## **Green Chemistry**



## **CORRECTION**

View Article Online
View Journal | View Issue



**Cite this:** *Green Chem.*, 2021, **23**, 10168

## Correction: Flow-through solvolysis enables production of native-like lignin from biomass

David G. Brandner, <sup>a</sup> Jacob S. Kruger, <sup>a</sup> Nicholas E. Thornburg, <sup>a</sup> Gregory G. Facas, <sup>a</sup> Jacob K. Kenny, <sup>a,b</sup> Reagan J. Dreiling, <sup>a</sup> Ana Rita C. Morais, <sup>a</sup> Tom Renders, <sup>a,c</sup> Nicholas S. Cleveland, <sup>a</sup> Renee M. Happs, <sup>a</sup> Rui Katahira, <sup>a</sup> Todd B. Vinzant, <sup>a</sup> Daniel G. Wilcox, <sup>a</sup> Yuriy Román-Leshkov\* <sup>d</sup> and Gregg T. Beckham\* <sup>a,b</sup>

DOI: 10.1039/d1gc90119b

rsc.li/greenchem

Correction for 'Flow-through solvolysis enables production of native-like lignin from biomass' by David G. Brandner et al., Green Chem., 2021, **23**, 5437–5441, DOI: 10.1039/D1GC01591E.

The originally published figures had the first and second R-group structures in Fig. 2 and 4 transposed, such that the propyl alcohol and methoxy propyl groups were switched. The corrected figures indicating the correct R-group structures are as follows:

<sup>&</sup>lt;sup>a</sup>Renewable Resources and Enabling Sciences Center, National Renewable Energy Laboratory, Golden, CO 80401, USA. E-mail: gregg.beckham@nrel.gov

<sup>&</sup>lt;sup>b</sup>Center for Bioenergy Innovation, Oak Ridge National Laboratory, Oak Ridge, TN, USA

<sup>&</sup>lt;sup>c</sup>Center for Sustainable Catalysis and Engineering, KU Leuven, Heverlee, Belgium

<sup>&</sup>lt;sup>d</sup>Department of Chemical Engineering, Massachusetts Institute of Technology, Cambridge, MA, USA. E-mail: yroman@mit.edu

**Green Chemistry** Correction

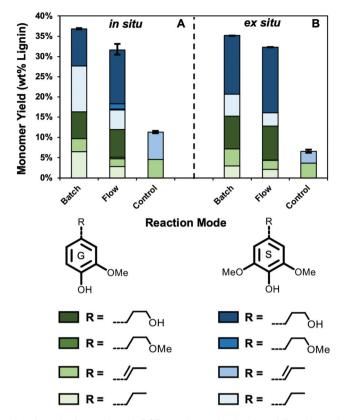


Fig. 2 Monomer yield and selectivity data from in situ and ex situ RCF experiments in batch and flow-through modes. (A) Results from in situ batch and flow-through RCF experiments, including an in situ flow-through control reaction with biomass and carbon support in methanol. (B) Results from ex situ flow solvolysis and subsequent batch and flow-through hydrogenolysis reactions after 1 week of solvolysis liquor storage, as well as an ex situ control of solvolysis liquor run over carbon support only in flow. Product selectivity is shown for syringyl monomers in blue and guaiacyl monomers in green. These data are also provided in Table S2. All experiments were conducted in duplicate, and the error bars are the range for total monomer yield. Batch reactions: either 30 mL (23.76 g) of ex situ solvolysis liquor or 0.313 g poplar in 30 mL methanol, 0.05 g catalyst (either 15 wt% Ni/C or activated carbon support), 30 bar H<sub>2</sub> at 225 °C, 3 h (exclusive of 30 min heating ramp). Flow reactions: 2 mL min<sup>-1</sup> methanol or ex situ solvolysis liquor, 5 g poplar (in situ) or no biomass (ex situ), 0.9 g catalyst (either 15 wt% Ni/C or activated carbon support), 1600 psig, 200 sccm H<sub>2</sub>, 225 °C, 3 h (exclusive of 1 h heating ramp for in situ runs).

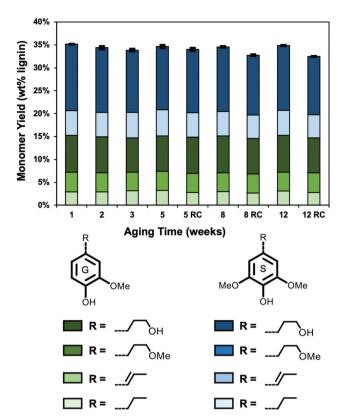


Fig. 4 Time-resolved study of ex situ batch RCF reactions on solvolysis liquor produced in flow and stored in methanol or reconstituted after solvent evaporation (denoted as RC). The monomer yield and selectivity for batch hydrogenolysis reactions of solvolysis liquor produced in flow. The as-made flow solvolysis liquor was tested at 1, 2, 3, 6, 8, and 12 weeks. Removing the methanol before aging was also tested at 5, 8, and 12 weeks. These data are also provided in Table S3. All experiments were conducted in duplicate, and the error bars are the range of the total monomer yield. Reaction conditions: 30 mL ex situ solvolysis liquor, 0.1 g 15 wt% Ni/C catalyst, 30 bar H2 at room temperature, 225 °C, 3 h (exclusive of 30 min heating ramp).

The Royal Society of Chemistry apologises for these errors and any consequent inconvenience to authors and readers.