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## Comparison of fractal dimensions from nitrogen adsorption data in shale via different models

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The roughness of pore surfaces in shale reservoirs can affect the fluid flow, which makes it necessary to be characterized. Fractal dimension, a key component in fractal geometry, can be used to describe the surface irregularities. In this paper, we evaluated and compared the fractal dimensions of several shale samples with three major fractal models based on nitrogen adsorption isotherms. The results showed that Frenkel–Halsey–Hill (FHH), Neimark, and Wang–Li models all can be applied for fractal dimension characterization of shale samples. From theoretical thermodynamics, these three models should be considered identical based on the FHH equation. However, the experimental data obtained from these samples showed that the fractal dimensions that are derived from the Neimark model and Wang–Li model are the same while a discrepancy was observed with the results from the FHH model. The difference in the fractal dimensions in the experimental data among these three models was attributed to the micropore structures. It was found that as the micropore surface area or the micropore volume increases in the samples, the difference in the fractal dimensions would increase as well. If the number of micropores present in the samples is limited, all three models can become suitable for fractal dimension calculation in shale samples, otherwise, the Neimark or Wang–Li model is preferred.

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### 1. Introduction

Unconventional reservoir resources now play an important role in total energy consumption.<sup>1,2</sup> For the unconventional reservoirs with low porosity and permeability, the surface roughness of the pores in a porous media would impact fluid flow and heat transfer.<sup>3</sup> During oil production in two-phase flow in the subsurface, the roughness of the pore surface can affect the phase distribution of flow regimes and lead to variations in phase relative permeability.<sup>4</sup> Knowing the surface roughness of the pores can assist in understanding oil/gas flow which requires characterization of pore surface precisely. Traditional techniques to evaluate surface roughness are based on the concept of isolated deviations from a planar surface area. However, this method has the difficulty of identifying a small number of structural parameters that can describe the roughness for a variety of purposes that can accurately reflect the pore surface.<sup>5</sup> Fractal dimensionality proposed by Avnir *et al.* (1984) is an excellent method to characterize the complex surface

geometries that can overcome the limitations of traditional methods. Avnir *et al.* (1984) found that at the molecular level, the surface of most materials reflects a fractal behavior with fractal dimension varying from 2 to 3, where 2 means a perfectly smooth surface and 3, significantly rough and a disordered surface.<sup>6</sup>

The fractal dimension of a solid surface can be determined with a variety of techniques such as porosimetry,<sup>7</sup> electrochemical methods,<sup>8</sup> small angle scattering,<sup>9</sup> and adsorption isotherms.<sup>5</sup> With some assumptions, adsorption isotherms have been employed for the surface roughness characterization in different materials such as carbon blacks,<sup>10</sup> carbon fibers,<sup>11</sup> and aerosol particles.<sup>12</sup> Up to date, various fractal models based on the adsorption isotherms have been proposed and applied to analyze the fractal dimension of the solid surface such as the fractal version of Frenkel–Halsey–Hill (FHH) model which is based on the classical FHH theory,<sup>5,13</sup> the thermodynamic model which was developed by Neimark<sup>14</sup> and the Wang–Li model.<sup>15</sup>

Nitrogen adsorption nowadays has become a standard technique for pore structure analysis in shale characterization.<sup>16–21</sup> In addition to its applicability for pore size distribution, pore surface area and pore volume determination, researchers have combined fractal dimension analysis with adsorption isotherms to obtain more information from the pores.<sup>22–26</sup> Based on the literature, nearly all the authors utilized the FHH model solely to characterize fractal dimensions of

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shale rocks without any strong basis. Thus, to date, the following questions have remained unanswered: is the FHH model the most suitable one for fractal dimension analysis of shale rocks? If not, which model would provide us with more accurate understanding of this complicated rock pore structures?

This study attempts to answer the above questions. In order to do so, 19 shale samples from the Bakken Formation have been collected and gas adsorption data has been acquired from these samples. In the next step, several mainstream fractal models were employed to analyze the adsorption isotherms. Based on the comparison of the results, some suggestions have been made to select the best fractal model for analyzing the pore structure of shale samples in the future.

## 2. Basic fractal theory of the gas adsorption

### 2.1. FHH fractal theory

In order to apply the classical Frenkel–Halsey–Hill (FHH) theory on fractal materials, Pfeifer *et al.* (1989, 1984)<sup>5,13</sup> assumed the film of the fluid that is absorbed on the sample surface could be regarded as a number of spheres with radius  $z$  representing a monolayer. Thus, the volume of this absorbing film is equal to the number  $n(z)$  of spheres multiplied by the sphere volume ( $\approx z^3$ ). Therefore, the fractal dimension can be defined by assuming that  $n(z)$  is proportional to  $z^{-D}$ . Then the amount of fluid that is adsorbed as a function of the film thickness  $z$  on a fractal surface is given by:

$$N \propto z^{3-D} \quad (1)$$

where  $D$  is the fractal dimension, and  $z$  is the radius. Based on the condensation regime, the mean radius curvature of the interface is:

$$z \propto [-\ln X]^{-1} \quad (2)$$

where  $X = P/P_0$ , the relative pressure,  $P$  is the equilibrium pressure on the sample while  $P_0$  is the saturation pressure of nitrogen at 77 K. Substituting eqn (2) into eqn (1), one obtains the expression of the fractal surface prediction in the capillary condensation regime in a log–log format:<sup>27</sup>

$$\ln N = a + (D - 3) \ln(-\ln X) \quad (3)$$

where  $a$  is a constant value.

### 2.2. Neimark fractal theory

Neimark took a thermodynamic approach to determine the surface fractal dimension of a porous solid ( $D_N$ ) which can be expressed by:<sup>28</sup>

$$S(r) \sim r^{2-D_N} \quad (4)$$

where  $S(r)$  is the surface area and  $r$  is the length of the yardstick which is used to measure the surface area.<sup>14</sup> Then the fractal

dimension  $D_N$  can be calculated through the following equation:<sup>14</sup>

$$\ln S(r) = k - (D_N - 2) \ln r \quad (5)$$

where  $k$  is a constant and  $S$  can be derived from the Kiselev equation as follows:

$$S = - \int_{N(X)}^{N_s} \mu dN = \frac{RT}{\sigma} \int_{N(X)}^{N_s} (-\ln(X)) dN \quad (6)$$

and  $r$ , the average radius of curvature of the meniscus at the interface between condensed adsorbate and gas, increases as the relative pressure  $X$  increases following Kelvin's equation:

$$r = - \frac{2\sigma V_L}{RT \ln X} \quad (7)$$

where  $\sigma$ ,  $R$ ,  $T$ ,  $V_L$  are the surface tension, universal gas constant, the temperature, and the molar liquid adsorbate, respectively.  $N_s$  is the adsorption quantity as the relative pressure  $X$  tends to become 1.

### 2.3. Wang–Li fractal theory

Considering the correlation between the area of the fractal surface and the volume circumscribed by the surface that is proposed by Mandelbrot (1982),<sup>28</sup> Wang and Li calculated the fractal dimension based on the following equation:<sup>15</sup>

$$S(r) = k_0^{D_{WL}} r^{2-D_{WL}} V^{D_{WL}/3} \quad (8)$$

where  $k_0$  is the factor relating surface area with the corresponding volume. Thus, by assuming that the liquid cannot be compressed,  $V$  can be calculated as:

$$V = [N_s - N(X)] V_L \quad (9)$$

Combining eqn (5) and (7)–(9), the following expression can be obtained:

$$\ln A(X) = l + D_{WL} \ln B(X) \quad (10)$$

where  $l$  is a constant,  $A(X)$  and  $B(X)$  can be described as:

$$A(X) = \frac{-\int_{N(X)}^{N_s} \ln(X) dN(X)}{r^2(X)}, B(X) = \frac{[N_s - N(X)]^{1/3}}{r(X)} \quad (11)$$

## 3. Materials and methods

19 shale aliquots were collected from the Bakken Formation from the cores that are retrieved from several wells drilled in the Williston Basin, ND. These shale samples are mainly composed of quartz and clay minerals. All samples were crushed into powders with grain size less than 250  $\mu\text{m}$  (60 mesh). Data from samples #17, #18, and #19 were analyzed previously and presented in the study by Liu *et al.* (2017)<sup>26</sup> and some of the other samples are studied by Abarghani *et al.* (2020) who focused more on the organic chemistry.<sup>29</sup> Prior to the adsorption measurements, all powders were degassed for 8 hours at 110 °C to remove moisture and volatiles that may exist in the sample



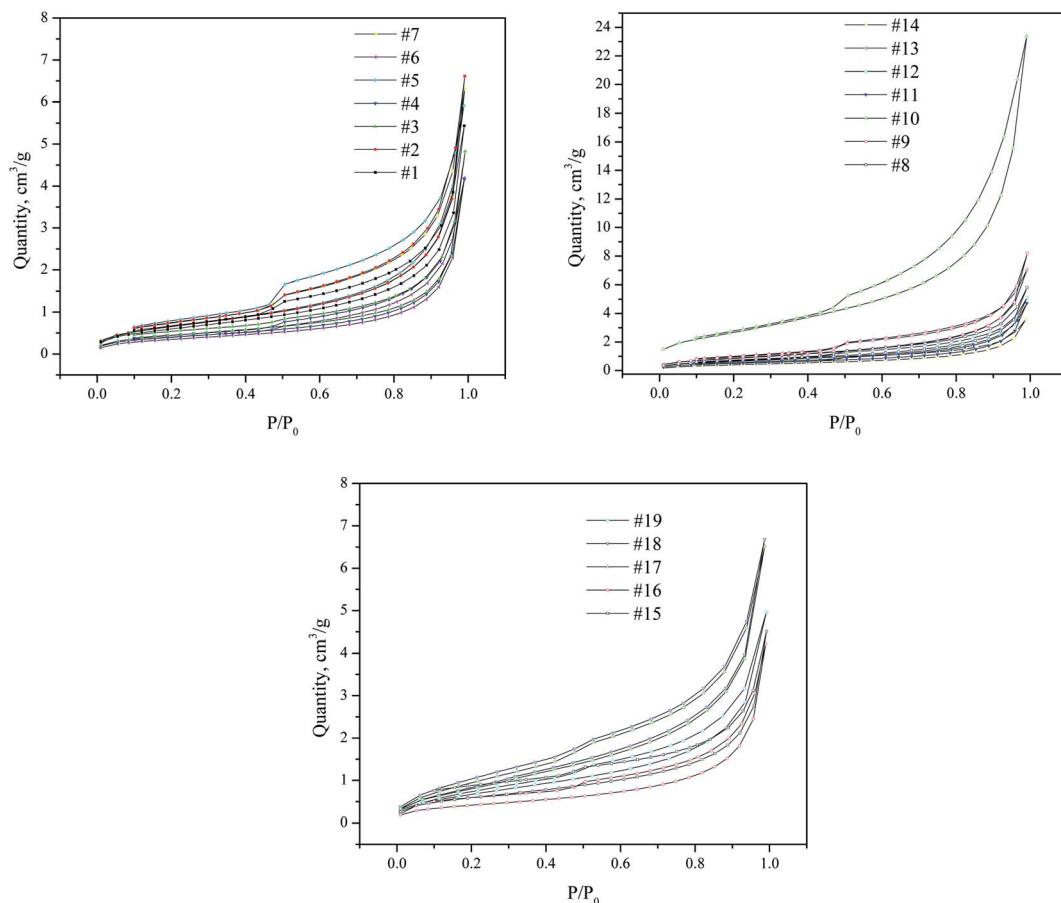


Fig. 1 Gas adsorption isotherms of all the shale samples.

pores. Low-pressure nitrogen adsorption experiment was performed on a Micromeritics® Tristar II apparatus at 77 K. The gas adsorption quantity was monitored and recorded as the relative pressure increases from 0.01 to 1. The outcome will provide us with the pore structure information such as the pore

size distribution (PSD) while micropore volume and micropore surface area can be quantified using the Barrett–Joyner–Halenda (BJH) model.<sup>30</sup>

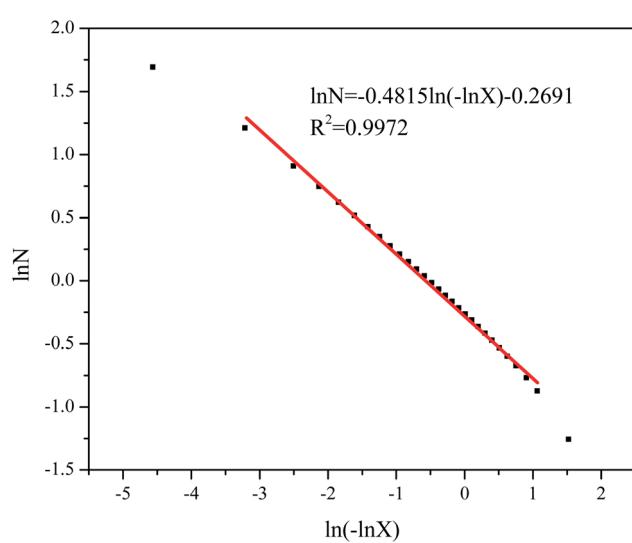


Fig. 2 The FHH fractal analysis of sample #1 (adsorption branch).

Table 1 Summary of the fractal dimensions of the shale samples using FHH theory

Samples	$D_{FHH}$	$P/P_0$ range scale	$R^2$
#1	2.519	0.085–0.961	0.997
#2	2.506	0.084–0.956	0.999
#3	2.529	0.056–0.953	0.998
#4	2.519	0.053–0.990	0.995
#5	2.491	0.092–0.959	0.998
#6	2.503	0.055–0.990	0.999
#7	2.506	0.055–0.959	0.998
#8	2.507	0.050–0.956	0.996
#9	2.506	0.084–0.957	0.996
#10	2.487	0.050–0.954	0.998
#11	2.534	0.055–0.991	0.996
#12	2.528	0.080–0.958	0.996
#13	2.498	0.048–0.958	0.995
#14	2.499	0.094–0.956	0.997
#15	2.565	0.084–0.959	0.992
#16	2.495	0.053–0.956	0.999
#17	2.435	0.113–0.883	0.984
#18	2.454	0.112–0.884	0.981
#19	2.522	0.071–0.935	0.990



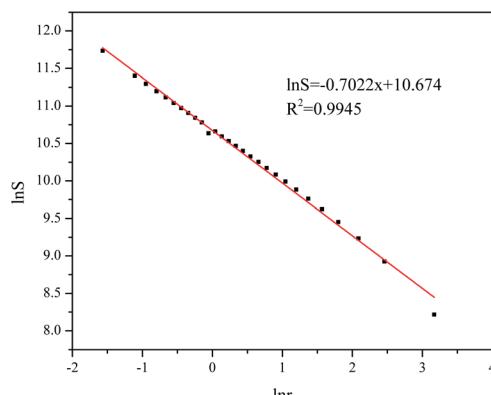


Fig. 3 The Neimark fractal analysis of sample #1 (adsorption branch).

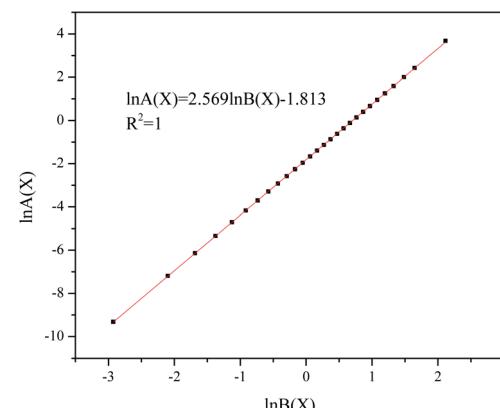


Fig. 4 The Wang-Li fractal analysis of sample #1 (adsorption branch).

## 4. Results

### 4.1. Nitrogen adsorption isotherms

Gas adsorption isotherms of all shale samples can be seen in Fig. 1. At extremely low relative pressures, the amount of adsorbed gas will depend on the micro-pore volume. As the relative pressure increases, multilayer adsorption will be formed. Hence, the knee-bend shape of the adsorption isotherms in the figure can indicate the transition from the monolayer adsorption to the onset of the poly-molecular adsorption. At the higher relative pressure, the gas in the mesopores and macropores starts to condense. During the desorption stage, as the relative pressure decreases, the quantity of the gas adsorbed will decrease. Therefore, the desorption curve will coincide with the adsorption curve which is caused by the “tensile strength effect”, creating hysteresis loops. The hysteresis loops that is observed in all isotherms indicate the

existence of mesopores. Based on the recommendations by the International Union of Pure and Applied Chemistry,<sup>31</sup> the shape of these hysteresis loops show the major pores in these samples are slit shaped. The difference between the gas adsorption quantities at the same relative pressure of these samples explains that these samples have different pore structures, such as pore volume and pore surface area.

### 4.2. FHH fractal model

The adsorption branch of the isotherms in these samples was used for fractal dimension analysis. Fig. 2 displays the FHH fractal analysis of sample #1 as a representative of all samples. In a certain  $P/P_0$  range (0.0085–0.961) (mainly the poly-molecular adsorption region), linear correlations exist between  $\ln(-\ln X)$  and  $\ln N$  which demonstrate that eqn (3) can be applied for fractal dimension calculations and analysis. Table 1 summarizes fractal dimensions of all samples with

Table 2 Summary of the fractal dimensions of the shale samples using Neimark fractal theory

Samples	$D_N$	$P/P_0$ range scale	$R^2$
#1	2.702	0.010–0.961	0.994
#2	2.631	0.010–0.956	0.997
#3	2.619	0.010–0.953	0.996
#4	2.498	0.010–0.953	0.989
#5	2.696	0.010–0.959	0.993
#6	2.495	0.055–0.959	0.991
#7	2.680	0.010–0.991	0.995
#8	2.702	0.010–0.956	0.995
#9	2.718	0.010–0.957	0.994
#10	2.743	0.053–0.921	0.993
#11	2.591	0.010–0.959	0.996
#12	2.742	0.010–0.958	0.993
#13	2.747	0.011–0.958	0.990
#14	2.687	0.010–0.956	0.995
#15	2.804	0.010–0.959	0.992
#16	2.539	0.010–0.956	0.994
#17	2.866	0.011–0.832	0.988
#18	2.898	0.010–0.883	0.994
#19	2.882	0.011–0.884	0.986

Table 3 Summary of the fractal dimensions of the shale samples using Wang-Li fractal theory

Samples	$D_{WL}$	$P/P_0$ range scale	$R^2$
#1	2.569	0.010–0.961	1.000
#2	2.517	0.010–0.956	1.000
#3	2.528	0.010–0.953	1.000
#4	2.392	0.010–0.958	0.999
#5	2.540	0.010–0.959	1.000
#6	2.408	0.010–0.959	0.999
#7	2.556	0.010–0.959	1.000
#8	2.564	0.010–0.959	1.000
#9	2.589	0.010–0.957	1.000
#10	2.627	0.010–0.954	1.000
#11	2.473	0.010–0.959	1.000
#12	2.596	0.010–0.958	1.000
#13	2.586	0.011–0.958	1.000
#14	2.549	0.010–0.956	1.000
#15	2.666	0.010–0.959	1.000
#16	2.425	0.010–0.956	1.000
#17	2.782	0.011–0.883	0.999
#18	2.820	0.010–0.883	0.998
#19	2.866	0.011–0.934	0.995



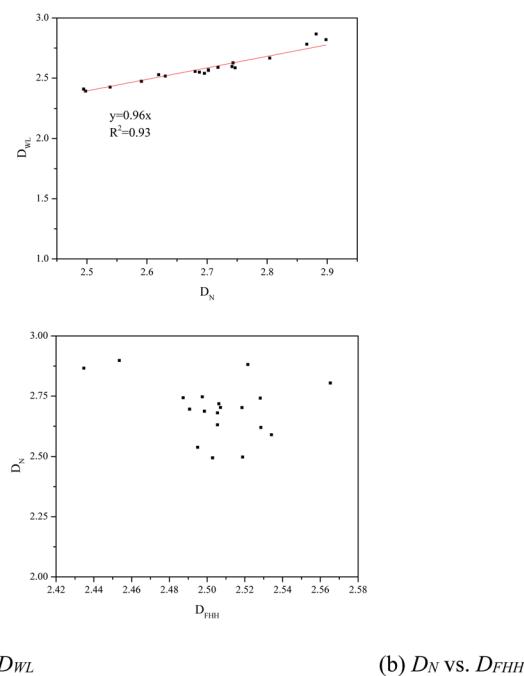


Fig. 5 Comparison of the fractal dimensions of shale samples using different models.

corresponding relative pressure intervals. The fractal dimension of all samples was calculated between 2 and 3, meaning those values are in a reasonable data range (2–3) based on the literature. Sample #15 has the largest  $D_{FHH}$  values while sample #17 the smallest value. The  $P/P_0$  range of these samples based on the FHH analysis varies between 0.10–0.88, showing that most measured data points in the experiment can be utilized for the FHH fractal analysis (Table 1).

#### 4.3. Neimark fractal model

Neimark fractal model was employed to estimate the fractal dimension of shale samples in this study as well. Fig. 3 shows the analysis result of sample #1 as a general representation. If relative pressure value is measured between the 0.010 and

0.961, linear correlations could exist between  $\ln S$  and  $\ln r$ , indicating the suitability of the application of the Neimark fractal model in the calculation of fractal dimension of the samples. The Neimark fractal dimensions  $D_N$  of all samples can be seen in Table 2. All fractal dimensions are also measured in the reasonable interval (2–3) based on previous studies and recommendation.<sup>4</sup> The  $P/P_0$  range which can be utilized in Neimark theory is very similar as the  $P/P_0$  range in the FHH model. From Table 2, sample #18 was calculated with the largest fractal value while sample #6 had the smallest fractal dimension value.

#### 4.4. Wang–Li model

Fig. 4 shows the fractal analysis results of representative sample #1 based on the Wang–Li fractal model. If the relative pressure ranges from 0.010 to 0.961, linear correlations can be established between the  $\ln A(X)$  and  $\ln B(X)$ . The fractal dimension values of all samples from this model also are found between 2 and 3 (Table 3), indicating that Wang–Li fractal model can also be applied in the fractal dimension calculation of our shale samples. Sample #4 and sample #6 have very close fractal dimension values and sample #17, #18, #19 have larger fractal dimension values compared with other samples, and these findings follow the results that are obtained by the Neimark model.

## 5. Discussions

Considering Tables 1–3, it is concluded that the fractal dimensions of samples would vary based on the model that is used. It can be seen that the FHH fractal dimension varies between 2.435 (sample #17) to 2.565 (sample #15) which is within a smaller range compared to the Neimark model (2.495–2.898) and the Wang–Li model (2.392–2.866). Furthermore, comparing all shale samples in this study, the fractal dimension values of the samples are close based on the Neimark model and Wang–Li model which were not the case in the FHH model. Overall, the results show that it'd necessary to compare all mainstream fractal dimension performance in pore structure

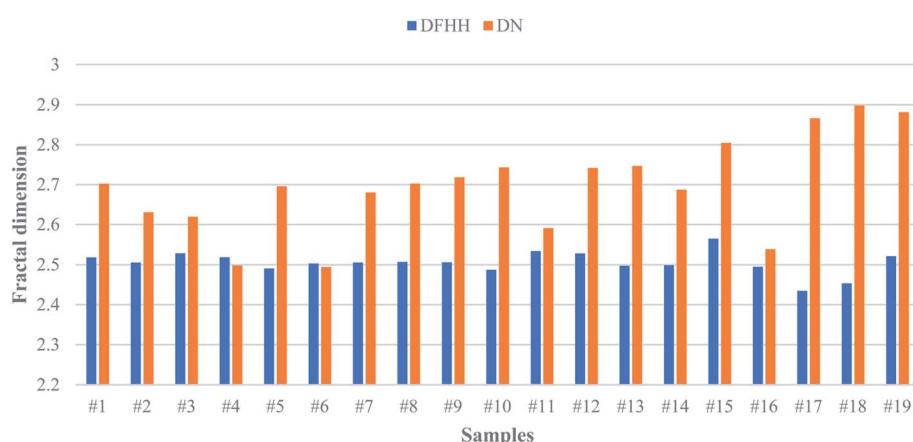


Fig. 6 The  $D_{FHH}$  and  $D_N$  of all the testing shale samples.



analysis and make an informed decision for future studies as which model is truly representing the samples nature.

Fig. 5 is a simple correlation between the fractal dimensions of these three models. Linear correlations exist between the  $D_N$  and  $D_{WL}$  (Fig. 5a) with the slope of the curve close to unity. This is an indication that fractal dimensions from Neimark and Wang–Li model for these shale samples are almost similar. However, it can be seen that there isn't any meaningful correlation between  $D_{FHH}$  and  $D_N$  (Fig. 5b).

The fundamental dependence of FHH model is on the pore volume of the absorbing film and its relationship with the pore radius (eqn (3)) while Neimark method foster to relate the surface area of the absorbing film to the pore radius.<sup>32</sup> Considering the Wang–Li model, the fundamental dependence of the theory is to correlate the pore volume of the absorbing film, pore surface area and the pore radius altogether. FHH model operates based on eqn (2) while Neimark and Wang–Li models are based on eqn (6) in a condensation regime. It should be note that both equations are very similar in their mathematical/physical format thus all the three models are based on Kelvin's equation.

In the condensation regime, concerning eqn (3), the FHH model can be written as:

$$N = K[\ln(P_0/P)]^{-(3-D_{FHH})} \quad (12)$$

The partial differentiation of eqn (12) can will become:

$$dN = K(D_{FHH} - 3)[\ln(P_0/P)]^{D_{FHH}-4} d[\ln(P_0/P)] \quad (13)$$

Substituting  $dN$  in eqn (13) into eqn (6) ends in the following expression:

$$S = K(D_{FHH} - 3) \frac{RT}{\sigma} (D_{FHH} - 2)^{-1} [\ln(P_0/P)]^{D_{FHH}-2} \quad (14)$$

In the next step, substituting  $r$  in eqn (7) to replace  $\ln(P_0/P)$ , the following equation will be derived:

$$S = K \frac{D_{FHH} - 3}{D_{FHH} - 2} \left( \frac{RT}{\sigma} \right)^{3-D_{FHH}} (2V_L)^{D_{FHH}-2} r^{(2-D_{FHH})} \quad (15)$$

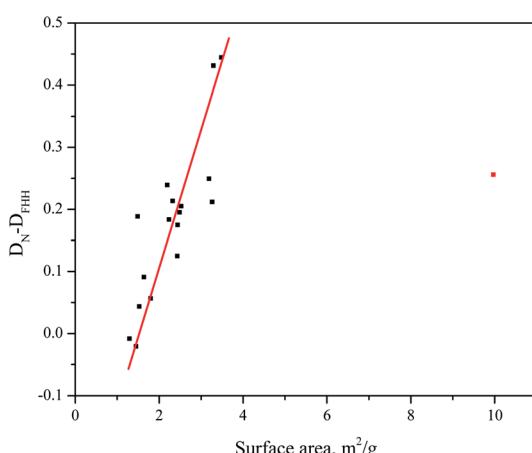


Fig. 7 The correlations between the surface area and  $(D_N - D_{FHH})$ .

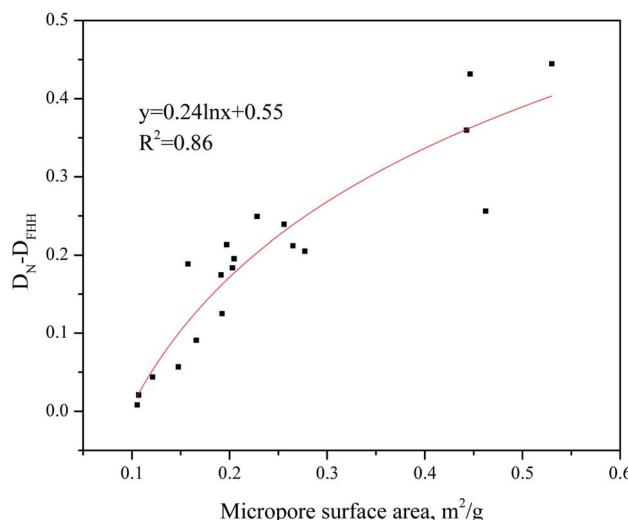
or

$$S/r^2 = K \frac{D_{FHH} - 3}{D_{FHH} - 2} \left( \frac{RT}{\sigma} \right)^{3-D_{FHH}} (2V_L)^{D_{FHH}-2} r^{-D_{FHH}} \quad (16)$$

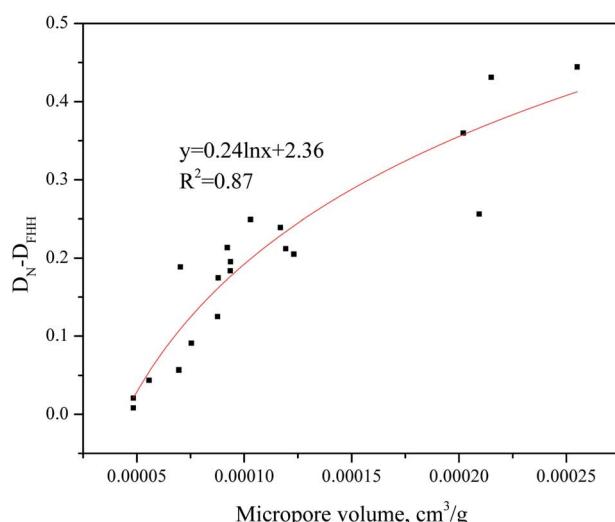
Through transforming eqn (15) and (16) into the double log format, the following is obtained:

$$\begin{aligned} \ln S &= \ln \left[ K \frac{D_{FHH} - 3}{D_{FHH} - 2} \left( \frac{RT}{\sigma} \right)^{3-D_{FHH}} (2V_L)^{D_{FHH}-2} \right] \\ &\quad - (D_{FHH} - 2) \ln r \\ &= \text{constant} - (D_{FHH} - 2) \ln r \end{aligned} \quad (17)$$

or



(a) Micropore surface area



(b) micropore volume

Fig. 8 The correlations between the micropore structures and  $(D_N - D_{FHH})$ .



$$\begin{aligned} \ln(S/r^2) &= \ln \left[ K \frac{D_{\text{FHH}} - 3}{D_{\text{FHH}} - 2} \left( \frac{RT}{\sigma} \right)^{3-D_{\text{FHH}}} (2V_L)^{D_{\text{FHH}}-2} \right] \\ &\quad + D_{\text{FHH}} \ln \frac{1}{r} \\ &= \text{constant} + D_{\text{FHH}} \ln \frac{1}{r} \end{aligned} \quad (18)$$

Eqn (17) is representing the curve in Fig. 5 while the format of eqn (18) is similar to eqn (10). These findings confirm that from a theoretical point of view, the fractal dimension calculation equations provided by the Neimark and Wang–Li can be derived by combining the Kelvin equation and the FHH fractal model. FHH model can also be viewed as a model with thermodynamics basis. From the thermodynamics viewpoint, these three models should be identical in the applicability of the FHH equation.<sup>33</sup>

However, the discrepancy that is observed in the experimental data from these shale samples from each model does exist. In order to find the answer to this important question, one should reconsider factors that introduce the difference in the data between among these models. Since the results from  $D_N$  and  $D_{WL}$  are very close, it was decided to only compare  $D_N$  and  $D_{\text{FHH}}$  in this study. Fig. 6 illustrates the histogram of fractal dimensions of from  $D_N$  and  $D_{\text{FHH}}$  of these shale samples. This figure explains that the  $D_{\text{FHH}}$  and  $D_N$  values from some of the samples are very close, for example, samples #4, #6, though the  $D_{\text{FHH}}$  and  $D_N$  values of samples #17, sample #18 are notably different.

Sahouli *et al.* (1996)<sup>10</sup> acquired FHH and Neimark model to study the fractal dimensions of commercial rubber grade carbon blacks. They found that the BET surface area can be used to explain the difference between the fractal dimensions that are calculated from different models. They argued if the BET surface area is large, the difference between the fractal dimensions would become significant. On the contrary, if the BET surface area is measured smaller, the fractal dimensions from these two methods will get closer to one another. In order to verify whether this theory is applicable to geomaterial samples

as well, correlations between the BET surface area on the x-axis and the difference between the  $D_N$  and  $D_{\text{FHH}}$  ( $D_N - D_{\text{FHH}}$ ) on the y-axis is plotted in Fig. 7. For the most samples, as the BET surface area increases, the difference between the  $D_N$  and  $D_{\text{FHH}}$  increases except sample #10 (the red point in Fig. 7). Therefore, it can be concluded that BET theory and its relationship with various outcomes by different fractal models that is proposed by Sahouli *et al.* (1996)<sup>10</sup> cannot fully explain the factors that may cause the difference in fractal dimensions or at least fully explain such discrepancy on geomaterials.

We further correlated the micropore structures (micropore volume and micropore surface area) and the  $D_N - D_{\text{FHH}}$  value which can be seen in Fig. 8. As the micropore surface area or the micropore volume increases in the samples, the value of  $D_N - D_{\text{FHH}}$  increases which fits the logarithmic law. This infers that in the shale samples, micropore structures could be responsible for the difference in fractal dimensions from these two different models.

## 6. Model selection

Considering the shale samples in this study, fractal dimensions from Wang–Li and Neimark model found to be similar and different from the FHH model results. As a result, Neimark and FHH models are compared in this section for further verifications. Based on the discussion earlier, both FHH and Neimark models are based on thermodynamics theories. Jaroniec *et al.* (1990)<sup>34</sup> studied the gas adsorption behavior on fractal surfaces in heterogeneous microporous solids from the thermodynamics viewpoint and concluded that microstructures could affect the fractal dimensions outcome. The correlations between the  $D_{\text{FHH}}$ ,  $D_N$  and the micropore surface area and micropore volume can be seen in Fig. 9 and 10, respectively. It can be seen that there isn't any clear correlation between the micropore surface area, micropore volume and  $D_{\text{FHH}}$  (Fig. 9) while positive relationships can be established between the micropore structures and  $D_N$  (Fig. 10). Collectively, this means that the  $D_N$  would not only reflect the fractal dimension in the capillary condensation regime but also infers to the micropore

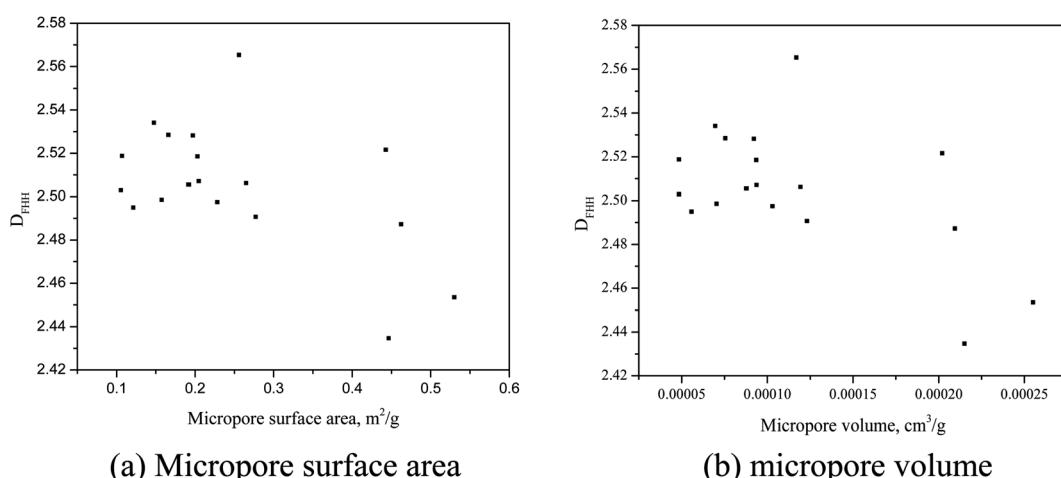


Fig. 9 The correlations between the micropore structures and  $D_{\text{FHH}}$ .



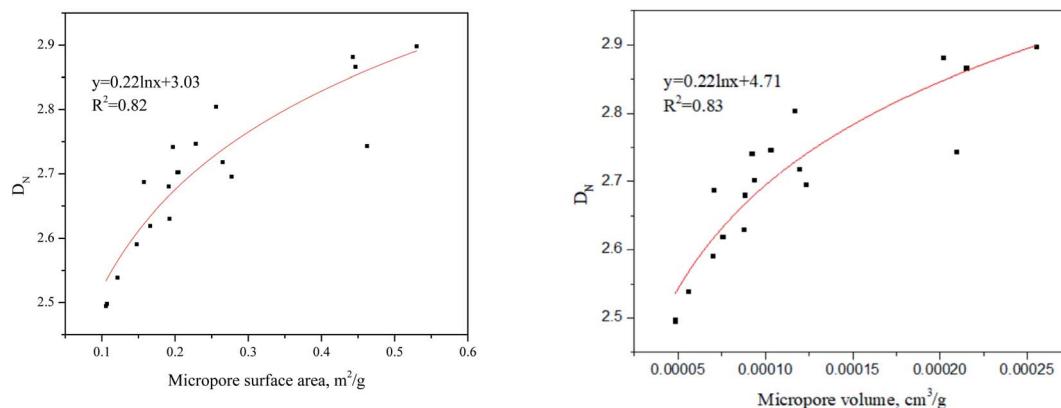


Fig. 10 The correlations between the micropore structures and  $D_N$ .

information of geomaterials. This is found beyond the ability of FHH model.

Based on the above discussion, it can be said, if micropores in the shale samples are not abundant, then either of the three models can be used and they will generate similar results. However, if shale sample or any geomaterial that has a fractal behavior has abundant micropores, the whole gas adsorption process will be a mixture of the poly-molecular and capillary condensation, thus  $D_N$  and  $D_{WL}$  which are affected by the micropores and the capillary condensation are preferred. Based on our previous studies, the micropores in the Bakken shale are mainly existing in the organic matter and clay minerals.<sup>29</sup> If the Bakken shale samples have abundant organic matter and clay minerals, the  $D_{FHH}$  will not be suitable for the characterization of pore structure. However, if the Bakken is free from huge quantities of clay minerals and organic matter, these three models can all be appropriate for analysis.

## 7. Conclusions

In this study, 19 shale samples were selected from the Bakken Formation and  $N_2$  adsorption experiments were performed to analyze their pore structures. Three different models (FHH model, Neimark model, and Wang–Li model) were employed to study and compare the fractal dimensions in these shale samples. The following few conclusions can be derived from this study:

(1) The FHH, Neimark model and Wang–Li model all can be applied for fractal dimension analysis of shale samples. The fractal dimensions obtained from the Neimark and Wang–Li model are similar while the results are different from the fractal dimension values calculated from FHH model.

(2) The microstructures in the shale samples are the main reason to explain the disagreement of the fractal dimensions results from the Neimark and FHH models. It is concluded that a larger micropore surface area (or the micropore volume), will lead to the major discrepancy between these two aforesaid models.

(3) If there aren't a large number of micropores in the shale sample, all these three models can be applied for fractal dimension calculation of geomaterials.

(4) Ultimately,  $D_N$  (or  $D_{WL}$ ) do not denote only the capillary condensation process in the pores but also infer to the micropore information which makes them preferred models to be used when micropores are abundant in the sample compare to  $D_{FHH}$ .

## Conflicts of interest

There are no conflicts to declare.

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