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Boosting $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ cathode stability using a concentrated aqueous electrolyte for high-voltage zinc batteries†

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We demonstrate that the capacity decay and voltage drop issues of the $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ cathode are significantly addressed by using a concentrated aqueous electrolyte based on Zn and Li salts. The resultant aqueous Zn// $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ battery achieves a high output voltage of 1.75 V and a long lifespan with 82.3% capacity retention over 2000 cycles. Joint structural and spectroscopic characterizations reveal that this battery operates through Li^+ (de)intercalation into the cathode along with Zn^{2+} plating/stripping at the anode.

Rechargeable aqueous Zn-based batteries (RAZBs) are promising for large-scale energy storage because of the advantages of the metallic Zn anode, including abundant resources, low cost, environmental benignancy, and high theoretical gravimetric and volumetric capacity (820 mA h g^{-1} and $5855 \text{ mA h cm}^{-3}$).¹ Moreover, aqueous electrolytes intrinsically offer high safety and their excellent ionic conductivity favors high-rate capability.² Cathode materials have been regarded as a critical component that govern the energy density and lifespan of batteries. Currently proposed cathodes for RAZBs generally exhibit limited average discharge voltage (e.g., MnO_2 polymorphs $\sim 1.35 \text{ V}$,³ vanadium oxides $\sim 0.85 \text{ V}$,⁴ and organic compounds $\sim 1.1 \text{ V}$ ⁵ (vs. Zn^{2+}/Zn)) or poor cycling stability.

Polyanion-type phosphate of $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ (LVP) features a high working voltage ($\sim 4.0 \text{ V}$ vs. Li^+/Li ($\sim 1.8 \text{ V}$ vs. Zn^{2+}/Zn)) and a robust crystal architecture enabling fast ion (de)intercalation, and has been widely employed as a cathode for nonaqueous Li-ion batteries.⁶ Chen *et al.* explored the electrochemical behaviour of an aqueous battery constructed by an

LVP cathode and Zn anode in $1 \text{ M Li}_2\text{SO}_4\text{-ZnSO}_4$ electrolyte, showing the feasibility of LVP application in RAZBs.⁷ It should be noted that polyanion-type phosphates in aqueous media often suffer from serious dissolution of active materials,⁸ leading to a short lifespan and voltage drop during cycling. In addition, the traditional aqueous electrolytes (concentration generally below 2 mol L^{-1}) cannot support the stable operation of high-voltage cathodes, due to the parasitic O_2 evolution.^{6a,9} Therefore, it is desirable to improve the stability and reversibility of the LVP cathode for RAZBs, but it remains unsolved.

Here, we tackle the capacity decay and voltage drop issues of the LVP cathode using a formulated electrolyte composed of 1 m zinc trifluoromethanesulfonate ($\text{Zn}(\text{OTf})_2$) and 15 m lithium bis(trifluoromethanesulfonyl)imide (LiTFSI) in water (m , mol kg^{-1}). This concentrated electrolyte can suppress the LVP dissolution and water-induced side reactions. As a result, a high output voltage of 1.75 V , a considerable energy density of $186.3 \text{ W h kg}_{\text{cathode}}^{-1}$, and a long-term stability with 82.3% capacity retention after 2000 cycles are characterized, which significantly stand out among those of the reported phosphate-based cathodes for RAZBs.

Fig. 1a presents the XRD Rietveld refinement of the as-prepared LVP. All of the diffraction peaks can be indexed to the monoclinic space group of $P2_1/n$ and a good agreement between the experimental data and calculated result is achieved ($R_{\text{wp}} = 4.92\%$ and $R_p = 3.85\%$). The refined lattice unit-cell parameters of $a = 8.6200 \text{ \AA}$, $b = 8.6080 \text{ \AA}$, $c = 12.0541 \text{ \AA}$, and $V = 894.3950 \text{ \AA}^3$ match well with those in previous reports.¹⁰ Fig. 1b schematically illustrates the crystal structure of LVP, which features a three-dimensional framework of VO_6 octahedra and PO_4 tetrahedra sharing O vertices and Li ions located in the interstitial space. As shown in the scanning electron microscopy (SEM) image (Fig. 1c), the as-prepared LVP/C composite has a nanoparticulate morphology and the particle size is in the range of $50\text{--}100 \text{ nm}$. The transmission electron microscopy (TEM) image further demonstrates that the LVP nanograins are uniformly and firmly confined in the carbon

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Fig. 1 (a) Rietveld refined XRD pattern of the as-prepared LVP. (b) Schematic illustration of the LVP crystal structure. (c) SEM image. (d) TEM and (e) HRTEM images, with the inset presenting the corresponding FFT pattern. (f) STEM image with elemental mapping images.

matrix (Fig. 1d). In the high-resolution TEM (HRTEM) image (Fig. 1e), the measured interplanar distance of 0.43 nm corresponds to the (020) plane of the monoclinic LVP. The crystalline particles are finely coated with an amorphous carbon shell. The Raman spectrum (Fig. S1, ESI†) shows two characteristic peaks at 1362 and 1581 cm^{-1} related to the defect-induced (D) band and graphitic-induced (G) band, respectively. The peak intensity ratio of the D to G band (I_D/I_G) is 0.9, suggesting a relatively high degree of graphitization that favours the electronic conductivity.^{10b} The carbon content is determined to be 10.8% according to the thermogravimetric analysis (Fig. S2, ESI†). The scanning transmission electron microscopy (STEM) with elemental mapping images (Fig. 1f) confirm the uniform distribution of elements in the as-prepared composite.

The electrochemical stability and reversibility of LVP cathodes in different aqueous electrolytes (*i.e.*, 1 m Zn(OTf)₂ (1 m Zn), 1 m Zn(OTf)₂ + 5 m LiTFSI (1 m Zn + 5 m Li), 1 m Zn(OTf)₂ + 10 m LiTFSI (1 m Zn + 10 m Li), and 1 m Zn(OTf)₂ + 15 m LiTFSI (1 m Zn + 15 m Li)) have been studied. Although the ionic conductivity of electrolytes gradually decreases with increasing salt concentration, a considerable conductivity of 14.9 mS cm^{-1} is characterized in 1 m Zn + 15 m Li (Fig. S3, ESI†). Fig. 2a–c display the cyclic voltammetry (CV) curves of LVP electrodes in different electrolytes at 0.2 mV s^{-1} . With the increase of LiTFSI content, the reversibility of the LVP cathode is significantly improved. Three stable pairs of redox peaks corresponding to the stepwise Li^+ extraction/insertion from/into the LVP structure have been observed in 1 m Zn + 15 m Li electrolyte (Fig. 2a), suggesting that this concentrated electrolyte can effectively inhibit the LVP dissolution and suppress the water-induced side reactions. In sharp contrast, the dilute 1 m Zn (Fig. 2c) and 1 m Zn + 5 m Li (Fig. 2b) electrolytes cannot support the stable operation of LVP, showing a rapid peak

Fig. 2 (a–c) CV profiles and (d–f) typical charge/discharge curves of LVP cathodes in (a and d) 1 m Zn + 15 m Li, (b and e) 1 m Zn + 5 m Li, and (c and f) 1 m Zn electrolytes. (g) Cycling stability of LVP cathodes in different electrolytes at 200 mA g^{-1} . (h) Long-term cycling performance of the LVP cathode in 1 m Zn + 15 m Li at 1000 mA g^{-1} . (i) Raman spectra of different electrolytes (O–H stretching vibration). (j) Optical images of LVP electrodes immersed in different electrolytes after 10 days.

current decay and an obvious O_2 evolution reaction above 2.0 V (*vs.* Zn^{2+}/Zn). The 1 m Zn + 10 m Li electrolyte moderately improves the stability of LVP with a slight decrease of the redox peaks upon cycling (Fig. S4, ESI†).

Fig. 2d–f present the typical charge/discharge profiles of LVP cathodes at 200 mA g^{-1} within the voltage window of 0.6–2.1 V (*vs.* Zn^{2+}/Zn). In 1 m Zn + 15 m Li electrolyte, the voltage profiles are well overlapped and a reversible capacity of 126.3 mA h g^{-1} at the 50th cycle is achieved. The three discharge platforms (1.75, 1.35, and 1.25 V) are consistent with the CV curves. Voltage profiles of LVP cathodes in 1 m Zn + 5 m Li (Fig. 2e) and 1 m Zn + 10 m Li (Fig. S5, ESI†) electrolytes suggest a better performance than that in 1 m Zn (Fig. 2d) but an inferior stability compared with the 1 m Zn + 15 m Li system. Fig. 2g displays the cycling performance of LVP cathodes in different aqueous electrolytes at 200 mA g^{-1} . Impressively, the 1 m Zn + 15 m Li system enables the highest cycling stability with a reversible capacity of 126.7 mA h g^{-1} after 200 cycles without obvious decay. Moreover, the Coulombic efficiency (CE) can reach a high value of 99.8%. For comparison, the 1 m Zn + 5 m Li and 1 m Zn + 10 m Li counterparts exhibit much lower CE (Fig. S6, ESI†) and inferior capacity retentions of 76.1% after 100 cycles and 81.2% after 150 cycles, respectively. As expected, a shorter lifespan is observed in the neat 1 m Zn electrolyte. Thereafter, the long-term cycling stability of LVP in 1 m Zn + 15 m Li was evaluated at 1000 mA g^{-1} (Fig. 2h). The initial capacity increase is mainly due to the electrode activation process as identified by the reduced charge-transfer resistance during cycling (Fig. S7, ESI†). After 2000 cycles, a reversible capacity of 89.7 mA h g^{-1} with 82.3% capacity retention and $\sim 100\%$ CE is achieved, indicating the feasibility of this battery system for practical applications.

Fig. 2i shows the Raman spectra of the hybrid Zn + Li electrolytes. The O–H stretching vibration of water molecules

(2800–3700 cm^{-1}) can be deconvoluted into three components located at around 3115.5 (peak 1), 3366.1 (peak 2), and 3585.8 (peak 3) cm^{-1} , corresponding to the strong, weak, and non H-bonds, respectively.^{5d} With the increase of salt concentration, these H-bond signals experience blueshift and gradually weaken, indicating the decrease of water activity and the disruption of the H_2O network connected by H-bonds. Similar evolution of the H_2O signal has been confirmed by the Fourier transformed infrared (FTIR) spectra (Fig. S8, ESI†). The reduced water activity in the concentrated electrolyte helps to expand the electrochemical window with much reduced water-induced side reactions (Fig. S9, ESI†) and inhibit the dissolution of active materials. To intuitively identify the solubility of LVP, a static soaking experiment was conducted by loading LVP electrodes into different solutions (Fig. 2j). The 1 m Zn + 15 m Li media can remain colorless and transparent even after 10 days, but the solution colors in the 1 m Zn and 1 m Zn + 5 m Li counterparts turn deep yellow and light yellow, respectively, caused by the serious dissolution of LVP. In addition, the formulated 1 m Zn + 15 m Li electrolyte supports a good reversibility of a Zn anode (Fig. S10, ESI†), which contributes to the stable operation of Zn//LVP batteries.

The rate performance of LVP in 1 m Zn + 15 m Li is evaluated by progressively increasing the current densities from 200 to 2000 mA g^{-1} (Fig. 3a). Reversible capacities of 124.2, 120.5, 116.6, 111.2 and 107.6 mA h g^{-1} are delivered at rates of 300, 500, 800, 1000 and 1500 mA g^{-1} , respectively. A high capacity of 100.5 mA h g^{-1} is achieved at 2000 mA g^{-1} . An average capacity of 119.2 mA h g^{-1} recovers as the rate stepwise returns to 200 mA g^{-1} . The typical voltage profiles (Fig. 3b) display an

average output voltage of ~ 1.5 V, corresponding to energy densities of 186.3 $\text{W h kg}_{\text{cathode}}^{-1}$ at 450 W kg^{-1} and 150.7 $\text{W h kg}_{\text{cathode}}^{-1}$ at 3000 W kg^{-1} . Meanwhile, the assembled aqueous battery achieves an energy density of 143.1 W h kg^{-1} at 346.1 W kg^{-1} based on the mass of LVP cathode and 200% Zn anode. The electrode process kinetics were further studied by CV (Fig. 3c). The CV profiles maintain similar shapes with tiny shift as the scan rate increases from 0.2 to 1.2 mV s^{-1} , demonstrating a good stability. According to the relation of $i = av^b$ (another type, $\log(i) = b\log(v) + \log(a)$),¹¹ the b values of the peaks O1, O2, O3, R1, R2, and R3 (marked in Fig. 3c) are determined to be 0.66, 0.65, 0.47, 0.66, 0.56, and 0.40 respectively (Fig. S11, ESI†). This demonstrates that a combination of diffusion and capacitive behaviors synergistically manages the charge-storage process of LVP, accounting for the high-rate capability. As calculated, a 56.5% fraction of the total charge is arising from the pseudocapacitive contribution (Fig. 3d, the calculation method is provided in the ESI†), which is comparable with other V-based cathodes.^{4a,11b,12} In addition, according to the galvanostatic intermittent titration technique (GITT, Fig. 3e and Fig. S12, ESI†), the ion diffusion coefficients range from 10^{-10} to 10^{-11} $\text{cm}^2 \text{s}^{-1}$, indicating the fast reaction kinetics.

The reaction mechanism of the LVP cathode in the hybrid 1 m Zn + 15 m Li aqueous electrolyte has been elucidated by a combination study of XRD, UV-visible (UV-vis) spectroscopy, X-ray photoelectron spectroscopy (XPS), and TEM analyses. Fig. 4a shows the initial two voltage profiles of LVP at 100 mA g^{-1} , where the marked states (points A–I) were collected for the *ex situ* XRD and UV-vis measurements. Except for the signal of the Ti foil current collector, the characteristic (020), (210), (121), ($\bar{1}21$), and (220) peaks of LVP are highly reversible during charge/discharge (Fig. 4b), ascribed to the Li^+

Fig. 3 (a) Rate performance and (b) corresponding voltage profiles of the LVP cathode in 1 m Zn + 15 m Li electrolyte. (c) CV curves and (d) typical capacitive contribution at 0.6 mV s^{-1} . (e) GITT profiles and (f) corresponding ion diffusion coefficient.

Fig. 4 (a) Voltage profiles during the initial two cycles. (b) XRD patterns and (c) UV-vis spectra at selected states (points A–I marked in (a)). XPS spectra of (d) V 2p and (e) Zn 2p regions. (f) Schematic illustration of the Zn//1 m Zn + 15 m Li/LVP battery chemistry.

extraction/insertion process. This XRD signal evolution of LVP is similar to the observation in the non-aqueous Li-based batteries.^{6b,10a} The UV-vis spectra (Fig. 4c) record the evolution of the V oxidation states with the references of V_2O_5 (V^{5+}), $VOSO_4$ (V^{4+}), and VCl_3 (V^{3+}). The pristine electrode features a typical absorption of V^{3+} with broad bands at around 440, 600 and 770 cm^{-1} . Upon charging ($A \rightarrow C$ and $E \rightarrow G$), the V^{4+} component intensifies along with the V^{3+} wane. At the fully charged state, a characteristic band of V^{4+} is detected, corresponding to the two- Li^+ extraction from LVP. The discharge process ($C \rightarrow E$ and $G \rightarrow I$) can revert the oxidation state of V to trivalence.

Fig. 4d and e show the variation of the V 2p and Zn 2p XPS regions, respectively. The V 2p_{3/2} (V 2p_{1/2}) XPS peak shifts from the pristine location of 516.8 (524.1) eV to 517.6 (524.9) eV at the fully charged state, resulting from the oxidation process from V^{3+} to V^{4+} .^{8c} After fully discharging, these V 2p peaks can recover to the pristine state. For Zn 2p spectra, no obvious Zn signal can be detected in the fully charged or discharged electrodes. This verifies that the cathode capacity comes from the Li^+ intercalation with a negligible contribution from the Zn^{2+} intercalation. In addition, HRTEM images confirm the reversible contraction/expansion of the (020) plane of LVP caused by the Li^+ extraction/insertion (Fig. S13, ESI†). STEM with the corresponding element mapping images reveal negligible Zn content in the discharged electrode (Fig. S13, ESI†), excluding the Zn^{2+} co-intercalation. According to the aforementioned results, the Zn//1 m Zn + 15 m Li/LVP battery chemistry operates through the reversible Li^+ extraction/insertion from/into the LVP cathode and the Zn^{2+} electrochemical plating/stripping at the anode during charge/discharge (Fig. 4f).

In conclusion, we report a high-voltage and long-life LVP cathode for aqueous Zn-based batteries. The issues of capacity decay and voltage drop facing LVP are effectively addressed by the formulated 1 m Zn + 15 m Li electrolyte. The resultant LVP cathode exhibits a high output voltage of 1.75 V and a superior capacity retention of 82.3% after 2000 cycles. This Zn//LVP battery chemistry experiences reversible Li^+ (de)intercalation into the polyanionic cathode along with Zn^{2+} plating/stripping at the anode during cycling. This work will inspire the design of efficient electrodes and electrolytes for rechargeable Zn-based batteries.

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Conflicts of interest

There are no conflicts to declare.

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