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Enhanced stability and ultrahigh activity of amorphous ripple nanostructured Ni-doped Fe oxyhydroxide electrode toward synergistic electrocatalytic water splitting†

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The development of high-performance catalysts for oxygen-evolution reaction (OER) is paramount for cost-effective conversion of renewable electricity to fuels and chemicals. Here we report, highly efficient, ultra-durable and earth-abundant Ni@Fe-NP electrocatalysts developed by solvothermal method for oxygen evolution reaction (OER). The newly developed oxygen electrode show prolonged stability and high catalytic-activity in line with water oxidation keeping alkaline condition which requires overpotential of only 211 mV at current density of 10 mA cm⁻². Collectively, the as-prepared amorphous Ni@Fe-NP rippled nanostructured electrode is the most effective oxygen evolution electrode in alkaline solution. Therefore, this study will offer exciting new avenues for designing self-supported electrode materials towards water splitting and other applications.

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1. Introduction

The scalable production of renewable energy by electrolytic water-splitting to hydrogen fuels is an alternative for replacing conventional fossil fuels. Therefore, efficient OER catalysts are urgently required to reduce the energy barrier to enhance the energy efficiency. A large overpotential (η) is required to generate H₂ which leads to slow oxygen evolution kinetics. Despite current improvement in the progress of heterogeneous-catalysts to negotiate OER (2H₂O → O₂(g) + 4H⁺(aq) + 4e⁻; E° (O₂/H₂O) = 1.23 V *versus* RHE; E° – standard potential and RHE – reversible hydrogen electrode)^{1–4} commercialization has been held up by absence of low-cost catalytic materials and also, these materials show high current densities (j) of >0.5 A cm⁻² at low η of <0.3 V over prolonged time periods. Metal oxides are the most durable and active water oxidation catalysts,^{1,2} so far, RuO₂ and IrO₂ are the benchmark OER catalysts, owing to their high catalytic activity,^{5,6} a myriad of perovskite^{3,7} and spinel⁸ solids have shown to be efficient catalysts. The low-cost transition metal nickel-iron (Ni-Fe) composites based electrocatalyst are promising to overcome the multistep electron transfer in OER reaction.^{9–23} In nickel-iron composites, nickel acts as active center of oxygen evolution reaction and iron increases the electrical conductivity.^{24,25}

The enhancing catalytic activity of iron is undeniable,^{26–31} but it show conductivity increment of the film.¹⁷ Most of the

reported OER catalyst are carbon-based powder materials which are coated on the conductive substrates such as GC or Ni foam using Nafion.³² However, these carbon based materials are unsuitable for OER due to large water electrolysis with higher positive cell voltage (2.0 V). So, it is required to develop alternative metal-rich nanomaterials as OER electrocatalyst with high activity and stable in the overall water splitting cell. Thus, amorphous nanomaterials are a new platform for the synthesis of advanced OER electrocatalyst.³³ A very strong synergistic effect upon the incorporation of Fe into Ni, even in a small amount, enhanced the catalytic activity.³⁴ Higher nickel oxidation state would be the additional beneficial to enhance the catalytic activity because increase of Ni–O bond.^{35–37} The Fe⁴⁺ sites are at edges or defects in NiOOH structure and enhancing the active site of the catalyst, which enhances the oxyl character and promotes O–O bond formation.^{38–46} Hence, the amorphous nanomaterials have moral prospects in the applications of OER since they enhanced the electrocatalytic activity while maintaining the stability.

Herein, we introduced an easy, ecofriendly and low-cost solvothermal method to produce mixed amorphous nanomaterials Ni@Fe-NP as an efficient and durable electrocatalyst for OER reaction. The solvothermal method offer amorphous nanomaterial with very high surface area, integrity, electrical conductivity and highest OER activity in alkaline solution. The prepared amorphous nanomaterial catalyst coated on the nickel foam electrode exhibits excellent OER electrocatalytic activity, long term stability with low overpotentials of 211 mV at current density of 10 mA cm⁻² and had a long term conventional

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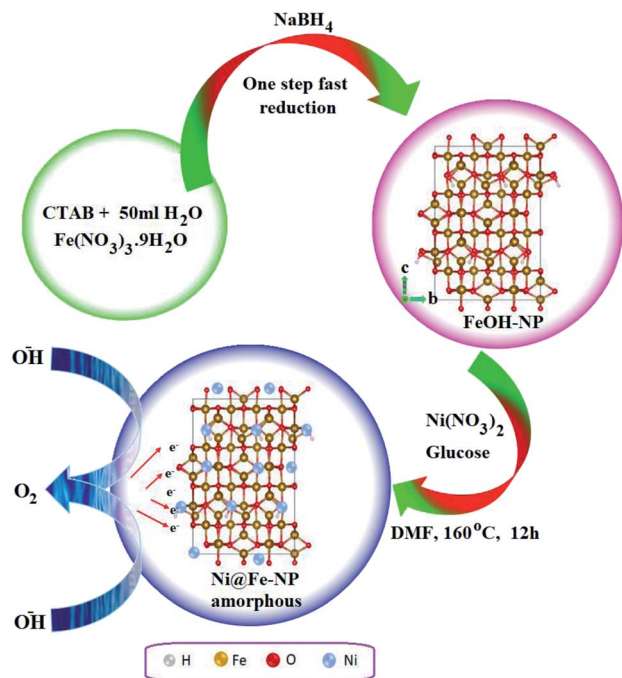


Fig. 1 Schematic route for amorphous Ni@Fe-NP.

alkaline electrolyzer stability over 150 h at 10 mA cm^{-2} . The outstanding OER performance of Ni@Fe-NP was close to the state of the art precious catalyst RuO_2 and IrO_2 .

2. Experimental section

2.1 Materials and methods

KOH, glucose, $\text{Ni}(\text{NO}_3)_2$, $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$, toluene and isopropanol were purchased from SAMCHUN chemicals; HCl was purchased from JUNSEI chemicals, NaBH_4 , CTAB, IrO_2 , 20%-Pt/C, Nafion® solution in lower aliphatic alcohol was purchased from Sigma Aldrich.

2.2 Synthesis of amorphous Ni@Fe nanoparticles

About 1 g $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$ and 1 g CTAB in 40 mL water was added to 0.2 g NaBH_4 in 10 mL H_2O for 10 min and stirring was continued for 30 min. The formed Fe-NP was centrifuged, washed and dried under vacuum. The weight ratio of nickel and Fe-NP was determined to be 3/7, 5/5 and 7/3 by adjusting the amount of nickel(II) nitrate and Fe-NP. The aforementioned prepared Fe nanoparticles was dispersed in 20 mL DMF, a small amount of nickel precursor $\text{Ni}(\text{NO}_3)_2$ and glucose (800 mg) was added to the dispersion. Then, the mixture was sonicated for 10 min and heated to 160°C (12 h) with stirring and cooled. The reaction mixture was centrifuged with ethanol/toluene mixture and acetone/toluene mixture and dried (60°C for 24 h). The resulting material was brown in color suggest the formation of fine particle with amorphous Ni@Fe-NP.

2.3 Characterization

The morphology of Ni@Fe-NP was determined using Hitachi S-4700 SEM (scanning electron microscope) operated at 10 kV

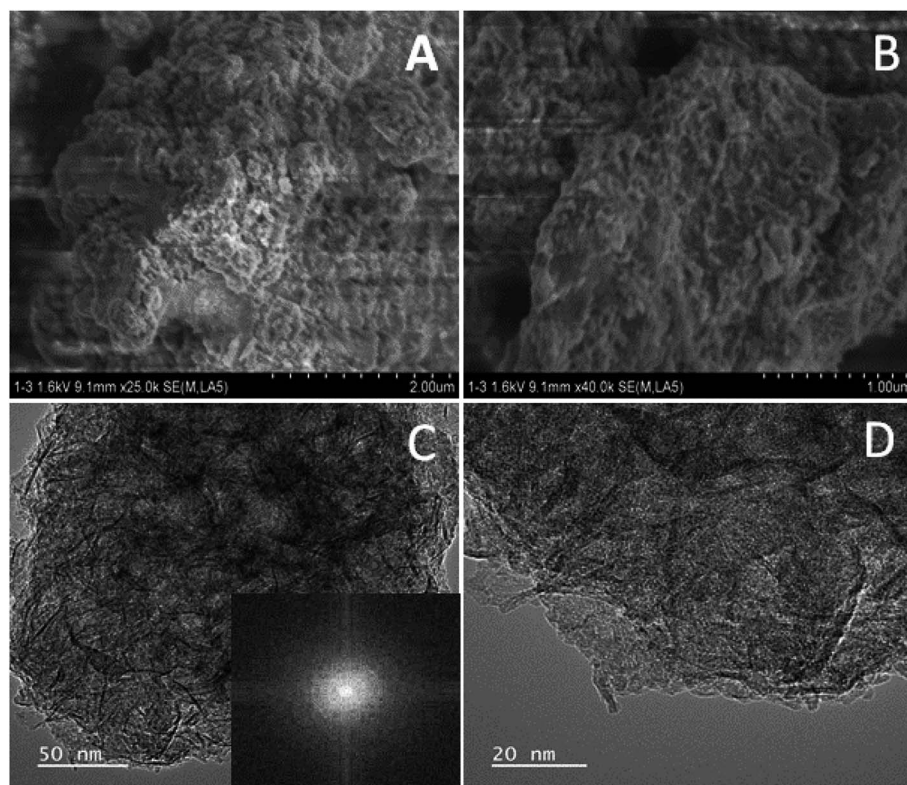


Fig. 2 SEM images (A & B) and TEM images of amorphous Ni@Fe-NP (C & D) (inset: selected area electron diffraction pattern).



and with EM 912 omega TEM (transmission electron microscope) operated at 120 kV. X-ray diffraction (XRD) of Ni@Fe-NP were recorded with Rigaku Smartlab diffractometer with Cu K α radiation (1.5406 Å; 40 kV; 40 mA). The elemental composition of Ni@Fe-NP were analysed by XPS (X-ray photoelectron spectroscopy) with ESCALAB-250 spectrometer (monochromated Al K α (150 W) source). Nitrogen adsorption-desorption isotherms were measured at -196°C using micromeritics ASAP 2020 accelerated surface area with porosimetry system. The specific surface area was determined on the basis of Brunauer–Emmett–Teller (BET) method from nitrogen adsorption data at a relative pressure range between 0.05 and 0.2. The total pore volume was calculated from the gas adsorbed with relative pressure of 0.99 and PSD (pore size distribution) was derived from adsorption branches by Barrett–Joyner–Halenda (BJH) method.

2.4 Preparation of electrode and electrochemical characterization

Using alumina slurry the working electrode was polished as mirror like surface and washed with water and acetone and dried. The slurry used was made by mixing 4.0 mg of catalyst in 1.0 mL solvent mixture (5 wt% Nafion and water (v/v = 1/9)) for 20 min in ultrasonicator. The commercially available IrO₂ catalyst was used for comparison: 1.0 mg mL⁻¹ of IrO₂ suspension was prepared using identical procedure. The slurry was placed on a precleaned working electrode and the electrode was allowed to dry at room temperature before measurement. The catalyst loading of 0.5 $\mu\text{g cm}^{-2}$ was use of the obtained (3/7, 5/5 and 7/3) catalysts or commercial IrO₂. Biologic VMP work station was employed for electrochemical measurements. Both Ni@Fe-NP catalysts and IrO₂ catalyst was used as working electrode directly without any other treatment. OER performances of Ni@Fe-NP electrodes were examined by OER polarization curves, chronoamperometry and EIS (electrochemical impedance spectroscopy). Electrochemical analyses were studied using three-electrode geometry. A glassy carbon was employed as working electrode, Ag/AgCl saturated with KCl and Pt wire was employed as reference and counter electrodes, respectively. The OER activity was evaluated by linear sweep voltammetry (LSV: scan rate = 10 mV s⁻¹). The impedance of each catalyst was measured by EIS (electrochemical impedance spectroscopy-100 kHz to 10 mHz) with a sinusoidal perturbation amplitude of 5 mV.

Here, the turnover frequency is rate of evolved molecular O₂ per surface active site per second which can be calculated by the equation: $\text{TOF} = [J \times A] / [4 \times F \times n]$, where J – current density at, A – electrode surface area, F – Faraday constant (96 485.3 C mol⁻¹) and n – number of moles of metal on electrode. The overpotential used for the calculation of TOF is 1.6 V vs. RHE.

3. Result and discussion

Fig. 1 illustrates the formation of amorphous Ni@Fe-NP. Upon fast reduction of iron nitrate using sodium borohydride, FeOH-

NP was obtained. The subsequent solvothermal methods involving Ni²⁺ doping on FeOH-NP surface with DMF in the presence of glucose at 160 °C (12 h). The FeOH-NP was completely converted into amorphous Ni@Fe-NP according to coordinating the etching process which offers high surface area, high electronic conductivity and high stability with enhanced activity.

The Ni was selected as a stimulant for OER activity because of its electrical conductivity, catalytic property and various applications towards our electrochemical feature. The FE-SEM image confirmed the amorphous nature of Ni@Fe-NP as well as a large amount of accessible catalytic active sites (Fig. 2). Further, to understand the composition of Ni@Fe-NP amorphous nanostructure with different ratio of Ni doping, EDS elemental mapping was record which shows a homogeneous distribution of Ni and Fe throughout the electrocatalyst surface and the corresponding results are given in Fig. S1.† The rippled nanolayer of amorphous Ni@Fe-NP was formed by internally connected mesoporous with high surface area and the calculated of pore size is around 2 to 10 nm (Fig. S2†).

The amorphous nanostructured Ni@Fe-NP electrocatalyst was studied using HR-TEM (Fig. 2), which shows that all amorphous rippled layer Ni@Fe-NP was well uniformly dispersed and nickel and iron are interconnected with each

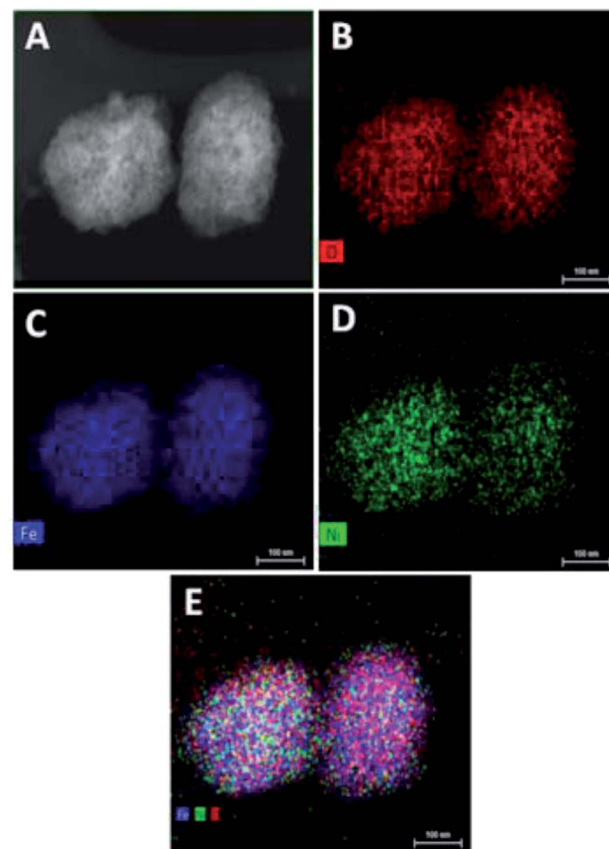


Fig. 3 TEM elemental mapping of Ni@Fe-NP: (A) STEM image; (B) oxygen element image; (C) iron elemental image; (D) nickel elemental image and (E) overlay of all O, Fe and Ni elemental image.



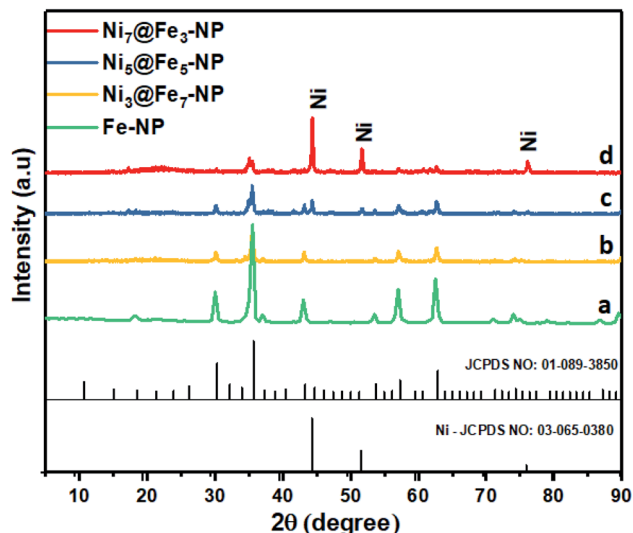


Fig. 4 XRD pattern of FeOH-NP (a); $\text{Ni}_3\text{@Fe}_7\text{-NP}$ (b); $\text{Ni}_5\text{@Fe}_5\text{-NP}$ (c) and $\text{Ni}_7\text{@Fe}_3\text{-NP}$ (d).

other which is in line with FE-SEM result. HR-TEM revealed that the solvothermal prepared Ni@Fe-NP are amorphous rippled layered are very thin and transparent with absence of typical metal lattice fringes for iron, nickel and their composites. Selected area of diffraction pattern shows a broad

diffused halo ring which confirms the solvothermal prepared Ni@Fe-NP having amorphous morphology.⁴⁷ The morphology results indicate that mesoporous amorphous Ni@Fe-NP is a hierarchically structured OER electrocatalyst which is beneficial for enhanced electrocatalytic O_2 evolution reaction. The XRD peak well matched with JCPDS no: 01-089-3850 (Fig. 4) and Fig. 4b–d shows different ratio of Ni-doped FeOH-NP.

The absence of additional peak formation in XRD confirms the purity of the electrocatalyst. The amorphous nature of Ni@Fe-NP catalyst can provide an abundant catalytically high active site for electrocatalytic reactions owing to their structural flexibility as well as larger density of unsaturated short-range coordination sites which gives rise to an easier O–O adsorption of reactants compared to the counterpart crystalline phases.⁴⁸ The formation of the amorphous rippled nano-structured Ni@Fe NP was confirmed by high-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM) (Fig. 3 and S3†) and EDX line scanning analysis (Fig. S3A and B†).

The intensity of nickel is higher than that of iron and oxygen in the center of amorphous nanoparticles which indicate that the small amount Ni atoms are homogeneously distributed at the interior of the amorphous nanoparticles; Ni atoms are mainly distributed in the inner surface of Fe whereas Fe–OH atoms coexist at the outer surface which confirm the

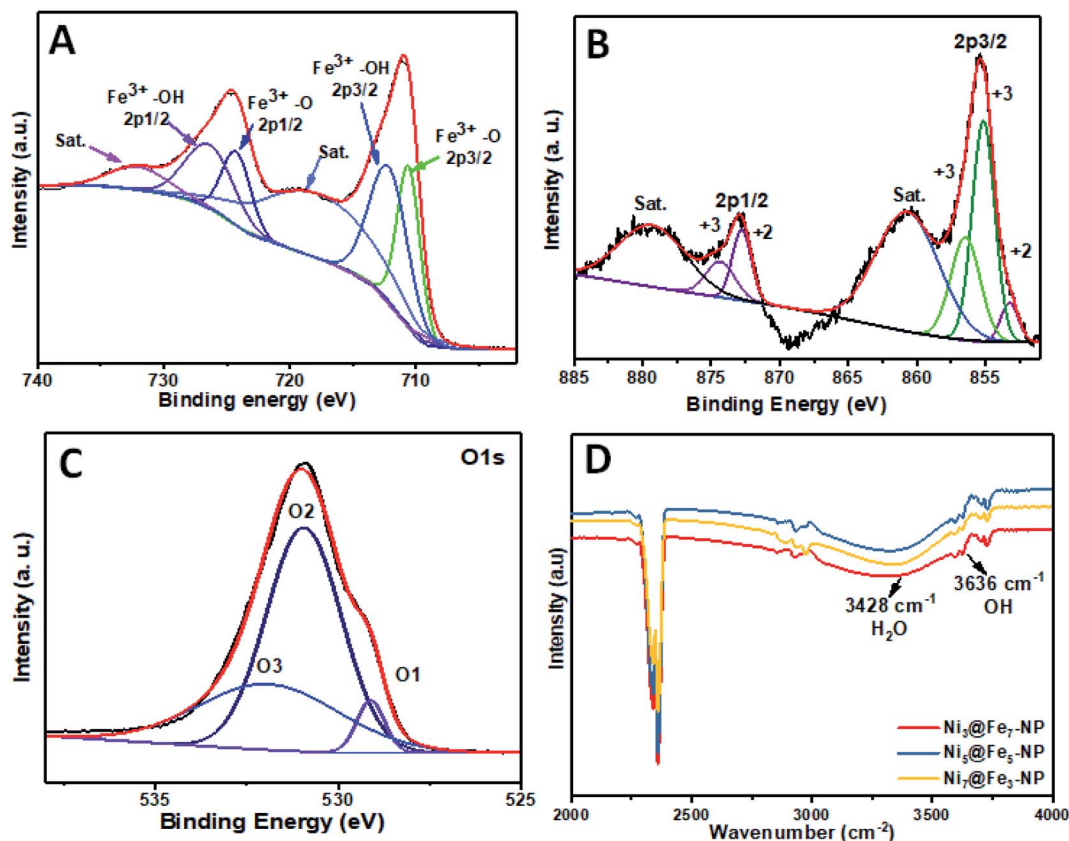


Fig. 5 High-resolution XPS spectra of (A) Fe; (B) Ni; (C) O and (D) FT-IR spectra of Ni@Fe-NP .

amorphous nature of Ni@Fe-nanoparticles. The composition of Ni@Fe-NP was determined by XPS; typical fitted Ni, Fe and O XPS spectra of Ni@Fe-NP obtained using the Gaussian fitting method (Fig. 5). The Ni, Fe and O was detected in the XPS spectrum with bimetallic composition. The high-resolution Ni 2p spectrum can be fitted into two spin-orbit peaks of Ni 2p_{3/2} and Ni 2p_{1/2} along with the corresponding shake-up satellites (Fig. 4b). The peaks are mainly fitted by two Ni environments: Ni²⁺ at 853.7, 855.1, 872.7 eV and Ni³⁺ at 856.2, 874.4 eV, respectively with 17.6 eV spin-energy difference which is the characteristic of M(OH)₂ phase.^{49,50} The Fe XPS shows peaks at 710.6 and 724.4 eV corresponds to Fe 2p_{3/2} and Fe 2p_{1/2}, respectively (Fig. 3A). After fitting, the peaks at 712.3 and 726.8 eV corresponds to Fe 2p_{3/2} and Fe 2p_{1/2} of Fe-OH in Ni@Fe-NP, respectively.^{51,52} The high-resolution O 1s spectrum (Fig. 4c) can be deconvoluted into three peaks at 529.7 (O 1), 530.9 (O 2) and 532.0 eV (O 3) and can be attributed to lattice oxygen species (O²⁻)^{53,54} and hydroxyl groups (-OH) or the surface adsorbed oxygen in Fe₂₁HO₃₂. The FT-IR was carried out for Ni@Fe-NP sample to confirm the Ni-Fe hydroxide formation (Fig. 4d). The presence of broad peak around 3636 cm⁻¹ corresponds to the non-hydrogen bonded O-H, broad shoulder peak at 3428 cm⁻¹, suggesting that the presence of hydroxide and oxy hydroxide species.

3.1 Electrochemical activity

The electrochemical OER activity of Ni₃@Fe₇-NP, Ni₇@Fe₃-NP, Ni₅@Fe₅-NP and IrO₂ was first evaluated by using homogeneously coated on GC electrode in the three electrode system. The OER polarization curves were harvested from LSV (linear sweep voltammogram) with potential range 1 to 1.8 V *versus* RHE in 0.1 M KOH (Fig. 6). The Ni₃@Fe₇-NP electrocatalyst requires an overpotential of 361 mV (without *iR* correction) to afford 10 mA cm⁻² which is a matric apt solar fuel synthesis⁵⁵ (thermodynamic OER potential - E^0 H₂O/O₂ -1.229 V). However, the electrocatalysts Ni₇@Fe₃-NP and Ni₅@Fe₅-NP requires the overpotentials of 411 and 381 mV, respectively at 10 mA cm⁻² which is smaller than that of commercial IrO₂ (511 mV) and RuO₂ anode electrocatalyst at 10 mA cm⁻² (Fig. 6A). The Tafel graph shows the slope value for Ni₃@Fe₇-NP and IrO₂ coated on GC as 98.9, 106 and 130 mV dec⁻¹, for GC (Fig. 6B). The low Tafel slope of Ni₃@Fe₇-NP signified the superior reaction kinetics in the OER. The Ni₃@Fe₇-NP undergo the OER reaction mechanism as given below equation:

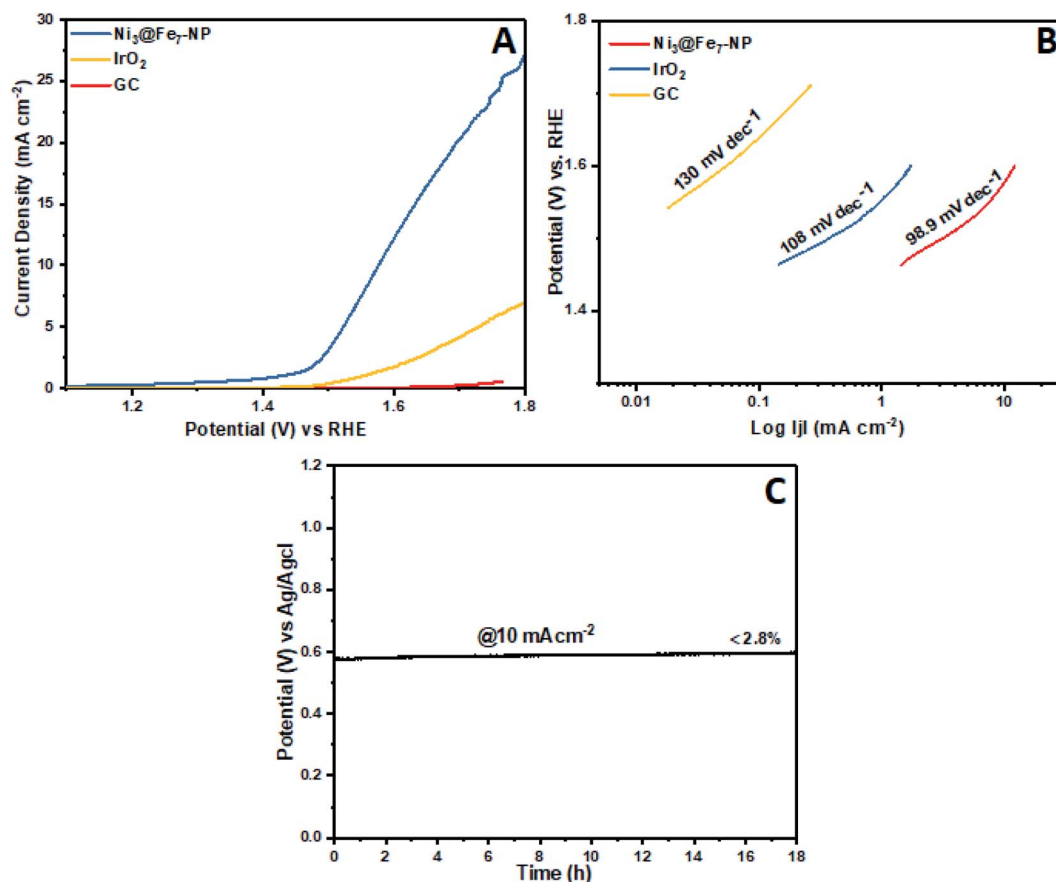


Fig. 6 OER polarization curves (no *iR*-corrected) of Ni@Fe-NP in a 0.1 M KOH, (A); oxygen evolution reaction LSV curves (B) Tafel slopes and (C) chronopotentiometric durability test at 10 mA cm⁻².





where M is the transition element. During electrochemical reaction forming the formed of beta-oxy/hydroxides active sites stimulating the for enhanced oxygen evolution reaction.⁵⁶ The calculated TOF of different ratio Ni-doped FeOH-NP was 0.072 s^{-1} , 0.0053 s^{-1} , 0.0046 s^{-1} for $\text{Ni}_3\text{@Fe}_7\text{-NP}$, $\text{Ni}_5\text{@Fe}_5\text{-NP}$, $\text{Ni}_7\text{@Fe}_3\text{-NP}$, respectively at OER potential 1.60 V (vs. RHE). The lower performance of Fe-NP electrode might be due to less active phase site for OER and the best activity of $\text{Ni}_3\text{@Fe}_7\text{-NP}$ due to the optimum ratio of nickel incorporate into Fe-NP. Further, controlled different ratio samples of $\text{Ni}_5\text{@Fe}_5\text{-NP}$ and $\text{Ni}_7\text{@Fe}_3\text{-NP}$ show OER overpotentials of 381 and 411 mV respectively, which indicate that the metal oxy/hydroxide^{57–59} nature of nickel and iron is responsible for the unsurprised performance of $\text{Ni}_3\text{@Fe}_7\text{-NP}$ (Fig. 7). The catalytic property of amorphous $\text{Ni}_3\text{@Fe}_7\text{-NP}$ was increased when compared with $\text{Ni}_7\text{@Fe}_3\text{-NP}$ due to change in oxidation state. These results confirmed that the key to obtain good amorphous oxy/hydroxide electrocatalysts toward OER. The optimal ratio combination of nickel and iron particles in $\text{Ni}_3\text{@Fe}_7\text{-NP}$ is indistinguishable to that found in the previous report.⁶⁰ Though Ni metal content plays very important role for the enhanced activity, the essential reason behind the enhanced activity is due to Ni and Fe active hydroxides formation during OER $[\text{M(II)} \text{ to } \text{M(III)}]$ ($\text{M} = \text{Ni, Fe}$), which promotes the enhanced activity in the OER.⁶¹ The enhanced activity of $\text{Ni}_3\text{@Fe}_7\text{-NP}$ catalyst exhibits good activity about 361 mV (0.1 M KOH) overpotential to obtain 10 mA cm^{-2} current density when compared with recent reported catalysts (Table S1†). The electrocatalyst active sites are usually appear at the electrocatalyst surface so as to well communication with the electrolyte.

Furthermore, ECSA (electrochemical active surface area) is universally recognized as important evidence that electrocatalysis is significantly connected to the interaction between the catalyst surface and reaction intermediates (adsorbates O–O formation). The electrocatalytic activity difference directly

determined by the reactivity of the catalyst surface which should be revealed by ECSA. The electrochemical double layer capacitance calculated on the basis of electrochemically active surface area for each system.^{62,63} Cyclic voltammogram (CVs) $\pm 50 \text{ mV}$ across the open circuit potential (OCP) were scanned at 10, 20, 30, 40 and 50 mV s^{-1} between the potential of 0.86 V to 1.16 V vs. RHE, at each scan rate, cyclic voltammogram curve shows the perfect broad rectangular behavior.

The rectangular behavior ratifies that the double layer capacitance may be because of the enhanced high electrochemical active surface area of the electrocatalyst. As we noticed that during CV from low scan rate to higher scan rate the i_a (anodic) and i_c (cathodic) cyclic voltammogram areas (current density) have been linearly increased up to $0.0190 \text{ mA cm}^{-2}$. The i_a (anodic) was measured with the potential at 0.88 V vs. RHE from each broad rectangular cyclic voltammogram spectra. The i_a anodic current densities for each scan is plotted against the scan rates and also calculated slope using linear fit as shown in Fig. 8. The slope exhibits the double layer capacitance of $\text{Ni}_3\text{@Fe}_7\text{-NP}$ (11.0 mF cm^{-2}), $\text{Ni}_7\text{@Fe}_3\text{-NP}$ (3.1 mF cm^{-2}) and $\text{Ni}_5\text{@Fe}_5\text{-NP}$ (1.9 mF cm^{-2}), respectively, the high value of double layer capacitance of electrocatalyst increases the interaction with electrolyte.

The outstanding OER activity and durability of Ni@Fe-NP electrocatalyst on a glassy carbon electrode initiate us to develop very cheap and porous anode for commercial water splitter. The Ni@Fe-NP electrocatalyst (0.5 mg cm^{-2}) was uniformly loaded on a porous nickel foam (0.5 cm^{-2}) as a current collector (Ni@Fe-NP/Ni foam substrate) to increase the active surface area and reduce the stress by giving a pathway for oxygen bubble evolution in a harsh alkaline solution. A current density of 10 mA cm^{-2} was delivered by Ni@Fe-NP/Ni foam support electrocatalyst at 211 mV overpotential which is 170 mV lower than that of $\text{IrO}_2/\text{Ni foam}$ support (overpotential of 381 mV at 10 mA cm^{-2}) as shown in Fig. 9A. The bare Ni foam requires a very high overpotential of 421 mV and also compared with the recently reported good OER activity nickel–iron based electrocatalyst (Table S1†). The Tafel slope of Ni@Fe-NP/Ni

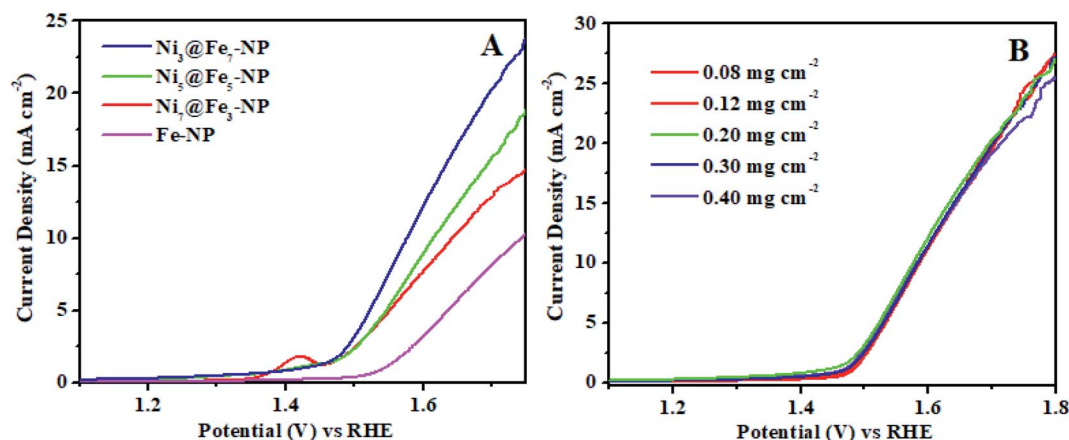


Fig. 7 Oxygen evolution reaction (A) LSV curves of amorphous Ni@Fe-NP electrocatalysts at different ratio synthesis with loading amount of 0.030 mg cm^{-2} and (B) LSV curves of $\text{Ni}_3\text{@Fe}_7\text{-NP}$ electrocatalyst at different loading amount on glassy carbon electrode.



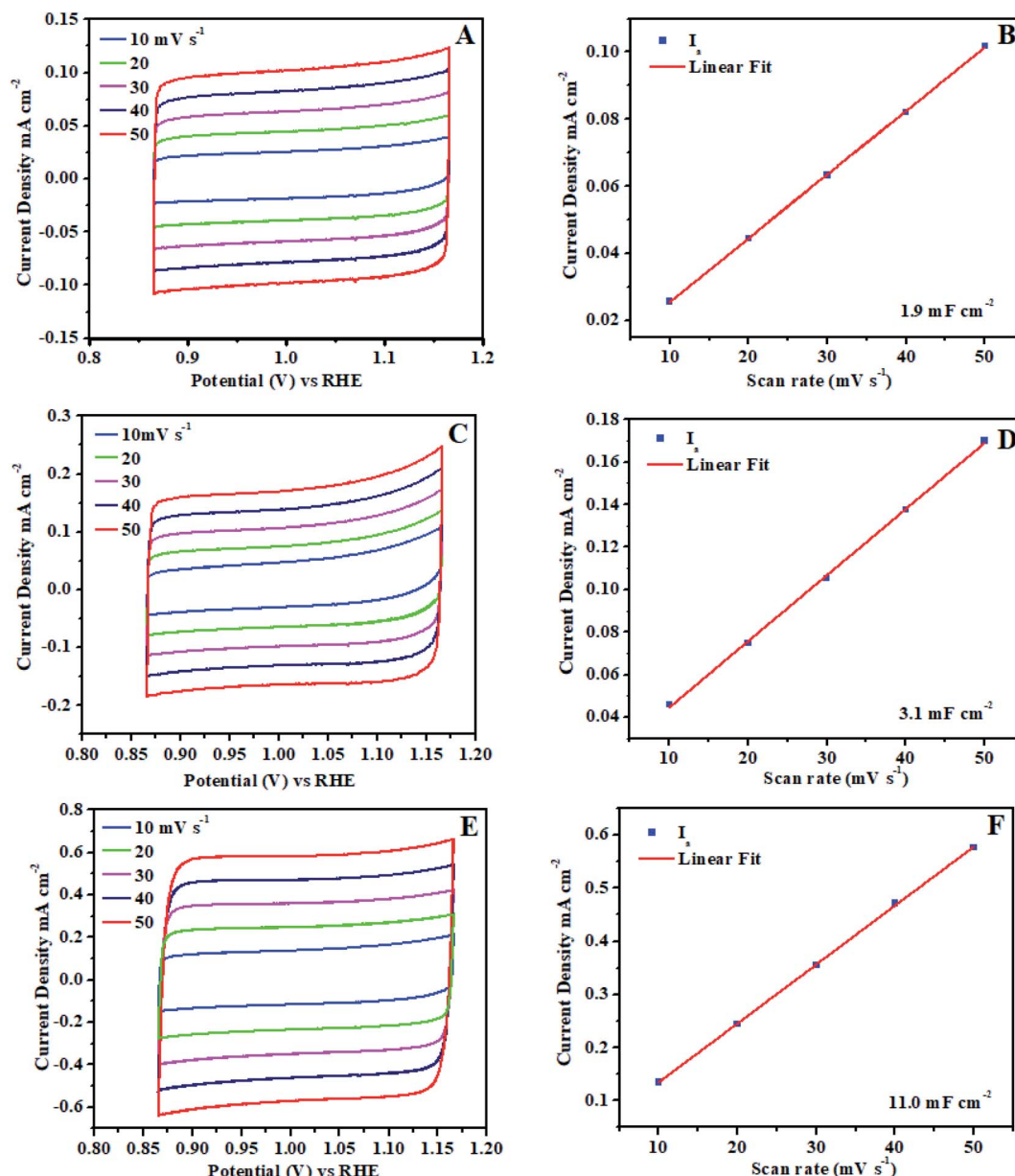


Fig. 8 Electrochemical active surface area (ECSA) of amorphous Ni@Fe-NP electrocatalyst: (A and B) Ni₅@Fe₅-NP, (C and D) Ni₇@Fe₃-NP, (E and F) Ni₃@Fe₇-NP.

foam electrode was 84.2 mV dec⁻¹ which was significantly small than that of IrO₂/Ni foam (164 mV dec⁻¹) and bare Ni foam (199 mV dec⁻¹) (Fig. 9B). Therefore, the Ni@Fe-NP/Ni foam electrode has highly favorable kinetics to overcome the sluggish OER issue in alkaline solution.

The long-term durable test of Ni@Fe-NP/Ni foam electrode with fixed current density of 10 mA cm⁻² over 130 h of continuous OER operation and catalyst morphology was displayed in Fig. S4.† The Ni@Fe-NP/Ni foam electrode exhibit exceptional electrode stability with an insignificant potential loss of 4.1% at 130 h for nonstop operating condition. During oxygen evolution reaction, gas bubbles liberation was continuously detected on the electrode surface whereas the previous reports shows that the RuO₂ is more unstable than IrO₂.^{64,65} The Ni@Fe-NP/Ni

foam electrode exhibits superior stability compared with recently reported Ni-Fe based OER electrocatalysts. The remarkable OER results of Ni@Fe-NP electrocatalyst allowed us to assemble a close to real scale conventional water electrolyzer with 20% Pt/C/Ni foam cathode (Fig. S7†).

The LSV in Fig. 9C shows the cell voltage of water electrolyzers, the precious Pt/C as a cathode and nonprecious (Ni@Fe-NP) as an anode. The precious catalyst IrO₂/Ni foam anode with 20% Pt/C/Ni foam cathode shows 1.62 V cell voltage at overall water splitting current density of 10 mA cm⁻². However, the non-precious Ni@Fe-NP/Ni foam anode electrode electrolyzer only required 1.57 V to reach 10 mA cm⁻² current density. The obtained voltage 50 mV is lower than that required by the voltage of precious metal anode of



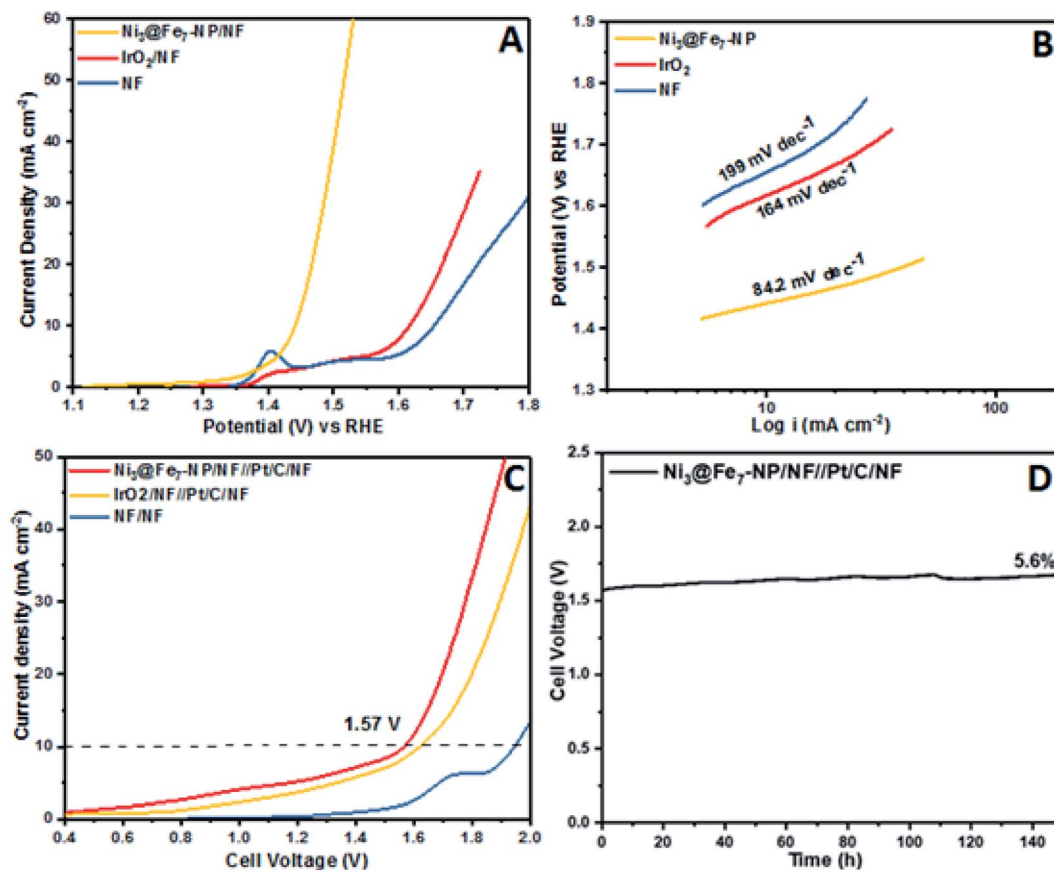


Fig. 9 Electrochemical: (A) OER LSVs curves of $\text{Ni}_3\text{@Fe}_7\text{-NP/NF}$, $\text{IrO}_2\text{/NF}$ and bare Ni foam (scan rate: 10 mV s^{-1}); (B) Tafel plot; (C) full cell LSVs (scan rate 10 mV s^{-1}); (D) chronopotentiometry durability test at constant current density of 10 mA cm^{-2} .

$\text{IrO}_2\text{/Ni}$ foam (Table S1†). The bare Ni foam water electrolyzer begins water splitting at 1.75 V. The long term durability water splitting test was investigated for the same two electrodes set up as shown in Fig. 9D. Initially, $\text{Ni}_3\text{@Fe-NP}$ electrocatalyst requires 1.57 V (without iR -correction) to reach 10 mA cm^{-2} and then it was gradually increased without major increment up to 1.67 V at 150 h continues the long-lasting test. To this end, after 150 h durability test, it required only 1.67 V afford 10 mA cm^{-2} .

The largest natural renewable resource is solar energy which is the ideal source to increase hydrogen production.⁶⁶ Accordingly, the solar renewable energy used alkaline water splitting into solar to hydrogen fuel production has shown in Fig. S9.† It is new pathway of renewable energy production. Therefore, the solar panel was coupled with usual electrolyzer due to high OCV and current density of GaAs thin film solar cell which can produce a maximum voltage of 6.1 V depends on the distance between solar panel and lamp (Fig. S5†). A common electrolyzer produces hydrogen fuel continuously by water splitting (Movie S2†).

Finally, the charge transfers resistance (R_{ct}) is measured for all different ratio electrocatalysts using electrochemical impedance spectroscopy technique to understand the influence of amorphous nature rippled nanostructure on the enhancement of the activity (Fig. S6†). This is due to its short charge

diffusion, ESCA and enhanced conductivity of the catalyst. The results are in line with OER results.^{38–44} Overall, our results (electrochemical active surface area (ECSA), XPS and interfacial charge transfer resistance) show that there is a strong oxy/hydroxide *in situ* formation leading to the best OER catalytic activity (0.1 M KOH) and stability.

4. Conclusion

In summary, oxygen vacancy-rich materials possess high amount of defects and edges with low coordinated metals. Oxygen vacancies in catalyst structures increase the number of active sites and the electrical conductivity, offering 10 mA cm^{-2} at low overpotential (211 mV). The low Tafel slope of $\text{Ni}_3\text{@Fe}_7\text{-NP}$ signified the superior reaction kinetics in the OER. The calculated TOF of different ratio Ni-doped FeOH-NP was 0.072 s^{-1} , 0.0053 s^{-1} , 0.0046 s^{-1} for $\text{Ni}_3\text{@Fe}_7\text{-NP}$, $\text{Ni}_5\text{@Fe}_5\text{-NP}$, $\text{Ni}_7\text{@Fe}_3\text{-NP}$, respectively at OER potential 1.60 V (vs. RHE). As expected, the as-prepared catalysts $\text{Ni}_3\text{@Fe}_7\text{-NP}$, $\text{Ni}_5\text{@Fe}_5\text{-NP}$, $\text{Ni}_7\text{@Fe}_3\text{-NP}$ show better OER activity. The long-term durable test of $\text{Ni}_3\text{@Fe-NP/Ni}$ foam electrode at fixed current density of 10 mA cm^{-2} over 150 h of continuous OER operation exhibit exceptional electrode stability with an insignificant potential loss of 5.6% at 150 h for nonstop operating condition. Each mixed-metal composition in this



first generation of OER catalysts produced by low cost, facile and scalable solvothermal method exhibits catalytic parameters that approach those of the most active catalysts in the literature. Given the broad applicability of current method and stoichiometric control of metal compositions, we confirm that solvothermal technique opens a new parameter space for optimization of heterogeneous electrocatalysts.

Conflicts of interest

There are no conflicts to declare.

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