



Gas-phase CO₂ electroreduction over Sn–Cu hollow fibers†

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CO₂ electroreduction to value-added chemicals by virtue of renewable electricity is significant for carbon emission abatement and renewable energy conversion/storage. Conventional CO₂ electroreduction occurring in aqueous solution or ionic liquid suffers from insufficient CO₂ solubility and a separation dilemma of the soluble products. In this work, we report that when using Sn–Cu hollow fiber electrodes, gas-phase CO₂ can be directly electroreduced into various multicarbon oxygenates. The faradaic efficiencies of acetaldehyde and acetone over a 0.3 wt% Sn–Cu hollow fiber electrode are 10 and 12% at the cell voltage of –1.4 V. The presence of an appropriate amount of SnO₂ nanoparticles decorated on a Cu hollow fiber surface not only facilitates the reaction kinetics with elevated current densities, but also improves the C–C coupling of intermediates, promoting the formation of multicarbon oxygenates.

The continuously elevating atmospheric CO₂ concentration which has arisen from tremendous fossil fuel consumption severely threatens the ecological environment.^{1,2} Utilizing CO₂ as a safe, economic and sustainable C₁ resource via modern techniques to obtain value-added chemicals could contribute to carbon emission abatement, which is of great importance.^{3–6} Comparing with the thermocatalytic conversion of CO₂, which requires harsh conditions and a massive amount of energy, the CO₂ electroreduction conducted under mild conditions exhibits great application potentials.^{7,8} Besides, the rapid-developing renewable electricity from wind and solar power would cause critical impacts on the transmission grid due to its randomness, intermittency and volatility, while CO₂ electroreduction could take in this low-grade renewable electricity in CO₂ conversion to obtain valuable chemicals.

Although CO₂ electrocatalysis has been widely studied for decades, the limited reaction kinetics constrained by the insufficient CO₂ solubility in liquid electrolyte (both aqueous solutions and ionic liquids),^{8–13} and the separation dilemma of soluble products from liquid electrolyte (since the energy required to recover the products is higher than the energy stored in the produced molecules),⁷ are still the two key issues. In spite of the many attempts of adopting gas-diffusion electrodes to alleviate the former issue by Sargent and other researchers, which could yield ethylene with a faradaic efficiency (FE) of 70%¹⁴ and a 62% C₂₊ product selectivity with a current density of 653 mA cm^{–2},¹⁵ for example, the complicated fabrication procedures and multi-component configuration (active component|hydrophobic binder|conductive additions) of such gas-diffusion electrodes still hinder the industrial applications of CO₂ electrocatalysis.

In contrast, the gas-phase CO₂ electrocatalysis would allow easy product separation, and could get rid of the CO₂ solubility problems at the same time. Centi *et al.* first came up with the idea of gas-phase CO₂ electroreduction and the possibility to obtain long-chain hydrocarbon products with Pt/C catalysts and solid electrolyte Nafion[®].¹⁶ Kriescher *et al.* reported a Cu felt electrode with Fumapem membrane, obtaining mainly methane with FEs no more than 0.12%.¹⁷ Recent studies from Gutiérrez-Guerra *et al.* used polybenzimidazoles (PBI) and Sterion[®] as the solid electrolyte for gas-phase CO₂ electroreduction at 90 °C, obtaining methanol and acetaldehyde with yields of 40 and 110 μmol g_{cat}^{–1} h^{–1} over Cu catalysts.^{18–20} However, these studies are all based on conventional types of Cu-based electrodes, with unsatisfying overall efficiencies and insufficient value-added multicarbon products for the electroreduction of gas-phase CO₂.

The porous hollow fiber (HF) electrode stands out as an alternative to the above-mentioned issues, which is fabricated *via* a combined phase-inversion and sintering process using commercial metal powder. This kind of self-supported gas-diffusion electrode can be adopted in electrochemical reaction systems without any binder. Its hierarchical pore

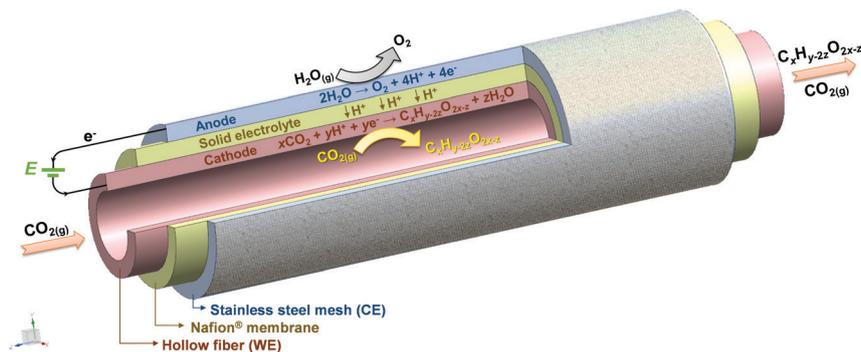
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Scheme 1 Schematic diagrams of a gas-phase CO₂ electrochemical reaction system based on Sn-Cu hollow fibers as the working electrode.

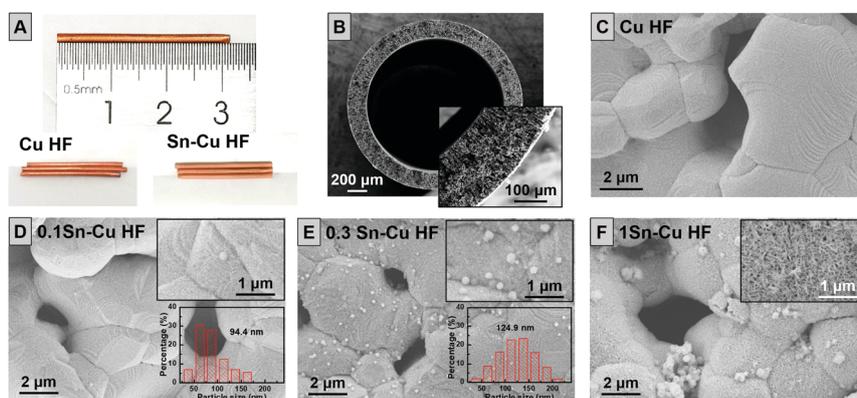


Fig. 1 Morphology of hollow fiber electrodes. (A) Photographs of Cu HF and Sn-Cu HF electrodes, (B) cross-section SEM of Cu HF, and surface SEM of (C) Cu HF, (D) 0.1Sn-Cu HF, (E) 0.3Sn-Cu HF and (F) 1Sn-Cu HF electrodes. Insets show the partially enlarged SEM images of hollow fibers, as well as the nanoparticle size distributions on the sample surface.

structure, good stability and conductivity, have shown unique advantages in electrocatalysis applications,^{21–23} and could be a suitable platform to study the gas-phase CO₂ electroreduction process.

On the other hand, Sn-based catalysts have been frequently used in CO₂ electroreduction due its intrinsic high activity. Lei *et al.* reported confined Sn in graphene which exhibited high CO₂ electroreduction activities with 85% HCOOH FE at -0.48 V overpotential.²⁴ Bai *et al.* found that alloying Sn with Pd reached nearly 100% HCOOH FE *via* an optimal surface Pd-Sn-O configuration at the lowest overpotential of -0.26 V.²⁵ An *et al.* revealed that Sn²⁺/Sn⁴⁺ species can reduce the overpotential and improve the HCOOH selectivity.²⁶ Liu *et al.* reported SnO₂ quantum wires with enhanced current density and improved HCOOH FE of over 80%.²⁷ Geng *et al.* found the Sn²⁺ node in ZIF-8 can accelerate HCOOH formation with a FE of 74% and a total current density of 27 mA cm⁻².²⁸ These findings indicate the great promotion of HCOOH formation by introducing Sn species in aqueous CO₂ electroreduction. However, during gas-phase CO₂ electroreduction, SnO₂ nanoparticles on the HF surface would play more important roles beyond facilitating the production of HCOOH species.

Here, a novel gas-phase CO₂ electrochemical reactor is developed based on Sn-Cu HF electrodes as illustrated in Scheme 1.

The porous Cu HF electrode is applied as a self-supported gas-diffusion electrode, while its surface is modified by Sn species *via* wet chemistry reduction with sodium citrate as the stabilizing agent and sodium borohydride (NaBH₄) as the reductive agent (see the ESI† for details). The Sn-based catalysts always help the formation of formate,^{24–28} while Cu-based catalysts are famous for the potential to promote C-C coupling and the formation of C₂ products such as ethylene and ethanol.^{8,29–31} The loadings of Sn element in Sn-Cu HFs are controlled by varying the molar ratio between the SnCl₂ precursor and Cu HF. The obtained samples are denoted as *x*Sn-Cu HFs, in which the *x* represents the loading of Sn element determined by ICP-OES (inductively coupled plasma-optical emission spectroscopy). Cu HF is also studied as the counterpart for comparison purposes.

As shown in Fig. 1A, the typical length of Cu HFs used in this work is about 3 cm with a color of light orange. The cross-section and surface scanning electron microscopy (SEM) images of Cu HF in Fig. 1B and C suggest the hollow structure of Cu HFs with an outer diameter of ~ 2 mm, as well as the porous fiber wall with a thickness of ~ 200 μ m. The characteristic finger-like pores are dispersed in the fiber wall without any visible macrovoids, while abundant pores are formed with an average size of 2–5 μ m on the smooth fiber surface. The porous



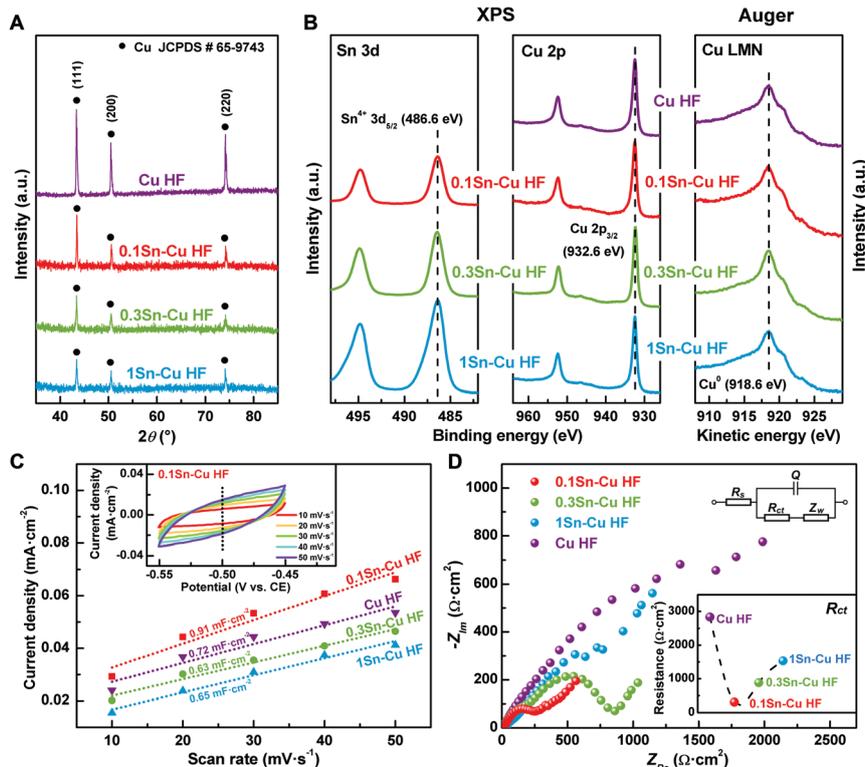


Fig. 2 Surface, bulk structure as well as electrochemical properties of hollow fiber electrodes. (A) XRD patterns, (B) Ag 3d, Cu 2p (XPS), Cu LMM (Auger) curves, (C) ECSA comparison, (D) EIS spectra and R_{ct} comparison of the as-prepared electrodes. Inset of (C) shows CV curves of 0.1Sn-Cu electrode in the range of -0.45 to -0.55 V vs. CE. Inset of (D) shows the equivalent circuit for EIS spectra fitting.

structure of Cu HFs benefits the diffusion of gaseous reactants and products by providing plenty of pathways for mass transfer.^{21,22} While the metallic nature of Cu HF guarantees sufficient electron conductivity, which would enlarge the three-phase boundary of reaction interfaces and facilitate the kinetics of CO_2 electroreduction.^{21,22} After the wet chemistry reduction preparation, no obvious appearance change could be observed for Sn-Cu HFs in Fig. 1A. While the SEM images in Fig. 1D–F clearly indicate the formation of SnO_2 nanoparticles or layer on the surface of Sn-Cu HFs. With the elevated loading of Sn component, not only the amount of SnO_2 nanoparticles increases, but also the average particle size enlarges from ~ 94 nm for 0.1Sn-Cu HF (Fig. 1D) to ~ 125 nm for 0.3Sn-Cu HF (Fig. 1E). For 1Sn-Cu HF, even a fabric-like SnO_2 layer is formed, composed of dense SnO_2 nanosheets vertically packed on the Cu HF surface (as shown in Fig. 1F).³² While for all Sn-Cu HF samples, the abundant pore structure of Cu HFs is still well-preserved, similar to other reported works.²³

Fig. 2A shows the bulk structure of each HF sample characterized *via* X-ray diffraction (XRD) measurements. Peaks appearing at 43.3 , 50.4 and 74.1° in all samples could be assigned to the characteristic peaks for (111), (200) and (220) planes of metallic Cu (JCPDS no. 65-9743), indicating that the main component of Cu HF and Sn-Cu HFs is metallic Cu.^{33,34} On the other hand, no diffraction peaks of all Sn-Cu electrodes corresponding to SnO_2 , SnO_x or other tin species^{23,25,26} could

be observed, suggesting the nanoparticles are amorphous with insufficient loadings.³⁵

In contrast to the bulk composition, the surface electronic states of catalysts can exert significant influence on the adsorption/desorption capacity as well as the catalytic performance. Fig. 2B shows the surface electronic states of Sn-Cu HFs characterized *via* X-ray photoelectron spectroscopy (XPS). For Cu 2p spectra in the binding energy (BE) range of 925–965 eV, a Cu 2p_{3/2} peak at 932.6 eV could be observed for each sample. Since the Cu 2p_{3/2} peaks for both Cu⁰ and Cu⁺ would appear around this binding energy range (while the Cu²⁺ 2p_{3/2} peak locates at ~ 942 eV), it is hard to distinguish the accurate electronic states of Cu with XPS results only.^{33,36} Thus the Auger curves of Cu LMM in the kinetic energy (KE) range of 908–929 eV (*i.e.* 558–579 eV for BE) were collected. The Cu LMM peak of each sample appears at 918.6 eV, while that of Cu⁺ locates at 916.8 eV, suggesting that the Cu⁰ species exists on the surface of all HF samples.³⁶ For Sn 3d spectra in the BE range of 482–498 eV, Sn 3d_{5/2} peaks at 486.6 eV could be observed for all Sn-Cu HF samples, which can be assigned to Sn⁴⁺ species rather than Sn²⁺ and Sn⁰ species with peaks at around 486.0 and 485.2 eV, respectively.^{23,25,26} Due to the oxophilic intrinsic property of the tin element, the Sn component existed in the SnO₂ state *via* the wet chemistry preparation route, as evidenced by the XPS results (Fig. 2B). This indicates the presence of SnO₂ nanoparticles or layer on the Cu HF surface as observed in the SEM images. Tin oxide can be formed rapidly when metallic Sn is exposed to air



due to the oxophilicity of Sn,²⁵ while the relatively lower oxygen affinity of Cu would keep it from being oxidized.²³ Meanwhile, the intensity of Sn 3d_{5/2} peaks increased with the elevated Sn component loading, indicating the growing amount of Sn⁴⁺ species on the surface of Sn-Cu HF.

The enrichment of SnO₂ on the Sn-Cu HF surface could further be confirmed *via* the surface atomic ratio extracted from quantified XPS results, and the average atomic ratio in each Sn-Cu HF sample obtained from ICP analysis.³⁵ Table S1 (ESI†) presents the comparison between the surface atomic Sn/Cu ratio detected by XPS, (Sn/Cu)_{XPS}, and the average atomic Sn/Cu ratio from ICP analysis, (Sn/Cu)_{ICP}, for Sn-Cu HF samples. It is clear that the (Sn/Cu)_{XPS} numbers are a hundred times that of (Sn/Cu)_{ICP}, demonstrating that the SnO₂ deposited *via* wet chemistry reduction preparation is enriched at the surface of Sn-Cu HF. It is also reported that SnO_x with a valence of +4 can play an essential role in the CO₂ electroreduction process.³⁷ This abundance of oxide species existing on the Cu electrode surface would affect the CO₂ electroreduction significantly.

The gas-phase CO₂ electrochemical reaction system based on a hollow fiber electrode is shown in Scheme 1 (see the ESI† for details). A single hollow fiber is used as the working electrode (WE) and support. A Nafion[®] membrane is covered on the surface of the hollow fiber as the solid electrolyte and diaphragm between the anode and cathode. Stainless steel mesh (SSM) is then deployed on the surface of Nafion[®], functioning as the counter electrode (CE). Both electrochemical characterization and reaction performance tests were conducted on this reaction system.

The electrochemical active surface areas (ECSAs) of Sn-Cu HF electrodes are determined based on their double-layer capacitances *via* a cyclic voltammetry (CV) method. All CV profiles (Fig. S2, ESI† and the inset in Fig. 2C) exhibit nearly symmetrical shapes in the range of -0.45 to -0.55 V vs. CE,

indicating the capacitive behaviors of double-layer capacitance for Sn-Cu HF electrodes. The cathodic and anodic current densities are obtained from the double layer charge/discharge CV curves at -0.5 V vs. CE. The double layer capacitance (*C*_{dl}), which is directly proportional to the ECSA, is then calculated by averaging the absolute values of cathodic and anodic current density slopes *via* linear fits.²² The obtained *C*_{dl} values are 0.72, 0.91, 0.63 and 0.65 mF cm⁻² for Cu HF, 0.1Sn-Cu HF, 0.3Sn-Cu HF and 1Sn-Cu HF, respectively (as shown in Fig. 2C). This implies that the ECSA of 0.1Sn-Cu HF is the largest, while the ECSAs of 0.3Sn-Cu HF and 1Sn-Cu HF are quite similar to each other.

The electrochemical impedance spectra (EIS) of Sn-Cu HF electrodes at -1.4 V vs. CE, as well as the corresponding charge transfer resistances (*R*_{ct}) are shown in Fig. 2D, which are obtained *via* the equivalent circuit shown in the inset. The *R*_{ct} of Cu HF is 2.8 kΩ cm², which is much larger than those of Sn-Cu HF. The *R*_{ct} increases monotonically from 0.3 kΩ cm² for 0.1Sn-Cu HF, to 0.9 kΩ cm² for 0.3Sn-Cu HF and 1.5 kΩ cm² for 1Sn-Cu HF with the increase of SnO₂ content. This phenomenon indicates that the presence of few SnO₂ nanoparticles significantly promotes the reaction kinetics for their high activities, leading to smaller *R*_{ct} corresponding to electrochemical reaction resistance. SnO₂ has been reported for its efficient, selective, and durable performance for CO₂ electroreduction.^{24–28} On the other hand, although SnO₂ is known as a p-type semiconductor with relatively fast electron transportation, the electronic conductivity of SnO₂ is still far below that of the metallic conductor. Therefore, the higher amount of SnO₂ nanoparticles and even SnO₂ layer on the Cu HF surface would hamper the charge transfer steps of electrochemical reaction due to the semiconductive nature of SnO₂, leading to increased *R*_{ct}.²⁵

Fig. 3 shows the gas-phase CO₂ electroreduction performance of hollow fiber electrodes at different potentials. No

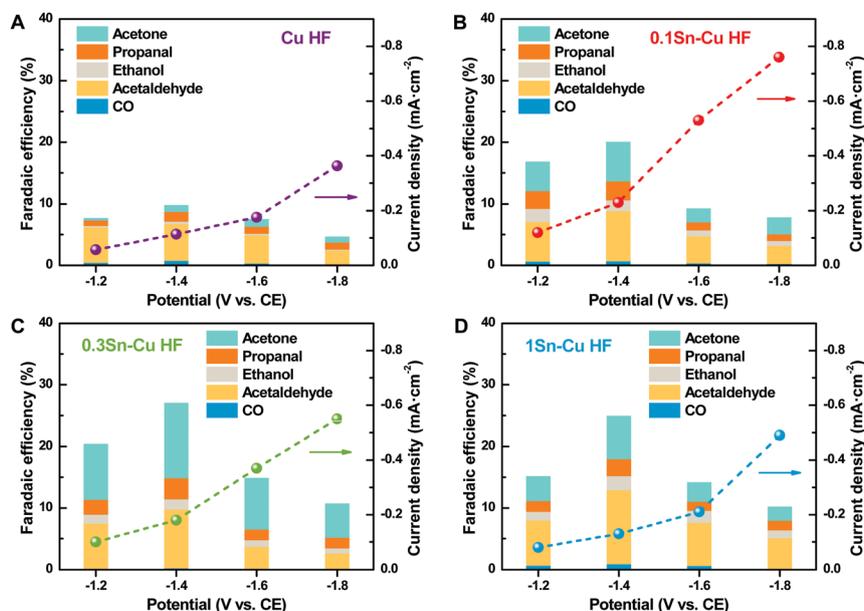


Fig. 3 Electrochemical reaction performance of hollow fiber electrodes. Faradaic efficiencies and current densities of (A) Cu HF, (B) 0.1Sn-Cu HF, (C) 0.3Sn-Cu HF and (D) 1Sn-Cu HF electrodes for gas-phase CO₂ electroreduction at different potentials.



reduction products are observed under open circuit voltage (OCV), *i.e.*, with no current applied, while a large variety of products is obtained under polarization conditions. Acetaldehyde could be observed as one of the main products for all electrodes with several other C₁–C₃ products, while no H₂ from the competitive H₂ evolution reaction could be detected in the examined conditions, which is consistent with the results of former gas-phase CO₂ electroreduction studies.^{16–20} The gas-phase electrocatalytic reduction of CO₂ is a complex multistep reaction involving shared intermediates and multiple reaction pathways.^{19,20} The formation of the different products can be described by a general reaction as shown in Scheme 1 for the cathodic reaction of CO₂ and H⁺ with e[−].

For the Cu HF electrode, the current densities are −0.06, −0.11, −0.18 and −0.36 mA cm^{−2} respectively, at working potentials of −1.2, −1.4, −1.6 and −1.8 V *vs.* CE. Acetaldehyde is the main reduction product at all conditions, which is in agreement with previous studies of gas-phase CO₂ electroreduction.^{18–20} At the potential of −1.4 V *vs.* CE, the total FE for all products is about 10%, while ~25 nmol cm^{−2} h^{−1} acetaldehyde is formed with a FE of around 6%. Table S2 (ESI[†]) summarizes the gas-phase CO₂ electroreduction performances on Cu-based catalysts reported in the literature. Although Gutiérrez-Guerra *et al.* obtained 55 nmol cm^{−2} h^{−1} acetaldehyde production (110 μmol g_{cat}^{−1} h^{−1} with a catalyst loading of 0.5 mg cm^{−2}) at a higher temperature and potential (90 °C, −2.75 V, −1.6 mA cm^{−2}), the FE of acetaldehyde is only 1%.¹⁸ This phenomenon indicates that the gas-phase CO₂ electroreduction system based on HF electrodes could be more efficient, and would be a better platform for developing novel electrocatalysts.

For Sn-Cu HF electrodes, a greater amount of C₃ products such as propanal and acetone could be observed. The current densities for 0.1Sn-Cu HF are greatly improved to −0.12, −0.23, −0.53 and −0.76 mA cm^{−2}, respectively, at each working potential. The small amount of SnO₂ nanoparticles deposited on the Cu HF surface facilitates the kinetics of gas-phase CO₂ electroreduction, leading to the elevated current densities and the reduced reaction resistance (Fig. 2D). Besides, the total FE for all reduction products is about 20%, among which 34 nmol cm^{−2} h^{−1} acetone is formed with a FE of around 6% at −1.4 V *vs.* CE. Although the proportion of acetone in all products has been increased, acetaldehyde is still the main product with a FE of ~8%. The yield of acetaldehyde leaps to 70 nmol cm^{−2} h^{−1}, which is higher than those reported in the literature as shown in Table S2 (ESI[†]),^{18–20} indicating the promoted activities for both C₂ and C₃ products with few deposited SnO₂ nanoparticles on the Cu HF electrode surface (0.1 wt%).

The current densities for 0.3Sn-Cu HF and 1Sn-Cu HF are not further increased. At a working potential of −1.2, −1.4, −1.6 and −1.8 V *vs.* CE, the current densities for 0.3Sn-Cu HF drop to −0.10, −0.18, −0.37 and −0.55 mA cm^{−2} respectively, while those for 1Sn-Cu HF keep decreasing to −0.08, −0.13, −0.21 and −0.49 mA cm^{−2}, but are still higher than those of Cu HF. The current density changes are consistent with the trend of R_{ct} in Fig. 2D. The larger amount of SnO₂ nanoparticles and

even SnO₂ layer on the Cu HF surface with its semiconductive property hinders the charge transfer steps. However, the total FEs for all products on both electrodes are elevated to about 27% and 24%. The increased SnO₂ nanoparticle deposition (0.3 wt%) further promotes the production of acetone and restrains the formation of acetaldehyde. For 0.3Sn-Cu HF, the production of acetaldehyde reduces to 64 nmol cm^{−2} h^{−1} with a FE of 10% at −1.4 V *vs.* CE, while in contrast that of acetone rises to 51 nmol cm^{−2} h^{−1} with a FE of 12%, indicating that the highly dispersed SnO₂ nanoparticles would facilitate further C–C coupling of C₂ intermediates on the Cu surface. While for 1Sn-Cu HF the acetaldehyde production rate keeps reducing to 58 nmol cm^{−2} h^{−1} with a FE of 12%, and that of acetone also drops back to 18 nmol cm^{−2} h^{−1} with a FE of 6%. The excessive SnO₂ loading (1 wt%) leads to the formation of a poorly conductive SnO₂ layer on the Cu HF surface, hindering the charge transfer procedures, resulting in the downward yields for both acetaldehyde and acetone.

It is believed that the sites with SnO₂ particles located on the Cu HF surface are the active centers. As illustrated in Fig. 3, although the Cu HF electrode itself shows some electrochemical activity for gas-phase CO₂ reduction to multicarbon products, the current density and their faradaic efficiencies are much lower compared to the Sn-modified electrodes. Introducing Sn species into aqueous CO₂ electroreduction usually promotes the formation of HCOOH,^{24–28} while during gas-phase CO₂ electroreduction, SnO₂ nanoparticles on the Cu surface play more important roles. The HCOOH species facilitated by virtue of SnO₂ are further converted into *CHO intermediates at the SnO₂/Cu interface, which subsequently dimerize into C₂ intermediate glyoxal (CHO)₂.^{38,39} The next steps include the formation of *COCHO and *CHCOH to obtain acetaldehyde and ethanol,^{38,39} while the adsorbed *CHCOH could further undergo intermolecular C–C coupling with an adjacent *CHO to form propanal and acetone.^{39,40} Thus, the CO₂ activation and subsequent coupling of the intermediates are enhanced by virtue of the decoration of SnO₂ on Cu surfaces, resulting in the improvement of the multicarbon product faradaic efficiencies. However, excess amount of SnO₂ hinders the performance greatly on the 1Sn-Cu HF electrode, implying a slowing of charge transfer due to the dielectric property of the SnO₂ layer. Therefore, the formation of multicarbon products with relatively high efficiency on the appropriate 0.3Sn-Cu HF electrode can be attributed to the synergistic effect between SnO₂ particles and Cu surface, which favour the HCOOH intermediate formation and the subsequent coupling of the key intermediate *CHO.

Conclusions

In summary, a novel gas-phase CO₂ electroreduction system is developed based on the Sn-Cu HF electrode in this work, taking the unique advantages of HFs such as large surface area, adjustable pore structure, good chemical stability and conductivity. The presence of an appropriate amount of SnO₂ nanoparticles



decorated on the Cu HF surface *via* NaBH₄ reduction preparation could optimize the surface active structure for the gas-phase CO₂ electroreduction, which not only facilitates the reaction kinetics to increase the current densities of CO₂ electroreduction, but also improves the C–C coupling of intermediates on the Cu HF surface, promoting the formation of multicarbon oxygenates, especially acetaldehyde and acetone. At a cell voltage of –1.4 V, the yields of acetaldehyde and acetone over the 0.3Sn–Cu HF electrode are 64 and 51 nmol cm^{–2} h^{–1} with FEs of 10 and 12%, respectively. These results highlight the advantages of Sn–Cu HF electrodes in efficient gas-phase CO₂ electroreduction to obtain multicarbon oxygenate products, and inspire the design and development of novel electrocatalytic systems.

Conflicts of interest

There are no conflicts to declare.

Acknowledgements

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