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Pretreatment by recyclable Fe₃O₄@Mg/Al-CO₃-LDH magnetic nano-adsorbent to dephosphorize for the determination of trace F[−] and Cl[−] in phosphorus-rich solutions

Si Chen,^{ab} Yongchun Xu,^{ab} Yu Tang,^{ab} Wei Chen,^{ab} ^{*ab} Shubin Chen,^{ab} Lili Hu^{ab} and Georges Boulon ^c

The magnetic nano-adsorbent Fe₃O₄@Mg/Al-CO₃-LDH (Mg/Al-type layered double hydroxide) with a CO₃^{2−} interlayer anion has been synthesized successfully on Fe₃O₄ nanoparticles via a urea hydrothermal method. It is confirmed that the nano-adsorbent can adsorb PO₄^{3−} rapidly and efficiently in multi-ion solutions; meanwhile, it did not adsorb any F[−] and Cl[−], even with a high amount of the nano-adsorbent or a longer adsorption time. This behaviour is beneficial for applications to remove PO₄^{3−} in phosphorus-rich solutions, and especially can be utilized to determine trace F[−] and Cl[−] anions in phosphorus-rich solutions by physical and chemical analysis methods including ion chromatography without serious interference from PO₄^{3−} for trace determinations. Herein, the hydrothermally synthesized Fe₃O₄@Mg/Al-CO₃-LDH was characterized via SEM, TEM, SAED, XRD, FTIR, magnetic hysteresis loop analysis and adsorption–desorption isotherm analysis. The structure and stability, adsorption mechanism, magnetic saturation value, specific surface area, total pore volume, phosphate adsorption capacity and recyclability are discussed. Using the optimized pretreatment conditions, Fe₃O₄@Mg/Al-CO₃-LDH was utilized successfully to adsorb PO₄^{3−} in real samples and determine trace F[−] and Cl[−] accurately by ion chromatography; this would be very beneficial for continuous analysis and on-line tests by physical and chemical analysis methods without interference from PO₄^{3−} in phosphorus-rich samples, leaving F[−] and Cl[−] even if in a trace content.

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1 Introduction

Currently, phosphate materials or its hybrid materials, presented as crystal, glass or ceramics, are widely applied¹ in numerous fields such as optics and electronics, as well as medical biomaterials for applications² in bone grafting and regeneration, drug delivery, *etc.* However, in the determination of target ions in solutions containing these materials, the matrix phosphate anion PO₄^{3−} seriously interferes in determinations by methods such as spectrophotometry,³ neutron activation,⁴ molecular absorption spectrometry,⁵ graphite furnace,⁶ electrothermal atomic absorption spectrometry,⁷ and inductively coupled plasma mass spectrometry.⁸ To determine anion impurities, the commonly used chromatography method will be affected seriously by interference from the phosphate anion. The signal from a high

concentration PO₄^{3−} will cover the peak or deform the peak shape of the target anion.^{9–11} Furthermore, it will make the analytical column overloaded, which will shorten the service life of the column. Once the analytical column is overloaded, a ghost peak will appear, or the next injection may not even be allowed.¹¹ Although solutions with a high concentration of PO₄^{3−} can be diluted greatly, this also reduces the content of the target anion, leading to a content much lower than the detection limit.¹⁰ After fully rinsing the loops¹¹ of the chromatograph for several runs using deionized water, a certain amount of PO₄^{3−} as carryover resulting from the previous injection may still be observed even if a blank sample is used. Therefore, an appropriate sample pretreatment to dephosphorize solutions with a high PO₄^{3−} content is particularly important.^{10,11}

A further issue is specifically related to the determination of trace F[−] and Cl[−] anions in phosphorus-rich solutions. If F[−] anions from the raw materials and products of the phosphate industry such as from phosphate ore, phosphate fertilizer, phosphogypsum enter the biological chain continuously during manufacturing processes, storage and utilization, the bio-accumulated F[−] will pose a serious threat to human life. Thus, it is necessary to monitor trace F[−] and Cl[−] anions in phosphorus-

^aKey Laboratory of Materials for High Power Laser, Shanghai Institute of Optics and Fine Mechanics, Chinese Academy of Sciences, Shanghai 201800, China. E-mail: weichen@sion.ac.cn

^bCenter of Materials Science and Optoelectronics Engineering, University of Chinese Academy of Sciences, Beijing 100049, China

^cInstitut Lumière Matière (ILM), UMR5306 CNRS-Université Claude Bernard Lyon 1, Université de Lyon, 69622 Villeurbanne, France



rich raw materials and final products.¹² Moreover, hydroxyapatite is a particularly promising bone-grafting material for dental and orthopaedic applications. The addition of trace F^- can construct a microenvironment favouring bone healing and bone regeneration,¹³ but its trace amount must be strictly controlled to avoid cell death or necrosis.¹⁴ Thus, all the above-mentioned factors make the accurate determination of trace F^- and Cl^- in phosphorus-rich solutions necessary, with the aim to fully keep F^- and Cl^- and adsorb PO_4^{3-} as much as possible during the pretreatment, which should be developed.

Layered double hydroxides (LDHs) are two-dimensional nanostructured anionic clays, with the general formula of $[M_{1-x}^{2+}M_x^{3+}(OH)_2]^{x+}[A_{x/n}^{n-}yH_2O]^{x-}$, where M is a metal cation and A is the interlayer anion with n -valence.^{15,16} Strong chemical bonds exist within the layer of $[M_{1-x}^{2+}M_x^{3+}(OH)_2]^{x+}$, but the bonds between the interlayer anion of $[A_{x/n}^{n-}yH_2O]^{x-}$ and the layer of $[M_{1-x}^{2+}M_x^{3+}(OH)_2]^{x+}$ are relatively weak. This makes LDHs promising ion-exchangers¹⁷ for applications to adsorb the PO_4^{3-} anion.^{17–30}

To efficiently adsorb PO_4^{3-} , the interlayer anion choice will play a key role. Based on LDHs, there are some good options to use the Cl^- anion,^{17,20,22–24,31} or NO_3^- anion,^{19,21,32} or Cl^- and SO_4^{2-} anions²⁵ as the interlayer anion. They can be used to adsorb PO_4^{3-} effectively, but their adsorption efficiencies are inevitably affected by carbon dioxide (CO_2) or carbonate (CO_3^{2-}) from the preparation process of the LDH, the solution environment and even the atmosphere.^{17,19,25}

Employing CO_3^{2-} as the interlayer anion, Zn–Al–LDH,¹⁸ Zr-modified MgFe–LDH(CO_3),²⁷ Fe_3O_4 @Mg–Al–LDH,²⁶ Mg–Fe LDH²⁸ and Fe_3O_4 @gelatin-encapsulated hydrotalcite³³ were prepared to adsorb PO_4^{3-} successfully by a co-precipitation method. By comparison, the hydrothermal method is a better way to prepare LDH with the CO_3^{2-} interlayer anion using urea, which can well control the size and crystallinity of the prepared nanoparticle.¹⁵ In the investigations for the preparation of LDH with CO_3^{2-} *via* the urea hydrolysis method,^{29,30,34–54} only two LDHs have been used as a phosphate adsorbent.^{29,30} Cu–Al LDH (CuAl/biomass carbon fibre-layered double hydroxide)²⁹ was synthesized at 110 °C for 12 h, and Zn–Al LDHs³⁰ were synthesized at 150 °C for 36 h.

Herein, an Mg–Al LDH was hydrothermally synthesized with $Mg(NO_3)_2$, $Al(NO_3)_3$, and urea, using CO_3^{2-} as the interlayer anion. To utilize magnetic solid phase extraction (MSPE), which can achieve the purpose of phosphate adsorption and its rapid separation, Fe_3O_4 magnetic nanoparticles were introduced into the Mg–Al LDH nano-adsorbent during the hydrothermal synthetic process. Using the prepared Fe_3O_4 @Mg/Al- CO_3 -LDH magnetic nano-adsorbent, adsorption–determination and recycle procedures were conducted, as described in Section 2.3. As described in Section 3.1, its structural properties were characterized *via* SEM, TEM, FTIR, and XRD, and its magnetic property, specific surface area, and porosity were also analysed. After optimizing the pretreatment conditions, as discussed in Section 3.2, the stability and recyclability after 15 cycles with high adsorption capacity is shown in Section 3.3. More importantly, it was found that the hydrothermally synthesized Fe_3O_4 @Mg/Al- CO_3 -LDH magnetic nano-adsorbent only adsorbed PO_4^{3-} , not F^- and Cl^- in solution.

This is undoubtedly beneficial to accurately determine the content of F^- and Cl^- in phosphate solutions by chromatography, and the practical applications are introduced in Section 4.

2 Experimental

2.1 Hydrothermally synthesized Fe_3O_4 @Mg/Al- CO_3 -LDH

The magnetic layered double hydroxide nano-adsorbent Fe_3O_4 @Mg/Al- CO_3 -LDH was synthesized *via* a urea hydrothermal method. After several trials, 0.6 g of Fe_3O_4 nanoparticles (ultrafine powder purchased from Macklin) was used and added to 15 mL solution of 0.1 mol L^{−1} NaOH (AR grade). After the mixture was dispersed by ultrasonication for 10 min, it was separated using a magnet for further use. Then 2.044 g $Mg(NO_3)_2 \cdot 6H_2O$ (AR grade), 1.500 g $Al(NO_3)_3 \cdot 9H_2O$ (AR grade), and 1.68 g urea (CH_4N_2O , AR grade) were added to 70 mL deionized water (Millipore Milli-Q Direct 8). The mixed salt solution was further mixed using a vortex mixer (NP-30S) for 15 min. The activated Fe_3O_4 and mixed salt solution were transferred to an autoclave and mixed for 2 h using the vortex mixer. Then the autoclave was heated at 120 °C for 12 h. Next, the autoclave was cooled to room temperature. The obtained product was separated by a magnet and washed with deionized water and ethanol (AR grade) three times, followed by drying in an oven at 60 °C for 12 h. Finally, the Fe_3O_4 @Mg/Al- CO_3 -LDH magnetic nano-adsorbent was obtained.

2.2 Instruments

SEM analysis was performed using an Inspect F50 field-emission scanning electron microscope (FEI) with a resolution of 2.0 nm. An acceleration voltage of 10 kV was applied during secondary electron imaging.

TEM analysis was performed using a JEM-2100F high-resolution field-emission transmission electron microscope (JEOL) with a point resolution of 0.24 nm and line resolution of 0.10 nm. To observe the morphology of the nanoparticles, the bright-field mode was utilized. To observe the electron diffraction from different regions on the nanoparticle, the selected area mode was utilized. An acceleration voltage of 200 kV was applied for both modes. The nanoparticles were dispersed by ethanol to form a suspending liquid before observation.

FTIR spectra were measured using a Nicolet Nexus Fourier transform infrared spectrometer (Thermo Fisher), in the range of 4000 to 400 cm^{−1} with a resolution of 4 cm^{−1}. The nanoparticles were mixed with KBr (SP grade) in the mass ratio of 1 : 100. After grinding in an agate mortar, the mixture was pressed into a thin disc sample.

XRD patterns were collected using a SmartLab9 X-ray diffractometer (Rigaku) with Cu- $K\alpha$ radiation of $\lambda = 0.15418$ nm in the 2θ range of 0.08–78° with the scanning step of 0.02° and the step time of 2 s.

Magnetic hysteresis loop analysis was performed using a SQUID vibrating sample magnetometer (Quantum Design) in the magnetic field range of $\pm 30\,000$ Oe.

Specific surface area and porosity were fitted from the N_2 adsorption–desorption isotherms, which were determined at 77



K using an ASAP 2460 Accelerated Surface Area and Porosimeter System (Micromeritics).

The contents of F^- , Cl^- , and PO_4^{3-} were determined using an ICS 5000+ ion chromatograph (Thermo Fisher) with a 25 μ L sample loop and a conductivity detector. An IonPac® AS18 (250 mm \times 4.0 mm i.d.) was applied as the anion exchange analytical column, which was protected by the guard column of IonPac® AG18 (50 mm \times 4.0 mm i.d.). The temperature of the column compartment was set to 30 $^{\circ}C$. For the eluent of NaOH solution, the flow rate through the anion exchange analytical column was 1.00 mL min $^{-1}$, and its concentration was automatically adjusted by an electrolytic eluent generator. When the test time was set to 35 min, the eluent concentration would be 25 mmol (0–13 min), 40 mmol (13–30 min), and 25 mmol (30–35 min). Manual injection was done in the operation.

2.3 Adsorption–determination and recycle procedures

The two main procedures are exhibited in Fig. 1 to adsorb PO_4^{3-} in a solution of $Fe_3O_4@Mg/Al-CO_3-LDH$ for the determination of F^- and Cl^- , and to recycle and reuse $Fe_3O_4@Mg/Al-CO_3-LDH$.

Specifically, 50 mg of the synthesized magnetic nano-adsorbent was added to 80 mL of sample solution. They were mixed in a beaker by a vortex mixer for 5 min. After the adsorbent was isolated from the suspension with a magnet, the residual solution was filtered using a 0.22 μ m membrane. It was bubbled with N_2 for 30 s to remove CO_3^{2-} , and then passed through an OnGuard II H column to remove the metal cations. At this time, the residual solution after adsorption on the $Fe_3O_4@Mg/Al-CO_3-LDH$ nanoparticles could be introduced into the ion chromatograph to determine F^- and Cl^- .

For the recycle procedure, the used $Fe_3O_4@Mg/Al-CO_3-LDH$ was collected and placed in 15 mL desorption solution, 5 wt% NaOH and 10 wt% Na_2CO_3 (AR grade), and further mixed using a vortex mixer for 30 min. With the aid of a magnet, the $Fe_3O_4@Mg/Al-CO_3-LDH$ nanoparticles were washed with deionized water and ethanol three times. This was followed by drying in an oven at 60 $^{\circ}C$ for 12 h, and then $Fe_3O_4@Mg/Al-CO_3-LDH$ was regenerated for use for a new cycle adsorption. It should be noted that NaOH in the desorption solution will not affect the stability of $Mg/Al-CO_3-LDH$ since it was synthesized in an environment of NaOH, as indicated in Section 2.1.

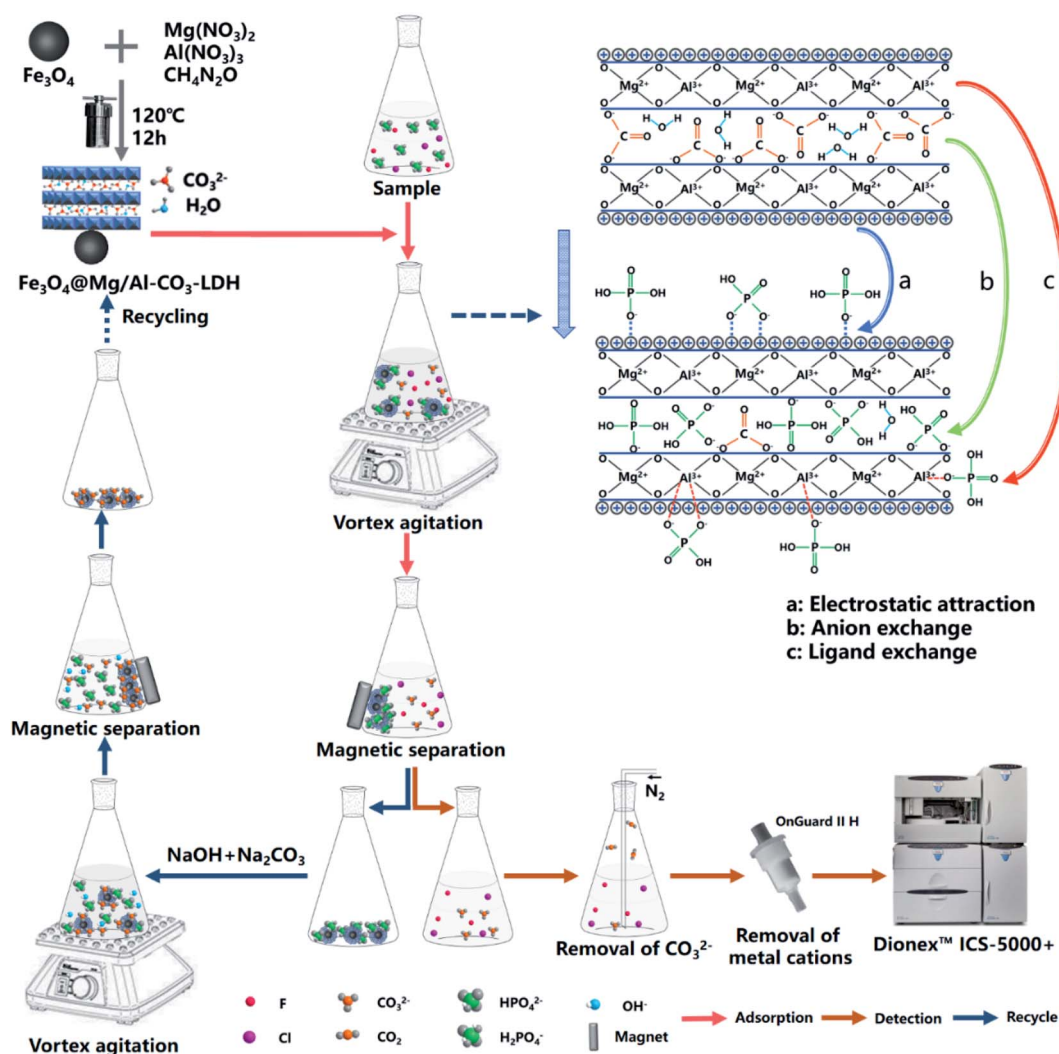


Fig. 1 Schematic illustration of the synthesis, adsorption, determination and recycle processes.



To evaluate the recyclability of the magnetic adsorbent, the phosphate adsorption capacity per unit mass of $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ was measured for each cycle. Briefly, 50 mg of the magnetic adsorbent was added to 80 mL mixed solution with $1.00 \text{ mg L}^{-1} \text{ F}^-$, $1.00 \text{ mg L}^{-1} \text{ Cl}^-$ and $C_0 = 100 \text{ mg P per L PO}_4^{3-}$ (based on P). Then, it was processed by 60 min mixing/adsorption, magnetic solid phase extraction-separation, filtering, bubbling, cation removal and chromatographic determination, as stated above. After determining the remaining phosphate concentration, C_e , which is also the equilibrium PO_4^{3-} concentration in the solution, the adsorption capacity, Q_e , of PO_4^{3-} was calculated by $Q_e = (C_0 - C_e)V/m$, where V is the solution volume in L and m is the dry weight of the nano-adsorbent in g.

3 Results and discussion

3.1 Characterization of $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$

Fig. 2 shows the electron microscopy analysis of Fe_3O_4 and the synthesized $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ magnetic nanoparticles. Both the SEM and bright-field TEM images show that Fe_3O_4 is an octahedral nanoparticle with clear edges and smooth surface, and its size is about 120 nm, as shown in Fig. 2(a) and (b). On the surface of Fe_3O_4 , $\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ was synthesized *via* the urea hydrothermal method. The shape of these irregular $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ nanoparticles is not like the octahedron of Fe_3O_4 , and on their surface, some protuberances exist, as shown in Fig. 2(c). According to the bright-field TEM image shown in Fig. 2(d), these protuberances also can be observed at the outer boundary of the bright gray region, and the bright gray region surrounding the dark region of Fe_3O_4 is characterized by a flake-like matrix. This is similar to the morphology of $\text{Fe}_3\text{O}_4@\text{CuMgAl-LDH}$ nanoparticles.⁵⁵ Due to the stacking of many small flakes, the hydrothermally synthesized $\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$

on Fe_3O_4 nanoparticles appears to consist of an agglomeration of plate-like structures.⁵⁶

Fig. 3(a) shows the high-resolution TEM image of the synthesized $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$, where the bottom-left dark region and the bottom-right bright region were chosen for SAED, as shown in Fig. 3(b) and (c), respectively. The selected area electron diffraction (SAED) for the dark region clearly shows 4.910 Å, 3.193 Å, 2.469 Å and 1.698 Å diffractions, corresponding to the (111), (220), (222) and (422) planes of Fe_3O_4 (PDF card: #19-0629). Also, the SAED for the bright region shows 1.541 Å and 1.476 Å diffractions, corresponding to the (110) and (113) planes of $\text{Mg}/\text{Al-LDH}$ (PDF card: #89-0460). Although the diffraction spots for the bright region are somewhat blurred, as shown in Fig. 3(c), the hexagonal diffraction pattern can still be observed, which is the typical diffraction pattern of LDH crystals.⁵⁵

Thus, the above electron microscopic analysis indicates that during the hydrothermal process, Fe_3O_4 retains its original crystalline state, and $\text{Mg}/\text{Al-LDH}$ is grown as small crystal plates. Their crystallization is also indicated by the XRD pattern shown in Fig. 4(a) for as-synthesized $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$. The diffraction peaks at the 2θ values of 18.24° (111), 30.08° (220), 35.46° (311), 37.04° (222), 43.12° (400), 53.50° (422), 57.04° (511), and 62.56° (400) correspond to the octahedral Fe_3O_4 crystal,²⁶ and the peaks at the 2θ values of 11.54° (003), 23.44° (006), 35.46° (012), 61.02° (110), and 62.56° (113) correspond to the Mg-Al-LDH crystal.^{26,57} More importantly, after 15 cycles of PO_4^{3-} -adsorption and regeneration of $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$, as stated in Section 2.3, both the XRD peak positions and intensities remained almost unchanged, as shown in Fig. 4(a) and (b). This indicates that even after 15 cycles, the

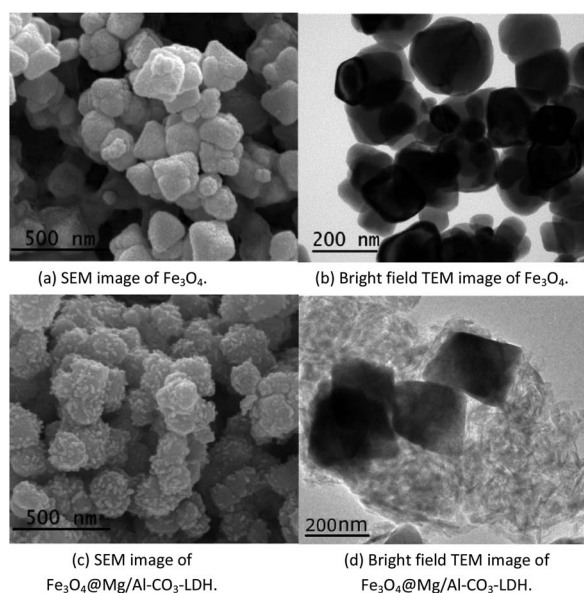


Fig. 2 Electron microscopy analysis of Fe_3O_4 nanoparticles and prepared $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ magnetic nano-adsorbent.

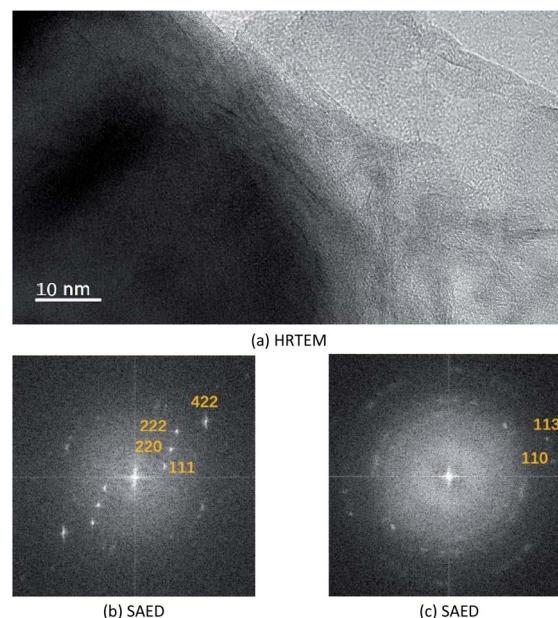


Fig. 3 High-resolution transmission electron microscopy (HRTEM) and selected area electron diffraction (SAED) for prepared $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$, where (b) corresponds to the area at the bottom-left of (a), and (c) corresponds to the area at the bottom-right of (a).



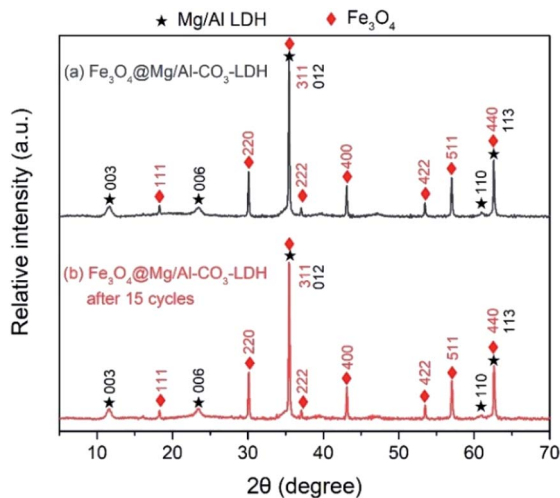


Fig. 4 XRD patterns of Fe₃O₄@Mg/Al-CO₃-LDH magnetic nano-adsorbent before and after 15 cycles of PO₄³⁻ adsorption and regeneration.

Fe₃O₄@Mg/Al-CO₃-LDH magnetic nano-adsorbent can still maintain its structural stability, and thus has important potential for recycling.⁵⁸

To explore the adsorption and desorption of PO₄³⁻, the FTIR spectra of Fe₃O₄@Mg/Al-CO₃-LDH were measured for the as-synthesized, PO₄³⁻-adsorbed, and regenerated after 15 cycles of PO₄³⁻ adsorption samples, as shown in Fig. 5(a)–(c), respectively. The Fe–O vibration peak⁵⁹ appeared at 586 cm^{−1} before and after adsorption and desorption, showing the stable assembly between Fe₃O₄ and Mg/Al-CO₃-LDH.

As shown in Fig. 5(a), the spectrum of the as-synthesized sample exhibits peaks at 448 cm^{−1}, 681 cm^{−1}, and 788 cm^{−1}, which are attributed to the vibration of Mg–OH,⁶⁰ Mg–O–Al,⁶¹ and Al–OH,⁶⁰ respectively. The two peaks located at 3445 cm^{−1} and 1637 cm^{−1} are related to the stretching and bending modes

of the water molecule existing in the interlayer structure, respectively.⁶² These peaks indicate the successful synthesis of the layered structure Mg/Al-LDH. As the interlayer anion, the vibration of CO₃²⁻ appears³⁵ at 1362 cm^{−1} and 1502 cm^{−1}. During the hydrothermal process, urea decomposes at high temperature and produces the CO₃²⁻ anion,⁶³ which then enters Mg/Al-LDH to form the interlayer anion. Moreover, there is a small peak located at 1385 cm^{−1}, corresponding to the NO₃[−] vibration, but it is rather weak. This is due to the use of nitrate during the synthetic process, where a small amount of NO₃[−] existing in Fe₃O₄@Mg/Al-CO₃-LDH was not replaced by CO₃²⁻.

As shown in Fig. 5(b), in the spectrum of the PO₄³⁻-adsorbed sample, the Fe–O vibration and the stretching and bending modes of the water molecule remained, but the vibrations resulting from Mg–OH, Mg–O–Al, and Al–OH almost disappear. Especially, there is no CO₃²⁻ vibration at 1502 cm^{−1}, and only a very weak CO₃²⁻ peak at 1362 cm^{−1}. On the other hand, new peaks at 2484 cm^{−1}, 2401 cm^{−1}, 1088 cm^{−1}, and 901 cm^{−1} appear, which are due to the vibrations of PO₄³⁻.^{25,64,65} These results clearly indicate that the anion exchange²⁶ really occurred for Fe₃O₄@Mg/Al-CO₃-LDH after adsorbing PO₄³⁻, which is the process to use PO₄³⁻ to replace CO₃²⁻. It is most probably the first mechanism for the synthesized Fe₃O₄@Mg/Al-CO₃-LDH to adsorb PO₄³⁻ in solution. Due to the disappearance of the vibrations of Mg–OH and Al–OH, it means that they can be protonated and become positively charged, and thus they can adsorb the negatively charged PO₄³⁻ due to electrostatic adsorption on the surface of LDH.²⁹ This may be the second mechanism to adsorb PO₄³⁻ in solution. The disappearance of the vibration of Mg–O–Al may be possibly explained by the fact that, as a ligand anion,²⁹ PO₄³⁻ can be complexed with the Al³⁺ cation on the surface of Fe₃O₄@Mg/Al-CO₃-LDH. This ligand exchange may be the third mechanism to adsorb PO₄³⁻ in solution. The ability to perform these three mechanisms for the synthesized Fe₃O₄@Mg/Al-CO₃-LDH is consistent with the reported PO₄³⁻-adsorbed LDHs.^{26,29,33}

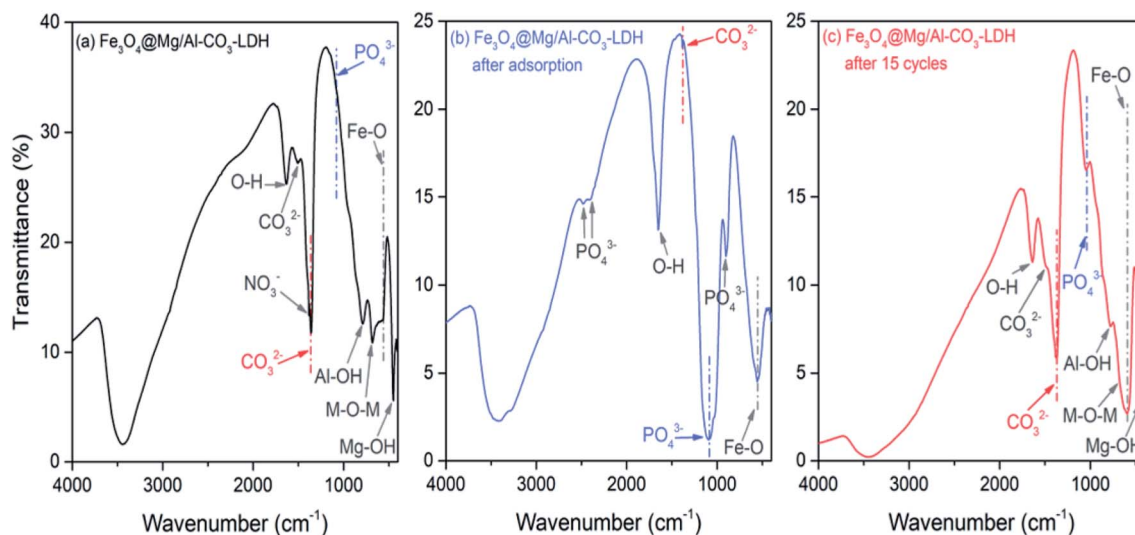


Fig. 5 FTIR spectra of Fe₃O₄@Mg/Al-CO₃-LDH magnetic nano-adsorbents. (a) As-prepared, (b) PO₄³⁻-adsorbed, and (c) regenerated after 15 cycles of PO₄³⁻ adsorption.



As shown in Fig. 5(c), in the spectrum of the regenerated sample after 15 cycles of PO_4^{3-} -adsorption, the positions and intensities of the FTIR peaks are almost the same as that in Fig. 4(a) of the as-synthesized sample. This means that the desorption was successful, and the regenerated $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ returned to its original state with a strong ability to be recycled. It should be noted that there is still a weaker peak at 1088 cm^{-1} due to PO_4^{3-} , which indicates a small amount of was PO_4^{3-} left in $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ after 15 cycles. However, it had no great effect on the phosphate adsorption capacity, as stated in Section 3.3, since most of the interlayer anions were exchanged by CO_3^{2-} during the desorption process.

It was reported⁵² that for MgAl-LDO calcined at 500°C for 4 h after its synthesis, the FTIR band of $-\text{OH}$ was shifted to a higher frequency from 1644 cm^{-1} to 1664 cm^{-1} after F^- adsorption, which may be due to the adsorption of F^- . However, as can be seen in Fig. 5(a)–(c), the band due to OH appears at 1637 cm^{-1} , 1640 cm^{-1} , and 1638 cm^{-1} for the as-synthesized, PO_4^{3-} -adsorbed, and regenerated $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ samples, respectively. Thus, the absence of a shift in the OH band means that the synthesized $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ did not adsorb F^- . This is in good agreement with the determination results by ion chromatography, indicating there was no change for the trace concentrations of F^- and Cl^- before and after adsorption (see Fig. 8 and 9 in Section 3.2, respectively). According to the literature, phosphate adsorption by some non-LDH adsorbents^{66–70} and some LDH adsorbents^{23–26,31,33} is greatly affected by F^- or Cl^- due to their adsorption. For LDHs, considering the bonding strength between the layers and interlayer anions in aqueous solution,¹⁷ the strength of phosphates is generally higher than that of F^- and Cl^- . Since there is a large amount of phosphate in aqueous solution, the adsorption possibility of phosphate is higher than that of F^- or Cl^- . However, it is still inevitable that a small amount of F^- and Cl^- will be adsorbed,^{23–26,31,33} although this possibility is small. Thus, to further decrease this possibility, for the synthesized nano-adsorbent of $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$, CO_3^{2-} was employed as the interlayer anion. The bonding strength of CO_3^{2-} is the highest,¹⁷ much greater than that of F^- and Cl^- . During the phosphate adsorption process, a lot of CO_3^{2-} anions will be exchanged in the solution, which will further inhibit the adsorption of trace F^- and Cl^- anions. Moreover, if some OH^- anions exist in solution, the adsorption efficiencies¹⁹ will further decline due to the combined effects of increasing competition from the OH^- anion and the Coulomb repulsion between the negative-charged surface of the LDH adsorbent and F^- or Cl^- . If there is insufficient positive charge such as H^+ on the surface of the LDH adsorbent, and there are enough anions such as CO_3^{2-} and PO_4^{3-} , which have a much higher bonding strength than F^- and Cl^- , to strongly compete with F^- and Cl^- anions, the synthesized magnetic nano-adsorbent $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ should not adsorb F^- and Cl^- anions.

Fig. 6 shows the magnetic hysteresis loops of Fe_3O_4 , and $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ before and after 15 cycles of PO_4^{3-} -adsorption. Compared with the magnetic saturation value of 102 emu g^{-1} for the pure Fe_3O_4 nanoparticles, that for the as-synthesized $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ drops to 36.75 emu g^{-1}

since the non-magnetic $\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ shields the magnetic Fe_3O_4 . Even if after 15 cycles, it was still 36.47 emu g^{-1} . This value is sufficient to achieve repeated rapid magnetic extraction and separation. More importantly, it should be noted that the two loop curves before and after PO_4^{3-} -adsorption come close to coinciding in shape. This truthfully reflects that the thickness of the $\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ coating layer did not change, which indicates almost no etching and degradation occurred even after 15 cycles of adsorption, separation and desorption. Based on this, the structural stability indicated by the above Fig. 4(b), which is also the result after 15 cycles of PO_4^{3-} -adsorption, means that the two-dimensional crystalline nanostructure of $\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ and the interlayer anion CO_3^{2-} in the layered double hydroxide were both maintained rather stably. Actually, it can be seen in Fig. 5(c) that after 15 cycles of adsorption, separation and desorption, the FTIR peak intensity of CO_3^{2-} is as strong as that of the as-synthesized $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$, as seen in Fig. 5(a). This means that the content of CO_3^{2-} was almost fully recovered even after 15 cycles of PO_4^{3-} -desorption, which can provide an excellent performance for stable dephosphorization.

Fig. 7(a) and (b) show the N_2 adsorption-desorption isotherms and BJH (Barrett-Joyner-Halenda) pore diameter distribution curves of $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$, respectively. In Fig. 7(a), there is a clear hysteresis loop at a high relative pressure of $P/P_0 > 0.6$, which is a typical type IV adsorption isotherm²⁸ according to the IUPAC classification. When $P/P_0 > 0.9$, there is no saturated adsorption platform, and rapid adsorption and desorption occur in this high pressure region. This indicates that the loop can be further classified as type H3,²⁸ which means the pores in $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ are mainly mesoporous. This was verified by Fig. 7(b), where the pore size distribution is mainly in the range of 5–50 nm, with an average size of 15.1 nm and total pore volume of $0.59\text{ cm}^3\text{ g}^{-1}$. The formation of these mesoporous pores in $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ is related to the slit-shaped pores or voids created within the aggregates of platy particles.^{28,71} Generally, the

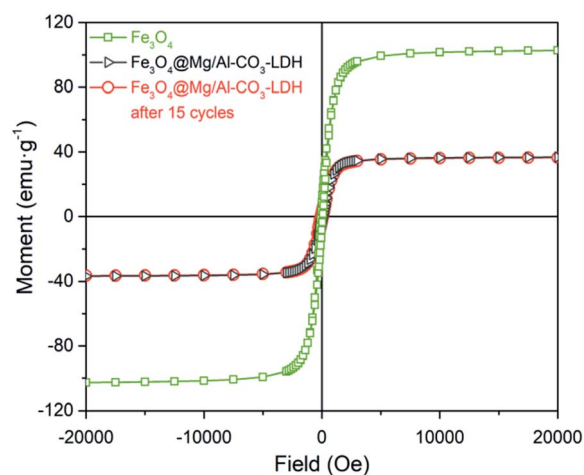


Fig. 6 Magnetic hysteresis loop analysis for Fe_3O_4 nanoparticle, and prepared $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ magnetic nano-adsorbent before and after 15 cycles of PO_4^{3-} -adsorption and regeneration.



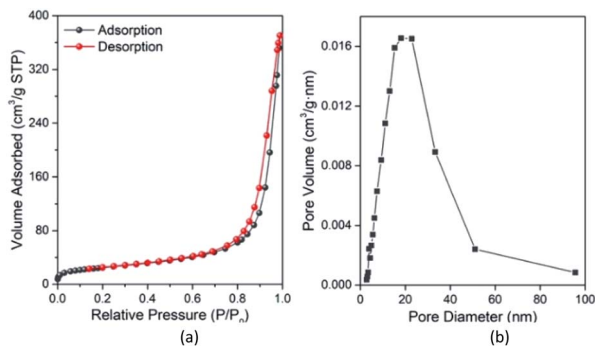


Fig. 7 N_2 adsorption-desorption isotherms (a) and Barrett-Joyner-Halenda (BJH) pore diameter distribution curve (b) of the prepared $Fe_3O_4@Mg/Al-CO_3-LDH$ magnetic nano-adsorbent.

specific surface area and total pore volume will affect the chance of contact between the adsorbent and the adsorbate, thereby affecting the adsorption effect of the adsorbent.^{28,72} According to the BET (Brunauer-Emmett-Teller) method,⁷³ the specific surface area of $Fe_3O_4@Mg/Al-CO_3-LDH$ was calculated to be $88.4 \text{ m}^2 \text{ g}^{-1}$. Thus, the hydrothermally synthesized $Fe_3O_4@Mg/Al-CO_3-LDH$ can adsorb PO_4^{3-} in solution rapidly and efficiently.

3.2 Optimized pretreatment by $Fe_3O_4@Mg/Al-CO_3-LDH$

For 80 mL solution containing $1.00 \text{ mg L}^{-1} F^-$, $1.00 \text{ mg L}^{-1} Cl^-$ and $100 \text{ mg P per L } PO_4^{3-}$ are the optimized adsorbent amount and adsorption time for $Fe_3O_4@Mg/Al-CO_3-LDH$, respectively. These optimized pretreatment conditions were utilized for the analysis of real samples, as stated in Section 4.

By using different amounts of $Fe_3O_4@Mg/Al-CO_3-LDH$ magnetic nano-adsorbent to adsorb PO_4^{3-} for the same adsorption time of 60 min, Fig. 8 shows the chromatograms, in which three chromatographic peaks at about 3 min, 7 min, 22 min correspond to F^- , Cl^- , and PO_4^{3-} , respectively. Their concentrations were calculated based on their peak area, and plotted at the top of Fig. 8. With the addition of $Fe_3O_4@Mg/Al-CO_3-LDH$ in the solution, the concentration of both F^- and Cl^- was always maintained at around 1.00 mg L^{-1} with the fluctuation of $\pm 2\%$, as shown in the top-left and top-middle of Fig. 8. This indicates that $Fe_3O_4@Mg/Al-CO_3-LDH$ will not adsorb any F^- and Cl^- anions in the solution regardless of the adsorbent amount used, which is the most important factor to determine trace F^- and Cl^- in solution. On the other hand, only a small amount of the nano-adsorbent, such as 20 and 50 mg, could make the residual PO_4^{3-} concentration decrease greatly from 100 mg P per L to 64.5 and 49.5 mg P per L , respectively, as shown in the top-right of Fig. 8. However, when the adsorbent amount was further increased to 80 mg , the residual PO_4^{3-} concentration did not further decrease since equilibrium between PO_4^{3-} and CO_3^{2-} was reached. Thus, the optimized adsorbent amount of $50 \text{ mg } Fe_3O_4@Mg/Al-CO_3-LDH$ is enough for 80 mL solution with $100 \text{ mg P per L } PO_4^{3-}$.

By using $50 \text{ mg } Fe_3O_4@Mg/Al-CO_3-LDH$ to adsorb PO_4^{3-} in 80 mL solution for different times, the residual concentration of

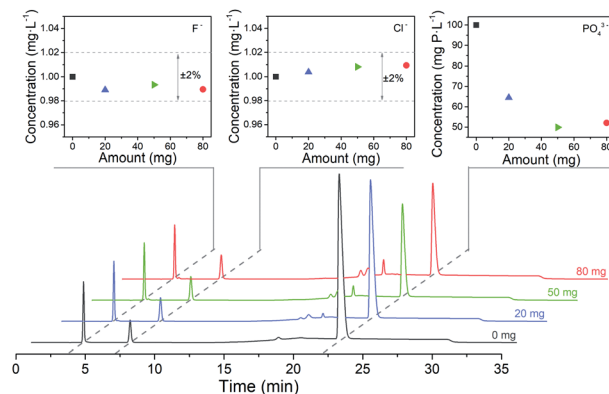


Fig. 8 Chromatograms for the solution with $1.00 \text{ mg L}^{-1} F^-$, $1.00 \text{ mg L}^{-1} Cl^-$ and $100 \text{ mg P per L } PO_4^{3-}$ using $0, 20, 50$, and $80 \text{ mg } Fe_3O_4@Mg/Al-CO_3-LDH$ magnetic nano-adsorbent, respectively. The same adsorption time of 60 min was applied.

PO_4^{3-} and F^- and Cl^- anions in the solution was determined by chromatography, as plotted in Fig. 9. According to Fig. 9(a), the concentration of both F^- and Cl^- was maintained at around 1.00 mg L^{-1} with the fluctuation of $\pm 2\%$, regardless of the adsorbent time used. Similarly, as indicated in the plots at the top of Fig. 8, $Fe_3O_4@Mg/Al-CO_3-LDH$ did not adsorb any F^- and Cl^- anions in the solution, no matter how long the interaction time. However, for PO_4^{3-} , even with fast magnetic separation immediately after the addition of $Fe_3O_4@Mg/Al-CO_3-LDH$ in the solution, the residual PO_4^{3-} concentration directly declined to 72.9 mg P per L . Also, after 2 and 5 min adsorption, it decreased to 60.3 and 52.2 mg P per L , respectively. With a further increase in the adsorption time, the adsorption of PO_4^{3-} slows down to the equilibrium stage, until the residual PO_4^{3-} concentration finally reached 48.1 mg P per L after 120 min adsorption. According to the formula for phosphate adsorption capacity,⁷⁴ as stated in Section 2.3, the capacity of $Fe_3O_4@Mg/Al-CO_3-LDH$ is 83.04 mg P per g for 120 min adsorption. Even for 5 min adsorption, it is still as high as 76.48 mg P per g . Thus, the optimized adsorption time was chosen to be $5\text{--}60 \text{ min}$ for the solution using $50 \text{ mg } Fe_3O_4@Mg/Al-CO_3-LDH$.

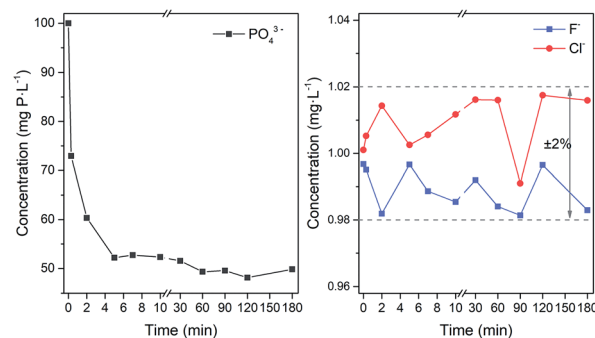


Fig. 9 Determined concentrations by chromatography for 80 mL solution with $1.00 \text{ mg L}^{-1} F^-$, $1.00 \text{ mg L}^{-1} Cl^-$ and 100 mg P per L with the adsorption time. In the adsorption experiment, the used $Fe_3O_4@Mg/Al-CO_3-LDH$ magnetic nano-adsorbent is 50 mg .

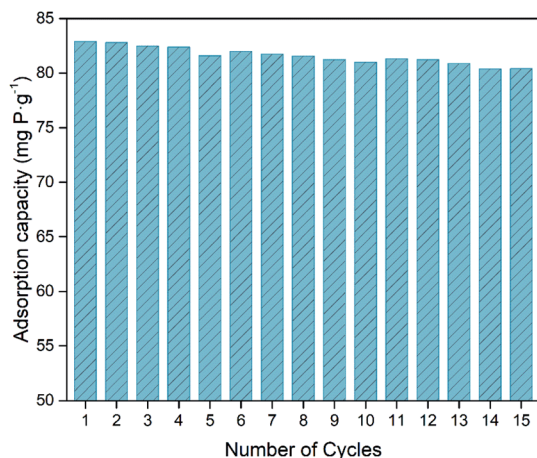


Fig. 10 Phosphate adsorption capacities of $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3$ -LDH magnetic nano-adsorbent for 15 cycles of PO_4^{3-} -adsorption-desorption, respectively. For each cycle, 80 mL solution with $1.00 \text{ mg L}^{-1} \text{ F}^-$, $1.00 \text{ mg L}^{-1} \text{ Cl}^-$ and 100 mg P per L is adsorbed by $50 \text{ mg Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3$ -LDH magnetic nano-adsorbent for 60 min. The desorption solution is 15 mL mixture of 5 wt% NaOH and 10 wt% Na_2CO_3 and the desorption time is 30 min.

3.3 Recyclability of $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3$ -LDH

The recyclability of an adsorbent is vital for its practical application,^{31,58} and the premise for recycling is the stability of its structure. The crystalline structure stability, the adsorption stability, and the coating layer stability of $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3$ -LDH after 15 cycles of PO_4^{3-} -adsorption and regeneration were

confirmed by XRD, as shown in Fig. 4(b), FTIR, as shown in Fig. 5(c), and magnetic hysteresis loop analysis, as shown in Fig. 6, respectively.

To evaluate the recyclability of the $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3$ -LDH magnetic nano-adsorbent, the phosphate adsorption capacities were determined for each cycle and shown in Fig. 10, where the 60 min adsorption, 30 min desorption and regeneration processes are stated in Section 2.3. The initial capacity of 83.04 mg P per g calculated from Fig. 9 was used for the as-synthesized $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3$ -LDH. For the subsequent cycles, the phosphate adsorption capacity decreased but very slowly. Even after 15 desorption-adsorption cycles, the capacity was still as high as 80.41 mg P per g , which is only 3.2% lower than the initial 83.04 mg P per g . Among the 15 cycles, the maximum decrease occurred in the 5th cycle, but not more than 1%, and the average decrease was as low as $\sim 0.2\%$. This clearly indicates that the synthesized $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3$ -LDH has excellent recyclability and stability, maintaining high phosphate adsorption capacities even after manifold cycles.

Table 1 presents the phosphate adsorption capacity, adsorption time, and recycle number of various magnetic adsorbents. These adsorbents, LDH adsorbents with interlayer anion and non-LDH adsorbents, can all be used to efficiently adsorb PO_4^{3-} in solution. Compared with most of the adsorbents, the phosphate capacity per unit mass of the synthesized $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3$ -LDH is as high as 76.48 mg P per g , higher than $1.8675\text{--}36.9 \text{ mg P per g}$, but somewhat lower^{25,31,69,74} than $128\text{--}252.88 \text{ mg P per g}$ of these four adsorbents. However, they used about 360–4320 min to adsorb phosphates in solution. It

Table 1 Comparison of the adsorption time, adsorption capacity and the number of reuse cycles by various magnetic adsorbents for the adsorption of the PO_4^{3-} phosphate group

Adsorbent	Interlayer anion for LDH ^g	Adsorption time (min)	Adsorption capacity ^d (mg P per g)	Cycle no.	Ref.
ZnFeZr adsorbent@ $\text{Fe}_3\text{O}_4/\text{SiO}_2$	Cl^-	60		20	23
Magnetic Fe/Mn oxide composites (TS-N)	Cl^-	90	26.0		24
$\text{Fe}_3\text{O}_4/\text{Zn}-\text{Al}-\text{Fe}-\text{La}-\text{LDH}$	Cl^- and SO_4^{2-}	1440	169.5	4 ^b	25
$\text{Fe}_3\text{O}_4@\text{Zn}-\text{Al}-\text{LDH}$	CO_3^{2-}	60	36.9		26
$\text{Fe}_3\text{O}_4@\text{Mg}-\text{Al}-\text{LDH}$			31.7		
$\text{Fe}_3\text{O}_4@\text{Ni}-\text{Al}-\text{LDH}$			26.5		
$\text{Fe}/\text{CaCO}_3\text{-PVA}$	Non-LDH		16.7		75
$\text{Fe}/\text{MgCO}_3\text{-PVA}$			16.3		
$\text{Fe}_3\text{O}_4@\text{SiO}_2\text{-CeO}_2$	Non-LDH	1440	10.8	2 ^c	76
$\text{Ce-Ti}@\text{Fe}_3\text{O}_4$	Non-LDH	1440	11.10		66
Carboxylated chitosan- Fe_3O_4	Non-LDH	60	1.8675		67
La-chitosan magnetic spheres	Non-LDH	300	27.78		68
$\text{ZrO}_2/\text{Fe}_3\text{O}_4$	Non-LDH	1440	29.5		77
Magnetic <i>Caragana korshinskii</i> biochar/Mg-Al-LDH	Cl^-	720	252.88	5 ^d	31
Fe_3O_4 @alkali-treated calcium-silicate	Non-LDH	4320	128	2 ^e	69
Fe_3O_4 @gelatin encapsulated hydrotalcite	CO_3^{2-}	40	32.73	4 ^f	33
NrGO/ Fe_3O_4	Non-LDH	360	135.3	5	74
Humic acid coated magnetite nanoparticles	Non-LDH	180	28.9		70
$\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3$ -LDH	CO_3^{2-}	5	76.48	15	This work

^a Adsorption capacity of phosphate, $Q_e = (C_0 - C_e)V/m$, where C_0 and C_e are the initial and equilibrium phosphate concentration in mg L^{-1} , V is the volume of phosphate solution in L, and m is the dry weight of the adsorbent in g. ^b The adsorption capacity decreased to 31 mg g^{-1} after 4 cycles.

^c The adsorption capacity decreased to 25.71 mg g^{-1} after 5 cycles. ^d The adsorption efficiency was reduced to 70.01% after 4 cycles. ^e The adsorption capacity decreased to 4.8 mg g^{-1} after 2 cycles. ^f The adsorption capacity decreased to 20.2 mg g^{-1} after 2 cycles. ^g The information is summarized from the description of preparation processes, or FTIR, XPS and other characterization in refs.



should be noted that the capacity is related to the adsorption time used. Even if the adsorption time used is as fast as 5 min, which is 1/8–1/288 of the reported times listed in Table 1, the adsorption capacity of 76.48 mg P per g for $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ is high enough to adsorb PO_4^{3-} rapidly and efficiently so as to determine F^- and Cl^- without serious interference due to PO_4^{3-} . In the case of the recycle number, which is one of the vital properties for the recyclability of an adsorbent, it is 15 cycles for $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$, more than the reported 2–5 cycles.²³ but there was no information about the phosphate adsorption capacity. According to Table 1, if only considering magnetic LDHs with a CO_3^{2-} interlayer anion, $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ behaves very well to adsorb PO_4^{3-} in solution, with four times greater cycle number and two times greater phosphate adsorption capacity.

4 Analysis of real samples

Phosphate and fluorophosphate laser glasses contain high PO_4^{3-} and a certain amount of various monovalent, divalent, trivalent metal cations. The leaching solutions from these glasses were determined before and after adsorption pretreatment using the $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ magnetic nano-adsorbent, and the chromatograms are shown in Fig. 11. As seen in Fig. 11(a) for the phosphate (P_2O_5 molar ratio of both N31 and N41 glasses is close to 60%) with high PO_4^{3-} but low F^- and Cl^- , the strong peak at 22.36 min due to PO_4^{3-} is too overloaded, and thus it seems to be a leading peak with 100 μS conductivity. After the adsorption pretreatment, the 22.36 min peak shape became normal and its intensity decreased greatly

to 10 μS . This indicates that $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ could efficiently adsorb PO_4^{3-} in the multi-ion leaching solution in a short time of only 5 min. On the other hand, $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ did not adsorb any F^- or Cl^- . The peaks at 3.79 and 7.34 min are due to F^- and Cl^- , respectively, and their intensities did not change after the adsorption pretreatment. As seen in Fig. 11(b) for the fluorophosphate with a high F^- and PO_4^{3-} content but low Cl^- , the 22.36 min PO_4^{3-} peak almost disappeared after the adsorption pretreatment by $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ for 5 min. The strong F^- peak at 3.79 min and the weak Cl^- peak at 7.34 min did not change after the pretreatment. Regardless of a high or low PO_4^{3-} content in a multi-ion solution, the synthesized $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ magnetic nano-adsorbent can adsorb and extract PO_4^{3-} rapidly. Also, regardless of a high or low F^- or Cl^- content in a multi-ion solution, the addition and extraction of the nano-adsorbent did not result in any change in the contents of F^- or Cl^- . These two facts determine the usefulness of the nano-adsorbent for specific applications, *i.e.* the removal of PO_4^{3-} , and especially the determination of F^-/Cl^- after removing PO_4^{3-} in a multi-ion solution. By using the $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ adsorption pretreatment, the pretreated solution can be utilized for other determination techniques or methods since there will be no serious interference from PO_4^{3-} in the solution. Considering chromatography, the determination time for the accurate determination of F^- and Cl^- can be greatly shortened after removing PO_4^{3-} . More importantly, without being affected by PO_4^{3-} and fully retaining trace F^- and Cl^- , a continuous analysis or on-line test can be done during processes in the laboratory and industry in fields such as pharmaceuticals and biomaterials. If PO_4^{3-} is not removed from a PO_4^{3-} -rich solution, the next injection must not be allowed.¹¹

By chromatography, Table 2 lists the determined results of F^- and Cl^- for various real samples, such as a certified reference ore material (GBW07108 containing F, Cl and P, as well as 66 other elements), silicate glass, fluorophosphate glass, phosphate laser glasses, and environmental water samples. Specifically, 80 mL sample solution was pretreated using $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ under the optimized conditions. For the certified ore sample, the determined values of 0.395 and 0.0071 mg L^{-1} are very close to the certified values of 0.406 and 0.0078 mg L^{-1} for F^- and Cl^- , respectively. After determining F^- and Cl^- for the other samples, a certain amount of F^- and Cl^- standard solutions was added, *i.e.* the added content was 1.00 mg L^{-1} . Subsequently, the contents of F^- and Cl^- in the solution re-pretreated by $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ were measured again. Accordingly, the spiked recoveries were calculated. As seen in Table 2, these spiked recoveries were all within an acceptable range of 95.7–104.9%. Thus, the above determinations prove the accuracy to determine F^- and Cl^- in multi-ion solutions pretreated by the synthesized $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ magnetic nano-adsorbent.

It should be noted that the pH values of real sample solutions may vary from sample to sample, especially when dissolving solid samples by acid or alkali. The pH value of the solution will affect the existing form of phosphate anions,^{17,26,29} such as PO_4^{3-} , HPO_4^{2-} and H_2PO_4^- . Thus, two phosphate

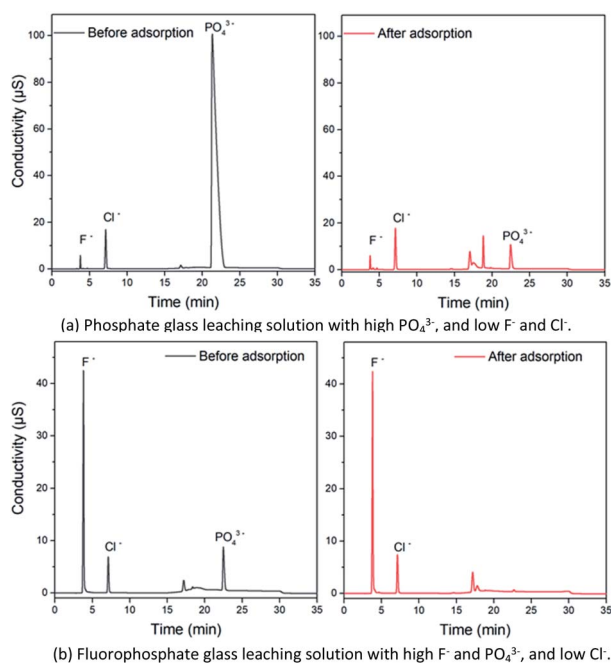


Fig. 11 Chromatograms for the leaching solutions of phosphate glass (a) and fluorophosphate glass (b) before and after 5 min adsorption by 50 mg $\text{Fe}_3\text{O}_4@\text{Mg}/\text{Al}-\text{CO}_3\text{-LDH}$ magnetic nano-adsorbent.



Table 2 Determination of F^- and Cl^- anions in a certified reference ore sample, silicate glasses, fluorophosphate glasses, phosphate glasses and river water samples by ion chromatography after adsorption pretreatment by $Fe_3O_4@Mg/Al-CO_3-LDH$

Sample	F^-			Cl^-		
	Added ($mg\ L^{-1}$)	Found ($mg\ L^{-1}$)	Recovery (%)	Added ($mg\ L^{-1}$)	Found ($mg\ L^{-1}$)	Recovery (%)
GBW07108 ^a	0.406 ^b	0.395	97.3	0.078 ^b	0.071	91.0
	1.00	1.444	104.9	1.00	1.092	102.1
Silicate glass	0	9.970	—	0	0.083	—
	1.00	10.927	95.7	1.00	1.069	98.6
Fluorophosphate glass	0	21.972	—	0	0.066	—
	1.00	23.012	104.0	1.00	1.060	99.4
N31 phosphate glass, pot melting	0	0.744	—	0	0.251	—
	1.00	1.738	99.4	1.00	1.245	99.4
N41 phosphate glass, pot melting	0	0.814	—	0	0.585	—
	1.00	1.800	98.6	1.00	1.558	97.3
N41 phosphate glass, continuous melting	0	1.267	—	0	0.459	—
	1.00	2.277	101.0	1.00	1.501	104.2
River water	0	0.153	—	0	7.351	—
	1.00	1.150	99.7	1.00	8.338	98.7

^a The certified reference ore samples were approved by the General Administration of Quality Supervision, Inspection and Quarantine of the People's Republic of China, which were mainly composed of silicate, carbonate and oxide of Al, Fe, Mg and Ca. ^b The certified content of F^- and Cl^- in the certified reference material GBW07108.

solutions were obtained by dissolving high purity Na_3PO_4 or NaH_2PO_4 in deionized water without adding any acid and alkali, and treated with the magnetic nano-adsorbent of $Fe_3O_4@Mg/Al-CO_3-LDH$, and their ion chromatogram peaks due to phosphate greatly decreased. The large decrease indicates the effective adsorption of both Na_3PO_4 and NaH_2PO_4 solutions. This implies that no matter the existing form of phosphate anions, such as PO_4^{3-} and $H_2PO_4^-$, the synthesized $Fe_3O_4@Mg/Al-CO_3-LDH$ can adsorb them efficiently. On the other hand, the pH value of real sample solutions as in the above applications is not adjusted by acid and alkali to avoid any further disturbance in the trace determination of F^- and Cl^- by ion chromatography.

5 Conclusion

Using the urea hydrothermal method, the layered double hydroxide $Mg/Al-CO_3-LDH$ was synthesized and aggregated as small crystal plates on Fe_3O_4 nanoparticles, which retained its original crystalline state with high magnetism. The magnetic saturation value of $36.47\ emu\ g^{-1}$ was sufficient to achieve rapid magnetic extraction-separation during PO_4^{3-} -adsorption by $Fe_3O_4@Mg/Al-CO_3-LDH$. As a recyclable magnetic nano-adsorbent, its structural stability was confirmed after 15 regeneration cycles for PO_4^{3-} -adsorption and desorption. The vibrations of the CO_3^{2-} and PO_4^{3-} groups, and the $Mg-OH$, $Al-OH$, and $Mg-O-Al$ bonds indicated that the mechanism for the adsorption of PO_4^{3-} by $Fe_3O_4@Mg/Al-CO_3-LDH$ is related to the anion exchange between the interlayer anion CO_3^{2-} and PO_4^{3-} in solution, the LDH surface electrostatic adsorption for PO_4^{3-} in solution, and the ligand exchange between LDH and PO_4^{3-} in solution. Since mesoporous pores are created within the aggregates of small crystal plates during the synthesis of $Fe_3O_4@Mg/Al-CO_3-LDH$, its large specific surface area and total pore volume are $88.4\ m^2\ g^{-1}$ and $0.59\ cm^3\ g^{-1}$, respectively.

These endow the magnetic nano-adsorbent with a high phosphate adsorption capacity of $83.04\ mg\ P\ per\ g$ for 120 min adsorption, or still up to $76.48\ mg\ P\ per\ g$ for rapid 5 min adsorption. Even after 15 desorption-adsorption cycles, the capacity was still as high as $80.41\ mg\ P\ per\ g$ with only a decline by 3.2%. Compared with other magnetic LDHs with CO_3^{2-} , the synthesized $Fe_3O_4@Mg/Al-CO_3-LDH$ exhibited very good ability to adsorb PO_4^{3-} , with four times greater cycle number, two times greater phosphate adsorption capacity, and eight-twelve times less adsorption time. More importantly, regardless of a high or low F^- or Cl^- content, and regardless of the used amount and adsorption time of $Fe_3O_4@Mg/Al-CO_3-LDH$, the addition and extraction of the nano-adsorbent did not result in any change in the contents of F^- and Cl^- in a multi-ion solution. Thus, the usefulness of the synthesized $Fe_3O_4@Mg/Al-CO_3-LDH$ is concentrated on two specific applications, the removal of PO_4^{3-} , and especially the accurate determination of F^- and Cl^- after the removal of PO_4^{3-} . By optimizing the nano-adsorbent amount and adsorption time, $Fe_3O_4@Mg/Al-CO_3-LDH$ was successfully utilized to adsorb PO_4^{3-} rapidly and determine F^-/Cl^- accurately by ion chromatography for real samples such as certified reference ore materials, phosphate laser glass, fluorophosphate glass, silicate glass and environmental water samples. Currently, these applications are greatly beneficial for product quality monitoring for extremely hazardous F^- and Cl^- to protect the ecological environment. On the other hand, excess P will lead to widespread eutrophication in aquatic environments, in which algal blooms are also harmful towards human health due to cyanotoxins.⁷⁸ With the further development and progress on the adsorption capacity, adsorption recovery velocity, and adsorption kinetics,^{78,79} studies will be devoted to online applications and widening the scope of these significant methods using LDH adsorbents, which will contribute immensely to environmental protection.



Conflicts of interest

There are no conflicts to declare.

Acknowledgements

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References

- 1 F. Vasconcelos, S. Cristol, J. Paul, L. Montagne, F. Mauri and L. Delevoye, *Magn. Reson. Chem.*, 2010, **48**, S142–S150.
- 2 A. Salama, *Int. J. Biol. Macromol.*, 2019, **127**, 606–617.
- 3 H. Parham and N. Rahbar, *Talanta*, 2009, **80**, 664–669.
- 4 V. P. Kolotov and E. A. Arafa, *J. Radioanal. Nucl. Chem.*, 1993, **172**, 357–362.
- 5 P. Venkateswarlu, *Anal. Chim. Acta*, 1992, **262**, 33–40.
- 6 Z. Ni, Z. Rao and M. Li, *Anal. Chim. Acta*, 1996, **334**, 177–182.
- 7 P. Bermejo-Barrera, A. Moreda-Piñeiro and A. Bermejo-Barrera, *Spectrochim. Acta, Part B*, 2002, **57**, 327–337.
- 8 U. Nygren, H. Ramebäck, D. C. Baxter and C. Nilsson, *J. Anal. At. Spectrom.*, 2005, **20**, 529.
- 9 F. S. Stover, *J. Chromatogr. A*, 2002, **956**, 121–128.
- 10 L. E. Vanatta, D. E. Coleman and A. Woodruff, *J. Chromatogr. A*, 2003, **997**, 269–278.
- 11 E. Kaiser, J. S. Rohrer and K. Watanabe, *J. Chromatogr. A*, 1999, **850**, 167–176.
- 12 L. Al Attar, M. Al-Oudat, K. Shamali, B. A. Ghany and S. Kanakri, *Environ. Technol.*, 2012, **33**, 143–152.
- 13 W. Qiao, R. Liu, Z. Li, X. Luo, B. Huang, Q. Liu, Z. Chen, J. Tsoi, Y. X. Su, K. Cheung, J. P. Matinlinna, K. Yeung and Z. Chen, *Biomater. Sci.*, 2018, **6**, 2951–2964.
- 14 D. Štepec and M. Ponikvar-Svet, *Acta Chim. Slov.*, 2019, **66**, 255–275.
- 15 F. L. Theiss, G. A. Ayoko and R. L. Frost, *Appl. Surf. Sci.*, 2016, **383**, 200–213.
- 16 V. Rives and M. Angeles Ulbarri, *Coord. Chem. Rev.*, 1999, **181**, 61–120.
- 17 Q. Zhang, F. Ji, T. Zhao, Q. Shen, D. Fang, L. Kuang, L. Jiang and S. Ding, *Appl. Clay Sci.*, 2019, **174**, 159–169.
- 18 M. P. Bernardo and C. Ribeiro, *Mater. Res.*, 2018, **21**, e20171001.
- 19 F. Li, J. Jin, Z. Shen, H. Ji, M. Yang and Y. Yin, *J. Hazard. Mater.*, 2020, **388**, 121734.
- 20 C. V. Luengo, M. A. Volpe and M. J. Avena, *J. Environ. Chem. Eng.*, 2017, **5**, 4656–4662.
- 21 H. Hatami, A. Fotovat and A. Halajnia, *Appl. Clay Sci.*, 2018, **152**, 333–341.
- 22 S. M. Ashekuzzaman and J. Jiang, *Process Saf. Environ. Prot.*, 2017, **107**, 454–462.
- 23 A. Drenkova-Tuhtan, M. Schneider, M. Franzreb, C. Meyer, C. Gellermann, G. Sextl, K. Mandel and H. Steinmetz, *Water Res.*, 2017, **109**, 77–87.
- 24 C. Chon, D. Cho, I. Nam, J. Kim and H. Song, *J. Soils Sediments*, 2018, **18**, 946–956.
- 25 W. Qiao, H. Bai, T. Tang, J. Miao and Q. Yang, *Colloids Surf., A*, 2019, **577**, 118–128.
- 26 L. Yan, K. Yang, R. Shan, T. Yan, J. Wei, S. Yu, H. Yu and B. Du, *J. Colloid Interface Sci.*, 2015, **448**, 508–516.
- 27 R. Chitrakar, S. Tezuka, J. Hosokawa, Y. Makita, A. Sonoda, K. Ooi and T. Hirotsu, *J. Colloid Interface Sci.*, 2010, **349**, 314–320.
- 28 K. S. Triantafyllidis, E. N. Peleka, V. G. Komvokis and P. P. Mavros, *J. Colloid Interface Sci.*, 2010, **342**, 427–436.
- 29 F. Hu, M. Wang, X. Peng, F. Qiu, T. Zhang, H. Dai, Z. Liu and Z. Cao, *Colloids Surf., A*, 2018, **555**, 314–323.
- 30 J. Zhou, S. Yang, J. Yu and Z. Shu, *J. Hazard. Mater.*, 2011, **192**, 1114–1121.
- 31 Q. Cui, G. Jiao, J. Zheng, T. Wang, G. Wu and G. Li, *RSC Adv.*, 2019, **9**, 18641–18651.
- 32 B. Bekele, L. Lundehøj, N. D. Jensen, U. G. Nielsen and C. Forano, *Appl. Clay Sci.*, 2019, **176**, 49–57.
- 33 I. A. Kumar and N. Viswanathan, *J. Environ. Chem. Eng.*, 2018, **6**, 208–217.
- 34 M. Ogawa and H. Kaiho, *Langmuir*, 2002, **18**, 4240–4242.
- 35 F. Yang, S. Sun, X. Chen, Y. Chang, F. Zha and Z. Lei, *Appl. Clay Sci.*, 2016, **123**, 134–140.
- 36 M. M. Rao, B. R. Reddy, M. Jayalakshmi, V. S. Jaya and B. Sridhar, *Mater. Res. Bull.*, 2005, **40**, 347–359.
- 37 S. Ma, C. Fan, G. Huang, Y. Li, X. Yang and K. Ooi, *Eur. J. Inorg. Chem.*, 2010, **2010**, 2079–2083.
- 38 S. Li, Y. Shen, D. Liu, L. Fan, X. Zheng and J. Yang, *Compos. Interfaces*, 2012, **19**, 489–498.
- 39 J. Wang, D. Li, X. Yu, M. Zhang and X. Jing, *Colloid Polym. Sci.*, 2010, **288**, 1411–1418.
- 40 T. Hibino and H. Ohya, *Appl. Clay Sci.*, 2009, **45**, 123–132.
- 41 B. Li, J. He and D. G. Evans, *Chem. Eng. J.*, 2008, **144**, 124–137.
- 42 P. Zhang, T. Yamaguchi, B. N. Nair, K. Miyajima and G. M. Anilkumar, *RSC Adv.*, 2014, **4**, 41051–41058.
- 43 M. Yang, J. Liu, Z. Chang, G. R. Williams, D. O'Hare, X. Zheng, X. Sun and X. Duan, *J. Mater. Chem.*, 2011, **21**, 14741–14746.
- 44 S. Radha and A. Navrotsky, *J. Phys. Chem. C*, 2014, **118**, 29836–29844.
- 45 B. Li and J. He, *J. Phys. Chem. C*, 2008, **112**, 10909–10917.
- 46 G. K. Sarma and M. H. Rashid, *J. Chem. Eng. Data*, 2018, **63**, 2957–2965.
- 47 X. Lei, W. Lu, Q. Peng, H. Li, T. Chen, S. Xu and F. Zhang, *Appl. Catal., A*, 2011, **399**, 87–92.
- 48 X. Yuan, Y. Wang, J. Wang, C. Zhou, Q. Tang and X. Rao, *Chem. Eng. J.*, 2013, **221**, 204–213.
- 49 B. Zhu, L. Chen, T. Yan, J. Xu, Y. Wang, M. Chen and H. Jiang, *Water Sci. Technol.*, 2018, **78**, 1179–1188.
- 50 P. Zhang, T. He, P. Li, X. Zeng and Y. Huang, *Langmuir*, 2019, **35**, 13562–13569.
- 51 Y. Zhang, L. Wang, L. Zou and D. Xue, *J. Cryst. Growth*, 2010, **312**, 3367–3372.
- 52 L. Bo, Q. Li, Y. Wang, L. Gao, X. Hu and J. Yang, *Environ. Prog. Sustainable Energy*, 2016, **35**, 1420–1429.



- 53 M. N. Sepehr, K. Yetilmezsoy, S. Marofi, M. Zarrabi, H. R. Ghaffari, M. Fingas and M. Foroughi, *J. Taiwan Inst. Chem. Eng.*, 2014, **45**, 2786–2800.
- 54 M. R. Berber, I. H. Hafez, K. Minagawa, M. Katoh, T. Mori and M. Tanaka, *J. Mol. Struct.*, 2013, **1033**, 104–112.
- 55 H. Zhang, G. Zhang, X. Bi and X. Chen, *J. Mater. Chem. A*, 2013, **1**, 5934–5942.
- 56 U. Costantino, F. Marmottini, M. Nocchetti and R. Vivani, *Eur. J. Inorg. Chem.*, 1998, 1439–1446.
- 57 M. Shao, F. Ning, J. Zhao, M. Wei, D. G. Evans and X. Duan, *J. Am. Chem. Soc.*, 2011, **134**, 1071–1077.
- 58 K. Mandel, A. Drenkova-Tuhtan, F. Hutter, C. Gellermann, H. Steinmetz and G. Sextl, *J. Mater. Chem. A*, 2013, **1**, 1840–1848.
- 59 N. Ammavasi and R. Mariappan, *J. Environ. Chem. Eng.*, 2018, **6**, 5645–5654.
- 60 R. Zeng, Z. Liu, F. Zhang, S. Li, Q. He, H. Cui and E. Han, *Trans. Nonferrous Met. Soc. China*, 2015, **25**, 1917–1925.
- 61 J. Shou, C. Jiang, F. Wang, M. Qiu and Q. Xu, *J. Mol. Liq.*, 2015, **207**, 216–223.
- 62 S. Arghavani-Beydokhti, M. Rajabi and A. Asghari, *Anal. Methods*, 2018, **10**, 1305–1314.
- 63 W. H. R. Shaw and J. J. Bordeaux, *J. Am. Chem. Soc.*, 1955, **77**, 4729–4733.
- 64 V. Siva Kumar, A. H. Padmasri, C. V. V. Satyanarayana, I. Ajit Kumar Reddy, B. David Raju and K. S. Rama Rao, *Catal. Commun.*, 2006, **7**, 745–751.
- 65 F. Loretta, S. Perumal and S. Ramalingom, *Asian J. Chem.*, 2013, **25**, 1921–1926.
- 66 A. A. Markeb, L. A. Ordosgoitia, A. Alonso, A. Sánchez and X. Font, *RSC Adv.*, 2016, **6**, 56913–56917.
- 67 E. Mohammadi, H. Daraei, R. Ghanbari, S. Dehestani Athar, Y. Zandsalimi, A. Ziaee, A. Maleki and K. Yetilmezsoy, *J. Mol. Liq.*, 2019, **273**, 116–124.
- 68 R. Cheng, L. Shen, Y. Zhang, D. Dai, X. Zheng, L. Liao, L. Wang and L. Shi, *Water*, 2018, **10**, 1659.
- 69 D. Jiang, Y. Amano and M. Machida, *J. Environ. Chem. Eng.*, 2017, **5**, 4229–4238.
- 70 M. Rashid, N. T. Price, M. Á. Gracia Pinilla and K. E. O'Shea, *Water Res.*, 2017, **123**, 353–360.
- 71 O. Mrózek, P. Ecorchard, P. Vomáčka, J. Ederer, D. Smržová, M. Š. Slušná, A. Machálová, M. Nevalová and H. Beneš, *Appl. Clay Sci.*, 2019, **169**, 1–9.
- 72 M. Gilanizadeh and B. Zeynizadeh, *New J. Chem.*, 2018, **42**, 8553–8566.
- 73 N. Passe-Coutrin, S. Altenor, D. Cossement, C. Jean-Marius and S. Gaspard, *Microporous Mesoporous Mater.*, 2008, **111**, 517–522.
- 74 M. Y. Akram, S. Ahmed, L. Li, N. Akhtar, S. Ali, G. Muhyodin, X. Zhu and J. Nie, *J. Environ. Chem. Eng.*, 2019, **7**, 103137.
- 75 C. Han, J. Lalley, N. Iyanna and M. N. Nadagouda, *Mater. Chem. Phys.*, 2017, **198**, 115–124.
- 76 J. Liu, J. Cao, Y. Hu, Y. Han and J. Zhou, *Water Sci. Technol.*, 2017, **76**, 2867–2875.
- 77 J. Wang, X. Shao, J. Liu, Q. Zhang, J. Ma and G. Tian, *Mater. Chem. Phys.*, 2020, **249**, 123024.
- 78 F. Yang, S. Zhang, Y. Sun, D. C. W. Tsang, K. Cheng and Y. S. Ok, *J. Hazard. Mater.*, 2019, **365**, 665–673.
- 79 D. Fang, X. Zhuang, L. Huang, Q. Zhang, Q. Shen, L. Jiang, X. Xu and F. Ji, *Sci. Total Environ.*, 2020, **725**, 138490.

