




## REVIEW

[View Article Online](#)  
[View Journal](#) | [View Issue](#)Cite this: *Mater. Adv.*, 2022,  
3, 888Recent progress in the development of  
electrocatalysts for the electrochemical  
N<sub>2</sub> reduction reactionKousik Bhunia, <sup>\*a</sup> Sanjeev Kumar Sharma, <sup>a</sup> Biraj Kanta Satpathy<sup>b</sup> and  
Debabrata Pradhan <sup>\*a</sup>

Ammonia is the second-most produced chemical throughout the world to maintain the global food supply and other chemical stocks. The annual worldwide ammonia production is currently more than 200 million tons through the Haber–Bosch process, which consumes an enormous amount of energy due to the requirement of high pressure (>10 MPa) and relatively high temperature (400–500 °C). In recent years, electrochemical N<sub>2</sub> reduction reaction (ENRR) under ambient conditions has received paramount attention in the scientific community. However, large-scale production of ammonia from the ENRR is limited by the lack of efficient cost-effective catalysts. The success of ENRR firmly depends on the efficiency of the electrocatalyst in a suitable electrolyte. However, identification and generation of the active sites in the electrocatalysts for ENRR remain elusive, impeding the development of the catalysts. In this review article, recent progress made in the development of efficient electrocatalysts for ENRR under ambient conditions is focused on with special attention on the physicochemical properties and active sites of the catalyst towards the NH<sub>3</sub> production rate by considering experimental as well as theoretical aspects. This review elaborates on key aspects for the development of an efficient and stable electrocatalyst for NH<sub>3</sub> production. In addition, the role of electrolytes and different sources of errors in the ENRR measurement for NH<sub>3</sub> production are outlined briefly.

Received 2nd August 2021,  
Accepted 18th November 2021

DOI: 10.1039/d1ma00680k

[rsc.li/materials-advances](https://rsc.li/materials-advances)

## 1. Introduction

Over the last few decades, the industrialization of populous developing countries has been demanding huge energy that primarily comes from fossil fuels leading to increased greenhouse gas emissions, not only resulting in depletion of non-renewable fossil fuel resources but also rapidly disturbing the climate. It has thus become an imperative objective of the scientific community to develop cleaner energy resources and technologies to mitigate fossil fuel use and maintain environmental sustainability. Ammonia (NH<sub>3</sub>) is the second-most manufactured synthetic chemical, which is extensively used as an agricultural fertilizer, chemical feedstock, and hydrogen carrier as well. For more than a century, the Haber–Bosch method has been the primary process of NH<sub>3</sub> production worldwide using nitrogen (N<sub>2</sub>) and hydrogen (H<sub>2</sub>) gas as precursors. The N<sub>2</sub> to NH<sub>3</sub> conversion is a multi-step complex

process, which requires a large amount of energy due to the high bond dissociation energy of the N≡N bond (940.95 kJ mol<sup>−1</sup>).<sup>1</sup> In particular, the Haber–Bosch process requires temperature and pressure in the range of 350–550 °C and 150–350 atm, respectively, to convert N<sub>2</sub> to NH<sub>3</sub> (N<sub>2</sub> + 3H<sub>2</sub> = 2NH<sub>3</sub>). Most importantly, the H<sub>2</sub> consumed for NH<sub>3</sub> production is exclusively produced from steam reforming of natural gas (CH<sub>4</sub> + 2H<sub>2</sub>O = 4H<sub>2</sub> + CO<sub>2</sub>), which emits around 450 million metric tons of CO<sub>2</sub> to the earth's atmosphere. Hence, it is one of the primary sources of environmental pollution and cause of rising global temperature. Therefore, an alternative energy-efficient and sustainable route for NH<sub>3</sub> production without hampering its supply chain is urgently required to protect our environment. The electrochemical nitrogen reduction reaction (ENRR) at ambient temperature and pressure is one such highly promising alternative method that requires only N<sub>2</sub> and H<sub>2</sub>O for NH<sub>3</sub> production, making the process completely green if solar/renewable energy is used. Hence, a great amount of effort has been directed toward ENRR research in the past couple of years indicating the prospects of this method.

In any chemical reaction, the catalyst plays a central role not only in increasing the yield and selectivity of the products but also in seamlessly driving the reaction with minimum inputs.

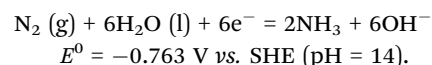
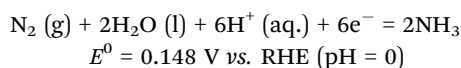
<sup>a</sup> Materials Science Centre, Indian Institute of Technology Kharagpur, Kharagpur 721302, West Bengal, India. E-mail: [kkousikmodabhunia@gmail.com](mailto:kkousikmodabhunia@gmail.com), [deb@matssc.iitkgp.ac.in](mailto:deb@matssc.iitkgp.ac.in)<sup>b</sup> School of Nanoscience and Technology, Indian Institute of Technology Kharagpur, Kharagpur 721302, West Bengal, India

Catalysts are thus the key and core ingredient for any electrocatalytic reaction. In heterogeneous catalysis, solid materials are majorly used as catalysts and thus their physicochemical properties have paramount importance to catalytic performance. The microstructure, especially steps, kinks, edge atoms, and surface electronic structures of the solid catalyst play significant roles in the efficiency and selectivity of the reaction. The literature reveals that a greater percentage of solid catalysts are noble and rare earth elements that have less abundance and are expensive. For those catalysts, support materials play an equally important role in reducing their amount for use in catalytic reactions while enhancing the overall performance. In particular, the support material controls the catalyst distribution and nucleation, and protects the nanostructure-based catalysts from agglomeration.

The morphology and composition of the catalysts play primary roles in the catalytic reactions including ENRR. The suitably designed surface controls the active sites for the adsorption/desorption of the reactive species while composition determines the surface oxidation state and electronic structure. Therefore, the design of efficient electrocatalysts is highly desirable for ENRR. Electrocatalysts for ENRR can be categorically placed in three groups: (i) metallic catalysts, (ii) metal-based catalysts including oxides, carbides, phosphides, and nitrides, and (iii) metal-free electrocatalysts. Understanding the reaction mechanism at these catalyst surfaces is important for developing and increasing their efficiency. For example, competitive hydrogen evolution reaction (HER) is an obstacle associated with ENRR, which leads to a decrease in its Faradaic efficiency (FE). The suppression of HER and the enhancement of the ENRR process are thus obvious fundamental objectives in the development of ENRR catalysts. So far, noble metal-based electrocatalysts such as Au,<sup>2</sup> Pd,<sup>3</sup> and Ru<sup>4</sup> have shown promising results towards ENRR. Similarly, non-noble metal-based electrocatalysts have also been explored. As compared to a sole electrocatalyst, a nanostructured electrocatalyst integrated with a suitable support material shows better activity.<sup>5</sup> The high electrocatalytic activity arises from the synergistic effect between the support and the catalyst, which mitigates the competitive HER. Therefore, the rational design of stable, active, and cost-effective catalysts to obtain a high yield rate and selectivity of NH<sub>3</sub> is the prime requirement for ENRR.

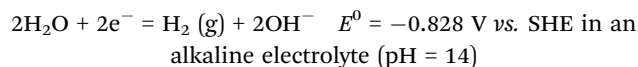
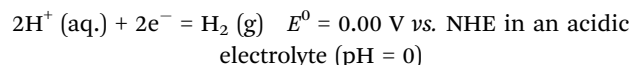
### 1.1 ENRR versus HER

To synthesize highly efficient ENRR electrocatalysts, it is important to understand the challenge associated with the ENRR kinetics at the catalyst surface. The electrochemical heterogeneous conversion process of N<sub>2</sub> to NH<sub>3</sub> at room temperature occurs *via* multiple proton-coupled electron transfer (PCET) reactions. In particular, electrochemical conversion requires six protons and six electrons for one N<sub>2</sub> molecule to produce NH<sub>3</sub> as per the following equations:<sup>6,7</sup>



Here, RHE and SHE stand for the reversible hydrogen electrode and the standard hydrogen electrode, respectively.

On the other hand, the competitive HER reaction requires only two electrons to produce one H<sub>2</sub> molecule. In addition, the potential required for HER is much closer (or lower than) that of the ENRR. Thus HER becomes a complementary reaction at the cathode for ENRR, which leads to poor selectivity towards NH<sub>3</sub> production. The HER at the cathode occurs as per the following equations:<sup>8</sup>



NHE stands for the normal hydrogen electrode. Both HER and ENRR thus fall into the same category of PCET reaction. Although many *in situ* techniques have been employed to understand the exact mechanism of ENRR, it remains unclear. Therefore, much more research endeavour is required to establish the ENRR reaction mechanism. Each PCET reaction step depicts its complexity and demands a higher potential for the progression of the reaction.

As ENRR proceeds *via* multiple electron and proton transfer processes, various intermediates are formed as presented in Fig. 1. Even though ENRR appears to be very favourable for NH<sub>3</sub> production as per the standard reduction potential chart, the achieved FE for ENRR remains mostly below 10%, which is far lower than the expected results. This is believed to be due to the kinetically preferred HER, which requires only two electrons whereas ENRR proceeds through a multi-step six electron process. This competing HER thus leads to a comprehensive FE loss for ENRR. The performance of ENRR further depends significantly on the electrolyte medium and its pH. Therefore, elimination of the unwanted HER from the electrolyte reduction becomes the most concerning issue for ENRR as it is difficult to avoid the protic medium. Furthermore, ENRR is highly affected by the mass transport of N<sub>2</sub>. The low solubility of N<sub>2</sub> in water, *i.e.*, only about 2 vol%, is another hurdle for ENRR. Therefore, the choice of electrolyte is another important factor to be considered in which ENRR should be preferred over HER.

### 1.2 ENRR mechanisms

ENRR over a heterogeneous catalyst follows two distinct pathways, named dissociative and associative pathways, with different intermediates and rate-limiting steps in terms of free energy.<sup>9–11</sup> According to the dissociative pathway (Fig. 1),<sup>11</sup> the adsorbed N<sub>2</sub> molecule undergoes dissociation at the catalyst surface followed by hydrogenation of the adsorbed N atom to form NH<sub>3</sub>. However, because of the high binding energy of the N≡N bond, the dissociative path requires more energy. On the other hand, the associative pathway is



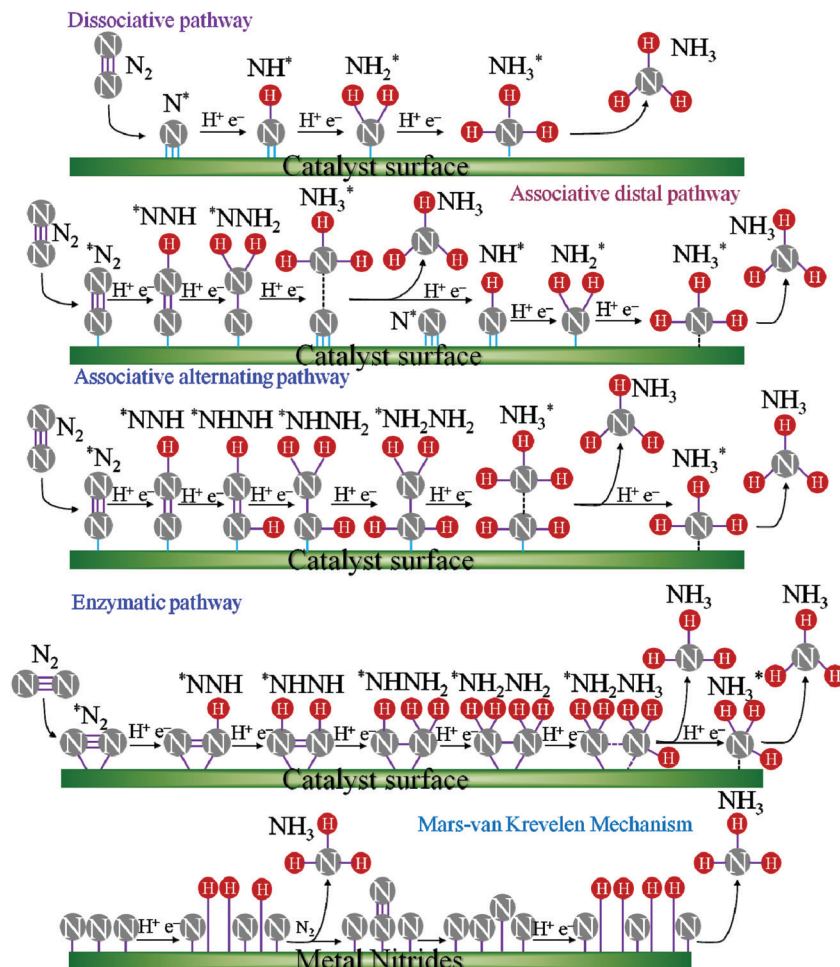


Fig. 1 The possible reaction mechanisms of ENRR. \* represents an adsorption site.

subdivided into two pathways: (i) associative distal pathway and (ii) associative alternating pathway. The ENRR mechanism usually follows the associative distal pathway or alternating pathway and/or both as shown in Fig. 1. The density functional theory (DFT) calculation reveals that the associative mechanism during the ENRR is governed by the specific active site of the catalyst.<sup>12</sup> The active site controls the adsorption of different active intermediate species during the progression of the reaction. In the distal pathway, the end atoms are attached to the active site, where the terminal atoms get hydrogenated by the PCET process through the formation of  $^*\text{NNH}$  and  $^*\text{NNH}_2$  intermediates, and then desorb from the catalyst surface as  $\text{NH}_3$ . In the alternating pathway, both the terminal and the end atoms are hydrogenated simultaneously by a PCET through the formation of  $^*\text{NNH}$ ,  $^*\text{NHNH}$ , and  $^*\text{NH}_2\text{NH}_2$  intermediates and desorb from the catalyst surface as an  $\text{NH}_3$  molecule consequently. Apart from that, in nature, nitrogenase enzymes perform biological  $\text{N}_2$  fixation under ambient conditions, where active sites have Fe and S along with Mo atoms, and the detailed mechanism of it remains elusive.<sup>13</sup> Nevertheless, both enzymatic and ENRR mechanisms require six protons and six electrons for the production of  $\text{NH}_3$ , which is the common

point in all the reaction mechanisms.<sup>13</sup> The ENRR mechanism was theoretically studied in an acid medium over transition metal surfaces by Nørskov and co-workers.<sup>14</sup> The free energy change for the  $\text{N}_{2\text{ads}}$  molecule and  $\text{N}_{\text{ads}}$  atoms towards catalytic  $\text{NH}_3$  conversion was calculated. Fig. 2 shows the volcano diagram of  $\text{N}_2$  reduction reaction considering a Heyrovsky-type reaction, which includes both dissociative (solid lines) and associative (dashed lines) mechanisms on both flat (black) and stepped (red) surfaces. The H-bonding effect is presented without (solid lines) and with (dotted lines). The DFT calculated negative free energy ( $-\Delta G$ ) values are presented with data points for a given reaction step. The right-hand side of the volcano plot represents the first proton transfer step, i.e.,  $\text{N}_{2(\text{g})} + \text{H}^+ + \text{e}^- \rightarrow ^*\text{N}_2\text{H}$ , indicating the activity of the metals for the associative mechanism whereas the  $\text{N}_2$  splitting is the rate-determining step for the dissociative mechanism. The metals on the left side have the same rate-determining steps for both the mechanisms (associative and dissociative). The x-axis represents the binding energy of N-adatoms. The large grey area inside the plot suggests the surface that is more favourable to be covered with H-adatoms. Mo, Fe, Rh, and Ru can be found at the top of the volcano plot suggesting their higher activity for



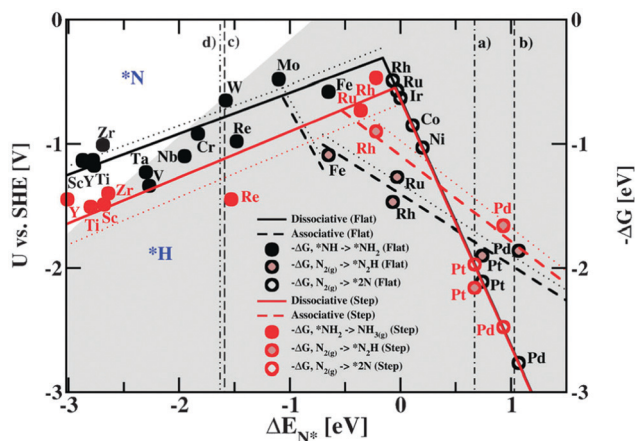


Fig. 2 Combined volcano diagrams (lines) for the flat (black) and stepped (red) transition metal surfaces for reduction of nitrogen with a Heyrovsky type reaction, without (solid lines) and with (dotted lines) the H-bond effect. Reproduced with permission from ref. 14. Copyright 2012, RSC.

ENRR. However, the surfaces of these catalysts are also predicted to be active sites for HER thereby leading to low FE for ENRR.

A completely different pathway named the Mars-van Krevelen (MvK) mechanism is proposed for transition metal nitride (TMN) catalysts which require relatively small overpotentials.<sup>15</sup> Different from the associative and dissociative pathways, here lattice N atoms are hydrogenated to produce  $\text{NH}_3$  from the surface of the TMNs and thus creating N vacancies. Subsequently, these N vacancies react with the dissolved  $\text{N}_2$  and generate a second  $\text{NH}_3$  molecule. Recently, Nash *et al.* experimentally proved the MvK mechanism over the  $\text{Cr}_2\text{N}$  catalyst.<sup>16</sup> Detailed bulk and surface analyses using XRD and XPS, respectively, reveal that the bulk of the catalyst is a pure  $\text{Cr}_2\text{N}$  phase whereas the surface possesses  $\text{CrN}$ ,  $\text{CrN}_x\text{O}_y$ , and  $\text{CrO}_x$  along with  $\text{Cr}_2\text{N}$ . The bulk  $\text{CrN}$  phase exhibits negligible ENRR activity compared with  $\text{Cr}_2\text{N}$  indicating that the latter is the active phase for ENRR. The isotopic batch cell study using  $^{15}\text{N}_2$  indicates the formation of  $^{14}\text{NH}_3$  and  $^{15}\text{NH}_3$  as identified from NMR analysis, which suggests active participation of surface N of  $\text{Cr}_2\text{N}$  to activate dinitrogen through the MvK mechanism as presented in Fig. 1. The authors also identified two possible reasons for the deactivation of the catalyst. Those are leaching of surface N from  $\text{Cr}_2\text{N}$  at lower potentials ( $< -0.4$  V) and silent conversion of the active  $\text{Cr}_2\text{N}$  to the inactive  $\text{CrN}$  at  $-0.2$  V. Using advanced instrumental tools such as surface-enhanced infrared absorption spectroscopy (SEIRAS) and differential electrochemical mass spectrometry (DEMS) Yao *et al.* studied ENRR on a Rh catalyst.<sup>17</sup> The authors identified the formation of  $\text{N}_2\text{H}_x$  ( $0 \leq x \leq 2$ ) species during the progression of ENRR with an  $\text{N}=\text{N}$  stretching mode at  $\sim 2020$   $\text{cm}^{-1}$  from SEIRAS analysis and the DEMS signal at  $m/z = 29$ . The study proposed a new two-step ENRR reaction pathway on the Rh surface, in which the ENRR involved two-electron transfer to  $\text{N}_2$  to form  $\text{N}_2\text{H}_2$  first and subsequent decomposition to  $\text{NH}_3$ .

### 1.3 Performance evaluation of electrocatalysts for NRR

The yield rate and Faradaic efficiency (FE) are the important indicators to define the catalytic conversion efficiency of an electrocatalyst. Therefore, it is important to describe the procedure for yield rate and FE calculation along with the factors that affect them. In an ideal condition, FE is supposed to be one or 100%. However, practically obtained FE for ENRR is much lower than the theoretical value. The Faradaic loss is a prominent issue, which is associated with the catalyst. Two major factors that strongly influence the FE of ENRR are applied potential and competitive HER. The ENRR at a lower potential leads to a higher FE. However, a higher reduction potential facilitates HER at the catalyst surface and thus loss of FE for ENRR. Another important point is the selectivity of ENRR. So far only two nitrogen-containing products are identified from ENRR, *i.e.*,  $\text{NH}_3$  and  $\text{N}_2\text{H}_4$ . The product selectivity of ENRR is another criterion to obtain high FE for  $\text{NH}_3$  conversion.

The yield rate is usually calculated from the salicylate method. The concentration of ammonia and hydrazine produced from ENRR is estimated from the calibration curve obtained from the UV-Vis absorption data. The ammonia yield rate is estimated by using the following equation:<sup>18</sup>

$$r[\text{NH}_3] = ([\text{NH}_3] \times V)/(t \times A)$$

where  $[\text{NH}_3]$  is the concentration ( $\mu\text{g mL}^{-1}$ ) of ammonia,  $V$  is the volume (mL) of the electrolyte,  $t$  is the electrolysis time (h), and  $A$  is the surface area ( $\text{cm}^2$ ) of the electrode.

The hydrazine yield is estimated from the following equation:

$$r[\text{N}_2\text{H}_4] = ([\text{N}_2\text{H}_4] \times V)/(t \times A)$$

where  $[\text{N}_2\text{H}_4]$  is the concentration ( $\mu\text{g mL}^{-1}$ ) of the produced hydrazine,  $V$  is the volume (mL) of the electrolyte,  $t$  is the electrolysis time (h), and  $A$  is the area ( $\text{cm}^2$ ) of the electrode.

Taking into account that three electrons are required for one ammonia molecule synthesis and four electrons for one  $\text{N}_2\text{H}_4$  from  $\text{N}_2$ , FE is calculated from the following equation:

$$\text{FE}_{\text{NH}_3} = (3 \times F \times [\text{NH}_3] \times 10^{-6} \times V)/(17 \times Q) + (4 \times F \times [\text{N}_2\text{H}_4] \times 10^{-6} \times V)/(32 \times Q)$$

where  $F$  is the Faraday constant,  $Q$  is the total charge, and other terms have their standard meaning.

## 2. Noble metal catalysts

### 2.1 Platinum (Pt)

Among the different noble metals, Pt and Pt-based materials are studied in almost every branch of catalyst science due to their high intrinsic conversion efficiency. Especially in fuel cell technology, Pt is considered as the benchmark catalyst due to its inherent HER activity, with HER being a competitive reaction for ENRR. As a result, Pt shows very poor FE towards ENRR as evident from the experimental results.<sup>19,20</sup> A few reports on Pt-based materials as electrocatalysts reveal their poor selectivity towards ENRR and very high activity towards HER.<sup>19</sup> For





example, Lan *et al.* studied ENRR using commercial Pt/C in a 0.5 M H<sub>2</sub>SO<sub>4</sub> electrolyte in a membrane electrode based assembly, where a mixed NH<sub>4</sub><sup>+</sup>/H<sup>+</sup> pre-exchanged Nafion membrane was used. The report shows a maximum NH<sub>3</sub> yield rate of  $1.14 \times 10^{-5} \text{ mol m}^{-2} \text{ s}^{-1}$  with a FE of  $\sim 0.52\%$  only at a cell voltage of 1.6 V.<sup>19</sup> Later on, Lan and Tao modified the experimental setup using a 0.1 M Li<sub>2</sub>SO<sub>4</sub> electrolyte with a mixed Li<sup>+</sup>/NH<sub>4</sub><sup>+</sup>/H<sup>+</sup> Nafion membrane and achieved an NH<sub>3</sub> yield rate of  $9.37 \times 10^{-6} \text{ mol m}^{-2} \text{ s}^{-1}$  with an improved FE of 0.83% at 80 °C temperature.<sup>20</sup>

## 2.2 Other noble metals (Rh and Ir)

Rhodium (Rh) and iridium (Ir) have been explored for ENRR. Like Pt, Ir is an important catalyst for the electrochemical water-splitting reaction. Ir has very limited performance towards ENRR due to its dominating HER activity over ENRR activity.<sup>21,22</sup> Recently, Sheet and Botte reported an Ir/C loaded gas-diffusion electrode as the cathode for ENRR and implemented it in a PEM-type electrochemical cell using a strong alkaline polymer-based gel electrolyte developed with a combination of polyacrylic acid and 6 M KOH. The best performance of Ir/C was achieved with an NH<sub>3</sub> yield of  $2.763 \times 10^{-11} \text{ mol cm}^{-2} \text{ s}^{-1}$  and a FE of 0.108% at 60 °C temperature and 0.25 V cell voltage.<sup>22</sup> Rh, another noble metal, has also been tested in the search for an efficient catalyst towards ENRR for NH<sub>3</sub> production.<sup>14,23</sup> Liu *et al.* reported a surfactant-free approach to synthesize atomic-level ultrathin two-dimensional Rh nanosheet (1 nm thick) nanoassemblies (Rh NNs) as an electrocatalyst for ENRR from the inorganic cyanogel polymer precursor RhCl<sub>3</sub>-K<sub>3</sub>Co(CN)<sub>6</sub>.<sup>24</sup> The Rh NNs exhibited an impressively high NH<sub>3</sub> yield rate of  $23.88 \mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$  in a 0.1 M KOH electrolyte at  $-0.2 \text{ V}$ . The as-synthesized electrocatalyst showed good selectivity (no hydrazine detected) and higher NH<sub>3</sub> yield rate compared to Rh nanoparticles

( $11.45 \mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$ ). However, the FE was found to be only 0.217% at  $-0.2 \text{ V}$  due to vigorous hydrogen generation. Chen *et al.* fabricated unusual 3D Rh particles with nanowires as the subunits using a reactive ionic liquid.<sup>25</sup> *n*-Octylammonium formate was used as a reaction medium, reducing agent, and template simultaneously for the successful construction of 3D Rh particles. Under ambient conditions, the as-prepared 3D Rh particles exhibited an excellent activity for ENRR with a high NH<sub>3</sub> yield of  $35.58 \mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$  at  $-0.2 \text{ V}$  and a FE of only 0.52% in 0.1 M KOH.

## 2.3 Gold (Au)

Au-based nanostructures are extensively explored in the field of nanoscience and nanotechnology.<sup>26</sup> Due to their specific electronic, optical, plasmonic, and catalytic properties, Au and Au-based materials are extensively studied in the field of biosensors, optoelectronics, and heterogeneous catalysis.<sup>26,27</sup> The intrinsic catalytic as well as the electronic properties of the catalyst can be manipulated by tuning the microstructure shape, size, and surrounding environment of the Au nanostructures.<sup>28,29</sup> The theoretical study revealed that the ENRR on the Au surface follows associative mechanisms that precede adsorption of the N<sub>2</sub> molecule at the electrode surface followed by hydrogenation of the N atoms. The success of the Au-based electrocatalysts towards ENRR is due to the strong N<sub>2</sub> adsorption ability of the Au surface composed of multifaceted facets with various steps and/or nanoclustering that facilitate the adsorption and reduction of N<sub>2</sub>.<sup>30,31</sup> Wang *et al.* synthesized flower-like Au nanostructures for ENRR with an NH<sub>3</sub> yield rate of  $25.57 \mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$  and a FE 6.05% at  $-0.2 \text{ V}$  (Table 1).<sup>32</sup> Zhang *et al.* correlated the coordination of the surface gold atoms with ENRR.<sup>33</sup> They found that the nanoporous Au film exhibits 5.8 times higher ENRR activity than the {111} facet exposed octahedral Au nanocrystal with an NH<sub>3</sub> production rate

**Table 1** ENRR performance of metal, bimetallic, and trimetallic alloy ENRR electrocatalysts

Catalyst	Electrolyte	Temperature	Yield rate ( $\mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$ )	FE (%)	Potentials vs. RHE (V)	Ref.
Au	LiClO <sub>4</sub>	20 °C	3.9 ( $\mu\text{g cm}^{-2} \text{ h}^{-1}$ )	30.2	−0.4	35
Au/Ni		Ambient	7.4	60	−0.14	42
Au	HCl	Ambient	25.57	6.05	−0.20	32
npPdH	0.1 M PBS	Ambient	20.4	43.6	−0.15	56
B	Na <sub>2</sub> SO <sub>4</sub>	Ambient	13.22	4.04	−0.80	81
Ru SA/N-C	H <sub>2</sub> SO <sub>4</sub>		120.9	29.6	−0.2	46
Rh	KOH	Ambient	23.88	0.217	−0.2	24
Mo	KOH	Room temp.	34.0	14.6	−0.3	82
Cu	HCl	Ambient	25.63	15.12	−0.40	83
Au <sub>1</sub> Cu <sub>1</sub>	H <sub>2</sub> SO <sub>4</sub>	Ambient	154.91	54.96	−0.2	84
Ag <sub>3</sub> Cu	Na <sub>2</sub> SO <sub>4</sub>	Ambient	24.59	13.28	−0.5	79
RhCu	KOH	Ambient	95.06	1.5	−0.2	85
Pt <sub>6</sub> Cu	Na <sub>2</sub> SO <sub>4</sub>	Ambient	16.5	6.15	−0.2	86
Pt <sub>3</sub> Fe	KOH	Ambient	18.3	7.3	−0.05	87
a-FeB <sub>2</sub>	LiClO <sub>4</sub>	Ambient	39.8 (−0.3 V)	16.7	−0.2	88
Rh <sub>2</sub> Sb	Na <sub>2</sub> SO <sub>4</sub>	Room temp.	228.85	1.54	−0.45	89
Pd	PBS	Ambient	4.5	8.2	0.1	53
Pd <sub>1</sub> Ag <sub>1</sub>	KOH	Ambient	24.1	$\sim 1.15$	−0.2	90
Pd <sub>3</sub> Cu <sub>1</sub>	KOH	Ambient	39.9	1.22	−0.25	78
PdCuIr	Na <sub>2</sub> SO <sub>4</sub>	Ambient	13.43	5.29	−0.30	91
Pd <sub>3</sub> Pb	Na <sub>2</sub> SO <sub>4</sub>	Ambient	18.2	21.46	−0.2	92
PdRu	HCl	Ambient	25.92	1.53	−0.1	93
PdRu	KOH	Ambient	37.23	1.85	−0.2	77



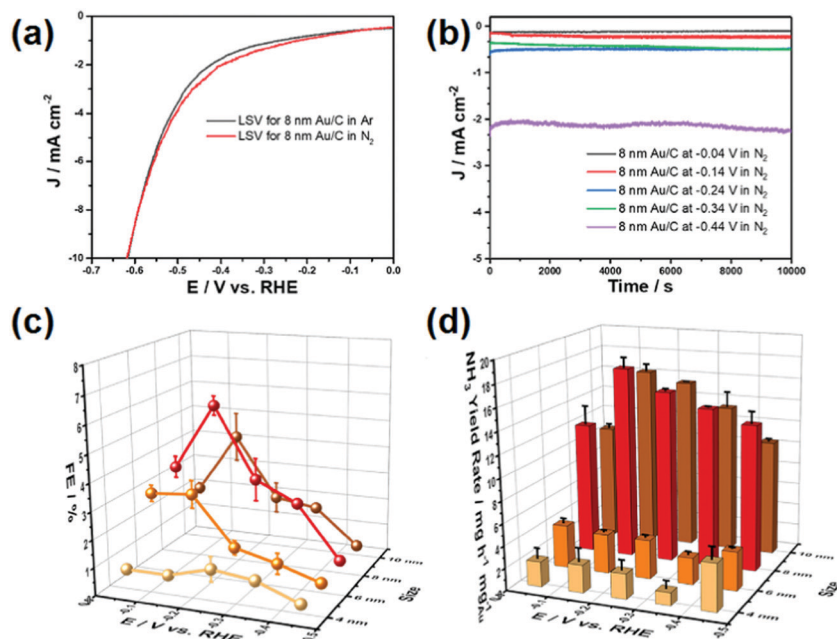


Fig. 3 (a) LSV curves of 8 nm Au/C. (b) Chronoamperometric curves of the 8 nm Au/C catalyst at different potentials. (c) Faradaic efficiency of the Au/C catalyst with different Au particle sizes. (d) Ammonia yield of the Au/C catalyst with different Au particle sizes. The error bar represents standard deviations of the results from three independent experiments. (Error bars in the figures represent standard deviations determined from three individual experiments.) Reproduced with permission from ref. 34. Copyright 2020, Elsevier.

of  $30.5 \mu\text{g h}^{-1} \text{mg}^{-1}$ . The higher ENRR activity of the nanoporous Au film was further theoretically confirmed by the binding energy of the intermediate species which depends on the coordination number of the surface atoms. Unlike Au (111) surface, the Au film favours the adsorption of the \*NNH intermediate species due to low coordination number Au atoms and thus facilitates the NH<sub>3</sub> production. Later on, Chen *et al.* reported a size-dependent ENRR rate over Au NPs.<sup>34</sup> Au NPs of 8 nm size among the as-synthesized Au NPs in the range of 4 nm to 10 nm showed the highest ENRR activity with FE and NH<sub>3</sub> production rate at 5.79% and  $17.49 \mu\text{g h}^{-1} \text{mg}_{\text{Au}}^{-1}$ , respectively (Fig. 3). The theoretical analysis revealed that the 8 nm size Au NPs have an optimum number of surface edge sites to suppress the HER and hence facilitate the ENRR. The rate-limiting step for NH<sub>3</sub> production was reported to be the formation of \*NNH from \*NN.<sup>34</sup> The free energy calculation revealed that Au(211) has the potential active site for ENRR.<sup>34</sup> The density of state of different Au models suggested that the 5d band of the Au(211) facet has a higher tendency to overlap with the 2p orbital of N<sub>ads</sub> in \*NNH than that of the Au(111) facet. Such stronger binding stabilizes the intermediate species and hence increases the NH<sub>3</sub> production rate.<sup>34</sup>

Nazemi *et al.* synthesized hollow Au nanocages to enhance ENRR under ambient conditions.<sup>35</sup> The hollow Au nanocages showed a FE of 30.2% at  $-0.4 \text{ V}$  (vs. RHE) with an NH<sub>3</sub> yield of  $3.9 \mu\text{g cm}^{-2} \text{h}^{-1}$  at  $-0.5 \text{ V}$  (Table 1). The FE increased from 30.2% to 40.5% with the temperature increasing from 20 °C to 50 °C at  $-0.4 \text{ V}$  indicating the role of temperature. The increase in FE with temperature is due to the high mass transportation rate at higher temperatures even though the solubility of N<sub>2</sub>

decreases. The hollow cages offer a large surface area for the reactant molecules than a solid one leading to three times more ENRR activity compared to the latter one. This suggests the urgency to develop an advanced microstructure for ENRR. In addition, a suitable support material for catalysts plays an important role. Support materials not only increase the stability of the catalyst but also facilitate adsorption and diffusion of the reactant molecules.<sup>36</sup> Qin *et al.* synthesized single Au atom supported hierarchical N-doped porous carbon to enhance ENRR. The N-doped porous carbon (NDPC) supported Au catalyst showed a FE of 12.3% with an NH<sub>3</sub> yield of  $2.32 \mu\text{g h}^{-1} \text{cm}^{-2}$  at  $-0.2 \text{ V}$ . Both the NDPCs and Au single-atom sites participated in ENRR under ambient conditions. The metal-free NDPCs reached a FE of only 2.1% at a potential of  $-0.6 \text{ V}$  further highlighting the significance of Au-NDPC heterojunction catalyst synthesis. The highly porous architecture of NDPCs provided more active sites and enhanced mass transportation during the ENRR process. The N and C sites stabilized the single atomic Au catalyst and retained the durability of the catalyst. The catalyst also selectively yielded NH<sub>3</sub> without the signature of N<sub>2</sub>H<sub>4</sub>. Li *et al.* reported amorphous Au NPs supported by the CeO<sub>x</sub>-RGO hybrid (a-Au/CeO<sub>x</sub>-RGO) for ENRR under ambient conditions.<sup>2</sup> Amorphous Au has higher chemical reactivity than the crystalline nanostructure towards small molecules. The a-Au/CeO<sub>x</sub>-RGO showed a FE of 10.10% with an NH<sub>3</sub> yield of  $8.3 \mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$  at  $-0.2 \text{ V}$ , which is much higher than its crystalline counterpart (c-Au/RGO, FE: 3.67%, NH<sub>3</sub> yield:  $3.5 \mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$ ). The role of CeO<sub>x</sub> was to increase the amorphous nature of Au NPs leading to increased catalyst performance. The surface oxidation state ( $\text{M}^{\delta+}$ ) of metal

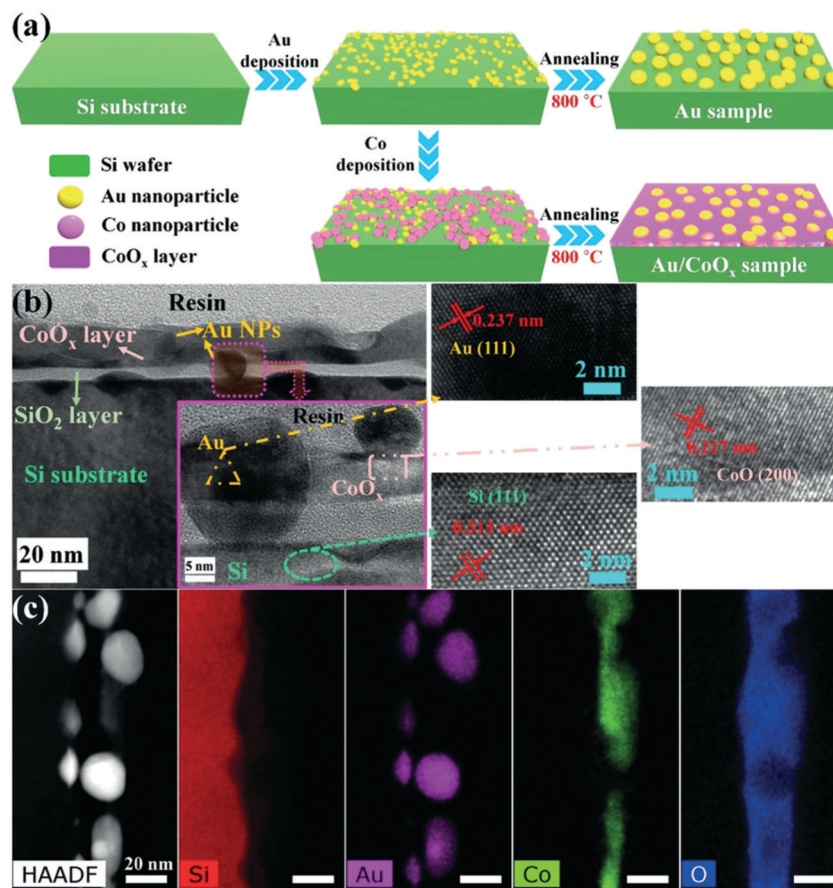


Fig. 4 Synthesis and structural characterization of Au-based samples. (a) Schematic of the vapour deposition and annealing to fabricate the Au-based samples. (b) Cross-sectional TEM and HRTEM images of the Au/CoO<sub>x</sub> sample. Inset: Magnified image of the specified area by HRTEM. High-magnification images on the right match the marked area in the inset. (c) STEM image with the corresponding elemental distribution maps for the Au/CoO<sub>x</sub> sample. Reproduced with permission from ref. 37. Copyright 2019, Wiley-VCH.

catalysts is another factor that plays a significant role in the electrochemical reaction by the redistribution of the surface electronic structure to enhance the adsorption ability of the catalyst towards reactant and radical species.<sup>37–39</sup> Zheng *et al.* introduced the CoO<sub>x</sub> layer to manipulate the local electronic structures of Au NPs with a positive valence site (Au<sup>+</sup>) to enhance the NH<sub>3</sub> production rate.<sup>37</sup> By using the vapour deposition method, small-sized Au and Co islands were homogeneously deposited onto the Si surface, followed by fast annealing at 800 °C forming a Au NPs/CoO<sub>x</sub> layer (Au/CoO<sub>x</sub>) (Fig. 4a). The CoO<sub>x</sub> layer created Au<sup>+</sup> active sites due to the strong charge exchange between them.<sup>40</sup> High-resolution transmission electron microscopy (HRTEM) images (Fig. 4b) indicated that the Au NPs had penetrated into the CoO<sub>x</sub> layer on the Si substrate. The cross-section analysis of the Au/CoO<sub>x</sub> sample (Fig. 4c) using scanning transmission electron microscopy (STEM) coupled with EDS mapping revealed the intimate contact between Au and CoO<sub>x</sub>. Elemental mapping showed the thin CoO<sub>x</sub> layer surrounding the bottom of the Au NPs while the top portion of the Au NPs was directly exposed to the external environment. Quasi *in situ* XPS after 10 h electrolysis showed a positive chemical shift of about 0.4 and 0.2 eV compared to the

original Au/CoO<sub>x</sub> sample. The down-field shift of the f-band centre of Au suggests the hybridized band formation through a strong electronic effect by Au NPs within an atomic dimension during ENRR.<sup>41</sup> The as-synthesized catalyst with the highest average oxidation state (*ca.* 40%) achieved an NH<sub>3</sub> yield of 15.1 μg cm<sup>−2</sup> h<sup>−1</sup> and a FE of 19% at −0.5 V. On the other hand, the Au catalyst showed much lower NH<sub>3</sub> yield and FE in the range of 2.0–6.1 μg cm<sup>−2</sup> h<sup>−1</sup> and 0.4–5.4%, respectively, in the potential range of −0.3 to −0.7 V.

Unlike the Au NP and oxide combination, Xue *et al.* reported the Ni and Au NP combination by a galvanic replacement method where Au was deposited over Ni for ENRR.<sup>42</sup> The atomic ratio of the Au–Ni catalyst was tuned by controlling the Au<sup>3+</sup> precursor concentration. The pristine Ni catalyst produced a negligible amount of NH<sub>3</sub>. The NH<sub>3</sub> yield rate significantly increased after the incorporation of Au. The highest NH<sub>3</sub> yield of 7.4 μg h<sup>−1</sup> mg<sub>cat</sub><sup>−1</sup> and FE of 67.8% at −0.14 V were obtained with Au<sub>6</sub>/Ni. In this metallic couple, Ni acts as an electron donor and enriches the Au surface electron density by a combination of support and size effects. XPS analysis provided clear evidence for the gradual shift of the Au 4f spectra towards lower energy binding, whereas Ni 2p shifted towards



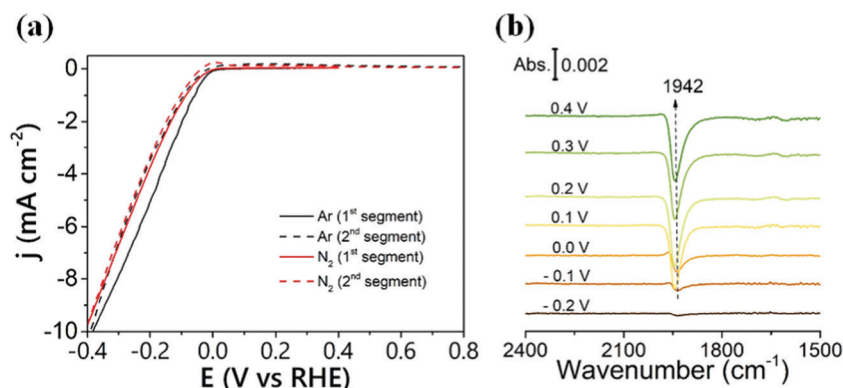
higher binding energy confirming the acceptor behaviour of the former. Moreover, the optimal Ni–Au donor–acceptor pair enhanced the pre-adsorption and activation of  $N_2$  and the desorption of  $NH_3$  from the catalyst surface.

## 2.4 Ruthenium (Ru)

Ruthenium (Ru), known for its use in the Haber–Bosch process, is another example of an efficient catalyst for ENRR.<sup>43</sup> The theoretical analysis revealed favourable nitrogen adsorption energy leading to a lower ENRR overpotential in both associative and dissociative mechanisms compared to that of Pt and Pd electrocatalysts.<sup>14</sup> Moreover, Ru is placed almost at the top of the volcano plot (Fig. 2) suggesting it to be one of the most active catalysts for ENRR. Thus, Ru-based nanostructured catalysts have been explored in recent years for ENRR. The fundamental role of the Ru catalyst towards the ENRR mechanism is highlighted here based on experimental and theoretical findings. Back *et al.* studied the mechanism of ENRR through both associative and dissociative pathways and compared with the energy state of Ru theoretically.<sup>44</sup> The calculated free energy diagram revealed that the kinetically facile intermediate of the dissociative pathway required a thermodynamic limiting potential of  $-0.71$  V, which is comparable to the associative pathway ( $-0.68$  V). The study highlighted that both associative and dissociative reaction pathways are probable during the ENRR. Previously, it was believed that the associative pathway is energetically more feasible than the dissociative pathway because of the high energy requirement to dissociate the  $N\equiv N$  bond ( $9.79$  eV).<sup>45</sup> In addition,  $NH_3$  formation is energetically more favourable than  $N_2H_4$  formation making Ru nanostructures more selective for  $NH_3$  synthesis. However, the competitive HER prohibits the ENRR by blocking the active sites due to the energetically preferential adsorption of  $*H$ .<sup>14</sup> Geng *et al.* developed Ru single atoms on nitrogen-doped carbon (Ru SAs/N–C), which showed very high activity toward ENRR.<sup>46</sup> At  $-0.2$  V, Ru SAs/N–C attained a FE of 29.6% with a partial current density of  $-0.13$  mA  $cm^{-2}$  and a yield rate of  $120.9$   $\mu g_{NH_3}$   $mg_{cat}^{-1}$   $h^{-1}$ . The high electrocatalytic activity of

Ru SAs/N–C arises from the strong chemical bond between Ru and  $N_2$  as confirmed by the  $N_2$ -temperature program desorption analysis. Zhang *et al.* demonstrated the synthesis of Ru dispersed N-doped carbon by the carbonization of Ru dispersed ZIF-8. The catalyst showed a maximum  $NH_3$  yield rate at about  $16.68$   $\mu g_{NH_3}$   $h^{-1}$   $mg_{cat}^{-1}$  at  $-0.4$  V and a FE of 14.23% at  $-0.3$  V for the 16 wt% Ru loaded catalyst.<sup>47</sup> The N-doped carbon frameworks not only ensured uniform dispersion of the Ru NPs but also protected the catalyst from dissolution during electrocatalysis. The residual hydrophobic nature of ZIF-8 remained in the carbon matrix which prohibited competitive HER. Furthermore, among the different N-doped carbons, the pyridinic N-type carbon moiety facilitated the adsorption of  $N_2$  in which Ru atoms accelerated dissociation.

Yao *et al.* studied the ENRR kinetics on a Ru thin film using a combination of surface-enhanced infrared absorption spectroscopy and electrochemical measurements.<sup>48</sup> Fig. 5a shows the voltammetry plots of the Ru thin film performed in a  $N_2$  and Ar-saturated  $HClO_4$  electrolyte. The cathodic scan reveals the onset of NRR and HER at 0 V and an increase in reduction current with decreasing potential. It is worth noting that the NRR current (solid red line) is slightly lower than the HER current (solid black line), suggesting that some active species adsorbed on the Ru surface get oxidized in the backward scan and thus showing a small peak between  $-0.1$  and 0 V. To identify the probable intermediate, surface-enhanced infrared absorption spectroscopy was used during the ENRR measurements. The  $*N_2H_x$  ( $0 \leq x \leq 2$ ) species was identified and the stability of the species was further studied. The  $*N_2H_x$  species was detected at a potential below 0.2 V in an  $N_2$  saturated  $HClO_4$  solution (Fig. 5b). The  $N=N$  stretching band at  $1940$   $cm^{-1}$  was observed at  $-0.1$  V and remained constant above 0.1 V. The  $N=N$  stretching band intensity was accompanied by the oxidation current in between the potential of  $-0.1$  and 0 V during the positive scan (Fig. 5a). The oxidation current is believed to arise from the electrochemical oxidation of the  $*N_2H_x$  species. The results (Fig. 5a and b) reveal that the oxidation current (dashed line) below 0 V potential arises from



**Fig. 5** (a) Cyclic voltammograms of a Ru film electrode deposited on the Si prism in Ar- (black line) and  $N_2$ -saturated (red line) 0.1 M  $HClO_4$  aqueous solutions. An Ag/AgCl electrode was used as the reference. Potential scan rate:  $2.5$   $mV$   $s^{-1}$ . (b) FTIR spectra recorded during the potential scan from  $-0.2$  to  $0.4$  V on the Ru film electrode in an  $N_2$ -saturated 0.1 M  $HClO_4$  solution. The reference spectrum was taken at  $-0.4$  V. Reproduced with the permission of ref. 48. Copyright 2019 ACS.



the oxidation of the  $*\text{N}_2\text{H}_x$  species whereas in the potential range of 0 and 0.4 V, the oxidation of  $*\text{N}_2\text{H}_x$  and  $\text{H}_{\text{ads}}$  surface species occurred. They also studied the ENRR kinetics in alkaline electrolytes and revealed that the N-related signal at the electrode surface is very weak in an alkaline medium. This observation highlights the feasibility of the Ru-based catalyst in an alkaline medium. Recently, Ru NP loaded  $\text{Ti}_3\text{C}_2$  MXene ( $\text{Ru@MXene}$ ) was tested for ENRR which showed an  $\text{NH}_3$  yield of  $2.3 \mu\text{mol h}^{-1} \text{cm}^{-2}$  at  $-0.4$  V with a FE of 13.13%.<sup>49</sup>

## 2.5 Palladium (Pd)

The Pd-based materials are widely explored as electrocatalysts in the field of the fuel cell, especially for ORR,<sup>50</sup> OER,<sup>51</sup> and HER,<sup>52</sup> as well as anode catalysts for alcohol electrooxidation reaction. Pd has thus been studied as an electrocatalyst for ENRR. Wang *et al.* reported carbon-supported Pd NPs (Pd/C) for ENRR under ambient conditions.<sup>53</sup> Under a potential, Pd can form Pd hydride, which promotes the surface hydrogenation reaction. The Pd/C catalyst showed an  $\text{NH}_3$  yield rate of around  $4.5 \mu\text{g mg}_{\text{Pd}}^{-1} \text{h}^{-1}$  and a high FE of 8.2% at 0.1 V. The Pd/C catalyst showed higher catalytic activity than Pt/C and Au/C with similar wt% mass loading. Interestingly, the HER activity of Pd was effectively suppressed in the neutral PBS electrolyte and  $\text{N}_2$  hydrogenation followed the Grotthuss-like hydride transfer mechanism. Free energy calculation suggested that the  $*\text{N}_2$  to  $*\text{N}_2\text{H}$  hydrogenation is the rate-limiting step for ENRR. Lv *et al.* reported a PdO/Pd heterojunction for ENRR.<sup>54</sup> The desired compositions of PdO/Pd decorated carbon nanotubes (PdO/Pd/CNTs) were synthesized through laser irradiation of PdO/CNTs in distilled water. The optimized PdO (82%)–Pd (18%) interface provided maximum active sites for  $\text{N}_2$  activation and proton transportation. In PdO/Pd/CNTs, both Pd and PdO sites were exposed for electrocatalysis where the Pd site strongly bound the  $\text{N}_2$  molecule while the PdO site facilitates the subsurface activated H protons to imitate  $\alpha$ -PdH and hydrogenate the adsorbed  $\text{N}_2$  molecule. The synergy of Pd and PdO contributed to the efficiency of the catalyst. They further studied defect-engineered titanium dioxide and the interfacial effect of supported palladium or platinum for ENRR, which demonstrated  $1847.3 \mu\text{g mg}_{\text{cat.}}^{-1} \text{h}^{-1}$  (Pd/ $\text{TiO}_2$ ) and  $2520.5 \mu\text{g mg}_{\text{cat.}}^{-1} \text{h}^{-1}$  (Pt/ $\text{TiO}_2$ ) yield at potential  $-0.1$  V, respectively.<sup>55</sup> Interestingly, the FE for NRR was higher on Pd/ $\text{TiO}_2$  (2.63%) as compared to Pt/ $\text{TiO}_2$  (1.57%). Xu *et al.* reported nanoporous palladium hydride (np-PdH) as an electrocatalyst for ENRR under ambient conditions, which showed a high  $\text{NH}_3$  yield rate of  $20.4 \mu\text{g h}^{-1} \text{mg}^{-1}$  with a FE of 43.6% at a low overpotential of  $-150$  mV.<sup>56</sup> Isotopic hydrogen labelling studies suggested that the lattice hydrogen atoms present in the np-PdH acted as the active hydrogen source. *In situ* Raman analysis and DFT calculations further revealed that the  $*\text{N}_2$  to  $*\text{N}_2\text{H}$  reduction energy barrier is the rate-limiting step of ENRR. The unique protonation nature of the np-PdH could provide a new dimension for designing efficient and robust electrocatalysts. To study the ENRR mechanism, the authors studied the isotopic labelling experiments on np-PdH<sub>0.43</sub>, as presented in Fig. 6. In the presence of  $^{15}\text{N}_2$ , two peaks with a coupling

constant of 73.2 Hz were detected in the baseline-subtracted  $^1\text{H}$  NMR spectra (Fig. 6b), which is consistent with a heteronuclear coupling constant between  $^1\text{H}$  and  $^{15}\text{N}$  of  $^{15}\text{NH}_4^+$ . The FTIR band at  $1439 \text{ cm}^{-1}$  corresponds to the N–H bending, which further provides evidence for  $\text{NH}_3$  generation. Three weak FTIR bands that appeared at 1177, 1241, and  $1325 \text{ cm}^{-1}$  were ascribed to the bending modes of  $\text{NH}_2\text{D}_2^+$  and  $\text{NH}_3\text{D}^+$  (Fig. 6c). XRD data suggest that there is no shift in the characteristic (111) peak at different potentials which underlines the structural durability of the catalyst. *In situ* Raman spectra of np-PdH<sub>0.43</sub> indicate a broad peak at  $1644.4 \text{ cm}^{-1}$  that relates to the overlapping of H–N–H/H–O–H bending and the peak intensity increase with potential indicates the adsorption of ammonia on the catalyst surface (Fig. 6d and e). Recently, Wang *et al.* achieved a record-high FE of up to 97% for ENRR in aqueous solution using a Pd/activated carbon cloth.<sup>57</sup> The high electrocatalytic activity is demonstrated by adjusting the three-phase interface, *i.e.*, gas/solid catalyst/liquid electrolyte, which favours ENRR over HER. The complete suppression of HER is facilitated by the three-interface contact due to high  $\text{N}_2$  coverage on the catalyst surface that weakens H adsorption as evidenced by the DFT calculations and experimental results. The authors further confirm the merits of a three-phase interface strategy for selective electrochemical reduction of  $\text{N}_2$  to  $\text{NH}_3$  using Ir- and RuPd-based catalysts, which are known to have strong H adsorption ability.

## 2.6 3d- and 4d-transition metal catalysts

Even though noble metals such as Au, Pd, and Ru show promising electrocatalytic activity towards ENRR, the scarcity and cost-ineffectiveness associated with these prompt the researchers to explore alternate materials without compromising the performance. In recent years, a variety of noble metal-free transition metal electrocatalysts have been studied for ORR,<sup>58</sup> OER,<sup>59</sup> and HER.<sup>60</sup> These were also extensively employed for ENRR. Transition metals are largely abundant in the mother earth and inexpensive, making them suitable alternatives to noble metal-based catalysts. Mukherjee *et al.* reported an atomically dispersed Ni site on N-doped carbon ( $\text{Ni-N}_x\text{-C}$ ), which exhibited an optimal  $\text{NH}_3$  yield of  $115 \mu\text{g cm}^{-2} \text{h}^{-1}$  at  $-0.8$  V in a neutral medium.<sup>61</sup> The as-prepared  $\text{Ni-N}_x\text{-C}$  catalyst showed a FE of  $21 \pm 1.9\%$  at  $-0.2$  V under alkaline conditions although the  $\text{NH}_3$  yield was lower. The atomically dispersed Ni sites were stabilized with nitrogen in the carbon matrix. The active site and probable reaction pathways through the DFT calculations reveal that the  $\text{Ni-N}_3$  sites are responsible for the experimentally observed catalytic activity and selectivity. The  $\text{N}_2$  molecule adsorbs on the top of the central Ni atom in an end-on configuration (Fig. 7) in which one N atom is chelated with Ni by a bond length of  $1.76 \text{ \AA}$ , whereas another one is tilted along with a Ni–N bond of the  $\text{Ni-N}_3$  site. The proximal N of the adsorbed  $\text{N}_2$  undergoes two hydrogenation steps to form  $*\text{NHNH}_2$  and  $*\text{NH}_2\text{NH}_2$ . The  $\text{N}\equiv\text{N}$  bond length in  $*\text{NH}_2\text{NH}_2$  is increased about 28% than that of the  $\text{N}_2$  gas molecule. Therefore, subsequent hydrogenation on the distal N is believed to break the  $\text{N}\equiv\text{N}$  bond and release one  $\text{NH}_3$ .



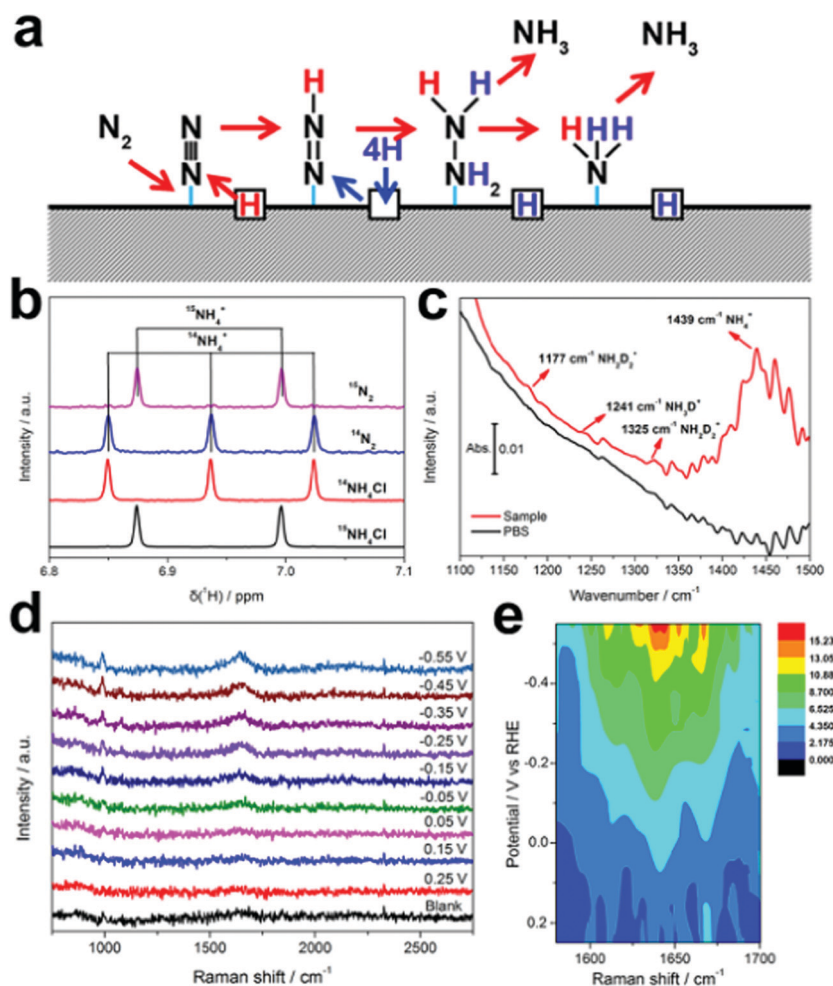


Fig. 6 (a) Proposed lattice hydrogen-involved reaction pathway for nitrogen reduction on palladium hydride. (b) Baseline-subtracted  $^1H$  NMR spectra of the post-electrolyte with  $^{15}N_2$  and  $^{14}N_2$  and the reference  $^{14}NH_4Cl$  and  $^{15}NH_4Cl$ . (c) FTIR spectra of the post-electrolyte with a deuterium substituted catalyst. (d) *In situ* Raman spectra and (e) the corresponding contour plots of np-PdH<sub>0.43</sub> at various potentials in a  $N_2$ -saturated electrolyte. Reproduced with permission from ref. 56. Copyright 2020, Wiley-VCH.

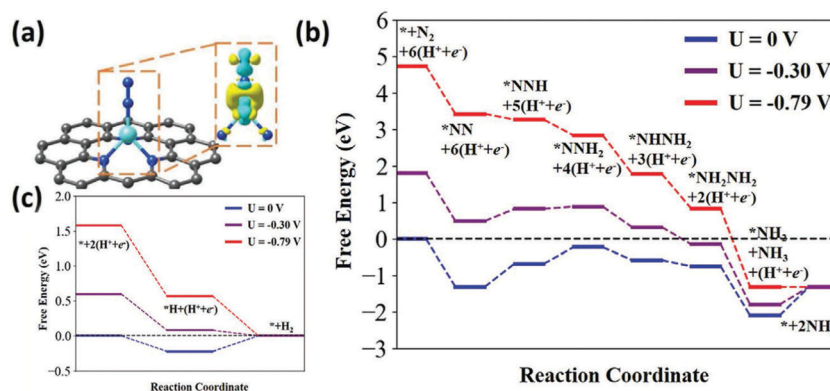


Fig. 7 (a) Atomistic structure and charge distribution of  $N_2$  adsorption on the Ni-N<sub>3</sub> active site. In this figure the cyan and yellow clouds show the charge depletion and accumulation; the gray, blue, cyan and white balls represent the C, N, Ni, and H atoms, respectively. The isosurface was set to be  $0.006 e \text{ \AA}^{-3}$ . (b) Predicted energy evolution of ENRR on a Ni-N<sub>3</sub> site under an applied potential of 0, -0.3, and -0.79 V versus RHE and (c) calculated free energy evolution for HER on the Ni-N<sub>3</sub> active site at 0, -0.3, and -0.79 V versus RHE. Reproduced with permission from ref. 61. Copyright 2020, Wiley-VCH.

Zang *et al.* reported on a single copper atom attached porous N-doped carbon network (NC-Cu SA) for ENRR by the combination of experimental and theoretical calculation.<sup>62</sup> The single-atom copper site exhibits high-density active sites

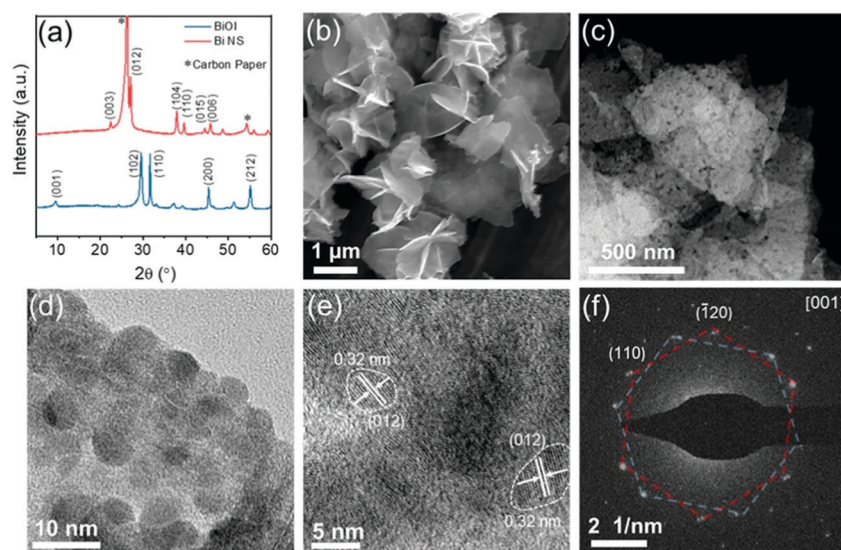
and the porosity of the catalyst leads to an  $\text{NH}_3$  yield rate of  $\sim 53.3 \mu\text{g}(\text{NH}_3) \text{ h}^{-1} \text{ mg}_{\text{cat}}^{-1}$  with a FE of 13.8% in 0.1 M KOH, and these were decreased to  $\sim 49.3 \mu\text{g}(\text{NH}_3) \text{ h}^{-1} \text{ mg}_{\text{cat}}^{-1}$  and 11.7% in the acidic medium (0.1 M HCl). The  $\text{N}_2$  temperature-programmed desorption ( $\text{N}_2$ -TPD) on NC-Cu SAC indicates a stronger desorption peak at higher temperature due to its higher binding energy for  $\text{N}_2$  and ability towards  $\text{N}_2$  fixation. The theoretical study revealed that the Cu- $\text{N}_2$  sites are more active than any Cu- $\text{N}_4/\text{N}_3$  site energetically. The Gibbs free energy change for carbon vacant and two N atoms connected Cu is favourable. To improve the electrocatalytic activity of Cu NPs towards ENRR, Lin *et al.* reported electron-deficient Cu nanocrystals for ENRR.<sup>63</sup> The Cu nanocrystals were interfaced with polyimide (Cu/PI). This strategy was found to be very efficient in boosting the ENRR activity of Cu nanocrystals by nurturing the electron density over the Cu nanocrystals and simultaneously suppressing the HER activity. Cu/PI showed a high yield rate of  $\text{NH}_3$  ( $17.2 \mu\text{g h}^{-1} \text{ cm}^{-2}$ ) in addition to a turnover frequency (TOF) value of  $0.26 \text{ h}^{-1}$ . Moreover, tuning of the Cu work function leads to improved  $\text{N}_2$  reduction and could achieve a high TOF value of  $0.26 \text{ h}^{-1}$ .

Molybdenum (Mo) is another transition metal used for  $\text{N}_2$  reduction because the d-electrons of Mo can weaken the  $\text{N}\equiv\text{N}$  triple bond. In the early experiments, Yandulov *et al.* reported the use of a single Mo centre for  $\text{N}_2$  reduction with efficiencies second to Fe/Mo nitrogenase.<sup>64</sup> Chen *et al.* successfully synthesized super small-sized Mo species through reduction of large-sized molybdenum oxide in a  $\text{H}_2$  atmosphere on a carbon support (carbon cloth).<sup>65</sup> The particle size decreased with increasing synthesis temperature. Remarkably, up to an average particle size of 0.95 nm was demonstrated using the developed method. The synthesized Mo catalyst showed an excellent activity towards ENRR with FE as high as 22.3% and a yield rate of  $7.02 \mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$  at 0 V vs. RHE under ambient

conditions using a 0.1 M KOH electrolyte. The high electrocatalytic activity is attributed to large active sites of super small-sized Mo NPs.

## 2.7 Bismuth (Bi)

The potential of the Bi metal towards ENRR arises from its poor HER activity due to the high Gibbs free energy barrier for hydrogen adsorption on its surface.<sup>66</sup> Thus Bi nanostructures have been widely investigated for ENRR.  $\text{N}_2$  molecules selectively adsorb on the Bi surface due to the overlap of the Bi 6p band and the N 2p orbital, which enhances the ENRR.<sup>67,68</sup> Moreover, due to the weak binding of  $\text{H}_{\text{ad}}$  atoms on the Bi surface, it can selectively promote  $\text{N}_2$  to  $\text{N}_2\text{H}^*$  reduction, and restrict surface electron accessibility for the HER process thus enhancing the  $\text{NH}_3$  production rate.<sup>67,69</sup> Li *et al.* reported two-dimensional mosaic Bi nanosheets (NSs) fabricated by an *in situ* electrochemical method as shown in Fig. 8.<sup>70</sup> The Bi NSs exhibited an average  $\text{NH}_3$  yield of  $2.54 \pm 0.16 \mu\text{g}_{\text{NH}_3} \text{ cm}^{-2} \text{ h}^{-1}$  ( $\sim 13.23 \mu\text{g mg}_{\text{cat}}^{-1} \text{ h}^{-1}$ ) with a FE of  $10.46 \pm 1.45\%$  at  $-0.8 \text{ V}$  in a 0.1 M  $\text{Na}_2\text{SO}_4$  electrolyte. The enhanced ENRR electrocatalytic activity was due to the semiconducting nature of the mosaic bismuth NSs, which limits surface electron accessibility and exposes effective p-orbital electron delocalized edge sites. Wang *et al.* successfully synthesized defect-rich Bi nanoplates by a low-temperature plasma bombardment approach as an ENRR electrocatalyst for  $\text{NH}_3$  production. The defect-rich Bi(110) nanoplates showed an  $^{15}\text{NH}_3$  yield rate of  $5.453 \mu\text{g mg}_{\text{Bi}}^{-1} \text{ h}^{-1}$  at  $-0.9 \text{ V}$  and a FE of 11.68% at  $-0.6 \text{ V}$  in aqueous solution under ambient conditions.<sup>71</sup> Xia *et al.* synthesized carbon fiber paper supported single-crystalline Bi NSs by *in situ* electrocatalytic topotactic transformation of BiOI NSs.<sup>72</sup> These Bi NSs exhibited an  $\text{NH}_3$  yield of  $12.49 \mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$  and a FE of 7.09% at  $-0.3 \text{ V}$  in a 0.1 M  $\text{NaHCO}_3$  electrolyte. Although the basal (001) plane of Bi NSs is relatively inert,



**Fig. 8** (a) XRD patterns of the BiOI precursor and Bi NSs; (b) SEM and (c) dark-field TEM images showing the nanosheet feature of Bi NSs; (d) TEM image of Bi NSs showing the mosaic structure; (e) high-resolution TEM image of Bi NSs; (f) SAED pattern of mosaic Bi NSs. Reproduced with permission from ref. 70. Copyright 2020, ACS.





the engineered exposed edge sites/planes (010) are conducive toward the adsorption and activation of  $N_2$  molecules as confirmed by the DFT calculations. Recently, Qiu and co-workers prepared multi-yolk-shell bismuth@porous carbon (MB@PC) composites *via* a facile simple hydrothermal reaction followed by pyrolyzation. This MB@PC composite showed an excellent performance with an  $NH_3$  yield of  $28.63 \mu g h^{-1} mg_{cat}^{-1}$  and a FE of 10.58% at  $-0.5 V$  in  $N_2$ -saturated  $0.1 M$  HCl solution. The synergetic effect of good conductivity, the highly porous feature derived from the carbon framework, and the intrinsic electrocatalytic ENRR activity of Bi NPs was the primary reason for excellent ENRR performance.<sup>73</sup>

Xu *et al.* demonstrated the ENRR activity using ultrathin Bi NSs prepared through the *in situ* electrochemical reduction-assisted exfoliation of BiOCl nanoplates (BiOCl NPs). This method facilitated an increase in electrochemically active surface area and under-coordinated Bi sites which accelerate electron transport capability. With these unique features, the as-converted Bi NSs exhibited a FE of 14.14% and an  $NH_3$  yield of  $11.11 mg h^{-1} mg_{cat}^{-1}$  at  $-0.5 V$  (vs. RHE) in  $0.1 M$   $Na_2SO_4$ , and high  $NH_3$  selectivity (nearly 100%).<sup>74</sup> One of the most significant breakthroughs has been achieved by Yan's group, attaining a very high FE of 66% and an  $NH_3$  yield of  $200 mmol g^{-1} h^{-1}$  in aqueous solution and under ambient conditions by utilizing a unique strategy of combining Bi nanocrystals (NCs) and  $K^+$ -supporting cations in water.<sup>67</sup> These studies suggest the potential of Bi-based electrocatalysts towards ENRR for producing a sizable amount of  $NH_3$ .

### 3. Bimetallic catalysts

Nanostructured metal catalysts such as Ru, Au, and Pd show significant electrocatalytic responses towards ENRR as discussed earlier.<sup>32</sup> However, the electrocatalytic activity of bimetallic alloy nanostructured catalysts is superior to their monometallic counterparts. The electrocatalytic performances of bimetallic nanostructured electrocatalysts depend on their surface electronic structure and thus on the shape, size, surface area, exposed facets, and compositions.<sup>75</sup> The high electrocatalytic activity of the bimetallic or alloy nanostructures arises from the synergistic effect of the component metals.<sup>76</sup> Thus bimetallic nanostructures have also been explored towards ENRR in recent years. Wang *et al.* reported ENRR using bimetallic PdRu nano tripods (TPs).<sup>77</sup> The highest average  $NH_3$  yield of  $37.23 mg h^{-1} mg_{cat}^{-1}$  and a corresponding FE of 1.85% was achieved at  $-0.2 V$  for PdRu TPs, which is higher than that of PdRu dendrite nanostructures and Pd NPs. This is attributed to the microstructures and alloying of Pd and Ru. Porous bimetallic alloys were synthesized and employed for ENRR. Bimodal porous  $Pd_3Cu_1$  exhibited an  $NH_3$  yield rate of  $39.9 \mu g h^{-1} mg_{cat}^{-1}$ .<sup>78</sup> Yu *et al.* reported bimetallic  $Ag_3Cu$  porous networks which exhibited excellent ENRR performance with an  $NH_3$  yield of  $24.59 \mu g h^{-1} mg_{cat}^{-1}$  and a FE of 13.28% at  $-0.5 V$  for ENRR.<sup>79</sup> The bimetallic catalyst showed higher activity than monometallic Cu and Ag in which its composition

played a significant role. Wang *et al.* reported bullet-like M-Te (M = Ru, Rh, Ir) porous nanorods (PNRs) for ENRR.<sup>80</sup> Among the MTe, optimized  $IrTe_4$  showed the highest FE and  $NH_3$  yield rate of 15.3% and  $51.1 \mu g h^{-1} mg_{cat}^{-1}$  at  $-0.2 V$ , respectively. Strong chemical adsorption between  $N_2$  and  $IrTe_4$  PNRs was indicated by  $N_2$  temperature-programmed desorption ( $N_2$ -TPD) and valence band X-ray spectroscopy measurements, which is the key feature towards the high ENRR of  $IrTe_4$  and suppression of HER. The high adsorption arises from the synergistic effect between the electron-rich Ir and highly electroactive surroundings of the Te atom.

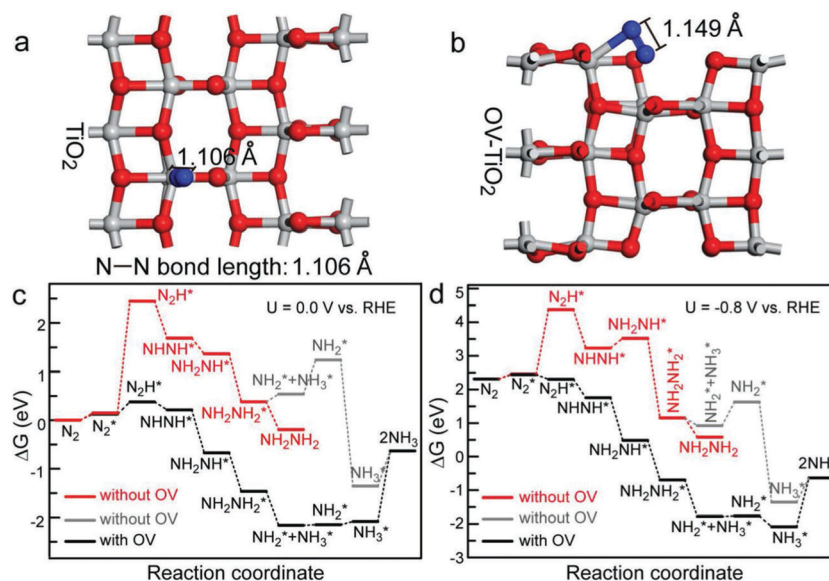
Table 1 compares the ENRR performance of single metal and bimetallic/trimetallic alloys under ambient conditions.

### 4. Transition metal oxides and defect-based catalysts

Over the years, transition metal oxides (TMOs) are explored almost in every type of energy conversion and storage device with reasonably satisfying results.<sup>94,95</sup> The catalytic activity of TMO-based materials arises from a combination of inherent electronic structure, microstructure, edges, defects, and interfacial structure in heterojunction and/or with support materials. Several TMOs such as  $TiO_2$ ,<sup>96</sup>  $Fe_2O_3$ ,<sup>97</sup>  $Mn_3O_4$ ,<sup>98</sup>  $NiO$ ,<sup>99</sup>  $Co_3O_4$ ,<sup>100</sup> and  $ZnO$ <sup>65</sup> have been studied as electrocatalysts for ENRR, which have demonstrated quite comparable performances with metal NP based catalysts (Au, Pd, and Ru). In oxides, oxygen vacancy defects play a crucial role in ENRR. An oxygen vacancy is created in an oxide-based semiconductor to form a defect centre.<sup>101</sup> A defect-rich oxygen vacancy exposes co-ordinately unsaturated metal sites, which enhances the chemisorption and activates inert  $N_2$  molecules. Fang *et al.* reported oxygen vacancy-contained  $TiO_2$  nanosheets as an electrocatalyst towards ENRR.<sup>102</sup> Oxygen vacancies were created by annealing the as-prepared  $TiO_2$  nanostructures under a  $H_2/Ar$  atmosphere. The high activity of the as-prepared oxygen vacant  $TiO_2$  is attributed to the synergistic effect between the structural features and microstructure of the catalyst. The DFT calculations suggest that the oxygen vacancies (OVs) can significantly lower the activation energy barrier of  $N \equiv N$  bond dissociation during  $N_2$  fixation (Fig. 9). Without OVs,  $TiO_2$  required a free energy of 4 eV for  $N_2$  activation, which makes  $TiO_2$  (without OV) inert to ENRR. The surface of the OV  $TiO_2$  site has much higher catalytic activity than the perfect  $TiO_2$  surface. The uphill energy of the first hydrogenation step is only 0.25 eV on the OV site, whereas as large as 2.29 eV is required for the perfect surface. After the first hydrogenation step, free energy changes for all steps toward the formation of  $NH_3$  are thermodynamically favourable on the OV site except for the desorption of  $NH_3$ . The two-dimensional  $TiO_2$  nanosheets provide a large number of active sites on their surface. The oxygen vacant  $TiO_2$  shows a 2.83 times higher  $NH_3$  yield rate than that of the as-prepared  $TiO_2$  nanostructures. Li *et al.* reported  $Ti^{3+}$  self-doped  $TiO_{2-x}$  nanowires on Ti mesh ( $Ti^{3+}$ - $TiO_{2-x}$ /TM) as the catalyst for ENRR.<sup>103</sup> The theoretical







**Fig. 9** (a and b) Adsorption configurations of the N<sub>2</sub> molecule on the perfect TiO<sub>2</sub> surface and at the OV site of OV-TiO<sub>2</sub>. (c) Free energy profile of the NRR process on the anatase(010) surface with and without OV at a potential of 0.0 V *versus* RHE. (d) Free energy profile of the NRR process on the anatase(010) surface with and without OV at a potential of -0.8 V *versus* RHE. The asterisks denote the adsorption. Reproduced with permission from ref. 102. Copyright 2020, Wiley-VCH.

calculation further suggests that the presence of Ti<sup>3+</sup> decreases the ENRR energy barrier and facilitates more number of active sites on the TiO<sub>2</sub> surface. In 0.1 M Na<sub>2</sub>SO<sub>4</sub>, Ti<sup>3+</sup>-TiO<sub>2-x</sub>/TM achieves a FE of 14.62% with an NH<sub>3</sub> yield of  $3.51 \times 10^{-11}$  mol s<sup>-1</sup> cm<sup>-2</sup> at -0.55 V. Qin *et al.* reported a carbon-doped TiO<sub>2</sub>/C (C-Ti<sub>x</sub>O<sub>y</sub>/C) material synthesized from the MIL-125(Ti) metal-organic framework (MOF) with an impressive FE of 17.8%. The high catalytic activity arises from the combination of C-Ti bond formation and oxygen vacancy.<sup>104</sup> The C-Ti binding is more favourable for N<sub>2</sub> activation than the non-substituted OV in TiO<sub>2</sub> catalysts.

Huang *et al.* reported the Mn<sub>3</sub>O<sub>4</sub> NPs@rGO composite (Mn<sub>3</sub>O<sub>4</sub>@rGO) for ENRR.<sup>105</sup> The theoretical study revealed that the N<sub>2</sub> molecule specifically adsorbed to a particular facet over the other. Mn<sub>3</sub>O<sub>4</sub>@rGO showed ENRR activity with excellent selectivity for NH<sub>3</sub> formation in 0.1 M Na<sub>2</sub>SO<sub>4</sub> solution with an NH<sub>3</sub> yield of 17.4 μg h<sup>-1</sup> mg<sub>cat</sub><sup>-1</sup> and a FE of 3.52% at -0.85 V. The rGO significantly improved the catalytic performance of Mn<sub>3</sub>O<sub>4</sub> by increasing the conductivity, surface area, and charge transfer kinetics across the electrode. The calculated binding energies (BE) of the N<sub>2</sub> molecule on the (221), (112), and (103) surface were -0.035, -0.32, and 0.29 eV, respectively, which suggest very weak adsorption of the N<sub>2</sub> molecule on the (221) surface whereas no adsorption on the (103) surface. On the other hand, the (112) surface exhibited decent adsorption of the N<sub>2</sub> molecule ( $E_{\text{binding}} = -0.32$  eV). The calculated binding energies also well agreed with the bond length between the N<sub>2</sub> molecule and the Mn atoms on different surfaces. Liu *et al.* reported ZnO quantum dot supported rGO (ZnO/rGO) for ENRR.<sup>106</sup> The DFT calculation revealed that the synergistic electronic coupling between ZnO and rGO significantly reduces the activation energy barrier for \*N<sub>2</sub>H species stabilization,

which is the rate-limiting step for ENRR. The as-synthesized ZnO/RGO showed an NH<sub>3</sub> yield of 17.7 μg h<sup>-1</sup> mg<sup>-1</sup> and a FE of 6.4% in 0.1 M Na<sub>2</sub>SO<sub>4</sub> at -0.65 V, which is higher than that of pure ZnO quantum dots and RGO.

## 5. Perovskite-based catalysts

Materials having the general formula ABO<sub>3</sub> are regarded as perovskite-type oxide materials where A is a rare-earth or alkaline earth element and B is a transition metal element. Though most of them have been used as electrolytes in ENRR, earlier studies have also used them as catalysts for NH<sub>3</sub> synthesis.<sup>107,108</sup> Co-based perovskites such as Sm<sub>0.5</sub>Sr<sub>0.5</sub>CoO<sub>3-δ</sub>, Ba<sub>0.5</sub>Sr<sub>0.5</sub>Co<sub>0.8</sub>Fe<sub>0.2</sub>O<sub>3-δ</sub> and La<sub>0.6</sub>Sr<sub>0.4</sub>Co<sub>0.2</sub>Fe<sub>0.8</sub>O<sub>3-δ</sub> have been tested as cathodes for electrochemical ENRR. However, the high thermal expansion coefficient, easy reduction of the active site, and evaporation of cobalt at higher temperatures raise a concern about their practical applicability.<sup>109,110</sup> Therefore it is highly desirable to develop cobalt-free perovskite oxide catalysts for NH<sub>3</sub> synthesis. In this regard, Amar *et al.* developed a new perovskite oxide La<sub>0.6</sub>Sr<sub>0.4</sub>Fe<sub>0.8</sub>Cu<sub>0.2</sub>O<sub>3-δ</sub> as a cathode catalyst for the electrochemical synthesis of NH<sub>3</sub> with a maximum production rate of  $5 \times 10^{-9}$  mol s<sup>-1</sup> cm<sup>-2</sup> at 450 °C.<sup>111</sup> Similarly, cobalt-free perovskite oxide SmFe<sub>0.7</sub>Cu<sub>0.3-x</sub>Ni<sub>x</sub>O<sub>3</sub> as the cathode material, a Nafion membrane as the electrolyte, and Ni-doped Ce<sub>0.8</sub>Sm<sub>0.2</sub>O<sub>2-δ</sub> as the anode have been tested for ENRR. The obtained ammonia yield rate was  $1.13 \times 10^{-8}$  mol cm<sup>-2</sup> s<sup>-1</sup> at 80 °C.<sup>112</sup> Recently, a different effective approach was demonstrated by Liu *et al.* The authors introduced oxygen vacancies into perovskite oxide LaCoO<sub>3</sub> (denoted as V<sub>O</sub>-LaCoO<sub>3</sub>) that remarkably increased the yield rate for NH<sub>3</sub>.<sup>113</sup> The Co atom and its adjacent oxygen vacancy created an active



centre that facilitated N<sub>2</sub> activation. The obtained NH<sub>3</sub> yield rate reached a maximum value of 182.2  $\mu\text{g}_{\text{NH}_3} \text{mg}_{\text{cat.}}^{-1} \text{h}^{-1}$ , which was 2.8 times higher than that of pristine LaCoO<sub>3</sub> (65.3  $\mu\text{g}_{\text{NH}_3} \text{mg}_{\text{cat.}}^{-1} \text{h}^{-1}$ ) leading to a FE of 7.6%. Further computational studies were carried out by the authors to understand the mechanism. The DFT calculation revealed that the oxygen vacancy increased the charge density around the valence band edge of V<sub>O</sub>-LaCoO<sub>3</sub> resulting in increased activation of N<sub>2</sub> at the V<sub>O</sub>-LaCoO<sub>3</sub> surface. The thermodynamic limiting potential for ENRR as compared to HER is also favourable for V<sub>O</sub>-LaCoO<sub>3</sub> in comparison to pristine LaCoO<sub>3</sub>.

## 6. Spinel-based catalysts

Spinel, having the general formula AB<sub>2</sub>O<sub>4</sub>, have been explored to some extent as electrolytes and catalysts for ENRR. The first report on a spinel oxide, *i.e.*, CoFe<sub>2</sub>O<sub>4</sub> prepared by a co-precipitation method was investigated by Amar *et al.*, which showed a maximum ammonia production rate of  $2.32 \times 10^{-10} \text{ mol s}^{-1} \text{ cm}^{-2}$  at 400 °C at 0.8 V.<sup>114</sup> A cost-effective sol-gel technique was also utilized to synthesize the same spinel oxide CoFe<sub>2</sub>O<sub>4</sub>, which produced  $6.5 \times 10^{-11} \text{ mol s}^{-1} \text{ cm}^{-2}$  ammonia through ENRR at 400 °C and 1.6 V, twice that of the value reported previously, using water vapour and nitrogen under atmospheric pressure.<sup>115</sup> This suggests that the synthesis techniques of catalyst materials have a strong impact on their ENRR performance. Ahmed *et al.* employed a one-pot solvothermal approach to synthesize CoFe<sub>2</sub>O<sub>4</sub> nanoclusters anchored on reduced graphene oxide as a nanocomposite catalyst for ENRR. They obtained a FE of 6.2% with a high NH<sub>3</sub> yield rate of  $4.2 \times 10^{-11} \text{ mol s}^{-1} \text{ cm}^{-2}$  in 0.1 M Na<sub>2</sub>SO<sub>4</sub> under ambient conditions along with excellent stability and durability for the long term ENRR performance.<sup>116</sup> Besides that, a low-cost material, *i.e.*, Mn<sub>3</sub>O<sub>4</sub>, known to be naturally abundant has been reported as an efficient electrocatalyst for ENRR. Sun and co-workers prepared Mn<sub>3</sub>O<sub>4</sub> nanocubes through a hydrothermal route and tested for ENRR in 0.1 M Na<sub>2</sub>SO<sub>4</sub> solution. The catalyst delivered a FE of 3.0% with an NH<sub>3</sub> yield of 11.6  $\mu\text{g mg}_{\text{cat.}}^{-1} \text{h}^{-1}$  at −0.8 V.<sup>98</sup> So far Mn<sub>3</sub>O<sub>4</sub> has been successfully tested as an ENRR electrocatalyst.<sup>105</sup> To further improve the performance of Mn<sub>3</sub>O<sub>4</sub> and suppress the HER, Li<sup>+</sup> ions were incorporated into the Mn<sub>3</sub>O<sub>4</sub> spinel. The spinel LiMn<sub>2</sub>O<sub>4</sub> was prepared by electrospinning and tested in 0.1 M HCl at −0.50 V. The as-synthesized catalyst showed a FE of 7.44% and an NH<sub>3</sub> yield rate of 15.83  $\mu\text{g mg}_{\text{cat.}}^{-1} \text{h}^{-1}$ , which are much higher than those of pristine Mn<sub>3</sub>O<sub>4</sub> reported earlier.<sup>117</sup>

Oxygen vacancies (OVs) were created in spinels to enhance the ENRR activity. Various OV-rich nanostructured spinel wrapped hollow nitrogen-doped carbon polyhedra such as OV-rich NiCo<sub>2</sub>O<sub>4</sub>@HNCP, OV-rich ZnCo<sub>2</sub>O<sub>4</sub>@HNCP, and OV-rich Co<sub>3</sub>O<sub>4</sub>@HNCP were reported to facilitate the ENRR. Among these, OV-rich NiCo<sub>2</sub>O<sub>4</sub>@HNCP showed a high NH<sub>3</sub> production yield of 4.1  $\mu\text{g h}^{-1} \text{ cm}^{-2}$ /17.8  $\mu\text{g mg}^{-1} \text{h}^{-1}$  and a FE of 5.3%.<sup>118</sup> However, there is still a vast opportunity to explore these spinel-based materials with rational design for enhancing the efficiency of ENRR.

**Table 2** Summary of oxides, perovskites, and spinels as ENRR electrocatalysts reported in recent years and their catalytic performance

Catalyst	Electrolyte	Temperature	Yield rate ( $\mu\text{g h}^{-1} \text{ mg}_{\text{cat.}}^{-1}$ )	FE (%)	Potentials vs. RHE (V)	Ref.
B-TiO <sub>2</sub>	Na <sub>2</sub> SO <sub>4</sub>	Ambient	14.4	3.4	−0.8	119
V-TiO <sub>2</sub>	LiClO <sub>4</sub>	Ambient	17.73	—	−0.50	120
			—	15.3	−0.40	
C-TiO <sub>2</sub>	Na <sub>2</sub> SO <sub>4</sub>	Ambient	16.22	1.84	−0.7	121
Fe-TiO <sub>2</sub>	LiClO <sub>4</sub>	Ambient	25.47	25.6	−0.40	122
VO <sub>2</sub>	Na <sub>2</sub> SO <sub>4</sub>	Ambient	14.85	3.97	−0.7	123
Cr <sub>2</sub> O <sub>3</sub>	HCl	Ambient	28.13	8.56	−0.75	124
Mn <sub>3</sub> O <sub>4</sub>	Na <sub>2</sub> SO <sub>4</sub>	Ambient	11.6	3.0	−0.8	98
Mo-	Na <sub>2</sub> SO <sub>4</sub>	Ambient	36.6	7.9	−0.5	125
MnO <sub>2</sub>						
Fe <sub>2</sub> O <sub>3</sub>	Na <sub>2</sub> SO <sub>4</sub>	Ambient	15.9	0.94	−0.8	126
NiO	Na <sub>2</sub> SO <sub>4</sub>	Ambient	29.1	10.8	−0.5	127
NiWO <sub>4</sub>	HCl	Ambient	40.05	19.32	−0.3	128
	Na <sub>2</sub> SO <sub>4</sub>		23.14	10.18		
FeMoO <sub>4</sub>	Na <sub>2</sub> SO <sub>4</sub>	Ambient	17.51	10.53	−0.6	129
Fe-SnO <sub>2</sub>	HCl	Ambient	82.7	20.4	−0.3	130
β-Bi <sub>2</sub> O <sub>3</sub>	Na <sub>2</sub> SO <sub>4</sub>	Ambient	19.92	4.3	−0.8	131
r-CeO <sub>2</sub>	Na <sub>2</sub> SO <sub>4</sub>	Ambient	16.4	~3.5	−0.5	132
Cr-CeO <sub>2</sub>	Na <sub>2</sub> SO <sub>4</sub>	Ambient	16.82	3.84	−0.7	133
Ta <sub>2</sub> O <sub>5</sub>	HCl	Ambient	15.9	8.9	−0.7	134
La <sub>2</sub> O <sub>3</sub>	Na <sub>2</sub> SO <sub>4</sub>	Ambient	17.04	4.76	−0.8	135
La <sub>2</sub> Ti <sub>2</sub> O <sub>7</sub>	HCl	Ambient	25.15	4.55	−0.55	136
LaCrO <sub>3</sub>	Na <sub>2</sub> SO <sub>4</sub>	Ambient	24.8	15	−0.8	137
LaFeO <sub>3</sub>	HCl	Ambient	18.59	8.77	−0.55	138

The ENRR performance of more oxides, perovskites, and spinels under ambient conditions is presented in Table 2 for comparison.

## 7. Phosphide-based catalysts

Transition metal phosphides (TMPs) have emerged as highly active and inexpensive electrocatalysts as well as cocatalysts for HER with performance comparable to that of the state-of-the-art Pt/C. A wide range of TMPs such as CoP,<sup>139</sup> Ni<sub>2</sub>P,<sup>140</sup> MoP,<sup>141</sup> Cu<sub>3</sub>P,<sup>142</sup> and FeP<sup>143</sup> have thus been studied for HER. Over the years, different compositions, microstructures, hetero-microstructures, and doped TMPs have been synthesized to enhance the performance. A review article by Wang *et al.* provides the details on the development of TMPs and their potential application for (photo) electrochemical water splitting.<sup>144</sup> However, TMPs for ENRR have not been largely explored. The same challenge, *i.e.*, suppression of HER activity, remains the limiting factor to enhance ENRR with TMP-based catalysts. Zhu *et al.* reported phosphorus as a modulating agent of the FeP<sub>2</sub> catalyst towards ENRR performance.<sup>145</sup> The synthesized P rich FeP<sub>2</sub>-reduced graphene oxide (FeP<sub>2</sub>-rGO) showed a FE and NH<sub>3</sub> yield rate of 21.99% and 35.26  $\mu\text{g h}^{-1} \text{ mg}_{\text{cat.}}^{-1}$  at −0.40 V, respectively. On the other hand, the FeP-rGO catalyst showed a lower FE and NH<sub>3</sub> yield of 8.57% and 17.13  $\mu\text{g h}^{-1} \text{ mg}_{\text{cat.}}^{-1}$  at −0.40 V, respectively. The ENRR suffers from the competitive HER at the electrode surface due to the low H adsorption energy to the catalyst surface in the latter case.  $\Delta G_{(\text{H})}$  is used as a parameter to quantify the metal hydrogen bond strength. The theoretical calculation of  $\Delta G_{(\text{H})}$  for FeP(211) and FeP<sub>2</sub>(101) indicates that FeP(101) is more



active towards HER than  $\text{FeP}_2(211)$ . The ENRR mechanism follows the distal pathways, which are energetically more favourable than the alternating pathways. The rate-determining step for ENRR is  $^*\text{N}_2$  to  $^*\text{NNH}$ . The  $\text{N}_2$  adsorption free energy for  $\text{FeP}_2(101)$  is higher than that for  $\text{FeP}(211)$ , which suggests the former to be more selective towards ENRR. The P-rich  $\text{FeP}_2$ -rGO decreases HER activity, increases  $\text{N}_2$  adsorption, and facilitates a large number of active sites towards ENRR compared with  $\text{FeP}$ . Jin *et al.* reported partially electrochemically reduced oxygen-doped  $\text{Cu}_3\text{P}$  nanosheets ( $\text{RO-Cu}_3\text{P}$ ) with rich surface phosphorus vacancies for the ENRR process.<sup>146</sup> Both  $\text{NH}_3$  and  $\text{N}_2\text{H}_4$  were formed during the ENRR process indicating that the reaction follows the alternating pathways. An  $\text{NH}_3$  yield of  $28.12 \mu\text{g h}^{-1} \text{cm}^{-2}$  with a FE of 17.5% was achieved under ambient conditions for the  $\text{RO-Cu}_3\text{P}$  catalyst with abundant phosphorus vacancies, which is 3.4 times higher than that of the pure  $\text{Cu}_3\text{P}$  catalyst. The surface phosphorus vacancy acts as an active site for ENRR, which is proven by controlled experimental as well as DFT calculations. The free energy change ( $\Delta G_{\text{NNH}}$ ) on a phosphorus vacancy on the surface of  $\text{Cu}_3\text{P}(110)$  is found to be 0.97 eV (at 0 V, pH = 0) for  $^*\text{N}_2$  to  $^*\text{NNH}$ . The  $\Delta G_{\text{NNH}}$  on the surface phosphorus vacancy of O- $\text{Cu}_3\text{P}$  structures was calculated to be 1.25 eV for  $\text{Cu}_3\text{P}_{0.98}\text{O}_{0.02}$  and 2.47 eV for  $\text{Cu}_3\text{P}_{0.96}\text{O}_{0.04}$ , which is higher than that required on the surface phosphorus vacancy of  $\text{Cu}_3\text{P}$ . This demonstrates that the superfluous oxygen doped in the phosphide crystal phase is not conducive to ENRR activity. The experimental and theoretical investigations suggest that the phosphorus vacancies on the surface of  $\text{Cu}_3\text{P}$  and O- $\text{Cu}_3\text{P}$  are the highly active species that lead to enhanced ENRR activity. Yang *et al.* synthesized  $\text{IrP}_2$  anchored P, N co-doped porous carbon nanofilms ( $\text{IrP}_2@\text{PNPC-NFs}$ ) by the plasma-assisted method.<sup>147</sup> The  $\text{IrP}_2@\text{PNPC-NFs}$  showed a FE and  $\text{NH}_3$  yield rate of 17.8% and  $94.0 \mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$ , respectively. The edge site of  $\text{IrP}_2$  was found to be very irregular and the low coordinated step atoms at the edge site of the  $\text{IrP}_2$  nanocrystals lowered the reaction energy barrier towards the ENRR while inhibiting the HER activity. The plasma-assisted strategy also makes it possible to synthesize other high-melting-point noble-metal phosphides (such as  $\text{OsP}_2@\text{PNPC-NFs}$ ,  $\text{Re}_3\text{P}_4@\text{PNPC-NFs}$ ) at lower temperatures.

## 8. Nitride-based catalysts

Transition metal nitrides (TMNs) are another class of materials that have high electronic conductivity with rich  $\text{N}_{\text{ad}}$  atoms. Theoretical as well as experimental investigations suggest that TMNs have huge potential for ENRR.<sup>148,149</sup> However, the chemical stability of the nitride-based materials is an obstacle in addition to competent HER.<sup>150</sup> Moreover the generation of  $\text{NH}_3$  from the nitrogen atom of the catalyst can give false-positive results (discussed later). Abghoui and Skúlason theoretically investigated TMNs for ENRR under ambient conditions and provided possible mechanistic insights considering several nitrides such as  $\text{ZrN}$ ,  $\text{MoN}$ ,  $\text{CrN}$ ,  $\text{MnN}$ ,  $\text{NbN}$ , and  $\text{VN}$

with a rocksalt structure.<sup>151</sup> The free energy diagrams were constructed on the rocksalt (100) structure using the associated mechanism to evaluate their performance in terms of onset potential for ENRR. The free energy of each intermediate was calculated at room temperature, pH = 0, and an applied potential of 0.0 V, which indicates that the potential determining step (PDS) is the first protonation of  $^*\text{N}_2$  to  $^*\text{NNH}$  for all the candidates except for  $\text{VN}$  and  $\text{NdN}$  where the formation of  $^*\text{NNH}_3$  is the PDS. Among these nitrides,  $\text{MoN}$  showed promising results with  $\Delta G_{\text{PDS}} = 0.83 \text{ eV}$ .<sup>151</sup> Zhang *et al.* demonstrated a  $\text{MoN}$  nanosheet array on carbon cloth ( $\text{MoN NA/CC}$ ) as an ENRR electrocatalyst in 0.1 M  $\text{HCl}$  under ambient conditions.<sup>152</sup> This catalyst showed an  $\text{NH}_3$  yield of  $3.01 \times 10^{-10} \text{ mol s}^{-1} \text{cm}^{-2}$  and a FE of 1.15% at  $-0.3 \text{ V}$  with high electrochemical durability and selectivity. DFT calculations suggested that  $\text{MoN NA/CC}$  catalyzes ENRR *via* the Mars-van Krevelen mechanism rather than the associative/dissociative Heyrovsky mechanism. Jin *et al.* reported nitrogen vacant 2D layered  $\text{W}_2\text{N}_3$  (Fig. 10) as an efficient and stable electrocatalyst for ENRR with a steady  $\text{NH}_3$  yield rate of  $11.66 \pm 0.98 \mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$  ( $3.80 \pm 0.32 \times 10^{-11} \text{ mol cm}^{-2} \text{s}^{-1}$ ) and FE of  $11.67 \pm 0.93\%$  at  $-0.2 \text{ V}$  for 12 cycles (24 h).<sup>153</sup> The *ex situ* synchrotron-based characterization of the catalyst before and after the catalytic cycle revealed the stability of 2D  $\text{W}_2\text{N}_3$ , which was attributed to the vacancies on 2D  $\text{W}_2\text{N}_3$  with the combinational effect of the high valence state of tungsten atoms and 2D morphology induced surface distortion. The DFT calculations suggested that the electron-deficient environment in the 2D layered  $\text{W}_2\text{N}_3$  effectively facilitates the electron acceptance from  $\text{N}_2$  and enhances the subsequent reduction rate.

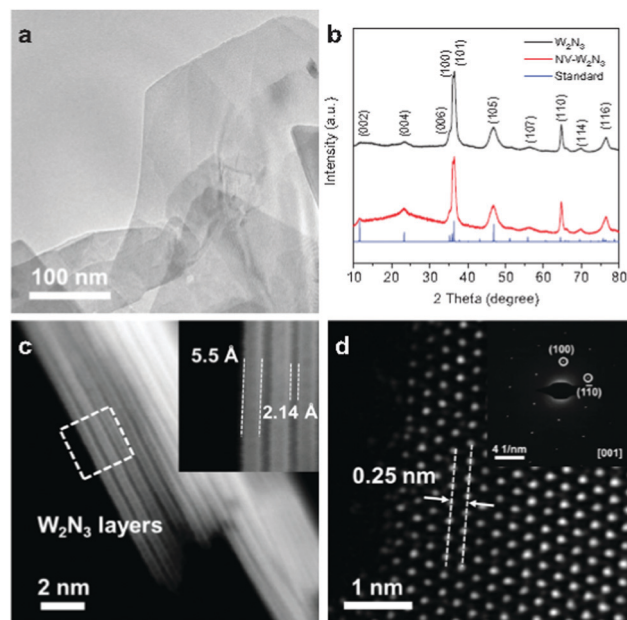


Fig. 10 (a) TEM image of  $\text{NV-W}_2\text{N}_3$ . (b) XRD patterns of  $\text{W}_2\text{N}_3$  and  $\text{NV-W}_2\text{N}_3$ . (c) HAADF-STEM images of  $\text{NV-W}_2\text{N}_3$  that show the single-layered thickness and interlayer spacing of  $\text{NV-W}_2\text{N}_3$ . (d) HAADF-STEM image and the corresponding SAED pattern (inset) of  $\text{NV-W}_2\text{N}_3$ . Reproduced with permission from ref. 153. Copyright 2020, Wiley-VCH.





Ren *et al.* synthesized Mo<sub>2</sub>N nanorods and studied the same as a catalyst for ENRR.<sup>149</sup> Mo<sub>2</sub>N/GCE delivered an NH<sub>3</sub> yield of 78.4 μg h<sup>-1</sup> mg<sub>cat.</sub><sup>-1</sup> with a FE of 4.5% at -0.3 V. The as-synthesized catalyst was found to be durable up to 10 cycles as confirmed by XPS and XRD analysis after the stability test. However, Hu *et al.* found that the decomposition of the tetragonal Mo<sub>2</sub>N catalyst led to NH<sub>3</sub> evolution, which was confirmed by isotope experiments and thus contradicts the previous report entirely.<sup>154</sup> The authors of the latter report suggested that isotope experiments are needed to evaluate the catalytic activity of the TMNs. Yang *et al.* reported VN nanoparticles as a stable electrocatalyst for ENRR with a yield rate of 3.3 × 10<sup>-10</sup> mol s<sup>-1</sup> cm<sup>-2</sup> and a FE of 6.0% at -0.1 V within 1 h.<sup>155</sup> The *ex situ* XPS measurement indicated the presence of the oxide and oxynitride species in the catalyst. However, the conversion of VN<sub>0.7</sub>O<sub>0.45</sub> to the VN phase leads to catalyst deactivation. The study highlights that the N site adjacent to the surface O atoms is the active site towards ENRR. Zhang *et al.* reported VN nanosheets on Ti mesh for ENRR as an active and selective electrocatalyst for ENRR in 0.1 M HCl at room temperature and atmospheric pressure and obtained an NH<sub>3</sub> yield of 8.40 × 10<sup>-11</sup> mol s<sup>-1</sup> cm<sup>-2</sup> at -0.50 V with a FE of 2.25%.<sup>156</sup>

## 9. Carbide-based catalysts

Transition metals carbides (TMCs) have also been explored in the search for a noble metal-free catalyst for ENRR. TMCs exhibit specific properties which are desirable for electrocatalysis, such as corrosion resistance, and high stability, melting point, and mechanical strength.<sup>157-159</sup> These specific properties have attracted increasing research interest for their potential application as electrocatalysts,<sup>160</sup> catalyst supports,<sup>161</sup> lithium-ion battery materials,<sup>162</sup> and solar cell materials,<sup>163</sup> particularly for energy generation and storage purpose.<sup>164</sup> The carbides are referred as an interstitial alloy. The electronic structure of the host metal of the carbide is altered due to the inclusion of the carbon atoms through the charge transfer process. The distinct electrocatalytic activity of the TMC arises from the electronic structure, due to the presence of carbon atoms in the metal lattice. For example, the excellent HER performance of the tungsten carbide arises from the filling of the d-states at the Fermi level of tungsten by alloying it with carbon.<sup>165</sup> Thereby, TMCs are investigated as electrocatalysts without certain disadvantages such as chemical susceptibility and durability. So far, TMCs are employed as HER, OER, and ORR cathode catalysts with excellent activity.<sup>165,166</sup> However, there are relatively few reports on the use of TMC materials for ENRR through nanostructuring,<sup>167</sup> combination with another material,<sup>168</sup> and exploiting hybrid structures.

The DFT calculation suggests that the metal site of the carbide can activate the N<sub>2</sub> molecule and stabilize the intermediate N<sub>x</sub>H<sub>y</sub> species while destabilizing the -NH<sub>2</sub> species during the desorption as NH<sub>3</sub>.<sup>82</sup> Although the carbide-based materials show promising ENRR activity theoretically, the experimental performance is not up to the mark due to the competitive HER under similarly applied potentials.<sup>169</sup>

Therefore different fabrication methods have been adopted to enhance the ENRR performance of the carbide-based catalysts by creating heterojunction interfaces with the generation of active sites for various elementary steps. DFT analysis indicates that all the crystallographic surfaces of the cubic MoC catalyst have the ability for adsorption and dissociation.<sup>170</sup> Ramaiyan *et al.* reported an origami-like Mo<sub>2</sub>C cathode catalyst for ENRR and achieved a maximum NH<sub>3</sub> synthesis rate of 2.16 × 10<sup>-11</sup> mol cm<sup>-2</sup> s<sup>-1</sup> with a FE of 1.8% at 30 °C using Nafion-212 as an electrolyte.<sup>171</sup> The authors revealed that numerous kinks at the surface of the origami-like structures are responsible for the catalytic ENRR. However, the synthesized origami-like Mo<sub>2</sub>C catalyst was found to be unstable during the ENRR process. XPS analysis after the electrolysis process indicates the formation of molybdenum oxycarbide which raises concern about catalyst susceptibility for long term uses. Qu *et al.* reported oxygen doped molybdenum carbide (O-MoC) embedded in nitrogen-doped carbon layers (N-doped carbon) for ENRR.<sup>172</sup> The O-MoC embedded N-doped carbon was synthesized from dopamine and molybdate. The catalyst showed a FE of 25.1% and an NH<sub>3</sub> yield rate of 22.5 μg h<sup>-1</sup> mg<sub>cat.</sub><sup>-1</sup> in 0.1 mM HCl + 0.5 M Li<sub>2</sub>SO<sub>4</sub>. The competitive HER was suppressed due to the interaction between O-MoC and N-doped carbon. The catalyst retained its performance after continuous electrolysis for 30 h. The carbon shelling around O-MoC provides physicochemical protection to O-MoC in the acidic electrolyte from structural dissolution. Liu *et al.* reported a Mo/Mo<sub>2</sub>C/MoC (Mo/Mo<sub>x</sub>C) heterostructure supported rGO for ENRR.<sup>173</sup> The catalyst showed an excellent yield rate of 20.4 μg h<sup>-1</sup> mg<sup>-1</sup> at -0.2 V and a FE up to 18.9% at -0.3 V. By controlling the precursor, well-dispersed Mo, Mo<sub>2</sub>C, binary MoC/Mo<sub>2</sub>C (Mo<sub>x</sub>C), and ternary Mo/MoC/Mo<sub>2</sub>C (Mo/Mo<sub>x</sub>C) NPs were synthesized on rGO and the authors experimentally and theoretically studied the influence of composition and hetero-interface on the ENRR performance (Fig. 11). The heterostructured Mo<sub>x</sub>C and Mo/Mo<sub>x</sub>C showed significantly enhanced ENRR activity. The heterojunction facilitates a higher number of available active sites compared to that of Mo and Mo<sub>2</sub>C only catalysts. DFT calculations further confirmed that the introduction of metallic Mo into binary and ternary carbides appreciably lowered the energy demand for NH<sub>3</sub> desorption from the catalyst surface.

Peng *et al.* reported the bio-inspired synthesis of a Fe<sub>3</sub>C@C core-shell structured catalyst for ENRR.<sup>174</sup> The core-shell structure acts as an active site and selectively contributes toward the NH<sub>3</sub> synthesis at low potentials. A FE of 9.15% and an NH<sub>3</sub> yield rate of 8.53 μg h<sup>-1</sup> mg<sub>cat.</sub><sup>-1</sup> at -0.2 V were achieved with the same catalyst. The degree of graphitization during the synthesis of the catalyst plays a prominent role in the ENRR. The catalyst prepared at 900 °C showed higher ENRR activity than the catalyst prepared at 700 °C. With increasing temperature, the degree of graphitization increases, whereas on further increasing the temperature to 1100 °C, the performance significantly decreases. The graphitization at 900 °C improved the electron transportation with optimum Fe content. With a further increase in graphitization, the Fe contribution towards





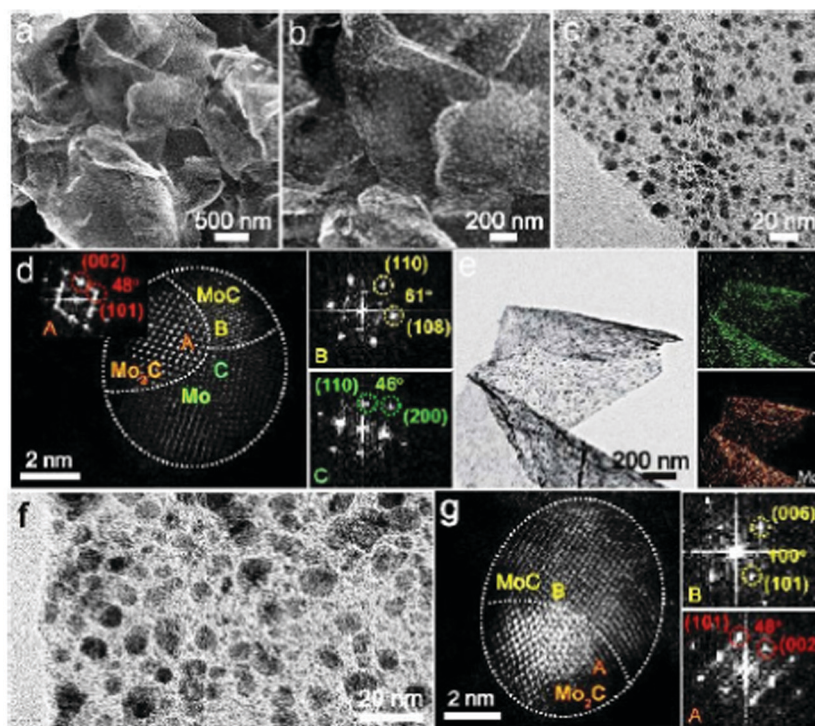


Fig. 11 (a and b) SEM, (c) TEM, (d) STEM, and (e) EDS mapping images of the Mo/Mo<sub>x</sub>C heterostructure. (f) TEM and (g) STEM images of the Mo<sub>x</sub>C heterostructure. Reproduced with permission from ref. 173. Copyright 2020, RSC.

ENRR decreases. DFT analysis suggested that the free energy change of the rate-limiting step over the Fe<sub>3</sub>C@C core-shell towards formation and desorption of NH<sub>3</sub> is more favourable than that of Fe<sub>3</sub>C. The observation indicates that the interaction between the carbon shell and the Fe<sub>3</sub>C core facilitates the charge transport in the catalyst.

MXene represents another group of novel 2D materials with the general formula M<sub>n+1</sub>C<sub>n</sub>, where M represents transition metals such as Ti, Zr, Hf, V, Nb, Ta, Cr, Mo, and W with  $n = 1, 2, 3$  along with the terminal functional groups (F, OH, and/or O).<sup>175,176</sup> Azofra *et al.* computationally investigated the possibility of d<sub>2</sub>-d<sub>4</sub> transition metal-based MXene (M<sub>3</sub>C<sub>2</sub>) as a model material for N<sub>2</sub> capture and reduction. The DFT calculation revealed that the transition metal atoms present at the terminal surface can activate the adsorbed N<sub>2</sub> and facilitate the ENRR under mild conditions.<sup>175</sup> Zheng *et al.* theoretically investigated the possible prospect of boron-doped MXene towards ENRR.<sup>176</sup> The B-doped Mo<sub>2</sub>CO<sub>2</sub> and W<sub>2</sub>CO<sub>2</sub> MXenes exhibited decent catalytic activity and selectivity with limiting potentials of  $-0.20$  and  $-0.24$  V, respectively. The boron centre mimics the empty and filled d-orbital electronic structure of transition metals and activates the N<sub>2</sub> molecule effectively. In addition, a high B-to-adsorbate electron donation tendency facilitates the hydrogenation of \*N<sub>2</sub> to \*N<sub>2</sub>H during the ENRR. A recent study further suggested that the terminal oxygen groups act as active sites for the HER and CO<sub>2</sub> reduction.<sup>160</sup> Even though there is a huge prospect for MXene materials toward ENRR, competitive HER mitigation is the main issue that needs to be addressed to unveil the higher efficiency of MXene towards ENRR. Luo *et al.*

reported Ti<sub>3</sub>C<sub>2</sub>O<sub>2</sub> 2D MXene for ENRR.<sup>177</sup> The surface Ti atoms act as active sites for N<sub>2</sub> adsorption in the single-layer T-Ti-C-Ti-C-T-T (T = terminal atoms) sandwich structure with maximum binding energy. The N<sub>2</sub> adsorption energy indicates that the middle Ti atoms are energetically preferable to the C and O sites. The terminal O atoms cannot overcome the high energy barrier for ENRR whereas the Ti site at the edge plane is preferred. Ti<sub>3</sub>C<sub>2</sub>T<sub>x</sub> MXene with a smaller sheet size shows higher performance than that with a large sheet size under  $-0.1$  V. The study also revealed that vertically aligned Ti<sub>3</sub>C<sub>2</sub>T<sub>x</sub> MXene has more active sites than the randomly oriented one. Vertically aligned Ti<sub>3</sub>C<sub>2</sub>T<sub>x</sub> MXene with a FeOOH nanosheet host was synthesized to overcome the thermodynamic obstacles. The FE of MXene/FeOOH reached 5.78% under  $-0.2$  V, which is 1.25 times higher than the maximum value of the MXene. The improved performance of the MXene was ascribed to a higher number of active sites of the vertically aligned MXene and the sluggish nature of FeOOH towards HER.

## 10. Sulfide-based catalysts

Over the past few years, metal sulfides have been widely studied as a potential candidate for various electrocatalytic activities.<sup>178–180</sup> Inspired by the natural nitrogenase enzymes (Mo-Fe protein), MoS<sub>2</sub> has been investigated as a catalyst for ENRR.<sup>181</sup> Sun and co-workers were the first to introduce and experiment on MoS<sub>2</sub> as a catalyst under room temperature and atmospheric pressure. The catalyst showed a FE of 1.17%



and an  $\text{NH}_3$  yield of  $8.08 \times 10^{-11} \text{ mol s}^{-1} \text{ cm}^{-2}$  at  $-0.5 \text{ V}$  in  $0.1 \text{ M Na}_2\text{SO}_4$ .<sup>182</sup> Later on, they further improved the FE to 8.34% with an  $\text{NH}_3$  yield of  $29.28 \mu\text{g mg}_{\text{cat}}^{-1} \text{ h}^{-1}$  at  $-0.40 \text{ V}$ , by designing defect-rich  $\text{MoS}_2$  nanoflowers.<sup>183</sup> Zeng *et al.* developed nanoflower-like N-doped  $\text{MoS}_2$  electrocatalysts and introduced rich sulfur vacancies to further enhance the FE to 9.14% with an  $\text{NH}_3$  yield of  $69.82 \text{ mg mg}_{\text{cat}}^{-1} \text{ h}^{-1}$  at  $-0.3 \text{ V}$  in  $0.1 \text{ M Na}_2\text{SO}_4$  solution.<sup>184</sup> Suryanto *et al.* developed  $\text{MoS}_2$  nanosheets decorated with Ru clusters and obtained a FE of 17.6% and an  $\text{NH}_3$  yield rate of  $1.14 \times 10^{-10} \text{ mol s}^{-1} \text{ cm}^{-2}$  attributed to the polymorphic engineering in Ru/2H- $\text{MoS}_2$ .<sup>185</sup> Thereafter several other studies based on  $\text{MoS}_2$  have been reported to date achieving FE from as low as 4.58% to 20.6% using different strategies.<sup>186–190</sup> Apart from  $\text{MoS}_2$ , other transition metal dichalcogenides such as  $\text{WS}_2$  have been tested as an ENRR catalyst with the lowest potential of  $-0.24 \text{ V}$  through an enzymatic mechanism using DFT.<sup>191</sup> Flower-like  $\text{SnS}_2$  and forest-like  $\text{ZnS}$  nanoarrays directly grown on Ni foam showed certain abilities towards ENRR. The  $\text{NH}_3$  yield and FE of  $^{15}\text{N}_2$  with flower-like  $\text{SnS}_2$  were  $9.08 \times 10^{-10} \text{ mol s}^{-1} \text{ cm}^{-2}$  and 10.3%, whereas for  $\text{ZnS}$ , they were  $5.27 \times 10^{-10} \text{ mol s}^{-1} \text{ cm}^{-2}$  and 5.62%, at  $-0.5 \text{ V}$ , respectively.<sup>192</sup> Similarly, cobalt disulfide ( $\text{CoS}_2$ ) NP-embedded N-doped carbon nanoboxes ( $\text{CoS}_2@\text{NC}$ ) derived from ZIF-67 have shown effective electrochemical  $\text{NH}_3$  production under ambient conditions. The catalyst showed an  $\text{NH}_3$  yield of  $17.45 \mu\text{g mg}_{\text{cat}}^{-1} \text{ h}^{-1}$  and a high FE of 4.6% at  $-0.15 \text{ V}$  vs. RHE.<sup>193</sup>

## 11. Metal-free electrocatalysts: heteroatom doped carbon-based catalysts

Metal and metal-based oxide, phosphide, carbide, nitride, and sulfide catalysts have been explored as potential ENRR electrocatalysts as discussed earlier. In addition to these, metal-free electrocatalysts have also been studied as ENRR electrocatalysts due to their  $\text{N}_2$  adsorption ability and weak interaction with  $\text{H}^+$  ions that specifically suppressed the HER.<sup>194–196</sup> However, pure carbon-based materials are inactive towards ENRR.<sup>197</sup> This led to the synthesis of a variety of heteroatom doped carbons for ENRR that exhibit considerable ENRR performance. In particular, N-doped porous carbon (NC) exhibited ENRR activity, where pyridinic and pyrrolic N-sites are identified as active sites for  $\text{N}_2$  adsorption and subsequent dissociation.<sup>198</sup> Polymeric carbon nitride (PCN),<sup>199</sup> N-doped carbon synthesized from biomass,<sup>200</sup> and zeolitic imidazolate frameworks (ZIF-8) have shown considerable ENRR activity.<sup>201</sup> The ENRR performance of these catalysts is attributed to the defects arising from the heteroatom doping. However, a recent study has shown that heteroatom-doped carbon materials are also efficient HER electrocatalysts.<sup>202</sup> Thus, suppression of HER is the fundamental task to obtain efficient carbon-based catalysts for ENRR.

Yu *et al.* studied boron-doped graphene for ENRR.<sup>203</sup> Boron doping redistributed the electron density in the graphene framework, where the electron-deficient boron sites enhanced

the binding capability of  $\text{N}_2$  molecules. DFT calculations based on different boron carbon models revealed that the  $\text{BC}_3$  site facilitates the lowest energy barrier for ENRR. At 6.2% of boron doping on graphene, an  $\text{NH}_3$  yield of  $9.8 \text{ mg h}^{-1} \text{ cm}^{-2}$  and a FE of 10.8% were achieved at  $-0.5 \text{ V}$  in aqueous solutions under ambient conditions. Qiao *et al.* revealed that the addition of boron (B) to nitrogen-doped graphene yields a higher Gibbs free energy of hydrogen adsorption ( $\text{DGH}^*$ ) indicating that  $^*\text{H}$  species were not easily adsorbed onto the active sites and hence suppressed HER.<sup>204</sup>  $\text{BC}_3$  sites in the boron-doped graphene exhibit as active centres for better ENRR activity compared to that of raw graphene.<sup>203</sup> Song *et al.* reported ENRR using N and P co-doped porous carbon with a trace of iron (0.028 wt%) (Fe-NPC).<sup>205</sup> The Fe-NPC catalyst was synthesized from solid-state pyrolysis of polyaniline aerogels with phytic acids and  $\text{FeCl}_3$ , which showed significantly enhanced electrocatalytic activity in an alkaline medium as compared to NPC. The Fe sites acted as active sites towards ENRR. In the presence of  $\text{SCN}^-$ , the ENRR was significantly decreased due to the strong affinity of the  $\text{SCN}^-$  ions towards the Fe site. Fe-NPC showed a FE and  $\text{NH}_3$  yield rate of 5.3% and  $4.36 \mu\text{g h}^{-1} \text{ mg}^{-1}$  at  $-0.1 \text{ V}$ . The *in situ* FTIR spectra at  $-0.1 \text{ V}$  for the Fe-NPC catalyst showed four peaks at 1126, 1273, 1412, and  $3256 \text{ cm}^{-1}$ . The peak at  $1126 \text{ cm}^{-1}$  indicates the cleavage of  $\text{N}\equiv\text{N}$  whereas the peaks at 1273, 1412, and  $3256 \text{ cm}^{-1}$  correspond to  $-\text{NH}_2$  wagging and  $\text{H}-\text{N}-\text{H}$  bending, suggesting the intermediate species formed during the ENRR process. It is to be noted that the ENRR process over the Fe-NPC catalyst follows associative pathways.

Wu *et al.* reported P-doped graphene (PG) for ENRR with a FE and  $\text{NH}_3$  yield of 20.82% and  $32.33 \mu\text{g h}^{-1} \text{ mg}^{-1}$  at  $-0.65 \text{ V}$ , respectively.<sup>197</sup> Two different types of bonded P atoms were present in PG, namely P-O and P-C, with an atomic percent of 0.47 wt%. The DFT calculation showed that the O functional group prefers to adsorb on P than the OH functional group energetically. Therefore, the O functional group is considered to be active for ENRR, and  $\text{N}_2$  adsorbs preferentially at the C site adjacent to the P-O bonding. This study also revealed that the PDS is  $^*\text{N}_2$  to  $^*\text{NNH}$  hydrogenation. Song *et al.* modified reduced graphene oxide (rGO) with tannic acid (TA) and studied the ENRR.<sup>206</sup> TA-rGO showed a yield rate and FE of  $17.02 \mu\text{g h}^{-1} \text{ mg}^{-1}$  and 4.83% at  $-0.75 \text{ V}$ , respectively. Qiu *et al.* reported boron carbide ( $\text{B}_4\text{C}$ ) nanosheets as an electrocatalyst for ENRR with an  $\text{NH}_3$  yield rate of  $26.57 \mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$  and a FE of 15.95% at  $-0.75 \text{ V}$ .<sup>196</sup> The  $\text{N}_2$  atom adsorption on the  $\text{B}_4\text{C}$  nanosheets (110) follows either end-on terminal N atom adsorption or adsorption to the adjacent  $\text{B}_4\text{C}$  site. Both configurations show a similar energy profile for  $\text{N}_2$  adsorption on the  $\text{B}_4\text{C}$  nanosheet. Free energy calculations showed that hydrogenation of  $^*\text{NN}$  to  $^*\text{NH}_2\text{NH}_2$  proceeds almost without a barrier. The  $^*\text{NH}_2-^*\text{NH}_2 \rightarrow ^*\text{NH}_2 + ^*\text{NH}_3$  step is the rate-limiting step of the ENRR on the  $\text{B}_4\text{C}(110)$  surface, which requires a free energy of 0.34 eV at a potential of 0 V.

Liu *et al.* developed a metal-free F-doped carbon catalyst by introducing F atoms into a 3D porous carbon framework for ENRR.<sup>207</sup> The F-doped carbon catalyst exhibited the highest FE of 54.8% for  $\text{NH}_3$  at  $-0.2 \text{ V}$ , which is 3.0 times higher than that



of pristine carbon frameworks (18.3%), and a yield rate of  $197.7 \mu\text{g}_{\text{NH}_3} \text{mg}_{\text{cat}}^{-1} \text{h}^{-1}$  at  $-0.3 \text{ V}$ . The improved performance of the F-doped carbon catalyst is due to the binding strength of  $\text{N}_2$  which facilitates dissociation of  $\text{N}_2$  into  $^*\text{N}_2\text{H}$  as revealed by mechanistic studies. Due to the different electronegativity between the F and C atoms, a Lewis acid site is created when the F atom is bonded to the C atom. As a result, the HER activity is suppressed significantly. On the other hand, the selectivity of  $\text{N}_2$  electroreduction into  $\text{NH}_3$  is enhanced because of the repulsive interaction between the Lewis acid site and proton  $\text{H}^+$ .<sup>207</sup> Wang and co-workers identified oxygen-doped graphene (O-G) derived from sodium gluconate as a new promising catalyst for the effective production of  $\text{NH}_3$  by catalyzing ambient electro-hydrogenation of  $\text{N}_2$ .<sup>208</sup> They obtained a sizable  $\text{NH}_3$  yield of  $21.3 \mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$  at  $-0.55 \text{ V}$  (vs. RHE) and a high FE of 12.6% at  $-0.45 \text{ V}$  in  $0.1 \text{ M HCl}$  solution with electrochemical and structural durability. The DFT calculations revealed that the  $\text{C}=\text{O}$  and  $\text{O}-\text{C}=\text{O}$  groups primarily contributed to the catalytic mechanism of ENRR as compared to the  $\text{C}-\text{O}$  group. Xia *et al.* reported sulfur-doped graphene (S-G) as an electrocatalyst towards ENRR under ambient conditions.<sup>209</sup> In  $0.1 \text{ M HCl}$ , an  $\text{NH}_3$  yield of  $27.3 \mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$  at  $-0.6 \text{ V}$  (vs. RHE) and a high FE of 11.5% at  $-0.5 \text{ V}$  (vs. RHE), which are significantly higher compared to the undoped graphene catalyst ( $6.25 \mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$ ; 0.52%), were achieved. The ENRR mechanism was further explored by DFT calculations, which revealed that carbon atoms nearest to substituted sulfur atoms act as underlying active sites for the ENRR on S-G. Further, they prepared S doped carbon nanospheres (S-CNSs) as an electrocatalyst with excellent selectivity towards ENRR, demonstrating an  $\text{NH}_3$  yield of  $19.07 \mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$  and a FE of 7.47% at  $-0.7 \text{ V}$  in a  $0.1 \text{ M Na}_2\text{SO}_4$  electrolyte.<sup>210</sup> The S-doped CNS showed much higher catalytic activity than that of the undoped CNS ( $3.70 \mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$ , 1.45%) which is similar to the previous discussion.<sup>209</sup> Importantly, this S-CNS catalyst also showed high stability for ambient  $\text{N}_2$  to  $\text{NH}_3$  conversion.

Cheng *et al.* adopted a novel one-step synthesis protocol to synthesize defect-rich S and N co-doped carbon cloth (CC) by using ammonium persulfate (APS) as the source of nitrogen and sulfur. The S/N co-doped CC catalyst, prepared at  $800^\circ\text{C}$  (CC-APS 800), exhibited a higher number of defects and heteroatom sites and acted as an active and stable electrocatalyst for ENRR with an  $\text{NH}_3$  yield of  $9.87 \times 10^{-10} \text{ mol s}^{-1} \text{cm}^{-2}$  and a FE of 8.11% at  $-0.3 \text{ V}$  in  $0.05 \text{ M H}_2\text{SO}_4$  solution.<sup>211</sup> Kong *et al.* synthesized B and N co-doped porous carbon nanofibers (B/N-CNf)s that exhibited much higher electrocatalytic performance than the only N- or B-doped carbon materials towards ENRR with a FE of 13.2% at  $-0.5 \text{ V}$  and an  $\text{NH}_3$  yield of  $32.5 \text{ mg h}^{-1} \text{mg}_{\text{cat}}^{-1}$  at  $-0.7 \text{ V}$  in an alkaline electrolyte. The synergistic effect of the B-N bond enhances the ENRR process, where N atoms increase the electronic conductivity and B atoms enhance the adsorption of  $\text{N}_2$  and charge transfer.<sup>212</sup> Boron and nitrogen dual-doped carbon nanospheres (BNC-Ns), prepared by another group, exhibited ENRR activity with an  $\text{NH}_3$  yield rate of  $15.7 \mu\text{g}_{\text{NH}_3} \text{h}^{-1} \text{mg}_{\text{cat}}^{-1}$  and a FE of 8.1% at  $-0.4 \text{ V}$  (vs. RHE) in a  $0.05 \text{ M H}_2\text{SO}_4$  electrolyte.<sup>213</sup>

**Table 3** Summary of phosphide, nitride, carbide, sulfide, and metal-free (heteroatom doped carbon) ENRR electrocatalysts reported in recent years and their catalytic performance

Catalyst	Electrolyte	Temperature	Yield rate ( $\mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$ )	FE (%)	Potentials vs. RHE (V)	Ref.
BP	HCl	Ambient	26.42	12.7	-0.60	215
CoP	KOH	Ambient	10.78	0.03	-0.4	216
AuPdP	$\text{Na}_2\text{SO}_4$	Ambient	18.78	15.44	-0.3	217
Mo-FeP	HCl	Ambient	13.1	—	-0.3	218
				7.49	-0.2	
Fe-Ni <sub>2</sub> P	HCl	Ambient	88.51	7.92	-0.3	219
BN	HCl	Ambient	22.4	4.7	-0.75	220
FeS <sub>2</sub>	$\text{Li}_2\text{SO}_4$	Ambient	11.5	14.6	-0.2	221
O-doped carbon	HCl	Ambient	18.03	—	-0.55	222
				10.3	-0.45	
B-N enriched carbon	KCl	Ambient	7.75	13.79	-0.3	223
N,P-co-doped carbon	HCl	Ambient	1.08	0.0754	-0.1	224

Recently, Zhang *et al.* reported a rationally synthesized boron, nitrogen, and fluorine ternary-doped carbon (BNFC) from the carbonization of cigarette butts saturated with the ionic liquid 1-butyl-3-methylimidazolium tetrafluoroborate ( $\text{C}_8\text{H}_{15}\text{N}_2\text{BF}_4$ ).<sup>214</sup> In this case, the high electrocatalytic activity toward the ENRR was due to the capability of N atoms in BNFC for the adsorption of hydrogen ions while the adjacent B or F heteroatoms offered Lewis acid sites for chemisorption of  $\text{N}_2$ . An  $\text{NH}_3$  yield rate of  $41 \text{ mg}_{\text{NH}_3} \text{h}^{-1} \text{mg}_{\text{cat}}^{-1}$  and a FE of 14% at  $-0.4 \text{ V}$  (vs. RHE) in a  $0.05 \text{ M H}_2\text{SO}_4$  electrolyte were recorded for BNFC electrocatalysts. However, in a  $0.1 \text{ M NaOH}$  electrolyte, a relatively high  $\text{NH}_3$  yield rate of  $39 \text{ mg}_{\text{NH}_3} \text{h}^{-1} \text{mg}_{\text{cat}}^{-1}$  with a FE of 16% at  $-0.4 \text{ V}$  (vs. RHE) was achieved. This is due to the capability of water dissociation and adsorption of generated protons by the doped nitrogen atoms present in BNFC electrocatalysts.<sup>214</sup>

Table 3 presents the ENRR performance of recently reported metal phosphide, nitride, carbide, sulfide, and metal-free electrocatalysts, indicating their potential.

## 12. Effect of electrolytes

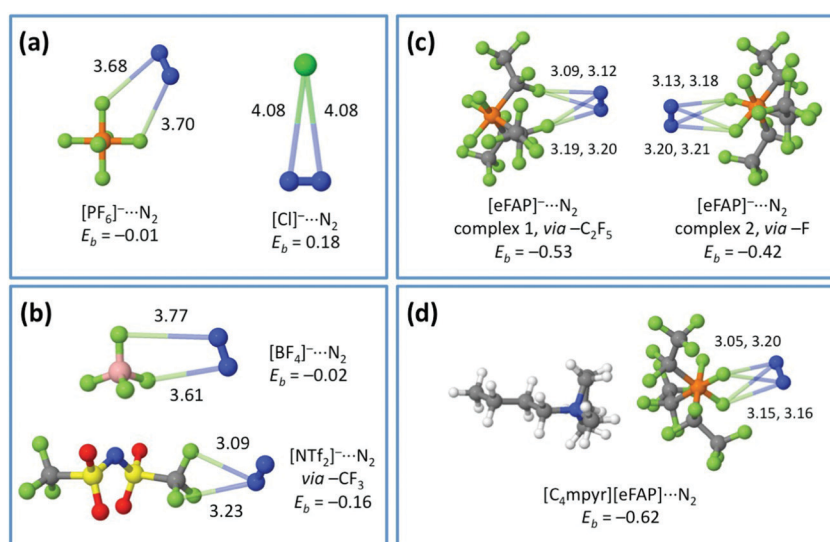
To achieve ENRR activity with high FEs, several other factors are needed to be considered to tackle the challenges in addition to suppressing the competing HER. In particular, besides having an efficient electrocatalyst, the choice of a suitable electrolyte (in terms of ions and pH) is one of the fundamentally important factors to enhance ENRR activity. For instance, acidic, neutral, and alkaline electrolytes have been tested taking into consideration pH adjustment. The pH value for ENRR systems is needed to be well adjusted using dilute  $\text{H}_2\text{SO}_4$ ,  $\text{HCl}$ ,  $\text{Na}_2\text{SO}_4$ ,  $\text{KHCO}_3$ , and  $\text{KOH}$  aqueous solutions. Chen *et al.* tested ENRR using a 30%  $\text{Fe}_2\text{O}_3$ -CNT electrocatalyst in different electrolytes with different pH values at a constant potential.<sup>225</sup> The highest  $\text{NH}_3$  yield rate of  $1.06 \times 10^{-11} \text{ mol cm}^{-2} \text{s}^{-1}$  was obtained in the  $0.5 \text{ M KOH}$  electrolyte, which was higher than that obtained in





0.25 M  $\text{KHSO}_4$  ( $7.87 \times 10^{-12} \text{ mol cm}^{-2} \text{ s}^{-1}$ ). In acidic electrolytes, due to the higher proton concentration, HER is significantly increased and thereby suppressing ENRR. In contrast, HER activity is significantly reduced in alkaline electrolytes. Recently, the effective suppression of HER activities was found for the ENRR using the neutral phosphate buffer solution (PBS) electrolyte.<sup>53,226</sup> PBS has a higher barrier for mass and charge transfer, which prohibits HER kinetics. Upon using Pd/C as an electrocatalyst, the authors were able to obtain a FE of 2.4% in 0.1 M PBS (pH = 7.2) as compared to <0.1% with 0.05 M  $\text{H}_2\text{SO}_4$  (pH = 1.2) and 0.1 M NaOH (pH = 12.9) electrolytes.<sup>53</sup> All these electrolytes were Ar-saturated. Zhang *et al.* showed a higher ENRR selectivity and a FE of 1.17% with  $\text{MoS}_2/\text{CC}$  in 0.1 M  $\text{Na}_2\text{SO}_4$  as compared to 0.09% in 0.1 M HCl due to the strong HER activity of the latter.<sup>182</sup> Moreover, to suppress HER and increase  $\text{N}_2$  solubility in the electrolyte, a mixture of water and low-proton (alcohols) solvents was also taken.<sup>227</sup> Kim *et al.* studied the water and 2-propanol (1 : 9, v/v) mixture as an electrolyte along with  $\text{H}_2\text{SO}_4$  as the supporting electrolyte.<sup>228</sup> The mixed solvent gave rise to a FE of 0.89% as compared to 0.07% for pure water. The observed result is far from being optimal as the FE could not exceed more than 1%. Alkali metal ions are also known to suppress the HER and have a strong ability to interact with molecular  $\text{N}_2$  in an electrolyte. Selection of counterions in the aqueous electrolyte was found to have a significant role with an order of  $\text{Li}^+ > \text{Na}^+ > \text{K}^+$  in terms of  $\text{NH}_3$  yield rate, which suggests a most favourable role of the smallest counterions. The steric effect and the relatively strong interaction between counterions and  $\text{N}_2$  play important roles in ENRR.<sup>35,229</sup> To enhance the FE, 0.1 M LiCl/ethylenediamine (EDA) and 0.05 M  $\text{H}_2\text{SO}_4$  solution were used as an electrolyte in the cathode and anode compartment, respectively, to study the effect of EDA towards ENRR. A much higher FE of 17.2% was obtained under ambient

conditions under this condition, possibly due to the wide electrochemical window of EDA in the negative potential region.<sup>230</sup> Similarly, a mixture of water/alcohols and aprotogenic (tetrahydrofuran, dimethyl sulfoxide) solvents were used as an electrolyte for ENRR.<sup>231,232</sup> In this regard, Lee *et al.* used a hydrophobic MOF (ZIF) coated Ag–Au catalyst to accumulate  $\text{N}_2$  molecules at the catalyst surface to suppress competitive HER. A mixed solvent containing ~1% ethanol in dry tetrahydrofuran (THF) was used as an electrolyte to enhance ENRR selectivity. Ag–Au@ZIF showed a FE of  $18 \pm 4\%$  under ambient conditions, far superior to many other ENRR studies having <1% FE at elevated temperature/pressure.<sup>233</sup> Electrolytes consisting of a mixture of water and an ionic liquid (IL) were also reported.<sup>234,235</sup> MacFarlane and co-workers reported a combination of hydrophobic and high nitrogen-solubility IL electrolytes, namely  $[\text{C}_4\text{mpyr}][\text{eFAP}]$ ,  $[\text{P}_{6,6,6,14}][\text{eFAP}]$ , and  $[\text{HMIM}][\text{NTf}_2]$ , as electrolytes and tested ENRR using a nanostructured Fe-based electrocatalyst.<sup>236</sup> The Fe-based catalyst deposited on a FTO substrate in the presence of  $[\text{P}_{6,6,6,14}][\text{eFAP}]$  showed the highest FE of 60%, which is much higher than that obtained with  $[\text{C}_4\text{mpyr}][\text{eFAP}]$  (30%) and  $[\text{HMIM}][\text{NTf}_2]$  (0.64%). The high efficiency with  $[\text{P}_{6,6,6,14}][\text{eFAP}]$  is attributed to the high solubility of  $\text{N}_2$  in ILs due to the strong interaction between  $\text{N}_2$  and the IL as confirmed by the DFT calculations. The DFT calculation suggests that the  $\text{N}_2$  molecules interact with ions such as  $\text{Cl}^-$  and fluorinated anions  $\text{BF}_4^-$  and  $\text{PF}_6^-$  weakly, whereas they strongly interact with  $[\text{eFAP}]^-$ . Two modes of favourable interactions were identified, namely in complex 1, the  $\text{N}_2$  atoms interact with the F atoms of the alkaline chains, and in complex 2, the  $\text{N}_2$  atoms interact with F atoms bonded with phosphorus as presented in Fig. 12. The  $\text{N}_2$  binding energy depends strongly on the delocalization of the negative charge. The interaction further increases with the addition of the cation.<sup>236</sup>



**Fig. 12** (a)–(c)  $\text{N}_2$  binding energies (in  $\text{kcal mol}^{-1}$ ) and bond distances in Å for various anions. The interaction with  $[\text{eFAP}]^-$  in panel (c) shows two distinct modes: complex 1 exhibits C–F interactions and complex 2 exhibits P–F interactions. Panel (d) introduces the cation to show the interaction with an ion pair of  $[\text{C}_4\text{mpyr}][\text{eFAP}]$ ; the interaction is the strongest of all those studied. Reproduced with permission from ref. 236. Copyright 2017, RSC.



Licht *et al.* used a molten hydroxide suspension of nano- $\text{Fe}_2\text{O}_3$  named the NaOH–KOH eutectic electrolyte, which showed high rates of ammonia generation upon addition of nano- $\text{Fe}_2\text{O}_3$  at modest temperatures of 200–250 °C.<sup>5</sup> As per the recent reports on ENRR, electrolytes play a vital role in HER suppression and enhancement of ENRR. Nevertheless, more experimental and theoretical studies could further improve ENRR under ambient conditions.

### 12.1 Lithium-mediated $\text{N}_2$ reduction reaction

As mentioned in the previous section, not only the catalyst but also the electrolyte plays an important role in ENRR. Among the different electrolytes tested for ENRR, a lithium-mediated ENRR is found to be the most promising one. Typically the lithium-mediated ENRR is performed in tetrahydrofuran solvent that can dissolve a high amount of  $\text{N}_2$  (as high as  $\sim 6$  mM) at 25 °C. The mechanism of Li-mediated  $\text{N}_2$  reduction is hypothesized as the reduction of  $\text{Li}^+$  ions in the presence of  $\text{N}_2$  forming lithium nitride ( $\text{Li}_3\text{N}$ ) at the cathode. The  $\text{Li}_3\text{N}$  species react with a proton source and produce  $\text{NH}_3$ . Ethanol has been used as a proton source for nitride to  $\text{NH}_3$  conversion. In 1994, Tsuneto *et al.* reported a Li-mediated ammonia synthesis with a yield rate of  $\sim 2$  to  $4$   $\text{nmol s}^{-1} \text{cm}^{-2}$  at 50 bar of  $\text{N}_2$  pressure.<sup>231</sup> McEnaney *et al.* experimentally proposed Li-recycling as a tool to produce  $\text{NH}_3$  using renewable energy.<sup>237</sup> First, a highly active Li metal surface was synthesized from LiOH electrolysis in a proton-free environment and then exposed to  $\text{N}_2$  to form  $\text{Li}_3\text{N}$ . Suryanto *et al.* recently demonstrated a phosphonium based cation such as trihexyltetradecylphosphonium ( $[\text{P}_{6,6,6,14}]^+$ ) as a proton source for lithium-mediated  $\text{NH}_3$  synthesis.<sup>238</sup>  $[\text{P}_{6,6,6,14}]^+$  is known to have excellent thermal, chemical, and electrochemical durability. The schematic reaction of electrochemical synthesis of  $\text{NH}_3$  is presented in Fig. 13. Herein, electrochemically generated  $\text{Li}_3\text{N}$  is reacted with the phosphonium cation to produce  $\text{NH}_3$  and form a ylide as a derivative. The original phosphonium cation is

regenerated from the protonation of phosphonium ylide which is a strong base. The author and his group have achieved the best performance at  $-0.75$  V *versus*  $\text{Li}^{0/+}$  with  $\text{N}_2$  to  $\text{NH}_3$  conversion FE as high as  $69 \pm 7\%$  and an  $\text{NH}_3$  yield rate of  $58 \pm 14$   $\text{nmol s}^{-1} \text{cm}^{-2}$ , at an average current density of about  $-22.5$   $\text{mA cm}^{-2}$ . The high reduction potential for the generation of the Li plate simultaneously leads to degradation of the electrode interface over time. The continuous regeneration from the Li salt thus limits the scalability of the process. Moreover, Schwalbe *et al.* observed the development of a solid electrolyte interface (SEI) layer as well as the accumulation of lithium and lithium-containing species at the electrode surface.<sup>239</sup> In this regard, Andersen *et al.* succeeded in developing a stable cycle of Li-mediated NRR through the implementation of the pulse deposition strategy as presented in Fig. 14.<sup>240</sup> Using this method, the authors achieved a FE of  $\sim 30\%$ . They revealed that the SEI layer not only prevents the catalyst from poisoning but also maintains its long-term Li cycling ability. The SEI layer is further found to control the diffusion rate during the electrolysis process.

## 13. Sources of false positives in ENRR and their elimination

Electrochemical  $\text{N}_2$  reduction has gained momentum in recent years due to its potential feasibility under ambient conditions, unlike the Haber–Bosch process. However, the large difference in yield rate and FE raised serious concerns about its actual applicability. Therefore, it is important to evaluate the pitfalls of ENRR, in particular, the inconvenient sources of error and their elimination from ENRR during the estimation of FE and yield rate. The recent developments of the catalyst for ENRR have been discussed in detail in the previous sections. However, a question may arise whether all the catalysts catalyze ENRR under ambient conditions? As we have seen, the conversion rates are in the range of nano or micromolar range with most of the catalysts. Such a low value could be contributed from other sources and/or impurities. For example, Ru is considered as one of the prominent candidates for ENRR in aqueous electrolytes. Theoretical as well as experimental evidence for the same is discussed earlier. However, Andersen *et al.* reported false-positive results with Ru-based catalysts.<sup>241</sup> Interestingly, the same catalyst does not reduce  $\text{N}_2$  at all under ambient conditions in aqueous electrolytes. The author and his group carried out a thorough investigation and revealed that the false-positives arise from  $\text{NO}_x$  impurities present in the  $\text{N}_2$  feed stream. Thus it is very important to eliminate such impurities to find the true nature of the catalyst in ENRR. In this regard, the authors have further proposed modified methods to carry out ENRR as presented in Fig. 15. The readers are urged to go through the modified methods for accurate measurement of  $\text{NH}_3$  production through ENRR using a suitable catalyst. In this regard, Suryanto *et al.* and Choi *et al.* reported excellent perspectives on the steps and missteps made in the ENRR study and suggested the directions to minimize

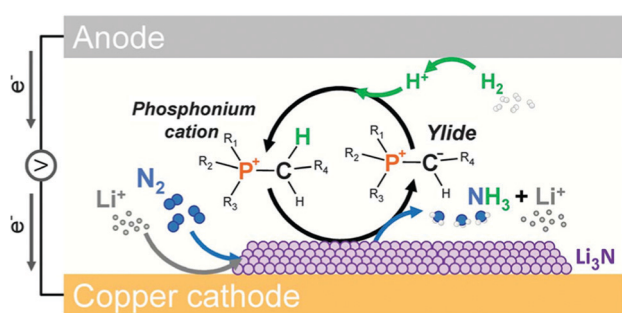


Fig. 13 Schematic illustration of sustainable electrosynthesis of ammonia from  $\text{H}_2$  and  $\text{N}_2$ . The cathode process involves the reduction of  $\text{Li}^+$  to the lithium metal that rapidly reacts with  $\text{N}_2$  to produce  $\text{Li}_3\text{N}$ , which is protonated to release the target product,  $\text{NH}_3$ . The proton carrier is the phosphonium cation, which forms an ylide structure in its deprotonated state; this cycles to the anode where it is regenerated back to the phosphonium form through the reaction with  $\text{H}^+$  derived from the oxidation of  $\text{H}_2$ . Reproduced with permission from ref. 238. Copyright 2021, AAAS.



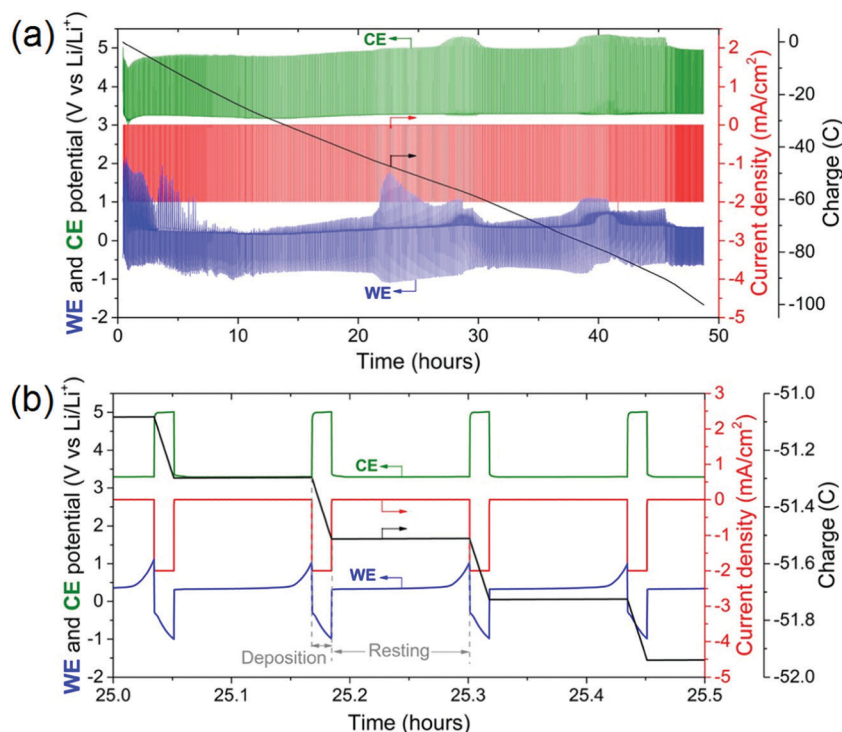


Fig. 14 (a) Cycling method between  $-2.0$  and  $0.0 \text{ mA cm}^{-2}$  (red), for a total of  $100\text{C}$  of charge passed (black). The WE potential (blue) and the CE potential (green) are stable across the entire experiment by varying the resting time. (b) A close-up of the cycling. Immediately after switching to a deposition current, the absolute value of the WE potential increases for the entire  $1 \text{ min}$  duration. When switching back to resting, the WE potential is initially stable just above  $0 \text{ V vs. Li}^+/\text{Li}$ , until it eventually starts becoming anodic after some minutes, suggesting dissolution of all surface Li species that were deposited in the preceding deposition pulse. At this point, another Li depositing pulse is applied. As the experiment did not have constant supervision, there are occasional points where the resting WE potential becomes very positive (e.g. around  $22$  and  $40$  hours) before the deposition pulse is applied. This is simply changed by shortening the resting time. Reproduced with permission from ref. 240. Copyright 2020, RSC.

missteps during the ENRR under ambient conditions.<sup>242,243</sup> A few recent studies thus clearly suggest sources of error for the estimation FE and yield rate of ENRR under ambient conditions in an aqueous electrolyte. It is important to identify such errors and eliminate those for correct measurements of  $\text{NH}_3$  yield and FE. In the following sections, the sources of errors that could potentially provide false positives in ENRR are elaborated.

### 13.1 Nitrogen-containing catalyst

Nitrogen-containing electrocatalysts, especially metal nitrides have been explored as efficient catalysts for ENRR. The mechanism of ENRR is generally explained by the Mars van Krevelen (MvK) mechanism which is discussed earlier. Recently Du *et al.* investigated the ENRR on vanadium nitride (VN) and niobium nitride ( $\text{Nb}_4\text{N}_5$ ) as model electrocatalysts to validate the ENRR at different pH and raised serious questions about the feasibility of these catalysts toward ENRR.<sup>150</sup> The authors revealed that VN and  $\text{Nb}_4\text{N}_5$  do not catalyze  $\text{N}_2$  under ambient conditions. The false-positive for  $\text{NH}_3$  arises from the nitrogen atoms present in the catalyst instead of true ENRR. The N-species present in the catalyst surface may lead to an erroneous conclusion. Therefore, it is important to take necessary precautions to avoid such missteps during ENRR. One simple strategy that could be implemented to avoid and remove the

contaminants from the catalyst is rigorous prewashing and following the pre-treatment method several times before studying the ENRR performance. The obtained pretreatment results must be subtracted from the final FE and yield rate.

### 13.2 Electrolyte

The false-positive detection of  $\text{NH}_3$  can arise from the electrolyte. Li *et al.* reported the identification process and elimination of contamination in an electrolyte which provides the false-positive.<sup>244</sup> The investigation found that a trace amount of nitrate and nitrite salts exist in the lithium-based electrolyte. Thus a significant amount of  $\text{NH}_3$  is produced with excellent reproducibility in the presence of bare electrodes (Ti foil, carbon paper, or copper foam) without loading any catalyst in both  $\text{N}_2$  and Ar-saturated  $\text{Li}_2\text{SO}_4$  solution. The detected  $\text{NH}_3$  arises from the trace amount of nitrate and nitrite present in the electrolyte which is electrochemically reduced to  $\text{NH}_3$  rather than  $\text{N}_2$ . In this regard, the author studied the ENRR using bare Ti foil as the working electrode and  $\text{Li}_2\text{SO}_4$  as the electrolyte. The false ENRR to  $\text{NH}_3$  as measured using the indophenol method is presented in Fig. 16. In particular, an apparent increase in absorbance is found in the experiments performed in both  $\text{N}_2$  and Ar atmospheres, which confirms that the  $\text{NH}_3$  yield is not from ENRR but due to contamination in the electrolyte. To eliminate the  $\text{NO}_x$  contamination from the





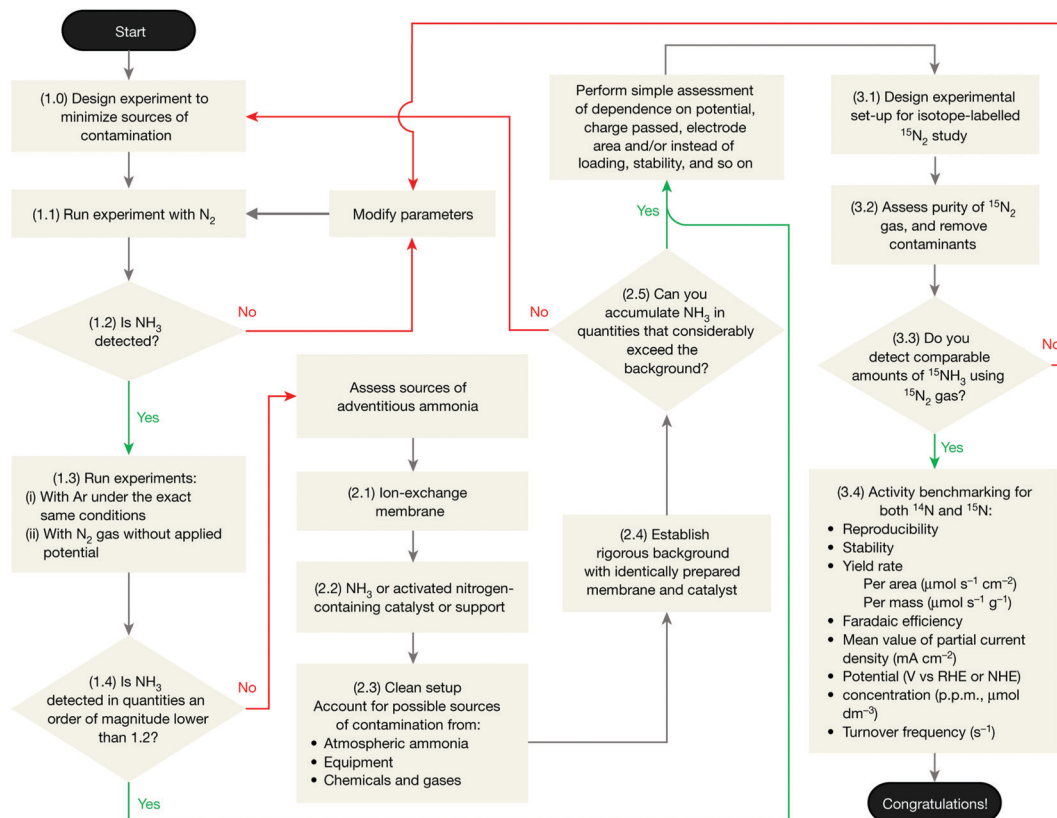


Fig. 15 Suggested protocol for the benchmarking of electrochemical nitrogen reduction. Reproduced with permission from ref. 241. Copyright 2019, Nature Research.

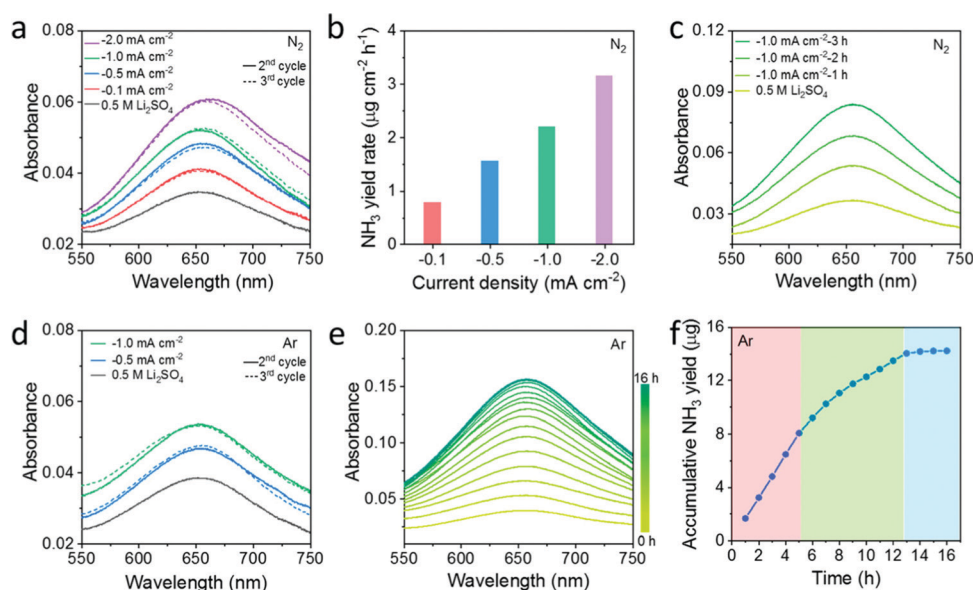


Fig. 16 False positive NRR performance observed in both  $\text{N}_2$  and  $\text{Ar}$  atmospheres using a bare Ti foil without loading any catalyst in a  $0.5 \text{ M Li}_2\text{SO}_4$  solution. (a) UV-Vis spectra for the indophenol blue indicator stained electrolytes after electrolysis at  $-0.1$ ,  $-0.5$ ,  $-1.0$ , and  $-2.0 \text{ mA cm}^{-2}$  in  $\text{N}_2$  for 1 h and (b) the corresponding ammonia yield rates at each current density. (c) UV-Vis spectra for the indophenol blue indicator stained electrolytes after electrolysis at  $-1.0 \text{ mA cm}^{-2}$  in  $\text{N}_2$  for 1, 2, and 3 h. (d) UV-Vis spectra for the indophenol blue indicator stained electrolytes after electrolysis at  $-0.5$  and  $-1.0 \text{ mA cm}^{-2}$  in  $\text{Ar}$  for 1 h. (e) UV-Vis spectra for the indophenol blue indicator stained electrolytes after electrolysis at  $-1.0 \text{ mA cm}^{-2}$  in  $\text{Ar}$  for 1–16 h and (f) the corresponding accumulative ammonia yield. In (a) and (d), the solid lines represent the results for the second cycle and the dashed lines show the results for the third cycle. In (a), (c), (d), and (e), the lowest line shows the result for the fresh electrolyte before electrolysis. Reproduced with permission from ref. 244. Copyright 2019, ACS.



electrolyte, the author annealed the  $\text{Li}_2\text{SO}_4$  salt at  $800^\circ\text{C}$  in an argon atmosphere. After annealing the electrolyte, the  $\text{NH}_3$  yield was found to be significantly reduced. This suggests that the presence of contamination in the electrolyte contributed to  $\text{NH}_3$  formation, thus giving the false-positive test. Therefore it is important to identify the source of contamination in aqueous electrolytes and eliminate it to estimate the correct  $\text{NH}_3$  yield rate.

### 13.3 Membrane separator

Currently, most of the reported ENRR studies are carried out in an H-cell with Nafion membrane as a separator. However, the Nafion membrane can absorb and release  $\text{NH}_3$  during the ENRR as reported by Liu *et al.*<sup>245</sup> This suggests that the Nafion membrane is a possible source of error in the ENRR process. On the other hand, Celgard 3401 and 3501 has poor ability to absorb  $\text{NH}_3$  as compared to Nafion and other membranes and thus must be considered for use in ENRR studies.

### 13.4 Gas purity

The feed gas must be ultrapure and devoid of any atmospheric contamination. The main source of contamination is  $\text{NO}_x$  species present in the  $\text{N}_2$  feed gas ( $^{14}\text{N}_2$  as well as  $^{15}\text{N}_2$ ). Dabundo *et al.* reported that the trace amount of  $\text{NO}_x$  in the  $\text{N}_2$  feedstock is enough to give a false positive test.<sup>246</sup> It must be noted that the electrochemical reduction of  $\text{NO}_x$  species to  $\text{N}_2$  is energetically favourable.<sup>243</sup> Thus enough care must be taken to eliminate any signal due to the contamination in the gas feed. Choi *et al.* suggested  $\text{NO}_x$  scrubbing to eliminate  $\text{NO}_x$  from the  $\text{N}_2$  feed gas.<sup>243</sup> To evaluate the FE and yield rate of  $\text{NH}_3$ , it is thus necessary to subtract the background signal from the ENRR signal obtained in the presence of  $\text{N}_2$ .

### 13.5 Background subtraction

To eliminate false positives from the experimental results, it is necessary to perform control experiments at open circuit potential and in the absence/presence of a catalyst in the absence and presence of  $\text{Ar}/\text{N}_2$ . The control experiments will provide clarity on the actual performance of the catalyst. However, many studies either ignore or do not perform sufficient and satisfactory control experiments.<sup>242,243</sup> This leads to potential errors in the assessment of the FE and yield rate of ENRR. Likewise, some reports have presented control experiments where the background  $\text{NH}_3$  is significant, and thus it cannot be ignored.<sup>242,243</sup> Therefore the researchers are suggested to perform control experiments as prescribed above to eliminate the potential error from the results.

## 14. Conclusions

For a sustainable global energy economy, persistent effort is needed through research and development to generate products from renewable resources through different strategies. The present context reveals that ENRR could serve as a potential alternative to synthesize  $\text{NH}_3$  against the conventional

fossil fuel-based energy economy even though ENRR is an energy-intensive reaction. In the present review, we have detailed the roles of the electrocatalysts in facilitating the ENRR at room temperature, which is the ultimate goal of the scientific community. To date, noble metal electrocatalysts such as Pd, Au, and Ru along with a few non-noble metal electrocatalysts have exhibited promising ENRR efficiency while keeping a lot of space for further improvement. This review highlights several key aspects that are important to develop efficient catalysts while taking into account the key features that control the catalyst efficiency and selectivity including nicks, steps, facets, porosity, and coordination number of the surface atoms. Designing nanostructured electrocatalysts with an optimized surface structure facilitates  $\text{N}_2$  adsorption and thereby ENRR. In particular, nanostructuring increases the active site density with a specific structure. To obtain enormous active sites on the catalyst surface, various synthesis routes have been developed in recent years. Furthermore, to improve the mass transport kinetics across the electrode/electrolyte interface, the catalyst can be anchored on a suitable support material, which allows minimal use of the catalyst while improving the product yield. Herein, we summarize the key achievements in catalyst development for ENRR.

(1) The catalytic activity significantly increases especially for the single atomic electrocatalyst supported and/or stabilized by the N-site over the pure bulk catalyst. The single atomic catalyst site at the surface is coordinated by different numbers of N-sites, which act as active sites to control the  $\text{N}_2$  reduction kinetics steps. The metal to N site coordination number strongly influences the rate-limiting step for ENRR.

(2) The oxygen vacancy in the oxide-based catalysts intrinsically enhances the catalytic conversion rate of  $\text{N}_2$  to  $\text{NH}_3$ . The oxygen vacant site of the catalysts plays a predominant role in the activation of  $\text{N}_2$  during the progression of the reaction and hence decreases the activation energy barrier for ENRR.

(3) Doping is another approach to obtain efficient catalysts that generate active sites for ENRR. The doping sites facilitate the adsorption as well as activation of  $\text{N}_2$ .

(4) Support materials integrated with catalysts play a crucial role in the suppression of HER. Especially, carbon shelling around the catalyst is found to play a prominent role in suppressing HER activity at the catalyst surface under a potential and facilitate the ENRR. Support materials also increase the catalyst distribution in the synthesis process and enhance mass transfer kinetics during the electrolysis process.

## 15. Challenges

Although impressive progress has been made in ENRR, there are still several major challenges that need to be addressed for the commercialization of the process. One of the major challenges associated with ENRR is the yield rate and FE. So far, the yield rate and FE are not up to the mark. In particular, the yield rate is mostly in micrograms per hour per milligram of catalyst or per centimetre square and FE is mostly less than 10% with a



few exceptions. Therefore, more efforts are needed for the enhancement of the yield rate and FE of ENRR. The requirement of higher negative potential for ENRR is another major obstacle that is associated with HER with almost every catalyst. Thus, efficient electrocatalysts must be explored which could show ENRR at lower negative potentials to make it viable for commercial application. Hence, efforts should be directed to suppress the HER activity while increasing the FE of the catalyst for ENRR. The theoretical calculation provides a certain model to mitigate HER; however, the feasibility of this active model is still unclear. Identification of suitable electrolytes is another feature that can increase the solubility of  $N_2$  while reducing the mass transport for HER and thereby increase the ENRR efficiency. Another important challenge associated with ENRR is measuring the evolved  $NH_3$  through the ENRR correctly and precisely. Considering a very small yield of  $NH_3$  (in microgram quantity per hour) through ENRR, it could be from other sources such as the atmosphere, supplied  $N_2$ , and nitrogen-containing chemicals or catalysts used in ENRR. Among these, the supplied  $N_2$  source is the main source of error as it often contains  $NO_x$  species that are easily reducible to  $NH_3$ . Similarly, nitrogen-containing catalysts and electrolytes are other potential sources of  $NH_3$  release through ENRR. Thus precautions must be taken to avoid these errors which show erroneous results. Furthermore, the most commonly used indophenol blue method is not suitable for low  $NH_3$  yield measurement. For detecting small quantities of  $NH_3$  yield, the need for sophisticated spectroscopy techniques including isotope labelling is another challenge. To meet these challenges more attention is required from the scientific community.

## 16. Future directions

As highlighted in the previous sections, the development of catalysts, effective methods of measurement, and improvement of  $NH_3$  yield are the immediate needs to make progress in realizing the ENRR in future. Although several electrocatalysts have been studied and they were suitably modified, the research on the same remains not substantial. In particular, the small-sized or single atomic catalytic centre could be a possible candidate to increase the active sites drastically and thus increase the  $NH_3$  yield and FE. The synthesis of desired reactive facets and forming uniform defects such as oxygen vacancies appear to be a couple of promising strategies for the development of catalysts for ENRR. Not only an electrocatalyst but also an appropriate electrolyte is another important aspect to make the ENRR process practically viable. The theoretical investigation along with experimental study can rationalize the ENRR and provide further insights to improve the performance. As ENRR is a more complex process than the HER and not well understood at the molecular level, computational studies could be highly beneficial. Considering that the active intermediates form during the ENRR, the role of the active site in the stabilization of active intermediates remains ambiguous. Some investigations suggested that the  $N_2$  adsorption ability of the

catalyst is the key step whereas others suggested that coordinately unsaturated atoms are primarily responsible. Therefore, further experimental as well as theoretical investigation is necessary to understand the active species of the catalysts under the given conditions. The adsorption of  $N_2$  and electron-coupled proton transfer to adsorbed  $N_2$  are energetically uphill processes. Therefore, *in situ* measurements could provide clues to precisely identify the active site for ENRR. Finally, it is very important to follow the correct steps to measure the effective reduction of  $N_2$  to  $NH_3$  and measure the evolved  $NH_3$  accurately. The possible sources of  $NH_3$  contamination must be avoided and appropriate spectroscopic techniques must be followed to measure the low yield  $NH_3$ . In summary, the ENRR to form  $NH_3$  has strong potential for the production of fertilizer and for use as an energy carrier after addressing the shortcomings which might take a few years from now. If progress is made in the right direction, reduction of  $N_2$  to  $NH_3$  will significantly reduce the global energy demand and carbon emission.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

This study was supported by the Science and Engineering Research Board (SERB), New Delhi, India, through the research grant EMR/2017/000697.

## References

- 1 K. Honkala, A. Hellman, I. N. Remediakis, A. Logadottir, A. Carlsson, S. Dahl, C. H. Christensen and J. K. Nørskov, *Science*, 2005, **307**, 555–558.
- 2 S.-J. Li, D. Bao, M.-M. Shi, B.-R. Wulan, J.-M. Yan and Q. Jiang, *Adv. Mater.*, 2017, **29**, 1700001.
- 3 G. Deng, T. Wang, A. A. Alshehri, K. A. Alzahrani, Y. Wang, H. Ye, Y. Luo and X. Sun, *J. Mater. Chem. A*, 2019, **7**, 21674–21677.
- 4 S. Dahl, E. Törnqvist and I. Chorkendorff, *J. Catal.*, 2000, **192**, 381–390.
- 5 K. Chu, Y.-P. Liu, J. Wang and H. Zhang, *ACS Appl. Energy Mater.*, 2019, **2**, 2288–2295.
- 6 J. Deng, J. A. Iñiguez and C. Liu, *Joule*, 2018, **2**, 846–856.
- 7 A. Chen and B. Y. Xia, *J. Mater. Chem. A*, 2019, **7**, 23416–23431.
- 8 X. Wen and J. Guan, *Nanoscale*, 2020, **12**, 8065–8094.
- 9 X. Guo, H. Du, F. Qu and J. Li, *J. Mater. Chem. A*, 2019, **7**, 3531–3543.
- 10 M. A. Shipman and M. D. Symes, *Catal. Today*, 2017, **286**, 57–68.
- 11 X. Chen, Y. Guo, X. Du, Y. Zeng, J. Chu, C. Gong, J. Huang, C. Fan, X. Wang and J. Xiong, *Adv. Energy Mater.*, 2020, **10**, 1903172.





- 12 J. Wang, Y. Liu, H. Zhang, D. Huang and K. Chu, *Catal. Sci. Technol.*, 2019, **9**, 4248–4254.
- 13 X.-F. Li, Q.-K. Li, J. Cheng, L. Liu, Q. Yan, Y. Wu, X.-H. Zhang, Z.-Y. Wang, Q. Qiu and Y. Luo, *J. Am. Chem. Soc.*, 2016, **138**, 8706–8709.
- 14 E. Skúlason, T. Bligaard, S. Gudmundsdóttir, F. Studt, J. Rossmeisl, F. Abild-Pedersen, T. Vegge, H. Jónsson and J. K. Nørskov, *Phys. Chem. Chem. Phys.*, 2012, **14**, 1235–1245.
- 15 Y. Abghoui, A. L. Garden, J. G. Howalt, T. Vegge and E. Skúlason, *ACS Catal.*, 2016, **6**, 635–646.
- 16 J. Nash, X. Yang, J. Anibal, M. Dunwell, S. Yao, K. Attenkofer, J. G. Chen, Y. Yan and B. Xu, *J. Phys. Chem. C*, 2019, **123**, 23967–23975.
- 17 Y. Yao, S. Zhu, H. Wang, H. Li and M. Shao, *Angew. Chem., Int. Ed.*, 2020, **59**, 10479–10483.
- 18 H. Xian, H. Guo, Z. Chen, G. Yu, A. A. Alshehri, K. A. Alzahrani, F. Hao, R. Song and T. Li, *ACS Appl. Mater. Interfaces*, 2020, **12**, 2445–2451.
- 19 R. Lan, J. T. S. Irvine and S. Tao, *Sci. Rep.*, 2013, **3**, 1145.
- 20 R. Lan and S. Tao, *RSC Adv.*, 2013, **3**, 18016–18021.
- 21 J. Nash, X. Yang, J. Anibal, J. Wang, Y. Yan and B. Xu, *J. Electrochem. Soc.*, 2017, **164**, F1712.
- 22 L. Sheets and G. G. Botte, *Chem. Commun.*, 2018, **54**, 4250–4253.
- 23 K. Kugler, M. Luhn, J. A. Schramm, K. Rahimi and M. Wessling, *Phys. Chem. Chem. Phys.*, 2015, **17**, 3768–3782.
- 24 H.-M. Liu, S.-H. Han, Y. Zhao, Y.-Y. Zhu, X.-L. Tian, J.-H. Zeng, J.-X. Jiang, B. Y. Xia and Y. Chen, *J. Mater. Chem. A*, 2018, **6**, 3211–3217.
- 25 T. Chen, S. Liu, H. Ying, Z. Li and J. Hao, *Chem. – Asian J.*, 2020, **15**, 1081–1087.
- 26 T. Xiao, J. Huang, D. Wang, T. Meng and X. Yang, *Talanta*, 2020, **206**, 120210.
- 27 J. Zeng, Q. Zhang, J. Chen and Y. Xia, *Nano Lett.*, 2010, **10**, 30–35.
- 28 Y. Yu, F. Cui, J. Sun and P. Yang, *Nano Lett.*, 2016, **16**, 3078–3084.
- 29 R. Omar, A. En Naciri, S. Jradi, Y. Battie, J. Toufaily, H. Mortada and S. Akil, *J. Mater. Chem. C*, 2017, **5**, 10813–10821.
- 30 M. M. Shi, D. Bao, B. R. Wulan, Y. H. Li, Y. F. Zhang, J. M. Yan and Q. Jiang, *Adv. Mater.*, 2017, **29**, 1606550.
- 31 D. Bao, Q. Zhang, F.-L. Meng, H.-X. Zhong, M.-M. Shi, Y. Zhang, J.-M. Yan, Q. Jiang and X.-B. Zhang, *Adv. Mater.*, 2017, **29**, 1604799.
- 32 Z. Wang, Y. Li, H. Yu, Y. Xu, H. Xue, X. Li, H. Wang and L. Wang, *ChemSusChem*, 2018, **11**, 3480–3485.
- 33 K. Zhang, R. Guo, F. Pang, J. He and W. Zhang, *ACS Sustainable Chem. Eng.*, 2019, **7**, 10214–10220.
- 34 C. Chen, C. Liang, J. Xu, J. Wei, X. Li, Y. Zheng, J. Li, H. Tang and J. Li, *Electrochim. Acta*, 2020, **335**, 135708.
- 35 M. Nazemi, S. R. Panikkanvalappil and M. A. El-Sayed, *Nano Energy*, 2018, **49**, 316–323.
- 36 Q. Qin, T. Heil, M. Antonietti and M. Oschatz, *Small Methods*, 2018, **2**, 1800202.
- 37 J. Zheng, Y. Lyu, M. Qiao, J. P. Veder, R. D. Marco, J. Bradley, R. Wang, Y. Li, A. Huang, S. P. Jiang and S. Wang, *Angew. Chem., Int. Ed.*, 2019, **58**, 18604–18609.
- 38 Y. Zhou, F. Che, M. Liu, C. Zou, Z. Liang, P. De Luna, H. Yuan, J. Li, Z. Wang, H. Xie, H. Li, P. Chen, E. Bladt, R. Quintero-Bermudez, T.-K. Sham, S. Bals, J. Hofkens, D. Sinton, G. Chen and E. H. Sargent, *Nat. Chem.*, 2018, **10**, 974–980.
- 39 F. S. Roberts, K. P. Kuhl and A. Nilsson, *Angew. Chem.*, 2015, **127**, 5268–5271.
- 40 J. Fester, A. Makoveev, D. Grumelli, R. Gutzler, Z. Sun, J. Rodríguez-Fernández, K. Kern and J. V. Lauritsen, *Angew. Chem., Int. Ed.*, 2018, **57**, 11893–12073.
- 41 C. Li, Q. Yuan, B. Ni, T. He, S. Zhang, Y. Long, L. Gu and X. Wang, *Nat. Commun.*, 2018, **9**, 3702.
- 42 Z.-H. Xue, S.-N. Zhang, Y.-X. Lin, H. Su, G.-Y. Zhai, J.-T. Han, Q.-Y. Yu, X.-H. Li, M. Antonietti and J.-S. Chen, *J. Am. Chem. Soc.*, 2019, **141**, 14976–14980.
- 43 N. Saadatjou, A. Jafari and S. Sahebdehfar, *Chem. Eng. Commun.*, 2015, **202**, 420–448.
- 44 S. Back and Y. Jung, *Phys. Chem. Chem. Phys.*, 2016, **18**, 9161–9166.
- 45 T. H. Rod, A. Logadottir and J. K. Nørskov, *J. Chem. Phys.*, 2000, **112**, 5343–5347.
- 46 Z. Geng, Y. Liu, X. Kong, P. Li, K. Li, Z. Liu, J. Du, M. Shu, R. Si and J. Zeng, *Adv. Mater.*, 2018, **30**, 1803498.
- 47 Z. Zhang, K. Yao, L. Cong, Z. Yu, L. Qu and W. Huang, *Catal. Sci. Technol.*, 2020, **10**, 1336–1342.
- 48 Y. Yao, H. Wang, X. Yuan, H. Li and M. Shao, *ACS Energy Lett.*, 2019, **4**, 1336–1341.
- 49 A. Liu, M. Gao, X. Ren, F. Meng, Y. Yang, Q. Yang, W. Guan, L. Gao, X. Liang and T. Ma, *Nanoscale*, 2020, **12**, 10933–10938.
- 50 M. Shao, T. Yu, J. H. Odell, M. Jin and Y. Xia, *Chem. Commun.*, 2011, **47**, 6566–6568.
- 51 C. Alegre, A. Stassi, E. Modica, C. Lo Vecchio, A. S. Aricò and V. Baglio, *RSC Adv.*, 2015, **5**, 25424–25427.
- 52 L. Zhang, Q. Chang, H. Chen and M. Shao, *Nano Energy*, 2016, **29**, 198–219.
- 53 J. Wang, L. Yu, L. Hu, G. Chen, H. Xin and X. Feng, *Nat. Commun.*, 2018, **9**, 1795.
- 54 J. Lv, S. Wu, Z. Tian, Y. Ye, J. Liu and C. Liang, *J. Mater. Chem. A*, 2019, **7**, 12627–12634.
- 55 J. Lv, Z. Tian, K. Dai, Y. Ye and C. Liang, *J. Colloid Interface Sci.*, 2019, **553**, 126–135.
- 56 W. Xu, G. Fan, J. Chen, J. Li, L. Zhang, S. Zhu, X. Su, F. Cheng and J. Chen, *Angew. Chem.*, 2020, **132**, 3539–3544.
- 57 H. Wang, Y. Chen, R. Fan, J. Chen, Z. Wang, S. Mao and Y. Wang, *Research*, 2019, **2019**, 1401209.
- 58 P. P. Patel, M. K. Datta, O. I. Velikokhatnyi, R. Kuruba, K. Damodaran, P. Jampani, B. Gattu, P. M. Shanthi, S. S. Damle and P. N. Kumta, *Sci. Rep.*, 2016, **6**, 28367.
- 59 F. Lyu, Q. Wang, S. M. Choi and Y. Yin, *Small*, 2019, **15**, 1804201.
- 60 X. Zou and Y. Zhang, *Chem. Soc. Rev.*, 2015, **44**, 5148–5180.
- 61 S. Mukherjee, X. Yang, W. Shan, W. Samarakoon, S. Karakalos, D. A. Cullen, K. More, M. Wang, Z. Feng, G. Wang and G. Wu, *Small Methods*, 2020, **4**, 1900821.



- 62 W. Zang, T. Yang, H. Zou, S. Xi, H. Zhang, X. Liu, Z. Kou, Y. Du, Y. P. Feng, L. Shen, L. Duan, J. Wang and S. J. Pennycook, *ACS Catal.*, 2019, **9**, 10166–10173.
- 63 Y.-X. Lin, S.-N. Zhang, Z.-H. Xue, J.-J. Zhang, H. Su, T.-J. Zhao, G.-Y. Zhai, X.-H. Li, M. Antonietti and J.-S. Chen, *Nat. Commun.*, 2019, **10**, 4380.
- 64 D. V. Yandulov and R. R. Schrock, *Science*, 2003, **301**, 76–78.
- 65 J. Chen, H. Wang, Z. Wang, S. Mao, J. Yu, Y. Wang and Y. Wang, *ACS Catal.*, 2019, **9**, 5302–5307.
- 66 J. Greeley, T. F. Jaramillo, J. Bonde, I. Chorkendorff and J. K. Nørskov, *Nat. Mater.*, 2006, **5**, 909–913.
- 67 Y.-C. Hao, Y. Guo, L.-W. Chen, M. Shu, X.-Y. Wang, T.-A. Bu, W.-Y. Gao, N. Zhang, X. Su, X. Feng, J.-W. Zhou, B. Wang, C.-W. Hu, A.-X. Yin, R. Si, Y.-W. Zhang and C.-H. Yan, *Nat. Catal.*, 2019, **2**, 448–456.
- 68 J. H. Montoya, C. Tsai, A. Vojvodic and J. K. Nørskov, *ChemSusChem*, 2015, **8**, 2180–2186.
- 69 Q. Hao, C. Liu, G. Jia, Y. Wang, H. Arandiyani, W. Wei and B.-J. Ni, *Mater. Horiz.*, 2020, **7**, 1014–1029.
- 70 L. Li, C. Tang, B. Xia, H. Jin, Y. Zheng and S.-Z. Qiao, *ACS Catal.*, 2019, **9**, 2902–2908.
- 71 Y. Wang, M.-M. Shi, D. Bao, F.-L. Meng, Q. Zhang, Y.-T. Zhou, K.-H. Liu, Y. Zhang, J.-Z. Wang, Z.-W. Chen, D.-P. Liu, Z. Jiang, M. Luo, L. Gu, Q.-H. Zhang, X.-Z. Cao, Y. Yao, M.-H. Shao, Y. Zhang, X.-B. Zhang, J. G. Chen, J.-M. Yan and Q. Jiang, *Angew. Chem., Int. Ed.*, 2019, **58**, 9464–9469.
- 72 L. Xia, W. Fu, P. Zhuang, Y. Cao, M. O. L. Chee, P. Dong, M. Ye and J. Shen, *ACS Sustainable Chem. Eng.*, 2020, **8**, 2735–2741.
- 73 Y. Qiu, S. Zhao, M. Qin, J. Diao, S. Liu, L. Dai, W. Zhang and X. Guo, *Inorg. Chem. Front.*, 2020, **7**, 2006–2016.
- 74 Y. Xu, T. Ren, S. Yu, H. Yu, S. Yin, Z. Wang, X. Li, L. Wang and H. Wang, *Sustainable Energy Fuels*, 2020, **4**, 3334–3339.
- 75 K. Bhunia, M. Chandra and D. Pradhan, *J. Nanosci. Nanotechnol.*, 2018, **19**, 332–355.
- 76 K. Bhunia, S. Khilari and D. Pradhan, *ACS Sustainable Chem. Eng.*, 2018, **6**, 7769–7778.
- 77 H. Wang, Y. Li, C. Li, K. Deng, Z. Wang, Y. Xu, X. Li, H. Xue and L. Wang, *J. Mater. Chem. A*, 2019, **7**, 801–805.
- 78 F. Pang, Z. Wang, K. Zhang, J. He, W. Zhang, C. Guo and Y. Ding, *Nano Energy*, 2019, **58**, 834–841.
- 79 H. Yu, Z. Wang, D. Yang, X. Qian, Y. Xu, X. Li, H. Wang and L. Wang, *J. Mater. Chem. A*, 2019, **7**, 12526–12531.
- 80 J. Wang, B. Huang, Y. Ji, M. Sun, T. Wu, R. Yin, X. Zhu, Y. Li, Q. Shao and X. Huang, *Adv. Mater.*, 2020, **32**, 1907112.
- 81 X. Zhang, T. Wu, H. Wang, R. Zhao, H. Chen, T. Wang, P. Wei, Y. Luo, Y. Zhang and X. Sun, *ACS Catal.*, 2019, **9**, 4609–4615.
- 82 L. Han, X. Liu, J. Chen, R. Lin, H. Liu, F. Lü, S. Bak, Z. Liang, S. Zhao, E. Stavitski, J. Luo, R. R. Adzic and H. L. Xin, *Angew. Chem., Int. Ed.*, 2019, **58**, 2321–2325.
- 83 C. Li, S. Mou, X. Zhu, F. Wang, Y. Wang, Y. Qiao, X. Shi, Y. Luo, B. Zheng, Q. Li and X. Sun, *Chem. Commun.*, 2019, **55**, 14474–14477.
- 84 Y. Liu, L. Huang, X. Zhu, Y. Fang and S. Dong, *Nanoscale*, 2020, **12**, 1811–1816.
- 85 J. Bai, H. Huang, F.-M. Li, Y. Zhao, P. Chen, P.-J. Jin, S.-N. Li, H.-C. Yao, J.-H. Zeng and Y. Chen, *J. Mater. Chem. A*, 2019, **7**, 21149–21156.
- 86 C. Fang, J. Hu, X. Jiang, Z. Cui, X. Xu and T. Bi, *Inorg. Chem. Front.*, 2020, **7**, 1411–1419.
- 87 W. Tong, B. Huang, P. Wang, Q. Shao and X. Huang, *Natl. Sci. Rev.*, 2021, **8**, nwaa088.
- 88 K. Chu, W. Gu, Q. Li, Y. Liu, Y. Tian and W. Liu, *J. Energy Chem.*, 2021, **53**, 82–89.
- 89 N. Zhang, L. Li, J. Wang, Z. Hu, Q. Shao, X. Xiao and X. Huang, *Angew. Chem.*, 2020, **132**, 8143–8148.
- 90 F. Pang, F. Wang, L. Yang, Z. Wang and W. Zhang, *Chem. Commun.*, 2019, **55**, 10108–10111.
- 91 R. D. Kumar, Z. Wang, C. Li, A. V. Narendra Kumar, H. Xue, Y. Xu, X. Li, L. Wang and H. Wang, *J. Mater. Chem. A*, 2019, **7**, 3190–3196.
- 92 J. Guo, H. Wang, F. Xue, D. Yu, L. Zhang, S. Jiao, Y. Liu, Y. Lu, M. Liu, S. Ruan, Y.-J. Zeng, C. Ma and H. Huang, *J. Mater. Chem. A*, 2019, **7**, 20247–20253.
- 93 Z. Wang, C. Li, K. Deng, Y. Xu, H. Xue, X. Li, L. Wang and H. Wang, *ACS Sustainable Chem. Eng.*, 2019, **7**, 2400–2405.
- 94 J. Desilvestro and O. Haas, *J. Electrochem. Soc.*, 1990, **137**, 5C–22C.
- 95 G. Maduraiveeran, M. Sasidharan and W. Jin, *Prog. Mater. Sci.*, 2019, **106**, 100574.
- 96 R. Zhang, X. Ren, X. Shi, F. Xie, B. Zheng, X. Guo and X. Sun, *ACS Appl. Mater. Interfaces*, 2018, **10**, 28251–28255.
- 97 M.-T. Nguyen, N. Seriani and R. Gebauer, *Phys. Chem. Chem. Phys.*, 2015, **17**, 14317–14322.
- 98 X. Wu, L. Xia, Y. Wang, W. Lu, Q. Liu, X. Shi and X. Sun, *Small*, 2018, **14**, 1803111.
- 99 X. Wang, J. Wang, Y. Li and K. Chu, *ChemCatChem*, 2019, **11**, 4529–4536.
- 100 X.-W. Lv, Y. Liu, R. Hao, W. Tian and Z.-Y. Yuan, *ACS Appl. Mater. Interfaces*, 2020, **12**, 17502–17508.
- 101 V. E. Henrich and P. A. Cox, *The Surface Science of Metal Oxides*, Cambridge University Press, Cambridge, 1994.
- 102 C. Fang, T. Bi, X. Xu, N. Yu, Z. Cui, R. Jiang and B. Geng, *Adv. Mater. Interfaces*, 2019, **6**, 1901034.
- 103 B. Li, X. Zhu, J. Wang, R. Xing, Q. Liu, X. Shi, Y. Luo, S. Liu, X. Niu and X. Sun, *Chem. Commun.*, 2020, **56**, 1074–1077.
- 104 Q. Qin, Y. Zhao, M. Schmallegger, T. Heil, J. Schmidt, R. Walczak, G. Gescheidt-Demner, H. Jiao and M. Oschatz, *Angew. Chem., Int. Ed.*, 2019, **58**, 13101–13106.
- 105 H. Huang, F. Gong, Y. Wang, H. Wang, X. Wu, W. Lu, R. Zhao, H. Chen, X. Shi, A. M. Asiri, T. Li, Q. Liu and X. Sun, *Nano Res.*, 2019, **12**, 1093–1098.
- 106 Y. Liu, Y. Li, D. Huang, H. Zhang and K. Chu, *Chem. – Eur. J.*, 2019, **25**, 11933–11939.
- 107 G. Marnellos and M. Stoukides, *Science*, 1998, **282**, 98–100.
- 108 G. Marnellos, S. Zisekas and M. Stoukides, *J. Catal.*, 2000, **193**, 80–87.
- 109 X. Dong, Z. Xu, X. Chang, C. Zhang and W. Jin, *J. Am. Ceram. Soc.*, 2007, **90**, 3923–3929.



- 110 C. Yu and S. B. Adler, *Chem. Mater.*, 2005, **17**, 4537–4546.
- 111 I. A. Amar, R. Lan and S. Tao, *J. Electrochem. Soc.*, 2014, **161**, H350–H354.
- 112 G. Xu, R. Liu and J. Wang, *Sci. China, Ser. B: Chem.*, 2009, **52**, 1171.
- 113 Y. Liu, X. Kong, X. Guo, Q. Li, J. Ke, R. Wang, Q. Li, Z. Geng and J. Zeng, *ACS Catal.*, 2020, **10**, 1077–1085.
- 114 I. A. Amar, R. Lan, C. T. G. Petit, V. Arrighi and S. Tao, *Solid State Ionics*, 2011, **182**, 133–138.
- 115 I. A. Amar, C. T. G. Petit, G. Mann, R. Lan, P. J. Skabara and S. Tao, *Int. J. Hydrogen Energy*, 2014, **39**, 4322–4330.
- 116 M. I. Ahmed, S. Chen, W. Ren, X. Chen and C. Zhao, *Chem. Commun.*, 2019, **55**, 12184–12187.
- 117 C. Li, J. Yu, L. Yang, J. Zhao, W. Kong, T. Wang, A. M. Asiri, Q. Li and X. Sun, *Inorg. Chem.*, 2019, **58**, 9597–9601.
- 118 F. Lai, J. Feng, X. Ye, W. Zong, G. He, C. Yang, W. Wang, Y.-E. Miao, B. Pan, W. Yan, T. Liu and I. P. Parkin, *J. Mater. Chem. A*, 2020, **8**, 1652–1659.
- 119 Y. Wang, K. Jia, Q. Pan, Y. Xu, Q. Liu, G. Cui, X. Guo and X. Sun, *ACS Sustainable Chem. Eng.*, 2019, **7**, 117–122.
- 120 T. Wu, W. Kong, Y. Zhang, Z. Xing, J. Zhao, T. Wang, X. Shi, Y. Luo and X. Sun, *Small Methods*, 2019, **3**, 1900356.
- 121 K. Jia, Y. Wang, Q. Pan, B. Zhong, Y. Luo, G. Cui, X. Guo and X. Sun, *Nanoscale Adv.*, 2019, **1**, 961–964.
- 122 T. Wu, X. Zhu, Z. Xing, S. Mou, C. Li, Y. Qiao, Q. Liu, Y. Luo, X. Shi, Y. Zhang and X. Sun, *Angew. Chem., Int. Ed.*, 2019, **58**, 18449–18453.
- 123 R. Zhang, H. Guo, L. Yang, Y. Wang, Z. Niu, H. Huang, H. Chen, L. Xia, T. Li, X. Shi, X. Sun, B. Li and Q. Liu, *ChemElectroChem*, 2019, **6**, 1014–1018.
- 124 H. Du, X. Guo, R.-M. Kong and F. Qu, *Chem. Commun.*, 2018, **54**, 12848–12851.
- 125 K. Chu, Y. Liu, Y. Li, Y. Guo, Y. Tian and H. Zhang, *Appl. Catal., B*, 2020, **264**, 118525.
- 126 X. Xiang, Z. Wang, X. Shi, M. Fan and X. Sun, *ChemCatChem*, 2018, **10**, 4530–4535.
- 127 Y. Li, Y. Liu, J. Wang, Y. Guo and K. Chu, *Inorg. Chem. Front.*, 2020, **7**, 455–463.
- 128 J. Wang, H. Jang, G. Li, M. G. Kim, Z. Wu, X. Liu and J. Cho, *Nanoscale*, 2020, **12**, 1478–1483.
- 129 J. Wu, Z. Wang, S. Li, S. Niu, Y. Zhang, J. Hu, J. Zhao and P. Xu, *Chem. Commun.*, 2020, **56**, 6834–6837.
- 130 L. Zhang, M. Cong, X. Ding, Y. Jin, F. Xu, Y. Wang, L. Chen and L. Zhang, *Angew. Chem.*, 2020, **132**, 10980–10985.
- 131 B. Chang, Q. Liu, N. Chen and Y. Yang, *ChemCatChem*, 2019, **11**, 1884–1888.
- 132 B. Xu, L. Xia, F. Zhou, R. Zhao, H. Chen, T. Wang, Q. Zhou, Q. Liu, G. Cui, X. Xiong, F. Gong and X. Sun, *ACS Sustainable Chem. Eng.*, 2019, **7**, 2889–2893.
- 133 H. Xie, H. Wang, Q. Geng, Z. Xing, W. Wang, J. Chen, L. Ji, L. Chang, Z. Wang and J. Mao, *Inorg. Chem.*, 2019, **58**, 5423–5427.
- 134 W. Fu, P. Zhuang, M. OliverLam Chee, P. Dong, M. Ye and J. Shen, *ACS Sustainable Chem. Eng.*, 2019, **7**, 9622–9628.
- 135 B. Xu, Z. Liu, W. Qiu, Q. Liu, X. Sun, G. Cui, Y. Wu and X. Xiong, *Electrochim. Acta*, 2019, **298**, 106–111.
- 136 J. Yu, C. Li, B. Li, X. Zhu, R. Zhang, L. Ji, D. Tang, A. M. Asiri, X. Sun, Q. Li, S. Liu and Y. Luo, *Chem. Commun.*, 2019, **55**, 6401–6404.
- 137 M. Ohrelus, H. Guo, H. Xian, G. Yu, A. A. Alshehri, K. A. Alzahrani, T. Li and M. Andersson, *ChemCatChem*, 2020, **12**, 731–735.
- 138 C. Li, D. Ma, S. Mou, Y. Luo, B. Ma, S. Lu, G. Cui, Q. Li, Q. Liu and X. Sun, *J. Energy Chem.*, 2020, **50**, 402–408.
- 139 J. Tian, Q. Liu, A. M. Asiri and X. Sun, *J. Am. Chem. Soc.*, 2014, **136**, 7587–7590.
- 140 E. J. Popczun, J. R. McKone, C. G. Read, A. J. Biacchi, A. M. Wiltrout, N. S. Lewis and R. E. Schaak, *J. Am. Chem. Soc.*, 2013, **135**, 9267–9270.
- 141 J. Kibsgaard and T. F. Jaramillo, *Angew. Chem., Int. Ed.*, 2014, **53**, 14433–14437.
- 142 J. Tian, Q. Liu, N. Cheng, A. M. Asiri and X. Sun, *Angew. Chem.*, 2014, **126**, 9731–9735.
- 143 P. Jiang, Q. Liu, Y. Liang, J. Tian, A. M. Asiri and X. Sun, *Angew. Chem.*, 2014, **126**, 13069–13073.
- 144 Y. Wang, B. Kong, D. Zhao, H. Wang and C. Selomulya, *Nano Today*, 2017, **15**, 26–55.
- 145 X. Zhu, T. Wu, L. Ji, Q. Liu, Y. Luo, G. Cui, Y. Xiang, Y. Zhang, B. Zheng and X. Sun, *Chem. Commun.*, 2020, **56**, 731–734.
- 146 M. Jin, X. Zhang, M. Han, H. Wang, G. Wang and H. Zhang, *J. Mater. Chem. A*, 2020, **8**, 5936–5942.
- 147 X. Yang, F. Ling, X. Zi, Y. Wang, H. Zhang, H. Zhang, M. Zhou, Z. Guo and Y. Wang, *Small*, 2020, **16**, 2000421.
- 148 Y. Abghoui, A. L. Garden, V. F. Hlynsson, S. Björgvinsdóttir, H. Ólafsdóttir and E. Skúlason, *Phys. Chem. Chem. Phys.*, 2015, **17**, 4909–4918.
- 149 X. Ren, G. Cui, L. Chen, F. Xie, Q. Wei, Z. Tian and X. Sun, *Chem. Commun.*, 2018, **54**, 8474–8477.
- 150 H.-L. Du, T. R. Gengenbach, R. Hodgetts, D. R. MacFarlane and A. N. Simonov, *ACS Sustainable Chem. Eng.*, 2019, **7**, 6839–6850.
- 151 Y. Abghoui and E. Skúlason, *Catal. Today*, 2017, **286**, 69–77.
- 152 L. Zhang, X. Ji, X. Ren, Y. Luo, X. Shi, A. M. Asiri, B. Zheng and X. Sun, *ACS Sustainable Chem. Eng.*, 2018, **6**, 9550–9554.
- 153 H. Jin, L. Li, X. Liu, C. Tang, W. Xu, S. Chen, L. Song, Y. Zheng and S.-Z. Qiao, *Adv. Mater.*, 2019, **31**, 1902709.
- 154 B. Hu, M. Hu, L. Seefeldt and T. L. Liu, *ACS Energy Lett.*, 2019, **4**, 1053–1054.
- 155 X. Yang, J. Nash, J. Anibal, M. Dunwell, S. Kattel, E. Stavitski, K. Attenkofer, J. G. Chen, Y. Yan and B. Xu, *J. Am. Chem. Soc.*, 2018, **140**, 13387–13391.
- 156 R. Zhang, Y. Zhang, X. Ren, G. Cui, A. M. Asiri, B. Zheng and X. Sun, *ACS Sustainable Chem. Eng.*, 2018, **6**, 9545–9549.
- 157 D. J. Ham and J. S. Lee, *Energies*, 2009, **2**, 873–899.
- 158 T. G. Kelly and J. G. Chen, *Chem. Soc. Rev.*, 2012, **41**, 8021–8034.
- 159 Z. Yan, M. Cai and P. K. Shen, *Sci. Rep.*, 2013, **3**, 1646.
- 160 G. Gao, A. P. O'Mullane and A. Du, *ACS Catal.*, 2017, **7**, 494–500.





- 161 Y. Liu, T. G. Kelly, J. G. Chen and W. E. Mustain, *ACS Catal.*, 2013, **3**, 1184–1194.
- 162 M. Naguib, J. Come, B. Dyatkin, V. Presser, P.-L. Taberna, P. Simon, M. W. Barsoum and Y. Gogotsi, *Electrochem. Commun.*, 2012, **16**, 61–64.
- 163 J. S. Jang, D. J. Ham, E. Ramasamy, J. Lee and J. S. Lee, *Chem. Commun.*, 2010, **46**, 8600–8602.
- 164 Y. Zhong, X. Xia, F. Shi, J. Zhan, J. Tu and H. J. Fan, *Adv. Sci.*, 2016, **3**, 1500286.
- 165 L. I. Johansson, *Surf. Sci. Rep.*, 1995, **21**, 177–250.
- 166 H. Jiang, Y. Yao, Y. Zhu, Y. Liu, Y. Su, X. Yang and C. Li, *ACS Appl. Mater. Interfaces*, 2015, **7**, 21511–21520.
- 167 M. Kuang, W. Huang, C. Hegde, W. Fang, X. Tan, C. Liu, J. Ma and Q. Yan, *Mater. Horiz.*, 2020, **7**, 32–53.
- 168 H. Cheng, L.-X. Ding, G.-F. Chen, L. Zhang, J. Xue and H. Wang, *Adv. Mater.*, 2018, **30**, 1803694.
- 169 M. Wang, S. Liu, T. Qian, J. Liu, J. Zhou, H. Ji, J. Xiong, J. Zhong and C. Yan, *Nat. Commun.*, 2019, **10**, 341.
- 170 I. Matanovic and F. H. Garzon, *Phys. Chem. Chem. Phys.*, 2018, **20**, 14679–14687.
- 171 K. P. Ramaiyan, S. Ozden, S. Maurya, D. Kelly, S. K. Babu, A. Benavidez, F. G. Garzon, Y. S. Kim, C. R. Kreller and R. Mukundan, *J. Electrochem. Soc.*, 2020, **167**, 44506.
- 172 X. Qu, L. Shen, Y. Mao, J. Lin, Y. Li, G. Li, Y. Zhang, Y. Jiang and S. Sun, *ACS Appl. Mater. Interfaces*, 2019, **11**, 31869–31877.
- 173 Y. Liu, X. Zhu, Q. Zhang, T. Tang, Y. Zhang, L. Gu, Y. Li, J. Bao, Z. Dai and J.-S. Hu, *J. Mater. Chem. A*, 2020, **8**, 8920–8926.
- 174 M. Peng, Y. Qiao, M. Luo, M. Wang, S. Chu, Y. Zhao, P. Liu, J. Liu and Y. Tan, *ACS Appl. Mater. Interfaces*, 2019, **11**, 40062–40068.
- 175 L. M. Azofra, N. Li, D. R. MacFarlane and C. Sun, *Energy Environ. Sci.*, 2016, **9**, 2545–2549.
- 176 S. Zheng, S. Li, Z. Mei, Z. Hu, M. Chu, J. Liu, X. Chen and F. Pan, *J. Phys. Chem. Lett.*, 2019, **10**, 6984–6989.
- 177 Y. Luo, G.-F. Chen, L. Ding, X. Chen, L.-X. Ding and H. Wang, *Joule*, 2019, **3**, 279–289.
- 178 B. Dong, X. Zhao, G.-Q. Han, X. Li, X. Shang, Y.-R. Liu, W.-H. Hu, Y.-M. Chai, H. Zhao and C.-G. Liu, *J. Mater. Chem. A*, 2016, **4**, 13499–13508.
- 179 C. Tan, Z. Luo, A. Chaturvedi, Y. Cai, Y. Du, Y. Gong, Y. Huang, Z. Lai, X. Zhang, L. Zheng, X. Qi, M. H. Goh, J. Wang, S. Han, X.-J. Wu, L. Gu, C. Kloc and H. Zhang, *Adv. Mater.*, 2018, **30**, 1705509.
- 180 M. Asadi, B. Kumar, A. Behranginia, B. A. Rosen, A. Baskin, N. Reppin, D. Pisasale, P. Phillips, W. Zhu, R. Haasch, R. F. Klie, P. Král, J. Abiadé and A. Salehi-Khojin, *Nat. Commun.*, 2014, **5**, 4470.
- 181 B. M. Hoffman, D. Lukoyanov, Z.-Y. Yang, D. R. Dean and L. C. Seefeldt, *Chem. Rev.*, 2014, **114**, 4041–4062.
- 182 L. Zhang, X. Ji, X. Ren, Y. Ma, X. Shi, Z. Tian, A. M. Asiri, L. Chen, B. Tang and X. Sun, *Adv. Mater.*, 2018, **30**, 1800191.
- 183 X. Li, T. Li, Y. Ma, Q. Wei, W. Qiu, H. Guo, X. Shi, P. Zhang, A. M. Asiri, L. Chen, B. Tang and X. Sun, *Adv. Energy Mater.*, 2018, **8**, 1801357.
- 184 L. Zeng, S. Chen, J. van der Zalm, X. Li and A. Chen, *Chem. Commun.*, 2019, **55**, 7386–7389.
- 185 B. H. R. Suryanto, D. Wang, L. M. Azofra, M. Harb, L. Cavallo, R. Jalili, D. R. G. Mitchell, M. Chatti and D. R. MacFarlane, *ACS Energy Lett.*, 2019, **4**, 430–435.
- 186 X. Li, X. Ren, X. Liu, J. Zhao, X. Sun, Y. Zhang, X. Kuang, T. Yan, Q. Wei and D. Wu, *J. Mater. Chem. A*, 2019, **7**, 2524–2528.
- 187 X. Zhao, X. Zhang, Z. Xue, W. Chen, Z. Zhou and T. Mu, *J. Mater. Chem. A*, 2019, **7**, 27417–27422.
- 188 L. Zeng, X. Li, S. Chen, J. Wen, F. Rahmati, J. van der Zalm and A. Chen, *Nanoscale*, 2020, **12**, 6029–6036.
- 189 L. Zeng, X. Li, S. Chen, J. Wen, W. Huang and A. Chen, *J. Mater. Chem. A*, 2020, **8**, 7339–7349.
- 190 J. Liang, S. Ma, J. Li, Y. Wang, J. Wu, Q. Zhang, Z. Liu, Z. Yang, K. Qu and W. Cai, *J. Mater. Chem. A*, 2020, **8**, 10426–10432.
- 191 X. Yao, Z. Chen, Y. Wang, X. Lang, W. Gao, Y. Zhu and Q. Jiang, *J. Mater. Chem. A*, 2019, **7**, 25961–25968.
- 192 X. Chen, Y.-T. Liu, C. Ma, J. Yu and B. Ding, *J. Mater. Chem. A*, 2019, **7**, 22235–22241.
- 193 P. Wei, H. Xie, X. Zhu, R. Zhao, L. Ji, X. Tong, Y. Luo, G. Cui, Z. Wang and X. Sun, *ACS Sustainable Chem. Eng.*, 2020, **8**, 29–33.
- 194 L. Zhang, L.-X. Ding, G.-F. Chen, X. Yang and H. Wang, *Angew. Chem., Int. Ed.*, 2019, **58**, 2612–2616.
- 195 P. Song, H. Wang, L. Kang, B. Ran, H. Song and R. Wang, *Chem. Commun.*, 2019, **55**, 687–690.
- 196 W. Qiu, X.-Y. Xie, J. Qiu, W.-H. Fang, R. Liang, X. Ren, X. Ji, G. Cui, A. M. Asiri, G. Cui, B. Tang and X. Sun, *Nat. Commun.*, 2018, **9**, 3485.
- 197 T. Wu, X. Li, X. Zhu, S. Mou, Y. Luo, X. Shi, A. M. Asiri, Y. Zhang, B. Zheng, H. Zhao and X. Sun, *Chem. Commun.*, 2020, **56**, 1831–1834.
- 198 Y. Liu, Y. Su, X. Quan, X. Fan, S. Chen, H. Yu, H. Zhao, Y. Zhang and J. Zhao, *ACS Catal.*, 2018, **8**, 1186–1191.
- 199 C. Lv, Y. Qian, C. Yan, Y. Ding, Y. Liu, G. Chen and G. Yu, *Angew. Chem.*, 2018, **130**, 10403–10407.
- 200 C. Zhao, S. Zhang, M. Han, X. Zhang, Y. Liu, W. Li, C. Chen, G. Wang, H. Zhang and H. Zhao, *ACS Energy Lett.*, 2019, **4**, 377–383.
- 201 S. Mukherjee, D. A. Cullen, S. Karakalos, K. Liu, H. Zhang, S. Zhao, H. Xu, K. L. More, G. Wang and G. Wu, *Nano Energy*, 2018, **48**, 217–226.
- 202 Q. Zhang, F. Luo, Y. Ling, L. Guo, K. Qu, H. Hu, Z. Yang, W. Cai and H. Cheng, *ChemCatChem*, 2018, **10**, 5194–5200.
- 203 X. Yu, P. Han, Z. Wei, L. Huang, Z. Gu, S. Peng, J. Ma and G. Zheng, *Joule*, 2018, **2**, 1610–1622.
- 204 Y. Jiao, Y. Zheng, K. Davey and S.-Z. Qiao, *Nat. Energy*, 2016, **1**, 16130.
- 205 P. Song, H. Wang, X. Cao, N. Liu, Q. Wang and R. Wang, *ChemElectroChem*, 2020, **7**, 212–216.
- 206 Y. Song, T. Wang, J. Sun, Z. Wang, Y. Luo, L. Zhang, H. Ye and X. Sun, *ACS Sustainable Chem. Eng.*, 2019, **7**, 14368–14372.
- 207 Y. Liu, Q. Li, X. Guo, X. Kong, J. Ke, M. Chi, Q. Li, Z. Geng and J. Zeng, *Adv. Mater.*, 2020, **32**, 1907690.



- 208 T. Wang, L. Xia, J.-J. Yang, H. Wang, W.-H. Fang, H. Chen, D. Tang, A. M. Asiri, Y. Luo, G. Cui and X. Sun, *Chem. Commun.*, 2019, **55**, 7502–7505.
- 209 L. Xia, J. Yang, H. Wang, R. Zhao, H. Chen, W. Fang, A. M. Asiri, F. Xie, G. Cui and X. Sun, *Chem. Commun.*, 2019, **55**, 3371–3374.
- 210 L. Xia, X. Wu, Y. Wang, Z. Niu, Q. Liu, T. Li, X. Shi, A. M. Asiri and X. Sun, *Small Methods*, 2019, **3**, 1800251.
- 211 S. Cheng, C. Li, Z. Yu, Y. Sun, L. Li and J. Yang, *RSC Adv.*, 2020, **10**, 9814–9823.
- 212 Y. Kong, Y. Li, B. Yang, Z. Li, Y. Yao, J. Lu, L. Lei, Z. Wen, M. Shao and Y. Hou, *J. Mater. Chem. A*, 2019, **7**, 26272–26278.
- 213 S. Xiao, F. Luo, H. Hu and Z. Yang, *Chem. Commun.*, 2020, **56**, 446–449.
- 214 Q. Zhang, F. Luo, Y. Ling, S. Xiao, M. Li, K. Qu, Y. Wang, J. Xu, W. Cai and Z. Yang, *J. Mater. Chem. A*, 2020, **8**, 8430–8439.
- 215 X. Zhu, T. Wu, L. Ji, C. Li, T. Wang, S. Wen, S. Gao, X. Shi, Y. Luo, Q. Peng and X. Sun, *J. Mater. Chem. A*, 2019, **7**, 16117–16121.
- 216 W. Guo, Z. Liang, J. Zhao, B. Zhu, K. Cai, R. Zou and Q. Xu, *Small Methods*, 2018, **2**, 1800204.
- 217 H. Wang, D. Yang, S. Liu, S. Yin, Y. Xu, X. Li, Z. Wang and L. Wang, *ACS Sustainable Chem. Eng.*, 2019, **7**, 15772–15777.
- 218 Y.-X. Luo, W.-B. Qiu, R.-P. Liang, X.-H. Xia and J.-D. Qiu, *ACS Appl. Mater. Interfaces*, 2020, **12**, 17452–17458.
- 219 C. Guo, X. Liu, L. Gao, X. Kuang, X. Ren, X. Ma, M. Zhao, H. Yang, X. Sun and Q. Wei, *Appl. Catal., B*, 2020, **263**, 118296.
- 220 Y. Zhang, H. Du, Y. Ma, L. Ji, H. Guo, Z. Tian, H. Chen, H. Huang, G. Cui, A. M. Asiri, F. Qu, L. Chen and X. Sun, *Nano Res.*, 2019, **12**, 919–924.
- 221 D. Feng, X. Zhang, Y. Sun and T. Ma, *Nano Mater. Sci.*, 2020, **2**, 132–139.
- 222 J. Chen, H. Huang, L. Xia, H. Xie, L. Ji, P. Wei, R. Zhao, H. Chen, A. M. Asiri and X. Sun, *ChemistrySelect*, 2019, **4**, 3547–3550.
- 223 C. Chen, D. Yan, Y. Wang, Y. Zhou, Y. Zou, Y. Li and S. Wang, *Small*, 2019, **15**, 1805029.
- 224 P. Song, L. Kang, H. Wang, R. Guo and R. Wang, *ACS Appl. Mater. Interfaces*, 2019, **11**, 12408–12414.
- 225 S. Chen, S. Perathoner, C. Ampelli, C. Mebrahtu, D. Su and G. Centi, *ACS Sustainable Chem. Eng.*, 2017, **5**, 7393–7400.
- 226 D. Strmcnik, P. P. Lopes, B. Genorio, V. R. Stamenkovic and N. M. Markovic, *Nano Energy*, 2016, **29**, 29–36.
- 227 F. Köleli and T. Röpke, *Appl. Catal., B*, 2006, **62**, 306–310.
- 228 K. Kim, N. Lee, C.-Y. Yoo, J.-N. Kim, H. C. Yoon and J.-I. Han, *J. Electrochem. Soc.*, 2016, **163**, F610–F612.
- 229 Y. Song, D. Johnson, R. Peng, D. K. Hensley, P. V. Bonnesen, L. Liang, J. Huang, F. Yang, F. Zhang, R. Qiao, A. P. Baddorf, T. J. Tschaplinski, N. L. Engle, M. C. Hatzell, Z. Wu, D. A. Cullen, H. M. Meyer, B. G. Sumpter and A. J. Rondinone, *Sci. Adv.*, 2018, **4**, e1700336.
- 230 K. Kim, C.-Y. Yoo, J.-N. Kim, H. C. Yoon and J.-I. Han, *J. Electrochem. Soc.*, 2016, **163**, F1523–F1526.
- 231 A. Tsuneto, A. Kudo and T. Sakata, *J. Electroanal. Chem.*, 1994, **367**, 183–188.
- 232 A. Tsuneto, A. Kudo and T. Sakata, *Chem. Lett.*, 1993, 851–854.
- 233 H. K. Lee, C. S. L. Koh, Y. H. Lee, C. Liu, I. Y. Phang, X. Han, C.-K. Tsung and X. Y. Ling, *Sci. Adv.*, 2018, **4**, eaar3208.
- 234 T. M. Pappenfus, K. Lee, L. M. Thoma and C. R. Dukart, *ECS Trans.*, 2019, **16**, 89–93.
- 235 A. Katayama, T. Inomata, T. Ozawa and H. Masuda, *Electrochem. Commun.*, 2016, **67**, 6–10.
- 236 F. Zhou, L. M. Azofra, M. Ali, M. Kar, A. N. Simonov, C. McDonnell-Worth, C. Sun, X. Zhang and D. R. MacFarlane, *Energy Environ. Sci.*, 2017, **10**, 2516–2520.
- 237 J. M. McEnaney, A. R. Singh, J. A. Schwalbe, J. Kibsgaard, J. Lin, M. Cargnello, T. F. Jaramillo and J. K. Nørskov, *Energy Environ. Sci.*, 2017, **10**, 1621–1630.
- 238 B. H. R. Suryanto, K. Matuszek, J. Choi, R. Y. Hodgetts, H.-L. Du, J. M. Bakker, C. S. M. Kang, P. V. Cherepanov, A. N. Simonov and D. R. MacFarlane, *Science*, 2021, **372**, 1187–1191.
- 239 J. A. Schwalbe, M. J. Statt, C. Chosy, A. R. Singh, B. A. Rohr, A. C. Nielander, S. Z. Andersen, J. M. McEnaney, J. G. Baker, T. F. Jaramillo, J. K. Nørskov and M. Cargnello, *ChemElectroChem*, 2020, **7**, 1542–1549.
- 240 S. Z. Andersen, Michael J. Statt, V. J. Bukas, S. G. Shapel, J. B. Pedersen, K. Krempel, M. Saccoccio, D. Chakraborty, J. Kibsgaard, P. C. K. Vesborg, J. Nørskov and I. Chorkendorff, *Energy Environ. Sci.*, 2020, **13**, 4291–4300.
- 241 S. Z. Andersen, V. Čolić, S. Yang, J. A. Schwalbe, A. C. Nielander, J. M. McEnaney, K. Enemark-Rasmussen, J. G. Baker, A. R. Singh, B. A. Rohr, M. J. Statt, S. J. Blair, S. Mezzavilla, J. Kibsgaard, P. C. K. Vesborg, M. Cargnello, S. F. Bent, T. F. Jaramillo, I. L. Stephens, J. K. Nørskov and I. Chorkendorff, *Nature*, 2019, **570**, 504–508.
- 242 B. H. R. Suryanto, H.-L. Du, D. Wang, J. Chen, A. N. Simonov and D. R. MacFarlane, *Nat. Catal.*, 2019, **2**, 290–296.
- 243 J. Choi, B. H. R. Suryanto, D. Wang, H.-L. Du, R. Y. Hodgetts, F. M. F. Vallana, D. R. MacFarlane and A. N. Simonov, *Nat. Commun.*, 2020, **11**, 5546.
- 244 L. Li, C. Tang, D. Yao, Y. Zheng and S.-Z. Qiao, *ACS Energy Lett.*, 2019, **4**, 2111–2116.
- 245 H. Liu, Y. Zhang and J. Luo, *J. Energy Chem.*, 2020, **49**, 51–58.
- 246 R. Dabundo, M. F. Lehmann, L. Treibergs, C. R. Tobias, M. A. Altabet, P. H. Moisaner and J. Granger, *PLoS One*, 2014, **9**, e110335.

