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Chromium-free Cu@Mg/ γ -Al₂O₃ – an active catalyst for selective hydrogenation of furfural to furfuryl alcohol†

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Development of a chromium (Cr)-free hydrogenation catalyst is very important to replace the existing hazardous Cr based catalyst used in the furfural hydrogenation to furfuryl alcohol. Herein, we report synthesis of well-dispersed copper nanoparticles supported on hydrothermally stable magnesium doped alumina (Cu@Mg/ γ -Al₂O₃) for selective hydrogenation of furfural to furfuryl alcohol. The prepared catalyst was characterized by X-ray Photoelectron Spectroscopy (XPS), Auger Electron Spectroscopy (AES), Powder X-ray Diffraction (PXRD), Surface Area Analysis (SAA), High Resolution-Transmission Electron Microscopy (HR-TEM), Temperature Programmed Reduction/Desorption (TPR/TPD) and Inductively Coupled Plasma-Atomic Emission Spectroscopy (ICP-AES) to understand textural properties of the catalyst. The prepared catalyst was found to be highly active and selective with 99% conversion of furfural and 94% selectivity for furfuryl alcohol under solvent free conditions at 443.15 K and 2 MPa of hydrogen pressure. It was also observed that the Cu@Mg/ γ -Al₂O₃ catalyst is reusable (up to six runs) while maintaining its high activity and selectivity ($\geq 94\%$) in the hydrogenation of furfural to furfuryl alcohol.

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1. Introduction

Furfural (FF) is considered as one of the most promising value-added chemicals that can be produced from lignocellulosic biomass and it is a useful raw material for C₄ and C₅ based chemical production.^{1,2} Furfural is industrially produced through the acid hydrolysis of agro-based biomass. Alternatively, it can be produced from woody biomass in an integrated forest biorefinery. Furfural is an important platform molecule and can be converted to other useful chemicals. Thus, many efforts have been devoted to the development of catalytic transformations of FF to other value-added chemicals such as furfuryl alcohol (FA), tetrahydro furfuryl alcohol (THFA) cyclopentanone, 2-methyl furan (2-MF), 1,2 pentane diols, tetrahydrofuran (THF).³ Furfuryl alcohol (FA) is one of the most important derivative of furfural which has much wider applications than furfural. Around 62% of the globally produced furfural is converted to FA.⁴ FA is extensively used as a monomer for cross-linked polymers to produce furan resins, which are used in foundry binders. These resins have excellent chemical,

thermal and mechanical properties along with the capability of resisting corrosion.⁵

Commercially, FA is produced through catalytic hydrogenation of furfural using Cu–Cr based catalyst. Although Cu–Cr based catalyst is active and highly selective for furfural hydrogenation, negative environmental effect of Cr is a major concern for this catalyst. Despite the high yield associated with the traditional Cu–Cr catalyst, it is not ideal due to the presence of Cr₂O₃ (chromium oxide) which can cause severe environmental pollution.⁶ Therefore, development of Cr-free catalytic system with high activity, selectivity, recyclability and able to perform reaction under industrially relevant conditions is highly desirable for hydrogenation of FF to FA. Thus, industries are looking for Cr-free catalyst with similar performance in terms of selectivity and activity. In recent years, various Cr-free catalytic systems based on Pt, Pd, Ru, Rh, Ir and Au have been reported for hydrogenation of furfural and have shown good catalytic conversion under mild reaction conditions.⁷ However, undesired product formation because of high catalytic activity and cost factors of precious metals have limited the commercial applications of noble metal based catalysts. In comparison to this, development of non-precious catalyst system has attractive advantages to meet the challenges of cost effectiveness and sustainability for industrial usage. In search of this, supported and non-supported metal heterogeneous catalysts based on Fe, Co, Ni and Cu were explored.⁸ Along with attractive advantages, these catalysts have some disadvantages like low activity, need of higher reaction temperature and lower selectivity towards the

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desired products. Therefore, to enhance catalytic activity and selectivity, doping small amount of appropriate heteroatom have been explored.

Magnesium supported materials found to exert high catalytic activity in the furfural hydrogenation.⁹ Various Mg incorporated catalysts such as Cu–Mg/ZnO,^{10,11} Mg-doped Pt/Al₂O₃,¹² Ni–Mg/SiO₂,¹³ Mg-doped Co–Ni nanocatalyst,¹⁴ Mg–TiO₂,¹⁵ Mg doped ZnO,¹⁶ graphene oxide/WS₂/Mg-doped ZnO nanocomposite¹⁷ have been explored in hydrogenation, hydrogen storage and other type reactions.^{10–17} However, limited detailed studies are reported in the literature to demonstrate the performance of magnesium doped catalyst in FF hydrogenation to FA. Therefore, we have synthesized and studied performance of magnesium doped heterogeneous Cu@Mg/γ-Al₂O₃ catalyst for the selective hydrogenation of FF to FA under solvent free conditions.

2. Experimental

2.1 Materials and methods

All reagents were purchased from commercial suppliers and used without further purification. All hydrogenation experiments were carried out under hydrogen. Column chromatography was carried out with Merck silica gel 60–120 mesh and the products were characterized and quantified by GC detection. ¹H NMR and ¹³C NMR (300 or 400 MHz and 75 or 100 MHz, respectively) spectra were recorded in CDCl₃. Chemical shifts (δ) are reported in ppm using TMS as an internal standard, and spin–spin coupling constants (J) are given in Hz.

2.2 Catalyst preparation

Cu@Mg/γ-Al₂O₃ catalyst was prepared in three steps as follows.

Step 1: 200 mL of deionised water was taken in a 1 L four neck round bottom flask and equipped with an overhead mechanical stirrer. Mg(NO₃)₂·6H₂O (6.63 g, 0.025 moles) was dissolved and 45 grams of γ-Al₂O₃ (45 g, 0.4413 moles) was added to Mg(NO₃)₂·6H₂O dissolved solution. The resulting slurry was kept for stirring for 2 h and aged at 70 °C for 4 h. The solid product was isolated by filtration and dried at 110 °C for 12 h in an air oven. Mg doped alumina catalyst was then calcined at 350 °C in the presence of air for 5 h to obtain MgO/γ-Al₂O₃ and then cooled to room temperature.

Step 2: in a 250 mL round bottomed flask 100 mL of deionized water was taken and 22.11 g of Cu(NO₃)₂·3H₂O (0.0915 moles) was added under stirring conditions at room temperature for complete dissolution of copper salt. To this solution, 20 g of calcined MgO/γ-Al₂O₃ catalyst added and stirred at room temperature for 2 h. The pH of the reaction mixture was maintained constantly (8 to 9) by the continuous addition of the base solution (30% NH₄OH). The resulting slurry was aged at 70 °C for 2 h. The solid product was isolated by filtration, washed thoroughly with deionised water (to make the catalyst free from base) and dried at 110 °C for 12 h in oven.

Step 3: the copper supported on MgO/γ-Al₂O₃ was further calcined at 750 °C for 4 h to get CuO@Mg/γ-Al₂O₃. CuO@Mg/γ-Al₂O₃ was then reduced under 3 bar of H₂ pressure at 350 °C to

get the final desired reduced Cu(0)@Mg/γ-Al₂O₃ catalyst. Copper nanoparticles anchored on various supports like SiO₂, TiO₂, CeO₂, MoO₃ and γ-Al₂O₃ are also prepared (refer SI for catalyst preparation†) and their performance were checked for FF to FA conversion.

3. Results and discussions

3.1 Catalyst characterization

3.1.1 X-ray diffraction analysis (XRD). X-ray diffraction (XRD) of the prepared samples were analysed in the range of 5° ≤ 2θ ≤ 80° using Cu Kα radiation (γ = 1.5406 Å). The XRD pattern of the samples revealed a highly ordered distinguished two set of peaks as shown in Fig. 2. The diffraction peaks at 43.37°, 50.56° and 74.21° corresponds to (111), (200) and (220) planes, respectively indicating the formation of Cu⁰ from CuO under reduced conditions (JCPDS file no. 04-0836). Peak broadening observed for Cu(0)@Mg/γ-Al₂O₃ is consistent with the small particle size ~5.1 nm. The average crystal sizes calculated using Scherrer formula is 5.0 nm. The XRD results agree well with the HR-TEM analysis indicating that the average particles are constituted of a single crystalline domain. Further, to understand the catalyst stability, high-temperature XRD analysis was performed under atmospheric conditions at various temperatures (Fig. 2B–D).

The catalyst did not show any phase change up to 200 °C and gradual conversion of Cu(0) to CuO is clearly observed after 200 °C. At 300 °C most of the Cu(0) is converted to CuO and the total conversion is observed at 400 °C (Fig. 1D). The XRD patterns of the calcined catalysts did not show any clear peaks corresponding to magnesium species. This could be due to the low concentration of Mg in the sample but it could also be a sign of high dispersion of Mg species, since no characteristics structures are observed.

3.1.2 HR-TEM and XPS analysis of Cu@Mg/γ-Al₂O₃. To investigate the surface morphology and internal structure of the Cu@Mg/γ-Al₂O₃, HR-TEM analysis was conducted (Fig. 3). From HR-TEM it is clearly evident that the copper nanoparticles (Cu⁰) are well dispersed onto the support with the average particle size of copper to be 5 nm. From HR-TEM images it is clear that the formed copper nanoparticles are having two distinguished *d*-spacing of 0.21 and 0.18 nm corresponds to the (111) and (200) lattice planes of the Cu(0). The elemental mapping of the

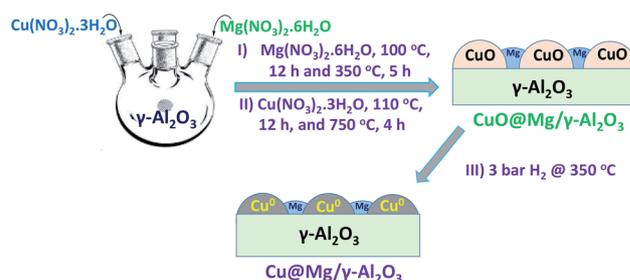


Fig. 1 Schematic representation for synthesis of Cu@Mg/γ-Al₂O₃.



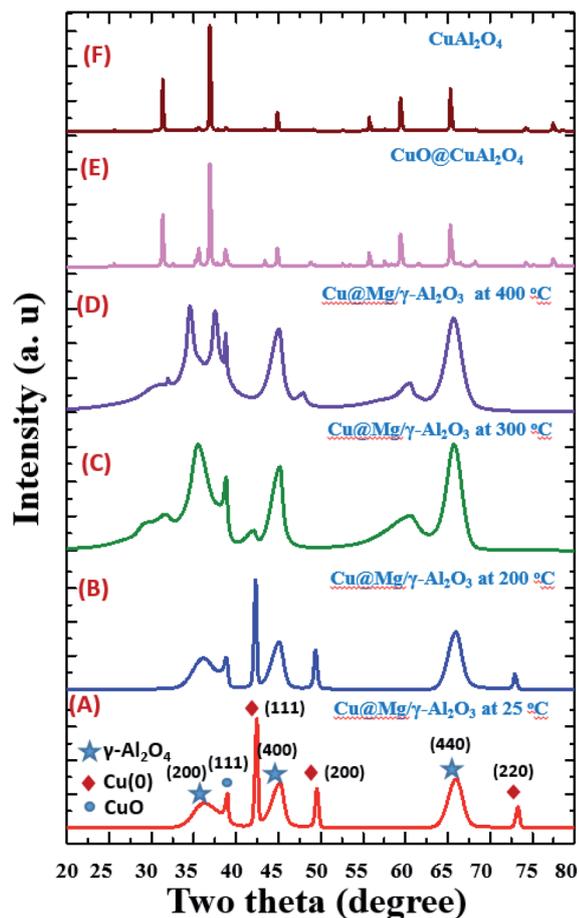


Fig. 2 Temperature dependent XRD spectrum of Cu@Mg/ γ -Al₂O₃ from 25 °C to 400 °C (images A–D), standard CuO@CuAl₂O₄ (E) and CuAl₂O₄ (F).

prepared catalyst also confirms the uniform distribution of Cu and Mg on γ -Al₂O₃ support.

To confirm the oxidation state and surface composition of the catalyst XPS experiments were recorded. As shown in Fig. 4, the binding energies of Cu@Mg/ γ -Al₂O₃ was observed at 932.6 and 952.3 eV corresponds to the spin orbit coupling of Cu 2p_{3/2} and Cu 2p_{1/2} which confirmed the metallic nature Cu(0) of copper nanoparticles (Fig. 4B). The surface scanning of Cu@Mg/ γ -Al₂O₃ by HR-TEM also confirms the uniform distribution of copper throughout the sample (Fig. 3E–H). The peak positions observed at 933.3 and 953.3 eV with the corresponding satellite peaks at 942.5 and 963.8 eV confirmed the Cu 2p core level in the +2 oxidation state (Fig. 4A) of CuO. In contrast, in the case of freshly reduced Cu(0)@Mg/ γ -Al₂O₃, the binding energies were observed at 932.6 and 952.3 eV corresponding to the zero oxidation state of copper in the reduced catalyst and no satellite peaks at the corresponding positions were observed which strongly suggest the complete reduction of small amount of CuO present in Cu@Mg/ γ -Al₂O₃ (Fig. 4A) to Cu(0)@Mg/ γ -Al₂O₃ (Fig. 4B). The very low shake satellite peak observed at 942.5 eV and 963.8 eV in Cu@Mg/ γ -Al₂O₃ catalyst may be due to the small amount of copper oxide (CuO) formed due to copper

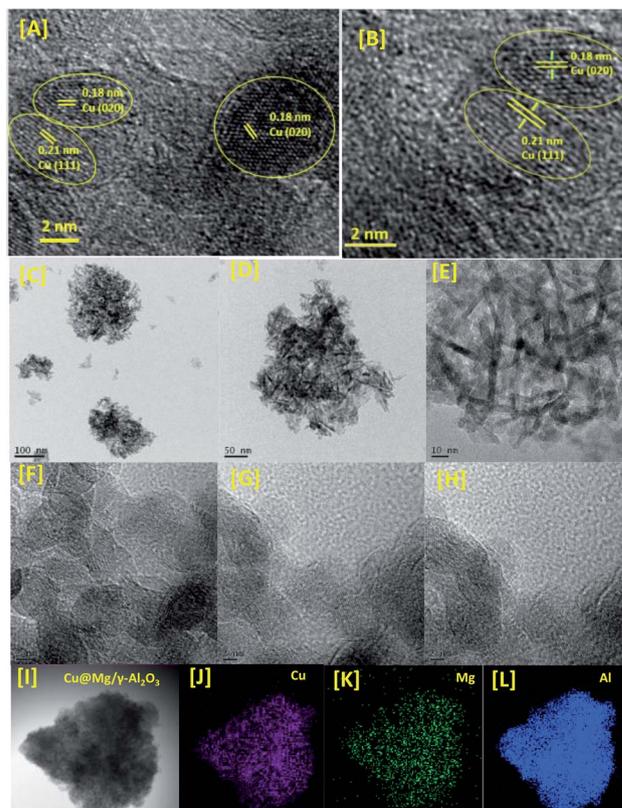


Fig. 3 HR-TEM images [A–I] electron diffraction [SAED pattern, B] and elemental mapping [Cu, Mg and Al from J to L] of Cu@Mg/ γ -Al₂O₃.

propensity for aerial oxidation. The formation of Cu(0) nanoparticles by reduction was further confirmed with Auger electron microscope (AES) analysis (refer ESI†). Cu@Mg/ γ -Al₂O₃ (fresh) and reused Cu@Mg/ γ -Al₂O₃ (recovered after 5th run) were characterized by Auger electron microscopic analysis to confirm the zero oxidation state of the copper, and no oxidation of metallic copper of Cu(0)@Mg/ γ -Al₂O₃ was found even after successive runs. The kinetic energy for fresh and reused catalyst was found to be 919 eV and 918.7 eV.

3.2 Catalytic activity: effect of support

As shown in the Table 1, for the catalytic hydrogenation of FF, copper nanoparticles anchored on various supports like SiO₂,

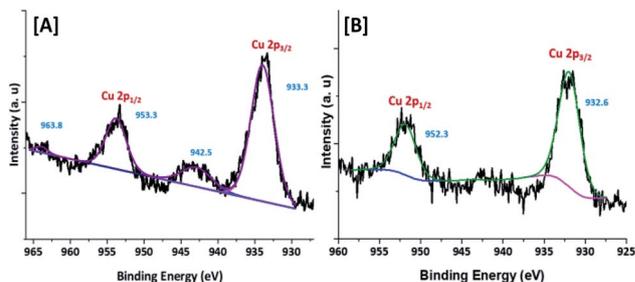


Fig. 4 XPS spectrum of [A] Cu@Mg/ γ -Al₂O₃ and [B] freshly reduced Cu(0)@Mg/ γ -Al₂O₃.



Table 1 Hydrogenation of furfural using various supported metal catalysts^a

Entry	Catalyst	Conv. [%]	Yield [%]				
			FA	2-MF	THFA	Furan	THF
1 ^b	Cu/ γ -Al ₂ O ₃	>99	74	16	3	2	Trace
2 ^{c,d}	Cu/ γ -Al ₂ O ₃	>99	83	0	1	4	0
3	Cu/SiO ₂	>60	10	40	Trace	Trace	Trace
4	Cu/TiO ₂	20	15	2	Trace	Trace	Trace
5	Cu/CeO ₂	45	23	Trace	Trace	Trace	Trace
6	Cu/MoO ₃	20	8	Trace	Trace	Trace	Trace
7	Pt/ γ -Al ₂ O ₃	>90	12	88	Trace	Trace	Trace
8	Rh/ γ -Al ₂ O ₃	>99	—	—	Trace	87	5
9	Ir/ γ -Al ₂ O ₃	>99	—	—	—	96	—
10	Pd/ γ -Al ₂ O ₃	>99	—	—	—	99	—

^a Reaction conditions: furfural (2.6 mol%); catalyst (0.1 g, noble metal 2 mol%); H₂ (2 MPa); 443.15 K; 5 h. ^b Analyzed by GC using an toluene as internal standard. ^c Catalyst (0.1 g, Cu 0.4 mol%). ^d 12 h.

TiO₂, CeO₂, MoO₃ and γ -Al₂O₃ were evaluated under solvent free reaction conditions at different temperatures. Among the screened catalysts, copper nanoparticles supported on γ -Al₂O₃ was found to give the best conversion of FF >99% with FA yield of 74% in 5 h, extending the reaction time to 12 h gave further improvement in reaction yield of FA to 83%. γ -Al₂O₃ is extensively used as support in various active catalysts because of its unique mechanical and chemical properties^{12–15} and high surface area. γ -Al₂O₃ supported catalysts show favourable activity in many reactions such CO₂ hydrogenation,¹⁶ for hydrodesulfurization¹⁷ and reduction of NO_x.¹⁸ However, the formation of side products could not lead the conversion to maximum yields (Table 1, entries 1 and 2). In case of SiO₂, the deoxyhydrogenation product, 2-methyl furan (2-MF) is the major product with 40% yield along with only 10% yield of FA. On the other hand, other solid supports such as TiO₂ resulted in the moderate conversion with less yield (Table 1, entry 4). Next, it was observed that CeO₂ and MoO₃ were less effective for the selective hydrogenation of FF to FA (Table 1, entries 5 and 6). Also, we have compared alumina supported precious metal catalysts like Pt, Rh, Ir and Pd with non-precious catalysts, among them Pt has shown good conversion towards deoxyhydrogenated furfural to 2-MF with 88% yield. Rh, Ir and Pd could give decarbonylated product furan as a major product with 87%, 96% and 99% of yields (Table 1, entries 7–10) respectively. Nevertheless, copper metal sites combined with an aluminium oxide site can play a major role in the activity, selectivity and stability of the samples. Thus, aluminium oxide acts mainly as structural and textural promoter, providing a larger surface area for solids containing copper oxide.¹⁸ The preparation of supported catalyst can be seen in ESI.†

Further, in order to design efficient catalytic system for FF hydrogenation copper nanoparticles supported on bimetallic supported system was examined. Recently, magnesium doped copper and iron based catalysts successfully employed for transfer hydrogenation of furfural using isopropanol as a hydrogen donor.¹⁹ The increase in activity can be attributed to

Table 2 Promoter effect in conversion of furfural to furfuryl alcohol^a

Sr. no.	Bimetallic catalyst	FF conv. [%]	FA yield ^b [%]				
			FA	2-MF	Furan	THF	THFA
1	Cu–Co/ γ Al ₂ O ₃	65	45	4	0	0	5
2	Cu–Zn/ γ Al ₂ O ₃	90	70	16	4	1	0
3	Cu–Mg/ γ Al ₂ O ₃	>99	94	2	4	0	0
4	Cu–Ga/ γ Al ₂ O ₃	75	15	3	0	—	17
5	Cu–Mn/ γ Al ₂ O ₃	80	32	8	5	3	0
6	Cu–Zr/ γ Al ₂ O ₃	80	40	0	0	0	0

^a Reaction conditions: furfural (2.6 mol%); catalyst (0.1 g, noble metal 2 mol%); H₂ (2 MPa); 443.15 K; 5 h. In all the bimetallic catalysts, Cu/X metal ratios were maintained as 5 (10 wt% copper and 2 wt% X metal {X = Co, Zn, Mg, Ga, Mn and Zr}) on the support γ -Al₂O₃. ^b Analyzed by GC using toluene as an internal standard.

the change in the electronic and physical structure of the catalyst and in-turn enhances increase in the absorption ability of the reacting molecules on the host material. The high catalytic activity with Mg doped supports can be attributed due to increasing adsorption sites of hydrogen on MgO surface with low coordination sites on the catalyst surface.²⁰ Typically, MgO acts as a promoter to improve activity and/or selectivity acting as a basic site to polarise the C=O bond of furfural which in turn facilitate nucleophilic attack by hydrogen dissociatively adsorbed on adjacent Cu active sites. Besides this, the basic sites also help to reduce the concentration of Lewis acid centres on the support γ -Al₂O₃, which will decrease coke deriving from the acidic strength of γ -Al₂O₃. The same can be witnessed from CO₂-TPD data wherein basic site concentration is found to enhance in presence of MgO (see ESI for CO₂-TPD†). The effect of different metals as promoters such as: Co, Zn, Mg, Ga, Mn and Zr on catalytic activity of Cu/ γ -Al₂O₃ in FA synthesis was also studied (Table 2). Based on the literature reports and in our present investigation to increase the catalytic activity of copper supported catalyst for hydrogenation of FF, magnesium has been doped in various molar ratios and their catalytic activity were investigated (Table 3). MgO increases the strength of the interaction between Cu and Al₂O₃ and induces a spillover effect between these phases. Synergistic catalytic effect between the catalytically active metallic copper species and the Lewis basic

Table 3 Cu–Mg ratio effect in conversion of furfural to furfuryl alcohol^a

Sr. no.	Cu/Mg	FF conv. [%]	FA yield ^b [%]				
			FA	2-MF	Furan	THF	THFA
1	4	>99	90	3	2	1	1
2	5	>99	94	2	4	0	0
3	10	>99	80	15	0	0	0
4	15	>99	65	22	2	0	1

^a Reaction conditions: furfural (2.6 mol%); catalyst (0.1 g, Cu/Mg mol%); Cu/Mg = 4 (Cu: 0.2 mol% and Mg: 0.05 mol%); H₂ (2 MPa); 443.15 K; 5 h. ^b Analyzed by GC using toluene as an internal standard.



Table 4 Effect of supports on the hydrogenation of furfural using Cu–Mg catalysts^a

S. no.	Catalyst	H ₂ [MPa]	Time [h]	FF conv. [%]	Yield [%]				
					FA	2-MF	Furan	THF	THFA
1	Cu–Mg/ γ -Al ₂ O ₃	2	3	90	85	0	3	Trace	0
2 ^b	Cu–Mg/ γ -Al ₂ O ₃	2	5	>99	94	2	4	0	0
3 ^c	Cu–Mg/ γ -Al ₂ O ₃	2	5	>99	94	2	4	0	0
4	Cu–Mg/ γ -Al ₂ O ₃	2	4	>99	90	4	4	1	0
5	Cu–Mg/ γ -Al ₂ O ₃	1	10	>99	93	Trace	5	2	0
6	Cu/ γ -Al ₂ O ₃	2	10	>99	74	16	3	Trace	2
7	MgO/ γ -Al ₂ O ₃	2	10	Trace	0	Trace	0	Trace	0
8	Cu–Mg/SiO ₂	2	5	>99	44	0	26	9	17
9	Cu–Mg/TiO ₂	2	5	>99	39	49	8	4	Trace
10	Cu–Mg/CeO ₂	2	5	>99	2	53	0	0	0
11	Cu–Mg/MoO ₃	2	5	>99	32	Trace	0	0	0

^a Reaction conditions: FF (2.6 mol%); catalyst (2 g, Cu–Mg: Cu@Mg, Cu-0.2 mol%, Mg 0.05 mol%); H₂ (2 MPa); 443.15 K. ^b Cu/Mg = 5. ^c Reuse 3.

sites, which held the key to the hydrogenation reaction related to the hydrogen dissociation and the activation of the carbonyl groups attribute to its high catalytic efficiency. Another advantage of using MgO as a promoter for the preparation of Cu@Mg/ γ -Al₂O₃ catalyst arises from the possibility of forming a CuO–MgO solid solution at any molar ratio due to close ionic radii of Mg²⁺ and Cu²⁺ cations (Mg²⁺ 0.65 Å and Cu²⁺ 0.73 Å) and the particular lattice parameters of this mixed metal oxide structure. The formation of this mixed oxide phase favors increased metal-support interaction, and thus prevents catalyst deactivation *via* sintering. On the other hand, the promotion of copper catalysts by magnesium oxides increases the amount of hydroxylalkyl intermediate group formed on the catalysts surface during the process compared to the reaction carried out with the unprompted catalysts. ¹H NMR analysis of the reaction intermediate showed the formation of hydroxyalkyl intermediate in 9% yield, which transformed to FA with Cu–Mg/ γ -Al₂O₃.

Among all, Cu–Mg supported catalysts showed the most superior activity performance in terms of FF conversion, FA formation rate, and yield. Therefore, the Cu–Mg was employed hereafter to compare with other support materials (Table 4). In the case of γ -Al₂O₃, FF conversion attributed 90% conversion with 85% of FA product yield, increase in reaction time to 5 h further increases the conversion to 99% with 94% of product selectivity (Table 4, entries 1 and 2). On the other hand, other solid supports such as SiO₂, TiO₂, CeO₂ and MoO₃ resulted in moderate yields with 2-MF and furan as a major side products (entries 8 to 11). The support γ -Al₂O₃ with high surface area than other supports (Table 2, entries 8 to 11) shows highly dispersed copper species achieved the highest catalytic activity compared to the sample containing copper on SiO₂, TiO₂, CeO₂ and MoO₃. The presence of γ -Al₂O₃ interacting with copper oxide provides a lower sintering under optimized reaction conditions.²¹ It is also clearly noticeable that the magnesium doped catalysts are comparatively higher in activity than magnesium free catalysts (Table 4, entries 1–5 vs. 6). These results clearly show that the combination of Cu(0) nanoparticles and Mg on γ -Al₂O₃ support is uniquely effective for the

synthesis of FA from FF under solvent-free conditions. Furthermore, the addition of a second metal MgO as promoter has been found to improve activity and/or selectivity by acting as a basic site to polarise the >C=O bond facilitating nucleophilic attack by hydrogen dissociatively adsorbed on neighbouring Cu active sites. Moreover, with a capacity for oxygen storage, MgO can release oxygen to oxidize the carbon formed on the catalyst surface. Particularly, the presence of the basic centre will strengthen the chemisorption of carbonyl group. Next, to understand the importance of hydrogen pressure, the reaction was performed at 1 MPa, which took almost 10 h to complete the conversion of FF to FA with 93% selectivity of desired product (Table 4, entry 5). As evident from Tables 1 and 2 the optimum condition for hydrogenation of furfural is at 443.15 K for 5 h at 2 MPa to get maximum yield of FA.

3.3 Catalyst stability and reuse experiments

From an industrial perspective, one of the main advantages of using heterogeneous catalysts such as Cu@Mg/ γ -Al₂O₃, is that they can be recovered and reused efficiently up to six consecutive runs (Fig. 5). The spent catalyst was recovered from the reaction mixture by simple centrifugation after the completion of the reaction and washed with EtOAc (3 × 10 mL) to remove all the organic substrates from the catalyst surface. No quantifiable

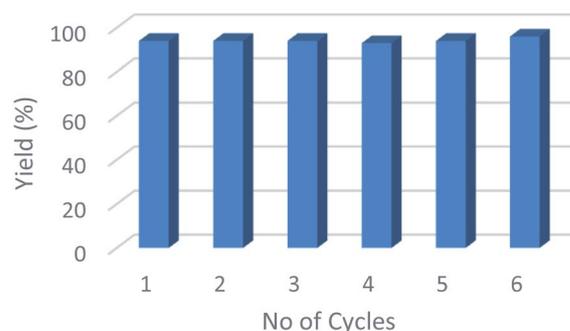


Fig. 5 Recyclability of the catalyst for reduction of furfural up to six consecutive runs.



Table 5 Recyclability of Cu@Mg/ γ -Al₂O₃ for hydrogenation of FF up to five runs^a

Reaction run	Run 1	Run 2	Run 3	Run 4	Run 5	Run 6
FA yield (%)	94	94	94	93	94	96

^a Reaction conditions: FF (2.6 mol%); Cu@Mg/ γ -Al₂O₃ (0.1 g); 443.15 K; H₂ (2 MPa); 5 h; yields analyzed by GC using toluene as an internal standard.

amount of leached Cu was detected in the filtrate as determined by ICP (AES) studies of both fresh and spent catalyst. Furthermore, the HR-TEM images of the used catalyst did not show any significant change in the shape and size of the support as well as the particle size of the active species, Cu(0). This suggests that the morphology of the catalyst remains the same even after multiple reaction cycles Table 5.

3.4 Representative reaction procedure

The hydrogenation of furfural was carried out in a 500 mL stainless steel autoclave PARR reactor. The vessel was charged with 2.6 mol of furfural, and 0.1 g of catalyst. The reactor was sealed, purged three times with H₂ at 2 MPa, then pressurized to 2 MPa, heated to 443.15 K and stirred at 300 rpm for 5 h with continuous H₂ flow (80 SLPH). Following the reaction, the autoclave was cooled to room temperature and the hydrogen gas was carefully released. The resulting reaction mixture was centrifuged and catalyst was separated from the reaction. The reaction mixture is then diluted with Toluene and analyzed by GC. Cu@Mg/ γ -Al₂O₃ catalyst provides FA product in good to excellent yields over short reaction times compared with reported catalyst in the absence of solvents and strong bases (see ESI Table 1†). Furthermore, the catalyst was applicable to preparative scale reaction; 500 g of FF afforded 502 g of FA in 96% isolated yield (ESI†).

4. Conclusions

The present study demonstrates high activity, selectivity and stability of chromium-free Cu-based catalyst supported on MgO-doped γ -Al₂O₃ in solvent free hydrogenation of furfural to furfuryl alcohol. The prepared catalyst is found to be selective in the hydrogenation of furfural to furfuryl alcohol with selectivity of 95% at 100% conversion of furfural. The remarkably high performance of this catalyst is attributed to the synergistic effect of copper and magnesium resulting in active Cu–Mg species on the surface of alumina.

Conflicts of interest

There are no conflicts to declare.

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