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Iron-based single-atom electrocatalysts: synthetic strategies and applications

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The performance and cost of electrocatalysts play an important role in the development and application prospects of energy conversion technology. Single-atom catalysts (SACs) have constituted a new frontier in the field of catalytic science in recent years. As a non-precious metal, iron (Fe)-SACs show great potential in the field of electrocatalysis, which is comparable to or even better than the performance of precious metal catalysts. However, a robust, generic synthetic strategy toward atomically dispersed Fe catalysts is still lacking, which is still a formidable challenge to maintain the dispersion of Fe atoms at high temperatures and to obtain high catalytic activity. In this review, the latest progress in the synthesis of Fe-SACs is introduced and summarized, and the electrochemical applications of Fe-SACs are further summarized and discussed. Herein, the relationship between the structural characteristics and performance of Fe-SACs is further introduced and discussed. Finally, the existing problems and development prospects of Fe-SACs are discussed.

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1. Introduction

Single-atom catalysts (SACs) combine the advantages of heterogeneous catalysts and homogeneous catalysts, and bridge the gap that exists between them with their unique performance. It is expected to become a bridge between homogeneous catalysis and heterogeneous catalysis, which has been a rising star in the field of catalysis in recent years.^{1,2} SACs have the advantages of maximum atomic utilization, uniform active sites, adjustable electronic environment, high catalytic activity

and selectivity, better stability, and excellent recyclability. However, whether in the process of preparation or in the subsequent application process, the strong trend of migration and aggregation of active atoms and the controllable preparation of SAC is still a challenging task.^{3–11} Transition noble metal monatomic catalysts such as ruthenium (Ru), silver (Ag), rhodium (Rh), palladium (Pd), iridium (Ir), platinum (Pt), and gold (Au) have been widely used in various electrochemical reactions such as oxygen reduction reactions (ORRs), hydrogen evolution reactions (HERs), carbon dioxide reduction reactions (CO₂RRs), and oxygen evolution reactions (OERs).^{12–15} However, the high cost and low natural abundance of precious metals seriously hinder the wide range of applications of these technologies. Therefore, the monatomic catalyst of non-precious metals has become the research focus of the majority of

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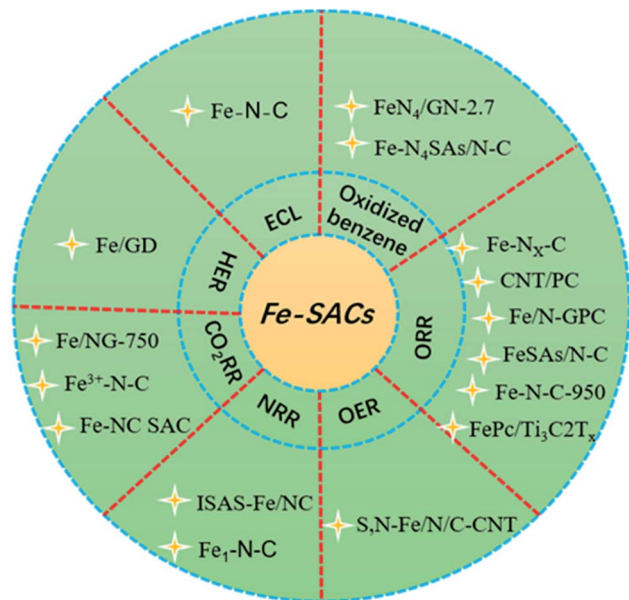


Fig. 1 Applications of Fe-SACs.

scholars. The latest research shows that iron (Fe)-SACs can be used in a variety of electrocatalytic reactions such as HERs, ORRs, nitrogen reduction reactions (NRRs), and CO₂RRs (Fig. 1), exhibiting the same or even better catalytic performance than precious metal catalysts (the specific performance of the catalyst is described in detail in the section describing applications of Fe-SACs).^{8,16–19} These results provide a new possibility for the substitution of precious metal catalysts and show a great application prospect.

To date, the preparation of Fe-SAC and its application in the field of electrocatalysis have not been reviewed. Therefore, it is necessary to comprehensively review the determinants of its preparation method, structure, and activity to provide a basis for the design of this type of catalysts and promote further research and development in this field. In this article, we present an in-depth understanding of Fe-based SACs from the following aspects: (1) the relationship between structural characteristics and performance, (2) the application in the field of electrocatalysis, and (3) the preparation strategy of Fe-based

SACs. Finally, we look forward to the prospects and challenges of Fe-SACs.

2. Active sites of monoatomic iron catalysts

Several factors affect the activity of Fe monatomic catalysts; however, it is still a great challenge to clarify their structure–property relationship. According to the current research progress of Fe monatomic catalysts, the active sites of Fe monatomic catalysts are closely related to the local environment of Fe atoms, that is, the coordination number and electronegativity of adjacent atoms. Therefore, most of the research studies are mainly focused on Fe–N–C catalysts. Although the Fe–N–C catalyst shows excellent catalytic performance, it usually leads to the formation of Fe active sites with different coordination configurations. The heterogeneity of these structures and components makes the determination of the active sites and the relationship between the structure and catalytic performance very complicated. Fe atoms have a large number of empty d orbitals and different types of coordination structures, thus according to the number of Fe atoms and coordinated nitrogen atoms in the active sites, there are mainly four types of active sites of Fe monoatomic catalysts: Fe–N₄, Fe–N₂, Fe–N₆, and Fe–N_x, among which Fe–N₄ is the most reported active site. The structure of the carrier comprising the location of these active sites and the surface loading rate also has a significant impact on the catalytic performance. Different types of Fe active sites show different catalytic properties for different electrocatalytic applications. In recent years, research efforts have been devoted to the theoretical simulation and experimental verification of Fe-SACs, mainly to establish the relationship between the local atomic structure and catalytic performance, in order to explore its potential application in electrocatalysis.

The monatomic Fe catalyst dispersed on nitrogen-doped graphene (Fe/NG) reported by Zhang *et al.*²⁰ consists of a pyridine-type Fe–N₄ structure, and nitrogen doping plays an important role in improving the conversion of CO. A small amount of Fe atoms loaded in NG could form a Fe–N₄ site capable of enhancing the adsorption of CO₂ and improving the activity of CO₂. Fig. 2a and b demonstrate that the mechanism includes the following steps: (1) CO₂ + * + H⁺ + e[−] → COOH*, (2) COOH* + H⁺ + e[−] → CO* + H₂O, and (3) CO* → CO + *, where * represents the active site on the surface of the catalyst. Moreover, the three free energy diagrams with different nitrogen doping configurations of graphite indicate that the nitrogen substitution on graphene improves the catalytic activity of the Fe–N₄ moieties by lowering the energy barrier of COOH* formation, as well as facilitating the CO* desorption step.

The Fe monoatomic catalyst Fe SAs/N–C reported by Yang *et al.*²¹ consists of a single Fe–N₄ as the active site and shows outstanding performance toward ORRs. They used extended X-ray absorption structure (EXAFS) and X-ray absorption near-edge structure (XANES) to study the coordination environment and chemical state of Fe–SAs/N–C. Fig. 3a shows that the single atom of Fe in Fe SAs/N–C may be in a low-valence state (0



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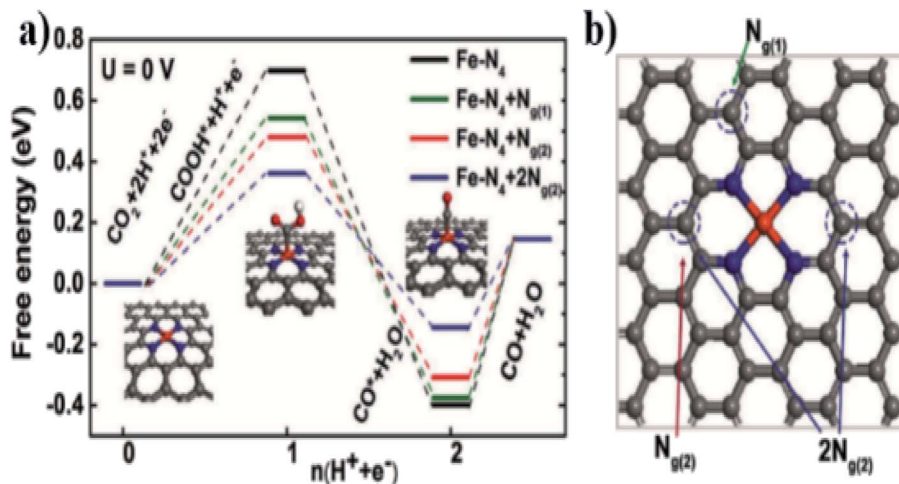


Fig. 2 Theoretical calculations and proposed mechanism on the nitrogen-coordinated Fe catalytic site. (a) Free energy diagram of electrochemical CO₂ reduction to CO on Fe–N₄ moieties embedded on graphene sheets. (b) Top view of the optimized structures of Fe–N₄ moieties embedded on graphene layers and potential nitrogen-substitution.

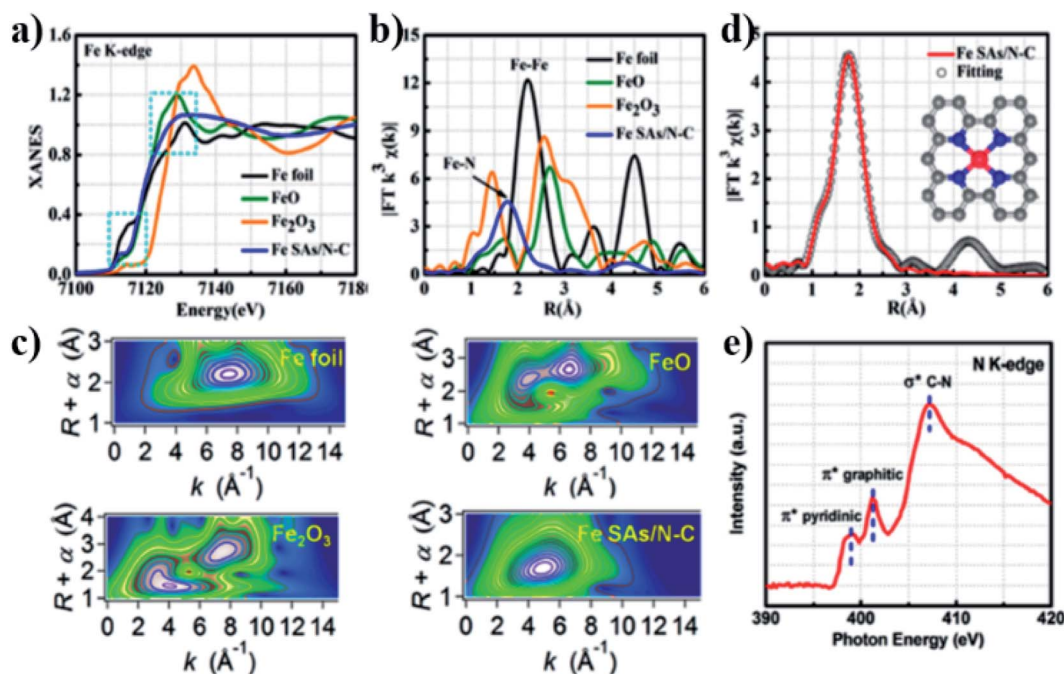


Fig. 3 (a) XANES and (b) FT-EXAFS curves of Fe SAs/N–C and references at the Fe K-edge. (c) WT-EXAFS of the Fe foil, FeO, Fe₂O₃ and Fe SAs/N–C. (d) FT-EXAFS fitting curve of the Fe SAs/N–C sample. Inset: atomic structure model of Fe SAs/N–C, Fe (red), N (blue), and C (gray). (e) N K-edge NEXAFS spectrum of Fe SAs/N–C.

$< \delta < 2$). Fig. 3b demonstrates that the main peak of the catalyst corresponds to Fe–N coordination, and its central position is about 1.5 Å. The results indicated that Fe atoms were loaded onto N-doped carbon nanosheets in the form of single atoms. Fig. 3c illustrates that the wavelet transform (WT) diagram of Fe SAs/N–C shows only one intensity maximum at 5 Å⁻¹, which can be specified as Fe–N coordination. The EXAFS measurement and fitting curve (Fig. 3d and Table 1) indicate that the Fe single atom has a good Fe–N₄ structure. Three peaks of pyridine N π*

Table 1 Structural parameters extracted from the Fe K-edge EXAFS fitting ($S02 = 0.74$)

Sample	Scattering pair	CN	R (Å)	σ_2 (10 ⁻³ Å ²)	ΔE_0 (eV)	R factor
Fe SAs/N–C	Fe–N	4.2	2.03	8.9	4.5	0.0078
Fe foil	Fe–Fe1	8*	2.48	5.9	0.5	0.0057
Fe foil	Fe–Fe2	6*	2.84	7.2	0.5	0.0057



(399.5 eV), graphitized N π^* (402.4 eV) transition, and the formation of C–N σ^* bond (408.5 eV) were observed in the N-K edge spectrum shown in Fig. 3e.

The activity of the ORR was enhanced by selectively breaking the C–N bond at the edge of the active site of Fe–N₄.²² Five Fe–N₄/C models with different edge N atoms were proposed through density functional theory (DFT) (Fig. 4a). At the equilibrium potential $U = -0.77$ V (vs. SHE) (Fig. 4b), the free energy change (ΔG) of the four-electron reduction path was negative, thus it was exothermic. However, Fig. 4c shows that the first electron transfer sub-step ($*\text{O}_2 + \text{H}_2\text{O} + \text{e}^- \rightarrow *\text{OOH} + \text{OH}^-$) has a maximum positive ΔG ; therefore, this step is a step that determines the rate of the reaction process. FeN₄-6r-c1 and FeN₄-6r-c2 have lower values of ΔG , which are 0.31 and 0.32 eV, respectively. However, for step 5 ($\text{OH}^* + \text{e}^- \rightarrow \text{O}^-$), FeN₄-6r-c1 showed higher resistance (0.72 eV) and better overcoming ability for FeN₄-6r-c2 with a higher cleavage degree (0.13 eV). In general, the defect FeN₄-6r-c2 is located at the edge of the cavity and has the lowest total reaction free energy change (0.32 eV). These results confirm that the C–N structure changes the charge density distribution and electronic structure of the active site.

Serov *et al.*²³ believed that the active site of the catalyst not only comprised Fe–N, but also included some in-plane and edge defects. Fig. 4d shows the schematic of in-plane Fe–N_x defects and edge defects in a hypothetical graphene sheet. Edge defects include nitrogen and oxygen, and they may also contain Fe–N_x. All these defects may act as potential active sites in ORRs.

Pan *et al.*²⁴ further revealed the intrinsic electronic properties of the coordination effect through DFT calculations, as shown in Fig. 5. The coordination mode of Fe–N leads to a change in the structure and electronic properties of the catalyst, thus affecting the path of the catalytic reaction and the formation of intermediates. The increase in the Fe–N coordination number facilitates the generation and activation of the crucial

intermediate O=Fe=O species, thereby enhancing the BOR activity. More interestingly, when the coordinated N atom is replaced with one or two C atoms, the BOR activity of the monatomic Fe site catalyst decreases gradually, showing obvious coordination sensitivity. Therefore, the monatomic Fe center fixed by four nitrogen atoms showed the highest BOR performance, with 78.4% conversion and 100% phenol selectivity at 30 °C, exceeding those of all reported BOR catalysts.

The ORR activity with typical Fe–N₄ active sites was improved by introducing suitable carriers. For example, the intrinsic ORR activity of the original Fe phthalocyanine (FePc) catalyst with the added two-dimensional (2D) material Ti₃C₂T_x as the carrier was twice as high as that of the FePc catalyst.²⁵ FeN₂ and FeN₆ active sites are considered to have great potential in the development of new advanced Fe-based monatomic electrocatalysts. Yansong Zhu²⁶ confirmed that the active site of a six-coordinated Fe(III) complex [Fe(III) (porphyrin)(pyridine)₂] was six-coordinated FeN₆. The non-noble metal catalyst for ORRs showed high activity and good durability. Zheng *et al.*²⁷ designed and developed a range of molecule-level graphitic carbon nitride (g-C₃N₄)-coordinated transition metals catalysts for these oxygen electrode reactions. The correlation of experimental and computational results confirmed that this high activity originated from the precise M–N₂ coordination in the g-C₃N₄ matrix.

Asnavandi *et al.*²⁸ first studied the overpotential of the surface without oxygen vacancies (OVs). Oxygen vacancies refer to vacancies formed in metal oxides or other oxygen-containing compounds where oxygen atoms (oxygen ions) in the crystal lattice break away, resulting in oxygen deficiency. Fig. 6a shows the geometric structure of the OER and the calculated ΔG . $\Delta G_{\text{max}} = 1.78$ eV, which led to an overpotential of 0.55 V when the OER occurred at the Fe site. When oxygen (represented by the circle in Fig. 6b) was removed to produce OV and the low

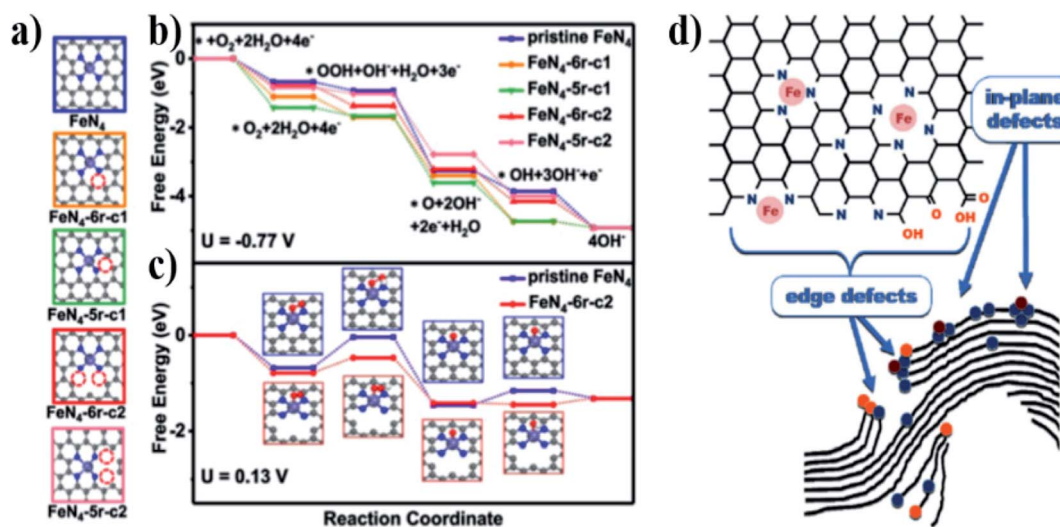


Fig. 4 (a) Five possible atomic configurations with different cracking degrees (6r or 5r refers to the six- or five-membered Fe–N₄ heterocyclic ring, respectively; c1 or c2 refers to the cleavage of one or two C–N bonds adjacent to Fe–N₄, respectively). Free energy diagram (b) at $U = -0.77$ V and (c) at $U = 0.13$ V (vs. SHE). (d) Schematic of the transition metal-containing nitrogen defects in graphene sheets (Fe–N_x) and other possible defects that may have catalytic activity in ORRs and its component reactions.



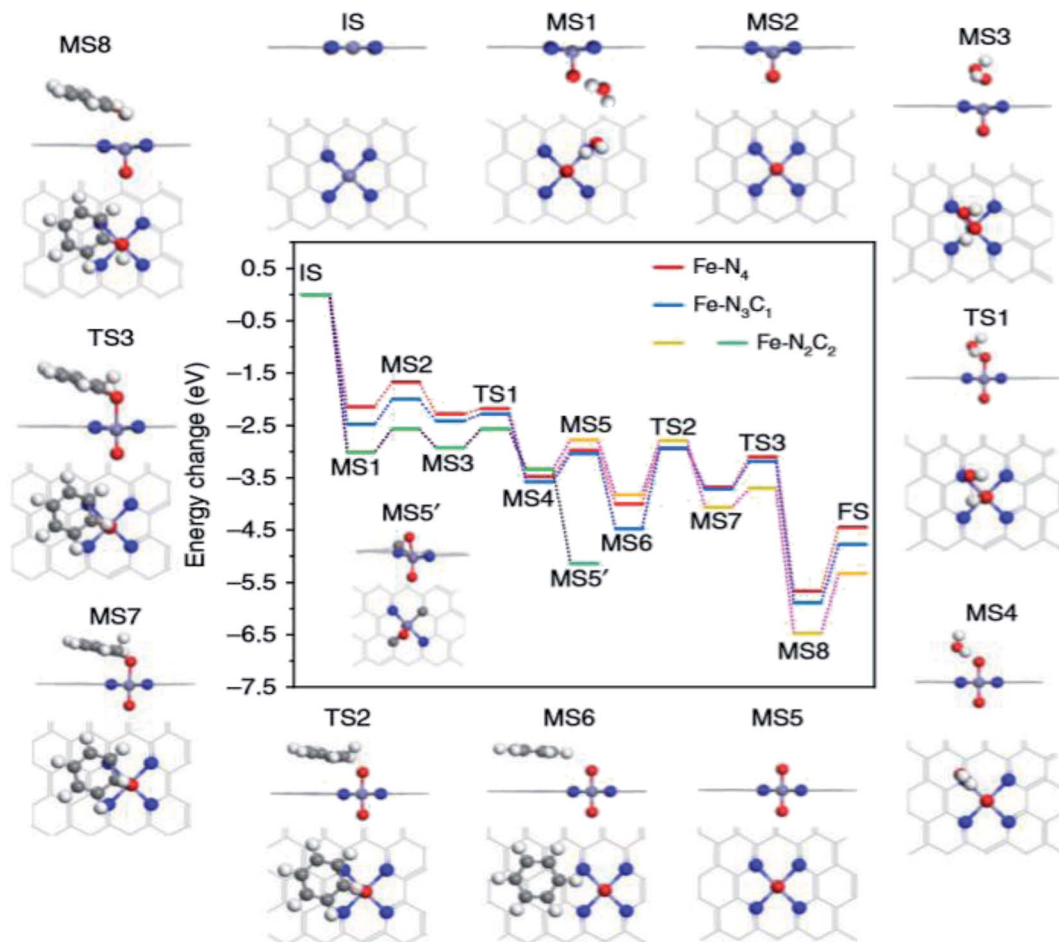


Fig. 5 DFT calculation. Energy diagram of benzene oxidation on Fe- N_xC_y SAs/N-C catalysts with the related reaction configuration on Fe- N_4 surrounded (IS: initial catalyst, MS1: the first H_2O_2 cleavage adsorption, MS2: Fe=O configurations, MS3: the second H_2O_2 adsorption on the opposite side, TS1: transition state of the formation for the second H_2O , MS4: the second H_2O adsorbed configuration, MS5: O=Fe=O moiety, MS5': the abnormal O=Fe=O species on Fe- N_2C_2 , MS6: adsorption of C_6H_6 , TS2: transition state of C-O bond generation, MS7: C_6H_6O adsorption structure, TS3: transition state of H transfer from C to O, MS8: product bonded species, FS: regeneration of activity Fe=O center). The white, gray, red, blue and bluish violet balls refer to H, C, O, N, and Fe atoms, respectively.

coordination metals (LCMs) were marked as Fe 4c and Ni 4c, the reactant species (O, OH, and OOH) got adsorbed and relaxed completely on it. Its geometric structure and calculated value of ΔG are shown in Fig. 6b; ΔG_{\max} is 1.41 eV and overpotential $\eta = 0.18$ V. Compared to the case without OV, the overpotential decreased by 0.37 V, which indicated that the LCM activity associated with OV was higher, which is consistent with the understanding in the earlier study that the high catalytic performance of NiFe-OOH results from poorly coordinated metals such as defects, steps, and edges.²⁹

In order to further describe the active sites and catalytic performance of Fe monoatomic catalysts, we collected some information about Fe monoatomic catalysts, including reaction precursors, types of active sites, and loading, as presented in Table 2. These are the key factors affecting its activity. Therefore, the activity of the catalyst can be regulated by selecting precursors or loading to form Fe active sites. For example, doping heteroatoms (such as P, S, and N) on the substrate aids in the adjustment of the electronic structure of the Fe active site. It is also possible to control the density of Fe active points

by changing the Fe loading rate, thereby adjusting the performance and application of the catalyst.

In short, the main factors affecting the catalytic activity of Fe-SACs and its potential application in electrocatalysis include the coordination structure and electronic structure of Fe, the morphology and electronic structure of the conductive matrix, and the total number of Fe atom active sites.

3. Synthetic strategies of Fe-SACs

Recently, various experimental techniques for the preparation of Fe single atoms have been reported. Moreover, according to the reported process, the preparation of Fe monoatomic catalysts can be summarized into the following three strategies.

3.1. Strategy of wrapping iron active sites in roasted metal-organic frameworks

In recent years, metal-organic frameworks (MOFs) have attracted significant attention because of their good porous structure and highly ordered arrangement of organic



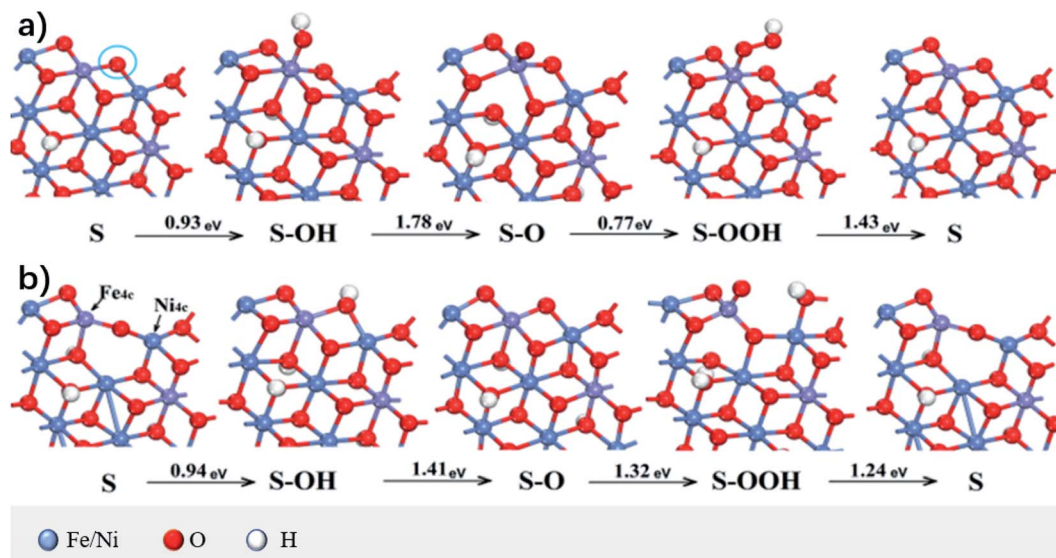


Fig. 6 OVs' effect on OER catalysis performance predicted by DFT calculations. Intermediate states (S represents the active site on the surface of the catalyst, S-OH, S-O, and S-OOH, four elementary reactions: ① $S + \text{OH}^- \rightarrow S\text{-OH} + e^-$, ② $S\text{-OH} + \text{OH}^- \rightarrow S\text{-O} + \text{H}_2\text{O} + e^-$, ③ $S\text{-O} + \text{OH}^- \rightarrow S\text{-OOH} + e^-$, ④ $S\text{-OOH} + \text{OH}^- \rightarrow S + \text{O}_2 + \text{H}_2\text{O} + e^-$) and Gibbs free energy changes associated with the elementary reactions of OERs on Fe-doped NiOOH (a) without OV and (b) with OV.

connectors and metal nodes. Both MOFs and MOF-derived materials can still maintain their specific shape and pore structure after pyrolysis at high temperatures. Notably, they provide a pathway for the effective transfer and diffusion of substrates and products, providing a high-quality platform for Fe active sites. The synergistic effect and pore limitation effect can be produced between the active site of Fe and the MOF shell. Metal nodes and aromatic connectors in MOFs can establish charge transfer interactions with Fe active sites by coordination or π - π interaction, thus performing collective functions compared to single-component materials. Moreover, the MOF shell effectively wraps the Fe active site and prevents the agglomeration and leaching of Fe atoms, thus improving the stability of the catalytic process. Therefore, MOF coating strategy is widely used in the preparation of Fe-SACs. However, although intensive efforts and great progress have been made in this area, the study on Fe active sites coated with porous MOFs is still in its infancy and many challenges still need to be overcome. The composition and spatial distribution of Fe active sites in MOFs are still difficult to control, and it is also very hard and challenging to effectively balance the relationship between heterogeneous nucleation and controllable growth of MOFs around Fe active sites and self-nucleation and homogeneous growth. Moreover, the electrical conductivity and ionic conductivity of MOFs are also important factors significantly affecting its electrocatalytic performance. For example, Qi-Long Zhu and his colleagues³¹ used MIL-101-NH₂ as the MOF host to accommodate dicyandiamide, the nitrogen source with high nitrogen content, and FeCl₃, the most readily available Fe source. In order to avoid the deposition of precursors on the outer surface of a MIL-101-NH₂ crystal, dicyandiamide and FeCl₃ were quantitatively coated by a double-solvent method. Fig. 7a shows the monatomic catalyst, Fe/N-GPC, obtained by

pyrolysis and acid etching of the synthesized MOF composite, exhibiting that the complete MOF skeleton of the catalyst was well maintained. Xiao *et al.*³³ pyrolyzed Fe triacetylacetonate Fe-doped ZIF-8 as the metal source, nitrogen source, and carbon source to form monatomic catalyst Fe-N-C-950 (Fig. 7b). Han *et al.*¹⁸ synthesized Fe-Phen complexes at room temperature using FeSO₄ and Phen as non-precious metal and organic ligands, respectively. Then, during the growth of ZIF-8, the Fe-Phen species were wrapped in nano-cages. The monatomic catalyst Fe-N_x-C was obtained after pyrolysis in an argon atmosphere at 900 °C (Fig. 7c). Jiang *et al.*²² used ZIF-8 as the host of MOFs to hold Fe(II)Pc. During the assembly of Zn(II) and 2-methylimidazole, Fe(II)Pc molecules were encapsulated in the cavity of a zeolite imidazole skeleton to form FePc-x@zif-8 nanocomposites. Monatomic catalyst Fe SAS-N/C-20 was obtained by pyrolysis and acid etching, and the complete MOF of the catalyst was well maintained (Fig. 7d). Li *et al.*³⁷ synthesized a flaky MOF by the interaction between N-rich dicyanoimidazole and ferric acetate. By using the MOF as the host, Fe acetate was coated, and the monatomic catalyst DCI-Fe was prepared by pyrolysis (Fig. 7e). Lü *et al.*¹⁹ prepared a bimetallic Fe/Zn zeolite imidazole framework (ZIF-8) by a hydrothermal method and then carbonized and etched it to obtain monatomic catalyst ISAS-Fe/NC (Fig. 7f). Zhang *et al.*³⁵ synthesized a Fe-containing rod-like MOF from ZrOCl₂ and tetra(*p*-carboxyphenyl)porphyrin and tetra(*p*-carboxyphenyl)porphyrin Fe in DMF and trifluoroacetic acid. In this porphyrin MOF, they successfully constructed the Fe atom-dispersed catalyst Fe1-N-C by reasonably controlling the distance between the adjacent Fe atoms (Fig. 7g). Zhang *et al.* prepared catalyst precursors with different Fe contents by using Fe ions to replace part of the original Zn ions to control Fe doping in ZIF-8. Through the subsequent high-temperature treatment, the Fe-doped ZIF was directly



Table 2 Brief introduction of some information on Fe-SACs

Sample	Active site	Precursor	Loading rate	Application	Reference
S,N-Fe/N/C-CNT	Fe-N _x	FeCl ₃ , KSCN, carbon nanotubes, 2,2'-bipyridine		ORR, OER	16
Fe-NC SAC	Fe-N ₄	Fe(NO ₃) ₃ , glucose, oxygen-rich porous carbon, melamine	12.1wt%	CO ₂ RR	17
Fe-N _x -C	Fe-N _x	FeSO ₄ , Phen, ZIF-8	0.81wt%	ORR	18
CNT/PC	Fe-N ₄	Fe(III)TMPPCl, PC, carbon nanotubes	2.9wt%	ORR	30
Fe/N-GPC	Fe-N ₄	FeCl ₃ , dicyandiamide, MIL-101-NH ₂	1.1wt%	ORR	31
Fe SAS/N-C	Fe-N ₄	PEI, Phen, FeCl ₂ , C ₃ N ₄ nano sheet	3.5wt%	ORR	21
Fe SAS-N/C-20	Fe-N ₄	Fe Pc, ZIF-8	0.20wt%	ORR	22
Fe-CBDZ	Fe-N _x	Fe(NO ₃) ₃ ·9H ₂ O, CBDZ		ORR	23
Fe-N-C	Fe-N ₄	Fe ³⁺ , ZIF-8	1.5wt%	ORR	32
Fe-N-C-950	Fe-N ₄	Fe(NO ₃) ₃ , ZIF-8	0.137wt%	ORR	33
Fe Pc/Ti ₃ C ₂ T _x	Fe-N ₄	Fe Pc, Ti ₃ C ₂ T _x	4.09wt%	ORR	25
PpPD-Fe-C	Fe-N ₆	<i>p</i> -Phenylenediamine, ferric chloride, carbon black	12.08wt%	ORR	26
Fe ³⁺ -N-C	Fe-N _x	FeCl ₂ , ZIF-8	2.6wt%	CO ₂ RR	34
Fe/NG-750	Fe-N ₄	Graphene oxide, FeCl ₃	0.52wt%	CO ₂ RR	20
ISAS-Fe/NC	Fe-N ₄	C ₃₄ H ₃₂ FeN ₄ O ₄ , ZIF-8	4.2wt%	NRR	19
Fe1-N-C	Fe-N ₄	FeCl ₂ ·4H ₂ O, meso-tetra (4-carboxyphenyl) porphine tetramethyl ester	4.51wt%	NRR	35
Fe-N-C	Fe-N _x	Glucose, dicyandiamide, FeCl ₂ ·4H ₂ O	0.26wt%	ECL	36
Fe/GD		Graphdiyne, FeCl ₃	0.680wt%	HER	8

converted into carbon with high specific surface area (SSA) to form a specific framework of the Fe-based porous carbon monoatomic catalyst Fe-ZIF.^{6,32,34,38}

3.2. Strategy including modified carbon-rich carriers

Carbon-rich carriers including graphene (or graphene oxide (GO)) sheets, carbon nanotubes (CNTs), carbon nanofibers,

carbon nanospheres, nano-carbon derived from polycarbonate, and other polymer-derived nano-carbon materials have porous structures for rapid mass and energy transfer and an adjustable chemical coordination environment, thus they can be considered as ideal carriers for Fe monoatomic catalysts. The use of chitosan, cyanamide, dicyandiamide, melamine, and porphyrin also shows the potential to capture Fe atoms *via* surface

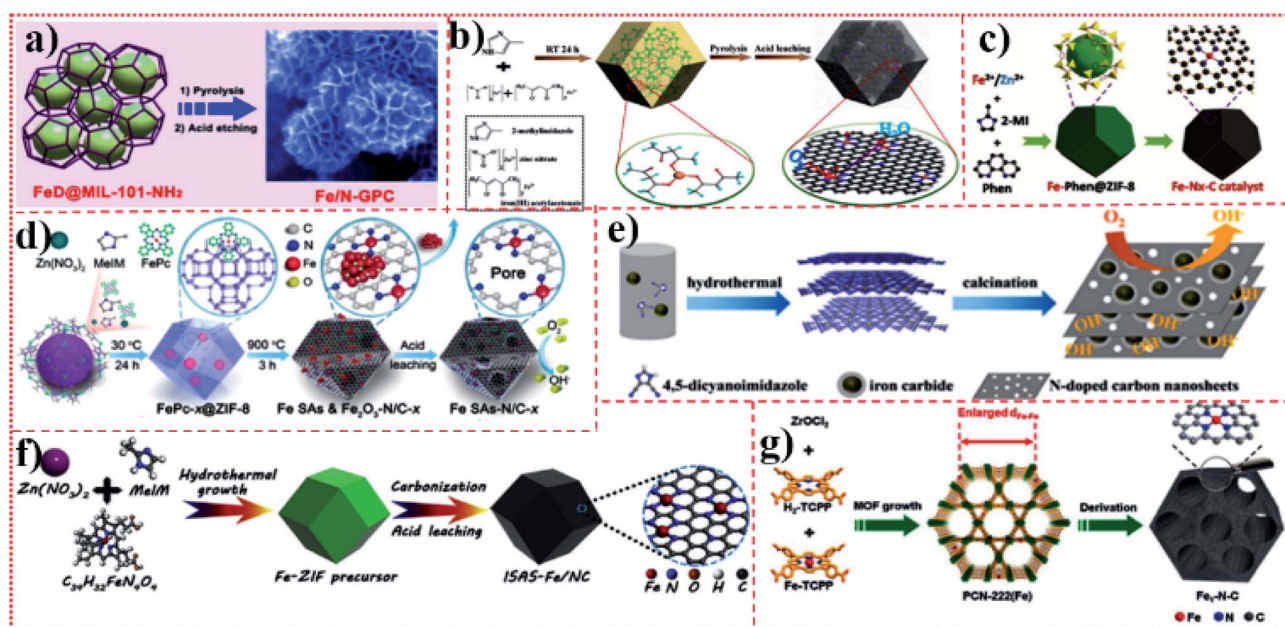


Fig. 7 (a)–(g) Schematic of Fe-SACs with a metal–organic framework as a catalytic application platform.



modification of carbon-rich carriers, in order to achieve efficient electrocatalytic performance. Although this strategy has been developed to some extent, it still faces multiple challenges to be addressed. The loading of this type of Fe monatomic catalyst is relatively low, which may limit its further development in large-scale applications. The carrier (graphene or GO) mainly depends on the structure of graphene or GO, which is fragile and easy to break, thus it is difficult to be characterized and controlled by a synthesis strategy. This method of preparing Fe active site by introducing doping and manufacturing defects to adjust the local electronic state on the surface of the carrier is difficult to control regularly. Chen *et al.*¹⁶ achieved monoatomic dispersion of Fe(S,N-Fe/N/C-CNT) on the layered carbon modified with N and S by coating 2-bipyridine and Fe salt precursors onto the surface of CNTs, followed by pyrolysis and acid etching in a nitrogen atmosphere (Fig. 8a). Zhu *et al.*³⁹ prepared CNT precursors by a one-step hydrothermal method using tellurium nanowires, glucosamine hydrochloride, and ammonium ferric sulfate (catalyst) at 180 °C for 15 h. The resulting hydrogel was soaked several times in distilled water to remove impurities and then freeze-dried. Finally, the monatomic catalyst Fe-N-CNTAS-5-900 was obtained by heat treatment in a nitrogen atmosphere for 2 h (Fig. 8b). Yang *et al.*¹³ used Fe-loaded F127 [F127 is a water-soluble surfactant of polyoxyethylene-polyoxypropylene-polyoxyethylene (PEO-PPO-PEO)] and $g\text{-C}_3\text{N}_4$ to form layered precursors, and then obtained monoatomic catalyst SA-Fe/NG by pyrolysis (Fig. 8c). Further, Mun *et al.*⁴⁰ used ferrous chloride hexahydrate and 1,10-phenanthroline (Phen) as precursors and mesoporous carbon foam as a support, and obtained

monoatomic catalyst FeNC-S-MSUFC by pyrolysis and acid etching (Fig. 8d). Yang *et al.*²¹ used polyetherimide (PEI) polymers as carbon precursors and Phen ligands as spatial isolating agents for Fe ions to promote their complete conversion into a single Fe atom without forming Fe nanoparticles (NPs), and N-doped porous carbon nanosheets as carriers to form a highly stable monoatomic catalyst, Fe SAs/N-C, by high-temperature pyrolysis (Fig. 8e). Zhang *et al.*²⁰ used GO as the precursor, annealed the mixture of GO and FeCl_3 in an Ar/ NH_3 atmosphere at 800 °C and fixed the Fe atom on graphene by a N bond, and obtained Fe/NG with monoatoms dispersed on NG (Fig. 8f). Zhao *et al.*¹⁷ reported a cascade anchoring strategy for synthesizing Fe-NC structures. Fe ions were first chelated with chelating agents (such as glucose), then fixed on oxygen-rich porous carbon carriers with high SSA, and finally pyrolyzed at a certain temperature to form Fe-N_x catalytic sites. The function of the chelating agent is to protect the Fe ion and combine it with the oxygen-rich carbon carrier (Fig. 8g). Sa *et al.*⁴¹ mixed CNTs with porphyrin Fe precursors, heated the CNTs adsorbed by porphyrin to 400 °C, and formed CNTs with a porphyrin layer *via* π - π interaction. Second, the surface of the composite was covered with a layer of silicon dioxide (SiO_2). Finally, the ternary composite was pyrolyzed at high temperatures, and then the SiO_2 layer was etched to obtain the Fe monoatomic catalyst CNT/PC (Fig. 8h). Varela *et al.*⁴² first carried out *in situ* polymerization using Fe chloride and aniline as precursors and ammonium persulfate as an oxidant, and then added Kaijin black carbon powder for continuous annealing and acid leaching cycles to synthesize the monoatomic Fe-doped N porous carbon black catalyst Fe-N-C. Choi *et al.*⁴³ prepared

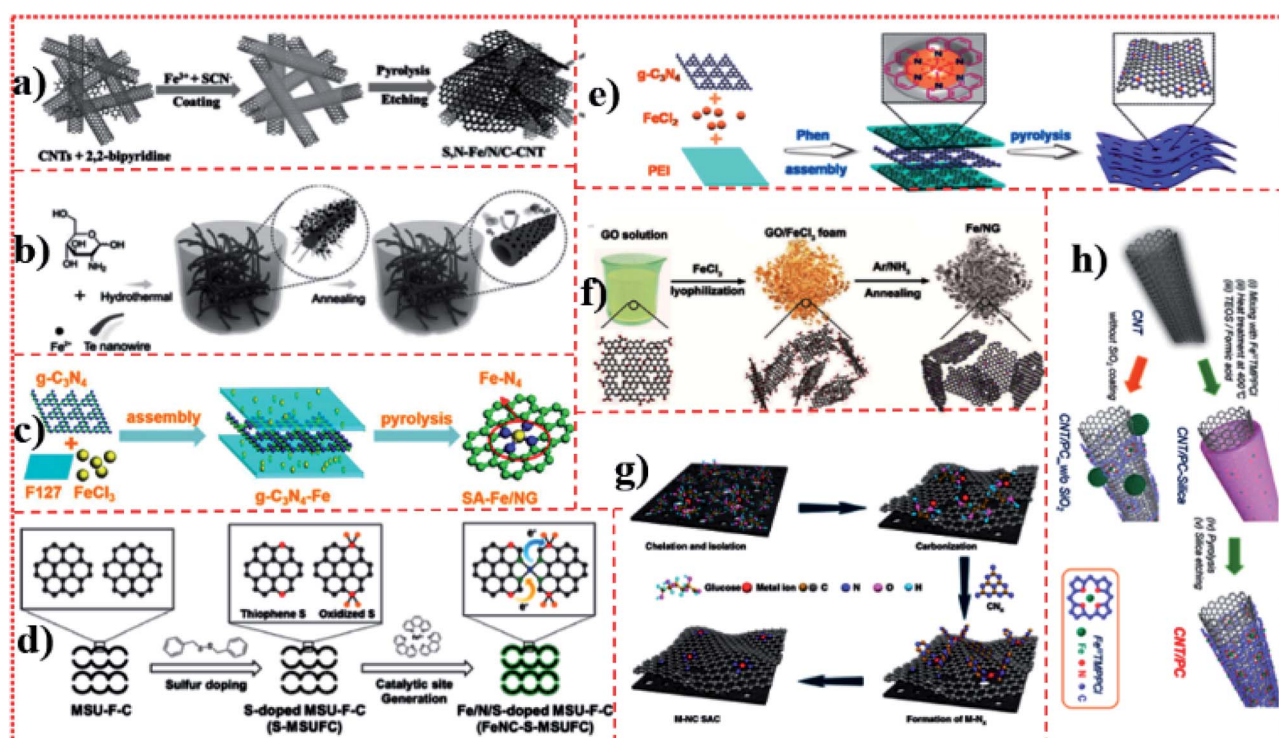


Fig. 8 (a)–(h) Schematic of Fe-SACs for the synthesis of the carbon matrix and metal complex hybrid.



monoatomic catalyst Fe–N–C by pyrolysis and acid etching using ferric acetate and Phen as precursors and ZIF-8 as a carrier. Jiang *et al.*⁴⁴ coated CNTs with glucose in the presence of Fe salt precursors, and then prepared monoatomic catalyst Fe@C–FeNC by pyrolysis in the presence of melamine.

3.3. Strategy for *in situ* preparation of small molecule precursors

The preparation process of Fe-SACs using an *in situ* strategy is relatively simple, can control the dispersion of Fe atoms, and easily used on a large scale. However, the small molecule precursors usually have a relatively low thermal decomposition temperature, which makes the carbonization of precursors difficult. Therefore, appropriate selection of small molecule precursors is very important. Thus far, most of the precursors are nitrogen-rich molecules. Moreover, the catalyst prepared by this method is also difficult to have a consistent geometric morphology, and the selectivity of the catalysts may also be poor. For example, Zhou *et al.*⁴⁵ easily synthesized novel low-cost ferrocene-based porous organic polymers (POPs) by the Schiff base reaction between melamine and ferrocene aldehyde without any catalyst. Through the direct carbonization of the synthesized ferrocene-based porous organic polymer, the transformation from amorphous ferrocene-based POP to the crystalline Fe₃C/Fe carbon composite was further realized to prepare monoatomic catalyst N-FC-800 (Fig. 9). Gu *et al.*³⁶ mixed glucose, dicyandiamide, and ferrous chloride tetrahydrate in an aqueous solution and then carried out freeze-drying and pyrolysis to obtain monoatomic catalyst Fe–N–C. Serov *et al.*²³ prepared

monoatomic catalyst Fe–CBDZ by pyrolysis and acid etching using ferric nitrate and carbendazim as precursors and SiO₂ powder as a template. Owing to the elimination of artificial carbon in the material design, the unique process method, and the reasonable selection of precursors based on high carbon content, high N/C ratio and low volatile content, the catalyst showed a higher active site density and a higher mass activity.

4. Electrochemical applications of iron-based single-atom catalysts

The development of efficient, durable, and economical non-precious metal monoatomic electrocatalysts is of great significance to the development and commercial application of electrochemical energy conversion technology; however, this is still a huge challenge. In recent years, Fe-SACs used in various reactions have been developed, which have excellent activity, selectivity, and stability. In the following chapters, the electrochemical applications of Fe-based monoatomic catalysts in key energy conversion reactions such as ORRs and CO₂RRs are introduced and summarized, in order to demonstrate the great potential of Fe-based monoatomic catalysts in achieving efficient and selective electrochemical processes.

4.1. Oxygen reduction reaction

Environmentally friendly energy storage process/device/technology that converts chemical energy into electricity through devices such as fuel cells and metal–air cells is essential to reduce pollution and the greenhouse effect because the

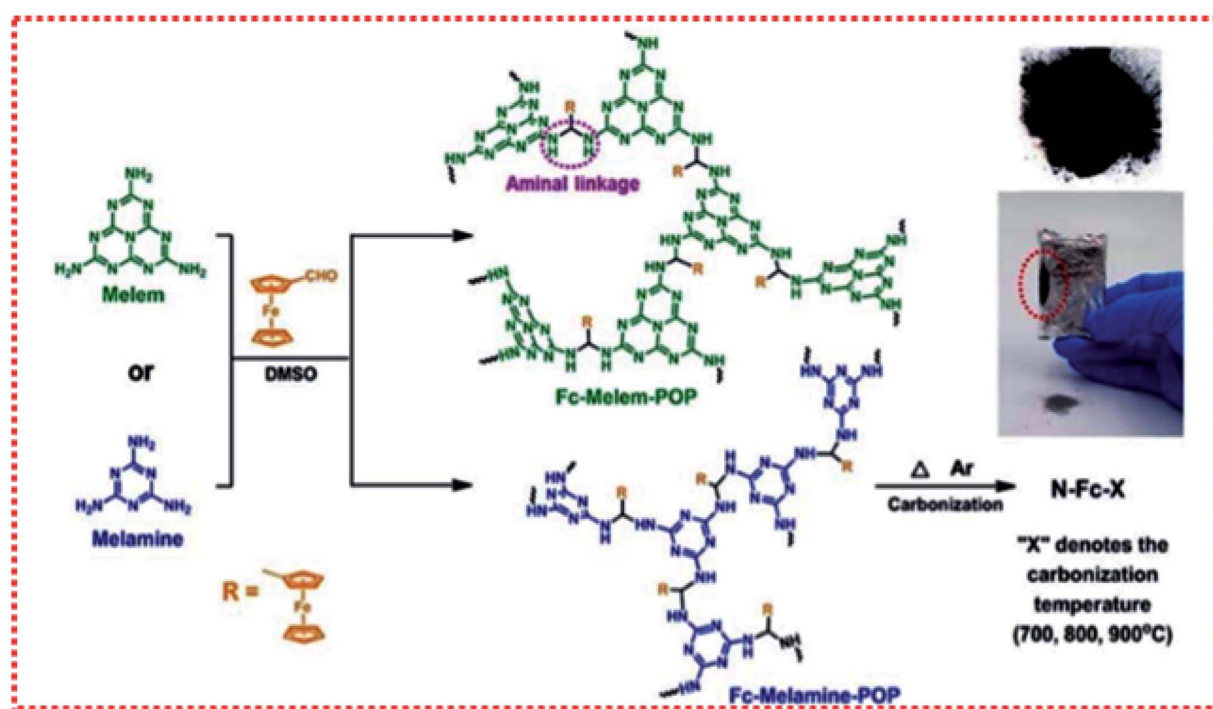


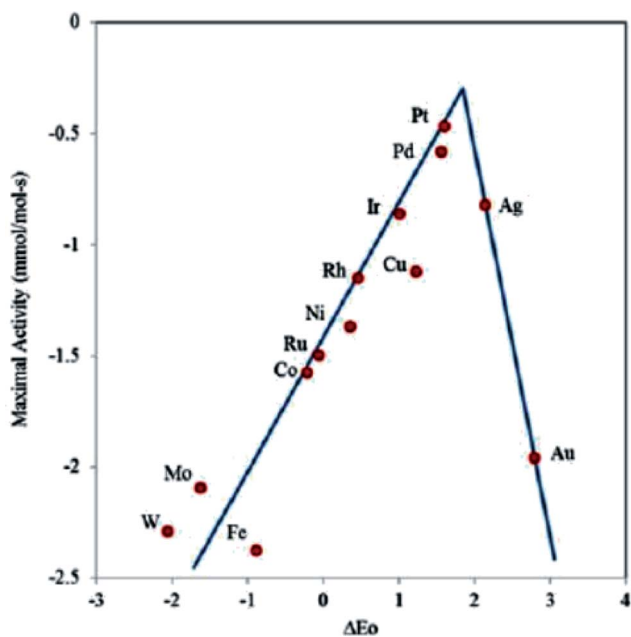
Fig. 9 Synthetic route for the preparation of ferrocene-based POPs and nitrogen-doped carbon catalysts.



Table 3 Electrode reaction of oxygen reduction reactions in different electrolytes

Reaction path	Electrolyte solution	Reaction equation
4e	H ⁺	O ₂ + 4H ⁺ + 4e ⁻ = 2H ₂ O
	OH ⁻	O ₂ + 2H ₂ O + 4e ⁻ = 4OH ⁻
2e	H ⁺	O ₂ + 2H ⁺ + 2e ⁻ = H ₂ O ₂
	OH ⁻	O ₂ + H ₂ O + 2e ⁻ = HO ₂ ⁻ + OH ⁻

world needs to shift from carbon and fossil fuel (coal, oil, and natural gas)-driven economy to more sustainable and green options.^{46,47} However, one of the main bottlenecks in the commercialization of these devices is the requirement of ORRs in their operation, because of their high overpotential due to the slow cathodic kinetics.⁴⁸ Fe-based monatomic catalysts are considered to be one of the most important (ORR) catalysts for oxygen reduction. They are potential substitutes for Pt-based catalysts; therefore, they have a bright future in the development of non-noble metal-based catalysts. At present, according to the different products, the path of the ORR can be divided into the following two types: one is the four-electron (4e) reaction mechanism of complete reduction, under acidic (or alkaline) conditions, in which oxygen is reduced to water (or OH⁻); and the other is a partial reduction of two-electron (2e) reaction mechanism. Under acidic (or alkaline) conditions, oxygen is reduced to hydrogen peroxide (or HO₂⁻). ORRs of two paths in different electrolytes are shown in Table 3.⁴⁹ In the fuel cell process, the 4e path is preferred because it provides high current efficiency, while the 2e reduction pathway is used in the industrial production of H₂O₂. Therefore, 4e complete

**Fig. 10** Volcano plot showing the relationship between the oxygen binding energy and the maximal activity calculated using the Sabatier analysis.

reduction of ORR catalyst is required when selecting the ORR catalyst.⁵⁰

Fig. 10 shows the construction of a “volcano map” based on theoretical calculation and experimental data.⁵¹ Although Fe is distributed at the bottom of the volcanic map, the activity of ORR can be improved by regulating the metal-carrier interaction and promoting the adsorption of key intermediate systems to reduce the Gibbs free energy of ORRs. Some Fe-based monatomic catalysts reported in recent years have excellent ORR catalytic activity, even exceeding that of the commercial Pt/C catalysts at the top of the “volcano map”.

The atomically dispersed Fe-N_x-C catalysts prepared by Han *et al.*¹⁸ showed ultra-high ORR activity, stability, and methanol resistance, and exhibited better performance than most Pt-free catalysts and industrial Pt/C catalysts in an alkaline electrolyte. The half-wave potential of ORRs of the catalyst was 0.91 V, which is higher than that of commercial Pt/C (0.82 V). The primary zinc-air battery with the Pt/C cathode catalyst showed excellent electrochemical performance with open-circuit voltage (OCV) as high as 1.51 V and power density as high as 96.4 mW cm⁻². The rechargeable zinc-air battery with the Fe-N_x-C catalyst and an alkaline electrolyte showed excellent cycle performance within 300 h, and the initial round-trip efficiency was 59.6%, as shown in Fig. 11a-d. Moreover, the rechargeable all-solid-state ZABS with Fe-N_x-C catalyst has a high OCV of 1.49 V, a long cycle life of 120 h, and foldability as shown in Fig. 12a-d. Zhu *et al.*³¹ prepared electrode using the Fe/N-GPC catalyst, which exhibited high catalytic activity with an initial potential of 0.85 V and a half-wave potential of 0.63 V. The electron transfer number of Fe/N-GPC was calculated to be 3.62–3.73 at 0.4–0.2 V, suggesting that the Fe/N-GPC electrode also mainly favored an efficient four-electron transfer process in acidic media, showing great application potential. The catalyst FeSAs/N-C electrode prepared by Yang *et al.*²¹ showed high ORR catalytic activity. Under alkaline conditions, the initial potential was 1.02 V and the half-wave potential was 0.91 V (Fig. 13a), while under acidic conditions, the initial potential was 0.95 V and the half-wave potential was 0.798 V (Fig. 13b). The electron transfer number of the FeSAs/N-C electrode was found to be 3.98 (Fig. 13c), indicating that the mechanism reaction of the FeSAs/N-C electrode is mainly 4e transfer process in an acidic or alkaline medium. The FeSAs/N-C catalyst is used as the cathode of proton exchange membrane fuel cell (PEMFC). At 0.1 and 0.2 MPa back pressure, the maximum power densities of FeSAs/N-C-based H₂/O₂ PEMFC were found to be 0.68 and 0.75 W cm⁻², respectively (Fig. 13d). When using this FeSAs/N-C catalyst for H₂/air PEMFC, this single PEMFC exhibited a peak power density of 0.35 W cm⁻², and the maximum power density of the Zn-air battery using the FeSAs/N-C catalyst was as high as 225 mW cm⁻² (Fig. 13e and f), indicating that FeSAs/N-C is an excellent Pt-free catalyst.

Zhou *et al.*⁴⁵ prepared the catalyst (N-FC-800), which showed high initial potential and half-wave potential of 0.96 and 0.82 V, respectively, exhibiting good activity. Based on this, a rechargeable zinc-air battery was assembled using N-FC-800 as the positive catalyst. Compared to commercial Pt/C, the N-FC-800 battery has a higher power density of 178 MW ± cm² and



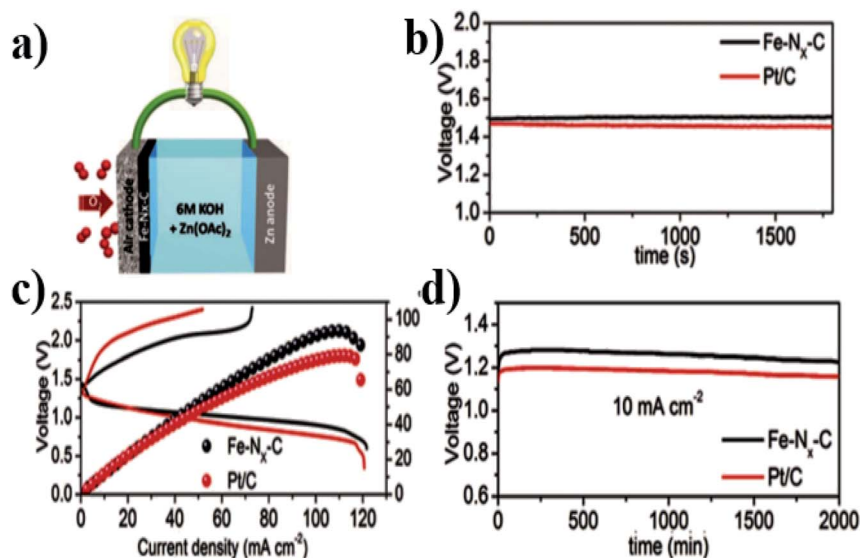


Fig. 11 (a) Schematic showing the structure of ZAB. (b) OCV plots of the liquid ZABs. (c) Discharging and charging polarization curves and the corresponding power density plots. (d) Long-term discharging performance of primary ZABs.

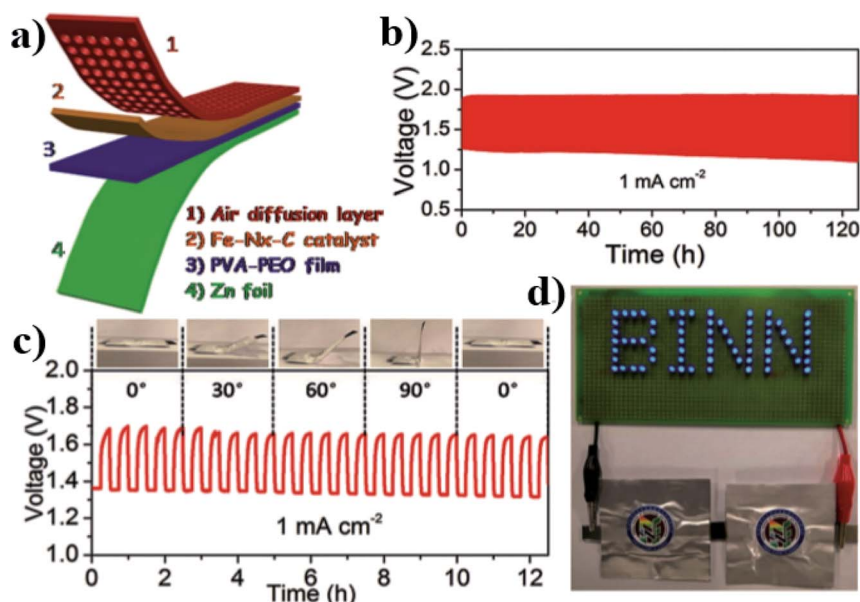


Fig. 12 (a) Schematic of all-solid-state ZAB. (b) Cycling performance of the all-solid-state ZAB tested at a current density of 1 mA cm^{-2} . (c) Foldability test of all-solid-state ZAB bended in different angles from 0° to 90° at a current density of 1 mA cm^{-2} . (d) A lighted LED array powered by two all-solid-state ZABs in series.

a smaller charge–discharge voltage gap of 0.94 V (Fig. 14a), good stability, and less activity attenuation (1.0%) in long charge–discharge cycles (Fig. 14b), and it successfully lit the LED lamp (Fig. 14c and d).

4.2. Oxygen evolution reactions

The OER is the reverse reaction process of ORRs, that is, the oxidation of H_2O to O_2 is the reaction of the air electrode in the metal–air battery during the charging process. In the past few decades, electrocatalytic OERs have received extensive attention

globally, and a large number of catalysts have been developed to improve the kinetics and stability of OER electrodes in different electrolytic environments. Among them, rutile RuO_2 and IrO_2 show good OER performance, and they are used as reference catalysts for research on OER performance.^{52,53}

Nonetheless, they are prone to further oxidation at high potentials, resulting in their instability at high potentials. More importantly, they are all precious metal catalysts, and their high costs are not suitable for large-scale production applications. Owing to the rapid development of monatomic catalysts in



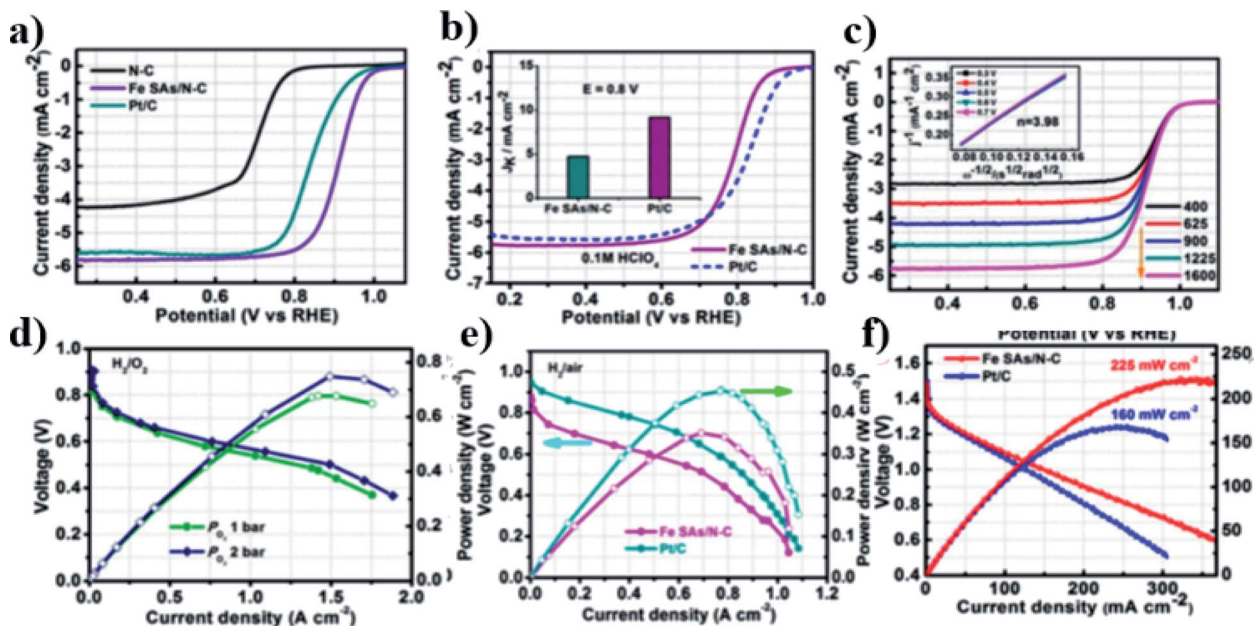


Fig. 13 (a) LSV curves of N-C, Fe SAs/N-C and Pt/C catalysts in O_2 saturated 0.1 M KOH. (b) LSV curves of Fe SAs/N-C and Pt/C catalysts in 0.1 M HClO_4 . (c) LSV curves of Fe SAs/N-C at different rotation rates. Inset: $K-L$ plots. (d) H_2/O_2 PEMFC performance of Fe SAs/N-C-based MEA. (e) H_2/air PEMFC performances using Fe SAs/N-C and Pt/C as cathode catalysts. (f) Discharge curves and the corresponding power density plots with Fe SAs/N-C and Pt/C as cathode catalysts.

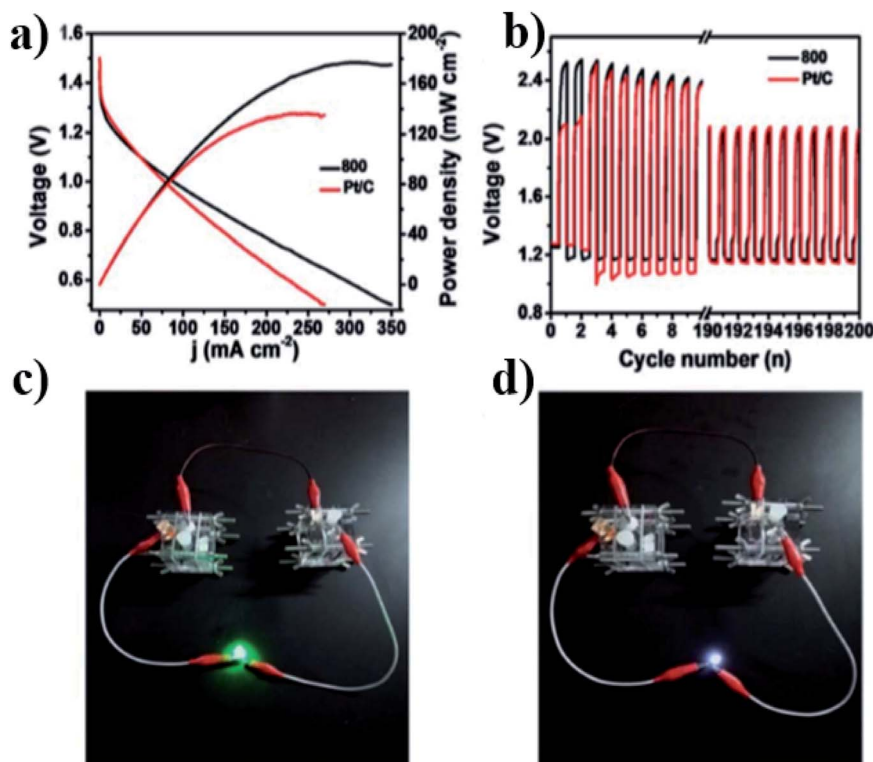


Fig. 14 (a) Discharge polarization curves and the corresponding power density curves of primary zinc-air batteries using the N-FC-800 as air catalysts (mass loading of 1 mg cm^{-2}); (b) cycling performance of rechargeable zinc-air batteries at a current density of 10 mA cm^{-2} ; (c and d) photographic images of a two-electrode rechargeable zinc-air battery lighting up a LED light (blue for (c) and white for (d)).



recent years, it has been found that Fe-based monatomic catalysts also have good OER activity. For example, Junxing Han¹⁸ prepared the Fe-N_x-C catalyst and compared it with the most advanced OER catalyst RuO₂. The overpotential of the Fe-N_x-C catalyst was found to be 600 mV when the current density was 10 mA cm⁻² (marked as E_{j10}), which is close to the overpotential of RuO₂ (530 mV). Potential difference ΔE (ΔE = E_{j10} - E_{1/2}) is an important parameter to evaluate the redox catalytic performance of electrocatalysts. The ΔE value of the Fe-N_x-C catalyst is about 0.92 V, which is better than that of RuO₂ for OERs (E_{j10}) (ΔE = 0.94 V). Guoqiang Shen⁵⁴ report a facile adsorption-oxidation strategy to anchor Fe(III) atomically on ultrathin TiO₂ nanobelt to synergistically lower the spin state (e_g filling ~1.08) to enhance the adsorption with oxygen-containing intermediates and improve the electro-conductibility for lower ohmic loss. The electronic structure of the catalyst is predicted by DFT calculations and perfectly confirmed by experimental results. The catalyst exhibits superior performance for OERs with an overpotential 270 mV @ 10 mA cm⁻² and 376 mV @ 100 mA cm⁻² in an alkaline medium, which is much better than that of IrO₂/C and RuO₂/C.

4.3. Carbon dioxide reduction reactions

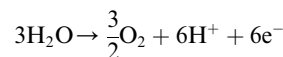
The electrochemical reduction of CO₂ to CO is a 2e/proton reaction, which includes two basic steps.⁵⁵⁻⁵⁷ CO₂ is first adsorbed on the surface of the catalyst, and one electron is transferred to the adsorbed CO₂ to generate surface-adsorbed CO₂⁻; the subsequent combination of CO₂⁻ and a proton occurs to form *COOH, where * represents the adsorbed substance on the surface. Then, *COOH reacts with protons to remove H₂O to form *CO intermediates. Finally, the free gaseous CO was formed by peeling off the surface of the catalyst. Based on this reaction path, an ideal catalyst needs to have a suitable adsorption energy for the main intermediates, which is beneficial to promote the activation of CO₂ to form *COOH and the desorption step of *CO. The electrochemical reduction of CO₂ to CO provides a promising pathway to reduce CO₂ emissions and increase the value of chemical fuel to alleviate the energy crisis. Therefore, development of efficient and selective CO₂RR electrocatalysts is of great significance. Fe-based monatomic catalysts exhibit the highest atomic efficiency and low coordination metal sites and show excellent activity in various reactions. Compared with the nano-cluster or nano-particle catalyst, the monatomic catalyst has a relatively uniform active center and geometric configuration, which gives the reaction substrate a similar environment, which is very beneficial to improve the catalytic selectivity. Therefore, Fe monatomic catalysts show great hope in achieving high efficiency and selectivity in the CO₂RR process. Gu *et al.*³⁴ prepared a catalyst Fe³⁺-N-C consisting of dispersed monatomic Fe sites, which could produce CO at an overpotential as low as 80 mV. At an overpotential of 340 mV, the local current density reached 94 mA cm⁻³. The active sites of the catalyst were discrete Fe³⁺ ions, which coordinated with pyrrole nitrogen (N) atoms on N-doped carbon carriers and maintained +3 oxidation states in the process of electrocatalysis, which was possibly achieved by electronic coupling with conductive carbon carriers. Electrochemical data show that compared to the

traditional Fe²⁺ site, the Fe³⁺ site undergoes faster CO₂ adsorption and weaker CO absorption, thus obtaining better activity. Huan *et al.*⁵⁸ prepared Fe_{0.5}d material as a catalyst with the highest activity and the best selectivity, which could produce CO with high FY (up to 90%) and low overpotential (190 mV overpotential relative to the equilibrium potential of CO₂/CO in 0.5 M NaHCO₃ aqueous solution) and could be electrolyzed for a long time. Interestingly, the selectivity of these materials for CO₂ reduction depends on the ratio of isolated FeN₄ sites to Fe-based NPs, and the higher the ratio, the better the selectivity. These positions are reminiscent of soluble Fe porphyrins, and they have been proved to be excellent catalysts for the conversion of CO₂ to CO. Zhang *et al.*¹⁶ synthesized dispersed Fe atoms on nitrogen-doped graphene (Fe/NG) as efficient electrocatalysts for the reduction of CO₂ to CO. The reduction overpotential of Fe/NG was low, and the Faraday efficiency was as high as 80%. The evidence of structural analysis and control experiments of the catalyst system exhibited that the isolated Fe-N₄ structure was the main reason for the reduction of CO₂ to CO. Some Fe-N-C catalysts composed of uniformly dispersed Fe-N_x sites showed impressive high activity and remarkable selectivity for CO and hydrocarbons. In the future industrial CO₂ gas diffusion cathode (CCCS), these catalysts can replace carbon-supported Au catalysts for the reaction of CO₂RR to CO/H₂ gas mixtures.^{42,59}

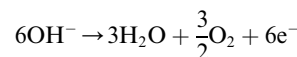
4.4. Nitrogen reduction reactions

The traditional Haber-Bosch nitrogen production process requires high temperatures, high pressures, *etc.*, and the ammonia synthesis process usually requires about 485 kJ mol⁻¹ energy input.⁶⁰ Clearly, this is large energy consumption, and thus, ways to reduce this requirement are also highly desirable. Moreover, subsequent discussion also confirms that this is actually a very challenging goal. Under this background, electrochemical reduction of nitrogen to ammonia is considered as a promising alternative to the energy- and capital-intensive Haber-Bosch process; thus, it has attracted significant attention in the scientific community. The basic equation of the process can be expressed as follows:⁶¹

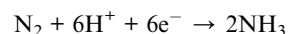
Anode (acid condition)



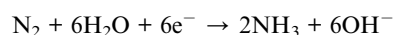
Anode (alkaline condition)



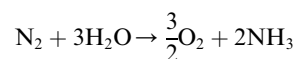
Cathode (acid condition)



Cathode (alkaline condition)



Overall



vacancies, amorphous phases, and structural defects, are used to adjust the electronic structure of the catalyst to obtain better catalytic performance. (2) The main challenge of Fe-SACs is that the loading of Fe active sites is very low, and further addition of Fe inevitably leads to the formation of Fe NPs. It is thus necessary to find or develop porous carriers such as porous 2D materials and 0D materials with abundant accessible surfaces or vacancies that can carry more monatomic active sites. (3) Enhancing the electrical conductivity of Fe-SACs is also an important approach to improve its electrocatalytic activity, for example, it can be achieved by improving the graphitization of carbon-containing materials. (4) It is also essential to use the method of theoretical calculation to study the catalytic performance of the active site of Fe-SACs. Thus far, little work has been done in this area. Therefore, the use of theoretical calculation method to select suitable materials will also be of great significance. (5) For researchers who study Fe-SACs, the development of its application in new fields should be regarded as an important task.

Although several challenges are encountered, there is a reason to be hopeful for Fe monoatomic catalysts that can be used for electrocatalysis, because the progress of *in situ* and non-*in situ* characterization techniques and the development of theoretical simulation can provide support for the study of the catalytic mechanism of Fe monoatomic catalysts. With the continued research on Fe monoatomic catalysts, its application in the field of electrocatalysis will be more mature and become the star of the catalyst research.

Conflicts of interest

The authors declare no conflict of interest.

Acknowledgements

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