


REVIEW

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2, 4497Recent advances on the removal of dyes from
wastewater using various adsorbents: a critical
review†Soumi Dutta,^a Bramha Gupta,^a Suneel Kumar Srivastava ^{*b} and
Ashok Kumar Gupta^{*c}

The rapid increase in toxic dye wastewater generated from various industries remains a severe public health issue and prime environmental protection concern, posing a major challenge to existing conventional water treatment systems. Consequently, various physicochemical and biological treatment processes have been studied, which exhibit varying removal abilities depending on their experimental constraints. Among them, adsorption is considered to be the most efficient due to its high removal efficiency, easy operation, cost-effectiveness, and recyclability of the adsorbents. Considering this, the present review article focused on presenting a comprehensive summary of the various types of adsorbents such as commercial activated carbon, metal oxide-based, carbon-based, metal-organic framework, and polymer-based adsorbents used in dye remediation of contaminated water. The effects of several critical factors such as initial dye concentration, solution pH, temperature, and adsorbent dose on the dye adsorption performance are also described. In addition, the adsorption mechanisms responsible for dye removal are explained based on electrostatic attraction, ion exchange, surface complexation, and π - π interactions. Finally, critiques, future perspectives, and a summary of the present article are given. Various adsorbents such as carbon-based materials, metal oxides, bio-adsorbents, and polymer-based materials, have been shown to be efficient for the removal of dye pollutants from wastewater. Thus, it is anticipated that dye removal by adsorption can provide a feasible solution for the treatment of dye-laden water.

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1. Introduction

The rapid growth of the global population, climate change, and industrial development has significantly affected water quality, resulting in an increasing freshwater crisis worldwide. Considering this, various consumers and polluters of freshwater significantly contribute to freshwater depletion.^{1,2} Among them, the increasingly used dyes including methylene blue (MB), rhodamine B (RhB), methyl orange (MO), Congo red (CR), Disperse Violet 26, methyl red, and crystal violet are the most important sources of industrial pollutants originating from different industries such as the textile, cosmetic, leather, food, pharmaceutical, paint and varnish, and pulp and paper industries (Table 1).^{3–16} According to a

recent estimate, about 70 lakh tons of dyes are produced annually worldwide.¹⁷ The release of this industrial waste dye into water jeopardizes human health and the environment. Consequently, research in this area is ongoing, which is obvious from the drastic upsurge in the number of research articles published on 'Dye Removal' in 2016–2020, as displayed schematically in Fig. 1.

The direct disposal of untreated dye-containing effluent into natural water bodies has an adverse effect on the photo-synthetic activity in aquatic ecosystems.¹⁸ It creates mutagenic or teratogenic effects on aquatic organisms and fish species due to the existence of metals¹⁹ and aromatics.²⁰ Further, the presence of dyes in the environment has mild to severe toxic effects on human health, including carcinogenic, mutagenic, allergic, and dermatitis effects, kidney disease.²¹ It has been reported that chromium-based dyes are generally complex in structure and cause carcinogenic effects on human health.²² Thus, the disposal of dyes in the environment contaminates the water bodies, subsequently affecting the water quality, aquatic life, and human health. Table 1 also describes the ecotoxicological effects of dyes on living organisms. The sources and pathways of various dye pollutants in water bodies are depicted in Fig. 2.

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Table 1 Classification, examples, applications, solubility in water, and ecotoxicological effects of dyes

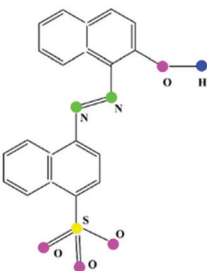
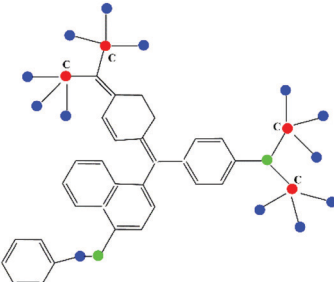
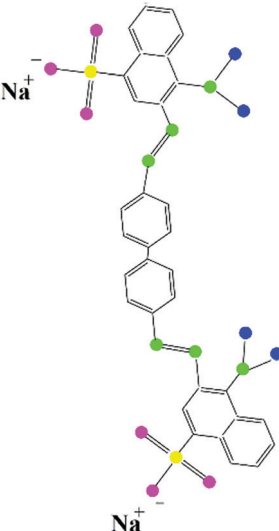
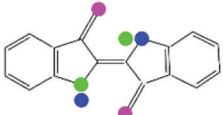
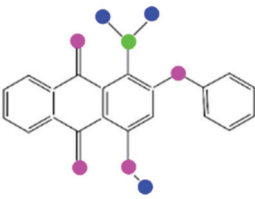
| Type of dye | Example of chemical structure of dye | Examples of dyes | Dye application | Solubility in water | Ecotoxicological effects | Ref. |
|--------------|---|--|---|---------------------|---|--------------------------|
| Acid dye |  <p>Acid red 88</p> | Acid yellow 36, Acid orange 7, Acid blue 83, Acid blue 7 | Textile, leather, and pharmaceutical industries; nylon, wool, silk, and modified acrylics | Water soluble | Vomiting, nausea, diarrhea, carcinogenic and mutagenic effects | 3 and 72–75 |
| Basic dye |  <p>Basic blue 26</p> | Methylene blue (MB), Basic red 1 or rhodamine 6G, Basic yellow 2 | Paper, poly-acrylonitrile modified nylons, and modified polyesters | Water soluble | Altering the chemical and physical properties of water bodies and causing detrimental effects to the flora and fauna | 3, 72, 76 and 77 |
| Direct dye |  <p>Direct red 28</p> | Congo red (CR), Direct red 28, Direct black 38 | Coloring paper products | Water soluble | Toxic to aquatic animals and plants; carcinogenic, mutagenic, and dermatitis | 3, 72 and 78–80 |
| Vat dye |  <p>Vat blue 1</p> | Vat blue 1, Vat acid blue 74 | Insoluble pigment, indigo, and natural fibers, cellulosic fibers | Water insoluble | Severely affects the quality and clearness of water resources such as lakes and rivers; dermatitis, allergic conjunctivitis, rhinitis, and other allergic reactions | 3, 72, 73, 76, 81 and 82 |
| Disperse dye |  <p>Disperse red 60</p> | Disperse red 9, Disperse violet 1, Disperse red 60 | Polyester, nylon, cellulose acetate, and acrylic fibers | | Mutagenic; carcinogenic; causes soil and water pollution | 3, 72 and 83 |



Table 1 (continued)


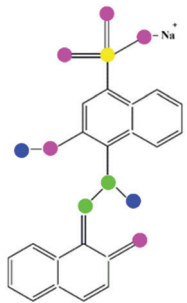
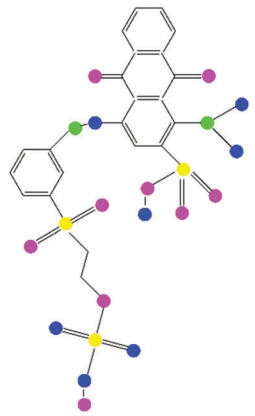
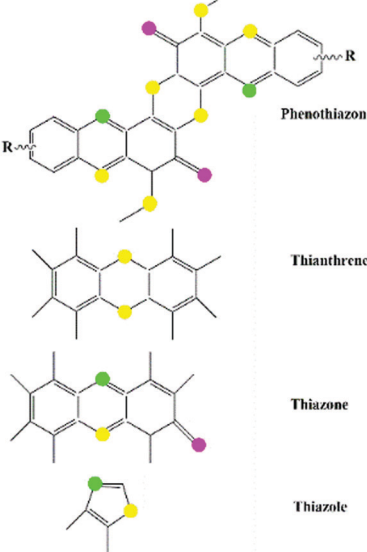

| Type of dye | Example of chemical structure of dye | Examples of dyes | Dye application | Solubility in water | Ecotoxicological effects | Ref. |
|--------------|--|---|--|---------------------|---|------------------|
| Nitro dye |  <p>Chromophore of nitro dye</p> | Naphthol yellow (II) | Dye wool | | Decreases light penetration and photosynthetic activity; carcinogenic and mutagenic | 3, 72 and 84 |
| Mordant dye |  <p>Mordant black 17</p> | Mordant red 11, Mordant Black 17 | Textile fibres such as wool, silk, and leather | | Shows allergic reactions | 3, 72, 85 and 86 |
| Reactive dye |  <p>Reactive blue 19</p> | C.I. reactive red 120, C.I. reactive red 147, C.I. reactive blue 19 | Dyeing cellulosic, silk, and wool fibres | | High and unwanted levels of dissolved solids in the effluent Allergic reaction in eyes, skin, mucous membrane, and the upper respiratory tract | 3 and 72 |
| Sulphur dye |  <p>Phenothiazonethianthrene</p> <p>Thianthrene</p> <p>Thiazone</p> <p>Thiazole</p> | Sulfur brilliant green, Sulfur blue, Sulfur Black 1, Leuco Sulfur Black 1, Phthalic anhydride | Dyeing cellulosic fibres and cotton | Water insoluble | Skin irritation; itchy or blocked noses; sneezing and sore eyes; carcinogenic | 3, 72 and 76 |



Table 1 (continued)

| Type of dye | Example of chemical structure of dye | Examples of dyes | Dye application | Solubility in water | Ecotoxicological effects | Ref. |
|-------------|---|---|---|---------------------|---|------------------|
| Azo dyes |  <p>Chromophore of azo dyes</p> | Direct Black 22, Disperse Yellow 7, Acid Orange 20, Methyl red, Methyl orange (MO), Trypan blue | Textile industry for dyeing process and food coloring | | Causes carcinogenicity in humans and animals. 73 and If inhaled or swallowed, it affects the eye, skin, and digestive tract. Affects aquatic life if present in excess. | 3, 15, 72, 87–90 |

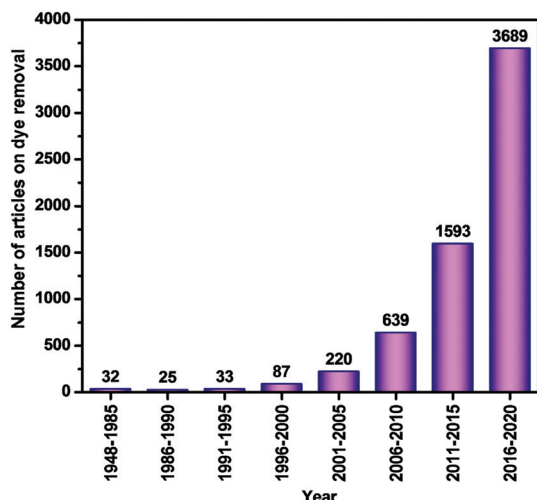


Fig. 1 Frequency of publications on dye removal with selected keyword 'Dye Removal' (details are given in Section A of the ESI†).

Accordingly, researchers have focused on the remediation of dye wastewater using coagulation/flocculation, electrocoagulation, filtration, adsorption, ion-exchange, advanced oxidation processes (AOPs), activated sludge processes (ASP), sequencing batch reactors (SBR), membrane bioreactors (MBR), moving bed bio-film reactors (MBBR), and constructed wetlands (CW).^{23–30} The coagulation process involves the destabilization of charged suspended and colloidal impurities.^{31,32} The electrocoagulation method employs a direct current source between metal electrodes containing iron or aluminum submerged in dye-contaminated water. Metal ions create a wide range of coagulated species and metal hydroxides at a certain pH, which destabilize and agglomerate suspended particles or precipitates and adsorb dye molecules.^{23,33} In the filtration techniques, the separation of dissolved and suspended particles is carried out by sieving and particle capturing mechanisms.^{32,34,35} Adsorption methods involve the movement of solids from the bulk liquid to the surface of the adsorbent.^{26,36} The ion-exchange method involves the removal of dyes through the strong interactions between the functional groups on ion exchange resins and charged dye molecules.

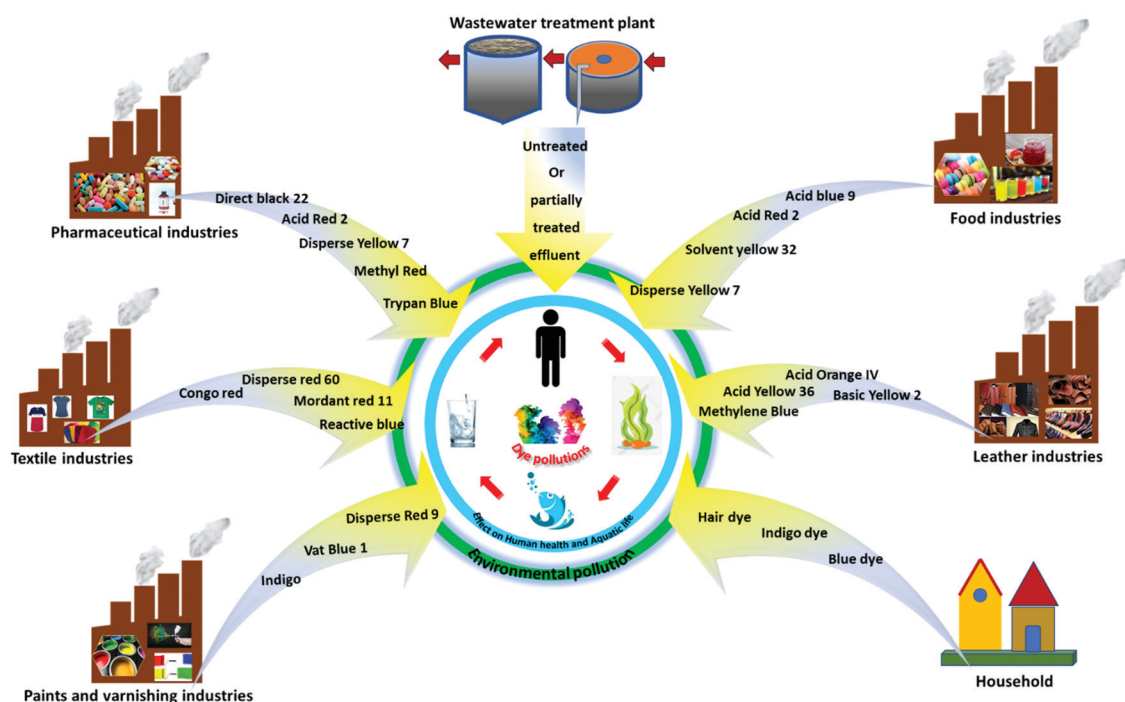


Fig. 2 Sources and pathways of dyes in the environment.



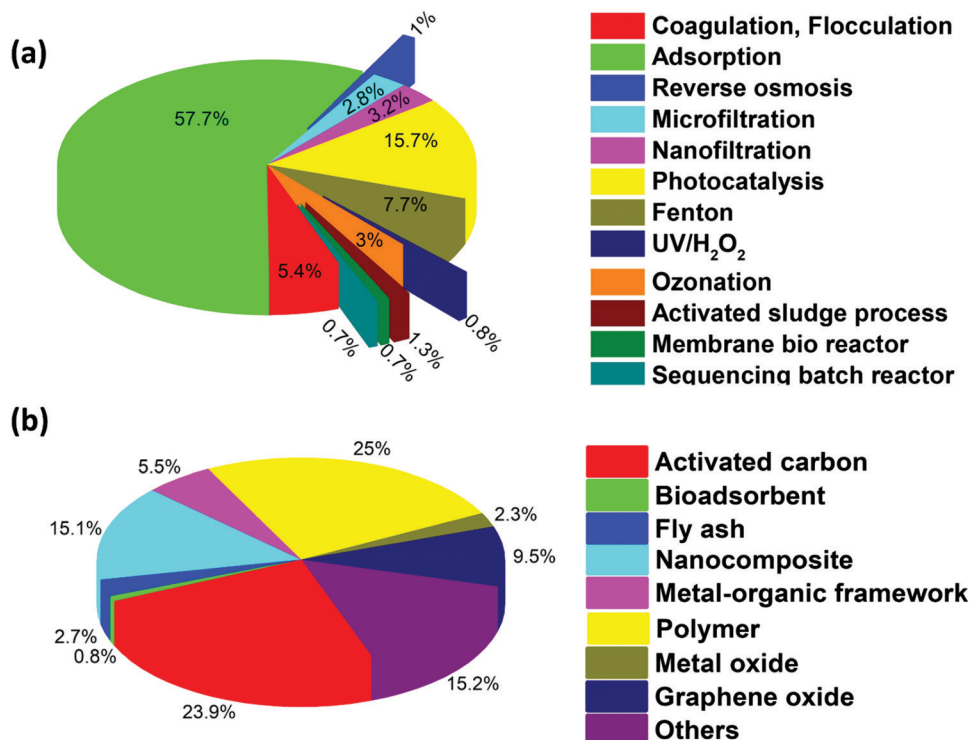


Fig. 3 Pie-chart showing the percentage of literature available on dye removal for (a) various physicochemical and biological techniques. Keywords: dye, water, treatment, and name of each technique, as mentioned in the plot. (b) Adsorption techniques using different adsorbents. Keywords: dye, water, adsorption, and the type of each adsorbent as mentioned in the plot. (Details are given in Section B and C of the ESI,† respectively).

The formation of strong linkages between the resins and the dye molecules results in the separation of dyes from wastewater.²⁹ The use of AOPs, such as ozonation, ultraviolet/hydrogen peroxide (UV/H₂O₂), Fenton, ultrasound, anodic oxidation, and photocatalytic processes, have been efficiently employed to treat dye wastewater. AOPs involve the formation of active radicals, which degrade targeted contaminants.^{35,37–43} The suspended and/or attached growth of bacterial systems (*i.e.*, ASP, MBBR, SBR, CW, and MBR) have been employed in the biodegradation of dye molecules.^{44,45} The number of articles on various existing physicochemical and biological treatment techniques is shown in Fig. 3a, which confirms that among these technologies, adsorption is considered to be one of the most important and useful decontamination processes. It is considered to be a fast, low cost, simple, sludge-free process, having high efficiency and/or selectivity, mechanical stability, and recycling facilities.^{14,46–51} The adsorption process is widely used for the remediation of different pollutants from wastewater, including heavy metals, arsenic, and dyes.^{52–59} Additionally, a pie chart displaying the percentage of literature available on dye removal using various adsorption techniques is shown in Fig. 3b. Considering this, the present study aims to review dye removal from polluted water *via* the adsorption process using various types of adsorbents. Specifically, several adsorbents, including activated carbon, metal oxide-based, carbon-based, bio-adsorbent, metal-organic framework (MOF), and polymer-based materials, are widely applied for the adsorption of dye from polluted water.^{13,14,60–67} These adsorbents possess the advantages of easy fabrication, high effective

surface area, multi-functionalities, high surface volume ratio, high reactivity, large number of active sites, reusability, low cost, and high efficiency to treat recalcitrant compounds.^{68,69}

According to the available literature, several techniques such as chemical oxidation, coagulation, filtration with coagulation, precipitation, adsorption, and biological treatments have been frequently used to remove dyes from industrial and domestic effluents. However, the use of each of these methods in separation has merits and disadvantages. For example, coagulation is most commonly used method in industry, which does not involve the formation of harmful and toxic intermediates. However, inherent sludge formation and its disposal remain its biggest drawback. Further, the choice of method is also guided by operational costs. Considering this, the adsorption process is considered to be one of the most effective and inexpensive treatment processes to remove dyes in wastewater. Accordingly, the present article presents a review of the challenges and opportunities of the adsorption methodology available as the current state of the art in the removal of dyes from contaminated water. This covers the classification of dye effluents released from various industries, their solubility in water, chemical structures, and impact of these toxic compounds on the environment and human health, and the types of adsorbents used in the remediation of dyes are reviewed. This is followed by an updated review on the removal of different dyes using a variety of adsorbents. In addition, the adsorptive separation of dyes is also assessed in terms of the critical factors influencing dye separation, maximum adsorption capacity, adsorption mechanisms, and adsorption kinetics. It is anticipated that

the current review will be helpful in identifying cost-effective and efficient adsorption methods for the remediation of industrial dyes in wastewater. Finally, the present review also targets various research gaps and their possible solution.

2. Dyes: sources, classifications, and ecotoxicological effects

A dye is generally described as substances capable of imparting color through physical/chemical binding on a substrate to which it is applied. The presence of chromophores in dye accounts for the development of color, which auxochromes are attached to.⁶⁵ Table 1 describes the classification of dyes based on their physicochemical properties, applications, ecotoxicological effects, and water solubility. These dyes exhibit aromatic molecular structures originating from hydrocarbons, such as benzene, toluene, naphthalene, anthracene, and xylene.⁷⁰ Dyes are mainly derived from two significant sources, including natural and anthropogenic. The natural sources include plants, different insects, animals, and minerals, whereas synthetic dyes are man-made or manufactured using various organic molecules.^{3,71} However, the multifaceted applications of dyes in daily life involve their release together with other toxic organic/inorganic chemicals from industrial effluents, resulting in detrimental effects on the environment.⁷¹ Therefore, it is necessary to protect the environment from these toxic dye/dye effluents released in water by subjecting them to various physical, chemical, biological treatments or their combinations. Fig. 2 shows the sources and pathways of different dyes originating from various sources, such as industry, wastewater treatment plants and households, contributing to environmental pollution. Dyes can be classified considering their chemical structure, physicochemical attributes, origin, and applications.²² This classification also considers the extremely hazardous/toxic industrial effluents that are carcinogenic to human health and the environment.^{1,21} Accordingly, Table 1 describes acid, basic, reactive, nitro, vat, disperse, azo, mordant dyes, *etc.*

3. Existing treatment processes for the remediation of dyes

Previously, conventional treatment processes were employed using proper regulatory guidelines for the treatment of dyes in wastewater.⁹¹ However, advanced dye removal processes have been established considering the discharge limit. They include several biological (*e.g.*, ASP, MBR, SBR, MBBR, and CW), coagulation/flocculation, and advanced physicochemical processes (such as adsorption, filtration, photocatalysis, Fenton reaction, ozonation, UV/H₂O₂, and anodic oxidation) reported for the purification of dye-contaminated wastewater.^{29,36,92–95} Biological processes use attached and suspended growth systems for the removal of dyes using aerobic and anaerobic or facultative bacteria.⁹⁶ In the coagulation/flocculation process, various coagulants are employed to destabilize the charged suspended and colloidal impurities.³² The advanced physicochemical processes are based on the principle of the sieving process, solid-liquid

separation, attraction–repulsion, free radical reactions, catalytic oxidation, and electrochemical reactions. Adsorption is another simple facile process extensively used in the treatment of industrial dye effluents. This process involves the movement of dye molecules present in the liquid phase to a solid surface of various adsorbents.^{26,36} Membrane processes such as reverse osmosis (RO), nanofiltration (NF), and microfiltration (MF) have also been successfully employed in the treatment of dye-laden water (more than or about 90% removal efficiency). However, pore blockage and membrane fouling during these processes are still major drawbacks.^{93,97–99} In AOPs, active radicals are generated, mainly hydroxyl radicals, which play an important role in degrading persistent dye compounds. However, the high cost/energy requirements and the formation of toxic by-products are a few major constraints in their practical application.^{35,100}

In addition, biological processes, such as ASP, MBR, SBR, and MBBR, have shown good efficacy for dye removal. However, the good removal efficiency of dyes by biological processes is overshadowed by their limitations such as space requirements, low removal rate, and inefficiency to treat recalcitrant dye components. The number of articles published on various existing physicochemical and biological processes are compared and shown in Fig. 3a, which presents that adsorption is the most studied process for dye removal. Overall, it can be inferred that in comparison to the existing advanced oxidation, filtration, and biological treatment processes, the adsorption process is beneficial for treating dye wastewater owing to its easy operation, low cost, high efficiency, recycling of the adsorbents, suitability for the treatment of persistent dye compounds and applicability.^{40,101}

4. Overview of various adsorbents for the removal of dyes

At present, various adsorbents such as bio-sorbents, carbon-based nano-adsorbents, transition metal-based oxides, MOFs, and polymer-based adsorbents are used to treat dye-containing wastewater. The pie-chart in Fig. 3b displays the percentage of the literature available on dye removal using various adsorbents, where it can be observed that adsorbents such as polymer-based materials and activated carbon are studied more for the removal of dyes.

The possible responsible mechanisms (*i.e.*, surface complexation, electrostatic interaction, and van der Waals force) and processes (*i.e.*, surface diffusion and intraparticle pore diffusion) for the adsorption of dyes are discussed and shown in Tables 2–7. The detection wavelengths for the targeted dyes in the reported studies are also mentioned in Tables 2–7, which may be helpful for readers to measure the concentrations of these dyes. In the following sections, the above-mentioned adsorbents are discussed in detail. The classes of dye molecules, their ecotoxic effects, adsorptive removal of dyes using various classes of adsorbents together with their sub-categories, the critical influencing factors, and responsible adsorption mechanisms are displayed as a flow chart in Fig. 4.



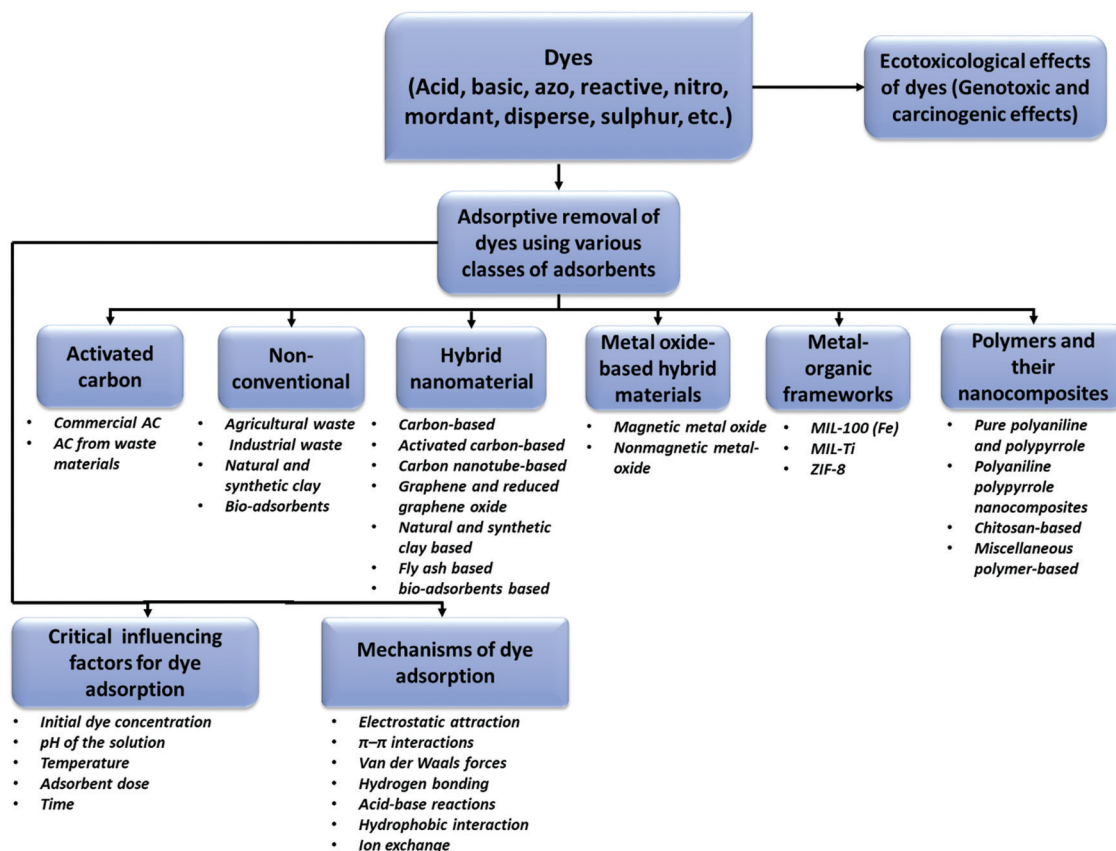


Fig. 4 Flow chart showing the classes of dye molecules, their ecotoxic effects, removal using different classes of adsorbents together with their sub-categories, critical influencing factors, and probable adsorption mechanisms.

4.1. Activated carbon

Activated carbon-based adsorbents are widely studied in the field of adsorption owing to their robust chemical stability, low density, structural diversity, and suitability for field-scale applications. These unique characteristics generally originate from their internal pore morphology, surface characteristics, porosity, pore volume, chemical structure, and presence of functional groups from their source material, including their activation.^{102–104} The commercial activated carbon and activated carbon synthesized from various waste materials are discussed in the subsequent section.

4.1.1 Commercial activated carbon. Researchers have reported the use of various commercial activated carbons as adsorbents for the separation of different dyes from wastewater.^{62,105,106} For instance, Malik (2004) developed an effective carbon-based adsorbent from mahogany sawdust and directly applied it to adsorb dyes. The experimental data well correlated with the Langmuir model, exhibiting an adsorption capacity of 518 and 327.9 mg g⁻¹ for Direct Blue 2B and Direct Green B dyes, respectively.¹⁰⁵ In another study, Mohammadi *et al.* reported the removal of an anionic dye (*i.e.*, MO) using mesoporous carbon CMK-3 (*i.e.*, carbon material kinetic-3) as an adsorbent and observed the extraction of the dye within 60 min. Further, their studies indicated that acidic media facilitated the removal of the dye more than basic media. An increase in the

initial dye concentration also has a positive effect on the adsorption capacity. The analyzed equilibrium data well fitted the Langmuir isotherm, following monolayer adsorption (adsorption capacity at 25 °C: 294.1 mg g⁻¹).⁶² In another study, Djilani *et al.* used activated carbon prepared from apricot stones and achieved an adsorption capacity of 36.68 and 32.25 mg g⁻¹ for MB and MO at a pH of 4.85 and 4.87, respectively. The corresponding adsorption data was found to be well correlated with the Langmuir isotherm.¹⁰⁶ In another study, Rahman (2021) used activated carbon synthesized from red oak (*i.e.*, *Quercus rubra*) for the adsorption of MB and observed adsorption efficiency of 97.18%.¹⁰⁷ According to Giannakoudakis *et al.*, the adsorption of Reactive Black 5 dye on the three different forms of commercial activated carbon, namely, Norit Darco 12 × 20 (DARCO), Norit R008 (R008), and Norit PK 1-3 (PK13) followed the Langmuir, Freundlich, and Langmuir–Freundlich models, achieving an adsorption capacity of 348, 527, and 394 mg g⁻¹ in 24 h by the corresponding commercial activated carbon as adsorbents, respectively.¹⁰⁸ Activated carbon was also produced from spent tea leaves (STAC) to remove malachite green (MG), which showed an adsorption capacity of 256.4 mg g⁻¹ at 45 °C. These studies showed an increment in the adsorption of MG from aqueous solution up to pH 4 and then became more or less unaltered at higher pH.¹⁰⁹



4.1.2 Activated carbon from waste materials. Different waste materials such as lemongrass leaf, rice husk, orange peel, and spent tea leaves have been reported as important sources for deriving activated carbon, which can be effectively applied as adsorbents in dye remediation.^{110–114} For example, Ahmad *et al.* utilized lemongrass leaf-based activated carbon to remediate methyl red from contaminated water. Their findings showed an optimum dye adsorption capacity of 76.923 mg g⁻¹ at pH 2 within 5 h. An increase in the adsorption rate of methyl red dye was mainly observed with an increase in temperature, dye concentration, and contact time. Their thermodynamic study indicated that the adsorption of methyl red dye is endothermic and follows a

physisorption process.¹¹⁰ In addition, Ding *et al.* treated rhodamine B using activated carbon obtained from treated rice husk and achieved its equilibrium removal (478.5 mg g⁻¹) within 5 h. The initial solution pH was found to have an insignificant effect on the adsorption of rhodamine B on the activated carbon.¹¹¹ In another work, Lam *et al.* reported an adsorption capacity of 28.5 mg g⁻¹ while investigating the adsorption of MG cationic dye using activated carbon prepared from orange peel.¹¹²

Jawad *et al.* prepared sulfuric acid-treated activated carbon derived from coconut leaves, exhibiting rough and irregular surfaces along with cavities, which was found to be a very effective adsorbent for MB dye (adsorption capacity: 149.3 mg g⁻¹). It is also found that the adsorption capacity increased with an increase in the initial concentration of MB.¹¹⁵ In another study, chemical activated carbon (ACC) prepared from jute sticks (morphological image is shown in Fig. 5) showed an adsorption capacity of 480 mg g⁻¹ for brilliant green dye.¹¹⁶ Guava leaf-based activated carbon exhibited a maximum adsorption capacity of 39.7 mg g⁻¹ to remove CR dye.¹¹⁷ Low-cost activated carbon derived from Brazilian agriculture waste was also used for the adsorption of dyes, including Basic Blue 26, Basic Green 1, Basic Yellow 2, and Basic Red 1, which exhibited an adsorption capacity in the range of 10–76 mg g⁻¹, 26–83 mg g⁻¹, 27–83 mg g⁻¹, and 21–70 mg g⁻¹, respectively.¹¹⁸ The adsorption performance of commercial activated carbon and activated carbon derived from various waste materials for the treatment of dye-contaminated water is presented in Table 2.

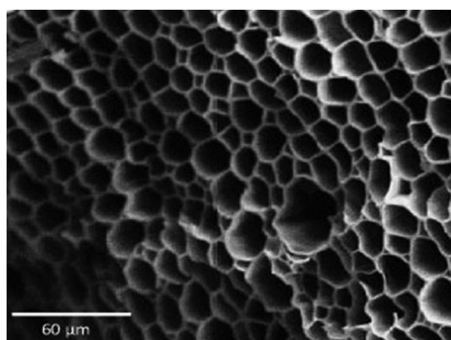


Fig. 5 Morphological image of chemical activated carbon (ACC) prepared from jute sticks [Reprinted with permission from ref. 116. Copyright 2010, Elsevier].

Table 2 Activated carbon (AC) as an adsorbent in dye removal

| Source of AC | Dyes | Experimental conditions | Adsorption capacity/ removal efficiency | Adsorption kinetics; isotherm; and mechanisms |
|---|--|--|---|---|
| Commercial activated carbon Saw-dust ¹⁰⁵ | Direct Blue 2B and Direct Green B | Time: 120 min pH: 3 | 518 and 327.9 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir isotherm model; chemisorption |
| Apricot stones and commercial activated carbon ¹⁰⁶ | Methylene blue (MB) and methyl orange (MO) | C_0 : 10 mg L ⁻¹ T : 298 K Dose: 0.5 g/50 mL pH: 4.85 (MB) and 4.87 (MO) Time: 60–180 min λ_{max} : 665 and 465 nm, respectively | Activated carbon prepared from apricot stones (ASAC): 36.68 and 32.25 mg g ⁻¹ , respectively. Commercial activated car- bon (CAC): 199.60 mg g ⁻¹ and 35.43 mg g ⁻¹ , respectively. | Pseudo-second-order kinetics; Langmuir isotherm; chemisorption and intraparticle diffusion |
| Mesoporous carbon material ⁶² | MO | Time: 60 min C_0 : 1000 mg L ⁻¹ Dose: 50 mg in 25 mL pH: 3–9 λ_{max} : 465 nm | 294.1 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; chemisorption |
| Red Oak (<i>Quercus rubra</i>) ¹⁰⁷ | MB | C_0 : 10 mg L ⁻¹ Dose: 0.25 g/50 mL pH: 10 T : 318 K Agitation speed: 175 rpm Time: 2 h λ_{max} : 660 nm | 97.18% | — |



Table 2 (continued)

| Source of AC | Dyes | Experimental conditions | Adsorption capacity/ removal efficiency | Adsorption kinetics; isotherm; and mechanisms |
|--|---|---|---|---|
| Norit Darco 12 × 20 (DARCO), Norit R008 (R008), and Norit PK 1-3 (PK13) ¹⁰⁸ | Reactive Black 5 | pH: 10 Dose: 1 g L ⁻¹ C ₀ : 500 mg L ⁻¹ Time: 24 h λ _{max} : 603 nm | 348, 527, and 394 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir or Langmuir–Freundlich model; intraparticle diffusion |
| Activated carbon from waste materials Lemongrass leaf ¹¹⁰ | Methyl red | pH: 2 Time: 5 h λ _{max} : 520 nm | 76.923 mg g ⁻¹ | Pseudo-first-order kinetics; Koble–Corrigan isotherm (R ² : 0.997); physisorption |
| Rice husk ¹¹¹ | Rhodamine B (RhB) | Time: 5 h pH < 3.20 T: 303 K λ _{max} : 554 nm | 478.5 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; chemisorption |
| Orange peel ¹¹² | Malachite green (MG) | C ₀ : 1 mg mL ⁻¹ λ _{max} : 617 nm | 28.5 mg g ⁻¹ | — |
| Coconut leaves ¹¹⁵ | MB | C ₀ : 30–400 mg L ⁻¹ pH: 3–11 | 149.3 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; physisorption |
| Guava leaf ¹¹⁷ | Congo red (CR) | C ₀ : 10–50 mg L ⁻¹ λ _{max} : 497 nm | 39.70 mg g ⁻¹ | Pseudo-second-order kinetics; Freundlich isotherm; multilayer adsorption |
| Brazilian low-cost agri-culture waste ¹¹⁸ | Basic Blue 26, Basic Green 1, Basic Yellow 2, and Basic Red 1 | C ₀ : 250 mg L ⁻¹ Dose: 0.3 g in 100 mL Time: 24 h λ _{max} : 618 nm, 625 nm, 433 nm, and 530 nm, respectively | 10–76, 26–83, 27–83, and 21–70 mg g ⁻¹ , respectively. | Electrostatic interactions |
| Spent tea leaves ¹⁰⁹ | MG | C ₀ : 220 mg L ⁻¹ Dose: 0.02 g/25 mL Time: 180 min λ _{max} : 617 nm | 256.4 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; chemisorption |
| Lemon peels/sodium alginate ¹¹⁹ | MB | C ₀ : 25 – 300 mg L ⁻¹ λ _{max} : 664 nm | 841.37 mg g ⁻¹ | Pseudo-first-order and pseudo-second-order kinetics; Langmuir isotherm; electrostatic interaction and external surface adsorption |

C₀: initial dye concentration; T: temperature; and λ_{max}: maximum wavelength detected for the analysis of dye.

4.2. Non-conventional adsorbents

In recent years, several non-conventional adsorbents have been gaining substantial attention as potential economic alternatives of costly adsorbent materials to remove toxic pollutants.¹²⁰ This includes the utilization of abundantly available agricultural, industrial, natural resources, bio wastes, *etc.* as waste materials. These waste materials prior to their application as adsorbents are subjected to various processes such as chemical treatment, conversion to powder form, and decomposition.^{60,121–123} Considering this, different waste materials to adsorb toxic dyes from contaminated water are described below.

4.2.1 Agricultural waste materials. Agricultural waste materials, such as raw maize cob, exhausted coffee ground powder, saw-dust, black cumin, neem leaf, pineapple leaf, and pine tree leaves, have been used by many researchers in dye remediation of contaminated water.^{60,121–125} Abubakar and Ibrahim (2019) used raw maize cob for the adsorption of bromophenol blue (96.5%) and bromothymol blue (94.4%) present in wastewater at the equilibrium time of 125 and 110 minutes, respectively. The effect of increasing the initial dye concentration on dye adsorption showed positive effects, and the dye adsorption followed the Temkin isotherm model.¹²² In another work, the adsorption of rhodamine B and rhodamine 6G on

exhausted coffee ground powder achieved an adsorption capacity of up to 5.3 and 17.4 μmol g⁻¹, respectively.⁶⁰ It was proposed that electrostatic, hydrophobic, and intermolecular interactions account for the adsorption of Rhodamine dye onto the adsorbent surface (Fig. 6). Sodium hydroxide-treated sawdust exhibited an adsorption

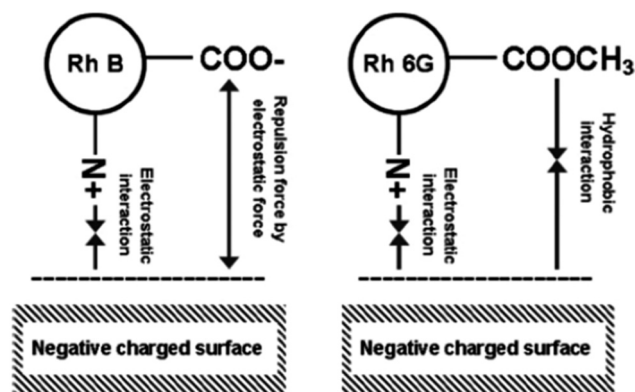


Fig. 6 Possible adsorption mechanisms on the surface of exhausted coffee ground powder [Reprinted with permission from ref. 60. Copyright 2017, Elsevier].



capacity of 55.86 mg g⁻¹ for brilliant green dye in 3 h.¹²¹ In a study by Siddiqui *et al.*, an antimicrobial *Nigella sativa* seed-based manganese dioxide/black cumin (MnO₂/BC) nanocomposite was used for the adsorption of MB (adsorption capacity: 185.19 mg g⁻¹ at pH 7.0 and 318 K). The process of adsorption was endothermic and best described by the Langmuir isotherm. The adsorption mechanism involved hydrogen bonding and electrostatic interactions of MB onto the surface of MnO₂/BC.¹²³ Pineapple leaf powder,¹²⁵ pine tree leaves,¹²⁶ and *Platanus orientalis* leaf powder¹²⁷ as adsorbents achieved the maximum removal capacities of 48.72, 71.94, and 114.94 mg g⁻¹, corresponding to the contact time of 150, 120, and 70 min in the removal of Basic green 4, Basic red 46, and MB dye, respectively. Neem leaf powder was also used for the adsorption of brilliant green dye,¹²⁴ which showed 0.554 mmol g⁻¹ adsorption capacity within 240 min. Microwave-assisted spent tea leaves exhibited a maximum adsorption capacity of 242.72 mg g⁻¹ for Eriochrome black-T adsorption in a contact time of 24 h.¹¹³

4.2.2 Industrial waste materials. Various industrial wastes, including fly ash, slurry, and ceramic wastes, have been regularly used as adsorbents for dye removal from contaminated water.^{128–131} Jain *et al.* used steel and fertilizer industrial waste as an adsorbent material for the adsorption of ethyl orange, metanil yellow, and Acid Blue 113 dyes. In this process, they achieved an adsorption capacity of 198, 211, and 219 mg g⁻¹, respectively.¹²⁸ Coal fly ash exhibited maximum removal efficiencies of more than 90% and up to 85% in 24 h for MB and crystal violet dyes, respectively.¹²⁹ Bhatnagar and Jain (2005) used carbonaceous slurry waste as an adsorbent to remove RhB and Bismark Brown R dye. They achieved an adsorption capacity of 91.1 and 85 mg g⁻¹ at a contact time of nearly 25 min for RhB and Bismark Brown R dye, respectively.¹³⁰ Ceramic adsorbents derived from industrial waste coal gangue achieved an adsorption capacity of 1.044 and 2.170 mg g⁻¹ for Cationic Red X-5GN and Cationic Blue X-GRRL dyes at a contact time of 180 min, respectively.¹³¹ The possible mechanisms displayed in Fig. 7 suggest electrostatic attraction, H-bonding, *etc.*, playing an essential role in the adsorption of

the X-5GN and X-GRRL dyes. Furthermore, industrial waste shells of eggs showed an adsorption capacity of 94.9 and 49.5 mg g⁻¹ in removing MB and CR, respectively.¹³²

4.2.3 Natural and synthetic clay. The easy availability, low cost, high porosity, high potential for ion exchange, and non-toxicity of several natural and synthetic clays have resulted in their significant use as adsorbents for dye removal from aqueous solution.^{133–136} For example, sulfuric acid-treated coal bearing kaolinite achieved a maximum adsorption capacity of MB dye corresponding to 101.5 mg g⁻¹.¹³³ In another work, the adsorptive behavior of RhB on sodium montmorillonite clay showed an adsorption capacity of 42.19 mg g⁻¹.¹³⁷ The adsorption process involved electrostatic attraction between the negatively charged adsorbent surfaces and positively charged cationic dye. Santos and Boaventura (2008) used sepiolite to remove Basic Red 46 and Direct Blue 85 dyes, achieving an adsorption capacity of 108 and 454 mg g⁻¹, respectively.¹³⁴ Acid-treated palygorskite was employed to remove crystal violet, cationic light yellow (7GL), MB, and MO dyes, exhibiting adsorption capacities of 223.43, 290.86, 86.53, and 276.11 mg g⁻¹, respectively.¹³⁶ Palygorskite modified by 3-aminopropyl triethoxysilane was successfully employed to remove reactive red 3BS, reactive blue KE-R, and reactive black GR dyes in 20 min with adsorption capacities of 34.23, 38.59, and 60.13 mg g⁻¹, respectively.¹³⁵ Kismir and Aroguz (2011) reported an adsorption capacity of 1.18 mg g⁻¹ for the adsorption of brilliant green dye on Saklikent mud as an adsorbent.¹³⁸ Flower-like¹³⁹ and hollow LDH¹⁴⁰ exhibited an adsorption capacity of 500.6 and 210 mg g⁻¹ in less than 10 min for methyl orange, respectively.

4.2.4 Bio-adsorbents. Significant advancement has been made in the field of dye removal from polluted water using biosorbents, such as *Spirulina platensis*, *Penaeus indicus* shrimp, cellulose, *Ganoderma lucidum*, wheat flour, and Graham flour.^{141–146} According to Dotto *et al.*, Acid Blue 9 and FD&C Red No. 40 were effectively adsorbed on the biosorbent synthesized from *Spirulina platensis*. The scanning electron microscopy (SEM) image of the *Spirulina platensis* biomass in Fig. 8 shows the presence of pores and cylindrical filaments on its surface, revealing the adsorption capability of *Spirulina platensis*. The experimental analysis showed a biosorption capacity of 400.3 and 1653.0 mg g⁻¹ for FD&C Red No. 40 and Acid Blue 9 dye, respectively, at initial solution pH of 2 and contact time of 100 min.¹⁴¹ The shell of *Penaeus indicus* shrimp was also found to be an effective adsorbent

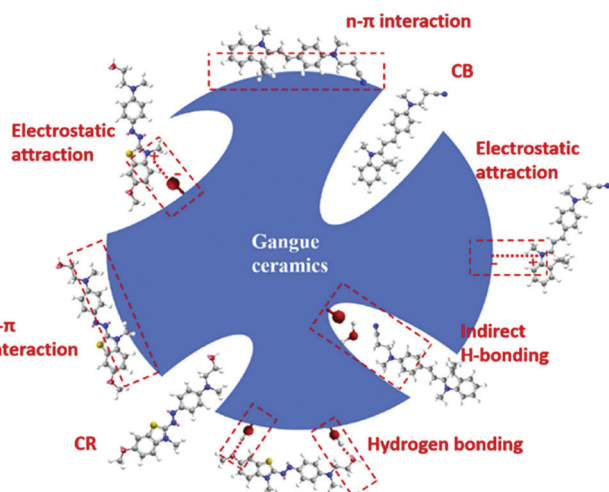


Fig. 7 Possible adsorption mechanisms of adsorption of cationic dyes by gangue ceramics [Reprinted with permission from ref. 131. Copyright 2019, Elsevier].

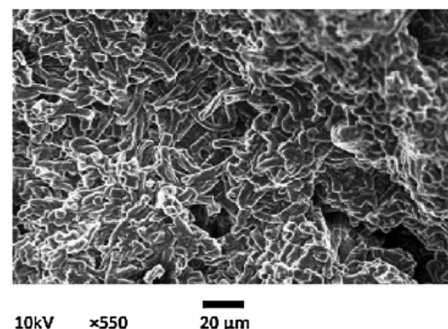


Fig. 8 Scanning electron microscopy image of *Spirulina platensis* biomass [Reprinted with permission from ref. 141. Copyright 2012 Elsevier].



for Acid Blue 25, and dye biosorption fitted well with the pseudo-second-order model.¹⁴² The optimum condition of this dye adsorption corresponds to pH 2 and 0.1 g L⁻¹ dose, resulting in an adsorption capacity of 1093 mg g⁻¹. The adsorption capacities of 2.197, 2.120, 2.038, and 1.480 mg g⁻¹ were achieved on neem sawdust for the removal of crystal violet, MB, MG, and RhB dyes, respectively, from contaminated water in 30 min.¹⁴⁷ The adsorption capacities of 1201 and 1070 mg g⁻¹ were observed

within 3 h on cellulose nanocrystal-reinforced keratin for the adsorption of Reactive Black 5 and Direct Red 80, respectively.¹⁴³ The adsorption process of both the dyes was well correlated with the Langmuir isotherm. Wu *et al.* used the spent substrate of *Ganoderma lucidum* for removing MG, safranin T, and MB dyes and observed the adsorption capacities of 40.65, 33, and 22.37 mg g⁻¹, respectively, in 4 h.¹⁴⁴ The adsorption performances of various non-conventional adsorbents are listed in Table 3.

Table 3 Non-conventional adsorbents in dye removal

| Examples of adsorbents | Dyes | Experimental conditions | Adsorption capacity/ removal efficiency | Adsorption kinetics; isotherm; and mechanisms |
|--|---|---|---|--|
| Waste materials from agricultural | | | | |
| Raw maize cob ¹²² | Bromophenol blue and bromothymol blue | C ₀ : 10–100 mg L ⁻¹ Dose: 0.5–4.0 g Time: 125 and 110 min, respectively λ_{max} : 591.22 and 430.9 nm, respectively | 96.53%, and 94.39%, respectively | Pseudo-second-order kinetics; Temkin isotherm; chemisorption |
| Exhausted coffee ground powder ⁶⁰ | Rhodamine (Rh) dye (Rh B and Rh 6G) | Dose: 50 mg/50 mL Time: 3 h λ_{max} : 554 and 526 nm, respectively | 5.255 and 17.369 $\mu\text{mol g}^{-1}$ | Pseudo-first-order kinetics and pseudo-second-order kinetics; Langmuir isotherm; chemisorption |
| NaOH treated saw dust ¹²¹ | Brilliant green | Time: 3 h Dose: 4 g L ⁻¹ C ₀ : 100 mg L ⁻¹ T: 303 K | 55.86 mg g ⁻¹ | Pseudo-second-order kinetics; Temkin and Redlich–Peterson isotherm; physisorption and boundary layer diffusion |
| <i>Nigella sativa</i> seed-based nanocomposite-MnO ₂ /BC ¹²³ | MB | Dose: 1.0 g L ⁻¹ C ₀ : 10 mg L ⁻¹ λ_{max} : 660 nm | 185.185 mg g ⁻¹ | Pseudo-second-order kinetics; Freundlich isotherm; intraparticle diffusion, and film diffusion action |
| Neem leaf powder ¹²⁴ | Brilliant green | C ₀ : 10–50 mg/dm ³ Time: 4 h T: 300 K λ_{max} : 624 nm C ₀ : 50 mg L ⁻¹ pH: 9.0 Time: 150 min Dose: 5 g L ⁻¹ T: 298 K λ_{max} : 618 nm | 0.149 to 0.554 mmol g ⁻¹ | First-order kinetics; Langmuir isotherm; external surface and pore diffusion |
| Pineapple leaf ¹²⁵ | Basic green 4 (BG4) | C ₀ : 20–100 mg L ⁻¹ Dose: 1–6 g L ⁻¹ T: 298–318 K Time: 0–120 min λ_{max} : 530 nm | 48.72 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; chemisorption |
| Pine tree leaves ¹²⁶ | Basic Red 46 (BR 46) | C ₀ : 20–100 mg L ⁻¹ Dose: 1–6 g L ⁻¹ T: 298–318 K Time: 0–120 min λ_{max} : 530 nm | 71.94 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; physisorption |
| <i>Platanusorientalis</i> leaf ¹²⁷ | MB | C ₀ : 20–180 mg L ⁻¹ Dose: 80 mg/50 mL T: 25–60 °C Time: 0–70 min λ_{max} : 664 nm | 114.94 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; endothermic adsorption |
| Microwave-assisted spent black tea leaves ¹¹³ | Eriochrome black T (EBT) | C ₀ : 10–400 mg L ⁻¹ Dose: 0.25–5.0 g L ⁻¹ T: 298–338 K Time: 24 h λ_{max} : 518 nm | 242.72 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; physico-chemical interaction |
| Rice husk ¹⁴⁸ | MB | C ₀ : 100 mg L ⁻¹ Dose: 250 mg L ⁻¹ pH: 10 T: 298 K λ_{max} : 664 nm | 1350 mg g ⁻¹ | Pseudo-first-order kinetics; Freundlich and Sips isotherm; electrostatic interaction |
| Waste materials from industry | | | | |
| Steel and fertilizer industries wastes ¹²⁸ | Ethyl orange, metanil yellow, and Acid Blue 113 | Time: 3 h pH: 7 \pm 0.5 λ_{max} : 475 nm, 432 nm, and 532 nm, respectively | 198 mg g ⁻¹ , 211 mg g ⁻¹ , and 219 mg g ⁻¹ , respectively | Pseudo-first-order kinetics; Langmuir isotherm; physisorption |
| Coal fly ash ¹²⁹ | MB and crystal violet (CV) | Dose: 0.08 g L ⁻¹ Time: 24 h λ_{max} : 665 nm and 590 nm, respectively | CV: > 90% MB: < 85% | Pseudo-second-order kinetics; Langmuir isotherm; endothermic adsorption for CV and exothermic reaction for MB dye. |



Table 3 (continued)

| Examples of adsorbents | Dyes | Experimental conditions | Adsorption capacity/ removal efficiency | Adsorption kinetics; isotherm; and mechanisms |
|---|--|--|--|--|
| Amine-functionalized biomass fly ash ¹⁴⁹ | Alizarin red S (ARS) and bromothymol blue (BTB) | Time: 10 min and 5 min, respectively λ_{max} : 422 nm and 432 nm, respectively pH: 5.5–6.5 | 13.42 and 15.44 mg g ⁻¹ , respectively | Linear pseudo-second-order kinetics; modified Langmuir–Freundlich isotherm; electrostatic interaction |
| Carbonaceous slurry waste ¹³⁰ | RhB and Bismark Brown R | Time: ~25 min λ_{max} : 554 nm and 460 nm, respectively | 91.1 mg g ⁻¹ and 85 mg g ⁻¹ , respectively | First-order and pore-diffusion; Langmuir isotherm; physisorption |
| Industrial waste coal gangue ¹³¹ | Cationic Red X-5GN (CR) and Cationic Blue X-GRRL (CB) | Time: 3 h pH: 2–12 | 1.044 mg g ⁻¹ and 2.170 mg g ⁻¹ , respectively | Pseudo-second-order and Elovich kinetics; Freundlich isotherm for CR and Langmuir isotherm for CB dye; electrostatic attraction, n- π interactions, and hydrogen bonding |
| Industrial waste shells of egg ¹³² | MB and CR | C_0 : 50–1000 mg L ⁻¹ T : room temperature Time: 10–120 min | 94.9 mg g ⁻¹ and 49.5 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Freundlich isotherm; Electrical double layer mechanism, and electrostatic attraction for MB and CR dye, respectively |
| Natural and synthetic materials Green clay minerals ¹⁵⁰ | MB | Time: 60 min 300 rpm Dose: 200 mg/250 mL T : 293 K λ_{max} : 665 nm Dose: 10 mg/100 mL pH: 7 λ_{max} : 530 nm | 241.96 mg g ⁻¹ | Langmuir isotherm; single-layer adsorption |
| Natural clay ¹⁵¹ | Basic Red 46 | Dose: 10 mg/100 mL pH: 7 λ_{max} : 530 nm | 594 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic interactions, including hydrogen bonding |
| Sodium montmorillonite ¹³⁷ | RhB | pH: 7 λ_{max} : 554 nm | 42.19 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; high electrostatic attraction |
| Sepiolite ¹³⁴ | Astrazon Red (Basic Red 46) and Sirius Blue (Direct Blue 85) | C_0 : 75 mg L ⁻¹ and 150 mg L ⁻¹ , respectively pH: 8 and 3.5, respectively T : 313 K and 303 K, respectively. λ_{max} : 525 nm and 590 nm, respectively | 108 mg g ⁻¹ and 454 mg g ⁻¹ , respectively | Langmuir isotherm and Freundlich isotherm; physisorption |
| Acid-treated palygorskite ¹³⁶ | Crystal violet (CV), cationic light yellow (7GL), MB, and MO | C_0 : CV, 7GL, MB, and MO, were 500, 500, 200, 500, and 200 mg dm ⁻³ , respectively. λ_{max} : 581, 415, 662, 463, and 642 nm, respectively | CV: 223.43 mg g ⁻¹ 7GL: 290.86 mg g ⁻¹ MB: 86.53 mg g ⁻¹ MO: 276.11 mg g ⁻¹ | Sips and Langmuir isotherm; bridging effect mechanism |
| Palygorskite modified by 3-aminopropyl triethoxysilane ¹³⁵ | Reactive red 3BS, reactive blue KE-R, and reactive black GR | Time: 20 min C_0 : 20–600 mg L ⁻¹ pH: 2–12 λ_{max} : 546 nm, 620 nm, and 602 nm, respectively | 34.23 mg g ⁻¹ , 38.59 mg g ⁻¹ , and 60.13 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic attraction |
| Saklikent mud ¹³⁸ | Brilliant green | C_0 : 1–20 mg L ⁻¹ Dose: 0.1 g/50 mL | 1.18 mg g ⁻¹ | Pseudo-first-order kinetics and intra-particle model at 25 °C and pseudo-second-order kinetics at the higher temperature. Langmuir isotherm; electrostatic attraction |
| Flower-like LDH ¹³⁹ | MO | λ_{max} : 625 nm C_0 : 100 mg L ⁻¹ Dose: 1 g pH: 3 T : 298 K | 500.6 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; chemisorption |
| Hollow LDH nanowires ¹⁴⁰ | MO | Time: 10 min C_0 : 5–40 mg L ⁻¹ Dose: 0.5 g L ⁻¹ Time: 90% removal at <10 min | 210 mg g ⁻¹ | Langmuir isotherm |



Table 3 (continued)

| Examples of adsorbents | Dyes | Experimental conditions | Adsorption capacity/ removal efficiency | Adsorption kinetics; isotherm; and mechanisms |
|--|---|--|--|--|
| Bio-adsorbents | | | | |
| <i>Spirulina platensis</i> ¹⁴¹ | Acid blue 9 and FD&C Red No. 40 | pH: 2 Agitation speed: 400 rpm and 225 rpm for Acid Blue 9 and FD&C Red No. 40, respectively. Time: 20–100 min λ_{max} : 408 and 500 nm, respectively. | 1653.0 mg g ⁻¹ and 400.3 mg g ⁻¹ , respectively, 95% for both | Avrami kinetic; electrostatic attraction |
| Shrimp shell ¹⁴² | Acid blue 25 | pH: 2 Dose: 0.1–0.4 g L ⁻¹ Time: 30 min λ_{max} : 600 nm | 1093 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir, Freundlich and Temkin isotherm; physisorption |
| Neem sawdust ¹⁴⁷ | CV, MB, MG, and RhB | C_0 : 6–12 mg L ⁻¹ Dose: 0.5 g in 100 mL T : 25–45 °C pH: 7.2 Time: 30 min λ_{max} : 592 nm, 664 nm, 616 nm, and 555 nm, respectively | 2.197, 2.120, 2.038, 1.480 mg g ⁻¹ , respectively | |
| Cellulose nanocrystal-reinforced keratin ¹⁴³ | Reactive Black 5 and Direct Red 80 | C_0 : 200 mg L ⁻¹ Time: 3 h pH: 3 Dose: 0.1 g/200 mL λ_{max} : 595 nm and 543 nm, respectively | 1201 mg g ⁻¹ and 1070 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic interaction |
| Spent substrate of <i>Ganodermalucidum</i> ¹⁴⁴ | MG, safranin T, and MB | C_0 : 10–120 mg L ⁻¹ pH: 6 Time: 4 h λ_{max} : 617 nm, 530 nm, and 664 nm, respectively | 40.65 mg g ⁻¹ , 33 mg g ⁻¹ , and 22.37 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Freundlich isotherm; chemisorption |
| Carbohydrate polymeric biodegradable adsorbent of wheat flour ¹⁴⁵ | Rhodamine B (RhB) | C_0 : 5.0 mg L ⁻¹ pH: 5.5 | 142.26 mg g ⁻¹ | Langmuir adsorption; electrostatic interaction, π – π conjugation, and hydrogen bonding conjugation |
| Wood-based colloidal cellulose nanocrystals ¹⁵² | Auramine O (AO) | pH: not adjusted C_0 : 2.5–30 mg L ⁻¹ λ_{max} : 430 nm | 20 mg g ⁻¹ | Pseudo-second-order kinetics; Freundlich isotherm; electrostatic interactions and hydrogen bonding |
| Egg shell membrane ¹⁵³ | Basic Fuchsin (BF) | pH: 6 Time: 25 min T : 298 K | 48 mg g ⁻¹ | Pseudo-second-order kinetics; Freundlich isotherm; electrostatic interactions |
| Arginine-modified starch resin ¹⁵⁴ | Acid fuchsin (AF) and Acid Orange G (AOG) | C_0 : 0.25 mmol/L Dose: 0.1 g/20 mL Time: 1 h T : 298 K | AF: 21.326 mg g ⁻¹ AOG: 23.485 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic attractions, prevalent hydrogen bonds, and hydrophobic interactions (van der Waals force) |

C_0 : initial dye concentration; T : temperature; and λ_{max} : maximum wavelength detected for the analysis of dye.

4.3. Hybrid nanomaterials

Nanomaterials have been extensively used for water treatment applications because of their enhanced surface area and high adsorption-to-mass ratio. Accordingly, the combination of two or more nanomaterials, which is referred to as hybrid nanomaterials, exhibits multi-functionalities found to be very effective to remove dyes from contaminated water, as described below.¹⁵⁵

4.3.1 Carbon-based hybrid nanocomposite. Carbon-based hybrid nanocomposites are associated with easy synthesis, cost-effectiveness, availability, non-toxicity, high porosity, *etc.*, similar to other carbon-based nanocomposites. Ultrafine nickel/carbon (dose: 2 g L⁻¹) on treatment with RhB and MB showed an adsorption capacity of 5.269 and 7.415 mg g⁻¹, respectively.¹⁵⁶ Manippady *et al.* investigated the adsorption of CR and MB dye

onto iron-carbon hybrid magnetic nanosheets and achieved an adsorption capacity of 531.9 and 185.2 mg g⁻¹, respectively, in 24 min.¹⁵⁷ In another study, a porous silicon-carbon-nitrogen (Si-C-N) hybrid was employed to remove methyl blue and acid fuchsin dyes, achieving an adsorption capacity of 1327.7 and 1084.5 mg g⁻¹, respectively.¹⁵⁸ The possible mechanism displayed in Fig. 9 suggests the presence of electrostatic interactions and van der Waals forces between the adsorbent and dye. An Ni/porous carbon nanotube nanocomposite was used to remove MG, CR, RhB, MB, and MO dye, exhibiting adsorption capacities of 898, 818, 395, 312, and 271 mg g⁻¹, respectively.¹⁵⁹

4.3.2 Activated carbon-based hybrid nanocomposites. Activated carbon-based hybrid nanocomposites have been widely used in the purification of contaminated water. Wang *et al.* observed an adsorption capacity of 416.67 mg g⁻¹ (303 K) using



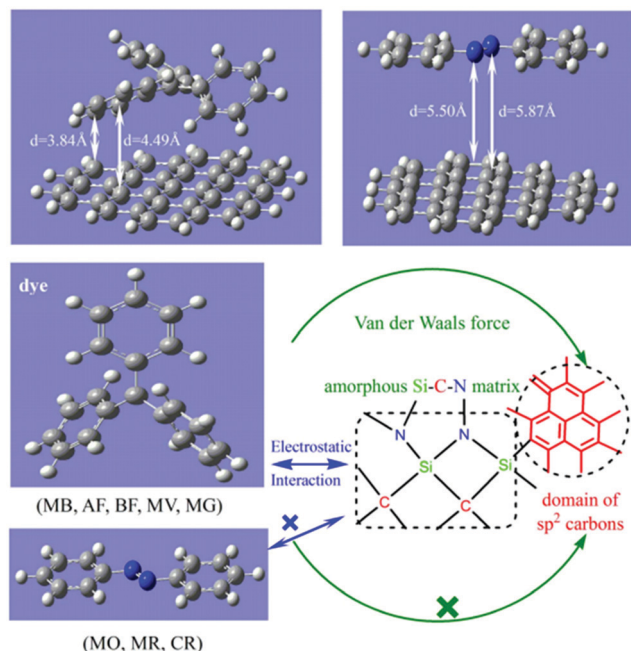


Fig. 9 Adsorption mechanisms for porous Si-C-N hybrid material [Reprinted with permission from ref. 158. Copyright 2015, Nature Research].

activated carbon aerogel immobilized with konjac glucomannan for the removal of MB.¹⁶⁰ In another study, ZnO nanoparticles loaded on *Parthenium* weed activated carbon achieved more than 99% removal of MB in 60 min.¹⁶¹ The adsorption of RhB and Orange G using sulfonic acid-modified activated carbon resulted in an adsorption capacity of 757.6 and 318.5 mg g⁻¹, respectively.¹⁶² Gong *et al.* used activated carbon synthesized from finger citron residue as a new type of adsorbent for the removal of harmful dyes, namely, anionic dyes such as MO and cationic dyes such as MB, from contaminated water, achieving an adsorption capacity of 934.58 (MO) and 581.40 mg g⁻¹ (MB).¹⁶³

4.3.3 Carbon nanotube-based hybrid nanomaterials. Recently, carbon nanotube (CNT)-based nanohybrid materials have received tremendous attention because of their high specific surface area, small sizes, and hollow structures.^{164,165} According to Gong *et al.*, these hybrids are more efficient for the adsorption of organic contaminants compared to even activated carbon.⁷⁰ Thus, the unique features of carbon nanotubes have been supplemented in the formation of several nanocomposites for dye removal from contaminated water. CNTs exhibited an adsorption capacity of 44.64 mg g⁻¹ for CI Reactive Red 2 dye.¹⁶⁶ Magnetic multi-walled CNT (MMWCNT) exhibited a poor adsorption performance for MB, neutral red, and brilliant cresyl blue dyes.⁷⁰ In another study, Yao *et al.* achieved a maximum adsorption capacity of 51.74 mg g⁻¹ MO dye on MMWCNT from wastewater.¹⁶⁷ Further, Sui *et al.* studied the adsorption of MB and MO on a synthesized calcium alginate/MWCNT hybrid and reported the maximum adsorption capacity of 606.1 and 12.5 mg g⁻¹, respectively.¹⁶⁸ HNO₃/NaClO/MWCNT nanohybrid¹⁶⁹ and magnetite/MWCNT¹⁷⁰ hybrid materials showed a maximum adsorption capacity of 55 and 48.06 mg g⁻¹ for the removal of bromothymol blue and MB dyes, respectively.

4.3.4 Graphene and reduced graphene oxide nanocomposites. Graphene oxide (GO) has been used as an adsorbent for dye removal from wastewater, such as Direct Red 81 and Indosol SFGL direct blue,¹⁷¹ crystal violet and methyl orange,¹⁷² and methylene blue.^{173–176} The adsorption mechanism involves strong interactions between graphene oxide (functionalized with hydroxyl and carboxylic groups) and active functional groups present in the dye.^{171,177} In addition, several studies have also been reported on GO and reduced graphene oxide (rGO)-based nanocomposites for the adsorption of dye from contaminated water. Zheng *et al.* prepared a 3D hierarchical GO-NiFe layered double hydroxide (LDH) sandwich hybrid as an adsorbent for the removal of CR and MO dye. Fig. 10 shows that the GO-NiFe-LDH is comprised of a hierarchically well-ordered structure, and both sides of GO are fully protected by ultrathin NiFe-LDH nanosheets, resulting in a sandwich-like architecture. The hybrid exhibited higher adsorption phenomena for CR and MO, as evident from the adsorption capacity values of 489 and 438 mg g⁻¹, respectively. This was ascribed to the presence of electrostatic attraction and ion exchange reactions between the dye molecules and hybrid adsorbents.¹⁷⁸ In another work, graphene/polyaniline (PANI)/Fe₃O₄ was used as a nano-adsorbent for the removal of CR from dye contaminated water.¹⁷⁹ It showed an excellent adsorption performance (adsorption capacity: 248.76 mg g⁻¹) for CR dye. MB dye (initial concentration: 250 mg L⁻¹) on treatment with GO showed an adsorption capacity of about 714 mg g⁻¹.¹⁷⁴ In another work, graphite oxide was used as an adsorbent to separate MB and MG dyes, with maximum adsorption capacities of 351 and 248 mg g⁻¹, respectively.¹⁸⁰ Heidarizad and Şengör (2016) used GO/magnesium oxide nanocomposites for the removal of MB dye and achieved an adsorption capacity of 833 mg g⁻¹ in a contact time up to 60 min.¹⁸¹ Investigations have also been reported using a combination of magnetic Fe₃O₄/carboxylate GO¹⁸² and GO/Fe₃O₄¹⁸³ nanostructures as adsorbents in dye removal. It was inferred that GO/Fe₃O₄ and Fe₃O₄/carboxylate GO achieved complete removal (MB) and maximum adsorption capacity of 36 mg g⁻¹ (MB) and 22.1 mg g⁻¹ (RhB), respectively.

Further, GO-based nanocomposites have been reported for dye removal such as porous core-shell graphene/SiO₂ nanocomposites for the removal of cationic neutral red dye,¹⁸⁴ whereas GO-shielded Mg-Al-LDH,¹⁸⁵ Au nanorod-doped Cu₂O core-shell nanocube-embedded rGO composite,¹⁸⁶ and GO-fabricated Fe-Al

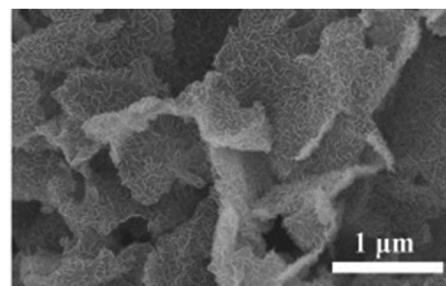


Fig. 10 FE-SEM image of GO-NiFe LDH [Reprinted with permission from ref. 178. Copyright 2019, Elsevier].



bimetal oxide composite¹⁸⁷ were reported for the removal of MB. Several other GO-based nanocomposites have also been reported to adsorb various classes of dyes, for example, the removal of MB using impregnated graphene in porous wood filters,¹⁸⁸ Fe₃O₄/GO composite,¹⁸⁹ Fe₃O₄ nanoparticle-functionalized GO/g-C₃N₄ nanocomposite,¹⁹⁰ and metal ferrite-enabled GO¹⁹¹ and PANI-GO-Fe₃O₄ hybrid nanocomposite¹⁹² for the removal of CR and MO.

4.3.5 Hybrids of natural and synthetic clay. Hybrids adsorbents comprised of natural and synthetic clay-based materials possess several advantages, such as low cost, non-toxicity, thermal resistance, porosity, ion exchange ability, and the possibility of modification with various functionalities.¹⁹³ Consequently, nanohybrids of natural and synthetic clay have been harnessed as adsorbents to remove dyes from wastewater. According to Marrakchi *et al.*, the maximum adsorption capacity of 40.97 and 190.97 mg g⁻¹ was achieved in 30 h on cross-linked chitosan/sepiolite clay for MB and reactive orange, respectively.¹⁹⁴ The removal efficiency of MO dye on an Mg-Al-layered double hydroxide supported MOF exceeded 99% at the onset of 20 min.¹⁹⁵ The adsorptive removal of reactive red, CR, and Acid Red 1 on an Mg-Al-layered double hydroxide fitted well with the Langmuir model.¹⁹⁶ The layered double hydroxide nanohybrid (Mg-Al-NO₃) exhibited a maximum adsorption capacity of 0.8, 1.089, and 1.418 mmol g⁻¹ for the adsorption of amaranth, diamine green B, and brilliant green dyes, respectively.¹⁹⁷

4.3.6 Hybrids of fly ash. Fly ash is generally considered a by-product from coal-based industries and is often used either alone or in combination with other materials as a hybrid adsorbent in water purification.^{198,199} This is mainly attributed to its high porosity, economic viability, and easy availability.²⁰⁰

The adsorption study on MB dye using fly ash geopolymer monoliths attained a maximum adsorption capacity of 15.4 mg g⁻¹ in 30 h and the adsorbent could be reused for up to five cycles.¹⁹⁹ Novais *et al.* reported the adsorption of MB dye on porous biomass fly ash-based geopolymer spheres. The findings showed an adsorption capacity of 79.7 mg g⁻¹ in 30 h and reusability for up to eight cycles.¹⁹⁸ Further, Duta and Visa (2015) conducted a study on the adsorption of a mixture of bemacid red and bemacid blue dye on fly ash-TiO₂ and noted the adsorption capacity of 4.0 and 1.2 mg g⁻¹, respectively.²⁰¹ In another study, a maximum adsorption capacity of 24.8 mg g⁻¹ was reported for the adsorption of Orange II dye on Ca(OH)₂/Na₂FeO₄ modified fly ash.²⁰²

4.3.7 Hybrids of bio-adsorbents. Bio-adsorbents can be easily modified and blended with other components, making them suitable as adsorbents for the removal of dyes from contaminated water. Cross-linked beads of an activated oil palm ash zeolite/chitosan composite showed an adsorption capacity of 199.2 and 270.27 mg g⁻¹ for MB and acid blue dye, respectively.²⁰³ Liu *et al.* reported that cellulose-*g*-poly(acrylic acid-co-acrylamide) exhibited an adsorption capacity of 1602 and 1814 mg g⁻¹ for of Acid Blue 93 and MB dye, respectively.²⁰⁴ A sulphonated bio-adsorbent from waste hawthorn kernel as adsorbent attained a maximum adsorption capacity of 151.5 mg g⁻¹ for MB dye with a contact time of up to 6 h.²⁰⁵ In another work, an adsorption study was conducted for the removal of MB dye on agricultural waste/GO.²⁰⁶ This study revealed a maximum adsorption capacity of 414.03 mg g⁻¹ (pH = 12) with the successful reuse of the adsorbent for up to five cycles. Further, the dye adsorption was well correlated with the Temkin isotherm. The performance of various hybrid materials as adsorbents for the treatment of dyes is presented in Table 4.

Table 4 Hybrid nanomaterial as adsorbents for dye removal

| Adsorbent | Dyes | Experimental conditions | Adsorption capacity/ removal efficiency | Adsorption kinetics, isotherm, and mechanisms |
|--|---------------------------------|---|--|--|
| Carbon-based hybrid nanocomposite Ultrafine Ni/C ¹⁵⁶ | RhB and MB | Dose: 2 g L ⁻¹ C ₀ : 5 mg L ⁻¹ Time: 2 h λ _{max} : 554 and 664 nm, respectively | 5.269 and 7.415 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Freundlich isotherm; chemisorption process |
| Iron-carbon hybrid magnetic nanosheets ¹⁵⁷ | CR and MB | Time: 24 min pH: 2 and 8, respectively Dose: 6 mg/15 mL λ _{max} : 662 and 664 nm, respectively | 531.9 and 185.2 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir isotherm; chemisorption |
| Hierarchically porous silicon-carbon-nitrogen hybrid materials ¹⁵⁸ | Methyl blue and acid fuchsin | C ₀ : 300 mg L ⁻¹ and 200 mg L ⁻¹ , respectively | 1327.7 mg g ⁻¹ and 1084.5 mg g ⁻¹ respectively | Pseudo-second-order kinetics; Langmuir isotherm; Chemisorption |
| Ni/porous carbon-CNT ¹⁵⁹ | MG, CR, RhB, MB, and MO | C ₀ : 20 mg L ⁻¹ Time: 60 min | 898 mg g ⁻¹ , 818 mg g ⁻¹ , 395 mg g ⁻¹ , 312 mg g ⁻¹ , and 271 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir isotherm; multilayer adsorption mechanism |
| Activated carbon-based hybrid nanocomposites Konjac glucomannan/ activated carbon aerogel ¹⁶⁰ | MB | C ₀ : 140 mg L ⁻¹ Dose: 10 mg/20 mL T: 313 K | 416.67 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; density gra- dient force and hydrogen bond interaction |



Table 4 (continued)

| Adsorbent | Dyes | Experimental conditions | Adsorption capacity/ removal efficiency | Adsorption kinetics, isotherm, and mechanisms |
|--|--|--|---|---|
| ZnO-NP-loaded <i>Parthenium</i> weed activated carbon (ZnONPs-PWAC) ¹⁶¹ | MB | C_0 : 100 mg L ⁻¹ pH: 6 Dose: 50 mg/100 mL Time: 60 min λ_{max} : 670 nm | ~ 99% | — |
| Sulfonic acid-modified activated carbon (MTLAC-SA) and MTLAC ¹⁶² | RhB and Orange G | C_0 : 200–800 mg L ⁻¹ λ_{max} : 664 nm and 476 nm, respectively | 757.6 mg g ⁻¹ using MTLAC-SA and 318.5 mg g ⁻¹ using MTLAC, respectively | Pseudo-second-order kinetics; Langmuir isotherm; homogeneous adsorption |
| Finger-citron-residue-based activated carbon ¹⁶³ | MO and MB | C_0 : 50–500 mg L ⁻¹ λ_{max} : 464 nm and 664 nm, respectively | 934.58 and 581.40 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir isotherm; π - π stacking interaction and electrostatic attraction |
| Carbon nanotubes ¹⁶⁶ | Procion Red MX-5B (CI reactive red 2) | Dose: < 0.25 g L ⁻¹ pH: 6.5 T: 291 K λ_{max} : 538 nm | 44.64 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; physisorption |
| Calcium alginate/multi-walled carbon nanotubes ¹⁶⁸ | MB and MO | pH: 4–12 for MB and <2 for MO | 606.1 and 12.5 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir isotherm; Opposite charge attraction |
| Magnetic multi-wall carbon nanotube ⁷⁰ | MB, neutral red, and brilliant cresyl blue | C_0 : 1.4–37.4 mg L ⁻¹ Dose: 0.5 g L ⁻¹ pH: ~7 | 15.74 mg g ⁻¹ , 20.33 mg g ⁻¹ , and 23.55 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Freundlich isotherm; van der Waals interactions occurring |
| Multi-wall carbon nanotubes ¹⁶⁷ | MO | C_0 : 20 mg L ⁻¹ T: 25 °C pH: ~7 Time: 2 h Dose: 15 mg/50 mL λ_{max} : 460 nm | 51.74 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; external diffusion, boundary layer diffusion, and intra-particle diffusion |
| Magnetite-loaded multi-walled carbon nanotubes ¹⁷⁰ | MB | C_0 : 20 mg L ⁻¹ Dose: 0.02 g/50 mL T: 25 ± 1 °C pH: 7 | 48.06 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic attraction and π - π stacking interactions |
| Magnetite/MWCNTs ¹⁶⁹ | MB | C_0 : 10–70 mg L ⁻¹ Dose: 0.02 g/25 mL Time: 0–11 min pH: 1 | 55 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic interactions, π - π dispersion interaction, hydrogen bonding, and electron donor-acceptor complex formation. |
| Graphene oxide, reduced graphene oxide, and their 3D hierarchical GO-NiFe LDH composite ¹⁷⁸ | CR and MO | Time: 225 min and 135 min, respectively | 489 and 438 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic attraction, ions exchange, and π - π stacking interaction |
| Graphene/PANI/Fe ₃ O ₄ ¹⁷⁹ | CR | C_0 : 100 mg L ⁻¹ Time: 2 h Dose: 25 mg/25 mL λ_{max} : 625 nm and 498 nm, respectively | 248.76 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic interaction, hydrogen bond, and π - π stacking interaction |
| Graphene oxide ¹⁷⁴ | MB | C_0 : < 250 mg L ⁻¹ λ_{max} : 664 nm | 714 mg g ⁻¹ | Freundlich isotherm; exothermal adsorption reaction, and π - π stacking interaction |
| Layered graphite oxide ¹⁸⁰ | MB and MG | Dose: 10 mg/500 mL λ_{max} : 663 nm and 617 nm, respectively | 351 mg g ⁻¹ and 248 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic attraction |
| Graphene oxide/magnesium oxide nanocomposites ¹⁸¹ | MB | C_0 : 5–100 mg L ⁻¹ Time: 5–60 min Dose: 0.1–1 g L ⁻¹ pH: 11 λ_{max} : 664 nm | 833 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic attraction, hydrogen bonding, and π - π interaction |
| GO/Fe ₃ O ₄ nanohybrids ¹⁸³ | MB | C_0 : 20 mg L ⁻¹ Dose: 3 mg/5 mL pH: 6 λ_{max} : 664 nm | ~ 100% | Adsorption mechanism followed by π - π interaction |
| Sandwiched Fe ₃ O ₄ /carboxylate graphene oxide nanostructures ¹⁸² | MB and RhB | C_0 : 10 mg L ⁻¹ MB and 5 mg L ⁻¹ RhB pH: 6 λ_{max} : 632 nm and 554 nm, respectively | 36 mg g ⁻¹ and 22.1 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; electrostatic attraction |



Table 4 (continued)

| Adsorbent | Dyes | Experimental conditions | Adsorption capacity/ removal efficiency | Adsorption kinetics, isotherm, and mechanisms |
|--|--|--|---|---|
| Magnetic GO/poly(vinyl alcohol) composite gels ²⁰⁷ | MB and methyl violet (MV) | Dose: 20 mg/5 mL C_0 : 0.2 mM Time: 0.5 h λ_{\max} : 662 nm and 583 nm, respectively | 270.94 and 221.23 mg g ⁻¹ , respectively | Pseudo-second-order kinetics, Langmuir isotherm; strong electrostatic attraction and complexation |
| Hybrids of natural and synthetic clay Cross-linked chitosan/sepiolite clay composite ¹⁹⁴ | MB and Reactive orange 16 | C_0 : 100 mg L ⁻¹ Dose: 2 g L ⁻¹ Time: 30 h pH: > 9 for MB and 3 for reactive orange 16 λ_{\max} : 665 nm and 496 nm, respectively | 40.986 mg g ⁻¹ and 190.965 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Freundlich isotherm; physisorption |
| MgAl-layered double hydroxide supported MOF ¹⁹⁵ | MO | Time: 20 min C_0 : 5–50 mg L ⁻¹ λ_{\max} : 463 nm | 99% and 600 mg g ⁻¹ | Pseudo-first-order kinetics; electrostatic attraction |
| Mg–Al-layered double hydroxide ¹⁹⁶ | Reactive Red, Congo red, and Acid Red 1 | Time: 60 min pH: 9–10 λ_{\max} : 543 nm, 500 nm, and 532 nm, respectively | 59.49 mg g ⁻¹ , 37.16 mg g ⁻¹ , and 108.0 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic attraction and ion exchange |
| Nanohybrid layered double hydroxides ¹⁹⁷ | Amaranth, diamine Green B, and brilliant green | T : Room temperature pH: 7–9.5 λ_{\max} : 520 nm, 623 nm, and 624 nm, respectively | 0.8 mmol g ⁻¹ , 1.089 mmol g ⁻¹ , and 1.418 mmol g ⁻¹ , respectively | Pseudo-second-order kinetics; ion exchange |
| Hybrids of fly ash Biomass fly ash geopolymer monoliths ¹⁹⁹ | MB | C_0 : 1–50 mg L ⁻¹ Time: 30 h λ_{\max} : 664 nm | 15.4 mg g ⁻¹ Reused up to five cycles | Freundlich isotherm; electrostatic attraction |
| Porous biomass fly ash-based geopolymer spheres ¹⁹⁸ | MB | C_0 : 10–125 mg L ⁻¹ Time: 30 h λ_{\max} : 664 nm | 79.7 mg g ⁻¹ Reused up to eight cycles | Freundlich isotherm; multilayer adsorption |
| Fly ash–TiO ₂ composite ²⁰¹ | Mixture of bemacid red and bemacid blue | C_0 : 10 mg L ⁻¹ each pH: 10.6 λ_{\max} : 444 nm and 652 nm, respectively | 4.003 and 1.194 mg g ⁻¹ | Pseudo-second-order kinetics; hydrogen abstraction, redox reactions, also the π -bonds |
| Ca(OH) ₂ /Na ₂ FeO ₄ modified fly ash ²⁰² | Orange II | C_0 : 50 mg L ⁻¹ Dose: 2000 mg L ⁻¹ | 24.8 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic interaction, hydrogen bonding |
| Hybrids of bio adsorbents Cellulose- <i>g</i> -poly(acrylic acid-co-acrylamide) ²⁰⁴ | Acid blue 93 (AB93) and MB | C_0 : 200 mg L ⁻¹ Time: 90 min. pH: 7 Dose: 0.4 g L ⁻¹ λ_{\max} : 664 and 607 nm, respectively | 1602 and 1814 mg g ⁻¹ , respectively | Pseudo-second-order kinetics, Freundlich isotherm; electrostatic interaction |
| Sulphonated bio-adsorbent from waste hawthorn kernel ²⁰⁵ | MB | C_0 : 25–400 mg L ⁻¹ Time: 0–360 min T : 25–60 °C Dose: 0.1 g in 50 mL λ_{\max} : 665 nm | 151.5 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; ion exchange process |
| Cross-linked beads of activated oil palm ash zeolite/chitosan ²⁰³ | MB and acid blue 29 | C_0 : 50–400 mg L ⁻¹ T : 50 °C pH: 3–13 λ_{\max} : 668 and 602 nm, respectively | 199.2 mg g ⁻¹ and 270.27 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Freundlich isotherm; physisorption |
| Agricultural waste/graphene oxide 3D ²⁰⁶ | MB | C_0 : 1000 mg L ⁻¹ T : 25 °C pH: 12 λ_{\max} : 663 nm | 414.03 mg g ⁻¹ The removal was > 90% after five cycles | Pseudo-second-order kinetics; Temkin isotherm; multimolecular layers of coverage and heterogeneous adsorption |

C_0 : initial dye concentration; T : temperature; and λ_{\max} : maximum wavelength detected for the analysis of dye.



4.4. Metal oxide-based (magnetic and non-magnetic) hybrid materials

In recent years, metal oxide-based nano-adsorbents have been widely applied in wastewater treatment due to their unique attributes such as large surface area, nano-size, high reactivity, high ability to blend, and robust solution mobility.^{1,208} Considering this, the performance of various metal oxide-based hybrid materials as adsorbents in dye removal is reviewed below.

4.4.1 Magnetic metal oxide nanocomposites. Magnetic nanomaterials exhibit additional advantages in the separation of the catalyst/adsorbent by applying an external magnetic field.²⁰⁹ Gao *et al.* used $\text{Fe}_3\text{O}_4/\text{CeO}_2$ as a magnetic composite for the removal of Acid Black 210. The maximum adsorption capacity (93.1 mg g^{-1}) achieved was six times higher than of the commercial CeO_2 . The corresponding experimental data fitted well with the Langmuir isotherm.²¹⁰ Fe_3O_4 magnetic nanoparticles, due to their large surface-to-volume ratio and pore size, showed an adsorption capacity of $150\text{--}600 \text{ mg g}^{-1}$ of Rhodamine 6G in 30 min.²¹¹ At room temperature, the adsorption of MO, Reactive Brilliant Red K-2BP, and Acid Red 18 in contaminated water on an amine/ Fe_3O_4 -functionalized biopolymer magnetic resin correlated well with the Langmuir adsorption isotherm.²¹² The corresponding adsorption capacity values were found to be 222.2, 101.0, and 99.4 mg g^{-1} , respectively. This high adsorption capacity was attributed to the presence of amine groups and the enhanced surface area of amine/ Fe_3O_4 -resin. In another study, Mg-ferrite magnetic nanoparticles exhibited relatively low adsorption capacity in the removal of methyl green (1.23 mg g^{-1}) and basic fuchsin (2.55 mg g^{-1}).²¹³ NaOH-treated wheat straw impregnated with Fe_3O_4 nanoparticles achieved a maximum adsorption capacity of 1374.6 mg g^{-1} in the removal of

MB from contaminated water.²¹⁴ The adsorption process (endothermic) was likely to be dependent on pH and temperature. The adsorption mechanisms were proposed considering the formation of a surface complex and ion exchange between the MB molecules and adsorbent. Further, a $\gamma\text{-Fe}_2\text{O}_3$ nano-adsorbent exhibited equilibrium adsorption of Acid Red 27 dye within 4 min at a low pH (<5.5), and a decrease in the dye removal efficiency was observed with an increase in temperature.²¹⁵ The adsorption of Acid Red 27 dye on $\gamma\text{-Fe}_2\text{O}_3$ followed both the Langmuir and Freundlich isotherms.

Mahapatra *et al.* reported a maximum adsorption capacity of 416.66 mg g^{-1} at pH 7 for the adsorptive decolorization of CR dye on an $\text{Fe}_2\text{O}_3\text{-Al}_2\text{O}_3$ nanohybrid. This higher adsorption capacity was primarily due to the interaction of the amine functional group of the CR dye molecules with the oxy-hydroxide group of the nanohybrid material.²¹⁶ An Fe-Mn-Zr metal oxide nanocomposite showed a maximum adsorption capacity of 196.07 and 175.43 mg g^{-1} for the adsorption of MO and eosin yellow dyes, respectively.²¹⁷ The saturation magnetization of the adsorbent was found to be enough for its rapid magnetic separation from water. Further, the maximum adsorption capacity of 714.29 mg g^{-1} with a contact time of 3 h was achieved by a core@double-shell-structured HNTs/ Fe_3O_4 /poly(DA + KH550) adsorbent in the removal of MB dye.²¹⁸

4.4.2 Nonmagnetic metal-oxide nanocomposites. Various nonmagnetic oxide hybrid nanomaterials have been applied as adsorbents in the removal of dyes from the contaminated water. According to Li *et al.*, the adsorption capacity of MO on nano-dimensional Co/Cr-codoped ZnO was 1057.9 mg g^{-1} due to its high specific surface area and positive charge on its surface.²¹⁹ Lei *et al.* noted a maximum adsorption capacity of 397 mg g^{-1} on ZnO- Al_2O_3 for the removal of CR dye in 12 h. This adsorbent consisted of microspheres a diameter in the range of $12\text{--}16 \mu\text{m}$, which were assembled by nanosheets with a thickness of nearly 60 nm.²²⁰ The maximum adsorption capacity of 367 mg g^{-1} for methyl blue dye on Ni-MgO hybrid is attributed to the hydrogen bonding between the N-atoms (which have high electron affinity and smaller atom radius) of methyl blue and OH group on the surface of MgO.²²¹ According to Lei *et al.*, a maximum adsorption capacity of 357 mg g^{-1} was achieved in 12 h for CR dye on NiO- Al_2O_3 . This was ascribed mainly to the synergistic effect, high specific surface area, and positive surface charge (at pH 7) of the adsorbent.²²² ZnV_2O_4 hollow spheres comprised of a flower-like structure and a large number of compacted nanosheets, as depicted in the SEM image (Fig. 11), exhibited an adsorption capacity of 153.14 mg g^{-1} in 40 min for MB.²²³ Table 5 presents the performance of metal and metal oxide-based hybrid

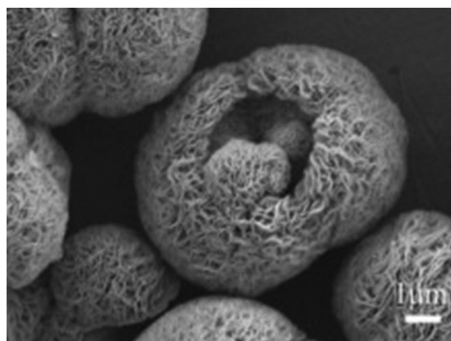


Fig. 11 Morphology of a metal oxide-based adsorbent, ZnV_2O_4 hollow spheres [Reprinted with permission from ref. 223. Copyright 2011, Elsevier].

Table 5 Metal oxide-based hybrid (magnetic and non-magnetic) nanocomposite materials for dye removal

| Adsorbent | Dyes | Experimental conditions | Adsorption capacity/ removal efficiency | Adsorption kinetics, isotherm, and mechanisms |
|---|--------------|--|--|--|
| Pure magnetic materials Fe_3O_4 ²¹¹ | Rhodamine 6G | pH ~ 7 Dose: $2.5\text{--}10 \text{ mg L}^{-1}$ Time: 30 min λ_{max} : 525 nm | $150\text{--}600 \text{ mg g}^{-1}$ | Fluorescence resonance energy transfer between the dye molecules and Fe_3O_4 magnetic nanoparticle |
| $\gamma\text{-Fe}_2\text{O}_3$ ²¹⁵ | Acid red 27 | pH < 5.5 Time: 4 min λ_{max} : 520 nm | $0.027 \text{ mmol g}^{-1}$ | Pseudo-second-order kinetics; Langmuir and Freundlich isotherm; physisorption and electrostatic attraction |



Table 5 (continued)

| Adsorbent | Dyes | Experimental conditions | Adsorption capacity/ removal efficiency | Adsorption kinetics, isotherm, and mechanisms |
|--|--|--|---|--|
| Magnetic-carbon-based nanocomposite | | | | |
| Magnetic graphene oxide modified by chloride imidazole ionic liquid ²²⁴ | Anionic: Glenn Black R (GR) and Orange IV (OIV) cationic: acridine orange (AO) and crystal violet (CV) | C_0 : 40 mg L ⁻¹ pH: 4 Dose: 0.01 g/25 mL λ_{max} : 520 nm, 440 nm, 490 nm, and 580 nm, respectively | GR, OIV, AO, and CV were 588.24, 57.37, 132.80, and 69.44 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic interaction |
| Magnetic graphene oxide freeze-dried ²²⁵ | RhB | Dose: 0.007 g/50 mL C_0 : 30–80 mg L ⁻¹ T: 25 °C λ_{max} : 553 nm | 126.58 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic interaction |
| Humic acid-Fe ₃ O ₄ ²²⁶ | Malachite green (MG) | Dose: 50 mg/50 mL λ_{max} : 618 nm | 79.3 mg g ⁻¹ | Pseudo-second-order kinetics; Freundlich isotherm; electrostatic attraction, π - π interaction, and hydrogen bonding |
| Magnetic graphene oxide ²²⁷ | MB and orange G | Dose: 20 mg/20 mL C_0 : 90 and 60 mg L ⁻¹ Time: 405 min λ_{max} : 667 and 475 nm, respectively | 64.23 mg g ⁻¹ and 20.85 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic interaction |
| Fe ₃ O ₄ /GO ¹⁸⁹ | MB and MO | C_0 : 1 mg L ⁻¹ pH: 6 λ_{max} : 644 and 466 nm, respectively | 666.7 and 714.3 mg g ⁻¹ , respectively | Langmuir isotherm; electrostatic interaction |
| Magnetic-based metal oxides | | | | |
| Fe ₃ O ₄ /CeO ₂ ²¹⁰ | Azo dye (Acid Black 210 (AB210)) | Dose: 50 mg/50 mL C_0 : 20–400 mg L ⁻¹ λ_{max} : 461 nm | 93.08 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; chemisorption |
| Iron oxide–alumina ²¹⁶ | CR | pH: 7 | 416.66 mg g ⁻¹ | Pseudo-second-order kinetics; Freundlich isotherm; multilayer adsorption |
| Fe–Mn–Zr metal oxide ²¹⁷ | MO and eosin yellow (EY) | Time: 62 min Dose: 0.45 g L ⁻¹ C_0 (MO): 11 mg L ⁻¹ , C_0 (EY): 25 mg L ⁻¹ λ_{max} : 464 and 517 nm, respectively | 196.07 and 175.43 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir isotherm; surface adsorption and pore diffusions |
| TiO ₂ /SiO ₂ /Fe ₃ O ₄ hollow magnetic microspheres ²²⁸ | MB | C_0 : 20 mg L ⁻¹ Dose: 0.5 g L ⁻¹ Time: 50 min | 147 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic interaction |
| Al cation-doped MgFe ₂ O ₄ ²²⁹ | MO | Time: 120 min Dose: 1 g L ⁻¹ | 274.6 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic interaction |
| CNT/MgO/CuFe ₂ O ₄ ²³⁰ | Methyl violet dye and Nile blue dye | Dose: 1 g L ⁻¹ C_0 : 10 mg L ⁻¹ λ_{max} : 584 and 638 nm, respectively | 36.46 mg g ⁻¹ and 35.60 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic interaction |
| Magnetic Fe ₃ O ₄ @UiO-66 ²³¹ | MB and MO | Dose: 20 mg/100 mL C_0 : 20 mg L ⁻¹ λ_{max} : 631 and 463 nm, respectively | 205 mg g ⁻¹ and 244 mg g ⁻¹ , respectively. | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic attraction and π - π stacking interactions |
| MgFe ₂ O ₄ ²¹³ | Methyl green (MG) and basic fuchsin (BF) | C_0 : 30 mg L ⁻¹ Dose: 0.8 g L ⁻¹ λ_{max} : 632 and 541 nm, respectively | 1.231 and 2.545 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir isotherm (MG) and Freundlich isotherm (BF); electrostatic interaction (MG) and hydrogen-bond interaction (BF) |
| MgFe ₂ O ₄ ²³² | MO | C_0 : 100 mg L ⁻¹ Dose: 1 g L ⁻¹ λ_{max} : 464 nm | 181.34 mg g ⁻¹ | Pseudo-second-order kinetics; Freundlich isotherm; electrostatic forces |
| Magnetic-based bio-adsorbents | | | | |
| Fe ₃ O ₄ -wheat straw ²¹⁴ | MB | Dose: 0.01–0.2 g/100 mL pH: 7 λ_{max} : 668 nm | 1374.6 mg g ⁻¹ | Pseudo-second-order kinetics; Freundlich isotherm; complexation formation and ion exchange |



Table 5 (continued)

| Adsorbent | Dyes | Experimental conditions | Adsorption capacity/ removal efficiency | Adsorption kinetics, isotherm, and mechanisms |
|---|--|---|--|--|
| Fe ₃ O ₄ -loaded protonated amine-modified hydrochar ²³³ | MB and MO | Dose: 40 mg/50 mL C ₀ : 100 mg L ⁻¹ T: 303 K λ_{max} : 664 and 464 nm, respectively | 148.84 mg g ⁻¹ (pH 11) and 202.02 mg g ⁻¹ (pH 5.0), respectively | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic interaction |
| Magnetic-based polymers Core@double-shell structured magnetic halloysite nanotube ²¹⁸ | MB | C ₀ : 70–130 mg L ⁻¹ T: 298 K Time: 3 h | 714.29 mg g ⁻¹ at 318.15 K | Pseudo-second-order kinetics; Langmuir isotherm; complexes formation, electrostatic interaction and π - π stacking interaction |
| Chitosan-Fe(III) hydrogel ²³⁴ | C. I. Acid Red 73 (AR 73) | pH: 12 Time: <10 min C ₀ : 50 mg L ⁻¹ | 294.5 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir-Freundlich isotherm; chemisorption |
| Fe ₃ O ₄ @C@polyaniline trilaminar core-shell ²³⁵ | MO | Dose: 8 mg/20 mL C ₀ : 60 mg L ⁻¹ | 120.2 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; chemisorption followed by electrostatic attraction and π - π interaction |
| Fe ₃ O ₄ @sodium alginate-Fe(III) polymer gel beads ²³⁶ | CR and Direct red 23 (DR 23) | Time: 30 min for CR and 60 min for DR 23 λ_{max} : 498 nm and 502 nm, respectively | 3333 and 1429 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic adsorption, hydrogen bonding, and surface complexation besides van der Waals forces |
| Magnetic halloysite-based molecularly imprinted polymer ²³⁷ | Sunset yellow (SY) | pH: 2 Dose: 0.005 g/0.01 L λ_{max} : 482 nm | 46.43 $\mu\text{mol g}^{-1}$ | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic attraction |
| Sulfonic acid-modified polyacrylamide magnetic composite ²³⁸ | Crystal violet (CV) and MB | pH: 10 C ₀ : 100–4000 mg L ⁻¹ Dose: 0.5 g L ⁻¹ Time: 360 min | 2106.37 mg g ⁻¹ and 1462.34 mg g ⁻¹ , respectively. | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic interaction, hydrogen bonding, and hydrophobic interaction |
| Fe ₃ O ₄ /graphite oxide nanosheet/citric acid-crosslinked β -cyclodextrin polymer ²³⁹ | MB | C ₀ : 50 mg mL ⁻¹ Dose: 10 mg/25 mL | 173 mg g ⁻¹ | Pseudo-first-order or the intraparticle diffusion model; Sips isotherm; electrostatic attraction, the Lewis acid-Lewis base interaction, the host-guest interaction, and the π - π interaction |
| Chitosan-fly ash/Fe ₃ O ₄ ²⁴⁰ | Reactive Orange 16 (RO16) | pH \sim 4 Dose: 0.08 g T: 303 K Time: 55 min λ_{max} : 493 nm | 66.9 mg g ⁻¹ | Pseudo-second-order kinetics; Freundlich isotherm; electrostatic attraction, dipole-dipole hydrogen bonding interactions, H-bonding, and n - π stacking interactions |
| Miscellaneous magnetic-based materials | | | | |
| Magnetic chelated silica particles ²⁴¹ | Naphthol blue black (NBB) and Eriochrome blue black R (EBBR) | C ₀ : 0.1 mmol L ⁻¹ λ_{max} : 618 nm and 569 nm, respectively | 3.76 and 1.83 mmol g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic attraction |
| Ionic liquid grafted-magnetic nanoparticles ²⁴² | Reactive Black 5 | C ₀ : 100 mg L ⁻¹ | 161.29 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic attraction and hydrogen bonding |
| Magnetic silica nanocomposite-immobilized <i>Pseudomonas fluorescens</i> ²⁴³ | Rhodamine B | C ₀ : 50 mg L ⁻¹ Dose: 1 g L ⁻¹ pH: 6 λ_{max} : 558 nm | 229.6 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic attraction and hydrogen bonding |
| Water-based ferro fluid ²⁴⁴ | Ponceau S | Ferrofluid dose: 20 mg mL ⁻¹ | 140.26 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic interaction |
| Clay/starch/Fe ₃ O ₄ ²⁴⁵ | Methyl violet (MV) | C ₀ : 10 mg L ⁻¹ Dose: 1.5 g L ⁻¹ pH 9 Time: 150 min T: 298 K | 29.67 mg g ⁻¹ | Pseudo-second-order kinetics; Freundlich isotherm; electrostatic interactions |



Table 5 (continued)

| Adsorbent | Dyes | Experimental conditions | Adsorption capacity/ removal efficiency | Adsorption kinetics, isotherm, and mechanisms |
|--|--|--|--|--|
| Activated carbon/bentonite/Fe ₃ O ₄ ²⁴⁶ | Reactive Red 198 | Dose: 2 g L ⁻¹ C ₀ : 5 mg L ⁻¹ pH: 8 Time: 50 min | 4.86 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm |
| Amine/Fe ₃ O ₄ -resin ²¹² | Anionic dye: MO, Reactive Brilliant Red K-2BP, and Acid Red 18 | Time: 180 min T: 25 °C pH 2.5, 5.5, and 7.0 respectively | RBR: 101.0 mg g ⁻¹ MO: 222.2 mg g ⁻¹ AR: 99.4 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; chemisorption involved ion exchange |
| Non-magnetic oxide nanocomposites Co/Cr-codoped ZnO ²¹⁹ | MO | Dose: 10 mg Time: 120 min λ _{max} : 200 nm | 1057.90 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; chemisorption and electrostatic interaction. |
| ZnO-Al ₂ O ₃ ²²⁰ | CR | C ₀ : 50 mg L ⁻¹ Dose: 10 mg/100 mL Time: 12 h T: 303 K | 397 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; chemisorption |
| Mesoporous MgO ²⁴⁷ | CR | C ₀ : 250 mg L ⁻¹ Dose: 0.02 g/50 mL Time: 60 min | 689.7 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic interaction. |
| MgO/SiO ₂ ²⁴⁸ | CR | Dose: 10 mg/50 mL C ₀ : 100 mg L ⁻¹ – 1000 mg L ⁻¹ T: 25 °C λ _{max} : 498 nm | ~4000 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic attractions and surface complexation |
| MgO-graphene oxide ²⁴⁹ | CR | C ₀ : 50 mg L ⁻¹ Dose: 10 mg/50 mL | 237 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic and π–π interactions |
| Ni–MgO ²²¹ | Methyl blue | C ₀ : 375 mg L ⁻¹ Dose: 0.1–0.5 g L ⁻¹ λ _{max} : 600 nm | 367 mg g ⁻¹ | Langmuir isotherm; electrostatic attraction and surface complexation |
| NiO–Al ₂ O ₃ ²²² | CR | C ₀ : 10–100 mg L ⁻¹ Dose: 10 mg/50 mL Time: 12 h T: 303 K pH: 7 | 357 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; positive negative charge attraction |
| ZnV ₂ O ₄ hollow spheres ²²³ | MB | C ₀ : 10 mg L ⁻¹ Time: 40 min λ _{max} : 664 nm | 96% and 153.14 mg g ⁻¹ | Pseudo-second-order kinetics; Freundlich isotherm; electrostatic attraction |

C₀: initial dye concentration; T: temperature; and λ_{max}: maximum wavelength detected for the analysis of dye.

(magnetic and non-magnetic) nanocomposites as adsorbents used in dye removal.

4.5. Metal–organic frameworks

Metal–organic frameworks (MOFs) have attracted much attention as adsorbents due to their fine tuneable pore structures and controllable structures/confined geometries. Besides, the large surface areas, multi-functionality, polar/polarisable bonds, and the possibility of the presence of host–guest interactions through the chemical modification of the organic ligands and/or the inorganic sub-units are also likely to play a unique role.^{250–255} According to Li *et al.*, MIL-53(Al)-NH₂ could rapidly bind with MB (208.3 mg g⁻¹) and MG (164.9 mg g⁻¹) due to the hydrogen bonding between the amino groups of the dyes and MOF. Further, MIL-Ti MOFs aided the ultrasound adsorption Basic Red 46, Basic blue 41, and MB from single and binary systems, exhibiting the maximum adsorption capacity of 1250, 1428, and 833 mg g⁻¹, respectively.²⁵⁷ This high adsorption capacity of

MIL-Ti MOFs was attributed to π–π interaction, H-bonding, and electrostatic interaction between the dye molecules and MOFs (Fig. 12). Further, the SEM image of the synthesized NH₂-MIL-125(Ti) having circular plates exhibited the transformation of its morphology due to the effect of the reactant concentration (Fig. 13), which also confirmed the excellent distribution of the nanomaterials. Haque *et al.* developed highly porous MIL-101 MOFs to study the adsorption of MO. The high adsorption capacity of 194 mg g⁻¹ depicted the significance of pore size and porosity in the adsorption of MO, following the mechanism of electrostatic interaction on MIL-101.²⁵⁸

Further, MIL-100(Fe) and MIL-100(Cr)-derived MOFs were also found to be efficient adsorbents in capturing MO and MB dye molecules from aqueous solution. MIL-100(Fe) showed an adsorption capacity of 1045.2 and 736.2 mg g⁻¹, while that of MIL-100(Cr) was 211.8 and 645.3 mg g⁻¹ for MO and MB, respectively.²⁵⁹ Further, magnetic MOFs have also been used for the adsorption of MB from dye-contaminated water.



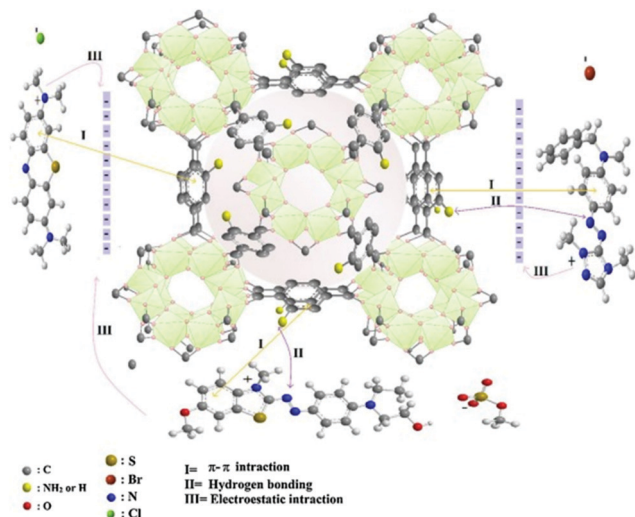


Fig. 12 Multiple dye adsorption mechanisms on MOFs [Reprinted with permission from ref. 257. Copyright 2018, Elsevier].

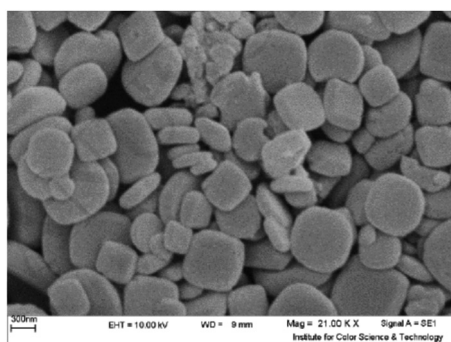


Fig. 13 Morphology of $\text{NH}_2\text{-MIL-125(Ti)}$ with circular plate [Reprinted with permission from ref. 257. Copyright 2018, Elsevier].

The adsorption mechanism involves hydrophobic interactions and/or $\pi\text{-}\pi$ interactions between the MB molecules and MOF. It was also noted that the adsorption capacity of a magnetic MOF increased from 84 to 245 mg g^{-1} on increasing the concentration of MB from 30 to 300 mg L^{-1} , respectively.²⁶⁰ In addition, the adsorption capacity of the zeolitic imidazolate framework comprising ZIF-8, ZIF-8@CNT, and ZIF-8@GO depicted stable and high reusability for over four cycles for the adsorption of MG, corresponding to an adsorption capacity of 1667, 2034, and 3300 mg g^{-1} , respectively.²⁶¹ Zhao *et al.* used a zirconium-based metal-organic framework (Zr-MOF) as an adsorbent for the removal of crystal violet and RhB dyes with the maximum adsorption capacity corresponding to 63.38 and 67.73 mg g^{-1} , respectively.²⁶² Table 6 describes various MOFs used as adsorbents in dye remediation from wastewater.

4.6. Polymers and their nanocomposites

Polymer-based adsorbents, such as polyaniline (PANI), polypyrrole (PPY), PANI/PPY copolymer, PANI/GO, PANI-modified rice husk composites, polymeric rice and Graham flour, polymeric turmeric powder, and chitosan, have found enormous applications in the field of dye treatment due to their easy fabrication, high effective surface area, high selectivity, interesting doping/de-doping chemistry, electrical transport characteristics, strong binding affinities, and porous surface texture.^{263–266} For most of the conducting polymer composites, the adsorption of dyes follows the mechanism of physisorption, hydrogen bonding, $\pi\text{-}\pi$ interactions, and electrostatic interaction.²⁶⁷ Further, the presence of active groups (*i.e.*, amine and imine) in the polymer facilitates the adsorption process. Many researchers have proposed the applications of polymer-based adsorbents to remediate dyes originating from industrial effluent (Table 7).

Table 6 Metal-organic frameworks (MOFs) for dye removal

| MOF | Dyes | Experimental conditions | Adsorption capacity/ removal efficiency | Adsorption kinetics, isotherm, and mechanisms |
|--|--|---|---|---|
| MIL-53(Al)- NH_2 ²⁵⁶ | MB and MG | C_0 : 5 mg L^{-1} Dose: 10 $\text{mg}/100\text{ mL}$ λ_{max} : 663 and 619 nm, respectively | 208.3 mg g^{-1} and 164.9 mg g^{-1} , respectively | Langmuir ($R^2 \sim 0.99$) and Freundlich isotherm ($R^2 \sim 0.97$); electrostatic attraction or repulsion. |
| MIL-Ti ²⁵⁷ | Basic Red 46, basic blue 41, and MB | Time: 30 min pH: 6.3 λ_{max} : 530, 605, and 665 nm, respectively | 1250, 1428, and 833 mg g^{-1} , respectively | Pseudo-second-order kinetics; Langmuir isotherm; $\pi\text{-}\pi$ interaction, hydrogen bonding, electrostatic interactions, and acid-base interactions |
| Porous MOF material-based on chromium-benzene dicarboxylate ²⁵⁸ | MO | C_0 : 30–50 mg L^{-1} λ_{max} : 464 nm | 194 mg g^{-1} | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic interaction |
| MIL-100 (Fe,Cr) ²⁵⁹ | MO and MB | C_0 : 400 mg L^{-1} | MIL-100(Cr): MO 211.8 mg g^{-1} MIL-100(Fe): MO 1045.2 mg g^{-1} MIL-100(Cr): MB 645.3 mg g^{-1} MIL-100(Fe): MB 736.2 mg g^{-1} 245 mg g^{-1} | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic interaction |
| ($\text{Fe}_3\text{O}_4/\text{Cu}_3(\text{BTC})$) ²⁶⁰ | MB | C_0 : 300 mg L^{-1} λ_{max} : 660 nm | | Pseudo-second-order kinetics; Freundlich isotherm; electrostatic interaction and $\pi\text{-}\pi$ stacking interaction and/or hydrophobic interactions |



Table 6 (continued)

| MOF | Dyes | Experimental conditions | Adsorption capacity/ removal efficiency | Adsorption kinetics, isotherm, and mechanisms |
|--|------------|---|---|--|
| Zeolitic imidazolate framework (ZIF) ZIF-8, ZIF-8@CNT, ZIF-8@GO ²⁶¹ | MG | Dose: 0.062, 0.031, and 0.018 g L ⁻¹ ZIF-8, ZIF-8@CNT, ZIF-8@GO, respectively. Time: 240 min C ₀ : 50 mg L ⁻¹ λ _{max} : 618 nm | ZIF-8: 1667 mg g ⁻¹ ZIF-8@CNT: 2034 mg g ⁻¹ ZIF-8@GO: 3300 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; electrostatic interaction |
| Zirconium-based MOFs ²⁶² | CV and RhB | C ₀ : 10 mg L ⁻¹ pH: 11 and 7, respectively. λ _{max} : 585 and 554 nm, respectively. | 63.38 mg g ⁻¹ and 67.73 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; chemisorption |

C₀: initial dye concentration; T: temperature; and λ_{max}: maximum wavelength detected for the analysis of dye.

Table 7 Polymers and their nanocomposites for dye removal

| Adsorbent | Dyes | Experimental conditions | Adsorption capacity/removal efficiency | Adsorption kinetics, isotherm, and mechanisms |
|---|---|--|--|---|
| Pure polyaniline and polypyrrole PANI and PPY ⁶¹ | CR | C ₀ : 20 mg L ⁻¹ pH: 6.55 T: 298 K Dose: 0.4 g L ⁻¹ and 1.73 g L ⁻¹ , respectively λ _{max} : 495 nm | 250.01 and 66.66 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir isotherm; chemisorption |
| PPY and PANI ²⁷² | Azo dyes: sunset yellow and CR | pH: 2 λ _{max} : 470 and 497 nm, respectively | 212.1 and 147 mg g ⁻¹ , respectively | π-π electron donor-acceptor interaction and electrostatic attraction |
| PANI powder ²⁷³ | MB | C ₀ : 3.9 mg L ⁻¹ λ _{max} : 664 nm | 13.854 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; chemisorption. |
| PANI ²⁷⁴ | MO | pH: 3 Time: 5 h λ _{max} : 498 nm | 92% | |
| PANI HNTs ²⁷⁵ | MB and acid green | pH: 3–11 λ _{max} : 664 nm and 642 nm, respectively | 69.44 and 57.87 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir isotherm; chemisorption involved electrostatic interaction |
| Polyaniline and polypyrrole based nanocomposites PANI/GO and PANI/RGO ²⁸⁰ | MB | Time: 270 min C ₀ : 50 mg L ⁻¹ λ _{max} : 660 nm | 14.2 and 19.2 mg g ⁻¹ , respectively | Pseudo-first-order kinetics; Langmuir isotherm; the presence of imine groups and π-π stacking interactions |
| PANI-modified rice husk composite ²⁸¹ | Acid red 18 | C ₀ : 40–120 mg L ⁻¹ λ _{max} : 523 nm | 100 mg g ⁻¹ | Pseudo-second-order kinetics; Langmuir isotherm; chemisorption |
| PANI/Fe ₃ O ₄ ²⁶³ | Acid Blue 40 | C ₀ : 50 mg L ⁻¹ λ _{max} : 620 nm | 216.9 mg g ⁻¹ | Pseudo-second-order kinetics; Freundlich isotherm; electrostatic interaction and H-bond formation |
| Alpha-cellulose/magnetite/PPY ²⁸² | Reactive Black 5 | pH: 3 | 62.31 mg g ⁻¹ | Langmuir isotherm; π-π* interactions, hydrogen bond formation |
| Starch/polyaniline ²⁷⁸ | Reactive Black and Reactive Violet 4 | λ _{max} : 597 and 577 nm, respectively pH: 3 | 811.30 and 578.39 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Toth model; electrostatic interaction |
| PANI/TiO ₂ ²⁸³ | MB | Dose: 2 g L ⁻¹ C ₀ : 400 mg L ⁻¹ λ _{max} : 664 nm | 458.10 mg g ⁻¹ | Pseudo-second-order kinetics; Temkin isotherm; chemisorption involves membrane diffusion, and intraparticle diffusion |
| PANI/Starch ²⁷⁹ | MB | C ₀ : 1–2 × 10 ⁻⁵ M Dose: 1.2 g L ⁻¹ | 6.8 × 10 ⁶ mol g ⁻¹ | Electrostatic interaction |
| Chitosan-based adsorbents Chitosan nanoparticles immobilized on a fibrous carrier ²⁹⁷ | Direct blue-86, photosens, theraphthal, and C.I. Reactive Blue 21 | pH: 4–6 C ₀ : 10–130 mg L ⁻¹ λ _{max} : 665, 679, 675, and 664 nm, respectively | 1097 ± 55, 1049 ± 43, 367 ± 22, and 296 ± 18 mg g ⁻¹ , respectively | Pseudo-second-order kinetics; Langmuir isotherm; Ion-exchange processes and hydrophobic binding |



Table 7 (continued)

| Adsorbent | Dyes | Experimental conditions | Adsorption capacity/removal efficiency | Adsorption kinetics, isotherm, and mechanisms |
|--|---|---|---|---|
| Chitosan-based magnetic-adsorbent ⁶⁴ | Acid orange 7 | T : 298 K pH: 6.2 ± 0.2 Dose: 2 g L^{-1} C_0 : 50 mg L^{-1} λ_{max} : 485 nm | 45.019 mg g^{-1} ; 98.01% | Pseudo-second-order kinetics; Sips and Redlich–Peterson isotherm; ion-exchange process |
| Fe_2O_3 -chitosan-bamboo sawdust ²⁹⁸ | Bromothymol blue | Time: 30 min Dose: 0.5 g L^{-1} pH < 7 λ_{max} : 453 nm | 217.39 mg g^{-1} | Pseudo-second-order kinetics; Langmuir isotherm; liquid-film and intraparticle diffusion mechanisms |
| Chitosan-ethylenediamine-tetraacetic acid-magnetic graphene oxide ³⁰¹ | RhB | Dose: $0.07\text{--}0.18 \text{ g L}^{-1}$ C_0 : $50\text{--}250 \text{ mg L}^{-1}$ λ_{max} : 554 nm | 1085.3 mg g^{-1} | Pseudo-second-order kinetics; Langmuir isotherm; chemisorption and physisorption |
| Chitosan hydrogel/ SiO_2 and chitin hydrogel/ SiO_2 ²⁹⁹ | Remazol black B, erythrosine B, neutral red, and gentian violet | C_0 : $0.05\text{--}100 \text{ mmol L}^{-1}$ | $0.081 \text{ mmol g}^{-1}$, 0.08 mmol g^{-1} , 0.88 mmol g^{-1} , and 0.17 mmol g^{-1} , respectively for chitosan hydrogel/ SiO_2 , whereas, $0.0062 \text{ mmol g}^{-1}$, 0.15 mmol g^{-1} , 1.06 mmol g^{-1} , and 0.14 mmol g^{-1} , respectively for chitin hydrogel/ SiO_2 | Freundlich isotherm; physical adsorption |
| Miscellaneous polymer adsorbents | | | | |
| Polyvinyl alcohol ³⁰⁰ | Bromothymol blue (BTB) and MB | pH: 6 Time: 10 min λ_{max} : 616 and 664 nm, respectively | 276.2 mg g^{-1} and 123.3 mg g^{-1} , respectively 98.65% and 61.32%, respectively | Pseudo-second-order kinetics; Langmuir isotherm; chemisorption |
| Poly(phenylenediamine) grafted electrospon carbon nanofibers ⁶³ | Coomassie brilliant blue (CBB) | C_0 : 100 mg L^{-1} Dose: $5 \text{ mg}/10 \text{ mL}$ Time: 5 h pH: 3 λ_{max} : 555 nm | 141 mg g^{-1} | Elovich kinetic; Redlich–Peterson isotherm; electrostatic interaction, π - π interactions, and intermolecular H-bonding |

C_0 : initial dye concentration; T : temperature; and λ_{max} : maximum wavelength detected for the analysis of dye.

4.6.1 Pure polyaniline and polypyrrole. Polyaniline is one of the most studied conducting polymers due to its many advantages, such as simple synthesis, presence of $-\text{NH}-$ groups, capability of doping, excellent physicochemical properties, mechanical flexibility, stability, low cost, and easy availability of its monomer.^{101,268} Alternatively, polypyrrole is another polymer studied for the removal of dyes from wastewater.⁶¹ Accordingly, Tanzifi *et al.* studied the adsorption of methyl orange on nano polyaniline at 298 and 338 K. They inferred that an increase in temperature enhanced the adsorption capacity for the dye from 3.34 to 32.04 mg g^{-1} and 3.28 to 30.28 mg g^{-1} corresponding to the initial dye concentration of 10 and 100 mg L^{-1} , respectively. The kinetics and isothermal studies established the pseudo-second-order model and validity of the Langmuir model (maximum monolayer adsorption capacity: 75.9 mg g^{-1}).²⁶⁹ PANI nanoparticles have also been utilized for the ultrasonication-assisted adsorption of crystal violet dye.²⁷⁰ The adsorption data fitted well with the Freundlich and Dubinin-Radushkevich isotherms. According to Sharma *et al.*, hyper crosslinked polyaniline (specific surface area: $1083 \text{ m}^2 \text{ g}^{-1}$) achieved the maximum adsorption capacity of 245 and 220 mg g^{-1} in 60 min for cationic crystal violet and anionic MO dyes in aqueous medium, respectively. These studies also predicted the fitting of the Langmuir adsorption isotherm for both dyes.²⁷¹ In another study, the adsorption of CR on PANI

and PPY exhibited a maximum adsorption capacity of 250.01 and 66.66 mg g^{-1} , respectively.⁶¹ Further, the experimental results revealed an increase in the adsorption efficiency with reaction time and adsorbent dosage. The kinetic data fitted well with the pseudo-second-order model, while the equilibrium adsorption findings best correlated with the Langmuir isotherm model. In another study, the adsorption of sunset yellow and CR on a PPY-MWCNT composite achieved an adsorption capacity of 212.1 and 147 mg g^{-1} , respectively.²⁷² The adsorption mechanism involved electrostatic attraction and π - π electron donor-acceptor interaction. According to Ayad and Zaghlool (2012), cross-linked PANI exhibited an adsorption capacity of 13.85 mg g^{-1} for cationic dyes such as MB (surface area: $349 \text{ m}^2 \text{ g}^{-1}$). The SEM image of crosslinked polyaniline at high magnification revealed a sponge-like structure, indicating the presence of pores (Fig. 14).²⁷³ Smita *et al.* used PANI to achieve a removal efficiency of 92% in 5 h for a toxic textile dye (MO) present in wastewater. The mechanistic study revealed that the electrostatic interaction between the counterions of the dye molecules and adsorbent was responsible for the adsorption of the dye.²⁷⁴ The adsorption of MB and acid green dye on PANI hollow nanotubes (internal diameter: $50\text{--}60 \text{ nm}$ and outer diameter: $5\text{--}10 \text{ nm}$) followed the Langmuir model, and their maximum adsorption capacity corresponded to 69.4 and 57.87 mg g^{-1} , respectively.²⁷⁵ Fig. 15 schematically



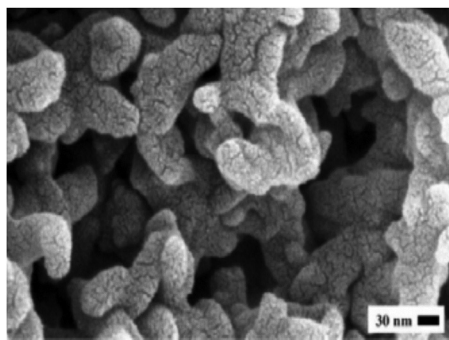


Fig. 14 Scanning electron microscopy image of crosslinked PANI [Reprinted with permission from ref. 273. Copyright 2012, Elsevier].

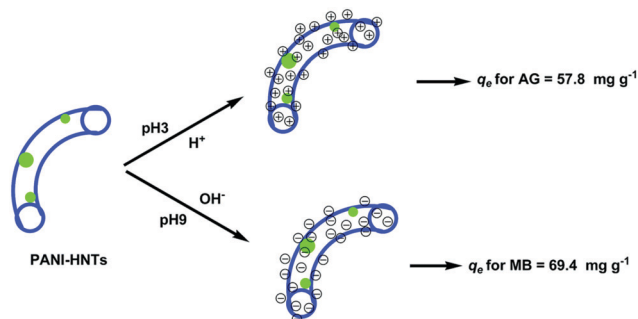


Fig. 15 Schematic illustration of PANI-HNTs at pH 3 and 9 (blue color: PANI-HNTs and green color: AG) [Reprinted with permission from ref. 275. Copyright 2018, The Royal Society of Chemistry].

represents the proposed chemical interaction between PANI hollow nanotubes with MB and acid green dyes at pH of 9 and 3, respectively. MB completely adsorbed on the nanotubes of PANI within 20 min, and the adsorption process well fitted the Langmuir isotherm (maximum adsorption capacity: 9.21 mg g^{-1}).²⁷⁶ Bhaumik *et al.* reported that the maximum monolayer adsorption capacity of Reactive Black 5 in aqueous solutions (pH 6) was 434.7 mg g^{-1} (318 K) on polyaniline nanofibers (diameter: 50–80 nm). The equilibrium isotherm data fitted the Langmuir isotherm.²⁷⁷

4.6.2 Polyaniline and polypyrrole-based nanocomposites.

Recently, polymeric nanohybrid materials have attracted significant attention in the field of wastewater treatment due to their high adsorption ability. For example, starch/polyaniline was used to treat reactive black and Reactive Violet 4 dyes, showing an adsorption capacity of 811.30 and 578.39 mg g^{-1} , respectively.²⁷⁸ The Toth isotherm model better described the single-component equilibrium adsorption, whereas the modified Freundlich model well fitted dye removal. In one study, PANI/starch was used to adsorb MB dye, which shown an adsorption capacity of $6.8 \times 10^6 \text{ mol g}^{-1}$.²⁷⁹ Further, El-Sharkaway *et al.* studied the removal of MB using PANI/GO and PANI/rGO nanocomposites. The adsorption capacity of PANI/GO and PANI/rGO for MB dye was 14.2 and 19.2 mg g^{-1} , respectively, in 270 min.²⁸⁰ Besides, Shabandokht *et al.* investigated the adsorption of Acid Red 18 dye using a PANI/HCl-modified rice husk composite, which showed an

adsorption capacity of 100 mg g^{-1} .²⁸¹ This study suggested that the Langmuir adsorption isotherm and pseudo-second-order kinetic model were compatible with the experimental results. In another work, Muhammad *et al.* removed Acid Blue 40 dye using polyaniline, Fe_3O_4 , and their composites and the corresponding adsorption capacity was found to be 130.5, 264.9, and 216.9 mg g^{-1} , respectively. The experimental result was better described by the Freundlich isotherm model and the mechanism involved electrostatic interactions and the significant amount of H-bonds present in PANI.²⁶³

In another study, the adsorption of RB5 dye-cellulose coated with magnetite nanoparticles and conducting PPY followed at pH 3 fitted the Langmuir model well (maximum adsorption capacity: 62.31 mg g^{-1}).²⁸² Further, Wang *et al.* also used PANI/ TiO_2 to remove MB dye with a maximum adsorption capacity of 458.10 mg g^{-1} , and the Langmuir adsorption isotherm well correlated with the experimental results. Chemical adsorption, membrane diffusion, and intraparticle diffusion were the responsible adsorption processes, while H-bonding, electrostatic interaction, and coordination interaction were the responsible adsorption mechanisms (Fig. 16). The attachment of MB on the surface of PANI mainly occurs on amino groups by electrostatic interaction and hydrogen bonding.²⁸³ Thus, a PANI zirconium oxide nanocomposite,²⁸⁴ PANI nanocomposite functionalized with zirconium(iv) and silicophosphate²⁸⁵ and PANI α -zirconium phosphate²⁸⁶ acted as efficient adsorbents for the removal of methylene blue and methyl orange dyes. The adsorption process for the cationic methylene blue dye²⁸⁷ and Acid Green 25²⁸⁸ on PANI nanotube/silica was best described by the pseudo-second-order kinetic model and Langmuir adsorption isotherm with the maximum monolayer adsorption capacity of 10.31 and 6.896 mg g^{-1} , respectively. Studies have also been reported

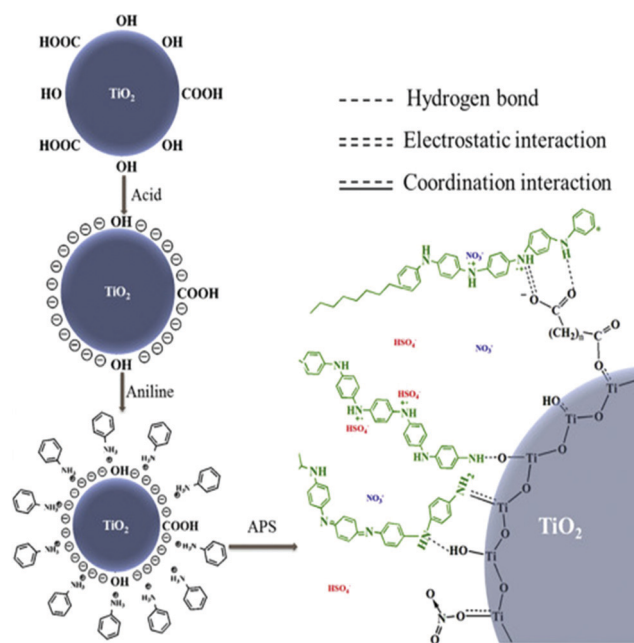


Fig. 16 Schematic showing the adsorption mechanisms of PANI/ TiO_2 [Reprinted with permission from ref. 283. Copyright 2019, Elsevier].

using PANI/silver,²⁸⁹ PANI/alumina,²⁹⁰ PANI/nickel ferrite,²⁹¹ and PANI/zinc ferrite²⁹² composites for the adsorption of brilliant green dye, anionic dyes (reactive red, Acid Blue 62, and Direct Blue 199), MB, and RhB, respectively.

4.6.3 Chitosan-based adsorbents. Chitosan is considered one of the most economical bio-polymers for dye removal, which can be extracted from natural resources. In comparison to other commercial adsorbents, it has attained great interest due to its unique properties such as cationic charge, high adsorption capacity, macromolecular structure, abundance, and cost-effectiveness.^{293,294} Chitosan is also an attractive source of natural polymers for the adsorption of pollutants from wastewater due to its biocompatibility, biodegradability, antibacterial properties, and nontoxicity.¹⁰¹ However, owing to its poor mechanical properties, low surface area, pH sensitivity, and low porosity, it is generally used in the form of a composite. Considering this, Janaki *et al.* reported that a PANI/chitosan composite efficiently removed Congo red, Coomassie brilliant blue, and Remazol brilliant blue R sulfonated anionic dye with a removal efficiency of 95.4%, 98.2%, and 99.8%, respectively. In contrast, it showed a removal efficiency of only 10.6% for the nonsulfonated cationic dye methylene blue.²⁹⁵

The adsorptive removal of Reactive Orange 16 on chitosan/PANI/ZnO agreed well with the Langmuir isotherm and corresponded to a maximum monolayer adsorption capacity of 476.2 mg g⁻¹.²⁹⁶ In another work, the removal of anionic dyes, namely Direct Blue 86, photosens, theraphthal, and C.I. Reactive Blue 21m was studied on chitosan supported on a fibrous carrier.²⁹⁷ The experimental data fitted the Langmuir isotherm and showed the maximum adsorption capacity of anionic dye in the range of 300–1050 mg g⁻¹ depending on the type, molecular size, and number of anionic groups in the dye. According to Cojocaru *et al.*, spinel ferrite (15%) dispersed in

the matrix of chitosan inter-linked with glutaraldehyde, showing an adsorption capacity of 45.02 mg g⁻¹ for Acid Orange 7 dye. The hydrogen bonding and hydrophobic interaction between the dye molecules and composite were responsible for the adsorption mechanism.⁶⁴ An Fe₂O₃/chitosan-bamboo saw-dust composite efficiently removed the acid dye bromothymol blue.²⁹⁸ The experimental data well correlated with the Langmuir isotherm model with an adsorption capacity of 217.39 mg g⁻¹ achieved in 30 min contact time using 0.5 g L⁻¹ adsorbent dose. Copello *et al.* treated Remazol black B, Erythrosine B, neutral red, and gentian violet dyes with chitosan hydrogel/SiO₂ and achieved the maximum adsorption capacity of 0.081, 0.08, 0.88, and 0.17 mmol g⁻¹, respectively.²⁹⁹

4.6.4 Miscellaneous polymer-based adsorbents. Agarwal *et al.* used polyvinyl alcohol (PVA) as an adsorbent for the removal of bromothymol and MB from wastewater. The corresponding adsorption isotherms were well fitted with both the Langmuir and Freundlich models. The adsorbent attained the maximum adsorption capacity in 10 min, corresponding to 276.2 and 123.3 mg g⁻¹, respectively.³⁰⁰ For the adsorption of Coomassie brilliant blue R 250 dye on poly(*para*-, *ortho*- and *meta*-phenylenediamine (PPDA)) grafted electrospun carbon nanofibers, the effective adsorption capacity of 141 mg g⁻¹ was achieved and the adsorption kinetics and isotherm data were well correlated with the Elovich kinetic and Redlich–Peterson isotherm models respectively.⁶³ The adsorption mechanism study suggested electrostatic interaction, π - π interactions, and intermolecular H-bonding controlled the dye sorption. Table 7 shows the removal of dye from contaminated water using conducting polymer, copolymer, and their nanocomposite-based adsorbents. Fig. 17 shows a schematic representation of dye pollution in water and its adsorptive removal using different adsorbents.

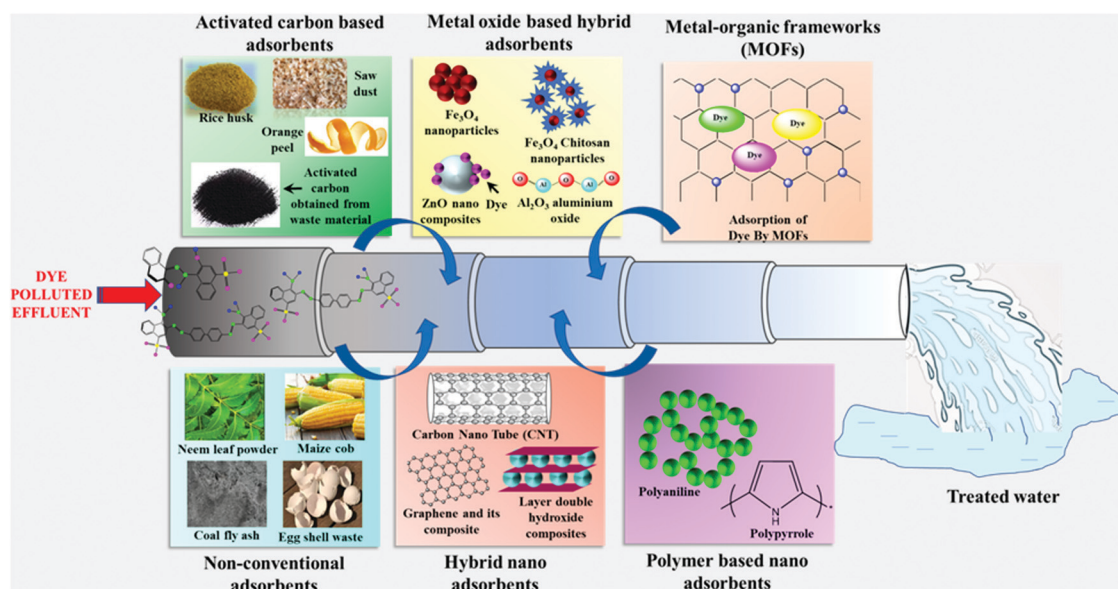


Fig. 17 Schematic presentation of water pollution from dye wastewater, their adsorptive removal using various adsorbents, and the production of treated water.



5. Critical factors influencing dye adsorption

Critical factors such as initial dye concentration, solution pH, temperature, adsorbent dose, and time play a significant role in the adsorptive removal of dyes (Table 8). In this regard, the initial dye concentration makes substantial contributions to the adsorption phenomena. It should be noted that an increase in dye concentration shows positive effects up to a certain limit. Further, the increasing tendency of adsorption for high levels of dye contaminants is directly related to the available active sites on the surface of the adsorbent. The enhanced adsorption capacity is initially accelerated due to the presence of unsaturated active sites in the adsorbent. As the surface of the adsorbent becomes saturated, a considerable reduction in the adsorption of dye occurs.^{14,302} According to Mane and Babu (2011), for brilliant green dye with an initial concentration of 100 mg L⁻¹, sodium hydroxide treated saw-dust exhibited an adsorption capacity of 55.86 mg g⁻¹.¹²¹ In another work, the adsorption capacities of 1602 and 1814 mg g⁻¹ were recorded on cellulose-g-poly(acrylic acid-co-acrylamide) as an adsorbent for the initial concentration of acid blue and MB of 200 mg L⁻¹, respectively.²⁰⁴ These observations suggest, in general, a high initial concentration results in a high adsorption capacity. In addition, the solution pH also plays an essential role in the adsorption of dye from contaminated water. According to Zhou *et al.*, a variation in pH

can affect the possible reactions between dye molecules and adsorbents due to the change in the ionization level and surface charge of the adsorbent.¹⁴ In general, low and high solution pH favor the adsorption of anionic and cationic dyes, respectively.³⁰³ This was substantiated by Daneshvar *et al.* and Phoemphoonthanyakit *et al.*, where they reported an adsorption capacity of 1093 mg g⁻¹ at pH 2 for Acid Blue 25 and 600 mg g⁻¹ at pH 7 for Rhodamine 6G.^{142,211} Further, the temperature has a prominent effect on the adsorption of dyes. Additionally, a variation in temperature is also helpful in identifying if adsorption process is endothermic or exothermic. In an exothermic process, the adsorption capacity decreases an increase in temperature, whereas it increases with an increase in temperature in an endothermic process.³⁰⁴

In general, an increase in the adsorbent dose has positive effects on the adsorptive removal of dyes, mainly due to the increment in the active sorption sites.³⁰³ In contrast, a higher dose may cause congestion in active sites of the adsorbent. Khan and Nazir (2015) achieved an adsorption capacity of 217.39 mg g⁻¹ for bromothymol blue at a dose of 0.5 g L⁻¹ using an Fe₂O₃/chitosan-bamboo saw-dust composite.²⁹⁸ In contrast, Ebrahimian Pirbazari *et al.* reported an adsorption capacity of 1374.6 mg g⁻¹ for MB at a dose of 1.0 g L⁻¹ NaOH-treated wheat straw impregnated with Fe₃O₄ nanoparticles.²¹⁴ These findings clearly demonstrate the positive effects manifested by an increased adsorbent dosage. Finally, an increase in

Table 8 Critical influencing factors affecting the adsorption process

| Critical influencing factor | Salient features | Influence on adsorption | Remarks | Ref. |
|-----------------------------|---|---|---|------------|
| Initial dye concentration | Showing the dissolved amount of dye in aqueous solution and the amount of dye adsorption are directly related to the active sites present on the surface of the adsorbent. | Increased dye concentration causes an increment in adsorption capacity until the unsaturated active sites of the adsorbent become saturated. | In an aqueous environment, the initial concentration of dye may vary from trace level to mg L ⁻¹ or even more. | 14 and 302 |
| pH of the solution | Has a prominent role in dye adsorption. | A variation in pH affects the reaction between dye molecules and adsorbents because of the change in the ionization level and surface charge of the adsorbents. | The pH of the dye effluent may vary depending on the presence of different types of salts (acidic and basic). | 14 and 303 |
| Adsorbent dose | Controls the degree of electrostatic charges provided by ionized dye molecules and causes the varying rate of adsorptions with changing pH. Showing the amount of adsorbent used to remove dye particles. | In the literature, it has been found that low and high pH favor the adsorption of anionic and cationic dyes, respectively. Generally, an increment in dose provides more active sites, which causes an increase in adsorption capacity. | High dose affects the economy of the treatment process. | 95 and 303 |
| Temperature | Directly related to the number of active sites available on the surface of the adsorbent. Shows the adsorption nature, whether it is endothermic or exothermic. | However, a high dose causes congestion in active sites. An increase in adsorption capacity with an increase in temperature shows the endothermic nature, whereas a decrease in adsorption capacity an increase in temperature shows the exothermic nature of reactions. | In general, an increase in temperature increases the adsorption capacity, but a higher temperature is not desirable. | 95 and 304 |
| Reaction time | Shows the contact time between adsorbent and adsorbate. | An increase in contact time causes positive effects on the adsorption until equilibrium among active sites of adsorbent and dye molecules is established. | High reaction time affects the economy of the treatment processes due to an increase in energy requirements. | 95 |



contact time may have a negative and/or positive effects on the adsorptive removal of dyes. When equilibrium is established between the active sites of the adsorbent and dye molecules, a further increment in the reaction time has no involvement in the adsorption. Khan and Nazir (2015) have observed an adsorption capacity of 217.39 mg g^{-1} for bromothymol blue in 30 min on an $\text{Fe}_2\text{O}_3/\text{chitosan-bamboo saw-dust composite}$.²⁹⁸ In contrast, an adsorption capacity of $1057.90 \text{ mg g}^{-1}$ for MO dye was achieved on a nano-dimensional Co/Cr-codoped ZnO adsorbent in 120 min, indicating that an increase in reaction time has positive effects on the adsorption process.²¹⁹

6. Mechanisms of dye adsorption

The adsorption of dye from contaminated water on the surface of an adsorbent is achieved *via* various adsorption mechanisms, as schematically shown in Fig. 18 and displayed in Tables 2–7. It should be noted that the adsorption of water pollutants on adsorbents is mainly guided by electrostatic attraction, π - π interactions, van der Waals forces, hydrogen bonding, acid-base reactions, and hydrophobic interaction.¹ Shen and Gondal reported that electrostatic and intermolecular interactions govern the adsorption of Rhodamine dye on the surface of the adsorbent.⁶⁰ According to Zheng *et al.*, the adsorption of anionic dyes, such as CR and MO on GO-NiFe-LDH, is achieved by electrostatic attraction and ion exchange phenomena.¹⁷⁸

Furthermore, the ion exchange mechanism involves the exchange of ions between a liquid (dye solution) and solid phase (adsorbent). Ebrahimian Pirbazari *et al.* suggested that two principal mechanisms are involved in removing the MB dye on NaOH-treated wheat straw impregnated with Fe_3O_4 , namely the formation of a surface complex and ion exchange between the dye molecule and adsorption surfaces.²¹⁴ The formation of a surface complex is a mechanism associated with the adsorption process, which is described by the binding of ions to various surface functional groups available onto the surface of the adsorbent and electrostatic interaction between the adsorbent-adsorbate surfaces. Cojocar *et al.* proposed that the formation of hydrogen bonds between Acid Orange 7 dye and adsorbents accounts for the adsorption process.⁶⁴ According to Siddiqui *et al.*, H-bonds between MB and MnO_2/BC arise due to the interaction between the -OH groups present in MnO_2/BC and the acceptor present in MB molecules.¹²³ Similarly, π - π bonding/ π -effects/ π -interactions (non-covalent) involve π systems, where similar to electrostatic interactions, positively charged molecules interact with negatively charged surfaces. Further, the adsorption process can follow more than one mechanism simultaneously. For example, the adsorption of Coomassie Brilliant Blue R 250 dye on the surface of adsorbents is governed by electrostatic interactions, π - π interactions, and intermolecular H-bonding.⁶³ The probable adsorption mechanisms involved in dye removal are shown in Fig. 18, together with the various adsorption processes.

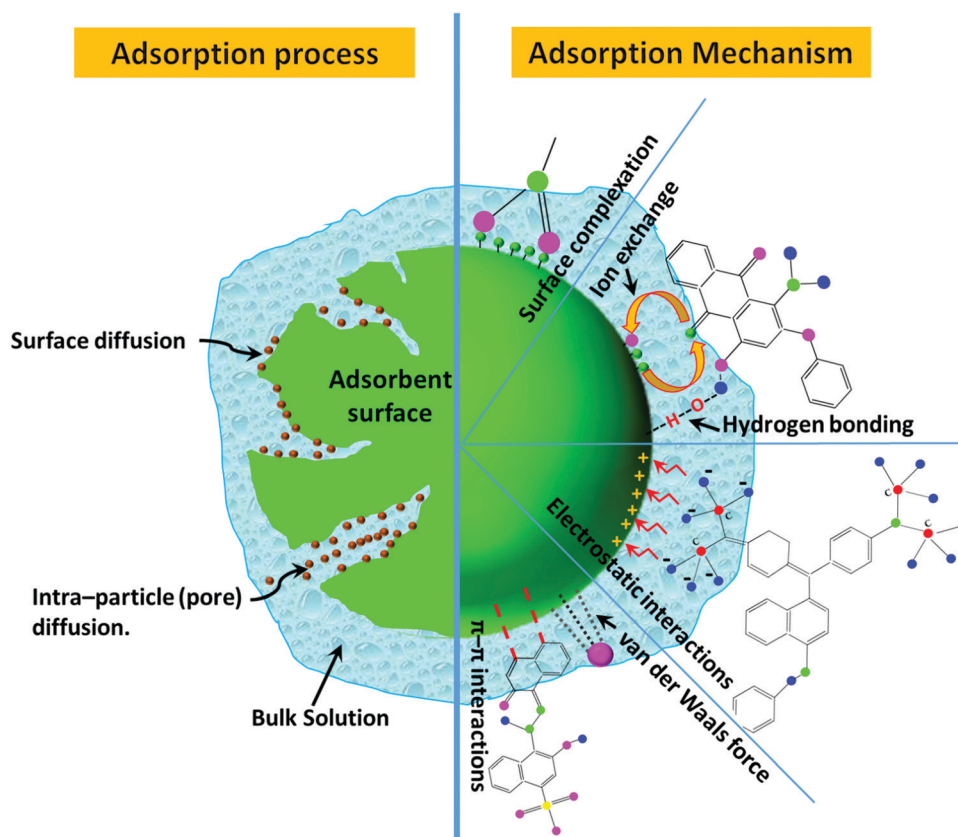


Fig. 18 Adsorption processes and mechanisms for dye removal from bulk liquid.



7. Critiques, future perspectives, and summary

7.1. Critiques and future perspectives

Adsorption is the most preferred technique for dye removal due to its ease of operation, high efficiency, recyclability, and cost-effectiveness. This is also one of the most suitable methods employed for both pilot and field-scale wastewater treatment facilities. The adsorption ability depends on the type of adsorbent used in the removal of dyes from contaminated water. Therefore, adsorbents should have easy availability, cost-effectiveness, high porosity, recycling ability, and abundant active sites on its surface. Recently, commercial adsorbents, such as industrial waste-based adsorbents for the treatment of dyes, pesticides, pharmaceuticals, *etc.*, have received considerable attention due to their involvement in waste minimization. Besides, metal oxide-based adsorbents are also preferred on a large scale due to their unique properties, such as highly active sites and ability to blend with other sorbents. Furthermore, metal-organic framework- and polymer-based adsorbents have also been explored as adsorbents in the treatment of dye-contaminated water owing to their enhanced surface activity and porosity. Considering this, future studies could target the better utilization of commercial and natural bio-adsorbents having good adsorption and desorption capabilities, recyclability, and cost-effectiveness. MOFs and polymer-based adsorbents can be widely researched for wastewater treatment. The adsorption techniques can also be explored in the field of micropollutant remediation such as dyes, pharmaceuticals, and other emerging contaminants at the field scale.

Continuing research is focused on adsorption as one of the prime strategies in the separation of dye from wastewater. However, challenges still exist in developing low-cost, high-performing adsorbents with significantly enhanced activity and long-term stability. In this regard, integrating agro-industrial waste, several naturally existing materials, and eco-friendly industrial waste materials with other biodegradable nanomaterials with no risk to human health and environmental sustainability may be the best alternative. Further, the choice of nanomaterials as adsorbents in wastewater treatment is guided by their high surface area and high adsorption capacity. However, the production cost of nano-adsorbents needs to be considered for their commercial use in any industrial effluent treatment. Despite this, the separation of nanomaterials after adsorption and their disposal are complex and costly processes.³⁰⁵

Additionally, cost-effectiveness in terms of reusability of the spent adsorbent should also be considered. Spent adsorbents need to be regenerated and activated by treating them with acid or alkali for their safe and effective reuse.³⁰⁶ Further, the economical and safe disposal or reuse of spent/exhausted adsorbents need to be considered.^{307,308} Dye-loaded spent adsorbents can be utilized to produce biochar materials, fuel cells, for energy production purposes, and also in landfilling.^{307,309} Simultaneously, the difficulties and limitations in the scale-up of the treatment technology at the commercial level need to be considered in terms of economic aspects and energy-related issues.

7.2. Summary

The disposal of colored dye wastewater in the environment has depleted freshwater resources and compelled scientists to rethink the availability of clean and safe water. It has been reported that the presence of toxic and colored compounds in dye-containing wastewater results in carcinogenic, mutagenic, allergic, and dermatitis effects on living organisms. This review article reported various classes of dyes and their applications, ecotoxic effects, and sources of dye-contaminated water. The textile, leather, and cosmetic industries were found to be the primary sources of dye-polluted water. Different existing treatment techniques were reviewed and compared for dye removal. Among them, adsorption was selected as a potential technique to treat dye wastewater due to its easy application, simple and scalable synthesis of adsorbents, high removal efficiency, and cost-effectiveness. In this direction, the various adsorbents reported for the removal of dyes from aqueous solution were highlighted. In addition, investigations revealing the adsorption kinetics and fitting of the adsorption isotherm were also presented. MOFs, metal-oxides, and hybrids of bio-adsorbents and carbon show significant adsorption ability for dye contaminants. Various critical factors, such as solution pH, adsorbent dosage, initial dye concentration, temperature, and equilibrium time, were identified as essential factors influencing the adsorption process. Besides, the driving forces responsible for the adsorption of dye molecules are electrostatic interactions, van der Waals forces, hydrogen bonding, and π - π interactions. Thus, the high removal efficiency and field applicability of the adsorption technique make this process suitable for the treatment of dye-contaminated water.

Conflicts of interest

There are no conflicts of interest to declare.

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