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On the effect of metal loading on the reducibility and redox chemistry of ceria supported Pd catalysts†

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The effect of Pd loading on the redox characteristics of a ceria support was examined using *in situ* Pd K-edge XAS, Ce L₃-edge XAS and *in situ* X-ray diffraction techniques. Analysis of the data obtained from these techniques indicates that the onset temperature for the partial reduction of Ce(IV) to Ce(III), by exposure to H₂, varies inversely with the loading of Pd. Whilst the onset and completion temperatures of the reduction of Ce(IV) to Ce(III) are different, both samples yield the same maximal fraction of Ce(III) formation independent of Pd loading. Furthermore, the partial reduction of Ce is found to be concurrent with the reduction of PdO and demonstrated that the presence of metallic Pd is necessary for the reduction of the CeO₂ support. Upon passivation by room temperature oxidation, a full oxidation of the reduced ceria support was observed. However, only a mild surface oxidation of Pd was identified. The mild passivation of the Pd is found to lead to a highly reactive sample upon a second reduction by H₂. The onset of the reduction of Pd and Ce has been demonstrated to be independent of the Pd loading after a mild passivation with both samples exhibiting near room temperature reduction in the presence of H₂.

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Introduction

Ceria (CeO₂) has extensive uses in the field of catalysis¹ as well as other important industrial applications.^{2–5} Platinum group metals (PGMs)⁶ and transition metals⁷ can be loaded onto a ceria support either separately, or in conjunction with other metals *e.g.* bimetallic systems. Once dispersed, the metals appear as either single particles, or atomic clusters.^{8–10} The catalytic properties of the material change as a function of the particle or cluster size. As the particle volume decreases, the surface area increases, resulting in an increase in their efficiency.¹¹ An added benefit of a reduced volume is reduced

cost.¹² Additionally, the combination of PGMs and their support can improve the oxygen storage capacity (OSC) and redox operation.^{13,14} The OSC of the ceria combined with the catalytic properties of the noble metal nanoparticles makes for a highly useful material.¹⁵ It has been suggested that the support enhances the activity of noble metal catalysis due to strong metal support interactions (SMSIs).^{16,17} There are several ways by which the SMSI effect can be explained *e.g.* formation of PGM–O–Ce bonds,¹⁸ alloy formation,¹⁹ diffusion of the PGM into the support and/or encapsulation of the PGM by the support,²⁰ and partial reduction of ceria by the PGM creating bridging hydroxyl moieties.²¹ In general, the reduction of an oxide support changes the chemical properties of the noble metals dispersed on its surface. In addition to being a reversible process,²² the reducibility of the support is improved. H₂ dissociates into atomic hydrogen by the noble metal while nearby oxygen atoms located on the support surface are removed. The localization of oxygen vacancy electrons results in the reduction of Ce(IV) to Ce(III).^{23–25} Charge transfer can occur *via* electronic interactions between the respective components in the system.^{26–29}

Chemical interactions, such as redox reactions, complicate these interactions and often influence the catalytic performance and reducibility of the loaded metal.^{30–32} Among the various PGMs, the use of Pd on ceria has been well documented

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such as in automotive exhaust catalysis,³³ steam reforming,³⁴ methanol synthesis,³⁵ abatement of methane,³⁶ C–H bond activation³⁷ and in various catalytic oxidation processes.^{38–41} In order to understand the reduction properties of palladium ions and their influence on the reactivity of a ceria support, it is necessary to study both the short and long range structures of the system and to obtain element specific information probing the supported Pd metal ions. This is accomplished by combining suitable, complimentary structural methods. This includes X-ray absorption spectroscopy (XAS), which comprises X-ray absorption near edge structure (XANES) and extended X-ray absorption fine structure (EXAFS), an element specific technique and useful to determine short-range geometric and electronic structural information. On the other hand, X-ray diffraction (XRD) is a powerful technique in determining the long-range structural order, respectively, present in a given system, but is less informative on dispersed metal ions and nano-crystalline metal particles which are present in small concentrations. Therefore, it is ideal to use a combination of these methods to probe the structure of a catalytic system to determine how the metal ions and supports dynamically interact in catalysis. Here we report the use of *in situ* Pd K-edge, Ce L₃-edge, and XRD techniques to determine the effect of the concentration of palladium on the reactivity of the Pd/CeO₂ system.

Experimental

The high-surface area ceria support was obtained from Rhodia-Solvay. The surface area of the support material was measured using BET analysis of 130 m² g^{−1}. The supported Pd catalysts were made by an incipient wetness impregnation method. The appropriate amounts of Pd nitrate solution (Johnson Matthey) were used to load palladium onto the ceria support. Materials were dried at 105 °C and calcined at 500 °C and these as-prepared catalysts were used for further *in situ* and *ex situ* characterization studies. XRD performed on the as-received samples is shown in Fig. S1 in the ESI† demonstrating phase purity and an average ceria crystallite size of approximately 5 nm and is reported in Table S1 (ESI†) and has previously been reported.⁴² ICP analysis quantifying the Pd content of the 1 wt% and 5 wt% Pd samples and the impurity content of the high surface area (HSA) ceria support is reported in Tables S2 and S3 (ESI†) respectively.

In situ XAS data of the 1 and 5 wt% Pd supported on ceria were acquired at the Ce L₃-edge (5723 eV) and Pd K-edge (24350 eV). XAS spectra were collected in step scan acquisition mode using transmission geometry at the BM26A beamline,³⁷ ESRF, equipped with a Si(111) double crystal monochromator. Measurements of all the samples were carried out in a transmission mode using ionization chambers. In a typical experiment on the Ce L₃-edge, pellets were made from 4 mg of the ceria samples mixed with 40 mg of fumed silica. On the Pd K-edge typically 100 mg of the ceria samples were used. The samples were purged under N₂ prior to exposing the catalyst in

a flow of 5% H₂/N₂. Data were obtained at room temperature followed by measurements at various temperatures during the temperature ramp from room temperature to 450 °C at 5 °C min^{−1}. The samples were then cooled in 5% H₂/N₂ to room temperature whilst data were collected at various temperatures during this process. Between the first and second cycles of H₂ treatment the samples were exposed to synthetic air at room temperature for 30 minutes. The second reduction cycle was only performed in part, heating to 100 °C in 5% H₂/N₂ at 5 °C min^{−1} on the Pd K-edge, as our aim was to monitor the reduction at the initial stages of the reaction. Data processing and analysis were performed using Athena.⁴³ Linear combination fitting (LCF) analysis of the Ce L₃-edge XANES was performed using a freshly calcined sample consisting of the bare ceria support and cerium nitrate as reference materials representing Ce(IV) and Ce(III), respectively. Similarly, LCF analysis on the Pd K-edge was performed using a Pd metal foil and PdO as reference materials.

X-ray diffraction patterns were obtained from the 11-ID-B beamline at the APS, using a 2D detector. The wavelength used was $\lambda = 0.1430$ Å with an obtainable Q range of 0.55 and 27.93 Å^{−1}. The samples were prepared using a sieve fraction between 100 and 150 µm to aid in gas flow through the sample. These were loaded into a 0.9 mm (internal diameter) fused silica capillary with a sample bed length of approximately 1 cm, and quartz wool plugs were used on either side of the sample to inhibit the movement of the sample with gas flow. Metal furnace heating elements mounted above and below the capillary were used to control the temperature.⁴⁴ All the samples were measured under a 3.5% H₂/He atmosphere during continuous heating and cooling at a rate of 10 °C min^{−1} between 30 °C and 450 °C. The samples were also held at 450 °C for 10 minutes prior to cooling. Between the first and second cycles of H₂ treatment the samples were exposed to 5% O₂/He at room temperature. XRD patterns were azimuthally integrated using FIT2D.⁴⁵ The XRD patterns were then refined using the GSAS software⁴⁶ with a batch Rietveld refinement method between 1.8 and 22° 2 θ .

Results and discussion

First, we discuss the results of temperature programmed reduction experiments and then the XAS analysis followed by XRD. In Fig. 1 the TPR profiles are reported as normalized by the integral intensity for 1 wt% Pd/CeO₂, 5 wt%Pd/CeO₂ and the high surface area CeO₂ support to highlight the temperature at which H₂ consumption occurs. The 5 wt% Pd/CeO₂ sample exhibits a maximum of H₂ uptake at approximately 65 °C, while the 1 wt% Pd/CeO₂ sample is shifted to approximately 155 °C, and HSA CeO₂ begins to show H₂ uptake only above 300 °C.

From these measurements it is clearly evidenced that the higher the content of Pd present in the sample the maximum in the H₂ consumption appears at lower temperature. However, while TPR measurements give a strong indication that the content of Pd strongly influences the temperature of reduction,



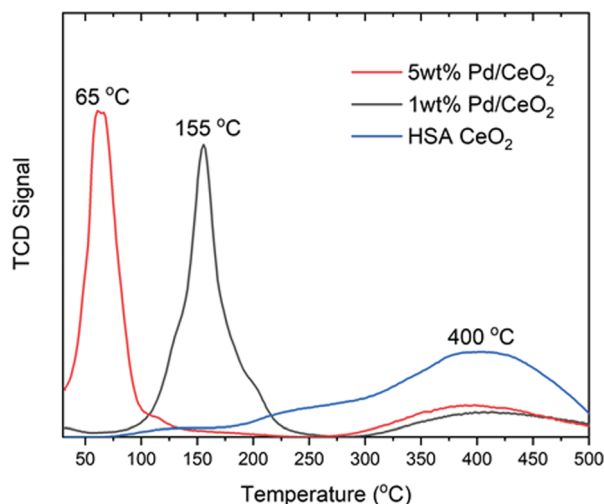


Fig. 1 TPR results from the Pd loaded ceria samples. TPR traces giving the normalized integral intensity TCD signal for 1 wt% Pd/CeO₂, 5 wt% Pd/CeO₂ and the CeO₂ support shown in black, red and blue respectively for the first cycle of reduction.

the method is insensitive to the individual components of the sample and cannot elucidate whether there is a synergistic effect between the reduction of Pd(II) to the metallic state and the formation of oxygen vacancies and reduction to Ce(III) in the CeO₂ support.

Pd K-edge XAS

To address the question of the role of Pd in promoting the reduction of CeO₂ we have employed XAS at both the Pd K-edge and Ce L₃-edge to provide detailed insight into the electronic structure changes of Pd and Ce ions along with XRD to monitor the geometric structural evolution. In Fig. 2 the Pd K-edge XANES spectra of 1 and 5 wt% Pd/CeO₂ catalysts recorded during reaction with hydrogen and heating to 450 °C, followed by cooling in a H₂/N₂ atmosphere and subsequently room temperature exposure to synthetic air, finally followed by reduction up to *ca.* 100 °C (see Fig. 2A and B) are shown. To analyse the Pd K-edge data multivariate curve resolution (MCR) was performed using an alternative least squares approach.^{47,48}

While typically analysis is performed using a linear combination fitting (LCF) method, here the nano-crystalline nature of the supported Pd leads to significant dampening of the oscillation in the post-edge region which results in a significant misfit between experimental and fitted data. MCR combats this by being able to computationally separate the pure spectral components present in a dataset consisting of multiple spectra obtained during an *in situ* experiment. Using MCR analysis it was possible to extract the significant components which, when compared to standard reference materials, can be readily identified as oxidic Pd(II) and nano-crystalline metallic Pd(0) species, see Fig. S2 (ESI[†]).

The XANES data of both the 1 wt% Pd/CeO₂ and 5wt% Pd/CeO₂ samples in their respective initial states clearly resemble that of PdO thus confirming the presence of Pd(II) in the

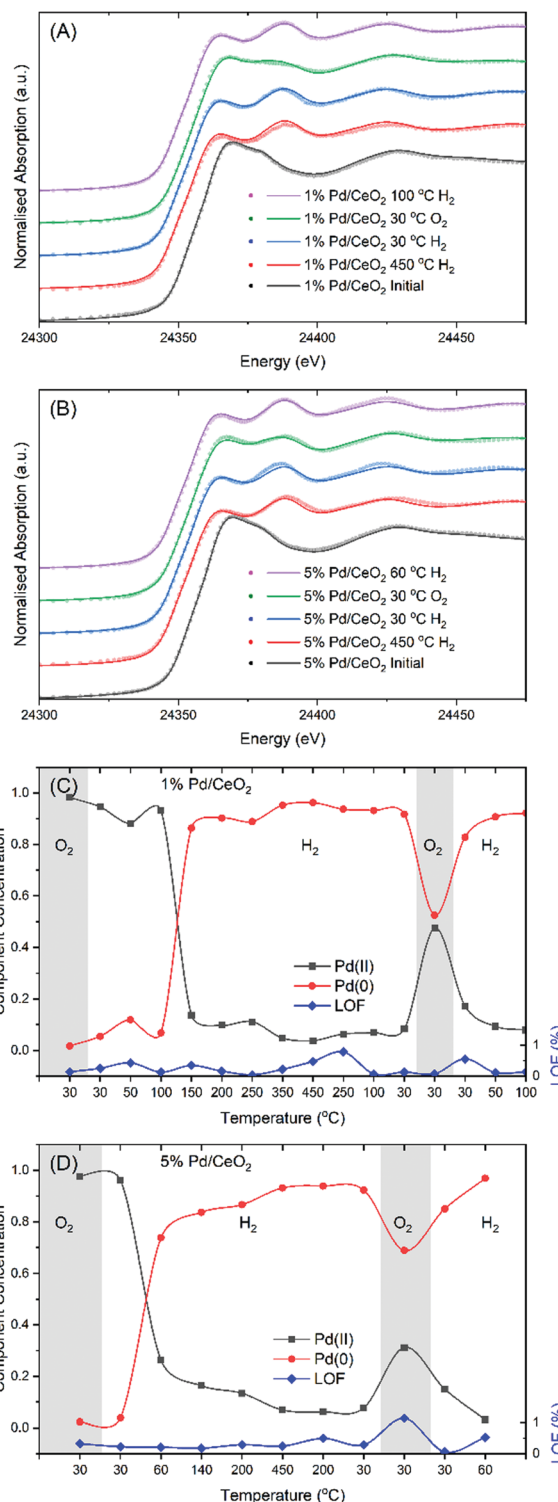


Fig. 2 Example of stacked (offset for clarity) Pd K-edge data showing the MCR analysis of the 1 wt% Pd/CeO₂ (A) and 5 wt% Pd/CeO₂ (B) samples after the initial reduction in 5% H₂/N₂ at 450 °C, cooled to 30 °C in 5% H₂/N₂, after passivation with synthetic air and after the second reduction in 5% H₂/N₂ spectra in black, red, blue, green and purple respectively. The raw data are shown as points whereas the MCR fitting is given as solid lines. The results of MCR analysis giving the proportion of oxidic (black), metallic (red) and the lack of fit (%) (blue) for the 1 wt% Pd/CeO₂ (C) and 5 wt% Pd/CeO₂ (D) samples.



as-prepared catalysts (black curves in Fig. 2A and B). Upon reduction by heating in 5% H₂/N₂, the XANES data of both 1 and 5wt% samples are similar to those of the Pd metal, both in the edge position and on the top of the edge and are interpreted as the formation of nano-crystalline Pd particles on the surface of the CeO₂ support (red curve). While at 450 °C, both samples are shown to be metallic, the reduction onset temperatures are notably different. The 1 wt% Pd/CeO₂ sample requires a temperature more than 100 °C before the Pd is reduced to a metallic state, see Fig. 2C. However, the majority of the 5wt% Pd/CeO₂ sample is reduced by 60 °C, Fig. 2D. These findings demonstrate that the reducibility of Pd is likely hindered by a greater dispersion of Pd on the CeO₂ surface.

To investigate this point further, EXAFS analysis was performed on the data collected after reduction and cooling to 30 °C, while remaining in the H₂ atmosphere. Curve fitting of the EXAFS can be used to estimate the Pd particle size through the determination of the average Pd–Pd coordination number. The results of the EXAFS fitting using Artemis⁴⁹ are given in Table 1. By using the empirically derived Hill equation,⁵⁰ coordination numbers of 5.9 and 7.8 equate to approximately 0.4 nm and 0.7 nm spherical particle size for the 1 wt% Pd and 5 wt% Pd samples respectively. The EXAFS analysis confirms the well dispersed nature of Pd in these supported samples even after reduction in hydrogen with a smaller Pd particle size obtained for 1 wt% Pd/CeO₂. Figures demonstrating the quality of fitting to the *R*- and *k*-space are given in the ESI,† Fig. S3.

After the samples were cooled to room temperature, passivation in synthetic air was performed which results in a partial oxidation of Pd(0) to Pd(II). The degree of oxidation is shown to depend on the Pd content and may be related to the metallic Pd cluster size as the 1 wt% Pd/CeO₂ sample oxidises to a greater degree than the 5 wt% Pd/CeO₂ sample. The white line intensity in Fig. 1A and B demonstrated that the two samples differ with an increased intensity observable for the 1 wt% Pd/CeO₂ sample. However, neither sample can be observed to undergo a full oxidation with respect to Pd ions, within the 30 minute exposure to synthetic air at 30 °C. From the MCR analysis reported in Fig. 1C and D it is revealed that 1 wt% Pd/CeO₂ converts to approximately 45% Pd(II), while for 5 wt% Pd/CeO₂ the degree of oxidation is only 30%. A direct overlay of the different spectra is given in supplementary Fig. S4 (ESI†) for clarity. A possible explanation for this result is that the smaller Pd particles found on 1 wt% Pd/CeO₂ have a greater surface area to volume ratio resulting in more surface atoms being exposed and readily oxidized. A second reduction step was then performed by heating in 5% H₂/N₂ with both samples showing

a rapid reduction back to metallic Pd at temperatures below 100 °C, as seen in the final state (purple curve) in Fig. 2A and B.

Ce L₃-edge XAS

Whilst XAS experiments performed at the Pd K-edge give access to the oxidation state and local coordination geometry of the Pd in the CeO₂ supported Pd samples, analysis of the Ce L₃-edge provides information on the oxidation state Ce in the CeO₂ support. In Fig. 3A and B we show the Ce L₃-edge XANES measured in the initial state, reduced at 450 °C and after cooling in 5% H₂/N₂ at 30 °C. In Fig. 3C and D we show the results of LCF analysis of the Ce L₃-edge data giving the fractions of Ce(III) during the *in situ* reduction experiment; the example fitting is shown in Fig. S5 (ESI†).

It appears that, whilst both samples show partial reduction of Ce(IV) to Ce(III), the reduction onset temperature is dependent on the Pd content in the sample. The 5 wt% Pd/CeO₂ sample shows that the maximal extent of reduction, ~15% Ce(III), is achieved below 150 °C. However, the 1wt% Pd/CeO₂ sample has an onset of reduction occurring above 150 °C with the maximum Ce(III) content being achieved only at approximately 350 °C. In our previous work,⁵¹ we were able to identify that in pure ceria the reduction process has an onset temperature > 300 °C and is temperature reversible implying a mechanism without the formation of oxygen vacancies. Based on the degree of reduction observed from the Ce L₃-edge XAS, approximately 15 mol% Ce³⁺ ions, the stoichiometry of the reduced ceria is estimated as CeO_{1.85} and is broadly in the range expected for this class of materials as reported elsewhere.¹

When considering the CeO₂ supported Pd samples, the reduction process is clearly demonstrated to be promoted by Pd to lower temperature and is temperature irreversible due to the consequence of oxygen vacancy formation. These results demonstrate that the reduction to Ce(III) is promoted by Pd and directly agrees with the Pd K-edge analysis and suggests that after reduction of the initial Pd(II), the extraction of oxygen from the ceria lattice occurs. This suggests that either reverse oxygen spill-over to the Pd ceria interface or the spill-over of hydrogen from the Pd surface drives the reduction of the ceria support. Furthermore, when compared to temperature programmed reduction experiments, shown in Fig. 1, only a single event for H₂ uptake is observed. This suggests that as soon as PdO is reduced the reduction of ceria proceeds.

In situ XRD

To further support the above presented results, experiments were conducted with X-ray diffraction. Here XRD has been analysed to determine the lattice parameter of the CeO₂ fluorite phase and where possible the evolution of the metallic Pd phase during the *in situ* reduction experiments. In Fig. 4A we show the refined CeO₂ lattice parameter from Rietveld analysis for the 1 wt% Pd/CeO₂ and 5 wt% Pd/CeO₂ samples in blue and black respectively. The temperature is denoted in the red curve and related to the right *Y* axis. Typical best fits for the Rietveld analysis are given in Fig. S6 and S7 (ESI†) for the 1 wt% Pd/CeO₂ and 5 wt% Pd/CeO₂ samples respectively showing a very strong

Table 1 EXAFS fitting results for the 1wt% Pd/CeO₂ and 5wt% Pd/CeO₂ samples after reduction in 5% H₂/N₂ and cooled to room temperature. The uncertainty on the coordination number (C.N.) is estimated as ±10% and the other uncertainties are given directly from Artemis

Sample	Scattering path	<i>R</i> (Å)	σ^2 (Å ²)	C.N.
1 wt% Pd/CeO ₂	Pd–Pd	2.78 ± 0.02	0.008 ± 0.003	5.9 ± 0.6
5 wt% Pd/CeO ₂	Pd–Pd	2.79 ± 0.02	0.009 ± 0.002	7.8 ± 0.8



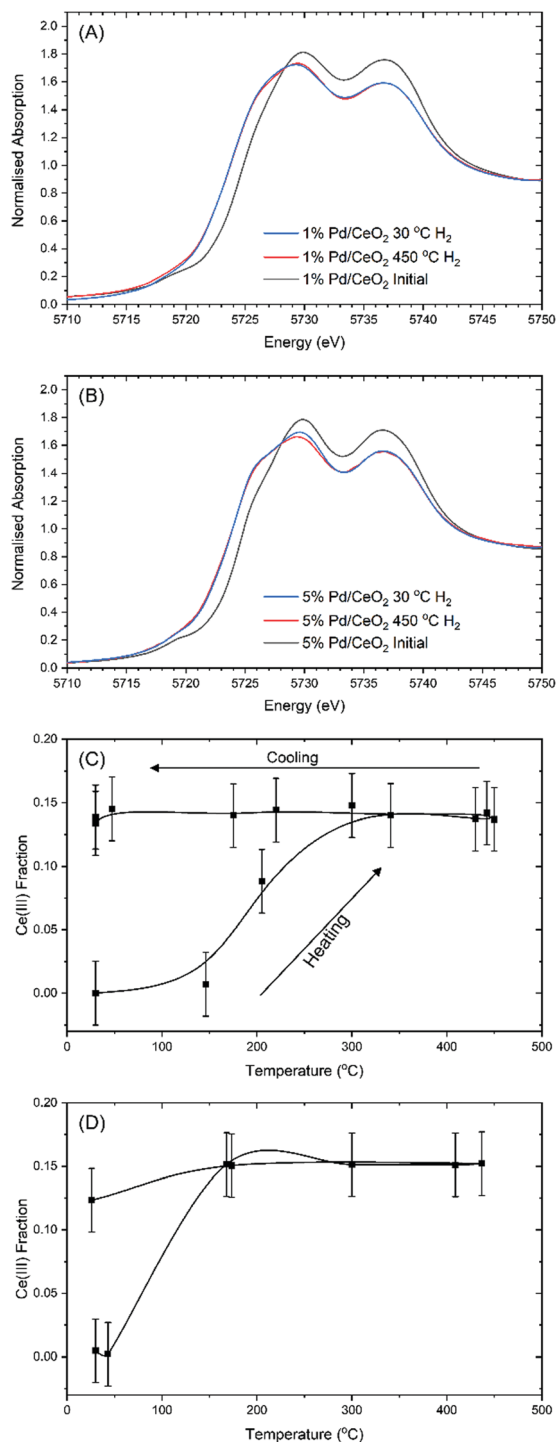


Fig. 3 Example Ce L₃-edge data from the 1 wt% Pd/CeO₂ (A), and 5 wt% Pd/CeO₂ (B) samples are shown for the initial as received material, after reduction at 450 °C, after cooling to 30 °C as black, red and blue curves respectively. The results of the linear combination fitting, represented by the fraction of Ce(III), performed using a cerium nitrate hexahydrate standard for Ce(III) and a fully oxidized high surface area ceria support material for Ce(IV) are given for 1 wt% Pd/CeO₂ (C) and 5 wt% Pd/CeO₂ (D).

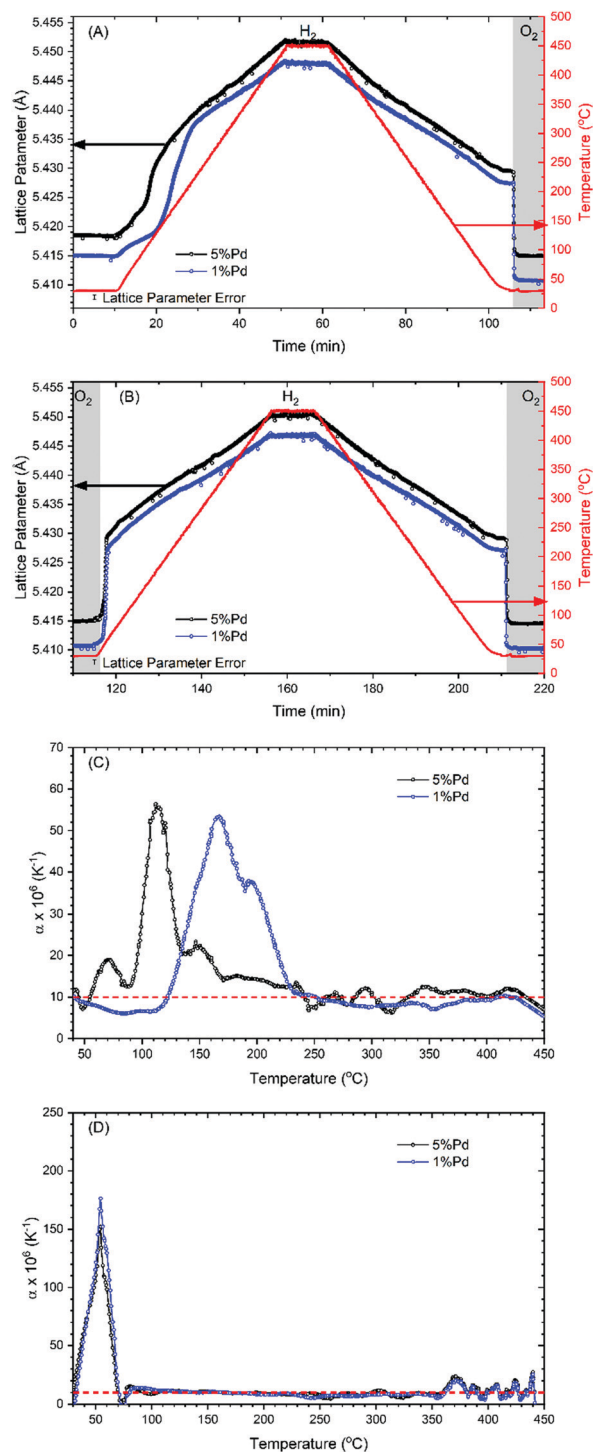


Fig. 4 Rietveld analysis of the fluorite CeO₂ phase giving the lattice parameters of 1 wt% Pd/CeO₂ and 5 wt% Pd/CeO₂ in blue and black respectively. (A) The first reduction cycle with lattice parameters on the left Y axis and temperature on the right Y axis. (B) The second reduction cycle. Note that the time in the x-axis in (B) is a continuation of the experiment reported in (A). Figures (C) and (D) give the instantaneous lattice expansion derived from the heating portion of first and second reduction cycles respectively.

agreement between the data and the fluorite CeO₂ model at all stages of the reduction experiments.

It is clear from Fig. 4A that the onset of an increase in the lattice parameter takes place above room temperature, after

admitting 3.5% H₂/N₂ into the capillary. While both samples exhibit a strong lattice expansion upon heating in H₂, the slight horizontal offset during the first reduction cycle, Fig. 4A, between the 1 wt% Pd/CeO₂ and 5 wt% Pd/CeO₂ samples evidences a difference in temperature at which the lattice expansion occurs. After the initial rapid expansion of the fluorite CeO₂ lattice, an approximately linear expansion can be seen with continuous heating up to 450 °C. The initial rapid increase in the lattice parameter is likely to be associated with the formation of Ce(III) ions, as indicated in the Ce L₃-edge XANES analysis. The formation of Ce(III) leads to an expansion of the ceria lattice due to their larger ionic radii as compared to the Ce(IV) ions.⁵² However, secondary to the expansion due to the formation of Ce(III) ions within the fluorite lattice, the linear thermal expansion also occurs. For ceria the linear thermal expansion coefficient is reported to be approximately $10 \times 10^{-6} \text{ K}^{-1}$. Upon cooling in a hydrogen atmosphere, the respective lattice parameters are observed to decrease linearly which is suggested to be due to the thermal contraction. On reaching room temperature, the respective lattice parameter values remain higher than the initial starting values suggesting an irreversible structure change, consistent with the Ce L₃-edge XAS analysis findings.

By considering the instantaneous expansion coefficient it is possible to deconvolute the two competing expansion effects and is described by:

$$\alpha(T) = \frac{1}{L} \frac{dL}{dT}$$

where L refers to the lattice parameter at room temperature, dL/dT to the change in the lattice parameter per change in temperature and $\alpha(T)$ to the expansion coefficient at temperature T . While the linear thermal expansion of ceria acts as a base line with a constant value of approximately $10 \times 10^{-6} \text{ K}^{-1}$ over the whole temperature range, the expansion due to the dynamic formation of Ce(III) results in distinct peaks at the instantaneous expansion coefficient. As such it is possible to directly extract the temperature at which the greatest rate of Ce(III) is formed and provide insight into the lattice restructuring associated with the CeO₂ reduction. Fig. 4C gives the instantaneous expansion coefficient for the 1 wt% Pd/CeO₂ and 5 wt% Pd/CeO₂ samples during the first heating cycle. Remarkably, this methodology returns curves that closely resemble those obtained from TPR measurements, shown in Fig. 1, and therefore demonstrates that the nonlinear expansion, due to the reduction of ceria, coincides with the reduction of the supported Pd particles. This method also clearly demonstrates that the temperature for the reduction, during the first reduction cycle, of ceria directly correlates with the wt% loading of Pd; higher Pd loadings lead to lower temperature reduction of the ceria support. It should also be remarked that respective Pd loaded samples show an expanded ceria lattice after cooling down in a reducing atmosphere as compared to their starting structures. The expanded final lattice provides further evidence that the reduction of ceria, promoted by Pd, is the result of a temperature irreversible process and confirms

the results obtained from the Pd K-edge and Ce L₃-edge XAS experiments.

However, when considering the second reduction cycle performed after mild passivation through room temperature reaction with air, shown in Fig. 4B, it is worth noting that the lattice parameter of CeO₂ returns to its starting value as soon as air was introduced after the first cycle of reduction, suggesting a complete reoxidation of reduced Ce(III) at this stage. Upon re-introducing 3.5% H₂/N₂ after the reoxidation, both 1% and 5% samples exhibit a near room temperature partial reduction of Ce(IV) to Ce(III). The respective lattice parameters rapidly increase to almost the same value observed for their first cycle, at a temperature well below 100 °C. Subsequent increases in temperature linearly increase the lattice parameter similar to that observed for the first cycle of reduction. The instantaneous expansion coefficient clearly shows that an inflection (see Fig. 4D) in the ceria lattice parameter is observed at approximately 50 °C for both the 1 wt% and 5 wt% loadings of Pd. When considering the instantaneous lattice expansion coefficient this process can be observed to occur rapidly resulting in an instantaneous expansion coefficient maximum of approximately $250 \times 10^{-6} \text{ K}^{-1}$. This confirms the previously discussed results from the Pd K-edge XAS measurements, and the mild passivation of the Pd by room temperature oxidation can be readily reduced and thus can promote the reduction of ceria.

After close inspection of the XRD patterns for the 5 wt% Pd/CeO₂ sample a very weak reflection associated with the (111) reflection of metallic Pd can be seen at 2θ of approximately 3.65° . The formation of the metallic Pd phase is evidenced in the colourmap given in Fig. 5A showing a slight increase in intensity (on a logarithmic scale) with a change from dark blue to light blue colour. To extract information on the lattice parameter of the metallic Pd from the (111) reflection a custom peak fitting tool was written in python. At the start of the experiment the Pd was noted as being oxidic Pd(II) from XAS measurements and therefore no metallic Pd is expected to be present allowing for the baseline correction to be achieved through subtraction of the first dataset corresponding to the initial starting material. Fig. S8 (ESI†) gives the surface colour map of the baseline corrected data which were used for further analysis. Examples of the quality of the peak fitting are given in Fig. S9 (ESI†). Attempts to also perform the same analysis on 1 wt% Pd/CeO₂ were made; however, no peak related to the Pd(111) reflection could be clearly detected as a consequence of the lower Pd content and expected lower crystallinity. The colour map for the 1 wt% Pd/CeO₂ sample is given in supplementary Fig. S10 (ESI†).

The baseline corrected data for the 5 wt% Pd/CeO₂ sample were used for sequential fitting with a single Gaussian peak to model the position and area of the peak giving insight directly into the Pd lattice parameter evolution and relative crystallinity throughout. The results of the Gaussian peak fitting are shown in Fig. 5B for the first and second reduction cycles. On first inspection the formation of crystalline Pd⁰ was found to occur above approximately 100 °C with a rapid increase in the peak area occurring during the initial phase of heating. Given that



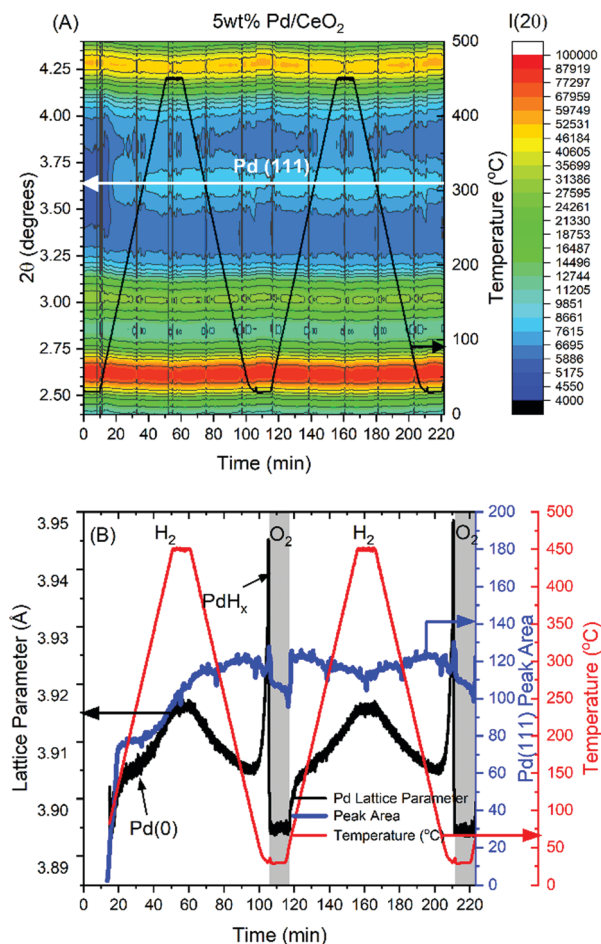


Fig. 5 (A) Surface colourmap illustrating selected XRD data collected on the 5% Pd/CeO₂ sample around the Pd(111) reflection region. Temperature is indicated with the black trace associated with the right Y axis. (B) The results of the Gaussian peak fitting to the Pd(111) reflection yielding the Pd lattice parameter and peak area in black and blue respectively. The temperature is given as the red trace associated with the second left Y axis.

XRD analysis is only sensitive to the long range structure, the initial reduction to a disordered Pd may be missed and could explain the temperature inconsistency between XAS which showed almost full Pd⁰ at approximately 60 °C and the XRD analysis which reveals crystalline Pd⁰ formation at around 100 °C.

With further heating of the sample, the Pd cubic lattice parameter is observed to increase with a maximum of 3.918 Å, in line with the expected lattice parameter taking into account thermal expansion. Concurrent to this, the relative crystallinity, observed from the peak area shown in Fig. 5B in blue, is observed to increase suggesting a partial sintering of the metallic Pd phase during heating. During cooling the lattice parameter is noted to decrease until around 50 °C before a rapid and substantial increase during further cooling to room temperature. This expansion is due to the formation of a PdH_x phase known to occur when Pd is treated under a hydrogen containing atmosphere at low temperature. Upon exposure to oxygen at room temperature the PdH_x phase is removed and the

Pd lattice parameter relaxes to 3.896 Å. In the Pd K-edge XAS spectra shown in Fig. 2 the exposure to oxygen leads to a partial oxidation to Pd(II) and from the XRD analysis it is found that this process is concurrent with only a very minor decrease in the Pd(111) reflection peak area. This result evidences that the passivation is only a surface oxidation process with the core remaining metallic. During the second reduction cycle, the lost intensity of the Pd(111) reflection is rapidly recovered suggesting that the surface PdO species is reduced as soon as hydrogen is reintroduced into the sample, in line with the results obtained from the Pd K-edge XAS.

Conclusions

In summary, combined *in situ* multi-edge XAS and X-ray scattering studies enabled us to determine the effect of palladium loading on a high-surface area support on the reactivity of both Pd(II) and Ce(IV) ions. The results clearly indicate that there is a promotion of the partial reduction of ceria due to the presence of Pd. The temperature at which the promoted reduction temperature of the ceria is also noted to inversely depend on the wt% loading of the Pd onto the ceria support; a higher loading of Pd leads to a lower reduction temperature of the Pd and the ceria support. This finding could be attributed to the strong interaction of metal ions with the support preventing the reduction of the initial PdO to metallic Pd. The promotion of the CeO₂ reduction is interpreted as the extraction of oxygen from the ceria lattice and is suggested to be due to a hydrogen spill over mechanism or reverse oxygen spill over mechanism.

More importantly, the findings obtained from the Pd K-edge XAS and XRD studies clearly demonstrate that passivation in air at room temperature only partially oxidises the supported Pd while a complete reoxidation of the reduced ceria (CeO_{1.85}) is observed. Based on this ceria lattice parameter change, we conclude that the restoration of the full stoichiometric fluorite phase CeO₂ takes place. Furthermore, the second reduction cycle, observed by XRD, demonstrates that the reduction of ceria, observed indirectly by analysis of the lattice parameter, is promoted to near room temperature irrespective of the Pd wt% loading. The Pd K-edge data corroborate this result showing that the Pd also undergoes near room temperature reduction by hydrogen following the mild passivation irrespective of the Pd wt% loading. These results indicate that with an initial pre-treatment cycle and subsequent passivation, the promoted reduction of ceria can be reduced to near room temperature without the requirement of high Pd wt% loadings and may have a direct impact on the relevant fields of catalysis where these classes of materials are currently utilised.

Author contributions

AHC and HRM performed the experiments, analysis, interpretation and manuscript drafting. DT and JF provided the samples used in the study. AL and KB optimised the beamlines for the experiments performed at ESRF and APS respectively and



provided user support throughout. TIH and GS contributed to the drafting of the manuscript, interpretation of results and supervision of both AHC and HRM.

Conflicts of interest

The authors do not have any conflict of interest to declare.

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Notes and references

- 1 A. Trovarelli, *Catalysis by Ceria and Related Materials*, Imperial College Press, London, 2002, vol. 2.
- 2 R. M. Heck and R. J. Farrauto, *Appl. Catal., A*, 2001, **221**, 443–457.
- 3 R. Craciun, B. Shereck and R. J. Gorte, *Catal. Lett.*, 1998, **51**, 149–153.
- 4 P. Pantu, K. Kim and G. R. Gavalas, *Appl. Catal., A*, 2000, **193**, 203–214.
- 5 Y. I. Matatov-Meytal and M. Sheintuch, *Ind. Eng. Chem. Res.*, 1998, **37**, 309–326.
- 6 H. Renner, G. Schlamp, I. Kleinwächter, E. Drost, H. M. Lüscho, P. Tews, P. Panster, M. Diehl, J. Lang, T. Kreuzer, A. Knödler, K. A. Starz, K. Dermann, J. Rothaut, R. Drieselmann, C. Peter and R. Schiele, *Ullmann's Encyclopedia of Industrial Chemistry*, Wiley-VCH Verlag GmbH & Co. KGaA, 2001.
- 7 D. Astruc, *Nanoparticles and Catalysis*, Wiley-VCH Verlag GmbH & Co. KGaA, 2008, pp. 1–48.
- 8 A. Neitzel, A. Figueroba, Y. Lykhach, T. Skála, M. Vorokhta, N. Tsud, S. Mehl, K. Ševčíková, K. C. Prince, K. M. Neyman, V. Matolín and J. Libuda, *J. Phys. Chem. C*, 2016, **120**, 9852–9862.
- 9 N. Acerbi, S. Golunski, S. C. Tsang, H. Daly, C. Hardacre, R. Smith and P. Collier, *J. Phys. Chem. C*, 2012, **116**, 13569–13583.
- 10 J. Zhou, A. P. Baddorf, D. R. Mullins and S. H. Overbury, *J. Phys. Chem. C*, 2008, **112**, 9336–9345.
- 11 M. E. Dry, *Catal. Today*, 2002, **71**, 227–241.
- 12 J. A. Rabó, *Catal. Today*, 1994, **22**, 201–233.
- 13 L. F. Liotta, A. Longo, A. Macaluso, A. Martorana, G. Pantaleo, A. M. Venezia and G. Deganello, *Appl. Catal., B*, 2004, **48**, 133–149.
- 14 L. F. Liotta, A. Longo, G. Pantaleo, G. Di Carlo, A. Martorana, S. Cimino, G. Russo and G. Deganello, *Appl. Catal., B*, 2009, **90**, 470–477.
- 15 H. Asakura, S. Hosokawa, K. Beppu, K. Tamai, J. Ohyama, T. Shishido, K. Kato, K. Teramura and T. Tanaka, *Catal. Sci. Technol.*, 2021, **11**, 6182–6190.
- 16 J. Graciani, A. B. Vidal, J. A. Rodriguez and J. F. Sanz, *J. Phys. Chem. C*, 2014, **118**, 26931–26938.
- 17 M. Ahmadi, H. Mistry and B. Roldan Cuenya, *J. Phys. Chem. Lett.*, 2016, **7**, 3519–3533.
- 18 H. Hirata, K. Kishita, Y. Nagai, K. Dohmae, H. Shinjoh and S. Matsumoto, *Catal. Today*, 2011, **164**, 467–473.
- 19 S. Bernal, J. J. Calvino, M. A. Cauqui, J. M. Gatica, C. Larese, J. A. Pérez Omil and J. M. Pintado, *Catal. Today*, 1999, **50**, 175–206.
- 20 S. Suhonen, M. Valden, M. Hietikko, R. Laitinen, A. Savimäki and M. Härkönen, *Appl. Catal., A*, 2001, **218**, 151–160.
- 21 G. Jacobs, U. M. Graham, E. Chenu, P. M. Patterson, A. Dozier and B. H. Davis, *J. Catal.*, 2005, **229**, 499–512.
- 22 S. J. Tauster, S. C. Fung and R. L. Garten, *J. Am. Chem. Soc.*, 1978, **100**, 170–175.
- 23 O. V. Safonova, A. A. Guda, C. Paun, N. Smolentsev, P. M. Abdala, G. Smolentsev, M. Nachtegaal, J. Szlachetko, M. A. Soldatov, A. V. Soldatov and J. A. Van Bokhoven, *J. Phys. Chem. C*, 2014, **118**, 1974–1982.
- 24 C. Loschen, S. T. Bromley, K. M. Neyman and F. Illas, *J. Phys. Chem. C*, 2007, **111**, 10142–10145.
- 25 T. Baidya, A. Gayen, M. S. Hegde, N. Ravishankar and L. Dupont, *J. Phys. Chem. B*, 2006, **110**, 5262–5272.
- 26 C. T. Campbell, *Nat. Chem.*, 2012, **4**, 597–598.
- 27 G. N. Vayssilov, Y. Lykhach, A. Migani, T. Staudt, G. P. Petrova, N. Tsud, T. Skála, A. Bruix, F. Illas, K. C. Prince, V. Matolín, K. M. Neyman and J. Libuda, *Nat. Mater.*, 2011, **10**, 310–315.
- 28 Y. Lykhach, S. M. Kozlov, T. Skála, A. Tovt, V. Stetsovych, N. Tsud, F. Dvořák, V. Johánek, A. Neitzel, J. Mysliveček, S. Fabris, V. Matolín, K. M. Neyman and J. Libuda, *Nat. Mater.*, 2016, **15**, 284–288.
- 29 D. O. Scanlon, B. J. Morgan and G. W. Watson, *Phys. Chem. Chem. Phys.*, 2011, **13**, 4279–4284.
- 30 S. Golunski and A. Walker, *Chem. Commun.*, 2000, 1593–1594.
- 31 G. Sankar, C. N. R. Rao and T. Rayment, *J. Mater. Chem.*, 1991, **1**, 299–300.
- 32 C. M. Y. Yeung and S. C. Tsang, *J. Phys. Chem. C*, 2009, **113**, 6074–6087.
- 33 J. Lin, L. Yang, T. Wang and R. Zhou, *Phys. Chem. Chem. Phys.*, 2017, **19**, 7844–7852.
- 34 R. Craciun, W. Daniell and H. Knözinger, *Appl. Catal., A*, 2002, **230**, 153–168.
- 35 N. Tsubaki and K. Fujimoto, *Top. Catal.*, 2003, **22**, 325–335.
- 36 J. Ma, Y. Lou, Y. Cai, Z. Zhao, L. Wang, W. Zhan, Y. Guo and Y. Guo, *Catal. Sci. Technol.*, 2018, **8**, 2567–2577.
- 37 L. M. Misch, J. A. Kurzman, A. R. Derk, Y. Il Kim, R. Seshadri, H. Metiu, E. W. McFarland and G. D. Stucky, *Chem. Mater.*, 2011, **23**, 5432–5439.
- 38 M. Danielis, S. Colussi, C. De Leitenburg, L. Soler, J. Llorca and A. Trovarelli, *Catal. Sci. Technol.*, 2019, **9**, 4232–4238.



- 39 E. M. Slavinskaya, T. Y. Kardash, O. A. Stonkus, R. V. Gulyaev, I. N. Lapin, V. A. Svetlichnyi and A. I. Boronin, *Catal. Sci. Technol.*, 2016, **6**, 6650–6666.
- 40 Z. Hu, X. Liu, D. Meng, Y. Guo, Y. Guo and G. Lu, *ACS Catal.*, 2016, **6**, 2265–2279.
- 41 S. Roy and M. S. Hegde, *Catal. Commun.*, 2008, **9**, 811–815.
- 42 H. R. Marchbank, A. H. Clark, T. I. Hyde, H. Y. Playford, M. G. Tucker, D. Thompsett, J. M. Fisher, K. W. Chapman, K. A. Beyer, M. Monte, A. Longo and G. Sankar, *Chem-PhysChem*, 2016, **17**, 3494–3503.
- 43 D. S. Mannel, M. S. Ahmed, T. W. Root and S. S. Stahl, *J. Am. Chem. Soc.*, 2017, **139**, 1690–1698.
- 44 P. J. Chupas, K. W. Chapman, C. Kurtz, J. C. Hanson, P. L. Lee and C. P. Grey, *J. Appl. Crystallogr.*, 2008, **41**, 822–824.
- 45 A. P. Hammersley, S. O. Svensson, M. Hanfland, A. N. Fitch and D. Häusermann, *High Press. Res.*, 1996, **14**, 235–248.
- 46 B. H. Toby, *J. Appl. Crystallogr.*, 2001, **34**, 210–213.
- 47 A. Voronov, A. Urakawa, W. van Beek, N. E. Tsakoumis, H. Emerich and M. Rønning, *Anal. Chim. Acta*, 2014, **840**, 20–27.
- 48 A. De Juan, J. Jaumot and R. Tauler, *Anal. Methods*, 2014, **6**, 4964–4976.
- 49 B. Ravel and M. Newville, *J. Synchrotron Radiat.*, 2005, **12**, 537–541.
- 50 A. M. Beale and B. M. Weckhuysen, *Phys. Chem. Chem. Phys.*, 2010, **12**, 5562–5574.
- 51 A. H. Clark, K. A. Beyer, S. Hayama, T. I. Hyde and G. Sankar, *Chem. Mater.*, 2019, **31**, 7744–7751.
- 52 R. K. Hailstone, A. G. DiFrancesco, J. G. Leong, T. D. Allston and K. J. Reed, *J. Phys. Chem. C*, 2009, **113**, 15155–15159.

