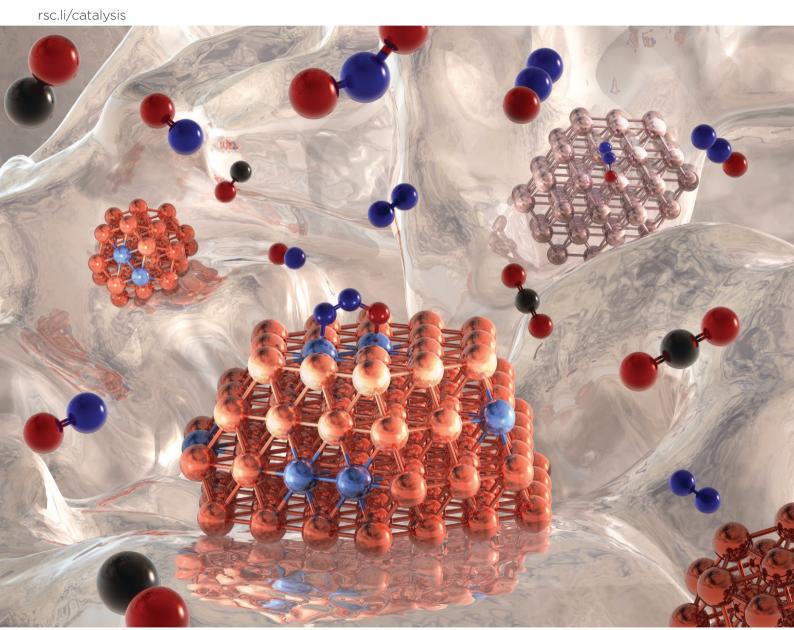
Catalysis Science & Technology

Volume 11 Number 11 7 June 2021 Pages 3621-3934



ISSN 2044-4761



PAPER

Konstantinos G. Papanikolaou and Michail Stamatakis The catalytic decomposition of nitrous oxide and the NO + CO reaction over Ni/Cu dilute and single atom alloy surfaces: first-principles microkinetic modelling

Catalysis Science & Technology



PAPER

View Article Online
View Journal | View Issue



Cite this: Catal. Sci. Technol., 2021, 11, 3681



Konstantinos G. Papanikolaou D and Michail Stamatakis D*

The development of platinum group metal-free (PGM-free) catalysts, which can efficiently reduce pollution-causing emissions, is an important task for overcoming major environmental challenges. In particular, nitrogen oxides (NO_x) are major contributors to air pollution, being one of the culprits for smog and ozone depletion. In this work, we employ density functional theory (DFT) and microkinetic modelling to investigate the decomposition of N_2O and the NO + CO reaction over two PGM-free Ni/Cu dilute alloys. On the first surface, Ni atoms are isolated on the host Cu(111), thereby forming a single atom alloy surface (i.e. Ni/Cu(111) SAA), while on the second, the same atoms are organised as Ni–Ni dimers (i.e. Ni₂Cu(111)). The same reactions are also simulated on pure Cu(111) (i.e. the host surface), and on Rh(111), which is used for benchmarking as Rh is a well-established PGM in emissions control catalysis. Our results suggest that the addition of trace amounts of Ni on Cu(111) may bring about significant improvement to the catalytic performance with regard to the catalytic decomposition of N_2O . Additionally, we determine that $Ni_2Cu(111)$ shows equivalent, or under some circumstances even better, performance as compared to Rh(111) for the NO + CO reaction. This work contributes to the long-standing efforts toward the design of efficient PGM-free catalytic materials for the reduction of noxious gases.

Received 2nd January 2021, Accepted 21st February 2021

DOI: 10.1039/d1cy00011j

rsc.li/catalysis

1. Introduction

The catalytic reduction of nitric oxide (NO) and the decomposition of nitrous oxide (N₂O) are reactions of central significance for the prevention and mitigation of critical environmental problems. The emissions of these molecules are, to a large extent, associated with automobiles, high which are equipped with the so-called three way catalyst (TWC). TWCs are composed of a complex mixture of oxides (e.g. γ -Al₂O₃, BaO), whereon noble metals Rh, Pt and Pd are deposited and hundertake the task of converting noxious gases (e.g. CO, NO, N₂O, C_xH_y) into environmentally acceptable products (i.e. N₂, H₂O, CO₂).

The catalytic reduction of NO by CO is a crucial reaction for controlling automobile emissions, and Rh is regarded as the most promising platinum group metal (PGM) to this end.¹ By and large, this is because Rh can activate the N-O bond at relatively low temperatures²⁻⁴ (the cleavage of this

Thomas Young Centre and Department of Chemical Engineering, University College London, Roberts Building, Torrington Place, London WC1E 7JE, UK. E-mail: m.stamatakis@ucl.ac.uk

bond is in many cases the rate determining step of the NO + CO reaction^{5,6}), and also because of its high resistance to common poisons (e.g. sulphur).⁷ As a result, the mechanism and kinetics of the NO + CO reaction over Rh catalysts have been the subject of extensive research for several experimental,⁸⁻¹⁴ and theoretical studies.¹⁵⁻¹⁹

Although Rh exhibits the best performance among other PGMs toward the reduction of NO, its high cost and limited resources are major shortcomings.1 Unsurprisingly, these downsides have turned the attention of the catalysis community into the search of TWCs that are either PGMfree²⁰⁻²⁹ or utilise minimal amounts of PGMs.³⁰⁻³³ For example, Asakura et al. showed that a NiCu/Al2O3 alloy catalyst exhibits distinct catalytic behaviour compared to its Cu/Al₂O₃ and Ni/Al₂O₃ monometallic counterparts.²¹ The three materials were subject to alternating lean-rich cycles similar to those a TWC may experience during operation. The performance of the Ni-based catalyst deteriorated considerably within the first lean-rich cycle; the Cu-based catalyst was found to be susceptible to oxidation, thereby losing its activity within short time under lean conditions. By contrast, the NiCu/Al₂O₃ catalyst retained very high N₂ productivity for large time intervals even under lean conditions, and could rapidly self-regenerate (i.e. transition

 $[\]dagger$ Electronic supplementary information (ESI) available. See DOI: 10.1039/d1cy00011j

from an oxide state to the corresponding metallic state) in the beginning of each rich period. The authors ascribed the self-regenerative property of NiCu/Al₂O₃ to the coexistence of Ni and Cu oxide species that remained in close contact at the end of lean periods.²¹ Tanaka and co-workers reported that the same bimetallic alloy supported on a Mg-Al mixed oxide serves as an efficient catalyst for hydrocarbon oxidation (i.e. another important reaction that happens over TWCs), under both reducing and oxidative atmospheres.20 Xing et al. synthesised a highly dilute PdCu/Al₂O₃ catalyst, whereby Pd atoms were atomically dispersed on the Cu host.³³ This catalyst not only showed excellent stability during the NO + CO reaction, but also was able to convert fully NO to N2 at relatively low temperatures (473 K).

In our recent theoretical work, we screened a number of dilute alloys for their performance on catalysing important "elementary" steps for the NO + CO reaction (e.g. direct NO dissociation, N2 association and CO oxidation).4 According to our results, a Ni₂Cu alloy, where Ni atoms are organised as Ni-Ni dimers over the Cu host surface, is promising in activating the N-O bond and is capable of performing facile N₂ association.⁴ In particular, Ni₂Cu exhibited the best performance among the investigated bimetallic surfaces, and similar, or in many cases even better, performance than the PGMs in TWCs (i.e. Rh, Pd and Pt). Finally, we argued that this alloy might, in practice, exhibit bifunctional behaviour,³⁴ where Ni sites cleave N-O bonds, while Cu sites serve as the loci for the oxidation of CO.35

In this paper, we employ density functional theory (DFT) and investigate in detail two very relevant reactions to the NO + CO chemistry over Ni/Cu(111) single atom and Ni₂Cu(111) dilute alloy surfaces; these are the formation and decomposition of N_2O^* , in particular, $NO^* + N^* \leftrightarrow N_2O^*$ and $N_2O^* \leftrightarrow N_2^* + O^*$, respectively, where * denotes an adsorbed species. Besides their relevance to the catalytic reduction of NO by CO (N2O is an exhaust gas and an adduct of catalytic surface chemistry),³⁶ these reactions are also of general interest.37 This is because N2O is a potent greenhouse gas and an undesired by-product of large-scale processes like the production of adipic and nitric acid.³⁸ The same reactions are studied over Rh(111), which is used for benchmarking, and also over Cu(111), which is the corresponding host metal surface. We identify different pathways for the activation of N2O* over all surfaces, and we demonstrate that the selectivity of this reaction can be tuned based on the size of the Ni cluster. Importantly, our calculations imply that the presence of small amounts of Ni on Cu(111) strengthens the binding of N₂O* to the surface, thereby preventing its desorption and promoting its dissociation. Finally, using the obtained DFT energetics we parameterise a microkinetic model for the NO + CO reaction over the four (111) surfaces. Our theoretical studies aim at providing a first assessment for the performance of the Ni/Cu dilute alloys toward the aforementioned reaction. These simulations reveal that the performance of Ni₂Cu(111) is certainly superior compared to that of Cu(111) and closely comparable to that of Rh(111). On

this basis, the present study highlights the potential of wellengineered Ni₂Cu alloys, which are composed of inexpensive and abundant metals, for emissions control technologies.

2. Methods

Density functional theory

Periodic DFT calculations were performed using the Vienna ab initio simulation package (VASP) version 5.4.1.39,40 Exchange and correlation effects were treated with the optB86b-vdW functional,41,42 which captures van der Waals (vdW) interactions. 43,44 The latter are important to our work and recent studies have shown that the inclusion of dispersion forces in DFT calculations may increase the binding strength of loosely bound adsorbates of the NO + CO reaction (i.e. N₂O*, CO₂) by as much as 0.7 eV. 16 A kinetic energy cut-off of 400 eV was used for the plane wave basis set that was adopted to describe the wave functions of valence electrons. The interactions between core and valence electrons were modelled by the projector augmented wave (PAW) method. 45 The electronic wave function was converged to 10^{-7} eV, and the structures were relaxed until the forces on each atom were less than 0.01 eV Å⁻¹. The optB86b-vdWcomputed lattice constants are 3.608 Å and 3.829 Å for Cu and Rh, respectively; these values agree well with the corresponding experimental values (3.596 Å and 3.793 Å for Cu and Rh, respectively).46 The metal surfaces were modelled by a 3×3 cell with 5 layers, of which the two bottom ones were fixed at the corresponding lattice constant, thereby simulating the bulk of the material, while the three top layers and any adsorbate atoms were relaxed during geometry optimisation. The Brillouin zone was sampled using a 9 \times 9 \times 1 Monkhorst-Pack k-point mesh. 47 The adsorption energy of N₂O was computed based on the following equation:

$$E_{\rm ads}(N_2O) = E_{\rm tot}^{N_2O+{\rm Slab}} - E_{\rm tot}^{\rm Slab} - E_{\rm tot}^{N_2O_{\rm (g)}}, \tag{1}$$

where $E_{
m tot}^{
m N_2O+Slab}$, $E_{
m tot}^{
m Slab}$ and $E_{
m tot}^{
m N_2O_{(g)}}$ are the total DFT energies for a slab with an N2O* thereon, a clean slab, and an N2O molecule in the gas phase, respectively (the pertinent results are reported in Table 1). The reported transition states were first approached using the dimer method, 48 fully converged with Newton's method, and verified by vibrational analyses, making sure that all the reported transition states had only one imaginary vibrational frequency. The reported activation barriers were computed as $E_a = E_{TS} - E_{IS}$, where E_{TS} and E_{IS} are the DFT energies of the transition and initial states, respectively. Vibrational frequencies were computed within the harmonic approximation where the energy of the system is expressed as a Taylor expansion that includes up to second order terms, and the second derivative was estimated within the finite-difference approximation with a displacement of 0.02 Å.

Microkinetic modelling

The microkinetic model for the NO + CO reaction included 16 reaction steps for Cu(111), Ni/Cu(111) single atom alloy (SAA),

Table 1 Adsorption energies (in eV) and bond distances (in Å) for the N₂O* adsorption geometries over the investigated surfaces. The adsorption energies and bond distances that correspond to the most stable adsorption structure(s) for each surface are shown in bold. A dash indicates either that the adsorption structure is not stable on the specific surface or that it is not a minimum on the potential energy surface (i.e. there was an imaginary frequency in the vibrational analysis). For comparison: $d_{N-N} = 1.14$ Å and $d_{N-O} = 1.20$ Å for gas N₂O (ref. 63)

Adsorption structure	Property	Rh(111)	Cu(111)	Ni/Cu(111) SAA	$Ni_2Cu(111)$
$\eta 1-(N_t\{top\})$	$E_{\rm ads}(N_2O)$	-0.71	-0.21	-0.70	-0.68
(denoted as η1)	$d_{ m N-O}$	1.20	1.20	1.20	1.21
` ,	$d_{ m N-N}$	1.15	1.15	1.15	1.15
$\eta 2$ -f(N _t {bridge},N _c {top})	$E_{\rm ads}({ m N}_2{ m O})$	-0.83	+0.15	-0.43	-0.74
(denoted as $\eta 2NbNt$)	$d_{ m N-O}$	1.22	1.23	1.23	1.23
. ,	$d_{ m N-N}$	1.35	1.29	1.29	1.31
$\eta 2-(N_t\{top\},O\{top\})$	$E_{\rm ads}({ m N}_2{ m O})$	-0.72	-0.20	-0.53	-0.68
(denoted as n2NtOt)	$d_{ m N-O}$	1.33	1.28	1.30	1.32
. ,	$d_{ m N-N}$	1.20	1.19	1.20	1.20
$\eta 2$ -(N _t {hcp},O{top})	$E_{\rm ads}({ m N_2O})$	_	-0.25	-0.44	-0.73
	$d_{ m N-O}$	_	1.30	1.31	1.32
	$d_{ m N-N}$	_	1.27	1.25	1.27

and Ni₂Cu(111) surfaces and 14 reaction steps for Rh(111) -(see Table 2). On the monometallic surfaces there was only one site type, while in the bimetallic surfaces there were Cu and Ni sites, denoted as Cu* and Ni*, respectively. Therefore, for the latter surfaces, we define the "local" coverages as follows:

$$\theta_i^{(m)} = \frac{N_i^{(m)}}{N_{\text{sites}}^{(m)}},$$
 (2)

where $N_i^{(m)}$ is the number of molecules of adsorbate species i that are bound to sites of type m (either Cu* or Ni*); and $N_{\text{sites}}^{(m)}$ is the number of sites of type m. We further define the total coverage of adsorbate i, θ_i , as:

$$\theta_i = \sum_{m=-1}^{N_{\text{st}}} x_m \, \theta_i^{(m)}, \tag{3}$$

where $N_{\rm st}$ is the total number of site types; the summation index m runs over these site types (for the bimetallic surfaces the two types are: Cu* and Ni*; for monometallic surfaces there is only one site type which can be either Cu^* or Rh^*); and x_m is the fraction of sites m on the surface, given as:

$$x_m = \frac{N_{\text{sites}}^{(m)}}{\sum_{\ell=1}^{N_{\text{st}}} N_{\text{sites}}^{(\ell)}}.$$
 (4)

All reactions were considered reversible, and the forward/ reverse rates were given by the typical mass-action law expressions used in microkinetic models, which contain the partial pressures of gas-phase species (considered as constants) and the surface coverages. The gas-phase species taken into account were NO, CO, N2, CO2, N2O, while the surface species were O*, CO*, N*, NO*, CO*, N* and N2O*, as well as the vacant site pseudo-species denoted as *. Regarding the N2O* species, three different adsorption geometries were taken into account (see the next section). The transitions from one adsorption geometry to another could happen through transformation reactions that were included in the reaction

Table 2 Reaction mechanism for the NO + CO reaction, and the corresponding forward (E_{fwd}) and reverse (E_{rev}) barriers (in eV). All reactions are treated as reversible, and dashes mean that the corresponding reaction does not take place on the catalyst surfaces. R1-R7 correspond to molecular adsorptions/desorptions; R8-R16 are surface reactions from which R10 and R11 are N2O* transformation reactions

		Rh(111)		Cu(111)		Ni/Cu(111) SAA		Ni ₂ Cu(111)	
Reaction & reaction number		E_{fwd}	$E_{ m rev}$	E_{fwd}	$E_{ m rev}$	E_{fwd}	$E_{ m rev}$	E_{fwd}	E_{fwd}
$NO_{(g)} + * \leftrightarrow NO*$	(R1)	0.00	2.87	0.00	1.55	0.00	2.10	0.00	2.65
$CO_{(g)} + * \leftrightarrow CO*$	(R2)	0.00	2.20	0.00	0.78	0.00	1.51	0.00	1.71
$N_{2(g)} + * \leftarrow N_2^*$	(R3)	0.00	0.79	0.00	0.15	0.00	0.79	0.00	0.77
$CO_{2(g)} + * \leftrightarrow CO_2^*$	(R4)	0.00	0.27	0.00	0.30	0.00	0.28	0.00	0.37
$N_2O_{(g)} + * \leftrightarrow N_2O^* \eta 2NbNt$	(R5)	0.00	0.83	0.00	0.00	0.00	0.43	0.00	0.74
$N_2O_{(g)}^{\circ} + * \leftrightarrow N_2O^* \eta 2NtOt$	(R6)	0.00	0.72	0.00	0.20	0.00	0.53	0.00	0.68
$N_2O_{(g)} + * \leftrightarrow N_2O^* \eta 1$	(R7)	0.00	0.71	0.00	0.21	0.00	0.70	0.00	0.68
$NO^* + * \leftrightarrow N^* + O^*$	(R8)	1.42	2.03	1.57	1.43	1.47	1.43	1.30	1.24
$NO^* + N^* \leftrightarrow N_2O^* \eta 2NbNt + *$	(R9)	1.50	0.40	0.44	0.94	0.51	0.45	0.60	0.68
$N_2O^* \eta 2NbNt \leftrightarrow N_2O^* \eta 1$	(R10)	0.46	0.30	0.14	0.56	0.24	0.50	0.37	0.31
$N_2O^* \eta 1 \leftrightarrow N_2O^* \eta 2NtOt$	(R11)	0.24	0.40	0.06	0.05	0.29	0.12	0.32	0.32
$N_2O^* \eta 2NtOt + * \leftrightarrow N_2^* + O^*$	(R12)	0.07	2.54	0.05	2.12	0.03	2.26	0.09	2.48
$N_2O^* \eta 2NbNt + * \leftrightarrow N_2^* + O^*$	(R13)	-	-	0.19	2.20	0.23	2.56	0.23	2.51
$CO^* + O^* \leftrightarrow CO_2^* + *$	(R14)	1.17	0.41	0.48	1.22	0.71	0.60	0.88	0.48
$NO^* + NO^* \leftrightarrow N_2O^* \eta 1 + O^*$	(R15)	-	_	0.84	1.82	1.27	1.60	1.30	1.69
$N^* + N^* \leftrightarrow N_2^*$	(R16)	1.85	2.14	0.64	3.6	0.88	3.40	0.62	2.81

mechanism (see R10-R11 in Table 2). The forward rate for reaction j on site-type m is formulated as follows:

$$R_{\text{fad},j}^{(m)} = k_{\text{fad},j}^{(m)} \prod_{g \in \mathcal{R}_{g}^{\text{gas}}} (P_g)^{-\nu gj} \prod_{i \in \mathcal{R}_{g}^{\text{surf}}} \left(\theta_i^{(\mu ij)} \right)^{-\nu ij}. \tag{5}$$

In the above equation, $\mathcal{R}_{j}^{\text{gas}}$ is the set of gas-phase reactant species of reaction j; P_{σ} is the partial pressure of gas species g; and v_{gj} is the stoichiometric coefficient of that gas phase species in reaction j. By convention, stoichiometric coefficients are negative for reactants and positive for products; if a species does not appear in a certain reaction, the corresponding stoichiometric coefficient is zero. Moreover, $\mathcal{R}_i^{\text{surf}}$ is the set of surface reactant species of reaction j; v_{ij} is the stoichiometric coefficient of surface species i in reaction j; and $\theta_i^{(\mu_j)}$ is the local coverage of surface species i on sites of type μ_{ii} . The latter term may or may not be equal to m, since, a reaction that is said to happen on site m (e.g. Ni*), may well involve another species adsorbed on a neighbouring site type (e.g. Cu*). For instance, when reaction R9 of Table 2 (NO* + N* \leftrightarrow N₂O* + *) happens on a Ni site, NO* is found on the Ni site, while N* is on Cu; therefore, the rate would be:

$$R_{\text{fwd},9}^{(\text{Ni*})} = k_{\text{fwd},i}^{(\text{Ni*})} \, \theta_{\text{NO*}}^{(\text{Ni*})} \, \theta_{\text{N*}}^{(\text{Cu*})}.$$

For further information on the considered configurations for events that involve two sites see Table S3 in the ESI.† Similarly, the reverse rate for reaction j on sitetype m is formulated as follows:

$$R_{\text{rev},j}^{(m)} = k_{\text{rev},j}^{(m)} \prod_{g \in \mathcal{P}_g^{\text{QAS}}} (P_g)^{\nu g j} \prod_{i \in \mathcal{P}_g^{\text{Surf}}} \left(\theta_i^{(\mu i j)} \right)^{\nu i j}.$$
 (6)

Note that $\mathcal{P}_{i}^{\text{gas}}$ and $\mathcal{P}_{i}^{\text{surf}}$ denote sets of products of reaction j, and the stoichiometric coefficients appear with their "original" positive signs, because of the convention mentioned earlier.

The rate constant calculations for the surface reactions $(k_{\text{fwd.}i}^{(m)} \text{ and } k_{\text{rev.}j}^{(m)})$ are calculated after invoking widely used transition state theory approximations. If a reaction cannot happen on a certain site, then $k_{\text{fwd},j}^{(m)} = k_{\text{rev},j}^{(m)} = 0$. We further define the net rate of reaction *j* on site *m* as:

$$R_i^{(m)} = R_{\text{fwd}, i}^{(m)} - R_{\text{rev}, j}^{(m)}. \tag{7}$$

The coverage profiles over the investigated surfaces can now be obtained by solving a system of ordinary differential equations (ODEs) written as

$$\frac{\mathrm{d}\theta_i^{(m)}}{\mathrm{d}t} = \sum_{i=1}^{N_\mathrm{R}} \nu_{ij} R_j^{(m)},\tag{8}$$

where $N_{\rm R}$ is the total number of (reversible) reactions. The ODEs were solved in Matlab R2017a, using the ode23s solver, which is capable of dealing with stiff equations. An important constraint that had to be satisfied is the site conservation law

$$\sum_{i=1}^{N_{\rm s}} \sum_{m=1}^{N_{\rm st}} x_m \, \theta_i^{(m)} = 1. \tag{9}$$

To calculate the rate constants of the reactions the following assumptions and approximations were adopted. Molecular adsorptions were assumed as non-activated events with a 2D gas as a transition state, where molecules retain translational and rotational degrees of freedom. Accordingly, the rate constants for molecular adsorptions were calculated using the Hertz-Knudsen equation assuming a sticking coefficient equal to unity (eqn (10)):49

$$k_{\rm ads} = \frac{A_{\rm st}}{\sqrt{2 \cdot \pi \cdot m_{\rm i} \cdot k_{\rm B} \cdot T}},\tag{10}$$

where m_i is the mass of molecule i; k_B is the Boltzmann constant; T is the temperature; and A_{st} is the effective area of the adsorption site. The pressure of gas phase-species is omitted in eqn (10) because it is explicitly taken into account in eqn (5) and (6). The rate constants for surface reactions and desorption events were calculated using the Eyring equation:50

$$k_{\text{fwd/rev},j}^{(m)} = \frac{k_{\text{B}}T}{h} \frac{Q^{\text{TS}}}{Q^{\text{IS}}} \exp\left(-\frac{E_{\text{a,fwd/rev},j}^{(m)}}{k_{\text{B}}T}\right), \tag{11}$$

where h is the Planck's constant; Q^{TS} and Q^{IS} are the partition functions of the transition and initial states, respectively. The rate constants of surface reactions were calculated using the approximation, and therefore translations and rotations of surface species were treated as vibrations; under these circumstances, the partition function of an adsorbed state (either initial or transition state) is equal to the vibrational partition function (q_{vib}) :

$$Q \approx q_{\rm vib} = \prod_{k=1}^{S} \frac{\mathrm{e}^{-\hbar\omega_k/(2k_{\rm B}T)}}{1 - \mathrm{e}^{-\hbar\omega_k/(k_{\rm B}T)}}, \tag{12}$$

where S is the number of vibrational modes; ω_k is the angular frequency of the kth normal mode of vibration; and \hbar is the reduced Planck's constant.

The net rates for N2 and N2O are calculated as follows:

$$R_{\rm N_{2,net}} = \sum_{m=1}^{N_{\rm st}} R_{\rm R_{3,net}}^{(m)}, \tag{13}$$

$$R_{\text{N}_2\text{O,net}} = \sum_{j=R5}^{R7} \sum_{m=1}^{N_{\text{st}}} R_{j,\text{net}}^{(m)}, \tag{14}$$

where $R_{i,\text{net}}^{(m)}$ is the net reaction rate of j on site m. Finally, the contribution of each elementary step to the total reaction rate was quantified using Campbell's degree of rate control (DRC) - (see eqn (15)):51,52

$$X_{\text{RC},j}^{(m)} = \frac{k_j^{(m)}}{R_{\text{N}_{2,\text{net}}}} \left(\frac{\partial R_{\text{N}_{2,\text{net}}}}{\partial k_j^{(m)}} \right)_{K_\ell^{(n)}, k_{\ell \neq j}^{(n \neq m)}} = \left(\frac{\partial \ln R_{N_{2,\text{net}}}}{\partial \ln k_j^{(m)}} \right)_{K_\ell^{(n)}, k_{\ell \neq j}^{(n + m)}}, \quad (15)$$

where $X_{RC,j}^{(m)}$ is the DRC coefficient for reaction j on site m; $R_{N_{2,net}}$ is the net reaction rate for the production of N_2 (eqn (13)) on site m (eqn (7)); $K_{\ell}^{(n)}$ is the equilibrium constant of reaction $\ell = 1,..., N_R$ on site $m = 1,..., N_{st}$; $k_{\ell \neq j}^{(n \neq m)}$ are the rate constants for all other steps than j that take place on either Cu^* or Ni^* (the site other than m). The larger the absolute value of $X_{RC,i}^{(m)}$ the larger the influence of that reaction step to the overall reaction rate; also when $X_{RC,j}^{(m)} > 0$, the reaction is ratelimiting, whereas for $X_{RC,j}^{(m)} < 0$ the reaction is rate-inhibiting.

3. Results and discussion

3.1. Adsorption of N2O on Ni/Cu dilute alloy surfaces

Gas-phase nitrous oxide is a linear molecule ($C_{\infty V}$ symmetry) and a harmful by-product of industrial processes (e.g. nitric acid production). Its catalytic decomposition has been investigated over many transition metals, including Rh,53 Cu,⁵⁴ Ru,⁵⁵ Pd,⁵⁶ Fe,⁵⁷ Ni,⁵⁸ Pt,⁵⁹ PdAu,⁶⁰ and PdCu.⁶¹ Here, we first examine the adsorption of nitrous oxide on Cu(111), Ni/Cu(111) SAA and Ni₂Cu(111) surfaces, but also on our "benchmarking surface" Rh(111).

It is known that N2O* may adopt a number of different adsorption geometries upon its interaction with metal surfaces. 56,62 Accordingly, we identify six stable adsorption geometries out of which four are displayed in Fig. 1, while the full list is given in the first section of the ESI.† These four adsorption structures are important because they are adopted by N_2O^* upon its decomposition to either to $N_2^* + O^*$ or $NO^* +$ N^* (see sections 3.2 and 3.3), and are denoted as: $\eta 1-(N_t\{top\})$, $\eta 2$ -f(N_t{bridge},N_c{top}), $\eta 2$ -(N_t{top},O{top}), and $\eta 2$ -(N_t{hcp}, O{top}) - (Fig. 1). Since we will be referring often to the first three throughout this paper, we adopt the following abbreviations for them: η1, η2NbNt and η2NtOt, respectively.

The computed adsorption energies for the four geometries, along with the N-O $(d_{
m N-O})$ and N-N $(d_{
m N-N})$ bond distances are summarised in Table 1. We note that the most preferred N2O* adsorption structure on Rh(111) is the η 2NbNt mode ($E_{ads}(N_2O) = -0.83 \text{ eV}$) – (Table 1). This type of adsorption can be considered as a weak chemisorption because: (1) the geometry of N₂O* deviates noticeably from the gas-phase geometry, which is linear; and (2) because the N-N bond is considerably elongated ($d_{\rm N-N}$ = 1.14 Å and 1.35 Å for gas-phase N₂O and η2NbNt N₂O*, respectively). The following most stable adsorption structures are the η1 and η 2NtOt with $E_{ads}(N_2O) = -0.71$ eV and $E_{ads}(N_2O) = -0.72$ eV, respectively. The former structure can be characterised as a strong physisorption owing to the unaffected geometry and bond lengths of η1 N2O* as compared to gas-phase N2O $(d_{N-N} = 1.14 \text{ Å and } d_{N-O} = 1.20 \text{ Å for gas N}_2\text{O})$ – (Table 1).

The activation of the N-N bond in the n2NbNt structure can be elucidated by careful examination of the electronic structure of this geometry (Fig. S2†).62 Our density of states (DOS) analyses indicate that in η 2NbNt the 2π and 3π orbitals of N2O* become broader as a result of their interaction with the metal states, whilst the same is not true for the $\eta 1$ structure where the same orbitals appear rather localised (Fig. S2†). The broadening of the 3π orbitals is indicative of electron back-donation, which in turn leads to the activation

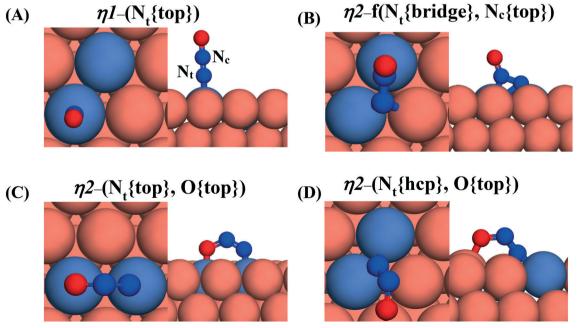


Fig. 1 Top and side views of (A) η 1-(N_t(top)); (B) η 2-f(N_t(bridge), N_c(top)); (C) η 2-(N_t(top), O(top)) and (D) η 2-(N_t(hcp), O(top)) adsorption structure. On the side view of (A) we highlight the terminal (N_t) and central (N_c) nitrogen atoms. Ni, Cu, N and O atoms are shown in purple, orange, blue and red, respectively. The adsorption geometries are shown over Ni₂Cu(111), but they are representative for all surfaces.

of the N-N bond. This result is in qualitative agreement with the work of Paul et al. 62 where the authors, by means of DFT calculations using the PW91 functional, found that the η2NbNt and η1 are ca. equally stable on Rh(111) ($E_{ads}(N_2O) =$ -0.35 eV and $E_{ads}(N_2O)$ -0.39 eV, respectively). Moreover, our calculations suggest that N₂O* is bound stronger by ca. 0.5 eV on Rh(111) compared to the work of Paul et al. 62 and this discrepancy may be attributed to the inclusion of nonlocal electron correlation effects in our calculations.¹⁶

We proceed by investigating the adsorption of N2O* over Cu(111) and the Cu-based alloy surfaces where Ni atoms are either distributed as isolated atoms or as Ni-Ni dimers. In general, we find that N2O* interacts weakly with Cu(111) (Table 1) and that the most stable adsorption geometries thereon are $\eta 2-(N_t\{hcp\},O\{top\})$ and $\eta 1$ for which $E_{ads}(N_2O) = -0.25$ eV and -0.21 eV, respectively. Yet, the presence of a small amount of Ni on the surface layer of Cu(111) brings about drastic changes with regard to the binding strength of N2O* (Table 1). Thus, the most stable adsorption geometry on the Ni/Cu(111) SAA surface is $\eta 1$ ($E_{ads}(N_2O) = -0.70$ eV), where the N_t atom of N₂O* interacts closely with the isolated Ni atom. By contrast, the η2NbNt and η2-(N_t{hcp},O{top}) are the most favourable adsorption modes for Ni₂Cu(111), with $E_{ads}(N_2O) = -0.74$ eV $E_{\rm ads}(N_2O) = -0.73$ eV, respectively. Crucially, the corresponding adsorption processes are about 0.5 eV more exothermic than the $\eta 1$ and $\eta 2-(N_t\{hcp\},O\{top\})$ modes on Cu(111), thereby highlighting the potential of the Ni/Cu dilute alloys for the decomposition of N2O*. With this in mind, we examine the latter reaction over Cu(111) and the Cu-based surfaces.

3.2. N₂O* formation and activation on Cu-based surfaces – the "conventional" reaction path

In order to verify the reliability of our data, we first perform calculations in relation to the activation of N2O* on the Rh(111) surface, and compare our results to those reported in previous theoretical works. The computed reaction pathway for the decomposition of N_2O^* to either $N_2^* + O^*$ or NO* + N* is displayed in Fig. S3.† In this "conventional" reaction pathway the transformation of NO* + N* to N2 + O* proceeds via the \u03c41 adsorption structure (Fig. S3\u00e4), and our computed activation barriers are congruent with previously calculated values. For example, Paul et al.62 reported an activation barrier of 0.34 eV for the transformation of the η2NtOt structure to the η1 structure; this number is in good agreement with our computed barrier ($E_a = 0.38$ eV from state (4) to state (3) in Fig. S3†). Another example is the required barrier for the decomposition of the η 2NbNt (state (1) in Fig. S3 \dagger) structure to NO* + N*. The values for this work and ref. 62 are 0.36 eV and 0.41 eV, respectively. Consequently, we use our computational setup and study the decomposition of N₂O* on Cu(111), Ni/Cu(111) SAA and Ni₂Cu(111) surfaces.

Fig. 2(A) shows the "conventional" decomposition pathway for Cu(111), where the $\eta 1$ structure "connects" the NO* + N* and N₂* + O* states. During the NO + CO reaction, the combination of NO* and N* species may result in the formation of N_2O^* , which ideally should be decomposed to $N_2^* + O^*$. Once formed, N₂O* adopts the η2NbNt structure, and starting from this geometry on Cu(111) (state (1) in Fig. 2(A)), we realise that the formation of N₂* and O* is thermodynamically and kinetically favoured over the formation of NO* and O*. In particular, the decomposition of η2NbNt N₂O* to NO* + O* requires the traversing of a barrier of 0.94 eV, while the three barriers to be traversed for the formation of $N_2^* + O^*$ are only 0.14 eV, 0.06 eV and 0.06 eV. Yet, we conjecture that Cu(111) will be susceptible to the production of N2O during the NO + CO reaction. This is because of the following reasons: (1) N_2O^* can be formed from NO* and N* species with a relatively small kinetic barrier of 0.44 eV (Fig. 2(A)); once N₂O* is formed from NO* and N* in the η 2NbNt structure (state (1) in Fig. 2(A)), its

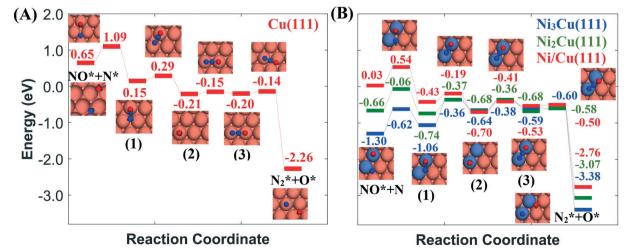


Fig. 2 Reaction path for the decomposition of N_2O^* to $NO^* + N^*$ or $N_2^* + O^*$ over (A) Cu(111) surface; (B) Ni/Cu(111) SAA, Ni₂Cu(111) and $Ni_3Cu(111)$ surfaces. The numbering of the adsorbed configurations of N_2O is as follows: (1) $\eta 2NbNt$, (2) $\eta 1$ and (3) $\eta 2NtOt$. The zero level corresponds to infinitely separated (and thus non-interacting) N₂O molecule and clean slab. States without any labelling are transition states. Side views of the different states are shown in the ESI.† Ni, Cu, O and N atoms are shown in purple, orange, red and blue, respectively.

desorption is the most probable scenario (Table 1); and (3) even in the $\eta 1$ and $\eta 2NtOt$ geometries, N_2O^* binds weakly on Cu(111) and its desorption will be proceeding at considerable rates even at moderate reaction temperatures.

On the contrary, we find that the decomposition of N2O* may be significantly promoted by embedding one or two Ni atoms on Cu(111), thereby forming a single atom alloy or a dilute alloy surface, 64-71 where in the latter case, Ni atoms are organised as dimers or trimers. We note that ab initio Monte Carlo simulations predict that small Ni clusters (e.g. Ni-Ni dimers) are abundant in Ni/Cu dilute alloy surfaces under vacuum conditions, while their thermodynamic stability can be further enhanced by exposing the alloy surface to CO at a range of partial pressures that lead to dopant fractional coverages less than 1.⁷² The computed desorption energies for η2NbNt N₂O* (state (1) in Fig. 2(B)) on Ni/Cu(111) SAA and Ni₂Cu(111) are 0.43 eV and 0.74 eV, respectively. By considering this adsorption structure as the starting point, we note that the transformation of N_2O^* to structure $\eta 1$ (i.e. state (2)) and $\eta 2NtOt$ (i.e. state (3)), and the decomposition of the latter to N_2^* + O would generally traverse small barriers, which are always less than 0.30 eV and 0.40 eV for Ni/Cu(111) SAA and Ni₂Cu(111), respectively. Thus, η 2NbNt N₂O* (state (1)) would prefer to decompose to N₂* + O*, than desorb to the gas phase (Fig. 2(B)).

The exothermic adsorption of $\eta 2NbNt\ N_2O^*$ (*i.e.* the first adopted structure after N_2O^* formation from NO^* and N^*) will, to certain extent, prevent the N_2O^* desorption to the gas phase. This will increase the probability of "trapping" N_2O^* to the catalyst surface and therefore the probability for its decomposition. Moreover, even stronger $\eta 2NbNt\ N_2O^*$ binding should be expected on Ni–Ni dimers and Ni single atoms that are embedded on more open surfaces than the densely packed (111) and on undercoordinated sites that can be found in catalytic nanoparticles.

Another point that merits consideration is that the selectivity toward the decomposition products (NO* + N* or N $_2$ + O*) can be altered by tuning the size of the Ni cluster. To better illustrate this point, we present the corresponding N2O* decomposition pathway over a Cu(111) with an embedded Ni trimer (Ni₃-Cu(111) in Fig. 2(B)). Interestingly, the kinetic barrier for the formation of the \(\eta 2NbNt\) geometry (state (1) in Fig. 2(B)) from NO* and N* increases monotonically at increasing size of the Ni cluster ($E_a = 0.51$ eV, 0.60 eV and 0.68 eV for Ni/Cu(111) SAA, Ni₂Cu(111) and Ni₃Cu(111), respectively). The opposite is true for the reverse reaction (i.e. η2NbNt N2O* to NO* + N*) for which $E_a = 0.97$ eV, 0.68 eV and 0.44 eV for Ni/Cu(111) SAA, Ni₂-Cu(111) and Ni₃Cu(111), respectively. This result underlines the importance of developing ways to control the architecture of dilute alloy surfaces and former studies discuss that this may be achieved under reactive conditions. 72-75

$3.3.\ N_2O$ formation and activation on Cu-based surfaces – an alternative reaction path

Besides the "conventional" route for the decomposition of N_2O^* (Fig. 2), we have identified an alternative reaction

pathway which, to the best of our knowledge, has not been reported before. This path exists only on Cu(111) and on the Ni/Cu dilute alloy surfaces. The decomposition of N₂O* to N₂* + O* happens without transformation to the $\eta 1$ structure as in the conventional pathway. In contrast, in this pathway the two decomposed states (*i.e.* NO* + N* and N₂* + O*) are "connected" via the $\eta 2$ -(N_t{fcc},O{top}) adsorption structure (this is as Fig. 1(D) but over an fcc site; the two adsorption structures exhibit the same binding strength – $E_{\rm ads}(N_2O)$ = -0.74 eV for Ni₂Cu(111)). After performing a number of test simulations, we could not identify the same path on Rh(111), and this might explain why it was not reported in previous studies. ⁶²

For all the Cu-based surfaces, Fig. 3 shows that $\eta 2NbNt$ N_2O^* is formed in the same way as in the reaction path of Fig. 2. Then the $\eta 2NbNt$ N_2O^* rotates around the axis of the N–N bond, thereby bringing the more electronegative O closer to the surface. Interestingly, once O is closer to the Ni/Cu(111) SAA, the N–O bond is immediately cleaved and the kinetic barrier for this process is only 0.23 eV (Fig. 3(B)). The ease by which the N–O is broken over the Ni/Cu SAA surface may be associated with the sharp and narrow distribution of the electron density of the single Ni atom close to the Fermi level, 4,76 and it is expected that back-donation to the 3π antibonding orbital of N_2O^* enables the facile activation of the N–O bond.

By contrast, the decomposition of N₂O* to N₂* and O* is taking place through the η^2 - (N_t{fcc},O{top}) geometry (state (2) and (3) in Fig. 3(A) and (C), respectively) over Cu(111) and Ni₂Cu(111). The intervening barriers between the η2NbNt and $N_2^* + O^*$ states are small (≤ 0.23 eV). Irrespective of these low kinetic barriers, Cu(111) is still expected to be prone to releasing N2O* to the gas phase given the generally weak N_2O^* -Cu(111) interaction (Fig. 3(A)). The same is not true for Ni₂Cu(111) where the N₂O* desorption energy is in the range of 0.65-0.74 eV, while the kinetic barriers that lead to N₂* + O* are between 0.06 eV and 0.23 eV (Fig. 3(C)). Given the similar energetics between the pathway of Fig. 3 and the "conventional" one, we conclude that both of them need to be considered in the reaction mechanism of the NO + CO reaction. Importantly, the existence of alternative N2O* decomposition paths may provide an explanation of the high selectivity to N₂ exhibited by dilute Cu-based alloys.³³

3.4. N_2O formation and activation on Cu-based surfaces through the formation of $(NO)_2^*$

Thus far, the formation of nitrous oxide was assumed to proceed through the coupling of NO* and N* species (Fig. 2 and 3). NO* is of course the product of the molecular adsorption of gas-phase nitric oxide. On the other hand, the existence of N* species implies prior scission of the N-O bond. In general, low-index coinage metal surfaces exhibit large kinetic barriers for the direct dissociation of NO* (E_a = 1.57 eV for Cu (111) and (100), and E_a > 2.5 eV for Ag and Au (111) and (100) surfaces),⁴ thereby being ineffective at activating the N-O

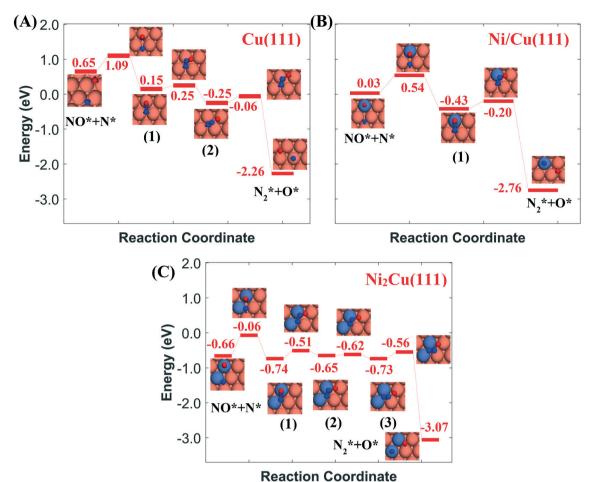


Fig. 3 A second reaction path for the decomposition of N₂O* on (A) Cu(111); (B) Ni/Cu(111) SAA and (C) Ni₂Cu(111). State (1) corresponds to a η 2NbNt structure in all panels. The η 2-(N_t{fcc},O{top}) structure is state (2) and state (3) in panels (A) and (C), respectively. The zero level corresponds to infinitely separated (and thus non-interacting) N₂O molecule and clean slab. States without any labelling are transition states. Side views of the different states are shown in the ESI.† Ni, Cu, O and N atoms are shown in purple, orange, red and blue, respectively.

bond of NO*. Yet, they are known to be active for the reduction of NO, which is mainly converted to N2O. The activity of coinage metal surfaces is ascribed to the formation of NO* dimer species (i.e. (NO)*) whose N-O bonds are more easily activated than those of monomeric NO*.33,54,77-79 This species is formed owing to vdW interactions between neighbouring NO* species,80 and may be observed even at relatively low NO* coverages over Cu(111).43 On the contrary, our calculations indicate that NO* is adsorbed as a monomer on Rh(111) and this is corroborated by near edge X-ray absorption fine structure spectroscopy.81

The most energetically favoured adsorption structure of NO* on Cu(111) is an N-down geometry where the N-O bond axis is perpendicular to the surface, and N is above an fcc hollow site $(E_{ads}(NO) = -1.55 \text{ eV})$. A stable NO dimer is formed when two NO* species are adsorbed on adjacent fcc sites (NO* + NO* state in Fig. 4(A)). We note that in the relaxed geometry of this state, the O atoms of the neighbouring nitric oxide adspecies are slightly tilted towards each other (Fig. 4(A)). The thermodynamic stability of this configuration has been confirmed by other DFT studies, as well as in scanning

tunnelling microscopy experiments. 43,80 The two neighbouring NO* species can be converted to N₂O* (with an η1 structure) and O* (see state (1) in Fig. 4(A)). This is happening via a transition state where one of the two NO* adsorbates bends down to the Cu(111) surface, while the other is slightly lifted (Fig. 4(A)). Once $\eta 1 N_2 O^*$ is formed, its decomposition occurs in the same way as in Fig. 2(A), namely through the formation of the η2NtOt structure. We note that the structure of the (NO)* transition state, and the computed barrier for the scission of the N-O bond via the (NO)* precursor ($E_a = 0.84$ eV) are in excellent agreement with the DFT calculations by Bogicevic and Hass ($E_a = 0.82 \text{ eV}$), ⁵⁴ thereby furnishing further evidence for the reliability of our calculations.

We continue by investigating the same reaction pathway over the Ni/Cu(111) SAA and Ni₂Cu(111) surfaces. Our calculations show that the formation of N2O* via the dimerisation route is indeed possible over small Ni clusters. In contrast to Cu(111), on these dilute alloys (NO)* adopts a flat geometry parallel to the surfaces in the transition state, and the computed kinetic barriers are 1.27 eV and 1.30 eV for Ni/Cu(111) SAA and Ni₂Cu(111),

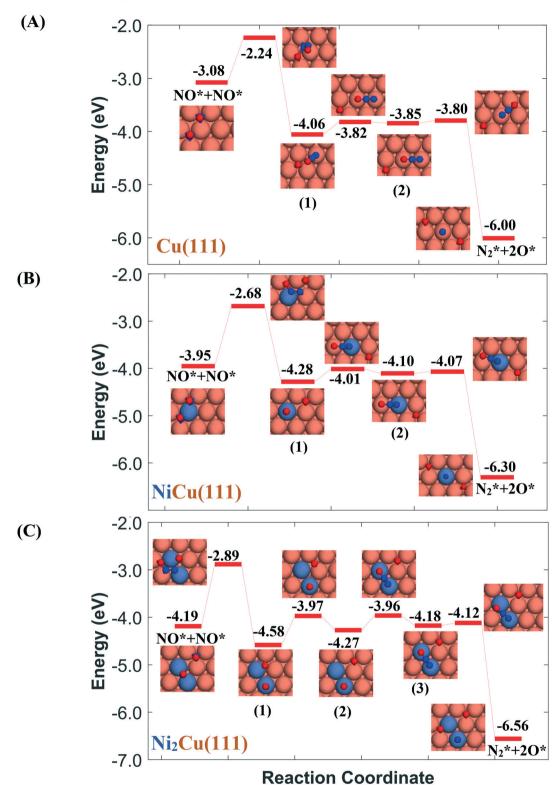


Fig. 4 Reaction pathway for the formation and decomposition of N_2O^* via $(NO)_2^*$ for (A) Cu(111); (B) Ni/Cu(111) SAA; and (C) Ni₂Cu(111). The zero level corresponds to two non-interacting gas-phase NO molecules and a clean slab. States without any labelling are transition states. Side views of the different states are shown in the ESI.† Ni, Cu, O and N atoms are shown in purple, orange, red and blue, respectively.

respectively (Fig. 4(A) and (B)). These values are higher than the computed barrier for $Cu(111) - (E_a = 0.84 \text{ eV})$, and this may be attributed to the extra energy cost required for

bending down both NO* species. Nevertheless, they are lower than or equal to the corresponding kinetic barriers for the direct dissociation of NO* ($E_a = 1.47$ eV and 1.30 eV

for Ni/Cu(111) SAA and Ni₂Cu(111), respectively).⁴ Therefore, the formation and decomposition of N2O* through dimerisation is another pathway that should be included in the reaction mechanism of the NO + CO reaction over the Cu-based alloy surfaces.

To elucidate the effect of the Ni cluster size to the formation rate of $\eta 1 N_2O^*$ and O^* via the $(NO)^*_2$ intermediate, we perform additional calculations for the Ni₃-Cu(111) surface (Fig. S5 \dagger). On this surface, we compute E_a = 1.77 eV and E_a = 1.37 eV for the splitting of the N-O bond *via* dimerisation (Fig. S5†) and via the direct NO* dissociation,4 respectively. Additionally, we note that on Ni dimers and trimers the formed $\eta 1 \ N_2O^*$ can be transformed to the η2NtOt (state (3) in Fig. 4(C) for Ni₂Cu), and decompose to $N_2^* + 2O^*$ only after O^* spillover to Cu(111). The barrier for O* diffusion from a mixed hollow site to a Cu hollow site over Ni₂Cu(111) (from state (1) to state (2) in Fig. 4(C)) is 0.61 eV. Therefore, this extra energy cost in conjunction with the large kinetic barrier for the scission of the N-O bond of (NO)* render the decomposition of N2O* through the dimerisation pathway less likely on Ni clusters with more than two Ni atoms.

3.5. The microkinetics of the NO + CO reaction over Ni/Cu dilute alloys

Using the computed energetics for the decomposition of N₂O* in conjunction with previous results for the formation of N₂*, CO* oxidation and NO* decomposition over Ni/Cu surfaces, 4 we parameterise a microkinetic model for the NO + CO reaction. Our studies include one site type for Cu(111) and Rh(111) surfaces, and two site types for the bimetallic surfaces (see section 2). The goal is a preliminary assessment of the catalytic performance of the Ni/Cu dilute alloys and a comparison to Cu(111) and Rh(111). Accordingly, the microkinetic simulations are performed in the absence of adsorbate-adsorbate interactions, 82-85 whose effects on the coverage profiles, and consequently on the catalytic performance of the Cu-based surfaces may be important (this is part of ongoing research). Regarding the bimetallic surfaces, we assume that Ni* species (single atoms or dimers) can be occupied by one adspecies (e.g. CO*), which can react with another adspecies on a Cu site (e.g. O*) and form a product on the Ni site (e.g. CO_2^*). Such events are treated as reactions that take place on the dopant site, and follow the energetics computed over the Ni site of the Ni/Cu surfaces. On the contrary, the Cu(111) energetics are used if the reaction involves two adspecies that are both on Cu sites (Table S3†). Despite their simplicity, such microkinetic models are capable of capturing the salient features of experimental trends, 86 providing mechanistic insights,⁸⁷ and aiding identification of the active site during catalysis.^{88,89}

The NO + CO reaction mechanism is composed of 16 reversible reaction steps, shown in Table 2 along with their forward and reverse barriers. For all simulations the total pressure is set to 16.0 Torr with $P_{\text{NO}} = P_{\text{CO}} = 8.0$ Torr, thereby replicating the experimental conditions of Belton and coworkers. 13 At this point, we note that the associative desorption of O2 and the formation of NO2 are reactions through which O* may be removed from the surface and they could be included in the microkinetic model. However, both of them exhibit very high kinetic barriers, and on this basis are excluded from the reaction mechanism. For example, the computed barrier for the O₂* association reaction on Cu(111) is 2.10 eV, while the barrier for the reverse process is just 0.16 eV (see section 7 in the ESI†); these values are in reasonable agreement with former DFT calculations. 90 Along the same lines, we find that the dissociation of NO₂ to NO* + O* is significantly more facile than its formation and its desorption (see section 7 in the ESI†).

We first simulate the NO + CO reaction on Rh(111). The total coverages of the surface species and the DRC analysis for this surface are shown in Fig. 5(A). The coverage profiles reveal that the catalyst surface is saturated with NO* species up to temperatures of 1000 K. Under these conditions, the high surface coverage gives rise to steric hindrance effects, which prevent the dissociation of NO*. This behaviour has been reported in the experimental work of Herman et al., and is in qualitative agreement with the fact that Rh(111) is catalytically active only at temperatures higher than 625 K.13 Moreover, our model predicts that surface sites are freed up by NO adspecies only at T > 1000 K; this high "T threshold" can be attributed to (1) the absence of the repulsive NO*-NO* interactions in our microkinetics (see Fig. S4 in the ESI†); and (2) the very strong NO*-Rh(111) interaction predicted by the optB86b-vdW functional. In particular, NO*-NO* interactions may contribute to the reduction of the surface coverage, and in turn, this will generate free sites whereon the dissociation of NO* can happen at lower temperatures than those predicted by our model. 91,92 Regarding the second point, we find that the most stable adsorption site for NO* on Rh(111) is hcp, in line with previous computational and experimental works. ^{5,93,94} However, we compute $E_{ads}(NO) = -2.85$ eV, which is larger than the PW91 values of Mavrikakis et al. 94 (-2.39 eV -2×2 cell) and of González et al. 93 (-2.62 eV - 3 × 3 cell). Unfortunately, at coverages of 0.11 ML, like in our DFT calculations, accurate experimental measurement of $E_{ads}(NO)$ is challenging because of the tendency of NO* to dissociate on Rh(111).94 The reduction of the NO* surface coverage gives rise to the formation of N* and O* at T > 1000 K. The accumulation of N* species in the temperature range of 1000-1200 K, is associated with the inefficiency of Rh(111) in forming η 2NbNt N₂O* (R9, E_a = 1.50 eV) and N₂* (R16, E_a = 1.85 eV) - (Table 2). Both reaction steps are rate-limiting with a positive DRC coefficient (0.19 $\leq X_{DRC,R9} \leq 0.30$) between 1100 K and 1300 K (Fig. 5(A)). Along the same lines, the buildup of O* is ascribed to the moderate activation barrier for the CO* oxidation reaction ($E_a = 1.17 \text{ eV} - \text{R}14 \text{ in Table 2}$), which is the only reaction that exhibits a reasonable activation barrier for the removal of O* from the surface.

The corresponding coverage profiles and DRC analysis for Cu(111) are displayed in Fig. 5(B). Cu(111) exhibits rather

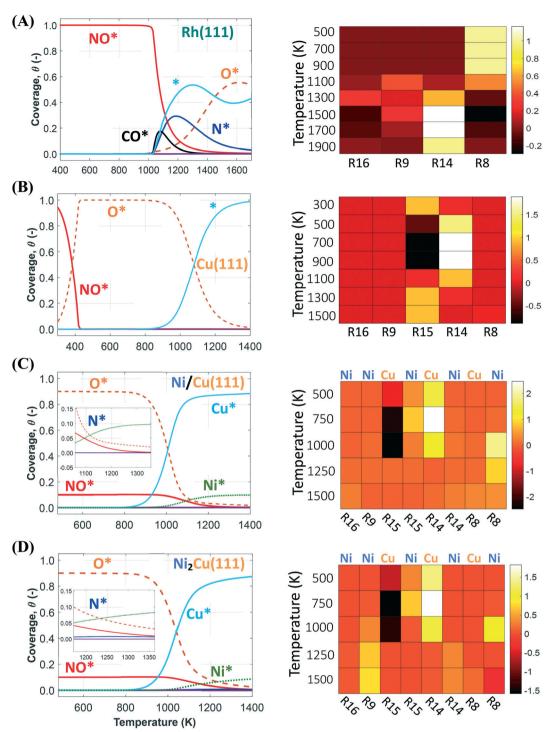


Fig. 5 Total coverage (eqn (3)) profiles and DRC coefficients (X_{RC}) for the NO + CO reaction steps for (A) Rh(111); (B) Cu(111); (C) Ni/Cu(111) SAA; and (D) Ni₂Cu(111). X_{RC} values are presented at various temperatures by means of heatmaps; the site whereon the reaction occurs is shown on the top of the heatmaps for the bimetallic surfaces.

different behaviour than Rh(111). In particular, at T < 350 K all surface sites are occupied by NO*, but at T > 350 K there is a sharp increase in the coverage of the O* species. This sharp transition is attributed to the activation of the N-O bond *via* the NO* dimerisation reaction ($E_{\rm a} = 0.84$ eV) – (R15 in Table 2), which converts 2NO* to O* and η 1 N₂O*. The

catalyst surface remains fully covered by O* within the temperature range of 420–900 K. Accordingly, our DRC analysis shows that under these conditions, the oxidation of CO* controls the reaction rate, and that the NO* dimerisation is an inhibiting step as it adds more O* onto the surface (Fig. 5(B)).

The last two coverage profiles shown Fig. 5 (panels (C) and (D)) are those for the Ni/Cu alloy surfaces. These surfaces contain a total of 10 000 sites, out of which 9000 are Cu sites (Cu*) and 1000 are Ni sites (Ni*). The coverage profiles are very similar in both cases, and indicate that Cu* sites are covered with O* up to ca. 900 K (similar to Cu(111)), while Ni* sites are poisoned by NO*. A disparity between the two surfaces is seen between 1000 K and 1500 K, where we observe a small build-up of N* over Ni₂Cu(111) only (Fig. 5(C) and (D)). The presence of N* on the latter surface is indicative of the direct NO* dissociation (R8, $E_a = 1.30$ eV - Table 2), which happens to a smaller extent on the SAA surface (R8, $E_a = 1.47$ eV - Table 2). Markedly, the N* accumulation remains at low levels thanks to the efficiency of Ni₂Cu(111) in forming N₂* and η2NbNt N_2O^* (Table 2). The latter can either decompose to N_2^* + O* (R10, R11, R12 and R13) or desorb (R5).

Next, we examine the activity and selectivity to N2 of the four surfaces. The latter metric is computed as

$$S_{\rm N_2/N_2O} = \frac{R_{\rm N_{2,net}}}{R_{\rm N_{2,net}} + R_{\rm N_{2}O_{net}}},$$
 (16)

 $R_{N_{2,per}}$ and $R_{N_2O_{per}}$ are the net reaction rates for N_2 and N_2O_2 respectively (see eqn (13) and (14)).

Fig. 6 displays the activity plots for the studied surfaces, where the catalytic rate is provided by the computed turnover frequency (TOF) at various temperatures. The observed trend for Rh(111) (Fig. 6(A)) can be rationalised based on the corresponding coverage plot (Fig. 5(A)). As seen in Fig. 6(A), the activity of Rh(111) is low below 950 K owing to the high NO* coverage, which hinders the direct NO* dissociation (Fig. 5(A)). On the contrary, for T > 950 K there is an increase in the catalytic activity. Initially the rate of N2O production is greater than that of N_2 , and only at T > 1200 K the two production rates become equal (Fig. 6(A)).

Similarly to Rh(111), the catalytic activity of Cu(111) can be explained from the coverage profile plot in Fig. 5(B). For this surface, low (i.e. 300-500 K) and high (i.e. 500-1400 K) temperatures can be discussed separately. Between 300 K and 420 K, we observe that the catalytic activity increases steadily (see Fig. S11 in the ESI†), and the surface transitions from a NO*-rich phase to an O*-rich phase. As discussed earlier, this transition is associated with the dimerisation reaction (R15 in Table 2), which consumes NO*, releases N2O and yields O*. At ca. 420 K, there is a sharp reduction in the catalytic activity (Fig. S11††), and this is the result of the poisoning of Cu(111) by O* species. The surface remains in the poisoned state for temperatures up to ca. 700 K, where the removal of O* species happens efficiently and the dimerisation reaction begins to take place again at considerable rates (see Fig. 6(B) and the heatmap in Fig. 5(B)). Finally, for T > 1000 K there is a decrease in the catalytic activity (Fig. 6(B)) because under these conditions, the gaseous state of the reactants is preferred over adsorption on the catalytic surface. Throughout the investigated temperature range, the production rate of N₂O is far greater than the production rate of N2, and this is attributed to the inability of Cu(111) to directly dissociate NO* as well as to the weak binding of the $\eta 1 N_2O^*$ produced by the dimerisation reaction.

On the other hand, enhanced catalytic activity can be achieved when Ni* species are present in Cu(111) (Fig. 6(C) and (D)). Remarkably, the production rate of N_2 is considerably larger on Ni/Cu(111) SAA than on Cu(111) and even more so on Ni₂Cu(111), where the N₂ and N₂O production rates become equal beyond 1000 K.

Given the importance of S_{N_a/N_aO} , this section concludes with an investigation on this metric, followed by suggestions for further improvements in this regard. Regarding Rh(111), our microkinetic model predicts that the main nitrogen-containing product from Rh(111) at T < 1000 K is N2O, whilst the production of N2 exhibits a substantial increase beyond 1100 K (Fig. 7(A)). The latter temperature corresponds to the point where the surface sites are freed up (Fig. 5(A)), and the dissociation of NO* is enabled. Notably, this trend is qualitatively in line with the reactor experiments of Peden et al.12 on Rh(111). The experiments showed that Rh(111) exhibits poor selectivity to N2 for reaction temperatures up to 700 K; yet, the authors observed a sharp increase in S_{N_a/N_aO} temperatures higher than that. One should expect that closer quantitative agreement can be accounting for coverage effects, which will tend

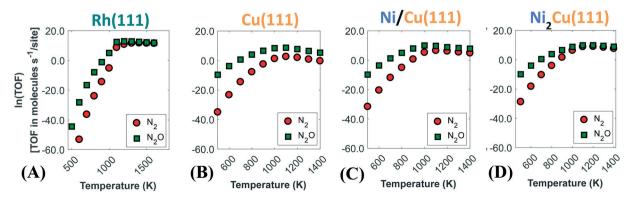


Fig. 6 Rates of production of nitrogen-containing products for (A) Rh(111); (B) Cu(111); (C) Ni/Cu(111) SAA; and (D) Ni₂Cu(111)

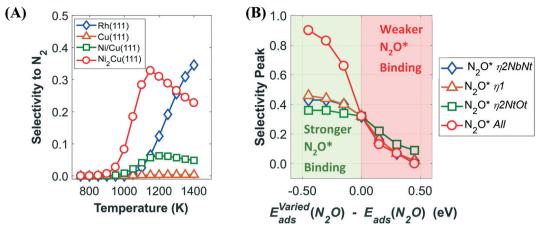


Fig. 7 (A) Selectivity to N_2 for Cu(111), Rh(111) and the Ni/Cu alloys. (B) Maximum of the N_2 selectivity peak at various N_2O^* adsorption energies. Values on the right correspond to smaller N₂O* binding strength on Ni* than the DFT-computed (red shade); values on the left correspond to larger N_2O^* binding strength on Ni* than the DFT-computed (green shade). In the simulations of panel (B) only the desorption energy of N_2O^* was varied, whilst all the other kinetic barriers were kept fixed at their DFT-computed values.

decrease the surface coverage at T < 1000 K (see Fig. S4†), thereby freeing up sites and shifting the profiles of Fig. 5 to lower temperatures.

The same analysis for Cu(111) reveals that this surface is indeed susceptible to the formation of N2O (Fig. 7(A)). We find that the main way of forming N_2O^* (in the $\eta 1$ structure) on Cu(111) is via the formation of the (NO) $_2^*$ intermediate followed by N-O activation (R15). This is in line with molecular beam/infrared spectroscopy studies on other Cu low-index surfaces.⁷⁷ The η1 N₂O* can go through one of the following paths: (1) desorb directly ($E_a = 0.21 \text{ eV}$); (2) transform to $\eta 2NtOt N_2O^*$ ($E_a = 0.06 \text{ eV}$) and either desorb $(E_a = 0.20 \text{ eV})$ or dissociate to $N_2^* + O^*$ $(E_a = 0.05 \text{ eV})$; (3) transform to $\eta 2NbNt N_2O^*$ ($E_a = 0.56 \text{ eV}$) and desorb spontaneously. Therefore, N2O* can easily undergo transformations over Cu(111), but in every new state there is a high probability for desorption, thereby explaining the poor N₂ selectivity of this surface.

Interestingly, the catalytic behaviour Ni/Cu(111) SAA and Ni₂Cu(111) appears to be more similar to Rh(111), which is well established for the NO + CO reaction, than to Cu(111), which is the host metal (Fig. 7(A)). In more precise terms, it is observed that on each of the dilute alloy surfaces the selectivity to N_2 remains low at T < 900 K but increases sharply at higher temperatures similarly to Rh(111). $S_{N,/N,O}$ for both Ni/Cu(111) SAA and Ni₂Cu(111) exhibits an interesting behaviour by which it first increases for T > 900K and then decreases at 1200 K.

To shed light on this behaviour, we have carried out additional microkinetic simulations for Ni₂Cu(111) where the activation barrier of one of the following events on Ni* is assigned a very large value (e.g. 2.5 eV): (1) NO* direct dissociation (R8); (2) N₂* formation (R16); (3) NO* dimerisation (R15); and (4) n2NbNt N2O* formation (R9). In doing so, we record how the selectivity peak responds to the obstruction of the aforementioned events (see section 9 in the ESI†). We determine that the selectivity spike in the two bimetallic surfaces is associated with the direct dissociation of NO* and the formation of η2NbNt N2O*, which could subsequently decompose to N₂* + O* (see section 9 in the ESI†). Therefore, it is the ability of Ni/Cu alloys to form and process n2NbNt N2O* that gives rise to the selectivity peak in Fig. 7(A). The selectivity to N_2 enters a downturn because at T> 1200 K, there is a rise in the N_2O^* desorption rate. On the other hand, the formation of N₂ on Rh(111) is solely relying on the direct dissociation of NO* and such a selectivity spike is not observed (Fig. 7(A)).

Accordingly, the higher intensity of the N₂ selectivity peak on Ni₂Cu(111) than on Ni/Cu(111) SAA can be explained by: (1) the higher concentration of N* species on Ni₂Cu(111) owing to its better ability to dissociate NO* as compared to Ni/Cu(111) SAA (see Table 2 and Fig. 5(D)); (2) the generally stronger interaction between N2O* and Ni2Cu(111) than that between N2O* and Ni/Cu(111) SAA (Table 2), noting that strong interaction will favour the decomposition of N₂O* over its desorption.

Moreover, we explore the effect of the N2O* binding strength on the height of the selectivity peak on Ni₂Cu(111) by performing a sensitivity analysis with respect to $E_{ads}(N_2O)$ - (Fig. 7(B)). Remarkably, the adsorption energy of N2O* appears to have a great impact upon the N2 selectivity at 1100-200 K (Fig. 7(B)). For example, shifting the adsorption energy of all N₂O* adsorption structures to more negative values by 0.15 eV and 0.30 eV (i.e. stronger binding) results to an increase in the maximum of the peak by 0.31 (from 0.33 to 0.67) and 0.52 (from 0.33 to 0.85), respectively. We conjecture that binding strengths of this magnitude may be provided by sites on more open low-index surfaces (e.g. (100) and (110)) but also on stepped surfaces, and if this is true, the presence of such sites will contribute dramatically to the N₂ selectivity at low temperatures. Therefore, this result underscores the potential of well-engineered dilute Ni/Cu alloys for the NO + CO reaction and creates motivation for further investigations.

Finally, given the importance of $E_{ads}(N_2O)$ we have computed the binding energy of N2O* using other vdW functionals, including optPBE-vdW, BEEF-vdW,95 and the Tkatchenko-Scheffler method (DFT-TS) - (see Table S4 in the ESI†). The latter method is similar to the DFT-D2 method of Grimme, ⁹⁶ with the difference that the dispersion coefficients and the damping function in the dispersion correction are dependent on the charge density.97 These additional calculations highlight that significant variations in the predicted $E_{ads}(N_2O)$ should be expected when treating vdW interactions based on different approaches, 98 thereby influencing the predictions of ab initio microkinetic and kinetic Monte Carlo models (see section 11 in the ESI†).

4. Concluding remarks

By means of DFT calculations, we performed a thorough investigation of the formation and decomposition of N2O* over Rh(111), Cu(111), a Ni/Cu(111) SAA surface and a Ni₂-Cu(111) surface, where Ni atoms form dimer clusters. The DFT-derived energetics, in conjunction with results from our previous work,4 were then used to parameterise a microkinetic model for the NO + CO reaction.

Our DFT calculations showed that the presence of a small amount of Ni over Cu(111) strengthens significantly the interaction between N2O* and the catalyst surface. This enhanced interaction is desirable because it prevents the desorption of N2O*, thereby benefiting the selectivity to N2 during the NO + CO reaction. Regarding the decomposition of N₂O*, we explored three competing reaction paths. In the first pathway the decomposition products (i.e. NO* + O* and $N_2^* + O^*$) are connected through the $\eta 1$ adsorption structure of N₂O*. In the second, the same products are connected through another N_2O^* adsorption structure (i.e. $\eta 2-(N_t\{fcc\},$ O(top)), and the third involves the formation of an (NO)* intermediate. These paths exhibit comparable energetics and therefore merit consideration when modelling the kinetics of the NO + CO reaction. We also demonstrated that the selectivity of the Ni/Cu dilute alloy surfaces can be manipulated by tuning the size of the Ni cluster; generally, the formation of NO* and atomic nitrogen is kinetically favoured over "large clusters" (e.g. trimers), whereas small clusters (i.e. dimers) and single atoms promote the dissociation of N₂O* to N₂* and atomic oxygen.

Finally, the performance of the Ni/Cu dilute alloy surfaces was assessed by means of microkinetic simulations for the NO + CO reaction. Our studies highlighted the potential of Ni₂Cu(111), which showed considerably improved catalytic performance as compared to Cu(111) and comparable performance to the best transition metal for the reduction of NO (i.e. Rh(111)). Future work could focus on the effect of adsorbate-adsorbate interactions on the reaction kinetics of the NO + CO reaction, 99-101 and explore the behaviour of other facets of the Ni₂Cu catalyst in an effort to quantify potential structure-sensitivity effects.

Conflicts of interest

There are no conflicts of interest to declare.

Acknowledgements

K. G. P. is funded by the Department of Chemical Engineering at University College London. The authors acknowledge the use the UCL High Performance Computing Facilities Kathleen@UCL in the completion of the simulations of this work. We are also grateful to the U.K. Materials and Molecular Modelling Hub, which is partially funded by EPSRC (EP/ P020194/1), for computational resources (HPC facility Thomas). K. G. P. thanks Sai Yadavalli for fruitful discussions on the performance of DFT exchange and correlation functionals.

References

- 1 V. P. Zhdanov and B. Kasemo, Surf. Sci. Rep., 1997, 29, 31 - 33.
- 2 W. T. Wallace, Y. Cai, M. S. Chen and D. W. Goodman, J. Phys. Chem. B, 2006, 110, 6245-6249.
- 3 D. Loffreda, D. Simon and P. Sautet, J. Catal., 2003, 213, 211-225.
- 4 K. G. Papanikolaou and M. Stamatakis, Catal. Sci. Technol., 2020, 10, 5815-5828.
- 5 H. J. Borg, J. F. C.-J. M. Reijerse, R. A. Van Santen and J. W. Niemantsverdriet, J. Chem. Phys., 1994, 101, 10052-10063.
- 6 D. N. Belton, C. L. Dimaggio, S. J. Schmieg and K. Y. S. Ng, J. Catal., 1995, 157, 559-568.
- 7 K. C. Taylor, Catal. Rev.: Sci. Eng., 1993, 35, 457-481.
- 8 F. Zaera and C. S. Gopinath, Phys. Chem. Chem. Phys., 2003, 5, 646-654.
- 9 C. S. Gopinath and F. Zaera, J. Catal., 2001, 200, 270-287.
- 10 C. H. F. Peden, D. W. Goodman, D. S. Blair, P. J. Berlowitz, G. B. Fisher and S. H. Oh, J. Phys. Chem., 1988, 92, 1563-1567.
- 11 L. H. Dubois, P. K. Hansma and G. A. Somorjai, J. Catal., 1980, 65, 318-327.
- 12 C. H. F. Peden, D. N. Belton and S. J. Schmieg, J. Catal., 1995, 155, 204-218.
- 13 G. S. Herman, C. H. F. Peden, S. J. Schmieg and D. N. Belton, Catal. Lett., 1999, 62, 131-138.
- 14 H. Permana, K. Y. Simon Ng, C. H. F. Peden, S. J. Schmieg, D. K. Lambert and D. N. Belton, Catal. Lett., 1997, 47, 5-15.
- 15 L. Tan, L. Huang, Y. Liu and Q. Wang, Appl. Surf. Sci., 2018, 444, 276-286.
- 16 A. Ishikawa and Y. Tateyama, J. Phys. Chem. C, 2018, 122, 17378-17383.
- 17 J. Liu, L. Tan, L. Huang, Q. Wang and Y. Liu, Langmuir, 2020, 36, 3127-3140.
- 18 V. P. Zhdanov and B. Kasemo, Catal. Lett., 1996, 40, 197-202.
- 19 J. Cortés and E. Valencia, J. Phys. Chem. B, 2006, 110, 7887-7897.
- 20 C. Y. Kang, M. Taniguchi, M. Uenishi and H. Tanaka, Chem. Lett., 2012, 41, 822-824.

- 21 H. Asakura, T. Onuki, S. Hosokawa, N. Takagi, S. Sakaki, K. Teramura and T. Tanaka, Phys. Chem. Chem. Phys., 2019, 21, 18816-18822.
- 22 K. Ueda, C. A. Ang, Y. Ito, J. Ohyama and A. Satsuma, Catal. Sci. Technol., 2016, 6, 5797-5800.
- 23 H. Yoshida, Y. Okabe, N. Yamashita, S. Hinokuma and M. Machida, Catal. Today, 2017, 281, 590-595.
- 24 K. Koizumi, H. Yoshida, M. Boero, K. Tamai, S. Hosokawa, T. Tanaka, K. Nobusada and M. Machida, Phys. Chem. Chem. Phys., 2018, 20, 25592-25601.
- 25 H. Yoshida, N. Yamashita, S. Ijichi, Y. Okabe, S. Misumi, S. Hinokuma and M. Machida, ACS Catal., 2015, 5, 6738-6747.
- 26 T. Hirakawa, Y. Shimokawa, W. Tokuzumi, T. Sato, M. Tsushida, H. Yoshida, J. Ohyama and M. Machida, ACS Appl. Nano Mater., 2020, 3, 9097-9107.
- 27 N. Takagi, K. Ishimura, H. Miura, T. Shishido, R. Fukuda, M. Ehara and S. Sakaki, ACS Omega, 2019, 4, 2596–2609.
- 28 H. Yoshida, Y. Kawakami, W. Tokuzumi, Y. Shimokawa, T. Hirakawa, J. Ohyama and M. Machida, Bull. Chem. Soc. Jpn., 2020, 93, 1050-1055.
- 29 C. B. Jones, I. Khurana, S. H. Krishna, A. J. Shih, W. N. Delgass, J. T. Miller, F. H. Ribeiro, W. F. Schneider and R. Gounder, J. Catal., 2020, 389, 140-149.
- 30 Y. Nishihata, J. Mizuki, T. Akao, H. Tanaka, M. Uenishi, M. Kimura, T. Okamoto and N. Hamada, Nature, 2002, 418, 164-167.
- 31 S. Hosokawa, T. Shibano, H. Koga, M. Matsui, H. Asakura, K. Teramura, M. Okumura and T. Tanaka, ChemCatChem, 2020, 12, 4276-4280.
- 32 L. Zhang, I. A. W. Filot, Y.-Q. Su, J.-X. Liu and E. J. M. Hensen, J. Catal., 2018, 363, 154-163.
- 33 F. Xing, J. Jeon, T. Toyao, K. Shimizu and S. Furukawa, Chem. Sci., 2019, 10, 8292-8298.
- 34 R. Réocreux, P. L. Kress, R. T. Hannagan, V. Çınar, M. Stamatakis and E. C. H. Sykes, J. Phys. Chem. Lett., 2020, 11, 8751-8757.
- 35 S. Kandoi, A. A. Gokhale, L. C. Grabow, J. A. Dumesic and M. Mavrikakis, Catal. Lett., 2004, 93, 93-100.
- 36 F. Zaera and C. S. Gopinath, Chem. Phys. Lett., 2000, 332, 209-214.
- 37 W. B. Tolman, Angew. Chem., Int. Ed., 2010, 49, 1018–1024.
- 38 H. Tian, R. Xu, J. G. Canadell, R. L. Thompson, W. Winiwarter, P. Suntharalingam, E. A. Davidson, P. Ciais, R. B. Jackson, G. Janssens-Maenhout, M. J. Prather, P. Regnier, N. Pan, S. Pan, G. P. Peters, H. Shi, F. N. Tubiello, S. Zaehle, F. Zhou, A. Arneth, G. Battaglia, S. Berthet, L. Bopp, A. F. Bouwman, E. T. Buitenhuis, J. Chang, M. P. Chipperfield, S. R. S. Dangal, E. Dlugokencky, J. W. Elkins, B. D. Eyre, B. Fu, B. Hall, A. Ito, F. Joos, P. B. Krummel, A. Landolfi, G. G. Laruelle, R. Lauerwald, W. Li, S. Lienert, T. Maavara, M. MacLeod, D. B. Millet, S. Olin, P. K. Patra, R. G. Prinn, P. A. Raymond, D. J. Ruiz, G. R. van der Werf, N. Vuichard, J. Wang, R. F. Weiss, K. C. Wells, C. Wilson, J. Yang and Y. Yao, *Nature*, 2020, 586, 248–256.
- 39 G. Kresse and J. Furthmüller, Comput. Mater. Sci., 1996, 6, 15-50.

- 40 G. Kresse and J. Hafner, Phys. Rev. B: Condens. Matter Mater. Phys., 1993, 47, 558-561.
- 41 M. Dion, H. Rydberg, E. Schröder, D. C. Langreth and B. I. Lundqvist, Phys. Rev. Lett., 2004, 92, 246401.
- 42 J. Klimeš, D. R. Bowler and A. Michaelides, J. Phys.: Condens. Matter, 2010, 22, 022201.
- 43 A. Shiotari, S. Hatta, H. Okuyama and T. Aruga, J. Chem. Phys., 2014, 141, 134705.
- 44 J. Klimeš, D. R. Bowler and A. Michaelides, Phys. Rev. B: Condens. Matter Mater. Phys., 2011, 83, 195131.
- 45 P. E. Blöchl, Phys. Rev. B: Condens. Matter Mater. Phys., 1994, 50, 17953-17979.
- 46 P. Haas, F. Tran and P. Blaha, Phys. Rev. B: Condens. Matter Mater. Phys., 2009, 79, 085104.
- 47 J. D. Pack and H. J. Monkhorst, Phys. Rev. B: Solid State, 1977, 16, 1748-1749.
- 48 G. Henkelman and H. Jónsson, J. Chem. Phys., 1999, 111, 7010-7022.
- 49 K. W. Kolasinski, in Surface Science, John Wiley & Sons, Ltd, Chichester, UK, 2012, pp. 51-114.
- 50 W. F. K. Wynne-Jones and H. Evring, J. Chem. Phys., 1935, 3, 492-502.
- 51 C. T. Campbell, ACS Catal., 2017, 7, 2770–2779.
- 52 C. Stegelmann, A. Andreasen and C. T. Campbell, J. Am. Chem. Soc., 2009, 131, 8077-8082.
- 53 Y. Li and M. Bowker, Surf. Sci., 1996, 348, 67-76.
- 54 A. Bogicevic and K. C. Hass, Surf. Sci., 2002, 506, L237-L242.
- 55 V. G. Komvokis, M. Marti, A. Delimitis, I. A. Vasalos and K. S. Triantafyllidis, Appl. Catal., B, 2011, 103, 62-71.
- 56 A. Kokalj, I. Kobal and T. Matsushima, J. Phys. Chem. B, 2003, 107, 2741-2747.
- 57 S. Y. Wu, C. H. Su, J. G. Chang, H. T. Chen, C. H. Hou and H. L. Chen, Comput. Mater. Sci., 2011, 50, 3311-3314.
- 58 H. Orita and N. Itoh, Surf. Sci., 2004, 550, 166-176.
- 59 R. Burch, S. T. Daniells and P. Hu, J. Chem. Phys., 2004, 121, 2737.
- 60 X. Wei, X. F. Yang, A. Q. Wang, L. Li, X. Y. Liu, T. Zhang, C. Y. Mou and J. Li, *J. Phys. Chem. C*, 2012, **116**, 6222–6232.
- 61 K. Kim, S. Baek, J. J. Kim and J. W. Han, Appl. Surf. Sci., 2020, 510, 145349.
- 62 J.-F. Paul, J. Pérez-Ramírez, F. Ample and J. M. Ricart, J. Phys. Chem. B, 2004, 108, 17921-17927.
- 63 J. L. Teffo and A. Chédin, J. Mol. Spectrosc., 1989, 135, 389-409.
- 64 M. D. Marcinkowski, M. T. Darby, J. Liu, J. M. Wimble, F. R. Lucci, S. Lee, A. Michaelides, M. Flytzani-Stephanopoulos, M. Stamatakis and E. C. H. Sykes, Nat. Chem., 2018, 10, 325-332.
- 65 M. B. Boucher, B. Zugic, G. Cladaras, J. Kammert, M. D. Marcinkowski, T. J. Lawton, E. C. H. Sykes and M. Flytzani-Stephanopoulos, Phys. Chem. Chem. Phys., 2013, 15, 12187-12196.
- 66 R. T. Hannagan, G. Giannakakis, Flytzani-Stephanopoulos and E. C. H. Sykes, Chem. Rev., 2020, 120, 12044-12088.

Paper

- 67 M. T. Darby, M. Stamatakis, A. Michaelides and E. C. H. Sykes, *J. Phys. Chem. Lett.*, 2018, 9, 5636–5646.
- 68 D. A. Patel, R. T. Hannagan, P. L. Kress, A. C. Schilling, V. Çınar and E. C. H. Sykes, J. Phys. Chem. C, 2019, 123, 28142–28147.
- 69 G. Giannakakis, M. Flytzani-Stephanopoulos and E. C. H. Sykes, *Acc. Chem. Res.*, 2019, **52**, 237–247.
- 70 G. Kyriakou, M. B. Boucher, A. D. Jewell, E. a Lewis, T. J. Lawton, A. E. Baber, H. L. Tierney, M. Flytzani-Stephanopoulos and E. C. H. Sykes, *Science*, 2012, 335, 1209–1212.
- 71 J. Liu, F. R. Lucci, M. Yang, S. Lee, M. D. Marcinkowski, A. J. Therrien, C. T. Williams, E. C. H. Sykes and M. Flytzani-Stephanopoulos, *J. Am. Chem. Soc.*, 2016, **138**, 6396–6399.
- 72 K. G. Papanikolaou, M. T. Darby and M. Stamatakis, *ACS Catal.*, 2020, **10**, 1224–1236.
- 73 K. G. Papanikolaou, M. T. Darby and M. Stamatakis, *J. Phys. Chem. C*, 2019, **123**, 9128–9138.
- 74 M. T. Darby, E. C. H. Sykes, A. Michaelides and M. Stamatakis, *Top. Catal.*, 2018, 61, 428–438.
- 75 M. Ouyang, K. G. Papanikolaou, A. Boubnov, A. S. Hoffman, G. Giannakakis, S. R. Bare, M. Stamatakis, M. Flytzani-Stephanopoulos and E. C. H. Sykes, *Nat. Commun.*, 2021, 12, 1549.
- 76 H. Thirumalai and J. R. Kitchin, *Top. Catal.*, 2018, **61**, 462–474.
- 77 W. A. Brown, R. K. Sharma, D. A. King and S. Haq, *J. Phys. Chem.*, 1996, **100**, 12559–12568.
- 78 Y. Wang, D. Zhang, Z. Yu and C. Liu, *J. Phys. Chem. C*, 2010, 114, 2711–2716.
- 79 Z. P. Liu, S. J. Jenkins and D. A. King, J. Am. Chem. Soc., 2004, 126, 7336–7340.
- 80 T. N. Pham, Y. Hamamoto, K. Inagaki, D. N. Son, I. Hamada and Y. Morikawa, *J. Phys. Chem. C*, 2020, **124**, 2968–2977.
- 81 I. Nakai, H. Kondoh, T. Shimada, R. Yokota, T. Katayama, T. Ohta and N. Kosugi, *J. Chem. Phys.*, 2007, **127**, 024701.
- 82 K. G. Papanikolaou, M. T. Darby and M. Stamatakis, J. Chem. Phys., 2018, 149, 184701.

- 83 M. Stamatakis, J. Phys.: Condens. Matter, 2015, 27, 013001.
- 84 K. G. Papanikolaou and M. Stamatakis, in *Computational Modelling of Nanomaterials*, 2020, pp. 95–125.
- 85 M. Stamatakis and S. Piccinin, ACS Catal., 2016, 6, 2105-2111.
- 86 J. K. Nørskov, F. Studt, F. Abild-Pedersen and T. Bligaard, in *Fundamental Concepts in Heterogeneous Catalysis*, John Wiley & Sons, Inc, Hoboken, NJ, USA, 2014, pp. 68–84.
- 87 L. C. Grabow and M. Mavrikakis, *ACS Catal.*, 2011, 1, 365–384.
- 88 S. Li, S. Singh, J. A. Dumesic and M. Mavrikakis, *Catal. Sci. Technol.*, 2019, 9, 2836–2848.
- 89 S. Bhandari, S. Rangarajan and M. Mavrikakis, *Acc. Chem. Res.*, 2020, 53, 1893–1904.
- 90 Y. Xu and M. Mavrikakis, Surf. Sci., 2001, 494, 131-144.
- 91 A. C. Lausche, A. J. Medford, T. S. Khan, Y. Xu, T. Bligaard, F. Abild-Pedersen, J. K. Nørskov and F. Studt, *J. Catal.*, 2013, 307, 275–282.
- 92 J. Schumann, A. J. Medford, J. S. Yoo, Z. J. Zhao, P. Bothra, A. Cao, F. Studt, F. Abild-Pedersen and J. K. Nørskov, ACS Catal., 2018, 8, 3447–3453.
- 93 S. González, C. Sousa and F. Illas, *J. Catal.*, 2006, 239, 431-440.
- 94 M. Mavrikakis, J. Rempel, J. Greeley, L. B. Hansen and J. K. Nørskov, J. Chem. Phys., 2002, 117, 6737–6744.
- 95 J. Wellendorff, K. T. Lundgaard, A. Møgelhøj, V. Petzold, D. D. Landis, J. K. Nørskov, T. Bligaard and K. W. Jacobsen, *Phys. Rev. B: Condens. Matter Mater. Phys.*, 2012, 85, 235149.
- 96 S. Grimme, J. Comput. Chem., 2006, 27, 1787-1799.
- 97 A. Tkatchenko and M. Scheffler, Phys. Rev. Lett., 2009, 102, 6-9.
- 98 S. Gautier, S. N. Steinmann, C. Michel, P. Fleurat-Lessard and P. Sautet, *Phys. Chem. Chem. Phys.*, 2015, 17, 28921–28930.
- 99 R. B. Getman, Y. Xu and W. F. Schneider, *J. Phys. Chem. C*, 2008, 9559–9572.
- 100 S. Matera, W. F. Schneider, A. Heyden and A. Savara, *ACS Catal.*, 2019, **9**, 6624–6647.
- 101 D. J. Schmidt, W. Chen, C. Wolverton and W. F. Schneider, *J. Chem. Theory Comput.*, 2012, **8**, 264–273.