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# Corrosion behaviour of 7075 aluminium alloy in acidic solution

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The objective of this work was to establish the influence of sodium molybdate on the corrosion kinetics of 7075 aluminium alloy in orthophosphoric acid aqueous solution. Corrosion rate was decreased from 75.98 to 3.24 g per m<sup>2</sup> per day. The mechanism of corrosion inhibition was studied using scanning electron microscopy, X-ray photoelectron spectroscopy, UV-Vis spectrophotometry and electrochemical impedance spectroscopy. It was revealed that heteropolyoxomolybdate species act as the corrosion inhibitor. They adsorb onto the surface and inhibit an anodic process. Their influence on a cathodic process is much weaker. Phosphomolybdenum blue species do not inhibit corrosion process and their formation is undesirable.

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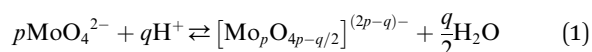
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## 1. Introduction

Aluminium alloys are widely used as a structural material due to their high strength-to-volume ratio, which is the result of the alloying process and subsequent heat treatment. 7075 alloy, belonging to the group of aluminium alloys with the highest mechanical properties, is one of the best examples. Usually, it is used in aerospace, mechanics, sport and leisure equipment. Unfortunately, its wear resistance is often insufficient for engineering applications and protective coatings are necessary.<sup>1,2</sup>

Wear resistant coatings onto 7075 alloy are produced in two surface finishing processes: hard anodising and plasma electrolytic oxidation.<sup>3,4</sup> Technology of these processes often requires etching in acidic solutions. This includes evaluation of the quality of hard anodic coating, *i.e.* destructive determination of its weight, as well as coating's removal when necessary, and is performed in H<sub>3</sub>PO<sub>4</sub> solutions. In these cases, metallic substrate must not undergo dissolution and efficient corrosion inhibitor is necessary. Up to now, the most common, cheap and effective inhibitor is CrO<sub>3</sub>.<sup>5</sup> Unfortunately, chromium(vi) species are highly toxic.<sup>6</sup> So far, the most tested corrosion inhibitors in acidic solutions were organic compounds including amines, nitrogen heterocycles, different kinds of polymers, organic dyes, Schiff bases and plant extracts.<sup>7–12</sup> Inorganic compounds were less popular. The most important here are molybdates.<sup>13–17</sup>

The chemistry of molybdenum in its highest oxidation state in aqueous solutions is complex. When adding a mineral acid to aqueous solution of orthomolybdate, addition and condensation processes occur and isopolyoxomolybdate is formed according to the eqn (1):



where  $q/p$  ratio defines the degree of protonation  $Z$  of a particular species. The most important examples of these species are dimolybdate  $[\text{Mo}_2\text{O}_7]^{2-}$ , trimolybdate  $[\text{Mo}_3\text{O}_{10}]^{2-}$ , tetramolybdate  $[\text{Mo}_4\text{O}_{13}]^{2-}$ , heptamolybdate  $[\text{Mo}_7\text{O}_{24}]^{6-}$ , octamolybdate  $[\text{Mo}_8\text{O}_{26}]^{4-}$ , and decamolybdate  $[\text{Mo}_{10}\text{O}_{34}]^{8-}$ . Much larger cluster can also be formed:  $[\text{Mo}_{36}\text{O}_{112}(\text{H}_2\text{O})_{16}]^{8-}$ ,  $\text{Na}_{48}[\text{H}_x\text{Mo}_{368}\text{O}_{1032}(\text{H}_2\text{O})_{240}(\text{SO}_4)_{48}] \cdot ca. 1000\text{H}_2\text{O}$  ( $x \approx 16$ ) and  $[\text{Mo}_{154}(\text{NO})_{14}\text{O}_{420}(\text{OH})_{28}(\text{H}_2\text{O})_{70}]^{25-}$ .<sup>18–21</sup>

When one or more additional elements are present in the solution during addition and condensation of orthomolybdate, heteropolyoxomolybdate is formed. About 60 elements on the periodic table, including phosphorus, can act as heteroatoms. The most well-known heteropolyoxomolybdate is  $[\text{PMo}_{12}\text{O}_{40}]^{3-}$ . It can be easily reduced to phosphomolybdenum blue  $[\text{PMo}_{12}\text{O}_{40}]^{7-}$ , where Mo exists both in V and VI oxidation state. This process is used for spectrophotometric determination of phosphorus concentration in the solution. The reduction reaction is complex and involves 2, 4 or even 6 electrons, depending on the applied reductant, pH, concentrations and proportion of the reagents.<sup>22</sup>

Aluminium, when immersed in H<sub>3</sub>PO<sub>4</sub> solution containing heteropolyoxomolybdate, act as an electron donor and phosphomolybdenum blue species are formed on its surface. It was initially assumed that their adsorption inhibits the corrosion of 1050 alloy.<sup>13</sup> Anodic coatings, produced onto 1050 alloy, were successfully stripped using Na<sub>2</sub>MoO<sub>4</sub> instead of CrO<sub>3</sub> and the coating weight was determined.<sup>15</sup> This was a very promising result, some issues however emerged. First, at certain Na<sub>2</sub>MoO<sub>4</sub> concentration range an insoluble salt precipitated on the aluminium. This complicates gravimetric determination of the anodic coatings' weight because appropriate concentration range of Na<sub>2</sub>MoO<sub>4</sub> should be found.<sup>15</sup> Second, an inhibition efficiency for some alloys such as 2024 seems to be insufficient

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for such an application.<sup>16</sup> Third, sodium molybdate decreases the dissolution rate of anodic coatings.<sup>23</sup> It is not known, however, whether chromate species behave in the same manner. Nevertheless, sodium molybdate still remains interesting candidate for chromium trioxide replacement.

In this work, the influence of sodium molybdate initial concentration on corrosion rate of 7075 alloy was studied. This is important from the practical point of view, because this alloy is often hard anodized and gravimetric determination of coating's weight is mandatory for such a process. What is more, the results of electrochemical and spectrophotometric studies revealed the mechanism of corrosion inhibition in the studied system and the role of phosphomolybdenum blue species.

## 2. Experimental

Aluminium rod, 10 mm diameter, made of 7075 aluminium alloy in the T6 state (heat treated and artificially aged) was obtained from Adamet-Niemet Poland (Table 1). Specimens, 2 mm thick, with a hole, 1.5 mm diameter, were prepared. They were ground with SiC papers (320 and 500 grit), rinsed with water, isopropyl alcohol, air-dried and weighted. The test solutions were prepared by dissolving appropriate amounts of Na<sub>2</sub>MoO<sub>4</sub>·2H<sub>2</sub>O in 0.5 M H<sub>3</sub>PO<sub>4</sub> to obtain concentrations  $c_{\text{Mo}} = 0, 10, 50$  and 100 mM. Their pH was adjusted using concentrated H<sub>2</sub>SO<sub>4</sub> at 1.05. The specimens were hanged in test solutions, 250 cm<sup>3</sup> per one specimen, using a nylon thread. The solutions were open to air. Their temperature,  $T = 303$  K, was controlled using a water bath. After  $t = 600$  min the specimens were rinsed with water, isopropyl alcohol, air-dried and weighted. Corrosion rates were calculated independently for three specimens, using eqn (2) and then averaged:

$$v_{\text{corr}} = \frac{\Delta m}{S \times t} \quad (2)$$

where  $\Delta m$  stands for weight loss of the specimen,  $S$  – its surface area and  $t$  – immersion time. The uncertainties were calculated using eqn (3):

$$\Delta x = \frac{t_{0.95, n-1} \times s_x}{\sqrt{n}} \quad (3)$$

where  $s_x$  is the standard deviation of an average  $x$ ,  $n$  stands for the number of independent experiments performed and  $t_{0.95, n-1}$  is the Student t-factor for 95% confidence level.<sup>24</sup> Uncertainty of any physical quantity  $x$ , presented in a figure in this work as an error bar, was calculated using this equation.

**Table 1** Chemical composition of 7075 aluminium alloy determined using energy-dispersive X-ray spectroscopy

Concentration of elements, wt%					
Al	Zn	Mg	Cu	Si	Fe
91.31	4.21	3.11	1.29	0.06	0.02

One specimen of the each set was then etched in 0.5 M H<sub>3</sub>PO<sub>4</sub> + 0.1 M Cr<sub>2</sub>O<sub>7</sub><sup>2-</sup> solution,  $T = 363$  K, to remove any insoluble corrosion product from the surface, and the corrosion rate was again calculated.

Microscopic examination of the surface of the alloy prior corrosion test and corroded specimens was performed using Phenom XL scanning electron microscope (Thermo Fisher Scientific Inc., Waltham, U.S.) equipped with an energy-dispersive X-ray spectrometer (EDS). Accelerating voltage was 15 kV and the spot size *ca.* 8 nm.

Additional characterisation of the corrosion products obtained when  $c_{\text{Mo}} = 100$  mM was performed using PHI 5000 Versa Probe II X-ray photoelectron spectrometer (ULVAC-PHI, Chigasaki, Japan). Al K $\alpha$  X-ray beam, 100  $\mu\text{m}$ , 25 W was applied. The photoelectron spectra were acquired from 300  $\times$  300  $\mu\text{m}$  areas, the analyser pass energy was 46.95 eV. The operating pressure in the chamber was  $<5 \times 10^{-7}$  Pa, the charging effect was compensated using a dual-beam charge neutraliser. One area of the sample, 3  $\times$  3 mm<sup>2</sup>, was pre-sputtered with an argon gas cluster ion beam to remove a potential contamination from the surface. The beam energy was 10 keV, beam current 30 nA and sputtering time 5 minutes. The carbon C 1s peak with binding energy of 284.8 eV was used as a reference for all XPS peaks. Spectrum background was subtracted using the Shirley method. PHI MultiPak<sup>TM</sup> data analysis software was used to calculate elemental compositions from the peak areas.

UV-Vis absorption spectra of the solutions before and after corrosion tests were measured in the quartz cuvettes, with 10 mm optical path length, using Cary 60 spectrophotometer (Agilent Technologies Inc., Santa Clara, US).

Working electrodes for electrochemical characterisation of the corrosion mechanism were prepared according to the following procedure. An electrical contact, made of aluminium alloy wire, was attached to the base of a 10 mm long cylindrical specimen. The wire was insulated from the solution using a heat shrink tube, the specimen and the electrical connection was then mounted in an epoxy resin. The surface area of the electrode, exposed to the solution was 0.785 cm<sup>2</sup>. Prior every experiment it was ground with SiC abrasive paper (320 and 500 grit), rinsed with water, isopropyl alcohol, and air-dried. Electrochemical analysis were performed using SP-300 potentiostat (Bio-Logic SAS, Seyssinet-Pariset, France). Working electrode was immersed in 100 cm<sup>3</sup> test solutions, 20 cm<sup>2</sup> platinum counter electrode and Ag|AgCl (3 M KCl) reference electrode were applied. The latter was placed in a Luggin probe filled with 0.5 M H<sub>3</sub>PO<sub>4</sub> solution. Test solutions contained 0.5 M H<sub>3</sub>PO<sub>4</sub> and 0, 10, 50, 100 mM of Na<sub>2</sub>MoO<sub>4</sub>, pH = 1.05. To ensure constant temperature of the solutions  $T = 303$  K, electrochemical tests were performed in a cell with a water jacket; the cell was open to air. All the experiments were performed in a Faraday cage.

Open circuit potential (OCP) of 7075 aluminium alloy was recorded for  $t = 580$  min prior further electrochemical characterisation of the system. OCP values, averaged over the last 40 min of immersion, were regarded as a corrosion potential  $E_{\text{corr}}$ . This was studied as a function of  $c_{\text{Mo}}$ . Values averaged over



three,  $c_{\text{Mo}} = 0$  mM, four  $c_{\text{Mo}} = 10$  and 50 mM or six,  $c_{\text{Mo}} = 100$  mM independent measurements are presented.

The main analytical method applied was electrochemical impedance spectroscopy (EIS). The impedance spectra were measured after  $t = 580$  min immersion of the specimens, when the OCP was sufficiently stable, in the frequency domain between 200 kHz and 10 mHz. A sinusoidal perturbation of potential equal to 5 mV of a root mean square was applied. First, the EIS spectrum was measured for  $c_{\text{Mo}} = 0$  mM, at OCP, in a stagnant solution. Then, the same solution was agitated using magnetic stirrer for 60 min, with agitation speed 250 rpm, and the spectrum was measured. Second, the EIS spectra were recorded for  $c_{\text{Mo}} = 100$  mM, at OCP, in the stagnant solutions. Then, the working electrode was polarised, either 100 mV anodically, or 100 mV cathodically vs. OCP. Time necessary for achieving the stationary state was 60 and 164 min respectively. Then, the EIS spectra were again measured. Third, the influence of sodium molybdate initial concentration,  $c_{\text{Mo}} = 0, 10, 50$  and 100 mM on the EIS spectra was studied at OCP, in stagnant solutions. The number of independent experiments was  $n = 3$  for  $c_{\text{Mo}} = 0$  mM,  $n = 4$  for  $c_{\text{Mo}} = 10$  and 50 mM and  $n = 6$  for  $c_{\text{Mo}} = 100$  mM. All the spectra were validated using a Kramers–Kronig transformation with a KK Test software, version 1.01.<sup>25,26</sup> Then, they were fitted with the appropriate electrical equivalent circuit (EEC) in a Zview software (Scribner Associates, version 3.5d). The weighted sum of squares of differences between measured and calculated impedances  $S$  were used to estimate the quality of the fit.

Corroding metal/solution interphase is modelled in EIS using resistance of the electrolyte  $R_s$  and a double layer capacitance of the electrode  $C_{\text{dl}}$  connected in parallel to a faradaic impedance. The latter takes into account various possible processes such as charge transfer, diffusion or adsorption. In real systems, time constants of the faradaic processes are distributed onto electrode. Thus, a constant phase element CPE is commonly used for modelling instead of the capacitor. The impedance of CPE is given by eqn (4):<sup>27</sup>

$$Z_{\text{CPE}} = \frac{1}{T_{\text{dl}}(j\omega)^\alpha}, \quad (4)$$

where  $T_{\text{dl}}$  is equal to the capacitance when  $\alpha = 1$ ,  $\omega$  is the angular frequency and  $j$  is the imaginary number. When aforementioned distribution of time constants occurs along the electrode's surface the double-layer capacitance can be calculated using eqn (5):<sup>27</sup>

$$C_{\text{dl}} = T_{\text{dl}}^{\frac{1}{\alpha}} \left( \frac{1}{R_s} + \frac{1}{R_{\text{ct}}} \right)^{1-\frac{1}{\alpha}} \quad (5)$$

where  $R_{\text{ct}}$  stands for the charge transfer resistance.

DC electrochemical methods were also applied to study the corrosion mechanism. Cyclic voltammograms of 0.5 M  $\text{H}_3\text{PO}_4$  solutions containing  $c_{\text{Mo}} = 0$  and 100 mM were recorded using a glassy carbon working electrode at a scan rate  $20 \text{ mV s}^{-1}$ ,  $T = 303 \text{ K}$ . Polarisation curves of 7075 aluminium alloy were obtained as a function of  $c_{\text{Mo}}$  in stagnant solutions,  $T = 303 \text{ K}$ . Cathodic and anodic branches of the curves were measured

independently, starting from the OCP, with the scan rate  $15 \text{ mV min}^{-1}$ .

## 3. Results and discussion

### 3.1. Gravimetric and spectroscopic analysis

Corrosion rate of 7075 aluminium alloy, estimated using a gravimetric method, decreases as sodium molybdate initial concentration  $c_{\text{Mo}}$  increases (Fig. 1). When  $c_{\text{Mo}} = 10$  and 100 mM, an insoluble salt precipitated on the surfaces of the specimens. This occurred to much lesser extent when  $c_{\text{Mo}} = 50$  mM. This salt was mostly dissolved in 0.5 M  $\text{H}_3\text{PO}_4 + 0.1 \text{ M Cr}_2\text{O}_7^{2-}$  hot (363 K) solution for one set of specimens. It can be concluded that the precipitation affected weight losses of the specimens only slightly. The lowest corrosion rate,  $3.24 \text{ g per m}^2$  per day, was obtained for  $c_{\text{Mo}} = 100$  mM. It corresponds to inhibition efficiency *ca.* 96%.

These results can be compared with those obtained for other aluminium alloys. Corrosion rate of 2024 alloy at  $T = 303 \text{ K}$ ,  $c_{\text{Mo}} = 25 \text{ mM}$  was  $2.74 \text{ g per m}^2$  per day.<sup>16</sup> In the case of 1050 alloy  $2.80 \text{ g per m}^2$  per day was obtained at  $T = 303 \text{ K}$ ,  $c_{\text{Mo}} = 10 \text{ mM}$ .<sup>17</sup>

Corrosion experiments were performed in aerated, acidic solutions. Thus, three cathodic processes are possible: reduction of  $\text{H}_3\text{O}^+$  to  $\text{H}_2$ ,  $\text{O}_2$  to  $\text{H}_2\text{O}$  and heteropolyoxomolybdate to phosphomolybdenum blue. The latter process was qualitatively studied using UV-Vis spectroscopy. Heteropolyoxomolybdates strongly absorb light in the ultraviolet range, therefore, analysed solutions had to be diluted 200 times. Sulphuric(vi) acid,  $\text{pH} = 1.05$ , was applied as a diluting agent to ensure the same pH and Mo/P ratio as in the corrosion experiments.

First of all, the absorption spectra of the solutions with different initial concentration of heteropolyoxomolybdates were recorded, prior corrosion experiments. The shape of the spectra does not depend on  $c_{\text{Mo}}$ , only intensities do. The spectra are composed of two overlapping absorption bands in the UV range with clearly visible maxima at 216 nm (Fig. 2a). This is Mo–O ligand-to-metal charge transfer band.<sup>22</sup> The UV range of the spectra did not change after the corrosion experiments. Weak absorption appeared, however, at  $\lambda > 500 \text{ nm}$  (Fig. 2b). When

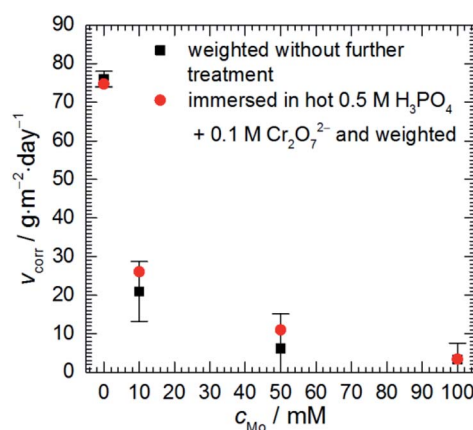


Fig. 1 Corrosion rate of 7075 aluminium alloy as a function of sodium molybdate initial concentration; 0.5 M  $\text{H}_3\text{PO}_4$ ,  $T = 303 \text{ K}$ ,  $t = 600 \text{ min}$ .



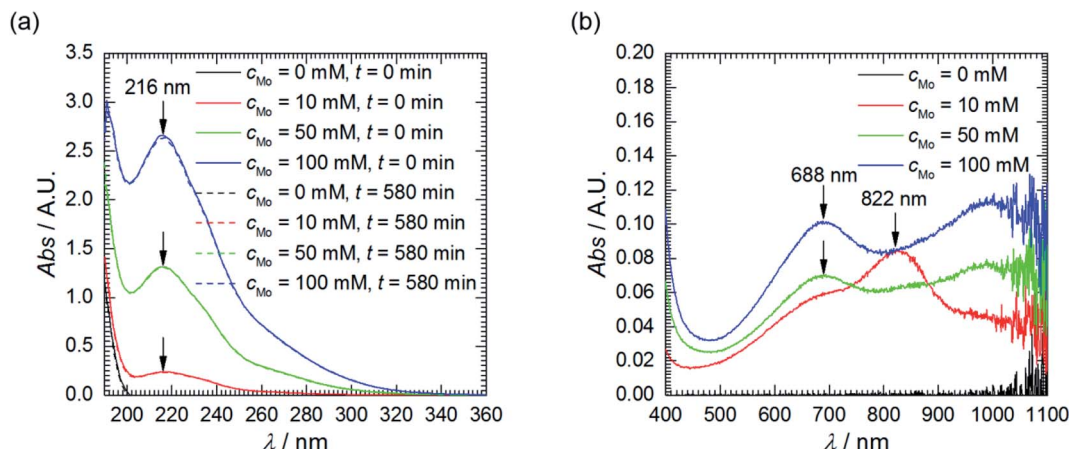


Fig. 2 UV-Vis absorption spectra of solutions as a function of  $c_{\text{Mo}}$ : (a) prior and after corrosion tests, diluted 200-fold using  $\text{H}_2\text{SO}_4$ , pH = 1.05; (b) after corrosion tests, undiluted.

$c_{\text{Mo}} = 10 \text{ mM}$ , two absorption bands are observed: at 688 and 822 nm. When  $c_{\text{Mo}} > 10 \text{ mM}$  the former becomes stronger and the latter diminishes. These are Mo(v)–Mo(vi) intervalent charge transfer bands. Intensity of the former,  $\lambda_{\text{max}}$  between 600 and 700 nm, is of moderate intensity, with absorption coefficient  $\varepsilon \approx 10\,000 \text{ dm}^3 \text{ mol}^{-1} \text{ cm}^{-1}$ . The latter,  $700 < \lambda_{\text{max}} < 800 \text{ nm}$ , is stronger,  $\varepsilon \approx 26\,000\text{--}34\,000 \text{ dm}^3 \text{ mol}^{-1} \text{ cm}^{-1}$ .

These absorption bands are used in analytical chemistry for determination of phosphorus concentration in aqueous solutions. Unfortunately, their positions and intensities strongly depend on the concentrations of reagents and proportions between them.<sup>22</sup> This explains the difference between  $c_{\text{Mo}} = 10 \text{ mM}$  and  $c_{\text{Mo}} > 10 \text{ mM}$  and, at the same time, makes impossible exact determination of concentration of phosphomolybdenum blue. Nevertheless, it can be roughly estimated. It is very low, ca.  $10^{-5}$  to  $10^{-6} \text{ mol dm}^{-3}$  and increases as  $c_{\text{Mo}}$  increases. This explains why the absorption band at 216 nm virtually did not decrease after the corrosion experiments and brings up the question of whether phosphomolybdenum blue can act as the corrosion inhibitor in the studied system. It could be useful to check whether its concentration is sufficiently high to cover the surface of the electrode and ensure the corrosion inhibition. The average diameter of phosphomolybdenum blue formed in these experiments remains unknown, but, for the estimation,  $\text{H}_3[\text{PW}_{12}\text{O}_{40}]$  Keggin structure, with average diameter of 0.8 nm, was assumed.<sup>28</sup> Rough calculation indicated, that such a low concentration is sufficient to ensure the complete coverage of the electrode. In addition, oxygen dissolved in the solution can decrease the concentration of phosphomolybdenum blue.<sup>22</sup> Thus, UV-Vis spectroscopy cannot answer the aforementioned question unambiguously. This was done based on the results of electrochemical investigation.

### 3.2. Microscopic analysis

Major alloying elements and impurities of 7075 alloy are Zn, Mg, Cu, Si and Fe. They form several intermetallics determining mechanical properties and corrosion resistance of the alloy. EDS maps of the specimens prior corrosion experiments

indicated that vast majority of the intermetallics were composed of Al, Cu and Fe, with different Cu/Fe ratios and Al contents. The brighter ones (Fig. 3a) are probably  $\text{Al}_7\text{Cu}_2\text{Fe}$ . EDS point analysis indicated that their Cu/Fe atomic ratio was between 1.3 and 2.2. Deviation from the stoichiometric value can be explained with the observation that standardless analysis of Cu can lead to errors.<sup>29</sup> The darker ones, in turn, are probably  $\text{Al}_{23}\text{CuFe}_4$ . Their Fe/Cu atomic ratio was between 3.3 and 4.0. This conclusion is in agreement with literature.  $\text{Al}_7\text{Cu}_2\text{Fe}$  and  $\text{Al}_{23}\text{CuFe}_4$  coarse particles are commonly formed during solidification of 7075 aluminium alloy.<sup>2,30,31</sup> The uncertainty of determination of Al–Cu–Fe intermetallics' stoichiometry does not influence further discussion of corrosion mechanism. It was revealed that particles containing Fe and Cu are more noble than matrix, regardless of the Cu/Fe ratio, whereas particles containing Mg are anodic.<sup>32</sup> EDS analysis revealed occasional presence of  $\text{Mg}_2\text{Si}$  particles. In this case the Mg/Si atomic ratio was 2.0. Formation of  $\text{Mg}_2\text{Si}$  particles in 7075 alloy was also confirmed in the literature.<sup>30</sup> Although aluminium alloy was solution treated and artificially aged,  $\text{MgZn}_2$  hardening particles are not visible. Their size is within nanometric range and that is beyond the resolution of the scanning electron microscope applied.

Microscopic analysis of the surfaces of corroded specimens revealed a corrosion mechanism and confirmed the inhibiting ability of sodium molybdate. The most severe corrosion was observed when  $c_{\text{Mo}} = 0 \text{ mM}$  (Fig. 3b). Trenching around  $\text{Al}_7\text{Cu}_2\text{Fe}$  and  $\text{Al}_{23}\text{CuFe}_4$  particles occurred. Excessive trenching caused mechanical detachment of these particles and their dissolution in the aerated electrolyte. Subsequently, copper ions reduced on the surface forming additional cathodic sites.<sup>33–35</sup> They are indicated with red arrows in Fig. 3b. Deep corrosion pits remained on the surface, where originally aforementioned intermetallic particles were located. Corrosion attack occurred also to some extent at grain boundaries. This probably is related to dissolution of very fine  $\text{MgZn}_2$  particles. They are anodic with respect to the matrix and precipitated within the grains in the grain boundary zones during artificial aging.<sup>36</sup>





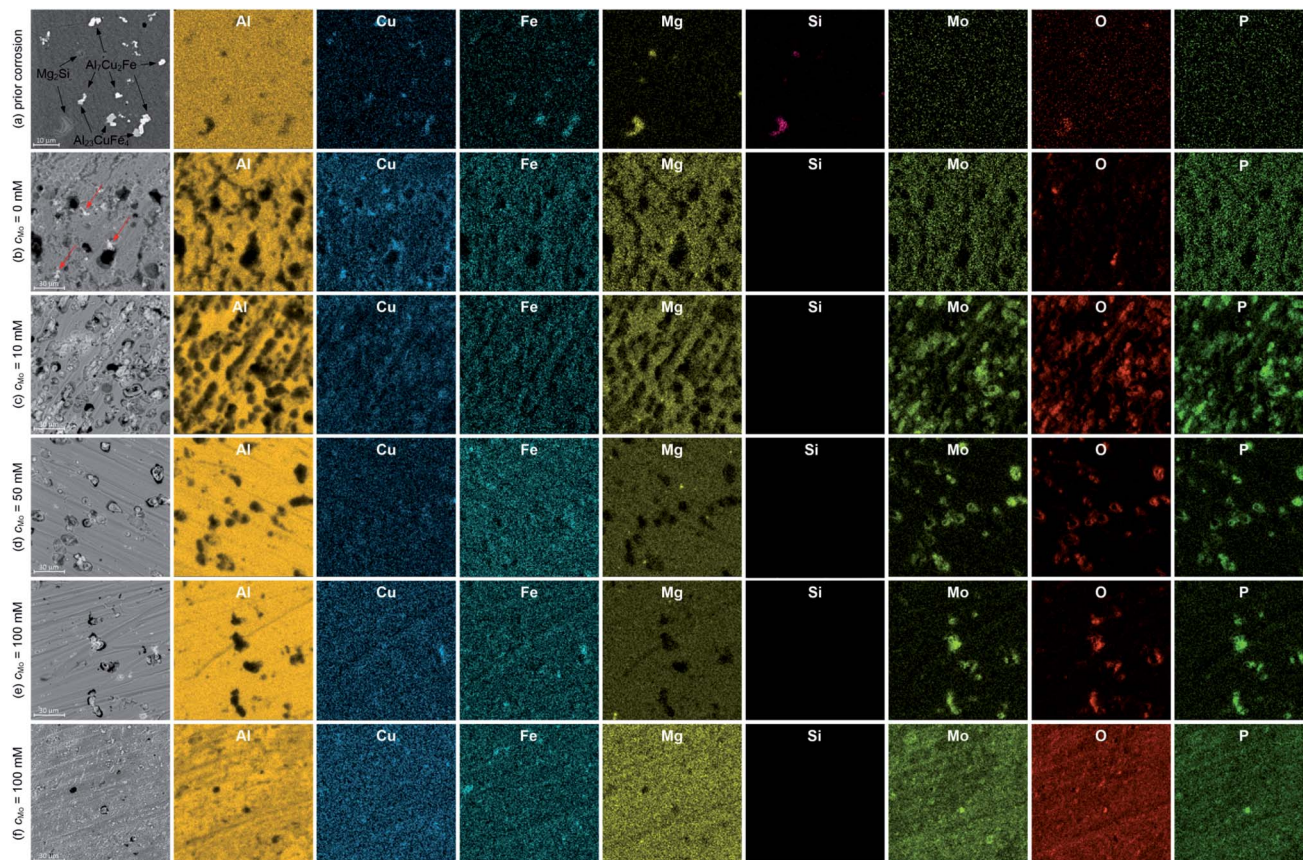


Fig. 3 Microstructures of 7075 uncorroded (a) and corroded (b)–(f) specimens together with spatial distribution of elements, colour intensity differences on EDS maps occur due to different concentration of elements; for  $c_{\text{Mo}} = 100$  mM two areas are depicted: (e) and (f),  $t = 580$  min,  $T = 303$ .

When  $c_{\text{Mo}} = 10$  mM, copper particles were hardly observed on the surface (Fig. 3c). The number of deep corrosion pits as well as their diameter decreased when compared to the uninhibited solution. Trenching around  $\text{Al}_7\text{Cu}_2\text{Fe}$  and  $\text{Al}_{23}\text{CuFe}_4$  intermetallics was partially hindered due to precipitation of Mo, P and O-rich salt. However significant number of shallow pits appeared. This may indicate that the Cu-containing intermetallics stopped serving as efficient cathodes in the corrosion cells. Thus, further depolarisation occurred within the matrix. This explains why precipitation of Mo, P and O-rich salt occurred not only on the surface of  $\text{Al}_7\text{Cu}_2\text{Fe}$  and  $\text{Al}_{23}\text{CuFe}_4$  intermetallics, but also on the matrix.

When  $c_{\text{Mo}} = 50$  mM corrosion rate was further decreased. Trenching occurred to much lesser extent when compared to uninhibited solution, Mo, P and O-rich particles were found only on the surface of  $\text{Al}_7\text{Cu}_2\text{Fe}$  and  $\text{Al}_{23}\text{CuFe}_4$  intermetallics. Some shallow pits, but much less than for  $c_{\text{Mo}} = 10$  mM were also observed (Fig. 3d). This suggests adsorption of heteropolyoxomolybdate/phosphomolybdenum blue species on the surface and further mitigation of matrix dissolution.

The lowest corrosion rate was achieved when  $c_{\text{Mo}} = 100$  mM. Localised corrosion was mostly suppressed; high concentration of heteropolyoxomolybdate/phosphomolybdenum blue species in the solution ensured sufficient matrix protection (Fig. 3e). At

the same time, such a high initial concentration of heteropolyoxomolybdate caused local precipitation of Mo, P and O-rich layer on the surface. Uniform distribution of these elements was revealed (Fig. 3f). Such a local precipitation of insoluble salt in the form of protective layers was also observed on 1050 and 2024 alloys.<sup>15,16</sup>

### 3.3. X-ray photoelectron spectroscopy

Further examination of Mo, P and O-rich layer, obtained at  $c_{\text{Mo}} = 100$  mM, was performed in three regions using X-ray photoelectron spectroscopy (XPS). Chemical composition of the layer is rather inhomogeneous (Table 2). Significant contribution from carbon C 1s, not shown in the table, was also detected because specimens were rinsed with isopropyl alcohol after exposition in the corrosive environment. The

Table 2 The chemical composition of the surface layer, at%

Measurement	O	Al	P	Mo
Area 1	75.3	5.7	6.7	12.3
Area 2	82.8	5.2	4.2	7.8
Area 3	79.9	0.0	5.3	14.8



**Table 3** The contribution of the fitted peaks for the corrosion layer, at%

Measurement	O 1s		Al 2p	P 2p	Mo 3d <sup>5/2</sup>	
	O salt	O oxide	Al(III)	P(V)	Mo(V)	Mo(VI)
Area 1	23.1	61.5	3.3	4.4	1.5	6.2
Area 2	52.3	24.7	4.8	6.1	2.1	10.0
Area 3 (pre-sputtered)	58.5	15.4	5.4	8.6	0.5	11.6

layer's phase composition is also inhomogeneous (Table 3). Oxygen exists both in the form of an oxide and salt. There are areas on the specimen, where either oxide or salt phase is dominant. Two oxidation states of molybdenum, v and vi were detected (Fig. 4a and b),<sup>37</sup> there is also contribution from Al(III) and P(V).

Pre-sputtering of the specimen with Ar clusters revealed that Mo(V) is mainly located on the surface of the corrosion layer, whereas Mo(VI) was found both on its surface and in the interior (Table 3, Fig. 4a and b). Thus, this layer can be composed of MoO<sub>3</sub> with possible certain degree of non-stoichiometry. This is related to a partial reduction of Mo(VI) to Mo(V). The oxide colouration may then become grayish.<sup>38</sup>

Another possibility is formation of a molybdenum bronze on the surface. This term refers to a variety of ternary oxide phases containing molybdenum at v and vi oxidation state and small cations such as Li<sup>+</sup>, Na<sup>+</sup>, K<sup>+</sup>, Rb<sup>+</sup>, Cs<sup>+</sup> and H<sup>+</sup>. These compounds exhibit intense colouration, metallic or semiconducting properties and resistance to attack by non-oxidising acids. The examples of molybdenum bronzes that could be formed during corrosion are H<sub>0.34</sub>MoO<sub>3</sub> and H<sub>0.93</sub>MoO<sub>3</sub>. The colour of hydrogen molybdenum bronzes depends on the amount of incorporated oxygen.<sup>39</sup>

Presence of Al(III) and P(V) in the pre-sputtered area indicate their incorporation to the corrosion layer, probably in the form of a salt.

The surface of the corrosion layer is composed of molybdenum at both oxidation states, oxygen and phosphorus. This

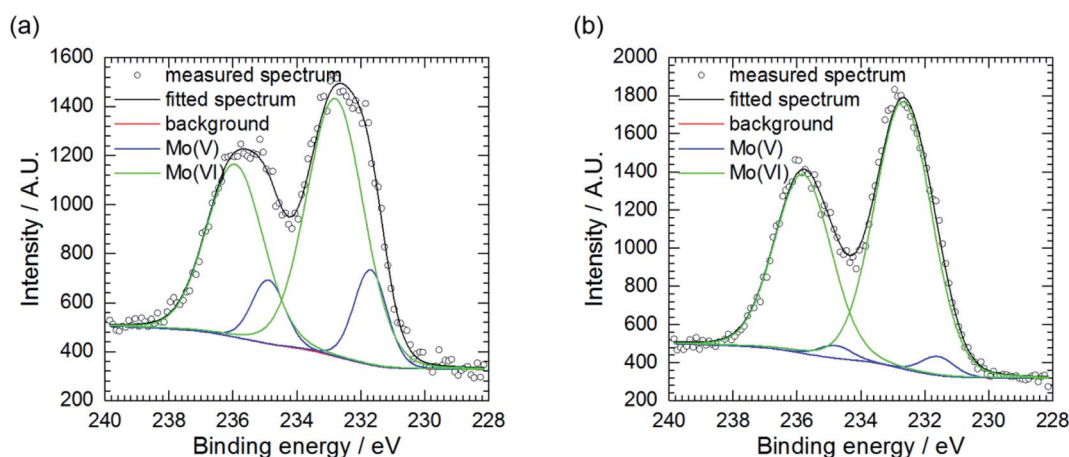
may correspond to phosphomolybdenum blue species adsorbed on the surface of the corrosion layer. Al(III) content might be related to aluminium adsorption or precipitation in the form of a salt.

The XPS study conducted is rather qualitative than quantitative *i.e.* the stoichiometry of the corrosion product could not be established. The studied system is very complex, numerous oxides and salts can be formed, they are also inhomogeneously distributed on the surface. Due to their small amount they were not detected during X-ray diffraction analysis. Thus, the mechanism of formation of the corrosion layer cannot be proposed. It should also be noted here that it depends on the concentration of heteropolyoxomolybdate species in the solution.

### 3.4. Electrochemical analysis

**3.4.1. Corrosion potential.** Open circuit potential (OCP) of 7075 aluminium alloy was measured as a function of initial concentration of sodium molybdate and immersion time (Fig. 5a). When  $c_{\text{Mo}} = 0$  mM, OCP gradually increased as the immersion time increased. This was related to the gradual change of surface's chemical composition caused by corrosion. The rate of OCP changes during last hour of the corrosion experiment was 3.5 mV h<sup>-1</sup>. This was sufficiently small to measure and analyse EIS spectra. When  $c_{\text{Mo}} = 10$  and 100 mM OCP values were initially much higher than for  $c_{\text{Mo}} = 0$  mM. Rapid increase of OCP was observed for  $c_{\text{Mo}} = 50$  mM. Relatively high value, comparable to that obtained at 100 mM, was achieved within 5 min after immersion (see inset of Fig. 5a). If the aforementioned rapid growth is neglected, it can be concluded that introduction of sodium molybdate to the corrosive environment temporarily increases OCP.

Corrosion potential  $E_{\text{corr}}$  was estimated as the average of OCP values measured for the last 40 min of immersion. Corrosion potentials obtained from independent measurements were then averaged and uncertainties of obtained values were calculated using eqn (3). It can be concluded that  $E_{\text{corr}}$  does not depend on  $c_{\text{Mo}}$  (Fig. 5b).



**Fig. 4** Mo 3d<sup>5/2</sup> XPS spectra of corrosion layer obtained at  $c_{\text{Mo}} = 100$  mM: (a) as obtained, area 2 and (b) area 3, pre-sputtered with Ar clusters.





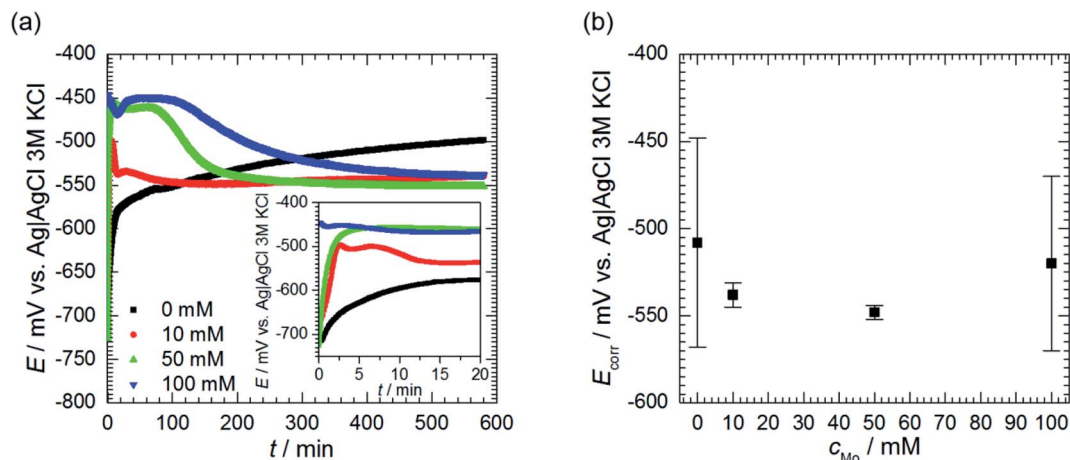


Fig. 5 Open circuit potential of 7075 aluminium alloy as a function of immersion time and initial concentration of sodium molybdate (a) and corrosion potential (b); 0.5 M  $\text{H}_3\text{PO}_4$ ,  $T = 303$  K.

**3.4.2. Electrochemical impedance spectroscopy.** First, the corrosion process in solution without inhibitor was studied. The impedance spectra are composed of two, slightly

depressed, capacitive loops, with frequencies at the maximum apex 13 Hz and 154 mHz with an additional, small inductive loop at frequencies below 35 mHz. They can be easily

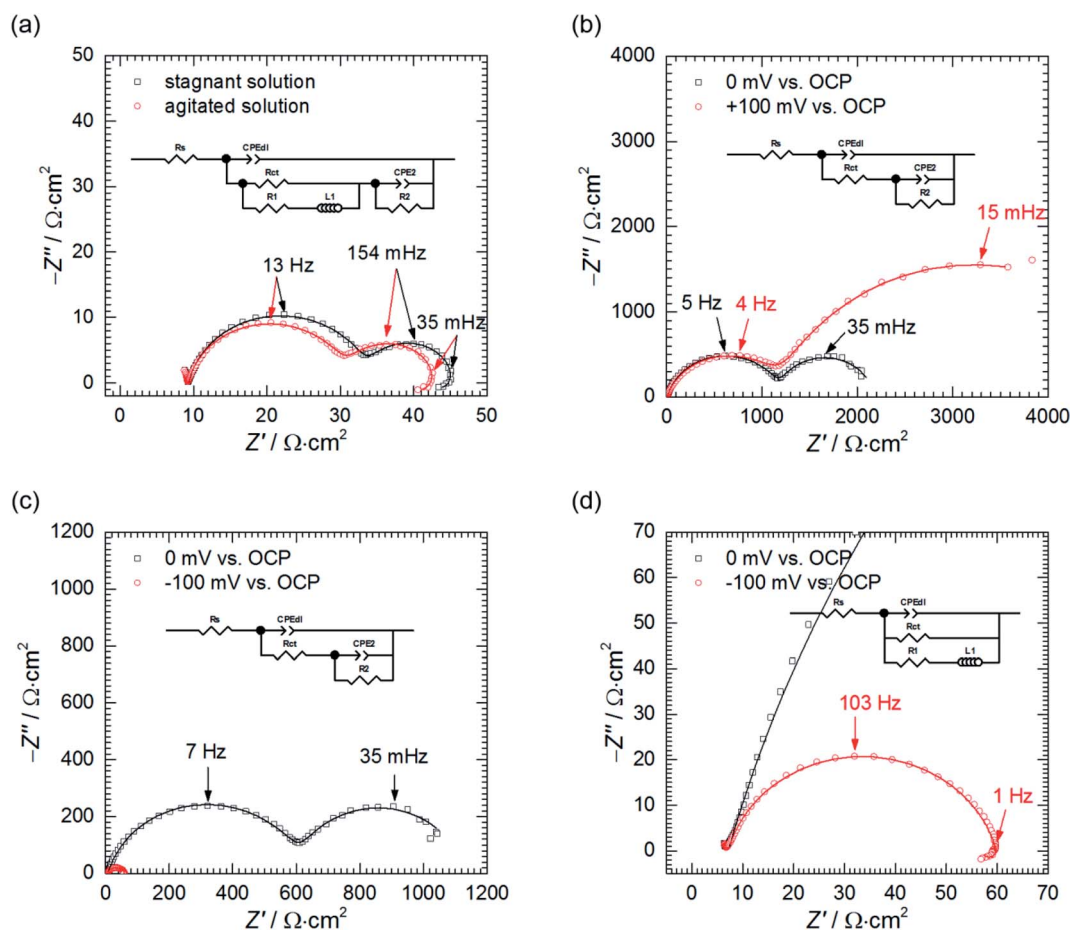


Fig. 6 Impedance spectra of 7075 aluminium alloy obtained: (a) at OCP in the stagnant and agitated solutions when  $c_{\text{Mo}} = 0$  mM; (b) at  $\eta = 0$  and +100 mV vs. OCP in the stagnant solution when  $c_{\text{Mo}} = 100$  mM; (c) at  $\eta = 0$  and -100 mV vs. OCP in the stagnant solution when  $c_{\text{Mo}} = 100$  mM; (d) and their magnified high frequency parts; empty markers represent data points, continuous lines fit obtained using the EEC; 0.5 M  $\text{H}_3\text{PO}_4$ ,  $T = 303$  K.



approximated using electrical equivalent circuit (EEC), which faradaic impedance consists of the charge transfer resistance  $R_{ct}$ , two additional resistances  $R_1$  and  $R_2$ , inductance  $L_1$  and the constant phase element  $CPE_2$  (Fig. 6a).

Such an EEC was introduced by Cao for three potential-dependent electrode processes, but he used a capacitor instead of the constant phase element  $CPE_2$ .

The first one of these three processes is the charge transfer, whose rate directly depends on the electrode's potential. High frequency capacitive loops in the EIS spectra correspond to the constant phase element  $CPE_{dl}$ , representing the double layer capacitance, connected in parallel to  $R_{ct}$ .

The other ones could be adsorption of two different species, where a surface coverage depends on electrode's potential.<sup>40</sup> They are visible in the obtained EIS spectra as the low-frequency capacitive and inductive loops. These adsorption processes are modelled using  $R_1$ ,  $R_2$ ,  $L_1$  and  $CPE_2$ . Unfortunately, their physical meaning is far more complex than  $CPE_{dl}$  and  $R_{ct}$ . According to Cao, they depend on changes of faradaic current and adsorption kinetics related to changes in surface coverage and electrode potential for both adsorbing species. What is more, they are mutually related.<sup>40</sup>

The low frequency capacitive loop can probably be related to adsorption of atomic hydrogen onto electrode's surface.<sup>27</sup> The low frequency inductive loop, in turn, might be attributed to adsorption of intermediates formed during Al dissolution. This was observed in non-aqueous<sup>41</sup> and aqueous alkaline solutions.<sup>42</sup> In acidic solutions, however, the charge transfer is believed to be too rapid to observe formation of intermediates.<sup>41</sup> Thus, the origin of the small inductive loop is different and was ascribed to the presence of gas bubbles on the electrode's surface. This was concluded after conducting the following experiment. First, the impedance spectrum of aluminium alloy was recorded after  $t = 580$  min of immersion in a stagnant solution. Then, agitation using a magnetic stirrer was started. When OCP again achieved stationary value, the impedance spectrum was measured and these two spectra were compared (Fig. 6a, Table 4). Double layer capacitances were calculated using eqn (5) and  $C_{dl} = 396 \mu F cm^{-2}$  was obtained for the stagnant solution. This value is relatively high when compared to the ideal one  $20 \mu F cm^{-2}$ .<sup>43</sup> The reason for this is increased surface area of the corroded electrode (see Fig. 3b).

In fact, for certain alloys, when selective corrosion occurs, the increase of electrode's surface area is such high that double layer capacitance achieves several to hundreds of  $mF cm^{-2}$ .<sup>43–46</sup> Agitation increased  $C_{dl}$  to  $463 \mu F cm^{-2}$ . This occurred because agitation facilitated liberation of  $H_2$  bubbles from the surface and aqueous solutions have much higher electric permittivity than gases. A slight decrease of the charge transfer resistance can be related to increase of the surface area caused by liberation of  $H_2$  bubbles.

Agitation changed the parameters describing the second capacitive loop *i.e.*  $T_2$ ,  $\alpha_2$  and  $R_2$  insignificantly. This is reasonable because, at the stationary state, agitation does not affect the adsorption processes.

Thus, the only possible explanation for *ca.* two-fold reduction in values of  $R_1$  and  $L_1$  in agitated solution seem to be  $H_2$

**Table 4** The results of fitting of the impedance spectra obtained at  $C_{M0} = 0$  and  $100$  mM using EECs from Fig. 6:  $S$  is the residual sum of squares and indicate the quality of the fit;  $R_1$  is the solution resistance;  $T_{dl}$  and  $\alpha_{dl}$  are parameters of  $CPE_{dl}$  representing the electrical double layer;  $R_{ct}$  is the charge-transfer resistance; the resistance  $R_2$  and the constant phase element  $CPE_2$  with parameters  $T_2$  and  $\alpha_2$  correspond to adsorption process,  $R_1$  and the inductance  $L_1$  are related to liberation of hydrogen bubbles; uncertainties of the fitted parameters, obtained from Zview, are given in brackets

Conditions	$S$	$R_s \Omega cm^2$	$T_{dl} \mu F s^{a-1} cm^{-2}$	$\alpha_{dl}$	$R_{ct} \Omega cm^2$	$R_1 \Omega cm^2$	$L_1 H cm^2$	$T_2 mF s^{a-1} cm^{-2}$	$\alpha_2$	$R_2 \Omega cm^2$
$C_{M0} = 0$ mM, $\eta = 0$ mV, stagnant solution	0.04	9(1)	829(12)	0.88(0.01)	25(1)	161(18)	2015(452)	84.5(1.6)	0.97(0.02)	12(1)
$C_{M0} = 0$ mM, $\eta = 0$ mV, agitated solution	0.04	9(1)	971(16)	0.87(0.01)	22(1)	88(9)	1236(221)	79.1(1.5)	0.92(0.02)	13(1)
$C_{M0} = 100$ mM, $\eta = 0$ mV, stagnant solution	0.12	8(1)	39(1)	0.86(0.01)	1210(7)	N.A.	N.A.	3549(125)	0.94(0.02)	955(25)
$C_{M0} = 100$ mM, $\eta = +100$ mV, stagnant solution	0.05	7(1)	50(1)	0.83(0.01)	1240(7)	N.A.	N.A.	1572(21)	0.81(0.01)	4076(95)
$C_{M0} = 100$ mM, $\eta = 0$ mV, stagnant solution	0.11	7(1)	66(1)	0.84(0.01)	620(4)	N.A.	N.A.	6589(236)	0.92(0.02)	496(17)
$C_{M0} = 100$ mM, $\eta = -100$ mV, stagnant solution	0.12	7(1)	84(1)	0.85(0.01)	53(1)	945(107)	5720(797)	N.A.	N.A.	N.A.





bubbles' liberation. The inductive loop cannot be solely related to adsorption, as it was proposed on the basis of Cao's model, because agitation does not affect adsorption processes at the stationary state. It has also nothing to do with diffusion because the imaginary part of the impedance related to diffusion is always negative.<sup>27</sup>

Second, the impedance spectra when  $c_{\text{Mo}} = 100$  mM were analysed. These were measured after  $t = 580$  min at the open circuit potential and consist of two capacitive loops (Fig. 6b and c). The first one, with frequency at the maximum apex 5–7 Hz corresponds to the double layer capacitance coupled with the charge transfer resistance. The other one, with frequency at the maximum apex *ca.* 35 mHz, is related to the potential-dependent adsorption process.<sup>47</sup> Adsorbing species are probably heteropolyoxomolybdate or phosphomolybdenum blue.

When the spectrum at OCP was recorded, the electrode was polarised,  $\eta = \pm 100$  mV *vs.* OCP. After the potential achieved the stable value, EIS spectra were recorded (Fig. 6b–d) and fitted using appropriate EECs' (Table 4).

Significant discrepancy between  $T_{\text{dl}}$ ,  $R_{\text{ct}}$ ,  $T_2$  and  $R_2$  fitted from both spectra registered at OCP can be observed. This is related to the corrosion itself, neither to the non-stationarity of the process nor to the fitting, and will be explained further in the text.

Anodic polarisation of the electrode did not significantly affect the double layer capacitance.  $C_{\text{dl}}$  calculated at OCP is between 10 and 16  $\mu\text{F cm}^{-2}$  whereas, at  $\eta = +100$  mV, it equals to 10  $\mu\text{F cm}^{-2}$ . These values are slightly lower than theoretical value of 20  $\mu\text{F cm}^{-2}$ , probably due to adsorption of corrosion inhibitor onto the electrode.  $R_{\text{ct}}$  obtained at OCP is 25–48-fold higher when compared to the solution without heteropolyoxomolybdates due to the same reason. When the electrode was polarised, charge transfer resistance increased only slightly.  $R_{\text{ct}}$  takes into account two electrochemical processes: aluminium oxidation and reduction of heteropolyoxomolybdate to phosphomolybdenum blue. The latter is still possible at the applied overpotential (Fig. 7).

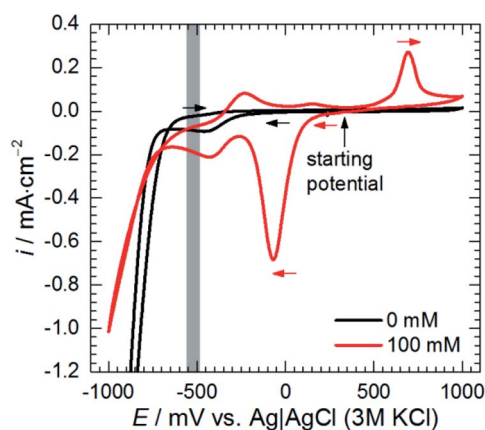


Fig. 7 Cyclic voltammograms of 0.5 M  $\text{H}_3\text{PO}_4$  solutions containing sodium molybdate,  $c_{\text{Mo}} = 0$  and 100 mM, obtained for glassy carbon working electrode at scan rate 20  $\text{mV s}^{-1}$ , grey zone indicates OCP range obtained for  $c_{\text{Mo}} = 100$  mM,  $T = 303$  K.

Anodic polarisation facilitates aluminium oxidation and impedes heteropolyoxomolybdate reduction. If phosphomolybdenum blue species were responsible for corrosion inhibition, aluminium oxidation would be facilitated and  $R_{\text{ct}}$  decrease. Charge transfer resistance, however, remained virtually unchanged. What is more, polarisation resistance, calculated as the sum of  $R_{\text{ct}}$  and  $R_2$ , increased significantly from 2165  $\Omega \text{ cm}^2$  to 5316  $\Omega \text{ cm}^2$ .

This was caused by the increase of  $R_2$  upon electrode's polarisation. It occurs when: (i) increasing electrode's potential causes increase of the adsorption rate, (ii) faradaic current decreases with increasing surface coverage, (iii) charge transfer resistance increases. These also result in decreasing the capacitance contributing to the faradaic impedance in Cao's model.<sup>47</sup> In this work  $\text{CPE}_2$  corresponds to this capacitor and its parameter  $T_2$  indeed decreased. In the light of these results, heteropolyoxomolybdate species can be regarded as the corrosion inhibitor in the studied system. Their reduction to phosphomolybdenum blue is then detrimental because seems to be followed by its desorption and exposition of the metal.

Cathodic polarisation, in turn, resulted in the slight increase of the double layer capacitance to 22  $\mu\text{F cm}^{-2}$ , significant decrease of the charge transfer resistance, disappearance of the low-frequency capacitive loop and appearance of the small, inductive one.  $R_{\text{ct}}$  determined at  $\eta = 0$  and  $-100$  mV takes into account reduction of  $\text{H}_3\text{O}^+$  to  $\text{H}_2$ , heteropolyoxomolybdate to phosphomolybdenum blue and  $\text{O}_2$  to  $\text{H}_2\text{O}$ . Cathodic polarisation facilitates charge transfer in all these cases, thus, significant decrease of  $R_{\text{ct}}$  was obtained when compared to  $\eta = 0$  mV. Reduction of heteropolyoxomolybdate occurs in two, virtually irreversible steps at *ca.*  $-65$  and  $-430$  mV *vs.*  $\text{Ag|AgCl}$  (3 M KCl) reference electrode. Phosphomolybdenum blue species are oxidised during the reverse scan at  $-237$ ,  $+148$  and  $+691$  mV *vs.*  $\text{Ag|AgCl}$  (3 M KCl). These potential values were obtained on the glassy carbon working electrode and may differ in the case of aluminium alloy. Lower value of  $R_{\text{ct}}$  obtained at  $\eta = -100$  mV when compared to  $\eta = +100$  mV means that heteropolyoxomolybdate is the anodic corrosion inhibitor.

Basing on these results the influence of heteropolyoxomolybdate/phosphomolybdenum blue species on the kinetics of hydrogen evolution cannot be determined. Cathodic polarisation facilitates hydrogen evolution, thus, the low-frequency capacitive loop, ascribed to atomic hydrogen adsorption, disappeared. At the same time, a small, inductive loop previously related to the presence of gas bubbles on the surface appeared (Fig. 6d).

The influence of  $c_{\text{Mo}}$  on the impedance spectra obtained at OCP was also studied (Fig. 8). When  $c_{\text{Mo}} = 10$  mM the inductive loop at the lowest frequencies, observed at  $c_{\text{Mo}} = 0$  mM disappeared, because such a concentration of heteropolyoxomolybdate is sufficient to significantly reduce the amount of evolving hydrogen.<sup>15,16</sup> This confirms the aforementioned hypothesis of the nature of the inductive loop. Further increase of  $c_{\text{Mo}}$  causes the increase of the impedance which stays in a good agreement with Fig. 1.

Resistances  $R_{\text{ct}}$  and  $R_2$  increase as the concentration of heteropolyoxomolybdate increases, whereas  $T_2$  decreases. As it was



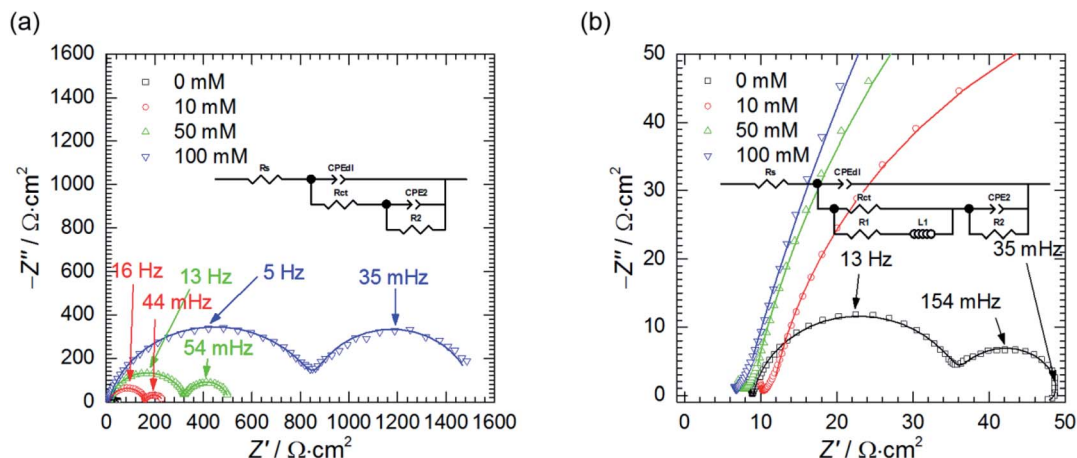


Fig. 8 Selected impedance spectra of 7075 aluminium alloy obtained at  $\eta = 0$  mV, in the stagnant solution, as a function of  $c_{\text{Mo}}$  (empty markers) fitted using the EEC, (continuous lines) (a) and their magnified high frequency parts with EEC used for fitting when  $c_{\text{Mo}} = 0$  mM (b);  $0.5 \text{ M H}_3\text{PO}_4$ ,  $T = 303 \text{ K}$ ,  $t = 580 \text{ min}$ .

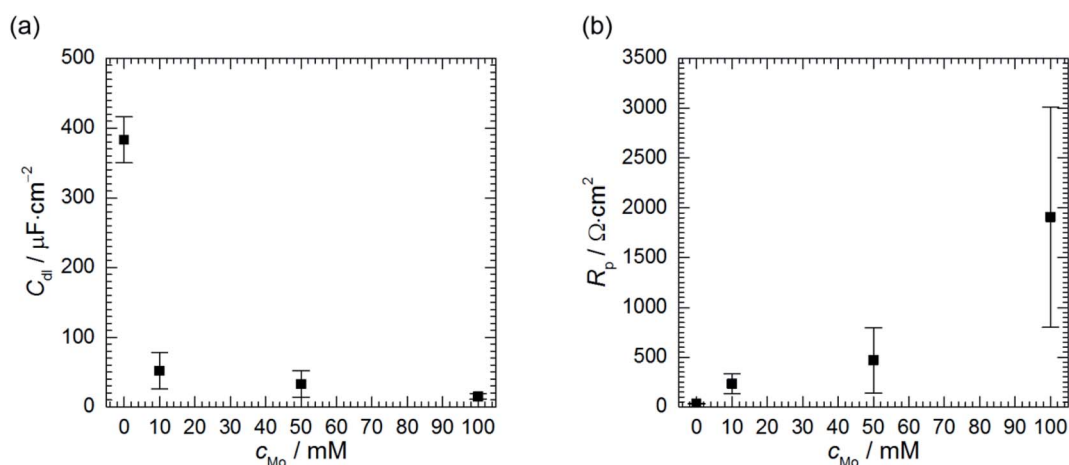


Fig. 9 Double layer capacitance (a) and polarisation resistance (b) as a function of  $c_{\text{Mo}}$ ,  $0.5 \text{ M H}_3\text{PO}_4$ ,  $T = 303 \text{ K}$ ,  $t = 580 \text{ min}$ .

already discussed, such a behaviour is related to increase of the charge transfer resistance, which was clearly observed, and decrease of the faradaic current caused by increasing surface coverage.<sup>47</sup>

Double layer capacitance decreases as  $c_{\text{Mo}}$  increases from  $383 \pm 8 \mu\text{F cm}^{-2}$  to  $15 \pm 4 \mu\text{F cm}^{-2}$  (Fig. 9a). The former, relatively high value, is related to high surface area of the

electrode after corrosion process. This decreases with increasing inhibitor concentration to the values typical for double layer capacitance of the metallic electrodes.

Corrosion rate is directly related to the polarisation resistance  $R_p$ , which is defined as the faradaic impedance when  $\omega \rightarrow 0$  Hz. It was calculated using eqn (6) when  $c_{\text{Mo}} = 0$  mM and eqn (7) when  $c_{\text{Mo}} > 0$  mM (Fig. 9b):

**Table 5** The averaged results of fitting of the impedance spectra obtained as a function of  $c_{\text{Mo}}$  using EECs from Fig. 8:  $S$  is the residual sum of squares and indicate the quality of the fit;  $R_s$  is the solution resistance;  $T_{\text{dl}}$  and  $\alpha_{\text{dl}}$  are parameters of  $\text{CPE}_{\text{dl}}$  representing the electrical double layer;  $R_{\text{ct}}$  is the charge-transfer resistance; the resistance  $R_2$  and the constant phase element  $\text{CPE}_2$  with parameters  $T_2$  and  $\alpha_2$  correspond to adsorption process, either heteropolyoxomolybdate or atomic hydrogen,  $R_1$  and  $L_1$  are related to liberation of hydrogen bubbles, uncertainties of the fitted parameters were calculated using eqn (3),  $n$  is the number of experiments

$c_{\text{Mo}}$ mM	$n$	$R_s$ $\Omega \text{ cm}^2$	$T_{\text{dl}}$ $\mu\text{F s}^{\alpha-1} \cdot \text{cm}^{-2}$	$\alpha_{\text{dl}}$	$R_{\text{ct}}$ $\Omega \text{ cm}^2$	$R_1$ $\Omega \text{ cm}^2$	$L_1$ H $\text{cm}^2$	$T_2$ mF $\text{s}^{\alpha-1} \cdot \text{cm}^{-2}$	$\alpha_2$	$R_2$ $\Omega \text{ cm}^2$
0	3	9(1)	739(269)	0.89(0.04)	26(3)	219(170)	2505(2679)	110(101)	0.99(0.04)	11(5)
10	4	11(2)	122(61)	0.89(0.01)	165(74)			55(25)	0.98(0.05)	68(27)
50	4	8(1)	91(52)	0.88(0.01)	266(190)			24(20)	0.98(0.06)	147(140)
100	6	7(1)	56(19)	0.85(0.01)	1000(621)			6(4)	0.92(0.04)	907(795)



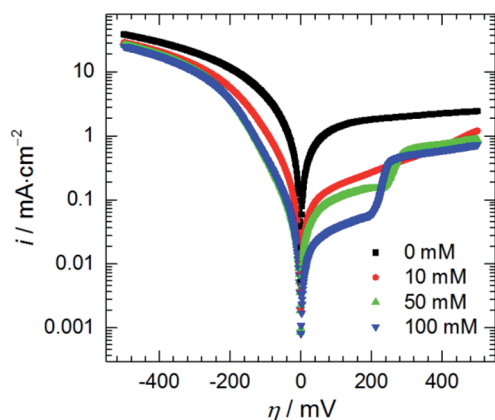


Fig. 10 Anodic and cathodic polarisation curves as a function of initial concentration of heteropolyoxomolybdate species, 0.5 M  $\text{H}_3\text{PO}_4$ ,  $T = 303\text{ K}$ , scan rate  $15\text{ mV min}^{-1}$ .

$$R_p = \frac{R_{ct}R_1}{R_{ct} + R_1} + R_2 \quad (6)$$

$$R_p = R_{ct} + R_2 \quad (7)$$

Polarisation resistance increases with increasing concentration of heteropolyoxomolybdate species. It is interesting to observe that its uncertainty increases as the  $R_p$  increases and is high at  $c_{\text{Mo}} = 100\text{ mM}$ . Relatively high uncertainties were also observed for  $R_{ct}$ ,  $R_2$  and  $T_2$  when  $c_{\text{Mo}} > 10\text{ mM}$  (Table 5). Evans explained that such a behaviour is related to the surface area of the specimen. When it is relatively small, decreasing corrosion rate causes a significant increase of the discrepancies between independent measurements.<sup>48</sup> This was not observed in Fig. 1 because the surface area of the specimens was 2-fold higher when compared to the electrodes prepared for electrochemical tests.

**3.4.3. Linear sweep voltammetry.** Cathodic and anodic polarisation curves were measured independently, starting from the open circuit potential, as a function of initial concentration of heteropolyoxomolybdate (Fig. 10). Tafel constants for anodic and cathodic processes were not determined, because the linear parts of the polarisation curves were not clearly visible. Such a behaviour is frequently observed for anodic curves. Lack of the linear region in cathodic curves is probably related to more than one cathodic reaction. Cathodic current density decreases as the  $c_{\text{Mo}}$  increases. This occurred despite heteropolyoxomolybdate species are reduced to phosphomolybdenum blue *i.e.* behave as additional depolariser in the corrosion cell. This means that cathodic sites in the matrix *i.e.*  $\text{Al}_7\text{Cu}_2\text{Fe}$  and  $\text{Al}_{23}\text{CuFe}_4$  particles are blocked to some extent. Indeed, presence of Mo, P and O in the vicinity of these intermetallics was confirmed. This effect, beneficial for the corrosion protection, may depend on the chemical composition of the intermetallic particles behaving as the local cathodes, and their surface area.  $\text{Al}_2\text{Cu}$ , for instance, can efficiently reduce heteropolyoxomolybdate to phosphomolybdenum blue. Since no protective film is formed in this case, heteropolyoxomolybdate

act as additional depolariser in the corrosion cell causing selective corrosion of the intermetallic, when it is not coupled with the matrix.<sup>45</sup> Thus, the influence of plastic deformation and heat treatment of the alloy may be important for inhibition efficiency in  $\text{H}_3\text{PO}_4$ – $\text{Na}_2\text{MoO}_4$  system. This issue will not be further discussed here.

Adsorption of heteropolyoxomolybdate species caused significant decrease of the anodic current density. This confirms that heteropolyoxomolybdate is anodic inhibitor. When  $c_{\text{Mo}} \geq 50\text{ mM}$ , sharp increase of current density around  $\eta = 200\text{ mV}$  occurred. This corresponds to oxidation peak of phosphomolybdenum blue at  $-237\text{ mV vs. Ag|AgCl|3 M KCl}$ .

## 4. Conclusions

Sodium molybdate, when dissolved in orthophosphoric acid aqueous solution forms heteropolyoxomolybdate species. They significantly decrease the corrosion rate of 7075 alloy from  $75.98$  to  $3.24\text{ g per m}^2$  per day. Obtained results suggest that even higher inhibition efficiency could be obtained at the higher concentration of sodium molybdate. The influence of temperature on the corrosion rate and inhibition efficiency of 7075 alloy should be further studied.

The mechanism of corrosion inhibition in  $\text{Na}_2\text{MoO}_4$ – $\text{H}_3\text{PO}_4$ –Al system was established. Heteropolyoxomolybdate species adsorb on the surface of the alloy and hamper aluminium oxidation process. This manifests as a significant increase of the charge transfer resistance and polarisation resistance. Anodic polarisation, at certain range of potential, facilitates the adsorption of heteropolyoxomolybdate. When its reduction to phosphomolybdenum blue is hampered, higher inhibition efficiency can be obtained. It was shown that trenching around  $\text{Al}_7\text{Cu}_2\text{Fe}$  and  $\text{Al}_{23}\text{CuFe}_4$  intermetallic particles, that are more noble than the matrix, does not occur at sufficiently high initial concentration of  $\text{Na}_2\text{MoO}_4$ . At the same time, heteropolyoxomolybdate inhibits cathodic process, but much weaker when compared to the anodic one. This is probably achieved due to precipitation of an insoluble salt, containing Mo, P and O, onto intermetallic particles.

## Conflicts of interest

There are no conflicts to declare.

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