Check for updates

Electrochemically active site-rich nanocomposites of two-dimensional materials as anode catalysts for direct oxidation fuel cells: new age beyond graphene

Kashmiri Baruah [ID] and Pritam Deb [ID] *

Direct oxidation fuel cell (DOFC) has been opted as a green alternative to fossil fuels and intermittent energy resources as it is economically viable, possesses good conversion efficiency, as well as exhibits high power density and superfast charging. The anode catalyst is a vital component of DOFC, which improves the oxidation of fuels; however, the development of an efficient anode catalyst is still a challenge. In this regard, 2D materials have attracted attention as DOFC anode catalysts due to their fascinating electrochemical properties such as excellent mechanical properties, large surface area, superior electron transfer, presence of active sites, and tunable electronic states. This timely review encapsulates in detail different types of fuel cells, their mechanisms, and contemporary challenges; focuses on the anode catalyst/support based on new generation 2D materials, namely, 2D transition metal carbide/nitride or carbonitride (MXene), graphitic carbon nitride, transition metal dichalcogenides, and transition metal oxides; as well as their properties and role in DOFC along with the mechanisms involved.

1. Introduction

The exponential increase in energy consumption in different sectors of human civilization has caused the overconsumption of fossil fuels, which is the prime reason for the rise in the CO_2 level in the atmosphere. To circumvent the diminishing sources of fossil fuel and exponential rise in pollution, research is focused on finding an alternative, which is renewable and environmentally benign energy source. As the renewable energy sources solar and wind are intermittent, we need a source that is constant and accessible in any situation. Fuel cells have attracted the attention of researchers as a green alternative. They basically convert the chemical energy residing in a chemical bond to electricity. They deliver high power density and good conversion efficiency. Fuel cells are of different types depending on the electrolyte and the fuels used, which will be discussed in detail in the next section. Despite having distinct advantages, fuel cells suffer from certain drawbacks, for instance, the sluggish redox reactions on the surface of the

Department of Physics, Tezpur University (Central University), Napaam, Tezpur 784028, Assam, India. E-mail: pdeb@tezu.ernet.in

Kashmiri Baruah is currently pursuing her PhD degree under the guidance of Prof. Pritam Deb in the Department of Physics, Tezpur University (Central University). Her research area focuses on the development of 2D material-based electro-catalysts for direct oxidation fuel cells.

Prof. Pritam Deb is the Group Leader of Advanced Functional Materials Laboratory at the Department of Physics, Tezpur University (Central University). He obtained his M.S. degree in Physics from University of Calcutta in 1995 and accomplished his PhD in Nanoscience from Jadavpur University in 2003. He has held many visiting positions in international institutions. His current research interests include energy materials, quantum materials and applications, surfaces and interfaces, and mesoscopic physics.

electrodes, fuel crossover, formation of intermediates, and poisoning of the catalyst surface. Thus, in order to accelerate the redox reactions, the search for an efficient and corrosion-resistant electrocatalyst has gained momentum. In this review, we shall highlight the anode catalyst aspect and its role in electrocatalysis either actively or passively. Two-dimensional (2D) materials have recently garnered interest in electrocatalysis compared to other nanostructured materials due to their intriguing properties. Large surface area, tunable electronic states, and largely exposed active sites render them promising candidates for electrocatalysis. The large specific surface area of these materials endows them with multifarious applications in direct alcohol fuel cells, which require high surface-to-volume ratio. The outstanding electronic properties of these materials arise due to the confinement of the electrons in the 2D region. Furthermore, these materials possess excellent mechanical strength and flexibility owing to their atomic dimension and stronger in-plane covalent bonding, which make them easily fabricable into flexible thin films. The electronic structure is a big differentiator of the catalytic properties as the catalysis follows the Sabatier principle. This principle states that the adsorption energy between the reactants and the catalyst must not be too high or too low.[1–3] This binding energy between the catalyst and the reactants of transition metals depends on the relative position of the d band and the Fermi level.[4,5] Thus, for better catalysis, one can functionalize the surface with different entities and tune the adsorption energies by optimizing the electronic structures. Theoretical simulations such as DFT can study the correlations of the electronic structure, catalyst structure, and composition of the catalyst with their catalytic properties and help in developing highly efficient electrocatalysts.[6] After the exfoliation of monolayer graphene in 2004,[7] different 2D materials have gained enormous research interest in this regard. So far, at least 19 kinds of new 2D materials, including hexagonal boron nitride,[8,9] transition metal dichalcogenides (TMDCs),[10] phosphorene,[11] graphitic carbon nitride,[12] and 2D transition metal carbides/nitrides or carbonitride (MXenes),[13] have been found. These 2D materials are more suitable for forming hybrid nanocomposites than their 3D counterparts and many of them exhibit good electrochemical properties. Some of their properties and application in DOFCs have been reviewed here. To increase the electrochemically active surface area, catalysts are generally supported on materials having high surface area. These supports provide a platform for the uniform distribution of active sites required for redox reactions. The supporting materials play an important role in electrocatalysis by (i) acting as an electron source with good electrical conductivity, (ii) holding the metal NPs *via* physical interaction, (iii) having a large surface area, (iv) providing better stability, (v) providing porosity, and (vi) having higher resistance toward corrosion under different operating conditions.[14,15] The usage of a catalyst support can reduce the amount of noble metal used as the catalyst. Over the decades, a variety of carbonaceous and non-carbonaceous materials have been investigated as the catalyst support.[16] Different carbonaceous supports are available depending on their structure, surface area, electrical conductivity, thermal stability, and different synthetic conditions.[17] Carbonaceous supports include mesoporous carbon, graphene, carbon nanotube (CNT), carbon black, and other forms of carbon in acid and basic media. CNTs, hollow nanospheres, and carbon nanofibres (CNFs) are potential supports for anode catalysts.[18–20] Despite having excellent conductivity, CNTs suffer from a poor porous structure and low surface area in comparison to Vulcan-XC.[21] Multiwalled carbon nanotubes (MWCNTs) are long, twisted, and possess closed ends; similarly, CNFs possess comparatively smaller surface area, large radius, and a high aspect ratio. Thus, it becomes difficult to deposit metal catalysts with high loading (around 40% or more), leading to a reduction in the performance of MWCNTs/CNFs as the catalyst support. Hence, short and functionalized MWCNTs or CNFs can be a good catalyst support in DOFCs.[22] Graphene is a better catalyst support than commercial C owing to its high electroactive behavior and durability.[23] However, the corrosion of carbonaceous supports hinders their performance. To solve the problem of corrosion of carbonaceous supports, non-carbonaceous supports such as titania, tungsten oxide, indium oxide, alumina silica, ceria, zirconia, and conducting polymers have been studied.[24,25] Thus, the unique structure of 2D materials make them efficient supports/substrates for nanostructured materials. Moreover, 2D materials possess controllable surface structures, which aid in tuning the particle size and distribution of the deposited catalysts. New generation 2D materials such as MXenes, graphitic carbon nitride, and TMDCs have been investigated as catalysts/catalyst supports in DOFCs.[26]

Apart from the nanocomposite 2D materials, there are also non-nanocomposite 2D materials that are nowadays being explored as electrocatalysts in fuel cell applications. A novel 2D–3D structure of 2D NiZn oxyphosphide nanosheets (NiZnP NSs) and 3D PdRu nanoflowers (PdRu NFs) was developed,[27] which exhibited enhanced MOR and EOR activity due to the abundant active sites owing to the unique structure of the catalyst. The mass activity corresponding to MOR and EOR is 1739.5 mA mg^{-1} and 4719.8 mA mg^{-1}, respectively, which are higher than that obtained from commercial Pd/C. Another group developed a 1D–2D hybrid heterostructure as the support for the Pt–Sn alloy catalyst.[28] They partially exfoliated CNTS to prepare the 1D–2D structure, which provided the synergistic effect of both 1D and 2D supports, thus facilitating the complete utilization of the catalyst. A power density of 568 mW cm^{-2} (at 60 °C) and 34 mW cm^{-2} (at 80 °C) was achieved for PEMFC and DEFC, respectively. Ultrathin CoNi nanosheets (NSs) deposited over 3D rGO foam[29] was employed for the oxidation of sodium borohydride in alkaline medium. CoNi-NS/rGO foam anode catalyst exhibited a higher peak power density of 91.3 mW cm^{-2} at 95.7 mA cm^{-2} and also exhibited a good fuel utilization capacity. This catalyst proved to be a potential alternative to noble metal catalysts and opens the path toward high fuel utilization metal catalysts by developing novel supports such as 3D rGO foam. Hollow nanodendrites of PdAg were developed by a unique self-template method and employed as an anode catalyst in ethylene glycol oxidation fuel cell.[30] This PdAg catalyst exhibited excellent ethylene glycol oxidation in alkaline medium and a current density of about 4168.8 mA mg$_{Pd}$$^{-1}$ was obtained, which is 3.8

times higher than that of Pd/C. The unique hollow structure facilitates charge transfer and reduces the amount of catalyst loading. Similar works include 1D PdCuTe nanowires (NWs) as ethylene glycol oxidation anode catalyst,[31] Ni–Co/NF,[32] CoB/Nifoam,[33] Ni@Pd,[34] AuCofiber/Cu catalyst,[35] and CuNiPd@Ni foam catalyst[36] employed as $NaBH_4$ oxidation anode catalyst. Despite providing excellent electrochemical activity, transition metal catalysts suffer from low fuel utilization. In this context, we cannot totally reduce the usage of noble metal catalysts. In order to lessen the loading of noble metal catalysts, more interacting support materials creating more exposed active sites are required. For instance, the 2D/2D composite of Bi_2WO_6/MoS_2 when used as a support for Pt NPs, which exhibited 1.5 times higher MOR in the presence of visible light and 2.2 times higher than that of Pt/C.[37] Co_3O_4 nanosheets oxidized ethanol in alkaline medium with an onset potential of 1.32 V *vs.* RHE and a current density of 50 mA cm^{-2} at 1.545 V.[38] Hence, in this review, we will focus on the application of new generation 2D materials and their nanocomposites as anode catalysts/supports in DOFCs.

2. Direct oxidation fuel cells and their types

Fuel cells (FCs) have been recognized as an alternative energy conversion system, particularly for low power consumption electronic devices and domestic transportation systems.[39,40] A FC converts the chemical energy stored in the chemical bond of organic and inorganic fuels into electrical energy.[41,42] It consists of the following components: a primary fuel electrode (anode), an electrode of oxidant (cathode), an electrolyte in between them, and an external circuit connecting the cathode and anode. Moreover, FCs have attained tremendous research interests because of their low pollutant emission, high power density, and superfast recharging.[43,44] FCs are of varying nature depending on the electrolyte used, types of ions transferring through the electrolyte, types of fuels, and the operating temperature range.[45,46] The classification of fuel cells is given in Table 1. At the anode/electrolyte interface, the primary fuel gets oxidized to produce protons (H^+ ions) in an acidic medium, whereas in a basic medium, OH^- ions (travel toward the anode from the cathode side) react with the fuel to oxidize it and the electrons generated move toward the cathode *via* the external circuit through a load. The electron then reduces the oxygen present at the cathode into water. This energy generated across the load is the useful electric energy output of the fuel cell. During the whole process, the heat energy generated at the interface of the electrode/contact, electrode/electrolyte interfaces, resistance caused by the migration of protons or hydroxides through the electrolyte, and electrons migrating through the external circuit is lost into the surroundings as waste.[45] The electrooxidation of these fuels on the electrode/electrolyte interface is very sluggish and the complete oxidation to CO_2 is not possible, which reduces the efficiency of the process. Besides, the low stability, limited availability, high cost, and CO poisoning of the mostly-used Pt catalyst have

discouraged its practical implementation.[47–49] Low cost, highly stable, and CO-resistant electroactive materials are becoming the quest of the day.

Based on the mode of fuel supply to the anode, FCs can also be classified into direct and indirect FCs. Fuels are supplied directly to the anode for electrooxidation in the direct FC, whereas in the latter, the primary fuel is first reformed into hydrogen-containing gas (named as secondary fuel) and then the secondary fuel is fed to the anode for further oxidation to produce electricity.[46,50] In cation exchange FC, oxygen reduction reaction is very slow, necessitating the use of noble metal as the cathode catalyst, which accelerates the electrochemical reactions at the cathode. However, the cost factor of noble metal prevents its large-scale production, which is being addressed and needs further improvement.[51,52] Water, which is produced as a byproduct at the cathode, needs to be timely removed from the fuel cell, failing which causes water flooding at the cathode and hampers the fuel cell performance as the oxygen mass transfer gets affected. On the other hand, in an alkaline or anion transfer FC, the oxygen reduction kinetics is fast and does not require noble metals unlike cation exchange FC. As hydrogen molecules are smaller than oxygen molecules with a large diffusion coefficient, the water produced at the anode does not affect the mass transfer of hydrogen considerably and is consumed at the cathode to produce hydroxide ions, leading to the reduction of cathode water flooding.[46,53] Although electrolytes such as cation exchange membranes, namely, Nafion and PEM, have dominated the fuel cell market, fuel crossover, high-priced membranes and noble metals, low activity, and complicated reactions involved in the oxidation of most of the organic fuels are the factors that have arrested the further development and applications of PEMFCs. Direct oxidation alkaline fuel cells, on the other hand, have gained momentum in the present years because of their potential to outperform the shortcomings of PEMFC. The direction of hydroxide ion flow in the AFC is opposite to that in the PEMFC, reducing the fuel crossover.[54] Moreover, in comparison to the aqueous electrolyte, the application of solid polymer electrolytes, such as anion exchange membranes (AEMs), helps in reducing carbonate formation from CO_2. PEMFCs can very well fit in with carbonaceous fuels due to their high tolerance toward CO_2, whereas AEMFCs can accommodate nitrogen-based fuels, for instance, ammonia and hydrazine, which are not suitable to be used in PEMFCs.[55] Pt-based electrocatalysts suffer from poisoning by the reaction intermediates such as CO in an acidic medium. This problem of poisoning can be solved by operating the fuel cell in an alkaline electrolyte, where the kinetics get improved and Pt-free catalysts can be used.[56,57] The electrooxidation of fuels such as ethanol and methanol in alkaline medium is independent of the structure, which offers scope for the usage of non-precious metals, such as Ni and Pd, and perovskite oxides in alkaline fuel cells.[58–60] Thus, the usage of alkaline electrolytes in fuel cells carries ample merits, for instance, improved efficiency, better reaction environment, reduced poisoning effects, minimal sensitivity to surface structure, and a broader range of affordable non-noble metal electrode materials to choose from.[61] Mixed transition metal oxides, such as Co-based oxides
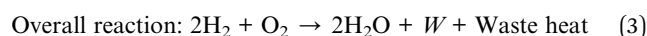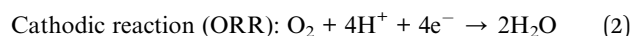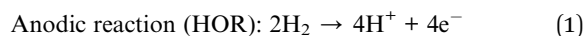
Table 1 Classification of fuel cells

Types of FCs	Description
1. Classification by electrolytes	
Alkaline Fuel Cell (AFC)	Aqueous alkaline solution (generally KOH) as the electrolyte
Proton Exchange Membrane Fuel Cell (PEMFC)/ Solid Polymer Fuel Cell (SPFC)/Solid Polymer electrolyte Fuel Cell (SPEFC)/Polymer Electrolyte Fuel Cell (PEFC)/Polymer Electrolyte Membrane Fuel Cell (PEMFC)	Solid proton conducting membrane as the electrolyte
Phosphoric Acid Fuel Cell (PAFC)	Phosphoric acid as the electrolyte
Molten Carbon Fuel Cell (MCFC)	Molten carbonate salt as the electrolyte
Solid Oxide Fuel Cell (SOFC)	Solid oxide ion conducting ceramic as the electrolyte
2. Classification by type of ions passing through the electrolyte	
Cation transfer fuel cell	Positively charged ions migrate through the electrolyte. Also known as acid electrolyte fuel cell
H^+ ion transfer PAFC H^+ ion transfer PEMFC	
Anion transfer fuel cell	Negatively charged ions passing through the electrolyte. Also known as alkaline type fuel cell
OH^- (AFC) CO_3^{2-} (MCFC) O^{2-} (SOFC)	
3. Classification by operating temperature	
Low temperature	60–80 °C
AFC (60–80 °C) PEMFC (80 °C)	
Intermediate temperature (PAFC)	∼200 °C
High temperature	High temperature range
MCFC (650 °C) SOFC (∼1000 °C)	
4. Classification by type of fuels used	
H_2–O_2 fuel cell	H_2 as the fuel and O_2 as the oxidant
H_2-air fuel cell, ammonia-air fuel cell, hydrazine-air fuel cell, hydrocarbon-air fuel cell, hydrogen–chlorine fuel cell, hydrogen–bromine fuel cell, *etc.*	These fuel cells are named according to the fuel used and air as the oxidant
Direct alcohol fuel cell (DAFC), for instance Direct Methanol Fuel Cell (DMFC), Direct Ethanol Fuel Cell (DEFC), *etc.*	Different alcohols are used as the primary fuel

($MnCo_2O_4$, $CoCo_2O_4$, or $NiCo_2O_4$), are stable in alkaline electrolytes as their surfaces remain covered by OH^- ions.[62,63] In alkaline medium, during alcohol oxidation, these adsorbed OH^- ions cause the dehydrogenation of adsorbed alcohols and assist in the desorption of the poisoning intermediates.[64,65] In this way, alcohol oxidation becomes more efficient in alkaline medium than in acidic medium. As the conductivity of the metal oxides are lesser than the Pt-based catalysts, the alcohol oxidation reaction can be compensated by making composites with other conducting 2D materials having a large surface area.

Hence, keeping the conditions alike, alkaline fuel cells provide better performance than acid/proton conducting fuel cells. The schematic of DAFC in acidic medium is shown in Fig. 1. In search of sustainable energy resources, hydrogen has proved to be a better option in reducing CO_2 emissions.[66,67] Hydrogen fuel cell is envisioned to meet the energy challenges as the only byproduct is water, thus making "hydrogen economy" viable. Although PEMFC has been commercialized in multifarious applications such as portable power, backup power, and domestic transport, the poisoning of platinum group elements as the catalyst and the difficulty in storage and transportation of hydrogen has reduced its feasibility.[68,69] In a H_2–O_2 fuel cell, the electrochemical reactions are explained in eqn (1)–(3).

$$\text{Anodic reaction (HOR): } 2H_2 \rightarrow 4H^+ + 4e^- \quad (1)$$

$$\text{Cathodic reaction (ORR): } O_2 + 4H^+ + 4e^- \rightarrow 2H_2O \quad (2)$$

$$\text{Overall reaction: } 2H_2 + O_2 \rightarrow 2H_2O + W + \text{Waste heat} \quad (3)$$

where W represents the useful electric energy supplied by the fuel cell.

The schematic of DAFC in basic medium is shown in Fig. 2.

Unlike hydrogen, alcohols such as methanol, ethanol, and ethylene glycol have much lower oxidation kinetics; however, they have received attention as they possess higher energy density and easier storage and transportation facility. Among direct alcohol fuel cells, DMFC is the simplest one as the complete oxidation of methanol to CO_2 releases only 6 electrons,[48] whereas the electrooxidation of ethanol liberates 12 electrons.[70] Regardless of the sluggish kinetics, ethanol has been attractive because of its high energy density (8 kW h kg^{-1} *vs.* 6.1 kW h kg^{-1} of methanol), less toxicity, and safety for large scale application as a renewable biofuel.[71,72] The electrochemical reactions taking place in the DMFC acidic medium are shown in eqn (4)–(6), and that of the basic medium in eqn (7)–(9). These redox reactions are very sluggish and tend to produce intermediates such as carbon monoxide, formaldehyde, and formic acid,[71] thereby reducing the conversion efficiency of the
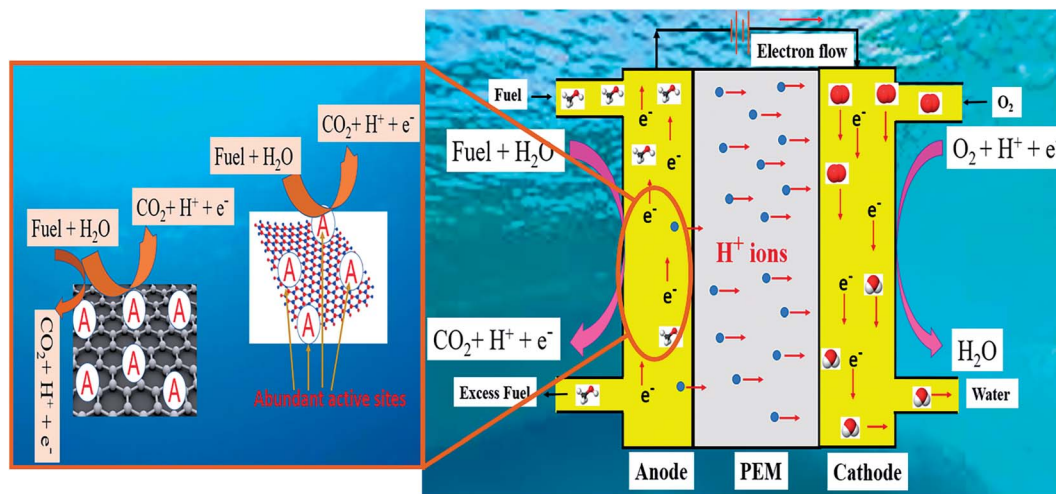
Fig. 1 Schematic of the mechanism of DAFC in acidic medium and electrochemical fuel oxidation on the 2D surface.
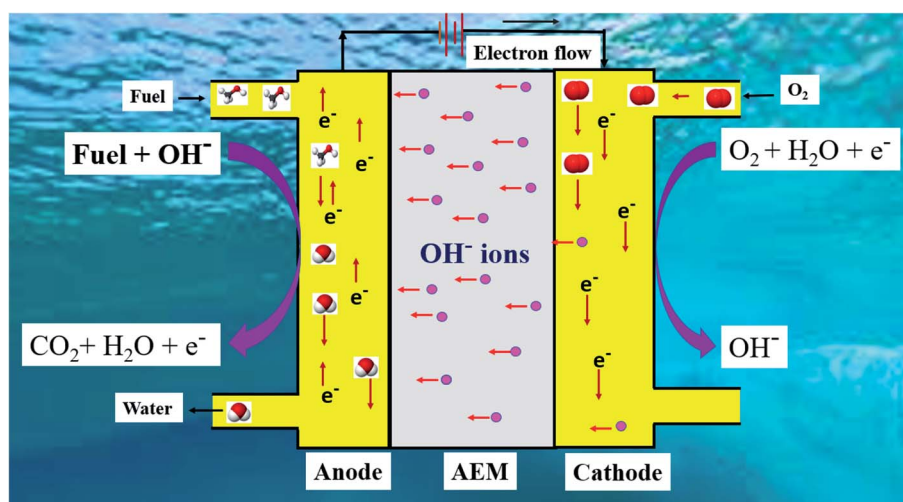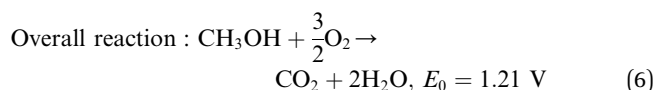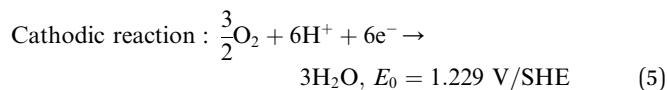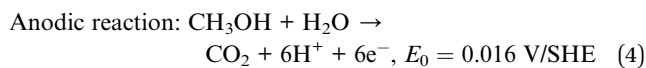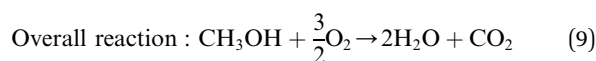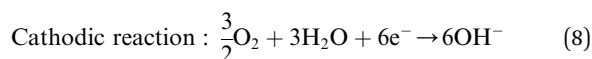

Fig. 2 Schematic of the mechanism of DAFC in basic medium.

fuel cell. Thus, the search for an efficient, non-platinum metal-based affordable catalyst is still ongoing.
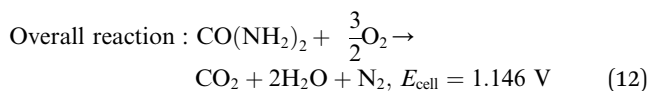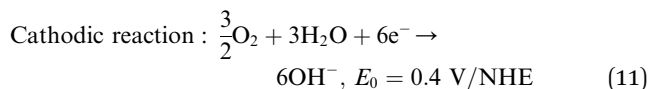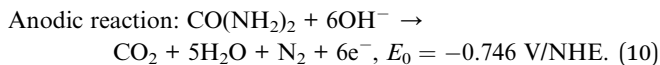
Anodic reaction: $CH_3OH + H_2O \rightarrow$
$$CO_2 + 6H^+ + 6e^-, E_0 = 0.016 \text{ V/SHE} \quad (4)$$

Cathodic reaction : $\frac{3}{2}O_2 + 6H^+ + 6e^- \rightarrow$
$$3H_2O, E_0 = 1.229 \text{ V/SHE} \quad (5)$$

Overall reaction : $CH_3OH + \frac{3}{2}O_2 \rightarrow$
$$CO_2 + 2H_2O, E_0 = 1.21 \text{ V} \quad (6)$$

In basic medium, the redox reactions of DMFC are

Anodic reaction: $CH_3OH + 6OH^- \rightarrow 5H_2O + 6e^- + CO_2$ (7)

Cathodic reaction : $\frac{3}{2}O_2 + 3H_2O + 6e^- \rightarrow 6OH^-$ (8)

Overall reaction : $CH_3OH + \frac{3}{2}O_2 \rightarrow 2H_2O + CO_2$ (9)

Urea is a non-toxic and non-flammable hydrogen-carrying compound (hydrogen content 6.71 wt%) having an energy density of 16.9 MJ L^{-1}, which is about 10 times higher than that of hydrogen.[73,74] Untreated urea-containing wastewater poses threat to the environment as it decomposes into ammonia and other nitrogen-containing pollutants. Traditional methods (such as nitrification and denitrification) used to treat this water are energy consuming.[75] In this regard, direct urea fuel cell (DUFC) outperforms these methods as it simultaneously solves the problem of wastewater treatment and electricity production by oxidizing urea/human/animal urine containing water into CO_2, H_2O, and N_2.[73,76] As urea can be transported and stored with ease unlike hydrogen, treating urine-rich water will be like killing two birds with one stone. The electrochemical redox reactions involved in a urea fuel cell are shown in the following eqn (10)–(12).

Anodic reaction: $CO(NH_2)_2 + 6OH^- \rightarrow$
$$CO_2 + 5H_2O + N_2 + 6e^-, E_0 = -0.746 \text{ V/NHE}. \quad (10)$$

Cathodic reaction : $\frac{3}{2}O_2 + 3H_2O + 6e^- \rightarrow$
$$6OH^-, E_0 = 0.4 \text{ V/NHE} \quad (11)$$

Overall reaction : $CO(NH_2)_2 + \frac{3}{2}O_2 \rightarrow$
$$CO_2 + 2H_2O + N_2, E_{cell} = 1.146 \text{ V} \quad (12)$$

3. Technological aspects of graphene-based anode catalysts

After the discovery of graphene by Novoselov et al.,[7] it has attracted tremendous research interest in fields where 2D materials have garnered demands. Graphene is a single layer of sp^2 hybridized carbon atoms packed in a hexagonal structure with stronger in-plane σ_{c-c} bonding than the out-of-plane π bonding. This mobile network of electrons multiplies its electronic conductivity. The unique aspects of graphene include high mechanical strength of about 1 TPa Young's modulus,[77] high surface area (up to 2675 $m^2 g^{-1}$),[78] high electrical (0.5–100 $S m^{-1}$) and thermal conductivity (3080–5150 $W m^{-1} K^{-1}$), and high electron mobility at room temperature (200 000 $cm^2 V^{-1} s^{-1}$),[79] making it a viable candidate for electrocatalysis and other applications where good thermal and electrical conductivity is the prime requirement. Different configurations of graphene possess different properties depending on the morphology, dimensions, number of layers, and presence of defects. It shows superiority over other dimensional carbon nanostructures owing to its astonishing electrochemical properties.[80] Carbon quantum dots, fullerenes, and carbon nanotubes (CNTs) are a few of the contenders of graphene; however, their scalability prevents them from outshining graphene in electrochemical applications. By rationally designing graphene, it can be used either as an electrocatalyst or a support material to enhance the catalytic process.[81] Tremendous research work (both theoretical and experimental) has been devoted to graphene and/or graphene nanocomposites with noble metal nanoparticles,[82] nanocrystals,[83] metal oxides,[84] etc., as electrocatalysts/supports. As an electrocatalyst support, graphene has shown excellent durability and catalytic activity owing to its large surface area, selectivity, stability, conductivity, and tunable properties.[82] Graphene-supported Pt decorated electrocatalyst performs better than the commercial catalyst Pt/ C without graphene.[85] Similarly, Pd-loaded graphene aerogel exhibits excellent activity compared to commercial Pd/C.[86] Pt and Pd are state-of-the-art electroactive metals used in fuel oxidation; however, easy poisoning by intermediates such as CO has guided researchers to form corrosion-resistant alloys such as Pt–Co, Pt–Fe, Pt–Ni, Pd–Co, Pd–Fe, and Pd–Ni[87] to improve the performance and lifetime of the catalyst. Moreover, Pt- and Pd-loaded graphene-supported electrocatalysts have also been developed for methanol oxidation fuel cells, such as PtCo/rGO, Pd/rGO, PdCo/rGO, and PtPd/rGO.[88–91] Besides, replacing

carbon atoms with atoms such as boron, nitrogen, sulfur, and phosphorus helps to increase the conductivity and electrochemical properties of graphene.[92–95] Iqbal et al.[96] reviewed the prospects and challenges of graphene-based fuel cells. Graphene's low sheet resistance, higher durability, and resistance toward corrosion make it a good candidate for bipolar plates in fuel cells. Moreover, its better stability and reduced crossover also help in attaining better polymer electrolyte membranes in PEMFCs. However, graphene-based electrocatalysts suffer from few technical drawbacks. The high degree of graphitization of carbon makes graphene chemically inert and it also lacks sufficient sites for the deposition of noble metal nanoparticles. Moreover, the catalytic mechanism of graphene-supported nanocrystals and heteroatom-doped graphene are yet not clear and need attention in order to develop highly stable and potential electrocatalysts. Usually, the large surface area of graphene tends to restack due to van der Waals forces, thus reducing the full usage of the electroactive sites. In this context, tuning the morphology such as preparing porous graphene,[97] functionalizing graphene oxide with metal oxide,[84] attaching it with carbon nanotubes,[98] or combining it with other inorganic materials[99] can be beneficial in minimizing the restacking and enhancing the electrochemical activity.

M. Li and coworkers[97] constructed B- and N-doped graphene aerogel-supported Pt catalyst (Pt/BN-GA) in MOR (schematic shown in Fig. 3). This unique macro and mesoporous structure featuring large surface area with uniform boron and nitrogen distribution along with Pt nanoparticles exhibits brilliant electrical conductivity, thus making Pt/BN-GA a better electrocatalyst, surpassing traditional catalysts, namely, Pt/GA, Pt/G, and Pt/C. A carbocatalyst comprising of Pd nanoparticles deposited on carbon–rGO (Pd@C–rGO) exhibited improved oxidation of ethylene glycol.[100] The smaller particle size of Pd nanoparticles and the large surface area of the rGO support contributed to the enhanced electrocatalytic activity of Pd@C– rGO. A bio-compatible electrocatalyst (Pt–Pd decorated rGO) developed from the extract of vermicast was employed for the oxidation of ethylene glycol (EG).[101] A mass activity of 803.4 mA mg^{-1} was obtained, which is 85% retained after 500 cycles, implying improved CO tolerance. The 2D carbon support, interaction between the metal nanoparticles and the support, and the changed electronic structure of Pt after Pd encapsulation contribute to the enhanced EG oxidation, paving the path for affordable and bio-compatible electrocatalysts. The in situ carbon atom was used to increase the interaction between the MoS_2/RGO support with noble metal Pd quantum dots (QDs) and this nanocatalyst was employed as a bifunctional catalyst for alcohol and water oxidation.[102] It delivered higher AOR activity. The support participated in the generation of active oxygen, further oxidizing the intermediates formed during the oxidation reactions. The improved catalytic activity of the nanocatalyst is due to the smaller particle size of Pd QDs and enhanced interaction between Pd QDs and the support $C@MoS_2$–RGO. Several reviews have been devoted to the contribution of graphene as the electrocatalyst, catalyst support,[103–106] and also as the membrane in PEMFC.[107,108] Hence, this timely and extensive review will focus on 2D materials
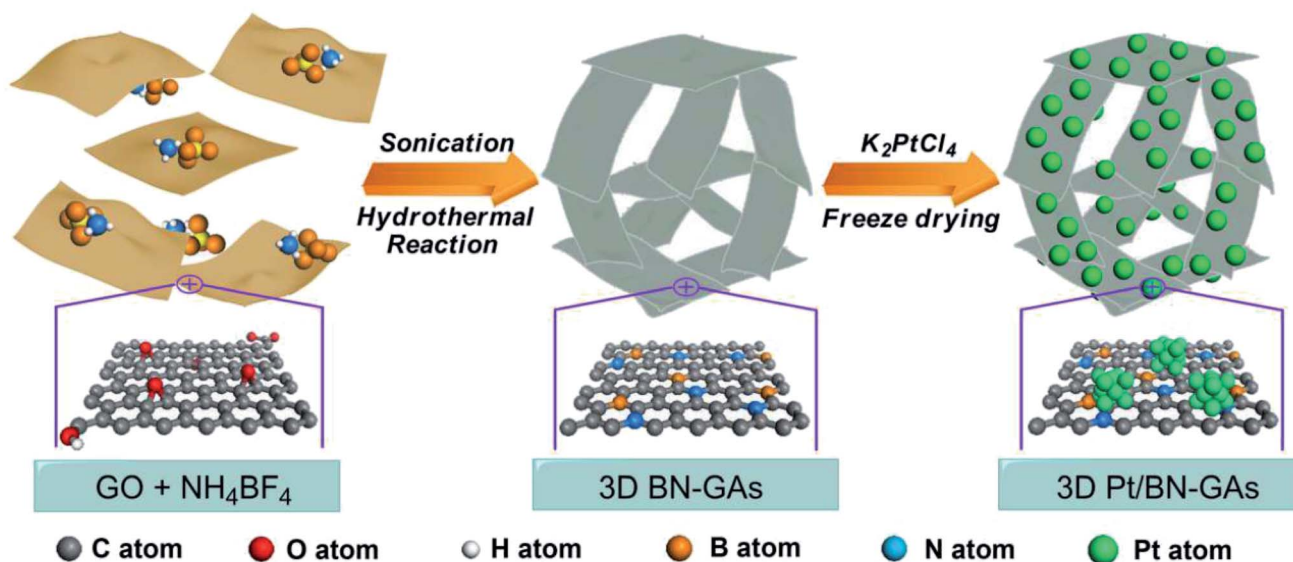
Fig. 3 Schematic of the formation of 3D Pt-doped BN-graphene aerogel. Reproduced with permission.[97] Copyright 2018, ACS.

beyond graphene and discuss their properties and application in DOFCs as anode catalysts or supports.

4. 2D materials beyond graphene

4.1 MXenes

MXenes, a new member, was included in the family of 2D materials after Naguib et al.[109] exfoliated MXenes by selectively etching A layer (Al) from the MAX phase (Ti_3AlC_2 in this case). The suffix 'ene' is used in analogy to graphene.[110] The MAX is a transition metal carbide and nitride usually represented by $M_{n+1}AX_n$, where n varies from 1 to 3, M is a transition metal, A can be any element belonging to groups 13–16 of the periodic table, and X can be either carbon, nitrogen, or their mixture.[111] MAX phases have hexagonal layered structures comprising of $M_{n+1}X_n$ layers held together by A layers, with X atoms occupying the octahedral sites.[112] The M–X bond, being a mixture of metallic/covalent/ionic, is stronger than the M–A bond, which is generally metallic.[113] Unlike the 2D inorganic analogues where the layers are held together by weak van der Waals forces, strong interlayer bonding in MAX renders it difficult to be exfoliated mechanically.[114,115] However, because of the differences in the reactivity of the M–X and M–A bonds, it is possible to exfoliate it by etching the A layer from $M_{n+1}AX_n$ using different etchants (such as HF, LiF + HCl, NH_4HF_2, etc.).[115,116] Despite the high yield of the etchant HF, highly concentrated HF is toxic.[117] To avoid the usage of corrosive HF and promote the industrial applications of MXenes, an alternative exfoliation method that is safe and fast is urgently required. Halim et al.[118] in 2014 reported ammonium bifluoride, NH_4HF_2, as a substitute for hazardous HF. Thereafter, Ghidiu et al.[119] proposed the etching of Al from Ti_3AlC_2 by forming HF in situ through a reaction between HCl and LiF, in which etching and intercalation were accomplished simultaneously. During etching and interaction with the acids, the transition metals on the surface get attached with anions such as OH^-, F^-, and O^{2-} present in the solution, introducing the term T_x into the formula of MXene as $M_{n+1}X_nT_x$, where T_x represents the surface anion terminals. These anions bestow them with a hydrophilic nature. Hence, a weaker hydrogen bond replaces the metallic bond M–A, making it easier for organic intercalants (dimethyl sulfoxide, urea, water) to intercalate between the layers such that a shearing force can delaminate the multilayers into single or few layers.[115,120,121] MAX phases possess a combination of ceramic and metallic properties. They exhibit stiffness, thermal stability, brittleness, strength like ceramics, and good thermal and electronic conductivity like metals.[122] Corresponding to the value of n in MAX, three lattice configurations are possible for MXene, viz., M_2X, M_3X_2, and M_4X_3, as shown in Fig. 4.[123] There are two ways in which more than one metal atom can be present in the M position, viz., the ordered phase and the solid solutions. In the ordered phase, single or bilayer of one metal is sandwiched between another one (e.g., Mo_2TiC_2 and $Ti_2Ta_2C_3$), whereas in a solid solution, the metals are randomly placed in the M position (e.g., $(Ti,V)_2C$ and $(Ti,Nb)_4C_3$).[124] To date, more than 70 MAX phases have been reported, out of which only 20 MXenes have been successfully exfoliated. Generally, MXenes possess a hexagonally close packed (hcp) structure. However, the crystal structure varies with the value of n in MXene as the M atoms in M_2X possess an hcp structure, whereas M_3X_2 and M_4X_3 possess the fcc structure.[125] MXenes possess a plethora of fascinating properties such as high electrical and metallic conductivity of about 6000–8000 S cm^{-1} along with hydrophilicity, large surface area, tunable structure, and good thermal conductivity.[126,127]

These intriguing properties make MXene an interesting candidate for numerous applications such as electrochemical energy storage devices,[128,129] electromagnetic shielding,[130] sensors,[131] FETs,[132] catalysis,[126,133] and biomedical
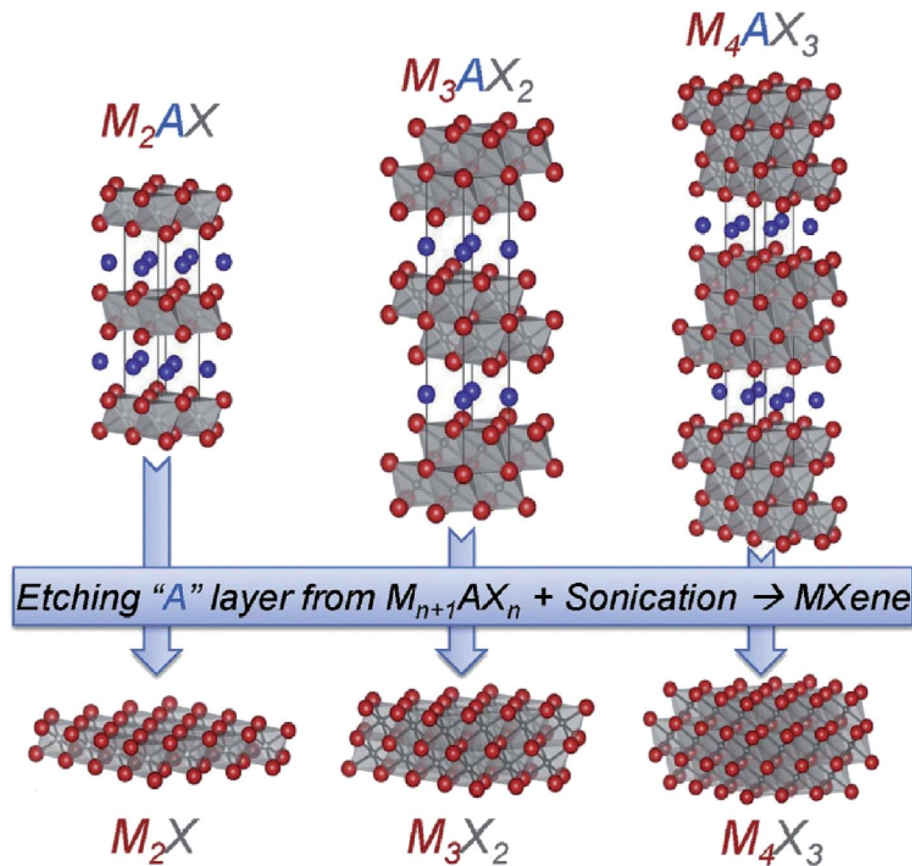
Fig. 4 Structure of different MAX phases depending upon the number of *n*. Reproduced with permission.[123] Copyright 2014, Wiley.

applications.[134] Recently, MXene has gained momentum in the domain of energy conversion and environmental application as a photocatalyst and an electrocatalyst.

4.2 Graphitic carbon nitride (g-C₃N₄)

Graphitic carbon nitride (g-C_3N_4) is similar to graphene with the sp^2 hybridized system having van der Waals interaction between the layers.[135,136] It is one of the most stable allotropes of carbon nitrides, consisting of tri-*s*-triazines connected by tertiary amines.[137] g-C_3N_4 is an environmentally benign material as it is composed of earth-abundant elements carbon and nitrogen, and ideally, a monolayer of g-C_3N_4 could possess a theoretical surface area of about 2500 m^2 g^{-1}.[138] It can be synthesized by the pyrolysis or polycondensation of various nitrogen-containing precursors (explained in Fig. 5) such as cyanamide, dicyandiamide, trithiocyanuric acid, triazine, heptazine, melamine, urea, and thiourea.[139–145] A different degree of condensation and synthetic processes affect the electronic structure, quality, and performance of graphitic carbon nitride.[146–148] The polymeric nature of g-C_3N_4 renders it flexibility in surface engineering by modification at the molecular level and also provides flexibility to the structure, which makes it a good host to other inorganic nanomaterials. g-C_3N_4 possesses high thermal stability up to 600 °C even in air, which is mainly due to the aromatic C–N heterocycles. This thermal stability value is the highest among organic materials and is also higher than high-temperature polymers and aromatic polyamides and polyimides.[149–151]

Besides, g-C_3N_4 is chemically stable in most solvents such as water, alcohols, tetrahydrofuran, *N*,*N*-dimethylformamide, toluene, glacial acetic acid, diethyl ether, and aqueous sodium hydroxide solution owing to the strong van der Waals interactions found between its layers.[152,153] The electronic structure of g-C_3N_4 and its bandgap depend upon the degree of condensation and are tuneable by protonating it or including complex metal cations such as Fe^{3+} and Zn^{2+}.[154,155] Wang and co-workers[156] predicted heptazine-based g-C_3N_4 as the most stable structure using *ab initio* studies. They also predicted the structure formed by thermal polycondensation and salt melt synthesis method (Fig. 6). Three structures were confirmed and their phase stability is in the order phase 1 > phase 2 > phase 3.

Here, phase 1 has a direct bandgap (2.87 eV), whereas phase 2 and 3 have indirect bandgaps (3.14 and 2.27 eV, respectively). g-C_3N_4 has grabbed attention in the fields of catalysis such as photocatalysis and electrocatalysis, *viz.*, HER, OER, and MOR, owing to its 2D structure, low cost, facile preparation methods, and N-rich composition.[157–159] However, the condensation method involved in the synthesis of g-C_3N_4 leads to a number of holes within the structure of g-C_3N_4, which further decreases its conductivity.[160] This decreased conductivity, on the other hand, has an adverse effect on the electrochemical performance of
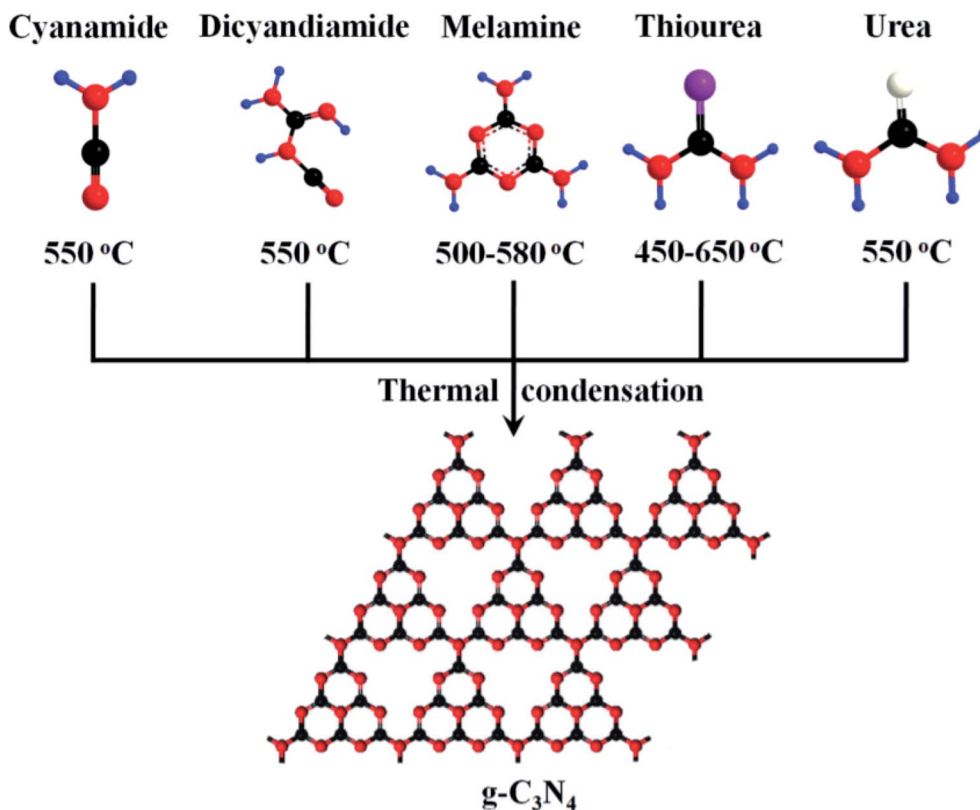
Fig. 5 Schematic diagram of the synthetic method of g-C_3N_4 by the condensation of different precursors–cyanamide, dicyandiamide, melamine, thiourea, and urea; here, different colors represent different atoms: black-C atom; red-N atom; blue-H atom; purple-S atom; white-O atom. Reproduced with permission.[144] Copyright 2015, Wiley.

pristine g-C_3N_4. Thus, developing composites of g-C_3N_4 with conducting materials can improve its performance as an electrocatalyst.[161] Besides, g-C_3N_4 can be used as a metal-support in FCs. In order to be a good catalyst support, it should possess certain properties such as high stability, electronic conductivity, porous structure, presence of functional groups on the surface with which the catalyst particle can be attached, easy synthesis, and low cost.[162] Among different catalyst supports, carbonaceous materials have been studied the most and have shown better performance. However, the most used commercial one, *i.e.*, carbon black, suffers from corrosion and reduction in its electroactivity due to the detachment of the catalyst nanoparticles.[163] Nitrogen, which is considered as an n-type dopant, can solve the corrosion-related problems of carbon-based electrocatalysts by increasing their durability.[164,165] Hence, g-C_3N_4, which contains a high amount of N, can resolve this issue as the lone electron pairs of nitrogen act as Bronsted acid and Lewis base,[162] capable of anchoring the catalyst and provide it with high resistance in acid as well as basic medium.[166] Moreover, surface protonation and doping with B, S, or any metal particles can enhance the conductivity of g-C_3N_4 as well as its catalytic activity.[161,167]

4.3 Transition metal dichalcogenides (TMDC)

Transition metal dichalcogenides (TMDCs) are another class of 2D materials that have gained interest in many fields such as

optoelectronic and electronic devices,[168–170] gas sensing,[171,172] energy storage,[173–175] and energy conversion devices[10,176,177] owing to their intriguing layer-dependent properties. TMDCs consist of transition metal (M) atoms with the formula MX_2, where M can be any transition element belonging to groups IV, V, and VI, and X is a chalcogen (S, Se, Te). The transition metals are hexagonally structured and inserted between two layers of X atom. Similar to graphene, trilayers in TMDCs are held together by interlayer van der Waals interaction, whereas strong covalent bonding exists within the layers. Almost 40 different types of TMDCs have been explored depending on the combination of M and X atoms.[178,179] Depending on the stacking configuration of the atoms, monolayer TMDCs can be found in two different forms, namely, trigonal prismatic phase (2H) and octahedral phase (1T). Thus, the overall crystal structure of TMDCs is hexagonal or rhombohedral with the M atoms in 2H or 1T coordination.[178–181] For instance, MoS_2 exists in two forms 2H and 1T, which can be changed from 2H to 1T by intercalating Li or K or by the transversal displacement of any of the sulfur planes. Depending on the polytype, the electronic properties of TMDCs vary, for instance, 2H MoS_2, WS_2, $MoSe_2$, and WSe_2 are semiconductors, whereas 1T MoS_2 and $NbSe_2$ are metallic.[182–184] The oxidation state of the metal and chalcogen atoms in TMDC is +4 and −2, respectively. Similarly, in multilayered TMDCs, a variety of polymorphs exist depending on the coordination phase each layer possesses. The most
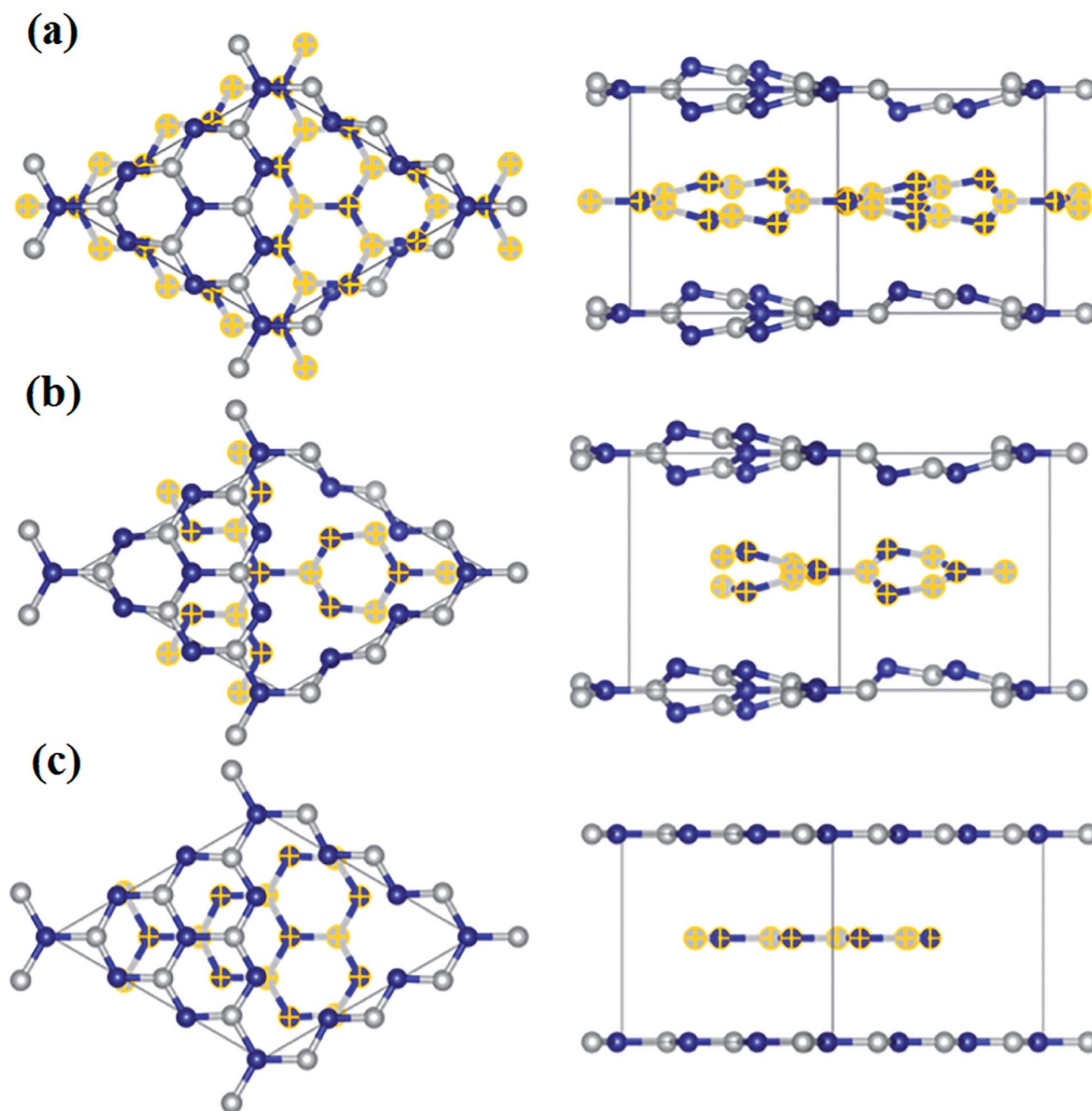
Fig. 6 Predicted structures of heptazine-based g-C_3N_4, (a) phase 1, (b) phase 2, (c) phase 3. Middle layer atoms are represented by yellow crosses. Reproduced with permission.[156] Copyright 2017, ACS.

commonly found polymorphs are 1T, 2H, and 3R (explained in Fig. 7), where 1, 2, and 3 represent the layer number in the unit cell; T, H, and R represent the tetragonal (D_{3d} group), hexagonal (D_{3h} group), and rhombohedral (C^5_{3v} group) symmetry of the crystal, respectively; 1T exhibits the metallic property, whereas 2H and 3R are semiconducting in nature.[185]

Depending upon the filling of the non-bonding d bands of groups 4 to 10 by the M atoms of TMDC, different electronic properties arise. TMDCs exhibit metallic properties when the d bands are partially filled; on the other hand, they display a semiconducting nature when the orbitals are fully occupied.[186,187] Although the impact of chalcogen atoms on the electronic properties of TMDCs is small in comparison to the transition metals, however, the atomic number of chalcogens

affects the band gap in a way that the bandgap decreases when the atomic number of the chalcogens increases. The variance in the size of chalcogen and metal ions determines the length of the M–X bond, which varies in the range of 3.15–4.03 Å.[187] Monolayer and few-layered TMDCs exhibit layer-dependent properties different from their bulk counterparts due to surface properties and quantum confinement. For instance, the Raman peaks of MoS_2, *viz.*, E2g^1 and A$_{1g}$, get blue- and red-shifted when the number of layers decreases due to partial coulombic interaction and probable stacking induced charge due to bonding between the layers.[188–190] The indirect bandgap of bulk MoS_2 (1.3 eV) converts to the direct bandgap (of 1.8 eV) in monolayer MoS_2.[191] The application of TMDCs in electrocatalysis has increased due to the edge-exposed surfaces of
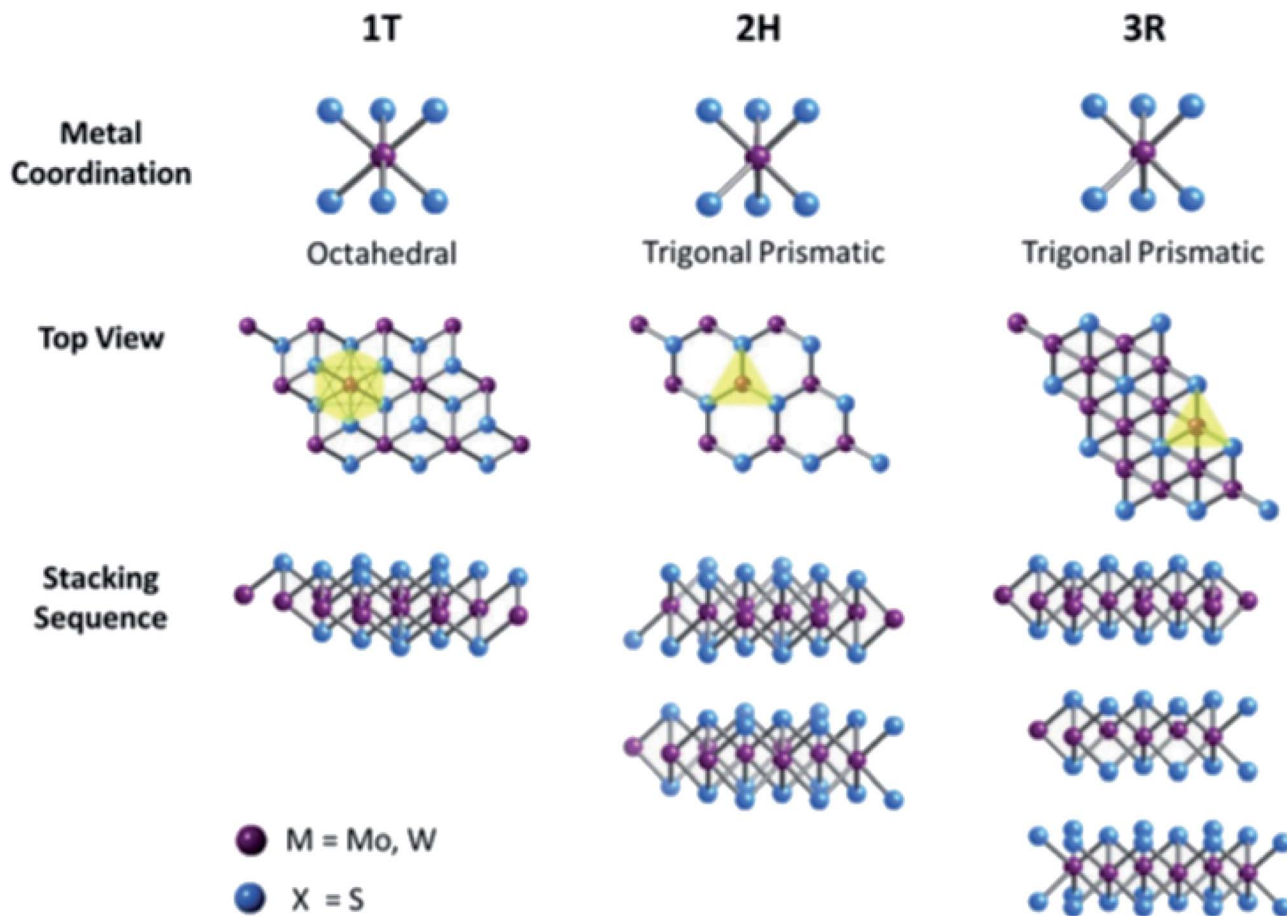
Fig. 7 Metal coordination and stacking sequence. The octahedral coordination gives tetragonal symmetry (1T), whereas distinct stacking sequences of trigonal prismatic layers yield different symmetries: 2H and 3R. Reproduced with permission under the terms of Creative Commons Attribution 3.0 Unported License (CC BY 3.0, facilitated open access).[185] Copyright 2017 RSC.

MoS_2, WS_2, WSe_2, and $MoSe_2$; hence, designing electrocatalysts with exposed edge sites with respect to the basal surfaces can enhance the electrochemical activity. Besides, electrical conductivity is another factor that determines the catalytic activity of TMDCs.[192–194] Different polymorphs of TMDCs possess distinct structure and electronic properties, which can be explored to understand the effect of different polymorphs in enhancing the electrocatalytic activity of TMDCs by rationally designing the catalyst. For instance, Ambrosi et al.[195] reported that 1T TMDCs are better HER electrocatalysts than their bulk counterparts semiconducting 2H because of more exposed edge sites, increased electrical conductivity, and reduced sheet size of the metallic 1T phase. Single or few-layered TMDCs can be obtained by top-down methods such as mechanical cleavage and chemical exfoliation method,[196,197] and bottom-up methods such as chemical vapor deposition and direct wet chemical synthesis methods.[198,199]

4.4 Transition metal oxides

Among various 2D nanomaterials, transition metal oxides (TMOs) have emerged as a feasible alternative to precious noble metals as electrocatalysts in direct oxidation fuel cells[200,201] due to their exceptional physical and electrochemical properties such as low cost, high stability, environment-friendliness, and tunable properties. Among the various metal oxides, NiO and spinel oxides MCo_2O_4 (M = Ni, Cu, Mn, Zn) have been attracting attention.[202] These spinel oxides are potential electrocatalysts owing to their brilliant electrochemical activity and electrical conductivity, which originate from the synergistic effect of their individual metal oxides. In the spinel structure, oxygen possesses fcc packing and the cations occupy both octahedral and tetrahedral sites. The spinel structure can be thought of as the rocksalt structure, where the cations in the octahedral interstices move to the tetrahedral ones to make the spinel. Their thermal and chemical stability, as well as acid–base and redox properties make them suitable for catalytic applications, especially those involving oxygen species.[203] Almost 30 different elements having valency in the range +1 to +6 are known to occupy the cation sites.[204] Alkaline electrolytes are more suitable for TMOs as they are more stable in basic than acidic ones. Different transition metals such titanium (Ti), cobalt (Co), copper (Cu), and manganese (Mn) are included in TMOs. The presence of oxygen ions in the TMOs manifests them the ability to hold on

to the charged ions present on their surfaces without any intermixing. Moreover, one can alter the stoichiometry of 2D TMOs by reducing them, which leads to non-linear and non-uniform charge distribution within the TMOs. It further screens the electric field at the nanoscale range. Thus, TMOs possess unique interfacial properties, which are beneficial for coulombic interactions.[205–207] Besides, when two or more TMOs are placed aside, their electric fields interact and a potential develops at the interface due to Fermi level shifting, which affects the electronic properties of the composites. Semiconductors can be synthesized from 2D TMOs by aligning their d orbitals normal to their planes, which leads to the re-alignment of spins and orbitals.[205] The cations in TMOs can possess different oxidation states and binding configurations, depending on which different electronic properties of the TMOs arise.[208] TMOs are potential candidates for different applications, namely, sensors,[209] energy storage,[210,211] hydrogen production,[212] electronics,[213] and biosystems.[214] There are two types of 2D TMOs: layered and non-layered. The layered TMOs are metal trioxides, e.g., MoO_3, TaO_3, and WO_3, which possess a layered structure and can be exfoliated by top-down methods.[215,216] On the other hand, non-layered TMOs are generally 3D crystals having strong interlayer chemical bonds, which cannot be exfoliated by top-down methods.[217] Metal oxides based non-noble metal catalysts have been a potential candidate in PEFCs because of few characteristics: (i) possess higher corrosion resistance than carbon as the metals in the oxides possess different oxidation states and when present in a high oxidation state, they do not get oxidized easily; (ii) used as cocatalysts or supports as they share strong interactions with the metal catalyst, which prevent their agglomeration. They can also tune the electrocatalytic properties of metals; (iii) they possess several hydroxyl groups on their surfaces, which functions as the cocatalyst of noble metal particles.[218,219]

5. 2D materials beyond graphene: application in DOFC as the anode catalyst/support

5.1 MXenes nanocomposites

MXene has been identified as a potential support material for fuel cell electrocatalysts and other renewable energy applications. The hybridization of metal nanoparticles with MXene makes a competitive electrocatalyst for DEFC.[220] Porous trimetallic nanospheres of PtRhFe loaded over ultrathin (1–2 layers, as confirmed by AFM) $Ti_3C_2T_x$ nanosheets, named as PtRhFe-PNS@MXene, is an excellent MOR electrocatalyst. The optimized stoichiometry of Pt : Rh : Fe was found to be 69 : 8 : 23, as mesoporous $Pt_{69}Rh_8Fe_{23}$-PNS@MXene exhibited the highest current density (3407.7 mA mg^{-1}), which was 4.23-fold that of commercial Pt/C. Intrinsic MXene could not show much ethanol oxidation reaction (EOR) activity, which increased manifold when used as a support material for metal nanospheres Pt, Rh, and Fe. Besides, the addition of Rh and Fe also had a synergistic contribution with Pt. The difference in the Raman shift between $Pt_{69}Rh_8Fe_{23}$-PNS@MXene and the

pure MXene samples clearly indicated the presence of a strong interaction between the metal alloys and $Ti_3C_2T_x$. Moreover, the XPS results confirm the electronic interactions between them. The mesoporous nature of the electrode $Pt_{69}Rh_8Fe_{23}$-PNS@MXene provides channels for seamless electrolyte ion flow, which enhances the EOR activity. $Pt_{69}Rh_8Fe_{23}$-PNS@MXene had a faradaic efficiency of 19.9% for ethanol, much smaller than that of Pt/C TKK (49.5%), $Pt_{69}Rh_8Fe_{23}$-PNS (38.6%), $Pt_{69}Rh_8Fe_{23}$-PNS@C (35.9%), and $Pt_{75}Fe_{25}$-PNS@MXene (41.8%), implying better capability of splitting the carbon–carbon bond. The lowest onset potential and better cycling stability of the electrode further confirm that $Pt_{69}Rh_8$-Fe_{23}-PNS@MXene is the best catalyst. Moreover, due to the coexistence of Rh and MXene, the $Pt_{69}Rh_8Fe_{23}$-PNS@MXene catalyst generated the highest current density, further confirming that they can promote the C1 pathway for EOR. The excellent stability and resistance to CO poisoning of the catalyst are due to the combined effect of the shifting of the Pt d-band center toward the Fermi level and the MXene surface containing hydrophilic terminations such as –O, –OH, and –F, which strongly connects with ternary alloys and decreases the bond of adsorbed CO with Pt. Thus, MXene has proved to be a great support for catalysts because of its hydrophilicity, rich functional groups attached to its surface, and chemical stability. MXene-supported Pd catalyst exhibits an MOR current density of 12.4 mA cm^{-2}, which is higher than that of Pd/C (7.6 mA cm^{-2}) (Fig. 8a and b).[221] Although pristine $Ti_3C_2T_x$ MXene does not show MOR activity (Fig. 8f), this increase in the MOR activity is due to the interaction between MXene and Pd, which is further established by the Tafel slope and turnover frequencies (TOFs) of the catalysts. The smaller Tafel slope (Fig. 8c) and higher TOF (Fig. 8d) of Pd/MXene than those of Pd/C suggest that MXene as a support increases the MOR kinetics of Pd. The durability of Pd/MXene remains intact even after 200 CV cycles (Fig. 8e). Second derivative analysis of the adsorption spectra (Fig. 8g) also adds to the point that Pd/MXene possesses more active Pd sites for methanol adsorption, originating mainly due to the surface-induced strong metal-support interaction effects. MXene as the catalyst support leads to more methanol adsorption as compared to carbon black because more Lewis basic sites are available on the surface of MXene, which is confirmed by the large and broad CO_2 temperature-programmed desorption (CO_2-TPD) peaks of Pd/MXene than that of Pd/C in the range of 450–900 °C (Fig. 8h).

Thus, more methanol molecules get adsorbed on these basic sites, leading to higher MOR activity. DFT calculations further confirm the metal-support interactions using electron density difference map (EDDM). The EDDM results imply that electrons migrate from the top surface of the MXene to the bottom atomic layers of the Pd nanoparticles. The –OH and –F terminations present on the surface of MXene behave as electron donors. In this way, MXene activates Pd active sites and enhances the MOR activity. Besides, Pd/MXene exhibits the most favorable methanol adsorption energy of −0.58 eV, which is higher than that of pristine MXene and Pd. Thus, the introduction of the MXene support provides more scope of
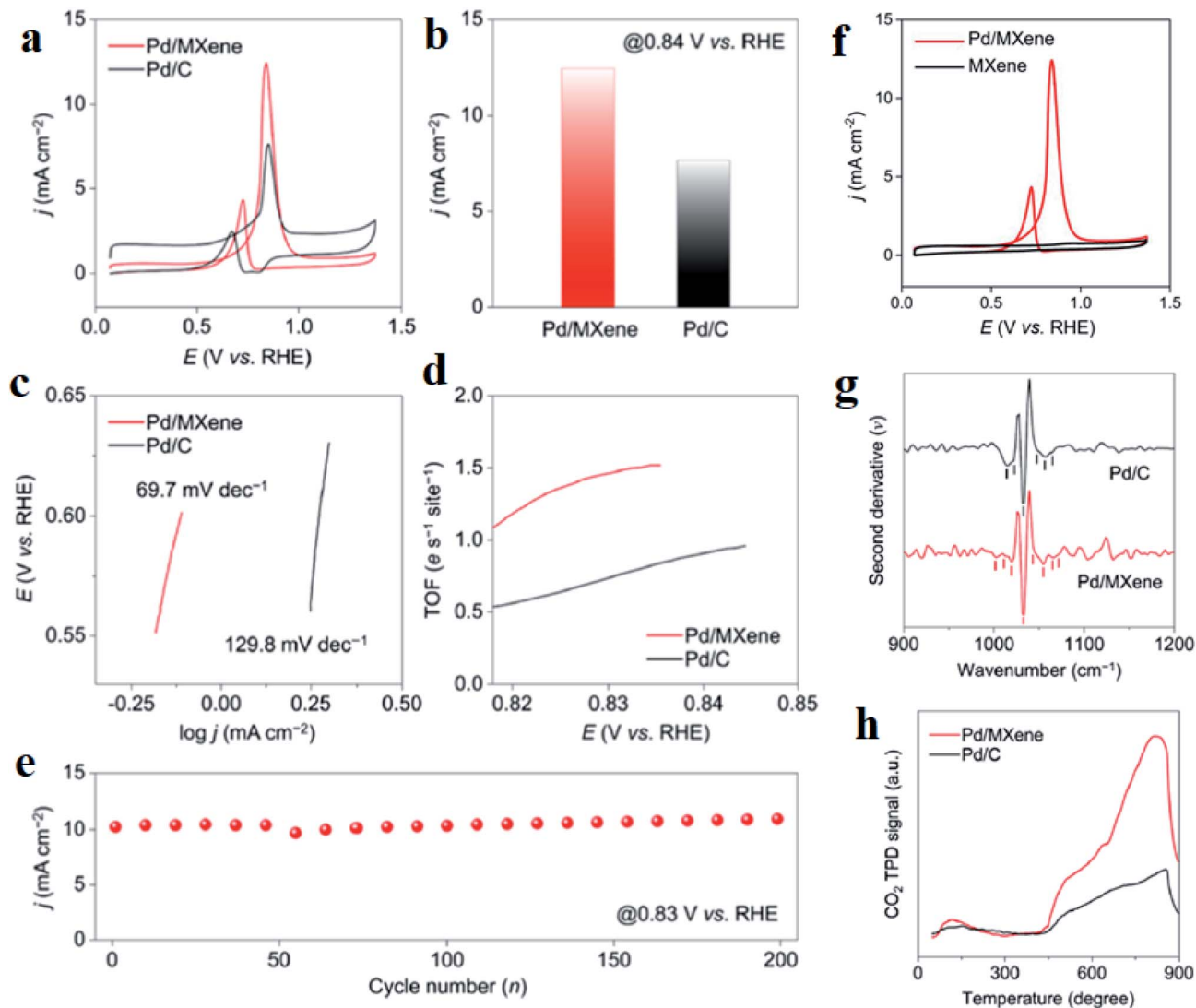
Fig. 8 (a) CVs of Pd with MXene and C as the support in 1 M methanol + 1 M potassium hydroxide, (b) current densities of Pd/C and Pd/MXene, (c) Tafel plots, (d) TOF plots, (e) current densities in the forward scan *vs.* the cycle number, (f) CVs of Pd/MXene and MXene in 1 M methanol + 1 M potassium hydroxide solution, (g) second derivative spectra of the catalysts after methanol adsorption, (h) CO_2-TPD spectra. Reproduced with permission.[221] Copyright 2020, ACS.

hydrogen bonding between the oxygen atom of methanol and the hydrogen atom of the hydroxyl group on the MXene surface, thereby improving the oxidation kinetics of the catalysts. For the first time, an MOR electrocatalyst has been developed by immobilizing Pt nanoparticles on MXene support.[222] The higher anodic current density for Pt/Ti$_3$C$_2$ MXene (about 3 times higher than that of Pt/C) and lower onset potential proves that MXene increases the MOR kinetics. The low charge transfer resistance of Pt/Ti$_3$C$_2$ MXene (as obtained from the EIS spectra) also contributes to the magnified MOR activity. CO poisoning of the Pt active sites takes place on both Pt/Ti$_3$C$_2$ and Pt/C; however, the current density of Pt/Ti$_3$C$_2$ is larger than that of Pt/C even after 7200 s. Besides, 85.1% ECSA of Pt/Ti$_3$C$_2$ is retained after 1000 CV cycles, with only 53.2% retention of ECSA of Pt/C, demonstrating the high stability of the catalyst due to the reduced agglomeration of Pt

nanoparticles on the MXene support, excellent stability of MXene under harsh environments such as strong acidic medium, and strong bonding between the MXene support and the metal nanoparticles. Despite having improved electrocatalytic activity and anti-poisoning effects, MXenes obtained using LiF/HCl etchant consist of negatively charged –O and –F terminations whose ability to trap noble metal precursors (such as $PtCl_4^{2-}$ and $PdCl_4^{2}$) reduces because of the repulsion offered by the terminations. Decorating the basal planes of the MXenes by positive charges, one can tune the surface charge, which acts as uniform dispersion sites for the metal nanoparticles. PDDA-modified Ti$_3$C$_2$T$_x$ MXene nanosheets modify the surface charge of MXene to positive, which act as growing sites for 1D worm-shaped Pt nanocrystals (named Pt NW/ PDDA-Ti$_3$C$_2$T$_x$) (schematically shown in Fig. 9)[223] and reduce the reaggregation of the MXene nanosheets. Yang *et al.*[223]
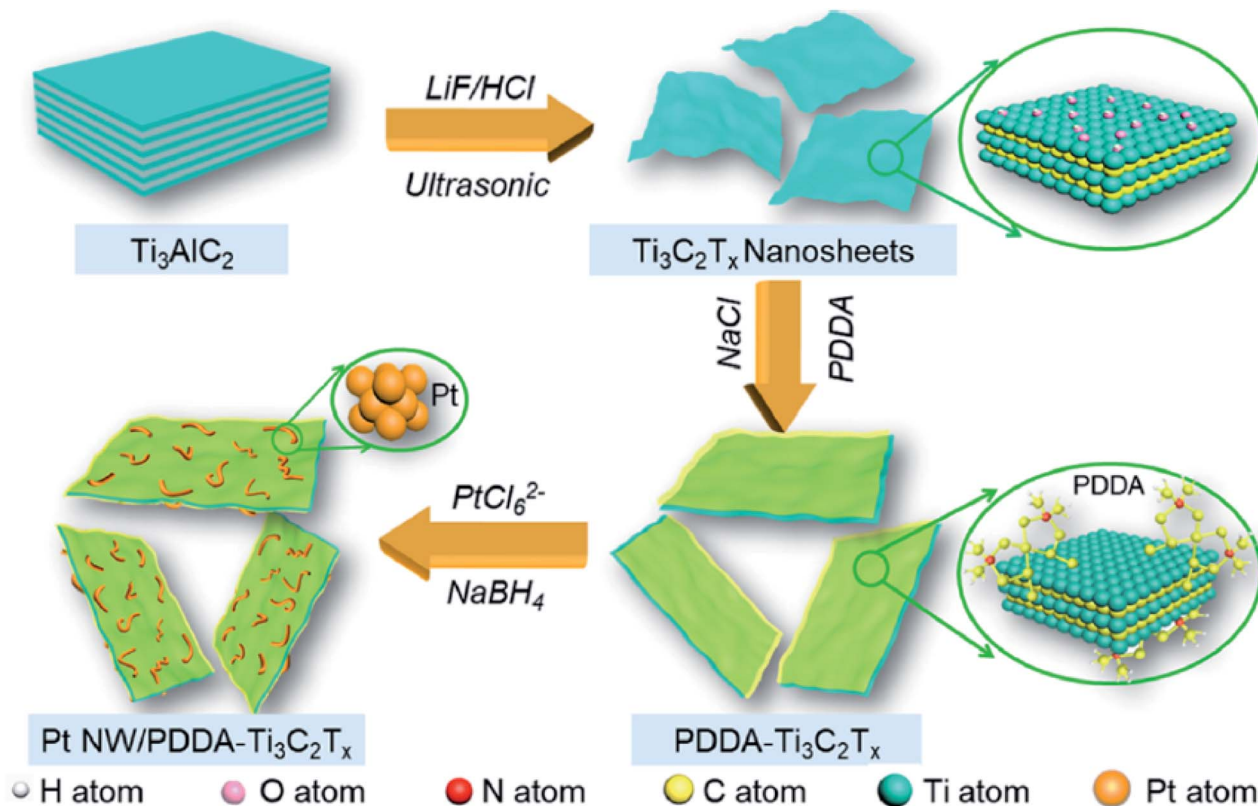
Fig. 9 Fabrication route of Pt NW/PDDA-$Ti_3C_2T_x$. Reproduced with permission.[223] Copyright 2020, ACS.

devoted this electrocatalyst Pt NW/PDDA-$Ti_3C_2T_x$ for MOR and it exhibited superior MOR activity owing to its high specific activity, good anti-poisoning, and stability for methanol oxidation, outshining traditional Pt catalysts loaded on carbon, CNT, reduced graphene oxide (RGO), and MXene supports. It delivered a high anodic current density of 17.2 mA cm^{-2}, outshining other electrodes such as Pt NPs-supported $Ti_3C_2T_x$, RGO, CNT, and C, which is due to the electroactive PDDA-Ti_3C_2 support, which increases the interfaces for triple-phase reactions, and homogeneously distributed grain boundary of the Pt nanoworms. The XPS results confirm the strong interaction between Pt and PDDA-$Ti_3C_2T_x$ than that with other carbonaceous supports. Lower onset potential (0.52 V) and peak potential (0.61 V) of CO oxidation compared to other electrodes ascertain the enhanced anti-poisoning ability of Pt NW/PDDA-$Ti_3C_2T_x$ (which is further ascertained by the Mulliken population surrounding the CO molecule). The reduction of CO poisoning of Pt NW/PDDA-$Ti_3C_2T_x$ is also confirmed by the downshifting of the d-band center relative to the Fermi energy. The uniform distribution of PDDA chains provides conductive pathways for the easy and fast migration of charges.

Another group[224] designed for the first time PtRu-decorated 2D MXene as the DMFC catalyst. They evaluated the performance of the electrocatalyst using response surface morphology (RSM) method, considering three factors (MXene composition, amount of Nafion loaded, and methanol concentration denoted by A, B, C) and current density as the response. The strong bond between PtRu and MXene offers better MOR activity (current density about 2.34 times higher than that of commercial PtRu/C), benefitting from the large active sites present on the surface of the catalyst (morphology in Fig. 10a and b). Moreover, the unique 2D surface of MXene furnishes fast charge/ion transfer, thus increasing the conductivity. They found from a survey that the PtRu/MXene electrocatalyst offers the highest current density among other catalysts owing to the uniform distribution of bimetals on the 2D structure of MXene. The response surface analysis is presented in a graphical form as a 2D contour and a 3D surface plot (Fig. 10c and d).

In the 2D contour, the response, i.e., the current density, increases when the factors A and B increase; thereafter, it starts decreasing after achieving a maximum value. These values of the factors A and B corresponding to the maximum response value are obtained within the red area of the contour (Fig. 10c), known as the high response value area. The 3D surface plot (Fig. 10d) also illustrates the same optimum factor values. The validation test of the model obtained by the RSM method using the optimum factors exhibits a current density of 187.05 mA mg_{PtRu}^{-1}, with only 0.25% error, which clearly indicates the successful development of the RSM model. Hence, MXene is a potential material support emerging in fuel cell applications. To overcome the problem of restacking and low charge transportation of MXene, composites with conducting materials have been developed.[225,226] An MOR electrocatalyst $Ti_3C_2T_x$–
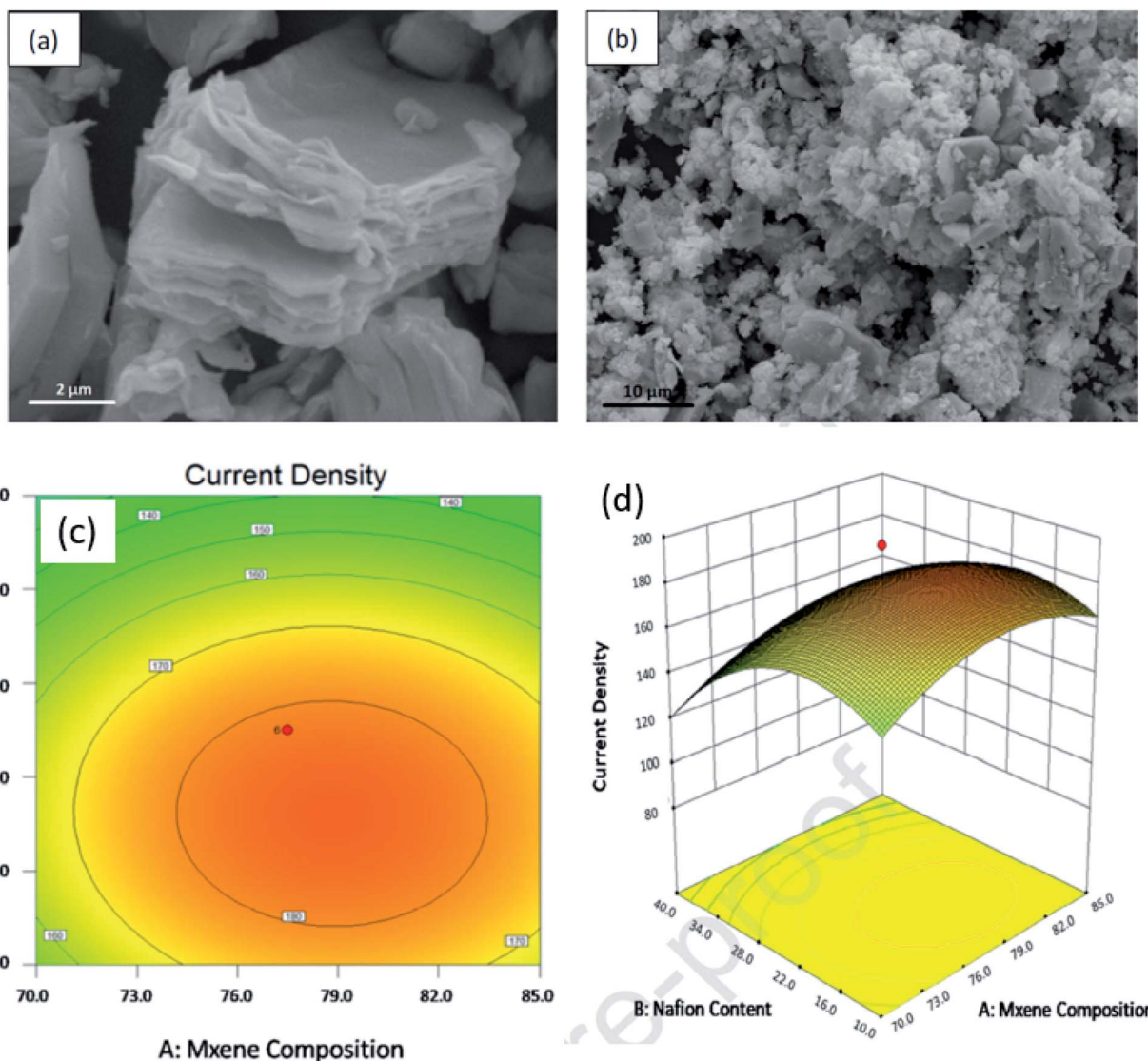
Fig. 10 SEM images of (a) MXene and (b) PtRu/MXene; response surface between the factors with response, (c) 2D contour and (d) 3D surface plot. Reproduced with permission.[224] Copyright 2020, Elsevier.

rGO composite support for Pd has been developed using the self-assembly of negatively charged $Ti_3C_2T_x$ and positively charged CTAB-modified rGO.[226] Pd/$Ti_3C_2T_x$–rGO of different stoichiometric ratios (1 : 1), (1 : 2), and (2 : 1) were developed and it was observed that the (1 : 1) ratio provided the highest ECSA value and peak current density. It thus demonstrates that an equal content of MXene and rGO provides an excess of accessible sites for Pd. Moreover, the interaction between MXene and Pd particles improves the stability. Besides, the activities (both mass and specific) of Pd/$Ti_3C_2T_x$–rGO (1 : 1) in alkaline medium are 446 mA mg^{-1} and 16.3 mA mg^{-1}, which are 1.7 and 1.57 times higher than that of the commercial Pd/C catalyst, respectively. Moreover, the mass and specific activity of Pd/$Ti_3C_2T_x$–rGO (1 : 1) is 3.04 and 2.83 times higher than that of Pd/$Ti_3C_2T_x$, respectively. The increased electrical conductivity of Pd/$Ti_3C_2T_x$–rGO (1 : 1) (obtained from the Nyquist plot) is due to the symbiotic effect of both MXene and

rGO. The current density also remains 212 mA mg^{-1} even after 7200 s, which is 9-fold that of the Pd/C current density. This high stability of the catalyst is due to the composite of $Ti_3C_2T_x$–rGO, which protects the defect sites from being corroded owing to the high corrosion resistance of $Ti_3C_2T_x$. This architecture inspires other MXene-based support materials for electrocatalysts in the field of FC applications. A porous 3D cross-linked nanoarchitecture Pd/MX–rGO was developed from nanosheets of $Ti_3C_2T_x$ and GO, with Pd NPs deposited over them.[227] A low onset potential of about 0.65 V and a peak potential of 0.71 V were obtained from formic acid oxidation using Pd/MX–rGO as the anode catalyst. It exhibited the highest current density (12 mA cm^{-2}) among other catalysts, viz., Pd/MX (3.3 mA cm^{-2}), Pd/rGO (6.1 mA cm^{-2}), and Pd/C (1.8 mA cm^{-2}). The strong interaction between Pd NPs and $Ti_3C_2T_x$ weakens the CO adsorption on the Pd active sites, further increasing formic acid oxidation. Moreover, low charge

transfer resistance (10.1 Ω) of the nanocomposite in comparison to other electrodes such as Pd/MX, Pd/rGO, and Pd/C is due to the 3D network, which provides multiple channels for the redox reactions to occur, which increase the triple-phase boundaries, leading to enhanced formic acid oxidation. High activity toward formic acid oxidation and better durability of the nanocomposite is obtained owing to the large surface area, 3D cross-linked porous structure, uniform dispersion of the Pd NPs, and the high conductivity of the nanocomposite. Another composite Pt–MXene–TiO$_2$ (ref. 228) was developed and employed for MOR by a photoactive-mediated electrocatalytic method. The nanocomposite Pt–MXene–TiO$_2$ consisted of TiO$_2$/MXene as the photoactive component, Pt as the MOR electrocatalyst, and MXene as the catalyst that administered a photoinduced electron–hole to lift the MOR activity of Pt and activate the CH$_3$OH molecules. A current density of 2750 mA mg$_{Pt}^{-1}$ was obtained under UV light irradiation, which is 3.9-fold higher than that in dark and 4.1 times that of Pt–MXene. This high current density reduces slightly to 1269.81 mA mg$_{Pt}^{-1}$ after 5000 s. This high current density is the highest among the reported photo-induced electrocatalysts. MXene here acts as the Ti source for the fabrication of MXene–TiO$_2$. This work offers novel pathways for developing stable and efficient anode catalysts for PEMFCs by exploiting the photo energy.

5.2 g-C$_3$N$_4$ nanocomposites

Nanoporous g-C$_3$N$_4$-supported PtRu MOR catalyst was developed for the first time, which delivered 78–83% higher power density than PtRu supported on Vulcan XC-72.[229] The peak current density of 60 wt% PtRu/C$_3$N$_4$ is more than twice that of 60 wt% PtRu/Vulcan XC-72 catalyst, commercially known as Pt–Ru/E-TEK. The superior performance of PtRu/C$_3$N$_4$ is accredited to the porous structure of C$_3$N$_4$. Well-developed pores provide a pathway for the effortless diffusion of fuels and intermediates into the catalyst surface, accelerating the reaction kinetics. Vulcan XC-72, on the other hand, consists of pores with random distribution, which do not favor fuel diffusion. Nitrogen atoms act as electron donors and increase the electrical conductivity, which further eases electron transfer and enhances the performance of the PtRu/C$_3$N$_4$ electrocatalyst. Moreover, the repeated triazine units of g-C$_3$N$_4$ undertake the coordination complex to anchor metal atoms or their alloys, increasing metal-support interaction. Despite having high electrical conductivity and high surface area, carbon black Vulcan XC-72R is not stable at high potential and acidic medium, causing corrosion, which further accelerates the lumping of Pt NPs and causes detachment from the support, ultimately hampering the ECSA and electrocatalytic activity. Besides, Pt NPs get stuck inside the pores, thus reducing the active interface of the triple-phase needed for electrochemical reactions. Carbon nanotubes, nanohorns, nanofibers, and nanocoils are different forms of graphitized carbon materials that have been explored as support materials. The oxygen functional groups present on the surface of carbon promote its corrosion, thereby reducing the durability of the catalyst. As suggested by the literature, the

incorporation of nitrogen into carbon reduces the surface functional oxygen groups and leads to enhanced tolerance toward oxidation.

Hence, doping carbon materials with O or N has been a trending method to obtain highly durable catalyst supports. Nitrogen as the dopant alters the electronic structure of the catalyst and decreases the interaction between Pt and the poisoning intermediates (confirmed by the increasing binding energy, as supported by XPS results). Moreover, N-doped carbon possesses high specific capacitance, influencing more and more charged species to be present within the Helmholtz layer, which provides additional sites for the removal of adsorbed poisonous intermediates by the surface groups. Inspired by all these potentials of nitrogen-doped carbon materials, g-C$_3$N$_4$ has been opted as a potential catalyst support. Mansor et al.[230] studied the effect of crystallinity, porosity, and composition on the electrocatalytic properties of the support by synthesizing three different g-C$_3$N$_4$ materials: polymeric carbon nitride (gCNM), poly(triazine) imide carbon nitride (PTI/Li$^+$Cl$^-$), and boron-doped graphitic carbon nitride (B-gCNM). gCNM was synthesized using thermolysis and condensation of dicyandiamide and melamine, B-gCNM was prepared using ionic liquid 1-butyl-3-methylimidazolium tetrafluoroborate to tune the electronic properties of gCNM by replacing carbon with boron, and PTI/Li$^+$Cl$^-$ was prepared by the ionothermal method. PTI/Li$^+$Cl$^-$ is the most crystalline as clear hexagonal shaped crystallites are observed, gCNM is the least crystalline, and B-gCNM lies in between them (Fig. 11e), whereas, B-gCNM possesses higher porosity (pore size of about 50–75 nm) than gCNM and PTI/Li$^+$Cl$^-$. Pt nanoparticles disperse in all the samples with more agglomeration in the g-C$_3$N$_4$ samples than in Vulcan (Fig. 11a–d), indicating that the catalyst deposition method is not optimized. B-gCNM and PTI/Li$^+$Cl$^-$ exhibit the highest stability, proposing that the crystallinity has a deeper connection with the stability of the catalyst, also suggesting that the presence of B and Li$^+$, Cl$^-$ as dopants may increase the stability of the catalyst. All the g-C$_3$N$_4$ supported Pt catalysts possess a lower initial ECSA value than that of commercial Pt catalysts because of their larger particle size and agglomeration problem. Pt–PTI/Li$^+$Cl$^-$ exhibits the best durability with only 19% ECSA loss after 2000 cycles, which is lower than the ECSA loss of Pt/Vulcan (36%), Pt/gCNM (81%), and Pt/B-gCNM (100%). The dependence of durability of g-C$_3$N$_4$-supported Pt catalysts on the initial ECSA value is manifested by the observation that Pt/B-gCNM, having the lowest ECSA value, exhibited the lowest durability. On the other hand, two other g-C$_3$N$_4$-supported electrocatalysts having higher ECSA value exhibited better durability, proposing the relation between metal-support interaction and electrochemical durability. All g-C$_3$N$_4$ supported electrocatalysts exhibited superior MOR activity than Pt/Vulcan. Pt/PTI–Li$^+$Cl$^-$ exhibited the lowest overpotential and Pt/B-gCNM the highest peak current density (Fig. 11f). Generally, a smaller particle size of the catalyst favors the MOR as it decreases the overpotential; however, in this case, despite having large particle sizes than the commercial catalyst, the g-C$_3$N$_4$-supported electrocatalyst exhibited the lowest overpotential, suggesting the fact that nitrogen present within or on
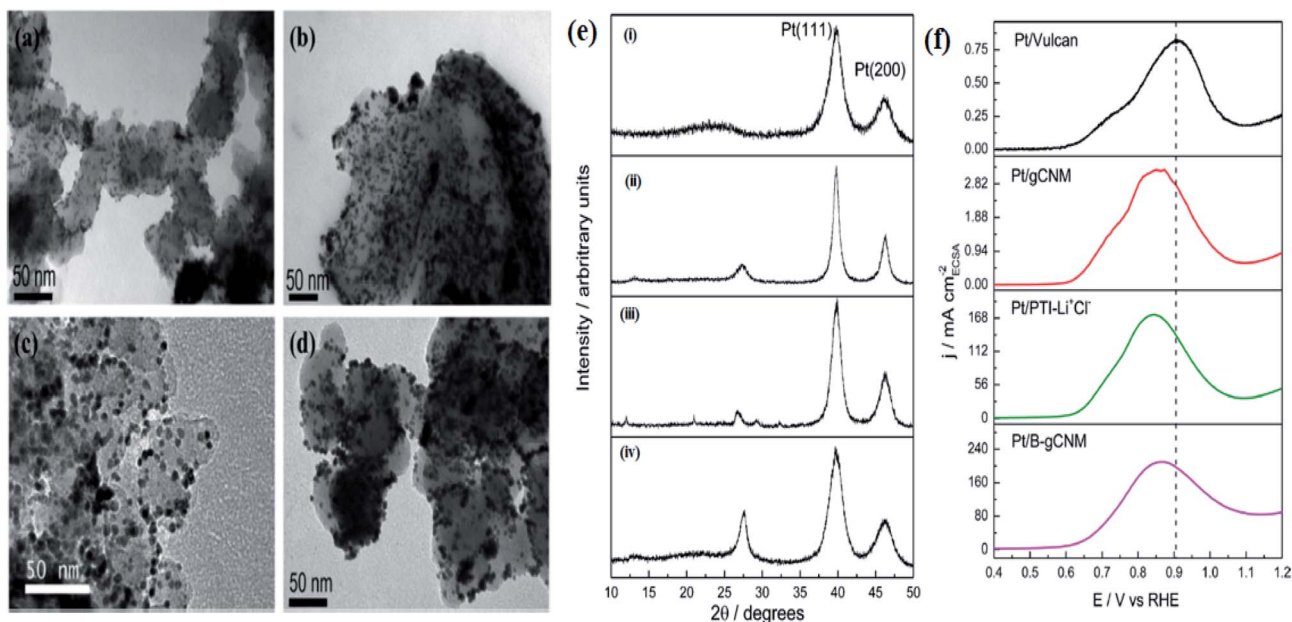
Fig. 11 TEM of Pt supported on (a) Vulcan, (b) gCNM, (c) PTILi⁺Cl⁻, (d) B-gCNM; (e) XRD pattern of the Pt catalyst supported on (i) Vulcan, (ii) gCNM, (iii) PTI/Li⁺Cl⁻, (iv) B-gCNM; (f) MOR of the Pt electrocatalysts supported all the three graphitic carbon nitrides in 1 M methanol + 0.1 M perchloric acid at a scan rate of 2 mV s⁻¹. Reproduced with permission.[230] Copyright 2014, ACS.

the support material leads to enhanced MOR activity. This work proves g-C$_3$N$_4$ as a potential alternative catalyst support to carbon as they exhibit higher corrosion resistance and enhanced MOR activity. A novel EOR electrocatalyst g-C$_3$N$_4$/graphite carbon/Pd nanocomposite (Pd@g-C$_3$N$_4$/GC) was developed.[231] The ultrathin g-C$_3$N$_4$ present as nano-islands on the nanosheet of GC in a discrete manner and the Pd nanoparticles are decorated over the GC, forming a three-phase boundary (confirmed by the HR-TEM images). The CV of different samples, namely, Pd/GC, Pd/AC, Pd@g-C$_3$N$_4$/GC, and Pd@g-C$_3$N$_4$/GC (with the composition of g-C$_3$N$_4$ varying from n = 1 to 0.0625) was done to evaluate the electrochemical performance in the absence and presence of ethanol. The CV peaks in the absence of ethanol are the characteristic peaks of hydrogen adsorption and desorption, and the development of palladium oxides and its reduction during the positive and negative scan, respectively, as well as the formation of the electrical double layer. The absence of CV peaks for Pd@g-C$_3$N$_4$ is due to the poor conductivity of g-C$_3$N$_4$ (ascertained by EIS), which leads to its poorer EOR performance. The higher ethanol oxidation peak current density of Pd@g-C$_3$N$_4$(0.0625)/GC (2156 A g⁻¹ Pd), which is higher than that of the other three catalysts, and lower onset potential is due to the suitable amount of g-C$_3$N$_4$, which improves the catalytic performance of Pd by increasing the Pd fixation sites owing to electron-coupling interaction between g-C$_3$N$_4$ and GC. Moreover, the nano-islands of g-C$_3$N$_4$ deposited on the GC surface favors the electron/ion diffusion of the electrolyte and the pyridine-type nitrogen-rich structure of g-C$_3$N$_4$ induces several electrochemically active sites when interacted with palladium nanoparticles. High graphitization degree and lesser defects of GC than AC increases its electronic conductivity, which contributed to the

faster charge transfer of Pd@g-C$_3$N$_4$(0.0625)/GC. Besides, Li et al. also established a relation between the EOR performance and the g-C$_3$N$_4$ content. They reported that excess of g-C$_3$N$_4$ content can cause blockage of the electronic transmission channel for the catalyst and excess of nitrogen may have a tendency of forming hydrogen bonding with ethanol, thereby reducing the EOR performance of Pd by hindering their contact with Pd. The addition of metal carbides and metal oxides as catalyst promoters into the noble metal catalyst increases the concentration of adsorbed OH groups on the metal surface, which favors the aldehyde to carboxylic acid transformation, thereby promoting ethanol oxidation. Compared to Pd/AC and Pd/GC, Pd@g-C$_3$N$_4$ (0.0625)/GC offers the highest electrochemical stability (after 200 CV cycles, the peak current density of Pd@g-C$_3$N$_4$ (0.0625)/GC is 1904 A g⁻¹ Pd), which is about two times of Pd/GC (966 A g⁻¹ Pd) and Pd/AC (954 A g⁻¹ Pd), on account of firstly, graphite carbon exhibiting more stable crystal structure than the amorphous one and, secondly, the electron-coupling of g-C$_3$N$_4$ and GC promoting the loading of Pd on the support surface. Thus, the Pd@g-C$_3$N$_4$/GC nanocomposite has proved to be a promising EOR anode catalyst.

Ni-based 2D g-C$_3$N$_4$ (named as Ni/gCN) supported EOR catalyst[232] outperforms its platinum counterpart Pt/g-C$_3$N$_4$ (ref. 233) and most of the reported electrocatalysts. The enhancement in the EOR activity of Ni/gCN is due to the formation of Ni(OH)$_2$, which adsorbs water to form OH species, which further reacts with adsorbed CH$_3$CO, leading to the formation of acetate and releasing the active sites on the catalyst surface. However, after adding MoS$_2$ to Pt/g-C$_3$N$_4$, the peak current density increases manifold due to the formation of the 2D–2D heterostructure of MoS$_2$ and g-C$_3$N$_4$. They varied the ethanol concentration and observed that with an increase in the alcohol concentration, the

charge transfer resistance decreases; hence, the best results (peak current density $\sim$122.8 mA g^{-1} and onset potential $\sim$0.46 V) are obtained for 3 M ethanol. Normally, the carbonaceous intermediates get adsorbed on the catalyst surface, leading to a decrease in the current density after few seconds and it reduces by 50% in the first 1000 s, whereas a completely opposite trend is observed for Ni/gCN, where the current density first increases from 77 to 86 A g^{-1} and then remains constant up to 1000 s. This unique trend of Ni/gCN is attributed to the less amount of adsorption of carbonaceous species on the active sites of the catalyst and its ability to regenerate the active sites.

5.3 TMDCs nanocomposites

TMDCs have attracted attention as a potential Pt alternative owing to their natural abundance and unique catalytic ability due to the excellent stability and favorable interactions with metal catalysts.[234] Among them, MoS_2 possesses several fascinating properties such as easy synthesis, longer active sites, low cost, and basal planes, making it a probable candidate for developing hybrid electrocatalysts. 3D nanodendrites of Au@Pt core–shell nanostructures were decorated over MoS_2 nanosheets to form Au@Pt/MoS_2.[235] Nanocomposites with a thick Pt shell (denoted as Au@Pt/MoS_2-2) exhibited higher ECSA and electrocatalytic activity than the catalysts Pt/C, Pt/MoS_2, and thin Pt shell (Au@Pt/MoS_2-1). Au@Pt/MoS_2-2 outperformed the other three electrocatalysts in the MOR performance with a mass activity of 6.24 A mg^{-1}, which is about 3389, 20.3, and 4.5-fold of Pt/C, Pt/MoS_2, and Au@Pt/MoS_2-1, respectively. The low charge transfer resistance of the thick shell reflects the faster reaction kinetics, which is ascribed mainly to the interruption of adsorption of the intermediate on the catalyst surface. The synergistic effects of the large surface area of MoS_2, the special porous structure of the Au@Pt core–shell, and the better catalytic activity of Pt nanoshells lead to the outstanding MOR performance of Au@Pt/MoS_2 electrocatalyst, which is

comparable to or better than several other reported performances. MoS_2 nanosheets prepared by other methods such as mechanical exfoliation, chemical vapor deposition, and liquid exfoliation are normally semiconducting (2H phase) in nature, whereas chemically exfoliated MoS_2 nanosheets (ce-MoS_2 NSs) are generally in the metallic phase. 0D–2D functional hybrid of water-dispersible noble metal nanocrystals (NM NCs) modified ce-MoS_2 was prepared using carboxymethyl cellulose as a stabilizer in an aqueous solution.[236] The electron transferability of ce-MoS_2 NSs increases after the incorporation of the NM NCs, which is also supported by the decrease in the charge transfer resistance. The MOR performance of Pd–MoS_2 NSs was found to be better than that of Pd/C in alkaline medium (anodic peak current density is 433.5 mA mg^{-1}, about 2.8 times that of the Pd/C catalyst). The metallic 1T phase present in ce-MoS_2 is the reason behind such increased conductivity and MOR activity.

After annealing at 300 °C for 1 h under an argon environment, the 1T phase transforms to the semiconducting 2H phase, which leads to a decrease in methanol oxidation (reduces from 48 mA to 16 mA) (Fig. 12a) and increases the charge transfer resistance (Fig. 12b). Thus, a little variance in the polymorphic forms of MoS_2 can predominantly affect the electrocatalytic activity. Moreover, the homogeneous distribution of Pd NCs on ce-MoS_2 NSs increases their surface area, contributing to higher MOR activity. The semiconducting nature of pure MoS_2 nanosheets limits their catalytic activity, which can be optimized by combining it with conducting graphene,[237] reduced graphene oxide (rGO),[238,239] etc. Graphene-like 2D structural MoS_2 nanosheets act as co-building blocks to develop 3D hybrid nanostructures, thereby lowering the charge transfer resistance of the catalyst. Ultrafine Pt nanoparticles decorated on the 3D architecture of graphene (G) and MoS_2 nanosheets (Pt/G–MoS_2) exhibited higher MOR and HER activity along with long-term stability and anti-toxic capacity, outshining catalysts such as Pt/G, Pt/MoS_2, and commercial Pt/

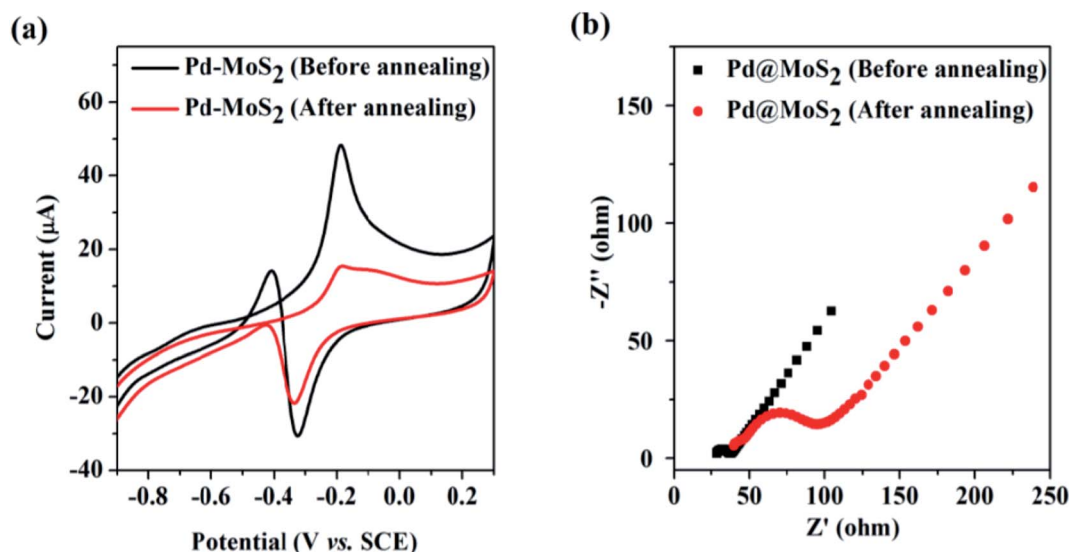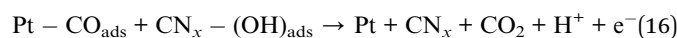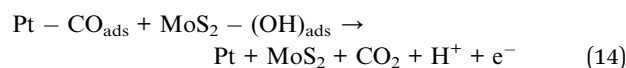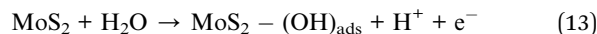Fig. 12   (a) CV of Pd–MoS_2-modified ITO electrodes in 0.5 M potassium hydroxide + 1.0 M methanol solution before and after annealing, (b) EIS measurement of Pd–MoS_2-modified ITO electrodes before and after annealing. Reproduced with permission.[236] Copyright 2014, RSC.

C with the same Pt loading.[237] Such 3D porous architecture provides multiple channels for the reactants to the interior of the catalyst and improves the electron transfer between the active sites and the matrix. The hydroxyl and epoxide groups present on the GO surfaces provide active sites for Pt^{2+} adsorption and the 3D structure offers large, accessible pores of varying sizes for the fast transportation of Pt^{2+} to the nucleation sites, resulting in the uniform distribution of Pt in the hybrid material. Pure MoS_2 nanosheets do not possess sufficient nucleation sites for Pt, hence leading to the formation of irregular shaped aggregates of Pt on its surface. On the other hand, comparatively low surface area and large micropores on carbon black-supported material lead to poor dispersion of Pt. Different G/MoS_2 ratio 9 : 1, 7 : 3, 5 : 5, and 3 : 7 have been considered, out of which $Pt/G_5-(MoS_2)_5$ provides the lowest oxidation potential, highest ECSA value, and better anti-poisoning ability. Thus, the porous 3D hybrid architecture helped in realizing a better electrocatalyst by preventing the agglomeration of MoS_2 nanosheets and utilizing its benefit to the fullest. When rGO is incorporated with MoS_2 and Pt nano-particles, the peak current density of MOR (7.35 mA cm^{-2}) and formic acid oxidation (6.8 mA cm^{-2}) are several folds higher than that of Pt–MoS_2 and Pt/C electrocatalysts,[238] suggesting that MoS_2/RGO is a promising Pt support in practical fuel cell application. Similarly, by inserting flower-like MoS_2 between ultrafine Pt nanoparticles and nitrogen-doped rGO (Pt@MoS_2/ NrGO),[239] a superior alcohol oxidation electrocatalyst and oxygen evolution reaction (ORR) catalyst was obtained owing to the symbiotic effect of Pt and NrGO. The Pt@MoS_2/NrGO cata-lyst manifested superior catalytic activity, with a mass activity of 448.0 mA mg_{Pt}^{-1} for methanol, 158.0 mA mg_{Pt}^{-1} for ethylene glycol (EG), and 147.0 mA mg_{Pt}^{-1} for glycerol, which are greater than that of commercial Pt–C by several folds. It exhibited high stability with only 18.92, 17.98, and 14.76% activity loss rate in the case of oxidation of methanol, EG, and glycerol, respectively, which is superior to Pt@NrGO and Pt/C. The existence of hydrophilic groups on the edge of NrGO and sulphur planes in MoS_2 stimulate water adsorption on the catalyst surface, which further assists the oxidation of CO to CO_2, thereby reactivating the Pt surface by removing the adsorbed CO species. In this way, the synergistic effect promotes the oxidation activity of Pt@MoS_2/NrGO. Bagasse is a bio-waste that creates environ-mental problems; thus, deriving carbon-based materials from bagasse can make the process energy-efficient and environment-friendly. MoS_2-supported porous nitrogen-doped carbon (CN_x) obtained from bagasse acts as a conductive support for Pt and is an excellent MOR catalyst.[240] The edge sites of MoS_2 that get covered due to agglomeration can be exposed by the formation of a composite with CN_x, which provides binding sites for the growth of MoS_2. Moreover, the combina-tion of CN_x with MoS_2 makes the edge sites and defects on MoS_2/CN_x electrochemically active, in addition to the edge sites of unsaturated bonding atoms. The mass current density of Pt/ MoS_2/CN_x (1030.2 mA mg_{Pt}^{-1}) and Pt/MoS_2/C (710.1 mA mg_{Pt}^{-1}) is higher than that of Pt/MoS_2 (162.6 mA mg_{Pt}^{-1}) and the commercial catalyst Pt/C (405.4 mA mg_{Pt}^{-1}), suggesting that the combination of MoS_2 and CN_x improves the conductivity and

enhances the catalytic activity. Pt/MoS_2/CN_x possesses better durability among other catalysts, leading to the fact that N doping in the carbon skeleton changes the asymmetricity of the hexagonal carbon network and introduces defects, in addition, supplying more anchoring sites for MoS_2 and Pt, leading to the improvement of electron transfer and MOR performance in acidic medium. Abundant Mo and S sites, oxophilic C–N defects, and the large porous structure assist in adsorbing more water molecules and recovering the Pt sites. Besides, the fast transport of CO_{ads} on various faces of MoS_2 imparts it resistance against CO poisoning. The electrochemical reactions involved in the MOR activity are explained in eqn (13)–(16).

$$MoS_2 + H_2O \rightarrow MoS_2 - (OH)_{ads} + H^+ + e^- \qquad (13)$$

$$Pt - CO_{ads} + MoS_2 - (OH)_{ads} \rightarrow \\ Pt + MoS_2 + CO_2 + H^+ + e^- \qquad (14)$$

$$CN_x + H_2O \rightarrow CN_x - (OH)_{ads} + H^+ + e^- \qquad (15)$$

$$Pt - CO_{ads} + CN_x - (OH)_{ads} \rightarrow Pt + CN_x + CO_2 + H^+ + e^- \quad (16)$$

5.4 Transition metal oxides nanocomposites

The electrocatalytic activity of oxide materials depends on different parameters such as surface area, morphology, and porosity, which are tunable using different synthetic methods, generally by varying the surfactants in the hydrothermal method. Taking advantage of the fact that binder-free electroactive material grown on Ni foam (NF) enhances the electrochemical properties of the material, binder-free Co_3O_4 was grown on NF and the effect of different counter anions on the morphology was observed. Chloride ions used in the solution lead to the forma-tion of Co_3O_4 microflower, sulfate ions lead to a microsphere-like structure, and acetate ions lead to a nanograss-like structure (Fig. 13).[241] The difference in the morphology of Co_3O_4 arises due to the variation in the anionic sizes and electrostatic interactions between the precursor phases because the growth of a particular crystallographic plane is related to the surface energy, which is governed by the adsorption of species during the synthetic process.[242,243] Thus, different anions prefer to adsorb on different crystallographic planes, forming different morphology of the oxide materials. The microsphere and nanograss-like Co_3O_4/Ni exhibit higher oxidation peak than microflower Co_3O_4/Ni due to their large surface area and porosity.

The lower onset potential of these morphologies than the reported materials is because of (i) direct growth of Co_3O_4 on NF, (ii) binder-free synthesis, and (iii) high surface area and porosity, leading to the better diffusion of electrolyte ions. At 0.6 V, the anodic peak current density lies in the order: micro-flower (28 A g^{-1}) < nanograss (34.9 A g^{-1}) < microsphere (36.2 A g^{-1}). The current decay after 1000 cycles and current retention in microsphere-Co_3O_4 and nanograss-Co_3O_4 after 1000 cycles are higher than that in the microflower morphology. Thus, by varying the morphology, we can tune the electro-catalytic properties of a catalyst and make the best use of it.
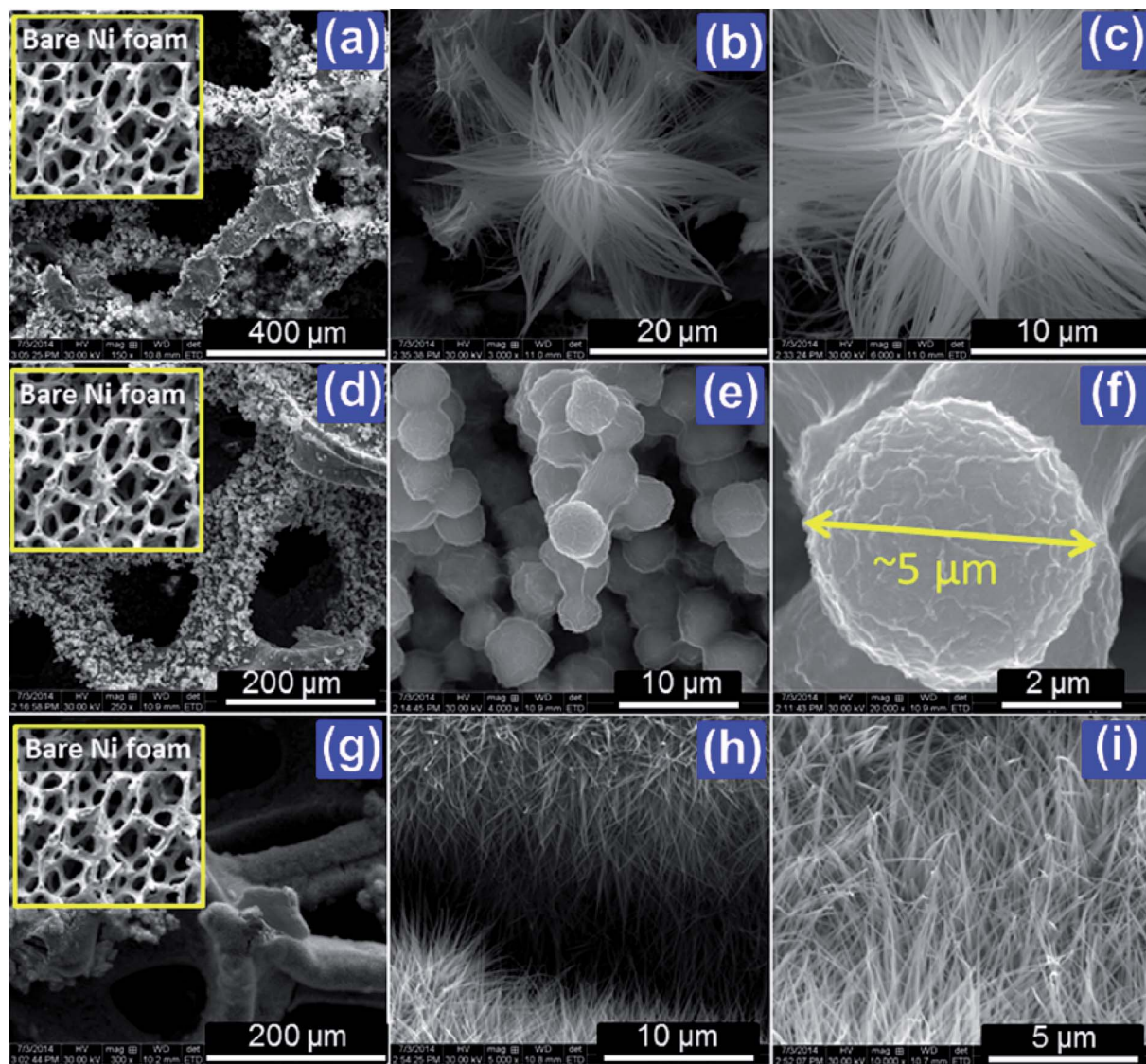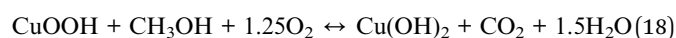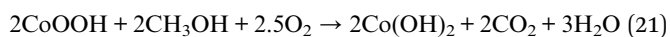
Fig. 13 FESEM images of Co_3O_4 grown on NF using different anions, (a–c) microflower, (d–f) microsphere, and (g–i) nanograss-like Co_3O_4. Reproduced with permission.[241] Copyright 2018, Elsevier.

Cu-based oxide catalysts have received special attention as DMFC catalysts because of their low cost and earth abundance. *In situ* grown CuO nanowires (NWs) on Cu substrate exhibit current density (50 A g^{-1} or 100 mA cm^{-2}) and stability (up to 1800 s) superior to other reported Cu-based electrodes.[244] The electrochemical reactions taking place on the CuO NW surface are explained as follows.

$$CuO + OH^- \leftrightarrow CuOOH + e^- \qquad (17)$$

$$CuOOH + CH_3OH + 1.25O_2 \leftrightarrow Cu(OH)_2 + CO_2 + 1.5H_2O \qquad (18)$$

Porous $MnCo_2O_4$ nanoflakes grown on conducting NF substrate outperform Co_3O_4/NF and other reported catalysts as the DMFC anode catalyst.[245] $MnCo_2O_4$/NF covers larger CV area and anodic current than Co_3O_4/NF (in 1 M KOH + 0.5 M methanol solution). Compared to Co_3O_4/NF, $MnCo_2O_4$/NF

displayed higher stability, holding 96 A g^{-1} and 91.5% retention after 2000 s. Negligible contribution from bare NF suggests NF to be an ideal substrate for the MOR electrocatalyst. Moreover, 66% current density retention is obtained after 1000 CV cycles, thus, making $MnCo_2O_4$ a promising electrocatalyst, opening the pathway for other metal oxide DMFC electrocatalysts. The mechanism of MOR of $MnCo_2O_4$ is as follows.

$$MnCo_2O_4 + OH^- + H_2O + 3e^- \rightarrow MnOOH + 2CoOOH \qquad (19)$$

$$MnOOH + CH_3OH + 1.25O_2 \rightarrow Mn(OH)_2 + CO_2 + 1.5H_2O \qquad (20)$$

$$2CoOOH + 2CH_3OH + 2.5O_2 \rightarrow 2Co(OH)_2 + 2CO_2 + 3H_2O \qquad (21)$$
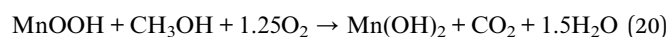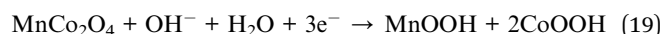
The electrochemical oxidation activity of different 2D material-based anode catalysts of DOFC are compared in Table 2.

Table 2 Comparison of the electrochemical performance of different anode catalysts for DOFC

Serial no.	Material (anode catalyst)	Fuel used	Onset potential (V)	Peak anode current density	Electrolyte medium	Ref.
1	$Pt_{69}Rh_8Fe_{23}$-PNS@MXene	Ethanol (1 M)	0.433	3407.7 mA mg^{-1}	Alkaline (KOH)	220
2	$Pd/Ti_3C_2T_x$	Methanol (1 M)	—	12.4 mA cm^{-2}	Alkaline (KOH)	221
3	Pt/Ti_3C_2	Methanol (0.5 M)	—	1.137 mA cm^{-2}	Acidic (H_2SO_4)	222
4	Pt NW/PDDA-$Ti_3C_2T_x$	Methanol (1 M)	0.52	17.2 mA cm^{-2}	Acidic (H_2SO_4)	223
5	PtRu/MXene	Methanol (2 M)	—	12.46 mA cm^{-2}	Acidic (H_2SO_4)	224
6	$Pd/Ti_3C_2T_x$–rGO	Methanol (1 M)	—	Mass activity (446 mA mg^{-1}), specific activity (16.3 mA mg^{-1})	Alkaline (KOH)	226
7	Pd/MX–rGO	Formic acid (0.5 M)	0.65	12 mA cm^{-2}	Acidic (H_2SO_4)	227
8	Pt–MXene–TiO_2	Methanol (1 M)	0.33	2750 mA mg$_{Pt}^{-1}$	Acidic (H_2SO_4)	228
9	PtRu/C_3N_4	Methanol	—	130 mA cm^{-2} (at 400 mV)	—	229
10	Pt/gCNM Pt/PTI–Li$^+$Cl$^-$ Pt/B-gCNM	Methanol (1 M)	—	3.21 mA cm^{-2}, 174 mA cm^{-2}, 209 mA cm^{-2}	Acidic ($HClO_4$)	230
11	Pd@g-C_3N_4/GC	Ethanol (1 M)	0.32	2156 A g^{-1} Pd	Alkaline (KOH)	231
12	Ni/gCN	Ethanol (3 M)	0.46	122.8 mA g^{-1}	Alkaline (NaOH)	232
13	Pt/g-C_3N_4/MoS_2	Ethanol	—	76.9 mA mg$_{Pt}^{-1}$	Alkaline (KOH)	233
14	Au@Pt/MoS_2	Methanol (1 M)	−0.24	6.24 A mg^{-1}	Alkaline (NaOH)	235
15	Pd–MoS_2 NSs	Methanol (1 M)	—	433.5 mA mg^{-1}	Alkaline (KOH)	236
16	Pt/G–MoS_2	Methanol (2 M)	—	13.3 mA cm^{-2}	Acidic (H_2SO_4)	237
17	Pt–MoS_2/RGO	Methanol (1 M), formic acid (0.5 M)	—	7.35 mA cm^{-2} (methanol) 6.8 mA cm^{-2} (formic acid)	Acidic (H_2SO_4)	238
18	Pt@MoS_2/NrGO	Methanol (1 M), ethylene glycol (1 M), glycerol (1 M)	—	448.0 mA mg$_{Pt}^{-1}$ for methanol, 158.0 mA mg$_{Pt}^{-1}$ for ethylene glycol (EG), and 147.0 mA mg$_{Pt}^{-1}$ for glycerol	Acidic (H_2SO_4)	239
19	Pt/MoS_2/CN_x	Methanol (0.5 M)	—	1030.2 mA mg$_{Pt}^{-1}$	Acidic (H_2SO_4)	240
20	Co_3O_4/Ni	Methanol (0.5 M)	0.32–0.34	Microflower (28 A g^{-1}), nanograss (34.9 A g^{-1}), microsphere (36.2 A g^{-1})	Alkaline (KOH)	241
21	CuO NWs/Cu	Methanol (0.5 M)	—	50 A g^{-1} or 100 mA cm^{-2}	Alkaline (KOH)	244
22	$MnCo_2O_4$/NF	Methanol (0.5 M)	1.3	96 A g^{-1}	Alkaline (KOH)	245
23	Pt/BN-GA	Methanol (1 M)	—	1184.5 mA mg^{-1}	Acidic (H_2SO_4)	97
24	Pd@C–rGO	Ethylene glycol (0.5 M)	−0.5	~3 mA cm^{-2}	Alkaline (KOH)	100
25	Pt–Pd decorated rGO	Ethylene glycol (0.5 M)	0.418	803.4 mA mg^{-1}	Acidic (H_2SO_4)	101
26	Pd–C@MoS_2/RGO	Methanol (1 M)	—	11.2 mA cm^{-2} (methanol), 2 mA cm^2 (ethylene glycol)	Alkaline (KOH)	102

6   Summary and outlook

In this review, we encapsulated a detailed description of fuel cells along with their mechanism and condensed different types of fuel cells depending on the types of electrolytes, ions, fuels, mode of fuel supply, and temperature range used in the fuel cell operation. We also outlined the problems pertaining to different types of fuel cells. Large specific surface area, tunable

electronic properties, and other intriguing properties make 2D materials outshine other nanostructured materials as anode catalysts in direct alcohol fuel cell application. Considering some of the drawbacks of graphene such as chemical inertness, insufficient loading sites for noble-metal nanoparticles, and restacking problem, this review focused on 2D materials (mainly MXene, graphitic carbon nitride, transition metal dichalcogenides, and transition metal oxides) beyond graphene and summarized their properties and application in direct alcohol fuel cell either as an active material or as a support/substrate. To date, MXene or composites of MXenes with conducting materials have been used as catalyst supports for noble metal nanoparticles or alloys in direct alcohol fuel cells. MXene as a support provides hydrogen bonding between alcohol molecules and hydroxyl groups on its surface, thereby increasing the catalytic activity. In MXene, (i) surfaces possess Lewis basic sites, which help in adsorbing more and more alcohol molecules, leading to enhanced electrochemical activity, (ii) hydrophilic terminations such as OH^- and F^- act as electron donors and promote the interaction between the metal and the support, further increasing the oxidation reaction, (iii) by garnishing the basal planes of MXene, its surface charge can be altered, which further behave as uniform distribution sites for the metal nanoparticles. Graphitic carbon nitride is considered a promising candidate as an electrocatalyst and has been used as the catalyst support for noble metal NPs or non-noble metals due to the following reasons: (i) its porous structure accelerates the diffusion of ions into the catalyst surface, making fuel oxidation effortless, (ii) nitrogen present in its structure increases the conductivity and acts as a electron donor, further increasing the electron transfer, (iii) its repeated triazine units anchor the metal atoms/alloys, thereby promoting metal-support interaction, (iv) N-doped carbon or $g-C_3N_4$ possess high specific capacitance and help in removing the adsorbed poisonous intermediates by providing extra sites for the surface groups. Transition metal dichalcogenides exhibit polymorphism and different polymorphs lead to different electrocatalytic activity. Mostly, MoS_2 has been explored as an anode catalyst support and composites with other conducting materials such as graphene and reduced graphene oxide have been explored to reduce its agglomeration, further increasing the electrocatalytic activity. The Mo and S atoms in MoS_2, C–N defects, and porous nature of MoS_2 help in adsorbing more H_2O molecules and assist in recovering the Pt sites. Besides, the various faces of MoS_2 speed up the transportation of the adsorbed CO species and improves their CO poisoning. 2D transition metal oxides are a good replacement of the noble metals due to the presence of multiple oxidation states of the transition metal. Spinel oxides are frequently studied anode catalysts. By varying the anions used in the synthetic process, one can obtain different morphology of metal oxides and can tune the electrochemical properties. Thus, we can conclude that for a better and faster electrochemical reaction and efficient electrocatalyst, one needs to keep in mind the following factors: (i) porosity of the catalyst as a porous structure enhances the electrocatalytic reactions, (ii) hydrophilicity of the material for ensuring durability and anti-poisoning ability, (iii) presence of

Lewis basic sites, (iv) metal-support interaction, (v) anti-poisoning of the noble-metal and electroactive material, (vi) a good choice of support/substrate, which can reduce the agglomeration of the active material. The 2D materials are mostly used as catalyst support and have come a long way; however, scalability and the synthetic methods need to be ameliorated. More novel 2D structures and nanocomposites with other nanostructured materials can be more explored as non-noble electrocatalysts. As we have seen that unique heterostructures can provide scope for increasing the surface area, porosity, interactions between the components, and expose more electrochemically active sites, thus, one can explore a variety of heterostructures such as 1D–2D, 2D–3D, 0D–1D, 0D–2D, and 0D–3D as anode catalysts for DOFCs.

Author contributions

Kashmiri Baruah prepared the original draft of the manuscript. Pritam Deb contributed to methodology, supervision, reviewing, and editing of the manuscript.

Conflicts of interest

The authors declare that they have no conflict of interest.

Acknowledgements

References

1 A. J. Medford, A. Vojvodic, J. S. Hummelshøj, J. Voss, F. Abild-Pedersen, F. Studt, T. Bligaard, A. Nilsson and J. K. Nørskov, *J. Catal.*, 2015, **328**, 36–42.

2 J. K. Nørskov, T. Bligaard, J. Rossmeisl and C. H. Christensen, *Nat. Chem.*, 2009, **1**, 37–46.

3 Z. W. Seh, J. Kibsgaard, C. F. Dickens, I. Chorkendorff, J. K. Nørskov and T. F. Jaramillo, *Science*, 2017, **355**, 6321.

4 J. K. Nørskov, T. Bligaard, J. Rossmeisl and C. H. Christensen, *Nat. Chem.*, 2009, **1**, 37–46.

5 A. Nilssona, L. G. M. Pettersson, B. Hammer, T. Bligaard, C. H. Christensen and J. K. Nørskov, *Catal. Lett.*, 2005, **100**, 111–114.

6 S. K. Behera, P. Deb and A. Ghosh, *Phys. Chem. Chem. Phys.*, 2016, **18**, 23220–23230.

7 K. S. Novoselov, A. K. Geim, S. V. Morozov, D. Jiang, Y. Zhang, S. V. Dubonos, I. V. Grigorieva and A. A. Firsov, *Science*, 2004, **306**, 666–669.

8 H. Zhang, *ACS Nano*, 2015, **9**, 9451–9469.

9 M. Fan, J. Wu, J. Yuan, L. Deng, N. Zhong, L. He, J. Cui, Z. Wang, S. K. Behera, C. Zhang, J. Lai, B. I. Jawdat, R. Vajtai, P. Deb, Y. Huang, J. Qian, J. Yang, J. M. Tour,

J. Lou, C. W. Chu, D. Sun and P. M. Ajayan, *Adv. Mater.*, 2019, **31**, 1805778.

10 S. K. Behera, P. Deb and A. Ghosh, *ChemistrySelect*, 2017, **2**, 3657–3667.

11 K. Baruah, S. K. Behera and P. Deb, *Bull. Am. Phys. Soc.*, 2017, **62**, 1121.

12 F. Fina, S. K. Callear, G. M. Carins and J. T. S. Irvine, *Chem. Mater.*, 2015, **27**, 2612–2618.

13 M. Naguib, M. Kurtoglu, V. Presser, J. Lu, J. Niu, M. Heon, L. Hultman, Y. Gogotsi and M. W. Barsoum, *Adv. Mater.*, 2011, **23**, 4248–4253.

14 B. Smitha, S. Sridhar and A. A. Khan, *J. Membr. Sci.*, 2005, **259**, 10–26.

15 S. S. Ozdemir, M. G. Buonomenna and E. Drioli, *Appl. Catal., A*, 2006, **307**, 167–183.

16 S. Sharma and B. G. Pollet, *J. Power Sources*, 2012, **208**, 96–119.

17 Y. Wang, K. S. Chen, J. Mishler, S. C. Cho and X. C. Adroher, *Appl. Energy*, 2011, **88**, 981–1007.

18 Y. Y. Xu, C. Gao, H. Kong, D. Y. Yan, Y. Z. Jin and P. C. P. Watts, *Macromolecules*, 2004, **37**, 8846–8853.

19 X. Wang, C. Hu, Y. Xiong, H. Liu, G. Du and X. He, *J. Power Sources*, 2011, **196**, 1904–1908.

20 J. Lobato, P. Canizares, D. Ubeda, F. J. Pinar and M. A. Rodrigo, *Appl. Catal., B*, 2011, **106**, 174–180.

21 A. Ermete, *J. Power Sources*, 2007, **170**, 1–12.

22 Y. Kim, S. M. Kwon, D. Y. Kim, H. S. Kim and H. J. Jin, *Curr. Appl. Phys.*, 2009, **9**, 100–103.

23 J.-Y. Choi, D. Higgins and Z. Chen, *J. Electrochem. Soc.*, 2012, **159**, 86–89.

24 D. J. Guo, X. P. Qju, W. T. Zhu and L. Q. Chen, *Appl. Catal., B*, 2009, **89**, 597–601.

25 A. S. Karakoti, J. E. S. King, A. Vincent and S. Seal, *Appl. Catal., A*, 2010, **388**, 262–271.

26 X. Jin, T.-H. Gu, K.-G. Lee, M. J. Kim, M. S. Islam and S.-J. Hwang, *Coord. Chem. Rev.*, 2020, **415**, 213280.

27 H. Xu, P. Song, Y. Zhang and Y. Du, *Nanoscale*, 2018, **10**, 12605–12611.

28 P. Chandran, D. Puthusseri and S. Ramaprabhu, *Int. J. Hydrogen Energy*, 2019, **44**, 4951–4961.

29 B. Li, Q. Yan, C. Song, P. Yan, K. Ye, K. Cheng, K. Zhu, J. Yan, D. Cao and G. Wang, *Appl. Surf. Sci.*, 2019, **491**, 659–669.

30 F. Gao, Y. Zhang, P. Song, J. Wang, C. Wang, J. Guo and Y. Du, *J. Power Sources*, 2019, **418**, 186–192.

31 L. Jin, H. Xu, C. Chen, T. Song, C. Wang, Y. Wang, H. Shang and Y. Du, *J. Colloid Interface Sci.*, 2019, **540**, 265–271.

32 M. Guo, Y. Cheng, Y. Yu and J. Hu, *Appl. Surf. Sci.*, 2017, **416**, 439–445.

33 S. Guo, J. Sun, Z. Zhang, A. Sheng, M. Gao, Z. Wang, B. Zhao and W. Ding, *J. Mater. Chem. A*, 2017, **5**, 15879–15890.

34 M. G. Hosseini and R. Mahmoodi, *New J. Chem.*, 2017, **41**, 13408–13417.

35 A. Balinait, A. Zabielait, L. Tamaauskait-Tamainait and E. Norkus, *J. Electrochem. Soc.*, 2018, **165**, 1249–1253.

36 C. Song, G. Wang, B. Li, C. Miao, K. Ma, K. Zhu, K. Cheng, K. Ye, J. Yan, D. Cao and J. Yin, *Electrochim. Acta*, 2019, **299**, 395–404.

37 H. Zhang, J. He, C. Zhai and M. Zhu, *Chin. Chem. Lett.*, 2019, **30**, 2338–2342.

38 L. Dai, Q. Qin, X. Zhao, C. Xu, C. Hu, S. Mo, Y. O. Wang, S. Lin, Z. Tang and N. Zheng, *ACS Cent. Sci.*, 2016, **2**, 538–544.

39 D. J. L. Brett, A. R. Kucernak, P. Aguiar, S. C. Atkins, N. P. Brandon, R. Clague, L. F. Cohen, G. Hinds, C. Kalyvas, G. J. Offer, B. Ladewig, R. Maher, A. Marquis, P. Shearing, N. Vasileiadis and V. Vesovic, *ChemPhysChem*, 2010, **11**, 2714–2731.

40 S. Chu and A. Majumdar, *Nature*, 2012, **488**, 294–303.

41 M. Winter and R. Brodd, *Chem. Rev.*, 2004, **104**, 4245–4269.

42 C. Rice, S. Ha, R. I. Masel and A. Wieckowski, *J. Power Sources*, 2003, **115**, 229–235.

43 G. Che, B. B. Lakshmi, E. R. Fisher and C. R. Martin, *Nature*, 1998, **393**, 346.

44 Z. Yang, J. Zhang, M. C. Kintner-Meyer, X. Lu, D. Choi, J. P. Lemmon and J. Liu, *Chem. Rev.*, 2011, **111**, 3577.

45 K. Sundmacher, *Ind. Eng. Chem. Res.*, 2010, **49**, 10159–10182.

46 X. Li, *Principles of Fuel Cells*, Taylor & Francis, 2005, p. 572.

47 L. Yang, J. Ge, C. Liu, G. Wang and W. Xing, *Curr. Opin. Electrochem.*, 2017, **4**, 83–88.

48 J. N. Tiwari, R. N. Tiwari, G. Singh and K. S. Kim, *Nano Energy*, 2013, **2**, 553–578.

49 M. D. Bhatt and J. Y. Lee, *Energy Fuels*, 2020, **34**, 6634–6695.

50 L. V. Mattos and F. B. Noronha, *J. Catal.*, 2005, **233**, 453–463.

51 K. Jukk, N. Alexeyeva, P. Ritslaid, J. Kozlova, V. Sammelselg and K. Tammeveski, *Electrocatalysis*, 2013, **4**, 42–48.

52 Y. Nie, L. Li and Z. Wei, *Chem. Soc. Rev.*, 2015, **44**, 2168–2201.

53 N. Ramaswamy and S. Mukerjee, *Chem. Rev.*, 2019, **119**, 11945–11979.

54 E. H. Yu and K. Scott, *Electrochem. Commun.*, 2004, **6**, 361–365.

55 S. Gottesfeld, D. R. Dekel, M. Page, C. Bae, Y. Yan, P. Zelenay and Y. S. Kim, *J. Power Sources*, 2018, **375**, 170–184.

56 Y. Zhao, L. Zhan, J. Tian, S. Nie and Z. Ning, *Electrochim. Acta*, 2011, **56**, 1967–1972.

57 J. H. Kim, H. K. Kim, K. T. Hwang and J. Y. Lee, *Int. J. Hydrogen Energy*, 2010, **35**, 768–773.

58 R. R. Adzic, M. L. Avramovivic and A. V. Tripkovic, *Electrochim. Acta*, 1984, **29**, 1353–1357.

59 K. Miyazaki, N. Sugimura, K. Matsuoka, Y. Iriyama, T. Abe, M. Matsuoka and Z. Ogumi, *J. Power Sources*, 2008, **178**, 683–686.

60 R. Kannan, A. R. Kim and D. J. Yoo, *J. Appl. Electrochem.*, 2014, **44**, 893–902.

61 W. Wang, R. Li, R. Zhang, J. Ma and B. Wang, *J. Electroanal. Chem.*, 2015, **742**, 110–121.

62 Y. Liang, Y. Li, H. Wang, J. Zhou, J. Wang, T. Regier and H. Dai, *J. Am. Chem. Soc.*, 2012, **134**, 3517–3523.

63 M. Hamdani, R. N. Singh and P. Chartier, *Int. J. Electrochem. Sci.*, 2010, **5**, 556–577.

64 R. Awasthi and R. N. Singh, *Carbon*, 2013, **51**, 282–289.

65 Y. Wang, Z. M. Sheng, H. Yang, S. P. Jiang and C. M. Li, *Int. J. Hydrogen Energy*, 2010, **35**, 10087–10093.

66 A. Rabis, P. Rodriguez and T. J. Schmidt, *ACS Catal.*, 2012, **2**, 864–890.

67 A. Zuttel, A. Remhof, A. Borgschulte and O. Friedrichs, *Philos. Trans. R. Soc., A*, 2010, **368**, 3329–3342.

68 Y. J. Wang, D. P. Wilkinson and J. Zhang, *Chem. Rev.*, 2011, **111**, 7625–7651.

69 D. Banham and S. Ye, *ACS Energy Lett.*, 2017, **2**, 629–638.

70 Y. Hong, H. J. Kim, H. J. Lee, J. Kim and S.-I. Choi, *Front. Chem.*, 2019, **7**, 608.

71 A. M. I. N. Azam, S. H. Lee, M. S. Masdar, A. M. Zainoodin and S. K. Kamarudin, *Int. J. Hydrogen Energy*, 2019, **44**, 8566–8574.

72 T. Iwasita, Methanol and CO electrooxidation, in *Handbook of Fuel Cells-Fundamentals, Technology and Applications Handbook of Fuel Cells*, ed. Wea. Vielstich, 2003, p. 603.

73 M. Zeng, J. Wu, Z. Li, H. Wu, J. Wang, H. Wang, L. He and X. Yang, *ACS Sustainable Chem. Eng.*, 2019, **7**, 4777–4783.

74 A. N. Rollinson, J. Jones, V. Dupont and M. V. Twigg, *Energy Environ. Sci.*, 2011, **4**, 1216–1224.

75 J. Wang, B. Gong, W. Huang, Y. Wang and J. Zhou, *Bioresour. Technol.*, 2017, **228**, 31–38.

76 B. K. Boggs, R. L. King and G. G. Botte, *Chem. Commun.*, 2009, **32**, 4859–4861.

77 C. Lee, X. Wei, J. W. Kysar and J. Hone, *Science*, 2008, **321**, 385–388.

78 H. Yang, S. Kannappan, A. S. Pandian, J.-H. Jang, Y. S. Lee and W. Lu, 2013, arXiv preprint, arXiv:1311.1413.

79 K. I. Bolotin, K. J. Sikes, Z. Jiang, M. Klima, G. Fudenberg, J. Hone, P. Kim and H. L. Stormer, *Solid State Commun.*, 2008, **146**, 351–355.

80 D. S. Hecht, L. Hu and G. Irvin, *Adv. Mater.*, 2011, **23**, 1482–1513.

81 D. Higgins, P. Zamani, A. Yu and Z. Chen, *Energy Environ. Sci.*, 2016, **9**, 357–390.

82 A. Ali and P. K. Shen, *J. Mater. Chem. A*, 2019, **7**, 22189–22217.

83 S. Cui, S. Mao, G. Lu and J. Chen, *J. Phys. Chem. Lett.*, 2013, **4**, 2441–2454.

84 M. Lei, Z. B. Wang, J. S. Li, H. L. Tang, W. J. Liu and Y. G. Wang, *Sci. Rep.*, 2014, **4**, 1–6.

85 H. Huang, S. Yang, R. Vajtai, X. Wang and P. M. Ajayan, *Adv. Mater.*, 2014, **26**, 5160–5165.

86 C.-H. A. Tsang, K. Hui, K. Hui and L. Ren, *J. Mater. Chem. A*, 2014, **2**, 17986–17993.

87 M. Mansor, S. N. Timmiati, K. L. Lim, W. Y. Wong, S. K. Kamarudin and N. H. Nazirah Kamarudin, *Int. J. Photoenergy*, 2019, **44**, 14744–14769.

88 R. Baronia, J. Goel, S. Tiwari, P. Singh, D. Singh, S. P. Singh and S. K. Singhal, *Int. J. Hydrogen Energy*, 2017, **42**, 10238–10247.

89 J. C. Ng, C. Y. Tan, B. H. Ong, A. Matsuda, W. J. Basirun, W. K. Tan, R. Singh and B. K. Yap, *Mater. Res. Bull.*, 2019, **112**, 213–220.

90 R. Kiyani, S. Rowshanzamir and M. J. Parnian, *Energy*, 2016, **113**, 1162–1173.

91 G. V. Reddy, P. Raghavendra, P. S. Chandana and L. S. Sarma, *RSC Adv.*, 2015, **5**, 100522–100530.

92 Z.-S. Wu, W. Ren, L. Xu, F. Li and H.-M. Cheng, *ACS Nano*, 2011, **5**, 5463–5471.

93 Y. Zheng, Y. Jiao, L. Ge, M. Jaroniec and S. Z. Qiao, *Angew. Chem.*, 2013, **125**, 3192–3198.

94 T. Mori, H. Tanaka, A. Dalui, N. Mitoma, K. Suzuki, M. Matsumoto, N. Aggarwal, A. Patnaik, S. Acharya, L. K. Shrestha, H. Sakamoto, K. Itami and K. Ariga, *Angew. Chem.*, 2018, **130**, 9827–9831.

95 C. N. R. Rao, K. Gopalakrishnan and U. Maitra, *ACS Appl. Mater. Interfaces*, 2015, **7**, 7809–7832.

96 M. Z. Iqbal, A. U. Rehman and S. Siddique, *J. Energy Chem.*, 2019, **39**, 217–234.

97 M. Li, Q. Jiang, M. Yan, Y. Wei, J. Zong, J. Zhang, Y. Wu and H. Huang, *ACS Sustainable Chem. Eng.*, 2018, **6**, 6644–6653.

98 D. Rajesh, P. I. Neel, A. Pandurangan and C. Mahendiran, *Appl. Surf. Sci.*, 2018, **442**, 787–796.

99 X. X. Yuan, X. L. Ding, C. Y. Wang and Z. F. Ma, *Energy Environ. Sci.*, 2013, **6**, 1105–1124.

100 R. Kannan, A. R. Kim, K. S. Nahm, H.-K. Leed and D. J. Yoo, *Chem. Commun.*, 2014, **50**, 14623–14626.

101 T. R. Kumar, D. J. Yoo, A. R. Kim and G. G. Kumar, *New J. Chem.*, 2018, **42**, 14386–14393.

102 R. Kannan, C. D. Lim, A. R. Kim, M. H. Lee and D. J. Yoo, *J. Nanosci. Nanotechnol.*, 2019, **19**, 4520–4528.

103 M. Mansor, S. N. Timmiati, K. L. Lim, W. Y. Wong, S. K. Kamarudin and N. H. N. Kamarudin, *Int. J. Hydrogen Energy*, 2019, **44**, 14744–14769.

104 J. Liu, H. J. Choi and L. Y. Meng, *J. Ind. Eng. Chem.*, 2018, **64**, 1–15.

105 M. Liu, R. Zhang and W. Chen, *Chem. Rev.*, 2014, **114**, 5117–5160.

106 N. Seselj, C. Engelbrekt and J. Zhang, *Sci. Bull.*, 2015, **60**, 864–876.

107 N. Shaari and S. K. Kamarudin, *Renew. Sustain. Energy Rev.*, 2017, **69**, 862–870.

108 S. Hossain, A. M. Abdalla, S. B. H. Suhaili, I. Kamal, S. P. S. Shaikh, M. K. Dawood and A. K. Azad, *J. Energy Storage*, 2020, **29**, 101386.

109 M. Naguib and Y. Gogotsi, *Acc. Chem. Res.*, 2015, **48**, 128–135.

110 A. Feng, Y. Yu, Y. Wang, F. Jiang, Y. Yu, L. Mi and L. Song, *Mater. Des.*, 2017, **114**, 161–166.

111 M. W. Barsoum, *Prog. Solid State Chem.*, 2000, **28**, 201–281.

112 W. Yang, K. R. Ratinac, S. P. Ringer, P. Thordarson, J. J. Gooding and F. Braet, *Angew. Chem., Int. Ed.*, 2010, **49**, 2114–2138.

113 M. Naguib, O. Mashtalir, J. Carle, V. Presser, J. Lu, L. Hultman, Y. Gogotsi and M. W. Barsoum, *ACS Nano*, 2012, **6**, 1322–1331.

114 X. D. Zhang, J. G. Xu, H. Wang, J. J. Zhang, H. B. Yan, B. C. Pan, J. F. Zhou and Y. Xie, *Angew. Chem. Int. Ed.*, 2013, **52**, 4361–4365.

115 M. Alhabeb, K. Maleski, B. Anasori, P. Lelyukh, L. Clark, S. Sin and Y. Gogotsi, *Chem. Mater.*, 2017, **29**, 7633–7644.

116 N. K. Chaudhari, H. Jin, B. Kim, D. S. Baek, S. H. Joo and K. Lee, *J. Mater. Chem. A*, 2017, **5**, 24564–24579.

117 X. Zhao, M. Radovic and M. J. Green, *Chem*, 2020, **6**, 544–546.

118 J. Halim, M. R. Lukatskaya, K. M. Cook, J. Lu, C. R. Smith, L. A. Naslund, S. J. May, L. Hultman, Y. Gogotsi, P. Eklund and M. W. Barsoum, *Chem. Mater.*, 2014, **26**, 2374–2381.

119 M. Ghidiu, M. R. Lukatskaya, M.-Q. Zhao, Y. Gogotsi and M. W. Barsoum, *Nature*, 2014, **516**, 78–81.

120 O. Mashtalir, M. Naguib, V. N. Mochalin, Y. Dall' Agnese, M. Heon, M. W. Barsoum and Y. Gogotsi, *Nat. Commun.*, 2013, **4**, 1716.

121 M. W. Barsoum, The $M_{n+1}AX_n$ phases and their properties, in *Ceram. Sci. Technol*, Wiley-VCH Verlag GmbH & Co. KGaA, Weinheim, 2010, p. 299.

122 T. Ouisse and M. W. Barsoum, *Mater. Res. Lett.*, 2017, **5**, 365–378.

123 M. Naguib, V. N. Mochalin, M. W. Barsoum and Y. Gogotsi, *Adv. Mater.*, 2014, **26**, 992–1005.

124 B. Anasori, Y. Xie, M. Beidaghi, J. Lu, B. C. Hosler, L. Hultman, P. R. C. Kent, Y. Gogotsi and M. W. Barsoum, *ACS Nano*, 2015, **9**, 9507–9516.

125 B. Anasori, M. R. Lukatskaya and Y. Gogotsi, *Nat. Rev. Mater.*, 2017, **2**, 16098.

126 H. Wang, Y. Wu, X. Yuan, G. Zeng, J. Zhou, X. Wang and J. W. Chew, *Adv. Mater.*, 2018, **30**, 1704561.

127 Q. Jiang, N. Kurra, M. Alhabeb, Y. Gogotsi and H. N. Alshareef, *Adv. Energy Mater.*, 2018, **8**, 1703043.

128 J. Nan, X. Guo, J. Xiao, X. Li, W. Chen, W. Wu, H. Liu, Y. Wang, M. Wu and G. Wang, *Small*, 2019, 1902085.

129 Z. Hu, X. Kuai, J. Chen, P. Sun, Q. Zhang, H. H. Wu and L. Zhang, *ChemSusChem*, 2019, **12**, 1–7.

130 F. Shahzad, M. Alhabeb, C. B. Hatter, B. Anasori, H. S. Man, C. M. Koo and Y. Gogotsi, *Science*, 2016, **353**, 1137.

131 A. Sinha, Dhanjai, H. Zhao, Y. Huang, X. Lu, J. Chen and R. Jain, *Trends Anal. Chem.*, 2018, **105**, 424–435.

132 B. Xu, M. Zhu, W. Zhang, X. Zhen, Z. Pei, Q. Xue, C. Zhi and P. Shi, *Adv. Mater.*, 2016, **28**, 3333–3339.

133 X. Q. Li, C. Y. Wang, Y. Cao and G. X. Wang, *Chem.–Asian J.*, 2018, **13**, 2742–2757.

134 M. Soleymaniha, M. A. Shahbazi, A. R. Rafieerad, A. Maleki and A. Amiri, *Adv. Healthcare Mater.*, 2019, **8**, 26.

135 J. J. Zhu, P. Xiao, H. L. Li and S. A. C. Carabineiro, *ACS Appl. Mater. Interfaces*, 2014, **6**, 16449–16465.

136 A. Thomas, A. Fischer, F. Goettmann, M. Antonietti, J. O. Muller, R. Schlogl and J. M. Carlsson, *J. Mater. Chem.*, 2008, **18**, 4893–4908.

137 Y. Zheng, J. Liu, J. Liang, M. Jaroniec and S. Z. Qiao, *Energy Environ. Sci.*, 2012, **5**, 6717.

138 T. Sano, S. Tsutsui, K. Koike, T. Hirakawa, Y. Teramoto, N. Negishi and K. Takeuchi, *J. Mater. Chem. A*, 2013, **1**, 6489.

139 J. Zhang, J. Sun, K. Maeda, K. Domen, P. Liu, M. Antonietti, X. Z. Fu and X. C. Wang, *Energy Environ. Sci.*, 2011, **4**, 675.

140 Q. J. Xiang, J. G. Yu and M. Jaroniec, *J. Phys. Chem. C*, 2011, **115**, 7355.

141 Y. Ji, H. Dong, H. Lin, L. Zhang, T. Hou and Y. Li, *RSC Adv.*, 2016, **6**, 52377–52383.

142 G. Algara-Siller, N. Severin, S. Y. Chong, T. Bjçrkman, R. G. Palgrave, A. Laybourn, M. Antonietti, Y. Z. Khimyak, A. V. Krasheninnikov, J. P. Rabe, U. Kaiser, A. I. Cooper, A. Thomas and M. J. Bojdys, *Angew. Chem., Int. Ed.*, 2014, **53**, 7450–7455.

143 J. Liu, T. Zhang, Z. Wang, G. Dawson and W. Chen, *J. Mater. Chem.*, 2011, **21**, 14398–14401.

144 S. Cao, J. Low, J. Yu and M. Jaroniec, *Adv. Mater.*, 2015, **27**, 2150–2176.

145 J. S. Zhang, X. F. Chen, K. Takanabe, K. Maeda, K. Domen, J. D. Epping, X. Z. Fu, M. Antonietti and X. C. Wang, *Angew. Chem. Int. Ed.*, 2010, **49**, 441.

146 H. J. Yan, Y. Chen and S. M. Xu, *Int. J. Hydrogen Energy*, 2012, **37**, 125–133.

147 F. Dong, Y. J. Sun, L. W. Wu, M. Fu and Z. B. Wu, *Sci. Technol.*, 2012, **2**, 1332–1335.

148 D. Mitoraj and H. Kisch, *Chem.–Eur. J.*, 2010, **16**, 261–269.

149 T. Komatsu and T. Nakamura, *J. Mater. Chem.*, 2001, **11**, 474–478.

150 S. C. Yan, Z. S. Li and Z. G. Zou, *Langmuir*, 2009, **25**, 10397–10401.

151 D. R. Miller, J. J. Wang and E. G. Gillan, *J. Mater. Chem.*, 2002, **12**, 2463–2469.

152 X. Wang, S. Blechert and M. Antonietti, *ACS Catal.*, 2012, **2**, 1596–1606.

153 G. P. Dong, Y. H. Zhang, Q. W. Pan and J. R. Qiu, *J. Photochem. Photobiol., C*, 2014, **20**, 33–50.

154 X. F. Chen, J. S. Zhang, X. Z. Fu, M. Antonietti and X. C. Wang, *J. Am. Chem. Soc.*, 2009, **131**, 11658–11659.

155 X. C. Wang, X. F. Chen, A. Thomas, X. Z. Fu and M. Antonietti, *Adv. Mater.*, 2009, **21**, 1609–1612.

156 J. Wang, D. Hao, J. Ye and N. Umezawa, *Chem. Mater.*, 2017, **29**, 2694–2707.

157 J. Duan, S. Chen, M. Jaroniec and S. Z. Qiao, *ACS Nano*, 2015, **9**, 931–940.

158 H. Huang, S. Yang, R. Vajtai, X. Wang and P. M. Ajayan, *Adv. Mater.*, 2014, **26**, 5160–5165.

159 J. Tian, R. Ning, Q. Liu, A. M. Asiri, A. O. Al-Youbi and X. Sun, *ACS Appl. Mater. Interfaces*, 2014, **6**, 1011–1017.

160 J. Yuan, Q. Gao, X. Li, Y. Liu, Y. Fang, S. Yang, F. Peng and X. Zhou, *RSC Adv.*, 2014, **4**, 52332–52337.

161 I. S. Pieta, A. Rathi, P. Pieta, R. Nowakowski, M. Hołdynski, M. Pisarek, A. Kaminska, M. B. Gawande and R. Zboril, *Appl. Catal., B*, 2019, **244**, 272–283.

162 N. Mansor, T. S. Miller, I. Dedigama, A. B. Jorge, J. Jia, V. Brázdová, C. Mattevi, C. Gibbs, D. Hodgson, P. R. Shearing, C. A. Howard, F. Corà, M. Shaffer, D. J. L. Brett and P. F. McMillan, *Electrochim. Acta*, 2016, **222**, 44–57.

163 M. Huang, G. Dong, N. Wang, J. Xu and L. Guan, *Energy Environ. Sci.*, 2011, **4**, 4513–4516.

164 S. Zhang, S. Tsuzuki, K. Ueno, K. Dokko and M. Watanabe, *Angew. Chem.*, 2015, **127**, 1318–1322.

165 S. A. Shaik, A. Goswami, R. S. Varma and M. B. Gawande, *Curr. Opin. Green Sustain. Chem.*, 2019, **15**, 67–76.

166 Z. Jiang, W. Wan, H. Li, S. Yuan, H. Zhao and P. K. Wong, *Adv. Mater.*, 2018, **30**, 1706108.

167 M. Inagaki, T. Tsumura, T. Kinumoto and M. Toyoda, *Carbon*, 2019, **141**, 580–607.

168 H. S. Lee, S.-W. Min, Y.-G. Chang, M. K. Park, T. Nam, H. Kim, J. H. Kim, S. Ryu and S. Im, *Nano Lett.*, 2012, **12**, 3695–3700.

169 C. Zhong, C. Duan, F. Huang, H. Wu and Y. Cao, *Chem. Mater.*, 2011, **23**, 326–340.

170 J. Pu, Y. Yomogida, K.-K. Liu, L.-J. Li, Y. Iwasa and T. Takenobu, *Nano Lett.*, 2012, **12**, 4013–4017.

171 S. Wu, Z. Zeng, Q. He, Z. Wang, S. J. Wang, Y. Du, Z. Yin, X. Sun, W. Chen and H. Zhang, *Small*, 2012, **8**, 2264–2270.

172 Q. He, Z. Zeng, Z. Yin, H. Li, S. Wu, X. Huang and H. Zhang, *Small*, 2012, **8**, 2994–2999.

173 G. Du, Z. Guo, S. Wang, R. Zeng, Z. Chen and H. Liu, *Chem. Commun.*, 2010, **46**, 1106–1108.

174 Y. Luo, Y. Zhang, Y. Zhao, X. Fang, J. Ren, W. Weng, Y. Jiang, H. Sun, B. Wang, X. Cheng and H. Peng, *J. Mater. Chem. A*, 2015, **3**, 17553–17557.

175 M. H. Yang, J. M. Jeong, Y. S. Huh and B. J. Choi, *Compos. Sci. Technol.*, 2015, **121**, 123–128.

176 C. Zhai, M. Zhu, D. Bin, F. Ren, C. Wang, P. Yang and Y. Du, *J. Power Sources*, 2015, **275**, 483–488.

177 Z. Gao, M. Li, J. Wang, J. Zhu, X. Zhao, H. Huang, J. Zhang, Y. Wu, Y. Fu and X. Wang, *Carbon*, 2018, **139**, 369–377.

178 Q. H. Wang, K. Kalantar-Zadeh, A. Kis, J. N. Coleman and M. S. Strano, *Nat. Nanotechnol.*, 2012, **7**, 699–712.

179 R. J. Smith, P. J. King, M. Lotya, C. Wirtz, U. Khan, S. De, A. O'Neill, G. S. Duesberg, J. C. Grunlan, G. Moriarty, J. Chen, J. Wang, A. I. Minett, V. Nicolosi and J. N. Coleman, *Adv. Mater.*, 2011, **23**, 3944–3948.

180 L. F. Matthesis, *Phys. Rev. B: Solid State*, 1973, **8**, 3719–3740.

181 R. Lv, J. A. Robinson, R. E. Schaak, D. Sun, Y. Sun, T. E. Mallouk and M. Terrones, *Acc. Chem. Res.*, 2015, **48**, 56–64.

182 X. Li and H. Zhu, *J. Materiomics*, 2015, **1**, 33–44.

183 Y. Ding, Y. Wang, J. Ni, L. Shi, S. Shi and W. Tang, *Physica B*, 2011, **406**, 2254–2260.

184 Q. H. Wang, K. Kalantar-Zadeh, A. Kis, J. N. Coleman and M. S. Strano, *Nat. Nanotechnol.*, 2012, **7**, 699–712.

185 R. J. Toh, Z. Sofer, J. Luxa, D. Sedmidubsky and M. Pumera, *Chem. Commun.*, 2017, **53**, 3054–3057.

186 M. Chhowalla, H. S. Shin, G. Eda, L. J. Li, K. P. Loh and H. Zhang, *Nat. Chem.*, 2013, **5**, 263–275.

187 S. A. Han, R. Bhatia and S.-W. Kim, *Nano Convergence*, 2015, **2**, 17.

188 K. F. Mak, C. Lee, J. Hone, J. Shan and T. F. Heinz, *Phys. Rev. Lett.*, 2010, **105**, 136805.

189 Q. H. Wang, K. Kalantar-Zadeh, A. Kis, J. N. Coleman and M. S. Strano, *Nat. Nanotechnol.*, 2012, **7**, 699–712.

190 C. Lee, H. Yan, L. E. Brus, T. F. Heinz, J. Hone and S. Ryu, *ACS Nano*, 2010, **4**, 2695–2700.

191 A. Kuc, N. Zibouche and T. Heine, *Phys. Rev. B: Condens. Matter Mater. Phys.*, 2011, **84**, 245213.

192 C. Tsai, K. Chan, F. Abild-Pedersen and J. K. Norskov, *Phys. Chem. Chem. Phys.*, 2014, **16**, 13156–13164.

193 D. Y. Chung, S. K. Park, Y. H. Chung, S. H. Yu, D. H. Lim, N. Jung, H. C. Ham, H. Y. Park, Y. Piao, S. J. Yoo and Y. E. Sung, *Nanoscale*, 2014, **6**, 2131–2136.

194 D. Voiry, J. Yang and M. Chhowalla, *Adv. Mater.*, 2018, **28**, 6197–6206.

195 A. Ambrosi, Z. Sofer and M. Pumera, *Chem. Commun.*, 2015, **51**, 8450–8453.

196 R. F. Frindt, *J. Appl. Phys.*, 1966, **37**, 1928–1929.

197 H. R. Gutiérrez, N. Perea-López, A. L. Elías, A. Berkdemir, B. Wang, R. Lv, F. López-Urías, V. H. Crespi, H. Terrones and M. Terrones, *Nano Lett.*, 2013, **13**, 3447–3454.

198 J. Xie, H. Zhang, S. Li, R. Wang, X. Sun, M. Zhou, J. Zhou, X. W. Lou and Y. Xie, *Adv. Mater.*, 2013, **25**, 5807–5813.

199 A. L. Elias, N. Perea-Lopez, A. Castro-Beltran, A. Berkdemir, R. T. Lv, S. M. Feng, A. D. Long, T. Hayashi, Y. A. Kim, M. Endo, H. R. Gutierrez, N. R. Pradhan, L. Balicas, T. E. M. Houk, F. Lopez- Urias, H. Terrones and M. Terrones, *ACS Nano*, 2013, **7**, 5235–5242.

200 Z. Yin, Y. Zheng, H. Wang, J. Li, Q. Zhu, Y. Wang, N. Ma, G. Hu, B. He, A. Knop-Gericke, R. Schlog and D. Ma, *ACS Nano*, 2017, **11**, 12365–12377.

201 P. Manivasakan, P. Ramasamy and J. Kim, *Nanoscale*, 2014, **6**, 9665–9672.

202 H. S. Jadhav, S. M. Pawar, A. H. Jadhav, G. M. Thorat and J. G. Seo, *Sci. Rep.*, 2016, **6**, 31120.

203 F. Carraro, O. Vozniuk, L. Calvillo, L. Nodari, C. La Fontaine, F. Cavani and S. Agnoli, *J. Mater. Chem. A*, 2017, **5**, 20808–20817.

204 R. J. Lad, *Surface Structure of Crystalline Ceramics, Physical Structure*, 1996, pp. 185–228, DOI: 10.1016/s1573-4331(96)80010-2.

205 K. Kalantar-zadeh, J. Z. Ou, T. Daeneke, A. Mitchell, T. Sasaki and M. S. Fuhrer, *Appl. Mater. Today*, 2016, **5**, 73–89.

206 J. Mannhart and D. Schlom, *Science*, 2010, **327**, 1607–1611.

207 D. Chimene, D. L. Alge and A. K. Gaharwar, *Adv. Mater.*, 2015, **27**, 7261–7284.

208 M. C. Biesinger, B. P. Payne, A. P. Grosvenor, L. W. Lau, A. R. Gerson and R. S. C. Smart, *Appl. Surf. Sci.*, 2011, **257**, 2717–2730.

209 C. Wang, L. Yin, L. Zhang, D. Xiang and R. Gao, *Sensors*, 2010, **10**, 2088–2106.

210 K. Bhattacharya and P. Deb, *Dalton Trans.*, 2015, **44**, 9221–9229.

211 G. Rajeshkhanna, E. Umeshbabu and G. R. Rao, *J. Chem. Sci.*, 2017, **129**, 157–166.

212 R. van de Krol, Y. Liang and J. Schoonman, *J. Mater. Chem.*, 2008, **18**, 2311–2320.

213 J. Meyer, S. Hamwi, M. Kröger, W. Kowalsky, T. Riedl and A. Kahn, *Adv. Mater.*, 2012, **24**, 5408–5427.

214 K. Kalantar-zadeh, J. Z. Ou, T. Daeneke, A. Mitchell, T. Sasaki and M. S. Fuhrer, *Appl. Mater. Today*, 2016, **5**, 73–89.

215 V. Nicolosi, M. Chhowalla, M. G. Kanatzidis, M. S. Strano and J. N. Coleman, *Science*, 2013, **340**, 1226419.

216 K. Kalantar-zadeh, J. Z. Ou, T. Daeneke, A. Mitchell, T. Sasaki and M. S. Fuhrer, *Appl. Mater. Today*, 2016, **5**, 73–89.

217 W. Yang, X. Zhang and Y. Xie, *Nano Today*, 2016, **11**, 793–816.

218 K. W. Park, J. H. Choi, B. K. Kwon, S. A. Lee, Y. E. Sung, H. Y. Ha, S. A. Hong, H. Kim and A. Wieckowski, *J. Phys. Chem. B*, 2002, **106**, 1869–1877.

219 J. A. Farmer and C. T. Campbell, *Science*, 2010, **329**, 933–936.

220 P. Wang, H. Cui and C. Wang, *Nano Energy*, 2019, **66**, 104196.

221 Z. Lang, Z. Zhuang, S. Li, L. Xia, Y. Zhao, Y. Zhao, C. Han and L. Zhou, *ACS Appl. Mater. Interfaces*, 2020, **12**, 2400–2406.

222 Y. Wang, J. Wang, G. Han, C. Dua, Q. Deng, Y. Gao, G. Yin and Y. Song, *Ceram. Int.*, 2018, **45**, 2411–2417.

223 C. Yang, Q. Jiang, H. Huang, H. He, L. Yang and W. Li, *ACS Appl. Mater. Interfaces*, 2020, **12**, 23822–23830.

224 N. Abdullah, R. Saidur, A. M. Zainoodin and N. Aslfattahi, *J. Clean. Prod.*, 2020, **277**, 123395.

225 C. Yang, Q. Jiang, W. Li, H. He, L. Yang, Z. Lu and H. Huang, *Chem. Mater.*, 2019, **31**, 9277–9287.

226 P. Zhang, C. Fan, R. Wang, C. Xu, J. Cheng, L. Wang, Y. Lu and P. Luo, *Nanotechnology*, 2019, **31**, 09LT01.

227 C. Yang, H. He, Q. Jiang, X. Liu, S. P. Shah, H. Huang and W. Li, *Int. J. Hydrogen Energy*, 2021, **46**, 589–598.

228 Y. Sun, Y. Zhou, Y. Liu, Q. Wu, M. Zhu, H. Huang, Y. Liu, M. Shao and Z. Kang, *Nano Res.*, 2020, **13**, 2683–2690.

229 M. Kim, S. Hwang and J.-S. Yu, *J. Mater. Chem.*, 2007, **17**, 1656–1659.

230 N. Mansor, A. B. Jorge, F. Corà, C. Gibbs, R. Jervis, P. F. McMillan, X. Wang and D. J. L. Brett, *J. Phys. Chem. C*, 2014, **118**, 6831–6838.

231 Z. Li, R. Lin, Z. Liu, D. Li, H. Wang and Q. Li, *Electrochim. Acta*, 2016, **191**, 606–615.

232 A. Lewalska-Graczyk, P. Pieta, G. Garbarino, G. Busca, M. Holdynski, G. Kalisz, A. Sroka-Bartnicka, R. Nowakowski, M. Naushad, M. B. Gawande, R. Zbořil and I. S. Pieta, *ACS Sustainable Chem. Eng.*, 2020, **8**, 7244–7255.

233 C. Zhai, M. Sun, L. Zeng, M. Xue, J. Pan, Y. Du and M. Zhu, *Appl. Catal., B*, 2019, **243**, 283–293.

234 H. Wang, H. Feng and J. Li, *Small*, 2014, **10**, 2165–2181.

235 S. Su, C. Zhang, L. Yuwen, X. Liu, L. Wang, C. Fan and L. Wang, *Nanoscale*, 2016, **8**, 602–608.

236 L. Yuwen, F. Xu, B. Xue, Z. Luo, Q. Zhang, B. Bao, S. Su, L. Weng, W. Huang and L. Wang, *Nanoscale*, 2014, **6**, 5762–5769.

237 Z. Gao, M. Li, J. Wang, J. Zhu, X. Zhao, H. Huang, J. Zhang, Y. Wu, Y. Fu and X. Wang, *Carbon*, 2018, **139**, 369–377.

238 C. Zhai, M. Zhu, D. Bin, F. Ren, C. Wang, P. Yang and Y. Du, *J. Power Sources*, 2015, **275**, 483–488.

239 S. Ramakrishnan, M. Karuppannan, M. Vinothkannan, K. Ramachandran, O. J. Kwon and D. J. Yoo, *ACS Appl. Mater. Interfaces*, 2019, **11**, 12504–12515.

240 B. Tang, Y. Lin, Z. Xing, Y. Duan, S. Pan, Y. Dai, J. Yu and J. Zou, *Electrochim. Acta*, 2017, **246**, 517–527.

241 G. Rajeshkhanna and G. Ranga Rao, *Int. J. Hydrogen Energy*, 2018, **43**, 4706–4715.

242 S. K. Meher, P. Justin and G. Ranga Rao, *Nanoscale*, 2011, **3**, 683–692.

243 G. Rajeshkhanna, E. Umeshbabu and G. Ranga Rao, *J. Colloid Interface Sci.*, 2017, **487**, 20–30.

244 S. M. Pawara, B. S. Pawar, A. I. Inamdar, J. Kim, Y. Jo, S. Cho, S. S. Mali, C. K. Hong, J. Kwak, H. Kim and H. Im, *Mater. Lett.*, 2017, **187**, 60–63.

245 H. S. Jadhav, A. Roy, W. J. Chung and J. G. Seo, *New J. Chem.*, 2017, **41**, 15058–15063.