotate the collector so that it will spray uniformly.<sup>104</sup> The previous problems related to the coating methods are nanoparticle leaching due to the unstable attachment of nanoparticles onto the polymer substrates. To overcome this disadvantage, electrospraying can become one of the promising methods.<sup>100</sup> The schematic diagram of the electrospraying method is shown in Fig. 30.

As mentioned by Ramasundaram *et al.*,<sup>105</sup>  $\text{TiO}_2$  was dispersed inside the DMF solution, which was then electrosprayed onto both sides of the electrospun PVDF mats with the distance between the needle and PVDF mats at 100 mm by applying 15 kV power. The PVDF- $\text{TiO}_2$  fibre coating was then dried overnight

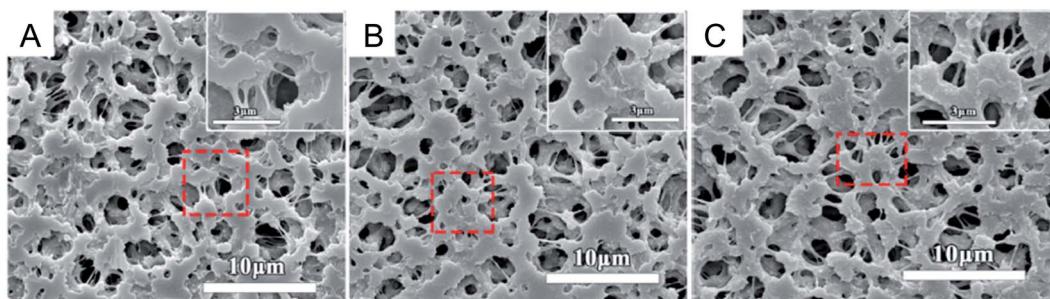


Fig. 29 SEM image of (A) 1 layer, (B) 3 layers and (C) 5 layers of the  $\text{TiO}_2$  PSS membrane.<sup>90</sup>



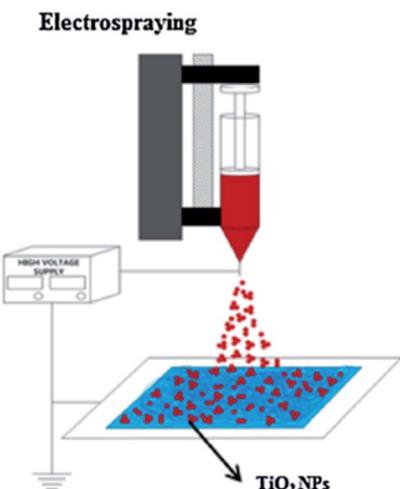


Fig. 30 The schematic diagram of the electrospraying method of the photocatalyst onto the substrate.<sup>105</sup>

at 120 °C under vacuum. From the SEM images in Fig. 31, TiO<sub>2</sub> droplets were deposited in a single spot on the PVDF mat. The individual and small aggregations of TiO<sub>2</sub> accumulated, becoming circular clusters with an average size of the TiO<sub>2</sub> clusters at approximately 20 nm. The number of clusters increased as the volume of TiO<sub>2</sub> loading increased. By using this method, it was stated that the PVDF electrospun membrane coated with TiO<sub>2</sub> using the electrospraying technique improved the photocatalytic activity, which completely degraded Bisphenol A, 4-chlorophenol and cimetidine in aqueous solution under UV irradiation within 100, 100 and 40 min, respectively. The clusters scattered on the overall surface of the electrospun PVDF mat, which helps in increasing the exposed area for TiO<sub>2</sub> to be penetrated by light. This is due to the active surface area of the photocatalyst improving the light penetration during photodegradation.

Besides, the same technique has been successfully implemented in previous literature written by Ryu *et al.*<sup>106</sup> Ag–TiO<sub>2</sub> photocatalyst nanoparticles were electrosprayed onto the nylon 6,6 polymer electrospun surface for methylene blue degradation

under visible light illumination. During the electrospraying procedure, the Ag–TiO<sub>2</sub> solution was electrosprayed by following several parameters. The stainless-steel spinneret with an inner diameter of 0.51 mm, 12 kV power and 10 cm distance between the spinneret and collector was applied. Moreover, 2.5 mL h<sup>-1</sup> flow rate of coating solution was performed in producing a thin film of photocatalyst onto the polymer electrospun surface. The prepared sample was then pressed for 2 min using a hydraulic press at 100 °C with pressure at 1000 psi to make the Ag–TiO<sub>2</sub> strongly attached onto the polymer surface, as well as prevent leaching. For the last step, the sample was washed with a dilute methanol solution to remove any excess unbound photocatalyst, and dried at room temperature for 24 hours. This electrospraying method was revealed to coat a thin layer film on the polymer surface, and is a simple method that can be implemented to save time. The SEM micrograph in Fig. 32 showed that the electrosprayed Ag–TiO<sub>2</sub> was evenly dispersed on the membrane surface without the formation of a large photocatalyst aggregation, resulting in it being tightly attached on the surface after heat-pressing treatment.

Furthermore, as mentioned in another past paper by Ramasundaram *et al.*,<sup>107</sup> the TiO<sub>2</sub> nanoparticles were electrosprayed onto the steel mesh/PVDF substrate. Steel mesh undergoes dip coating in PVDF solution to form a double layer substrate. The substrate was then further electrosprayed with TiO<sub>2</sub> to be utilized in the photocatalytic degradation of methylene blue and methyl orange dyes. The TiO<sub>2</sub> solution was electrosprayed on both sides of the prepared substrate with the conditions of 20 kV power, 6 mL h<sup>-1</sup> flow rate, and the distance between the needle and collector gap was 10 cm. The sample obtained was further pressed under heat treatment with several temperatures by applying 100 MPa pressure. Lastly, the sample was immersed in stirred deionized water overnight to remove any unbound TiO<sub>2</sub> nanoparticles, and dried under vacuum for 5 hours at 60 °C. The substrates were fully covered with aggregated TiO<sub>2</sub>. By implementing this promising technique, electrospraying offers easy control of the film thickness, an even distribution of the coating film, and faster time deposition because it did not require a calcination step. Overall, the voltage power and the

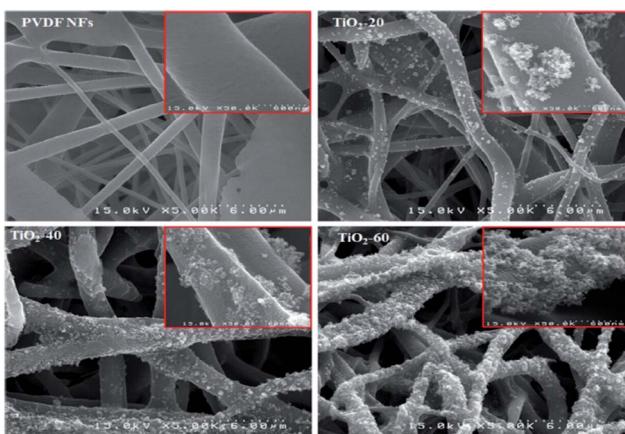


Fig. 31 SEM images of the TiO<sub>2</sub> deposition of the PVDF mat.<sup>105</sup>

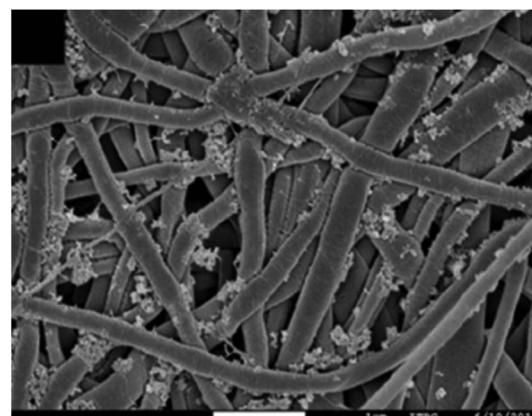


Fig. 32 SEM micrograph of the electrosprayed Ag–TiO<sub>2</sub> on the membrane surface.<sup>106</sup>



distance between the sample and substrate were important in optimizing the process condition.

**3.2.4 Atomic layer deposition.** A previously published paper has recorded the potential of the surface modification of polymer membranes with the immobilization of the photocatalyst onto the membrane surface using atomic layer deposition. Despite the polymer membrane, this technique also shows outstanding performance in depositing a thin film on another substrate surface. Moreover, the thin film produced was strongly attached to the surface, and can prevent the leaching of the photocatalyst during the water treatment analysis.<sup>108</sup> Besides the water treatment, atomic layer deposition is also a promising technique in various applications, such as photovoltaics, energy conversion, and transistors, and is used in display devices that need a precise thickness of the film coating, conformity and uniformity.<sup>109</sup> A chamber equipped with nitrogen flow and the precursor as the photocatalyst source to be deposited was needed in this study. The atomic layer deposition process is shown in Fig. 33, while the schematic diagram of the atomic layer deposition technique is illustrated in Fig. 34.

The previous paper mentioned by Li *et al.*<sup>91</sup> has successfully implemented the atomic layer deposition method by coating the flat sheet PVDF membrane with a 3D layer of TiO<sub>2</sub>/ZnO. Before the coating procedure can take place, the PVDF membrane must be dried in the ALD chamber at 110 °C for 30 min. During the deposition process, titanium tetraisopropoxide (TTIP) was used as a metal to eject TiO<sub>2</sub> by maintaining the TTIP pulse at 100 ms with 10 s of exposure, and purged in the chamber for 30 s. Deionized water (DI) was also used in this process by maintaining the pulse at 15 ms with 10 s of exposure, and purged at 30 s. Nitrogen was used during the procedure by applying 20 sccm flow rate in order to purge the residual components after deposition. To deposit ZnO on the surface of the PVDF membrane, diethylzinc (DEZ) was used. The condition of the DEZ pulse was maintained at 20 ms, while DI water was pulsed at 15 ms. The exposure and purge condition for DEZ and DI water were the same as the coating of TiO<sub>2</sub> from the previous one. TTIP was fixed at 80 °C, while DI water and DEZ

were maintained at room temperature during the deposition procedure. FESEM micrographs indicate the surface of the TiO<sub>2</sub>/ZnO-PVDF membrane in Fig. 35. The deposited granules become larger with increasing ZnO content. According to this technique, the 3D layer of TiO<sub>2</sub>/ZnO was successfully deposited onto the PVDF membrane surface for the photodegradation of methylene blue up to 80% after 30 minutes irradiation by visible light. This is because the crystal planes of TiO<sub>2</sub>/ZnO at (101) act as an important factor in improving the photodegradation performance. The (101) planes of TiO<sub>2</sub> are energetically high, and exhibit better photodegradation performance of the reduction of O<sub>2</sub> to O<sub>2</sub><sup>·-</sup> than the (001) planes. Moreover, the hexagonal wurtzite ZnO that is formed by ALD helps in producing (100), (002), (101), (102) and (110) crystal planes. According to Wang *et al.*,<sup>112</sup> the literature found that the rate of degradation is in the order of (100) > (110) > (111).

Furthermore, the previous literature indicates the atomic layer deposition method for the TiO<sub>2</sub> coating on the surface of the flat sheet PES membrane by using a low-pressure flow type ALD reactor.<sup>108</sup> This literature explained that the deposition process operated through a series of cyclic operations, which means that each cycle was divided into two half cycles. TiCl<sub>4</sub> acting as the precursor was pulsed in the first half cycle using 99.9999% pure nitrogen carrier gas, and underwent the self-terminating reactions on the substrate. After that, the residual component and by-product were removed by purging the chamber. For the other remaining half cycle, a DI water pulse was used as the second precursor that was carried out in the chamber by nitrogen gas. The same action was taken, including the self-terminating reaction, and the residue was purged at the end of the procedure. The flow rate of DI water and TiCl<sub>4</sub> were fixed at 200 sccm and 150 sccm, respectively. The pressures implemented for DI water and TiCl<sub>4</sub> were 8 hPa and 9 hPa, respectively. In addition, the pulsing times of TiCl<sub>4</sub>/N<sub>2</sub>/H<sub>2</sub>O/N<sub>2</sub> were 0.1 s/2 s/0.3 s/3 s, respectively, and the total cycles used to deposit the TiO<sub>2</sub> film was 1000. The characterization result shows that the TiO<sub>2</sub> deposited on the membrane surface was uniform, as can be seen in Fig. 36. Thus, it produced a rougher

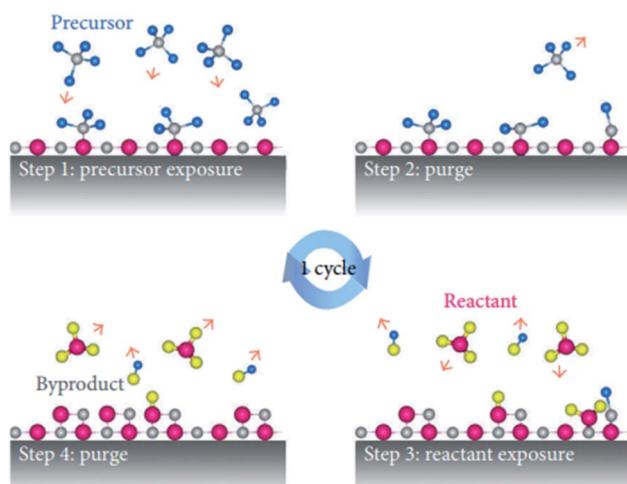


Fig. 33 Atomic layer deposition process.<sup>110</sup>

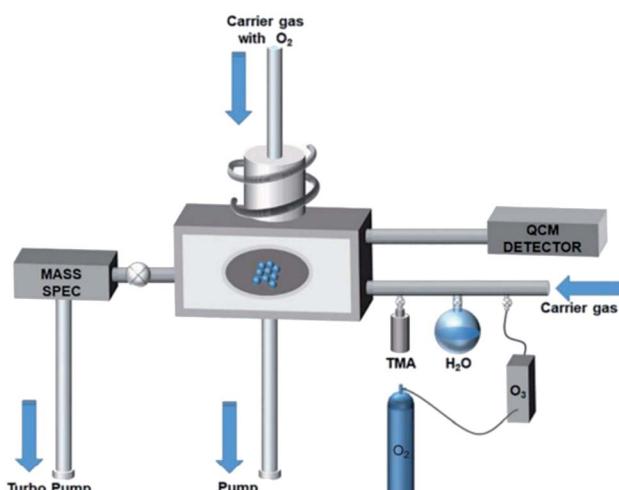


Fig. 34 Diagram of the atomic layer deposition technique.<sup>111</sup>



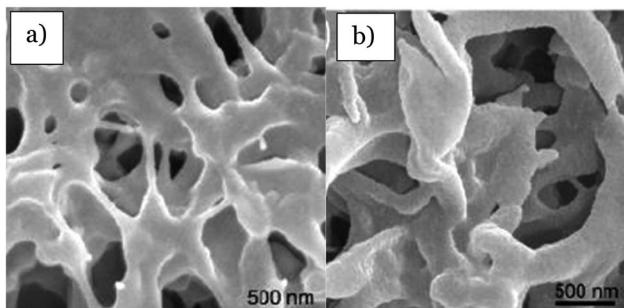


Fig. 35 FESEM images of (a) 1 : 1 layer of  $\text{TiO}_2/\text{ZnO}$  and (b) 1 : 5 layer of  $\text{TiO}_2/\text{ZnO}$  deposited on the PVDF membrane by ALD.<sup>91</sup>

surface texture. Moreover, the atomic layer deposition is shown to be a promising technique due to increasing the mechanical strength of the membrane, and  $\text{TiO}_2$  tightly wrapped the PES membrane skeleton. Thus, it reduced the leaching of  $\text{TiO}_2$ .

Another deposition of  $\text{TiO}_2$  on the polyvinyl alcohol (PVA) polymer flat thin layer using the atomic layer deposition method was reported.<sup>109</sup> According to this study, the PVA layer was prepared by spin coating on the silicon substrate with 3000 rpm speed, and labeled as the substrate sample. During the atomic layer deposition, tetrakis (dimethylamido) titanium (TDMAT) was used as the precursor of the Ti source, while  $\text{H}_2\text{O}$  acted as the reactant. Both TDMAT and  $\text{H}_2\text{O}$  operated with the pulse and purge time equal to 20 ms and 20 s, respectively, in the chamber. Moreover, the temperature of TDMAT and  $\text{H}_2\text{O}$  were set at 105 °C and 50 °C, respectively, while the chamber temperature was maintained at 150 °C. The pressure used in this study was 20 Pa, while the nitrogen flow rate was 20 sccm. This study implemented 100, 300, 500 and 1000 cycles to investigate the thickness of the film layer. The higher the number of cycles, the lesser the flexibility of the  $\text{TiO}_2$  nanosheet produced because different colours of the nanosheet can be seen from the optical interference at various regions. Besides, the higher the ALD cycles, the lower the surface area, which provides thicker nanosheets. Thus, it reduces the light penetration on the active sites of the photocatalyst to be reacted in the photodegradation procedure. Furthermore, the  $\text{TiO}_2$  produced by this technique shows better photodegradation of methyl orange under UV irradiation at fewer ALD cycles, which leads to an increase in its potentiality in photocatalysis

applications. The structure of the nanosheet of  $\text{TiO}_2$  tends to have higher efficiency in photocatalytic study due to the smaller size of the material compared with other structures. When the size of the photocatalyst is smaller, a larger number of atoms accumulated on the surface of the catalyst, which leads to an increase of the surface volume ratio. Hence, it enhances the charge carrier transfer rates, and thereby increases the catalytic activities.<sup>113</sup> Overall, many operational conditions, such as the nitrogen flow rate, precursor, pressure and pulsing time, are needed for operating the ALD system.

In summary for this section, the deposition of the photocatalyst on the polymeric membrane can be done with various methods. Many factors affect the photocatalytic degradation efficiency of the deposited photocatalyst, including the structure, size, band gap and crystal plane. For example, the anatase phase of  $\text{TiO}_2$  shows great photocatalytic activity due to its structural stability. Besides, the smaller size of the deposited photocatalyst also exhibited outstanding performance of the photocatalytic activity due to the exposed surface area being increased when the size decreased. Moreover, the larger and smaller band gaps of the photocatalyst were suitable to be irradiated under UV and visible light, respectively, according to their specific wavelength. The XRD crystal plane also played an important role in producing good photocatalytic activity. For example, the crystal plane of  $\text{TiO}_2$  at (101) is energetically high, which speeds up the reduction of  $\text{O}_2$  to  $\text{O}_2^{\cdot-}$  during the photocatalysis process. Sputtering is indicated as a promising method to sputter the photocatalyst onto the polymeric membrane due to the facile control of the film thickness, grain size and condition of the coating surface as either smooth or rough. However, the different types of polymers also affect the attachment of the photocatalyst on the membrane surface. This is important in order to avoid the leaching of the photocatalyst during the photodegradation of the pollutant in aqueous solution. Besides, the electrospraying method affected the performance of the photocatalytic activity. Although this method is faster, aggregation and larger photocatalyst clusters can be formed on the membrane surface when there is a higher amount of photocatalyst used for loading. Thus, it can block the pores and reduce the surface area for light penetration. Furthermore, the other deposition methods were dip coating and atomic layer deposition (ALD). Dip coating promotes the

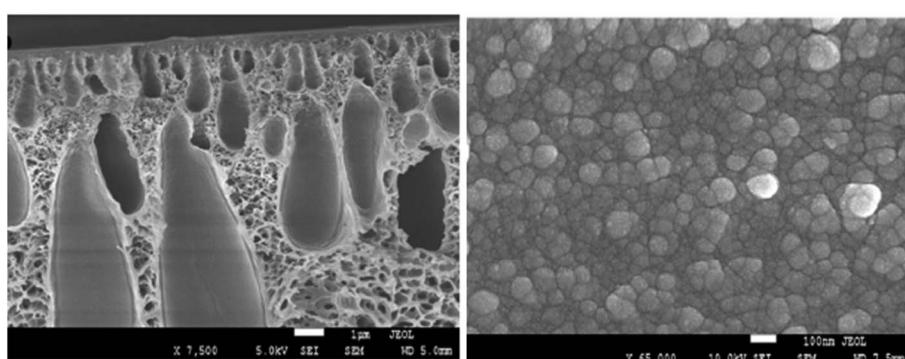


Fig. 36 SEM images of the uniform distribution of  $\text{TiO}_2$  on the flat sheet PES membrane.<sup>108</sup>



Table 9 The summary of the immobilization techniques of the photocatalyst onto the polymeric membrane for photocatalytic activity

Photocatalyst	Support	Method	Pollutant	Light source	Time (min)	Photocatalytic factor (%)	Removal	References
TiO <sub>2</sub>	PET flat sheet membrane	HIPIMS sputtering	Carbendazim Caffeine	UV-A/Vis (36 W, 370 nm)	420	High energetic pulse of HiPIMS	35 39	95
NiO	Graphene oxide flat sheet	DC sputtering	2-Chlorophenol	Visible (104 W)	210	High deposition time lead the increases of grains size	40	89
TiO <sub>2</sub>	Silica glass	RF sputtering	Methylene blue	Sunlight (950 W m <sup>-2</sup> )	45	Suitable band gap	83	99
TiO <sub>2</sub> /poly (sodium styrenesulfonate) (PSS)	PVDF flat sheet	Dip coating	Lanasol Blue 3R	UV (200 W, 385 nm)	120	Stable anatase phase	91.42	90
TiO <sub>2</sub>	PVDF electrospun mat	Electrospraying	Bisphenol A 4-Chlorophenol Cimetidine	UV	100 100 40	Small cluster of photocatalyst	100 100 100	105
Ag-TiO <sub>2</sub>	Nylon 6,6 electrospun	Electrospraying	Methylene blue	Visible (380–480 nm)	720	Well dispersed of photocatalyst increase the surface area	>90	106
TiO <sub>2</sub>	Steel mesh/ PVDF flat sheet	Electrospraying	Methylene blue Sulfamethoxazole Microcystin LR	UV (blacklight blue lamp, 24 W, 350–400 nm)	120 120 70	Well dispersed of photocatalyst increase the surface area	100 100 100	107
TiO <sub>2</sub> /ZnO	PVDF flat sheet	Atomic layer deposition	Methylene blue	Visible (xenon lamp, 200 W)	30	Larger size of granules and energetically high crystal plane	>80	91
TiO <sub>2</sub>	PVA	Atomic layer deposition	Methyl orange	UV (xenon lamp, 200 W)	150	Lower ALD cycle, small size (nanosheet) photocatalyst	80 (500 ALD cycle)	109

porous structure of the membrane due to the increasing granules from the increasing layer of excessive dip coating. Unfortunately, the aggregation of the photocatalyst occurred when a higher loading amount of photocatalyst was used. Moreover, having less ALD cycles was more favoured because it produces a higher surface area, as well as a thinner membrane that enhances the light penetration on the active sites of the photocatalyst. Thus, it provides outstanding performance of the photocatalytic activity. For depositing the photocatalyst onto the polymeric membrane, a previous article written by Singh *et al.*<sup>99</sup> shows the best deposition technique. The sputtered TiO<sub>2</sub> shows excellent photocatalytic result in that the methylene blue was degraded by 83% only within 45 min under sun light illumination. The summary of the immobilization techniques of the photocatalyst onto the polymeric membrane is revealed in Table 9.

## 4. Conclusions

The various modification methods for the polymeric membrane could be applied to enhance the efficiency of the photocatalytic activity under UV or visible light. This review paper has summarized the significant features of various techniques of the polymeric membrane immobilized with a photocatalyst either into or onto the membranes. From the previous review, it can be found that titanium dioxide is the most favoured

photocatalyst that has been chosen by researchers to be immobilized with polymeric membranes. It is because TiO<sub>2</sub> has great features, such as stability, availability and strong oxidation capability, to enhance the photocatalytic activity under UV light irradiation during the water treatment process. The blended and deposition techniques of the photocatalyst into and onto the polymeric membranes provide advantages and disadvantages. Mixed matrix membranes promote the strong attachment of the photocatalyst inside the membrane, which prevents the leaching of the photocatalyst during photodegradation in aqueous solution. However, a non-uniform dispersion of higher loading of the photocatalyst inside the membrane can cause photocatalyst agglomeration, which can block the pores and reduce the surface area. Thus, the lower the surface area, the lesser the light will penetrate into the active sites, resulting in low photocatalytic activity. Besides, deposition techniques of the photocatalyst (especially sputtering and atomic layer deposition) yield a uniform distribution of the photocatalyst due to the controllable deposition parameters. However, the leaching of the photocatalyst's problem might rise up depending on the condition of the polymeric membranes. Moreover, dip coating and electrospraying are simple methods, which can save time due to the easier procedure of the deposition method. However, these methods can cause aggregation and cluster formation of the photocatalyst on the membrane's surface, which reduce the photodegradation performance if the



photocatalyst is not distributed evenly. Therefore, the preparation of the dope composition, stirring condition, speed, distance, concentration, pressure, flow rate and temperature should be stressed to ensure the uniform, strong attachment of the photocatalyst on the membrane, and high photocatalytic efficiency can be produced. Moreover, the suitable techniques that have been reviewed in this paper may be useful for the future study with other applications. The role of the photocatalytic study is expected to be an energy-saving technology that can contribute to global climate change mitigation by using renewable energy and less chemical input.

## Conflicts of interest

There are no conflicts to declare.

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